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Densities of Alcohols

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Edited by K.R. Hall and K.N. Marsh



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## Preface

Critically evaluated experimental data covering the densities of organic compounds is essential for both scientific and industrial applications. Knowledge of densities is important in many areas, including custody transfer of materials, product specification, development of various predictive methods, and for characterizing compounds and estimating their purity.

Various compilations of densities for organic compounds have been published. The early Landolt-Börnstein compilation [23-ano] contained recommended values at specific temperatures. International Critical Tables [28-ano-1] provided recommended densities at 0 °C and values of constants for either a second or third order polynomial equation to represent densities as a function of temperature. This compilation also gave the range of validity of the equation and the limits of uncertainty, references used in the evaluation and those not considered. This compilation is one of the most comprehensive ever published. Timmermans [50-tim, 65-tim], Dreisbach [55-dre, 59-dre, 61-dre] and Landolt-Börnstein [71-ano] published additional compilations, primarily of experimental data. These compilations contained experimental data along with reference sources but no estimates of uncertainty for the data nor recommended values.

The Thermodynamics Research Center has published recommended values for the densities of organic compounds since 1942 in its two loose leaf publications: TRC Thermodynamic Tables - Hydrocarbons and Non-Hydrocarbons. These compilations are updated with four supplements per year. References to the literature values used in the selection and those not used in the selection appear in the references for each table. The accuracy of the values is apparent from the number of significant figures provided. More recently, the Design Institute of Physical Property Data, Project 801 has assembled a set of recommended equations for the densities of over 1500 compounds [89-dau/dan, 91-dau/dan, 92-dau/dan, 93-dau/dan, 94-dau/dan, 95-dau/dan, 96-daudan, 97-daudan]. Densities are represented by an equation fit to selected values from the freezing temperature to the critical temperature. References to sources of data used in the evaluation and those not used are given along with a quality assessment. In many cases, the equation does not fit density values at intermediate temperatures, especially at 293.15 K and 298.15 K, within the experimental uncertainty. Thus, the equation is not useful for purity comparisons, custody transfer, or product specification when the highest accuracy is required. Smith and Srivastava [86-smi/sri, 86-smi/sri-1] recently have published a compilation (in two volumes) which contains recommended values in tabular form as well as equations with statistical information regarding the fit. However, this compilation contains no indication of data quality or uncertainties.

The present volume contains densities for non-cyclic alcohols including monoalcohols, diols, and triols both fully saturated and with various extents of unsaturation which have been collected from the literature published from 1870 to early 1999. The various compilations listed above also have been consulted for sources of original data. This volume continues our effort in evaluation of the densities of organic compounds [see volume IV/8B [96-wil/mar] for the densities of alkanes, volume IV/8C [96-wil/mar-1] for the densities of alkenes, alkynes and alkadienes, volume IV/8D [97-wil/hon] for the densities of monocyclic non-aromatic hydrocarbons, volume IV/8E [98-wil/hon] for the densities of aromatic hydrocarbons, volume IV/8F [99-wil/hon] for the densities of polycyclic hydrocarbons]. All experimental density values have been evaluated critically and assigned numerical uncertainties individually. These assessments have been used to derive an equation to fit the data and to obtain recommended values with uncertainties. Detailed evaluation procedures appear in Chapter 1. Algorithms for the automatic selection of data used in the fit and for the selection of the type of equation and order of polynomial have been developed. The algorithms depend upon the assigned uncertainties, the distribution of density values over the experimental temperature range, and the magnitude and distribution of differences between observed and smoothed values. These algorithms can fit any kind of data to a function of independent variables. We have collected data for 829 compounds, consisting of data sets drawn from 1119 sources.

The volume contains six chapters; a list of references, and two indexes (Chemical Abstracts Service Registry Number Index and Chemical Name Index). Chapter 1 contains: a short introduction; a description of the tables; a detailed description of the methods used in the evaluation, selection and smoothing process; a glossary of symbols and a description of the order of compounds in the Tables used. Chapter 2 covers the monoalcohols, Chapter 3 contains the data for diols, and Chapter 4 has the triols. The tables contain the original literature data along with their estimated uncertainties and the evaluated data in both numerical form and as coefficients to equations with selected statistical information. When data cover a sufficient temperature range, graphical plots of the deviations of the experimental data from the recommended equation are given. The chemical name index contains the IUPAC names for the compounds, as well as alternate names that often appear in practice.

This volume should be useful to a wide community of researchers, data specialists, and engineers working in the field of physical and organic chemistry, chemical engineering, material science, environmental chemistry, chemical aspects of energy technology, and those engaged in the development of new predictive procedures. The book should also be of use to students and faculty in Chemistry and Chemical Engineering departments at universities as a reference book of evaluated thermophysical properties.

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College Station, June 1999

M. Frenkel, X. Hong, R.C. Wilhoit, K.R. Hall

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# 1 Introduction

## 1.1 Basic Concepts

The mass density of a substance is an intensive quantity defined by:

$$\rho = m/v \quad (1.1)$$

where  $m$  is the mass and  $v$  is the volume of the sample. Both these quantities are extensive quantities. Other densities often referred to in the literature are the relative density and the molar density. Relative density, also called specific gravity, is:

$$\rho_r = \rho/\rho_0 \quad (1.2)$$

where  $\rho_0$  is the density of a standard substance. It is necessary to specify the conditions of temperature and pressure for the standard substance. The most common reference material is water often at the temperature of its maximum density, 4 °C, at atmospheric pressure. The molar density is defined as

$$\rho_m = 1/V \quad (1.3)$$

where  $V$  is the volume occupied by one mole of the substance. The only densities reported in this volume are the mass densities; relative and molar densities have been converted to mass densities, and all densities have been reported in SI units. If the mass,  $m$ , in equation (1.1) has not been corrected for air buoyancy it gives the apparent density in air. The API specific gravity is:  $\rho(\text{API}) = 141.5/\rho_r - 131.5$ , in which  $\rho_r$  is  $\rho(288.68 \text{ K})/\rho_0(288.68 \text{ K})$ , and the standard substance is water at 288.68 K (60 °F).

The density of a material is a function of temperature and pressure but its value at some standard condition (for example, 293.15 K or 298.15 K at either atmospheric pressure or at the vapor pressure of the compound) often is used to characterize a compound and to ascertain its purity. Accurate density measurements as a function of temperature are important for custody transfer of materials when the volume of the material transferred at a specific temperature is known but contracts specify the mass of material transferred. Engineering applications utilize the density of a substance widely, frequently for the efficient design and safe operation of chemical plants and equipment. The density and the vapor pressure are the most often-quoted properties of a substance, and the properties most often required for prediction of other properties of the substance. In this volume, we do not report the density of gases, but rather the densities of solids as a function of temperature at atmospheric pressure and the densities of liquids either at atmospheric pressure or along the saturation line up to the critical temperature.

The purpose of this compilation is to tabulate the densities of compounds, hence only minimal description of experimental methods used to measure the density of liquids or solids appears. Detailed descriptions of methods for density determination of solids, liquids and gases, along with appropriate density reference standards, appear in a chapter by Davis and Koch in *Physical Methods of Chemistry*, Volume VI, Determination of Thermodynamic Properties [86-ros/bae].

The two principal experimental apparatuses used to determine the density of a liquid are: the pycnometer and the vibrating tube densimeter. The pycnometer method involves measuring the mass of a liquid in a vessel of known volume. The volume of the pycnometer, either at the temperature of measurement or at some reference temperature, is determined using a density standard, usually water or mercury. Using considerable care and a precision analytical balance accurate to  $\pm 10^{-5}$  g, it is possible to achieve densities accurate to a few parts in  $10^6$  with a pycnometer having a volume of 25 cm<sup>3</sup> to 50 cm<sup>3</sup>.



It is common to achieve accuracies of 1 part in  $10^5$  in using equation (1.1) with pycnometers as small as  $5 \text{ cm}^3$  and routine measurements can achieve 1 part in  $10^4$ . However the main sources of error in assigning density to a particular compound in a particular state arise from factors other than the measurement of mass and volume. See Section 1.4.1

The vibrating tube densimeter relies upon the fact that the frequency  $f$  of vibration for a U or V shaped tube depends upon the mass of material in the tube:

$$\rho = A / f^2 + B \quad (1.4)$$

Calibration of the apparatus is necessary; usually water and air or nitrogen are the reference materials. Vibrating tube densimeters designed to operate close to atmospheric pressure can achieve repeatability of parts in  $10^6$ . If the reciprocal of the frequency is linear in density, accuracies of 1 part in  $10^5$  are readily achievable.

The principal experimental method used to measure the density of a solid is determination of the mass of liquid displaced by a known mass of solid. It is essential that the solid have no appreciable solubility in the liquid, that all occluded air be removed from the solid and that the density of the displacement fluid be less than that of the solid lest the solid float. Densities of crystalline solids also can be determined from the dimensions of the unit cell. Davis and Koch discuss other methods for measuring the density of liquids and solids such as: hydrostatic weighing of a buoy and flotation methods.

## 1.2 Scope of the Compilation

Volume IV/8G presents observed values for the densities of non-cyclic alcohols. These values represent a compilation and evaluation of data from the scientific literature covering approximately the past 100 years. The values presented come from the TRC Source Database. The Thermodynamics Research Center has assembled these data over a period of years and has used them to provide the evaluated density values listed in the TRC Thermodynamic Tables - Non-Hydrocarbons. An additional literature search has been performed immediately before producing this compilation to locate new or missing data and to bring the collection up-to-date. This compilation should include at least 90% of the pertinent data reported in the literature. The usual experimental conditions are in contact with air at one atmosphere below the normal boiling point, and in equilibrium with the vapor phase above the normal boiling point. In the summary tables, temperatures reported on the Kelvin scale have been obtained by adding 273.15 to temperatures originally given on the Celsius scale.

Densities have units of kilograms per cubic meter ( $\text{kg}\cdot\text{m}^{-3}$ ). Values reported in units of grams per milliliter, where the liter is "the volume of one kilogram of water at its temperature of maximum density" convert to  $\text{kg}\cdot\text{m}^{-3}$  when multiplied by 999.972 (as defined by the 12th General Conference of the International Committee on Weights and Measure, 1964). Values of specific gravity relative to water at a stated reference temperature become density upon multiplication by the accepted density of water at the reference temperature. Most reported densities for liquids below the boiling point apply to the air-saturated liquid.

Compounds are identified by an IUPAC approved name [93-ano-1], the empirical molecular formula, and the Chemical Abstracts Service Registry Number. A summary table is available for each compound which includes the reported temperature and density values, an assigned uncertainty for the density, the difference between the observed and smoothed density values and an index key to the source of the data. A complete list of references, identified by the index keys, appears at the end of the volume.

Where appropriate, tables of smoothed, recommended values are given at integral multiples of 10 K over the experimental range of temperatures. Values at 293.15 K and 298.15 K are included when they are in the range of the original data set. The recommended values also have assigned uncertainties.

## 1.3 Description of Data Tables

Data for a particular compound are selected, evaluated and smoothed in one of four ways, depending upon the number and accuracy of the reported values and upon their distribution over the temperature range.

**Case 1.** When the data set consists of at least four acceptable, effectively distinct values (see section 1.5.3), the densities in selected subsets are fit to a function of temperature using the least squares criterion. A summary table for the selected set gives the densities, their estimated uncertainties, the deviations between observed and calculated values, an index key to the list of references and a plotting symbol. If sufficient space remains, some data outside the selected set also are included in the summary table along with reference keys to any remaining data. A plot of the deviations between observed and calculated values is shown for the selected subset. Error bars indicate the size of the estimated uncertainties for the data. Distinct plotting symbols identify the five data sources that have the smallest average estimated uncertainties. A single symbol represents all remaining data in the selected set. A table consisting of smoothed, recommended values (calculated from the fitted functions) is also given. Estimated uncertainties are given for the recommended values which also appear as a continuous line on the deviation plot. Densities of crystal phases are in a separate section of the table. In most cases, these densities have not been fit as a function of temperature. Values of parameters, statistical measures of the fit, and references to sources of critical constants appear at the beginning of these sections.

**Case 2.** For data sets that do not meet the criteria of Case 1, but contain acceptable values over a temperature range of at least two degrees, the results are smoothed using a linear function of temperature with an estimated coefficient of thermal expansion. A table of smoothed recommended values is presented.

**Case 3.** For data sets that do not meet the criteria of either Case 1 or 2 but contain two or more values at a single temperature, a recommended value is given for this temperature by taking a weighted average of the observed values.

**Case 4.** For data sets that contain only single values at one or two temperatures, the reported values are given rather than recommended values.

## 1.4 Evaluation, Selection and Smoothing of Data

### 1.4.1 Assignment of Uncertainties

The Thermodynamics Research Center staff have assigned an uncertainty value to each observed and recommended density value listed in the tables. The true value of the property has a 95% probability of being in the range covered by + or – the uncertainty about the reported value. Assignment of uncertainty is a subjective evaluation based upon what is known about the measurement when the value is entered into the database, and includes the effects of all sources of experimental error. The errors have been propagated to the listed density at the reported temperature. Uncertainties reported by the investigators are considered but not necessarily adopted. Often, investigators report repeatability, but they usually do not provide uncertainty.

Errors in density result from errors in temperature measurement or control; calibration of instruments; transfer, handling and weighing of samples; and impurities in the samples. At temperatures well below the critical temperature and near room temperature, standard techniques easily achieve accuracies of  $\pm 0.05\%$ . For the compounds in this compilation, that level corresponds to about  $\pm 0.4 \text{ kg}\cdot\text{m}^{-3}$ . Under these conditions, errors in temperature are not very significant. This level of accuracy only requires

temperatures to be known within  $\pm 0.5$  K. At temperatures approaching the critical temperature, measurements become more demanding because of the rapid increase in the magnitude of the coefficient of thermal expansion. Greater accuracy, in general, requires careful attention to calibration, mass determination and sample handling techniques. It is assumed that values obtained by pycnometers have been corrected for buoyancy of air, unless the author specifically says otherwise. This correction increases the apparent density by 0.05 - 0.1%. When this correction has not been made, the estimated uncertainty is greater.

Most measurements of densities of liquids below their normal boiling points are made in the presence of air. Densities reported here refer to liquids in equilibrium with a gas phase consisting of a mixture of air and vapor at a total pressure of one atmosphere below the normal boiling point and of vapor at the equilibrium vapor pressure above the boiling point. Thus air is not regarded as an impurity.

A major source of error in most measurements is the presence of impurities in the sample. The effect of an impurity depends upon its amount in the sample and upon the difference between its density and the density of the principal constituent. Even when the sample purity is provided quantitatively, the impurities often are not identified individually. Nevertheless, a report of sample purity reduces the estimated uncertainty because it can be taken as evidence that the investigator has considered sample purity. The most ubiquitous impurity in liquids is water, and, because its density differs significantly from those of hydrocarbons, it is a common source of error. Exclusion of water requires that the sample be protected from the atmosphere during transfer, and that special precautions be taken to remove the sample from containers.

### 1.4.2 Quantitative Effect of Impurity on Density of Liquids

The molar volume of a mixture of components,  $V$ , in terms of the mole fractions  $x_i$  and partial molar volumes of the components  $V_i$  is:

$$V = \sum_{i=1}^c x_i V_i \quad (1.5)$$

For an ideal solution, the partial molal volumes equal the molar volumes of the pure liquid components. Denoting component the main components as 1 and the impurities as  $> 1$ , the volume becomes:

$$V = x_1 V_1 + \sum_{i=2}^c x_i V_i \quad (1.6)$$

Then using,

$$\rho = M / V \quad (1.7)$$

and the molar mass of the mixture:

$$M = \sum_{i=1}^c x_i M_i \quad (1.8)$$

and assuming that the  $x_i$  are small for  $i > 1$ , then

$$\rho = \frac{\rho_1}{w_1} \left( 1 - \rho_1 \sum_{i=2}^c w_i v_i \right) \quad (1.9)$$

where  $v_i = V_i / M_i$  are partial specific volumes of the impurities and  $w_i$  is the mass fraction of component  $i$ . Finally, the density of the mixture is related to the density of the main component and the impurities  $i$  by:

$$\rho = \frac{\rho_1}{w_1} \left( 1 - \rho_1 \sum_{i=2}^c \frac{w_i}{\rho_i} \right) \quad (1.10)$$

The observed value of the density of a sample is sometimes presented as evidence of its purity. Assuming the sample contains a single impurity, equation (1.10) can be solved for  $\rho - \rho_1$ :

$$\rho - \rho_1 = \rho_1(1 - w_1 - \rho_1 w_2 / \rho_2) / w_1 \quad (1.11)$$

### 1.4.3 Procedure for Selection and Smoothing of Density Values - Case 1

A selected subset of the reported densities is fit to functions of temperature using the least squares criterion. Up to a boundary temperature  $T_b$  (approximately  $0.8T_c$ ), the calculated density  $\rho_x$  is represented by a polynomial in temperature with coefficients  $a_k$  of order  $p$ ,

$$\rho_x = \sum_{k=0}^p a_k T^k. \quad (1.12)$$

Above  $T_b$  the smoothed values are given by a modification of the Guggenheim equation [67-gug]

$$\rho_x = \left(1 + 1.75\theta + 0.75\theta^3\right) \left[ \rho_c + b_1(T_c - T) + b_2(T_c - T)^2 + b_3(T_c - T)^3 + b_4(T_c - T)^4 \right] \quad (1.13)$$

where  $T_c$  is the critical temperature and  $\theta = (1 - T/T_c)^{1/3}$ . Selected values of critical constants are constant. Continuity with equation (1.12) results from forcing the two functions and their first derivatives with respect to temperature to be equal at the boundary. When no values are available above this temperature, only the polynomial is used.

The following steps, implemented by a computer program written in C, generate the smoothed, recommended values. Input to the program consists of the set of observed density values, temperatures, estimated uncertainties, critical constants and values of certain parameters used by the program.

**Step 1.** Separate the initial data into two sets, corresponding to temperatures above and below  $T_b$ .

**Step 2.** Make an initial selection from the low temperature set by rejecting all points with zero uncertainty and all points with uncertainties above a limit determined by the data selection algorithm described in section 1.5.2. Zero uncertainties are assigned to values that are not experimental and are included for comparison only (these are most often values recommended in other compilations).

**Step 3.** Determine the effective number of data values,  $n_e$ , as described in 1.5.3. If the effective number of values is less than four, terminate the calculation. If the total number of values is more than eight and the effective number is greater than or equal to four but less than eight, make another initial data selection with relaxed selection criteria.

**Step 4.** For the  $j$ -th value in the set calculate normalized values,  $\rho_{n,j}$  and  $T_{n,j}$ , and weighting factors,  $w_j = 1/u_j^2$  where  $u_j$  is the uncertainty assigned to the  $j$ -th observed density and  $\rho_{n,j} = \rho_j - \bar{\rho}$  where  $\bar{\rho}$  is the mean value of the observed density in the set. and  $T_{n,j} = T^k - \bar{T}^k$  where  $\bar{T}^k$  is the mean value of the  $T_j^k$  value in the set..

**Step 5.** Using  $\rho_n = a_1 T_n$ , fit the data subject to least squares with points weighted by  $w_j$ .

**Step 6.** Calculate the standard deviation  $\sigma$  for this fit. Eliminate any points from this set for which  $|\delta_j| > 3.5\sigma$ , where  $\delta_j = \rho_j - \rho_{x,j}$ .

**Step 7.** Fit the remaining normalized values to a series of polynomials,  $\rho_n = \sum a_k T^k$ , starting with order 1 and increasing in order. Use  $w_j$  as weighting factors and stop increasing the order when satisfying one of the following conditions:

1. A value of  $p$  given as an input parameter to the program is reached, or
2.  $\chi_k^2 < 1.1[1 + 1 / (n - k)]^2 \chi_{k-1}^2$  (see glossary of symbols) and the deviations pass the random deviation test (see 1.5.4).

**Step 8.** If any points have  $|\delta_j| > 2.2\sigma$  for the final polynomial, eliminate these points and repeat step 7.

**Step 9.** Calculate parameter  $a_0$ .

**Step 10.** Apply the initial data selection described in step 2 to the high temperature data set.

**Step 11.** Fit the selected high temperature data with the modified Guggenheim equation using least squares with weighting factors  $w_j$ .

**Step 12.** The following procedure provides continuity at the boundary. Set equation (1.13) and its first derivative at  $T_b$  equal to the corresponding values from equation (1.12) at  $T_b$ . Eliminate parameters  $b_3$  and  $b_4$  from these two simultaneous equations to obtain a function containing parameters  $b_1$  and  $b_2$  which can be evaluated for the high temperature range using least squares. Do not use densities at temperatures within 2 K of the critical temperature.

**Step 13.** Generate the output table of temperature, observed densities, estimated uncertainties, and difference between observed and calculated densities and arrange it in order of year of publication with authors. For data from a particular source, arrange in order of temperature.

**Step 14.** Calculate the table of smoothed and recommended values with their corresponding estimated uncertainties.

Coefficients  $A, B, C, D$  and  $E$  listed in the heading of Table 1 for each compound correspond to  $a_0, a_1, a_2, a_3$  and  $a_4$  in equation (1.12) for temperatures below  $T_b$ .  $\sigma_i$  is the weighted standard deviation for individual points in this region (see the glossary). If the data set includes values above  $T_b$ , the coefficients  $A, B, C$  and  $D$  correspond to  $b_1, b_2, b_3$  and  $b_4$  in equation (1.13) for this range. The weighted standard deviation,  $\sigma_{c,w}$ , and the unweighted standard deviation for the fit,  $\sigma_{c,uw}$ , include both ranges. If the data set covers only values below  $T_b$  then  $\sigma_{c,w}$  and  $\sigma_{c,uw}$  represent that range only.

The uncertainty in the smoothed values depends upon the uncertainties in the original observed values and upon the magnitude of deviations between observed and calculated values. To approximate the contribution of these two effects at the temperature  $T$ , the uncertainties  $u_x(T)$  for the low temperature range are calculated from:

$$u_x(T) = \left[ u(T)^2 + \sum_k \sum_l C_{kl} (T^k - \bar{T}^k)(T^l - \bar{T}^l) \right]^{1/2}. \quad (1.14)$$

In this equation,  $u(T)$  represents the uncertainty of the observed data in the vicinity of  $T$  and is approximated by fitting a polynomial of order 1-3 to the estimated uncertainties as a function of temperature (other symbols appear in the glossary). Uncertainties in the smoothed data for the high temperature range are calculated using:

$$u_x(T) = \left[ u_x(T_b)^2 + h(T)^{-2} \right]^{1/2}, \quad (1.15)$$

where  $u_x(T_b)$  is the uncertainty calculated using equation (1.14) for the low temperature range at the boundary temperature  $T_b$  and  $h(T)$  is a polynomial in temperature fit to the reciprocals of the estimated uncertainties in the high temperature region.

The uncertainties in extrapolated data should increase as the extent of extrapolation increases. Since equation (1.15) does not always give this result, manual adjustment is sometime required in this range.

### 1.4.4 Procedure for Selection and Smoothing of Density Values - Case 2

When the data set for a particular compound satisfies the criteria for Case 2, it is smoothed by a linear function of temperature,

$$\rho_x = a_0 + a_1 T. \quad (1.16)$$

The coefficient  $a_1$  is either calculated from two densities of sufficient accuracy reported at different temperatures, preferably by the same investigator, or estimated by examination of the coefficient of expansion of similar compounds obtained from a least squares calculation. The constant term then results from equation (1.17) after eliminating values with large uncertainties

$$a_0 = \sum w_j (\rho_j - a_1 T_j) / \sum w_j. \quad (1.17)$$

The uncertainties for the smoothed values are:

$$u_x(T) = [\sigma_0^2 + \sigma_1^2 (T - \bar{T})^2]^2, \quad (1.18)$$

where  $\bar{T}$  is the weighted mean temperature for the accepted set,  $\sigma_0^2 = (\sum w_j \delta_j^2) / \sum w_j$  and  $\sigma_1$  is the estimated standard deviation of  $a_1$ .

### 1.4.5 Procedure for Selection and Smoothing of Density Values - Case 3

The recommended density at a particular temperature is the weighted mean observed density for that temperature. The corresponding uncertainty is the standard deviation from the mean for each value.

## 1.5 Calculation Procedures

### 1.5.1 Least Squares Calculation

Parameters of all the smoothing functions are adjusted to minimize the function

$$\chi^2 = \sum w_j \delta_j^2 \quad (1.19)$$

by the singular value decomposition of the matrix of independent variables of the function. The parameters are calculated by functions **svdcmp** and **svbksb** described in [88-pre/fla] modified to accept weighting factors. The covariance matrix used in equation (1.14) is calculated by the function **covar** from the same book.

### 1.5.2 Selection of Data Based upon Estimated Uncertainties

The selection procedure is:

**Step 1.** Obtain  $\Delta T$ , the range of temperatures covered by the data set.

**Step 2.** For each density value,  $\rho_j$ , in the set, calculate,

$$x_{jl} = \exp(q|T_j - T_l|) \quad (1.20)$$

$$z_l = \sum_{l \neq j} x_{jl} \quad (1.21)$$

$$z_2 = \sum_{l \neq j} u_l x_{jl} \quad (1.22)$$

$$y = u_j z_1^{1.5} z_2^{-1} \quad (1.23)$$

Accept point  $j$  if  $y \leq d$ ; reject it otherwise.

**Step 3.** Repeat steps 1 and 2 with points accepted in the first pass.

The accepted points are those that remain from Step 3. The constants  $q$  and  $d$  are:

$$q = -2.628g_1 \left[ 1 + (\Delta T / 30)^2 \right] / \Delta T$$

$$d = g_2 / \log_{10}(1+n).$$

The number  $z_2 / z_1$  is a weighted mean of all points in the set other than the  $j$ -th point. The weighting factor decreases exponentially with the difference in temperature of the  $l$ -th point from the  $j$ -th point. The parameter  $g_1$  determines the rate of decrease. This procedure compares the uncertainty of the  $j$ -th point to the weighted mean of other points. The parameter  $g_2$  determines the rejection level from this comparison for the  $j$ -th point. Larger values of  $g_2$  are less selective. Values for  $g_1$  and  $g_2$  are supplied to the algorithm. For all cases  $g_1$  is in the range of 1 to 2 (usually 1.8). The value of  $g_2$  is in the range of 2 to 3 ( $\text{kg}\cdot\text{m}^{-3}$ ) (usually 2.5).

### 1.5.3 Count the Effective Number of Density Values in a Set

The number of degrees of freedom in a least squares fit is the number of distinct data values minus the number of adjustable parameters. To obtain a meaningful smoothing of data, the order of the polynomial function is limited to values which gives three or more degrees of freedom. However, if two or more density values in the set are at the same (or nearly the same) temperature, they should count as only one point in calculating the degrees of freedom. In general, the effective number of density values minus the number of fitting parameters is used as the degrees of freedom. Effective data values are those that are separated by at least 1.2 K.

### 1.5.4 Testing a Set of Deviations between Observed and Calculated Density Values for a Random Distribution

One of the criteria for acceptance of the order of a polynomial least squares fit is that the deviations between calculated and random values be distributed “randomly” over the range of conditions covered by the data. The concept of randomness for this purpose probably cannot be defined rigorously. However, the following test for randomness is used whenever the original data set contains seven or more values.

**Step 1.** Sort the values in order of increasing temperature

**Step 2.** Separate the total range of temperature,  $\Delta T$ , into  $s$  subranges each of size  $\Delta T/s$ . Form  $s$  subsets of data corresponding to these temperature subranges.

**Step 3.** Make the following comparison for each subset  $j$  which has at least four members.

$$0.01 < \frac{\sum |\delta_j|}{n_s} \quad \text{and} \quad 0.2 < \frac{|\sum \delta_j|}{\sum |\delta_j|}.$$

If both comparisons are true for any subset, the test for randomness fails.

**Step 4.** Apply steps 2 and 3 to the data for  $s$  from 2 to an upper limit. The upper limit is determined by the number of values in the original set according to the following table.

$n$ , number of values in original set	maximum number of subsets
7 to 10	2
11 to 20	3
21 to 33	4
> 33	5

## 1.6 Glossary of Symbols

$a_k$	parameters in the polynomial function for densities at temperatures $\leq T_b$
$b_k$	$k$ -th parameter in modified Guggenheim equation for density at temperatures $> T_b$
$g_1, g_2$	parameters used in the data selection algorithm
$n$	number of accepted values of density in a set
$n_e$	effective number of accepted values of density in a set
$n_s$	number of density values in subset $s$
$p$	order of the polynomial for density values at temperatures $\leq T_b$
$s$	number of subsets in the random deviation algorithm
$u_j$	uncertainty assigned to the $j$ -th observed density value in a set
$w_j$	weighting factor for the $j$ -th density value in a set
$C_{k,l}$	Element $k,l$ of the variance-covariance matrix for the polynomial parameters
$T$	absolute temperature
$T_b$	boundary temperature
$T_c$	critical temperature
$T_j$	temperature for the $j$ -th observed density
$\overline{T^k}$	mean value of the $T_j^k$ values in a set
$T_{n,j}$	$T_j^k - \overline{T^k}$ , normalized value of the $j$ -th temperature raised to the $k$ power
$\delta_j$	$\rho_j - \rho_{x,j}$
$\theta_j$	$(1 - T_j/T_c)^{1/3}$
$\rho$	density
$\rho(\text{API})$	API specific gravity
$\overline{\rho}$	mean value of observed densities in a set
$\rho_o$	density of a standard substance
$\rho_c$	critical density
$\rho_j$	observed value of $j$ -th density in a data set
$\rho_m$	molar density
$\rho_{n,j}$	$\rho_j - \overline{\rho}$ , normalized density for the $j$ -th value
$\rho_r$	relative density
$\rho_{x,j}$	calculated value of the $j$ -th density in a data set
$\sigma$	$(\chi^2/n)^{1/2}$ , standard deviation for density values in a set
$\chi_k^2$	$\sum \delta_j^2$ for all values in a set fit to a polynomial of order $k$
$\Delta T$	$T_n - T_1$ , range of temperatures for data in a set



The following symbols refer to components in a mixture at a fixed temperature

$c$	number of components in the mixture
$i$	component number
$v_i$	partial specific volume of component $i$ in the mixture
$w_i$	mass fraction of component $i$ in the mixture
$x_i$	mole fraction of component $i$ in the mixture
$M_i$	molar mass (molecular weight) of component $i$
$V$	molar volume of a mixture
$V_i$	partial molal volume of component $i$ in the mixture
$\rho$	density of a mixture of components
$\rho_i$	density of pure component $i$

Symbols used in the tables:

$A, B, C, D, E$	coefficients in function for density (see section 1.4.3)
$\rho_{\text{calc}}$	calculated density, $\rho_x$
$\rho_{\text{exp}}$	observed value of $j$ -th density in a data set, $\rho_j$
$\sigma_i$	$(\sum w_j \delta_j^2 / \sum w_j)^{1/2}$ , for low temperature range only
$\sigma_{\text{c,w}}$	$(\sum w_j \delta_j^2 / \sum w_j)^{1/2}$ , for low and high temperature range combined
$\sigma_{\text{c,uw}}$	$[\sum \delta_j^2 / n(n - p - 2)]^{1/2}$ , for low and high temperature range combined
$2\sigma_{\text{est}}$	estimated uncertainty, $u_j$

## 1.7 Order of Compounds in the Tables

The density tables are organized into 3 main classes of compounds as described in the Table of Contents: monoalcohols, diols, and triols. Within each main class (except for the triols) there are several subclasses. They start with fully saturated compounds and proceed with increasing extents of unsaturation. Within each subclass the compounds are arranged in formula order. First with increasing number of carbon atoms in the empirical formula and then with increasing number of hydrogen atoms. Compounds with the same formula are sorted alphabetically by Table Name.

## References

- |            |                                                                                                                                                                     |
|------------|---------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| 67-gug     | Guggenheim, E.A.: Thermodynamics, 5th edition, Amsterdam: North-Holland Publishing Company (1957).                                                                  |
| 86-ros/bae | Rossiter, B.W., Baetzold, R.C.: Physical Methods of Chemistry, 2nd edition, Vol. VI, Determination of Thermodynamic Properties, New York: John Wiley & Sons (1986). |
| 88-pre/fla | Press, W.H., Flannery, B.P., Teukolsky, S.A., Vetterling, W.T.: Numerical Recipes in C, New York: Cambridge Univ. Press (1988).                                     |

## 2 Tabulated Data on Density - Monoalcohols

### 2.1 Alkanols

#### 2.1.1 Alkanols, C<sub>1</sub> - C<sub>4</sub>

**Methanol** [67-56-1] CH<sub>4</sub>O MW = 32.04 1

$$T_c = 512.64 \text{ K [89-tej/lee]}$$

$$\rho_c = 272.00 \text{ kg}\cdot\text{m}^{-3} \text{ [89-tej/lee]}$$

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_i = 5.5832 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (4.8307 \cdot 10^{-1})$  combined temperature ranges, weighted),  $\sigma_{c,uw} = 3.4016 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 176.15 \text{ to } 400.00 \text{ K}$	$T = 400.00 \text{ to } 512.64 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$	$\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3$ $+ D(T_c - T)^4]$
A	$1.14445 \cdot 10^3$	2.46064
B	-1.79908	$-5.82461 \cdot 10^{-2}$
C	$3.16450 \cdot 10^{-3}$	$5.61772 \cdot 10^{-4}$
D	$-3.87839 \cdot 10^{-6}$	$-1.89776 \cdot 10^{-6}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg}\cdot\text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg}\cdot\text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg}\cdot\text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg}\cdot\text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
<i>crystal</i>				473.15	$552.50 \pm 3.00$	-3.21	1887-ram/you(X)
78.15	$1041 \pm 3.00$		30-bil/fis-1	483.15	$525.40 \pm 3.00$	-2.04	1887-ram/you(X)
<i>liquid</i>				493.15	$490.00 \pm 3.00$	2.14	1887-ram/you(X)
296.09	$789.07 \pm 0.50$	0.56	1887-ram/you <sup>1)</sup>	498.15	$468.00 \pm 3.00$	6.30	1887-ram/you(X)
296.09	$789.09 \pm 0.60$	0.58	1887-ram/you <sup>1)</sup>	503.15	$441.80 \pm 5.00$	12.68	1887-ram/you <sup>1)</sup>
353.15	$736.80 \pm 1.00$	3.85	1887-ram/you <sup>1)</sup>	505.15	$430.10 \pm 5.00$	16.61	1887-ram/you <sup>1)</sup>
363.15	$723.90 \pm 1.00$	1.20	1887-ram/you <sup>1)</sup>	507.15	$412.70 \pm 5.00$	17.09	1887-ram/you <sup>1)</sup>
373.15	$713.50 \pm 1.00$	1.27	1887-ram/you(X)	509.15	$395.30 \pm 5.00$	21.13	1887-ram/you <sup>1)</sup>
383.15	$702.80 \pm 1.50$	1.26	1887-ram/you(X)	510.15	$386.60 \pm 5.00$	25.49	1887-ram/you <sup>1)</sup>
393.15	$689.90 \pm 1.50$	-0.68	1887-ram/you(X)	511.15	$370.50 \pm 5.00$	25.55	1887-ram/you <sup>1)</sup>
403.15	$677.70 \pm 1.50$	-1.36	1887-ram/you(X)	511.65	$364.20 \pm 0.00$	29.63	1887-ram/you <sup>1)</sup>
413.15	$664.90 \pm 1.50$	0.95	1887-ram/you(X)	293.15	$790.48 \pm 0.00$	-0.81	1893-ram/shi-3 <sup>1)</sup>
423.15	$649.40 \pm 1.50$	2.71	1887-ram/you(X)	343.15	$745.98 \pm 0.00$	2.97	1893-ram/shi-3 <sup>1)</sup>
433.15	$632.10 \pm 2.00$	2.92	1887-ram/you(X)	353.15	$735.50 \pm 0.60$	2.55	1893-ram/shi-3 <sup>1)</sup>
443.15	$616.00 \pm 2.00$	3.84	1887-ram/you(X)	363.15	$725.00 \pm 1.50$	2.30	1893-ram/shi-3 <sup>1)</sup>
453.16	$596.70 \pm 2.00$	1.43	1887-ram/you(X)	373.15	$714.00 \pm 1.50$	1.77	1893-ram/shi-3(X)
463.15	$578.00 \pm 2.00$	0.76	1887-ram/you(X)	383.15	$702.00 \pm 1.50$	0.46	1893-ram/shi-3(X)

<sup>1)</sup> Not included in Fig. 1.

cont.

## Methanol (cont.)

Table 2. (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
393.15	690.00 ± 1.50	-0.58	1893-ram/shi-3(X)	223.15	857.20 ± 0.50	-0.26	67-kom/man <sup>1)</sup>
403.15	677.00 ± 1.50	-2.06	1893-ram/shi-3(X)	233.15	847.80 ± 0.50	-0.06	67-kom/man <sup>1)</sup>
413.15	664.00 ± 1.50	0.05	1893-ram/shi-3(X)	243.15	838.40 ± 0.50	0.06	67-kom/man <sup>1)</sup>
423.15	649.50 ± 1.50	2.81	1893-ram/shi-3(X)	253.15	829.00 ± 0.40	0.11	67-kom/man <sup>1)</sup>
433.15	634.00 ± 2.00	4.82	1893-ram/shi-3(X)	263.15	819.60 ± 0.40	0.12	67-kom/man <sup>1)</sup>
443.15	616.00 ± 2.00	3.84	1893-ram/shi-3(X)	273.15	810.20 ± 0.40	0.11	67-kom/man <sup>1)</sup>
453.15	598.00 ± 2.00	2.71	1893-ram/shi-3(X)	283.15	800.80 ± 0.40	0.10	67-kom/man <sup>1)</sup>
463.15	577.00 ± 2.00	-0.24	1893-ram/shi-3(X)	293.15	791.30 ± 0.40	0.01	67-kom/man <sup>1)</sup>
473.15	553.00 ± 3.00	-2.71	1893-ram/shi-3(X)	298.15	787.00 ± 0.40	0.44	67-kom/man <sup>1)</sup>
483.15	525.50 ± 3.00	-1.94	1893-ram/shi-3(X)	413.15	636.94 ± 0.00	-27.01	69-zub/bag <sup>1)</sup>
493.15	490.00 ± 3.00	2.14	1893-ram/shi-3(X)	423.15	628.93 ± 0.00	-17.76	69-zub/bag <sup>1)</sup>
503.15	441.00 ± 5.00	11.88	1893-ram/shi-3 <sup>1)</sup>	433.15	621.12 ± 0.00	-8.06	69-zub/bag <sup>1)</sup>
507.15	414.50 ± 5.00	18.89	1893-ram/shi-3 <sup>1)</sup>	443.15	609.76 ± 0.00	-2.40	69-zub/bag <sup>1)</sup>
509.15	395.50 ± 5.00	21.33	1893-ram/shi-3 <sup>1)</sup>	453.15	594.11 ± 1.50	-1.18	69-zub/bag(X)
513.15	271.20 ± 0.00	19.30	1893-ram/shi-3 <sup>1)</sup>	463.15	573.39 ± 1.50	-3.85	69-zub/bag(X)
293.15	791.31 ± 0.06	0.02	32-ros(V)	473.15	550.99 ± 1.50	-4.72	69-zub/bag(X)
323.15	763.20 ± 0.40	0.55	50-hou/mas-1 <sup>1)</sup>	483.15	524.49 ± 1.50	-2.95	69-zub/bag(X)
333.15	753.60 ± 0.40	0.70	50-hou/mas-1 <sup>1)</sup>	493.15	489.00 ± 2.00	1.14	69-zub/bag(X)
343.15	744.20 ± 0.40	1.19	50-hou/mas-1(X)	498.15	466.90 ± 2.00	5.20	69-zub/bag(X)
353.15	734.70 ± 0.50	1.75	50-hou/mas-1(X)	503.15	440.01 ± 2.00	10.89	69-zub/bag(X)
363.15	725.10 ± 0.60	2.40	50-hou/mas-1 <sup>1)</sup>	505.15	426.20 ± 2.00	12.71	69-zub/bag(X)
403.15	671.80 ± 1.00	-7.26	55-kay/don(X)	507.15	409.70 ± 3.00	14.09	69-zub/bag(X)
413.15	657.40 ± 1.00	-6.55	55-kay/don(X)	509.15	387.81 ± 3.00	13.64	69-zub/bag(X)
423.15	642.00 ± 1.00	-4.69	55-kay/don(X)	511.15	346.87 ± 3.00	1.92	69-zub/bag(X)
433.15	625.80 ± 1.50	-3.38	55-kay/don(X)	512.65	274.57 ± 0.00	2.05	69-zub/bag <sup>1)</sup>
443.15	608.10 ± 1.50	-4.06	55-kay/don(X)	183.15	896.80 ± 0.20	-0.47	71-yer/swi(X)
453.15	589.10 ± 1.50	-6.19	55-kay/don(X)	193.15	886.70 ± 0.20	-0.36	71-yer/swi(X)
463.15	568.10 ± 2.00	-9.14	55-kay/don(X)	203.15	876.80 ± 0.20	-0.25	71-yer/swi(X)
473.15	544.80 ± 2.00	-10.91	55-kay/don(X)	213.15	867.30 ± 0.20	0.11	71-yer/swi(X)
483.15	517.00 ± 2.00	-10.44	55-kay/don(X)	223.15	857.40 ± 0.20	-0.06	71-yer/swi(X)
493.15	481.10 ± 3.00	-6.76	55-kay/don(X)	233.15	847.90 ± 0.20	0.04	71-yer/swi(X)
503.15	432.10 ± 5.00	2.98	55-kay/don <sup>1)</sup>	243.15	838.30 ± 0.20	-0.04	71-yer/swi(X)
512.58	272.00 ± 5.00	-23.47	55-kay/don <sup>1)</sup>	253.15	828.90 ± 0.20	0.01	71-yer/swi(X)
283.15	800.45 ± 0.10	-0.25	58-yam/kun(X)	263.15	819.70 ± 0.20	0.22	71-yer/swi(X)
288.15	795.81 ± 0.10	-0.19	58-yam/kun(X)	273.15	810.40 ± 0.20	0.31	71-yer/swi <sup>1)</sup>
293.15	791.32 ± 0.10	0.03	58-yam/kun <sup>1)</sup>	283.15	800.80 ± 0.20	0.10	71-yer/swi <sup>1)</sup>
273.15	809.98 ± 0.10	-0.11	59-mck/ski(X)	281.40	802.32 ± 0.20	-0.03	72-rei/eis(□)
176.15	904.60 ± 0.70	0.07	67-kom/man(X)	284.78	798.99 ± 0.20	-0.18	72-rei/eis(□)
183.15	897.00 ± 0.70	-0.27	67-kom/man <sup>1)</sup>	285.69	798.15 ± 0.20	-0.16	72-rei/eis(□)
193.15	886.80 ± 0.60	-0.26	67-kom/man <sup>1)</sup>	288.72	795.35 ± 0.20	-0.11	72-rei/eis(□)
203.15	876.50 ± 0.60	-0.55	67-kom/man <sup>1)</sup>	289.64	794.49 ± 0.20	-0.11	72-rei/eis(□)
213.15	866.60 ± 0.60	-0.59	67-kom/man <sup>1)</sup>	292.96	791.41 ± 0.20	-0.06	72-rei/eis(□)

<sup>1)</sup> Not included in Fig. 1.

cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.82	790.60 ± 0.20	-0.06	72-rei/eis(□)	323.15	762.70 ± 0.20	0.05	88-sun/bis(×)
296.97	787.67 ± 0.20	-0.01	72-rei/eis(□)	333.15	753.00 ± 0.20	0.10	88-sun/bis(×)
297.87	786.82 ± 0.20	-0.01	72-rei/eis(□)	205.16	875.03 ± 0.20	-0.02	88-sun/sch-1(×)
300.90	783.98 ± 0.20	0.02	72-rei/eis(□)	212.69	867.57 ± 0.20	-0.07	88-sun/sch-1(×)
301.62	783.29 ± 0.20	0.02	72-rei/eis(□)	223.11	857.33 ± 0.20	-0.17	88-sun/sch-1(×)
304.83	780.27 ± 0.20	0.04	72-rei/eis(□)	232.45	848.35 ± 0.20	-0.18	88-sun/sch-1(×)
305.70	779.45 ± 0.20	0.05	72-rei/eis(□)	243.17	838.12 ± 0.20	-0.20	88-sun/sch-1(×)
308.32	776.96 ± 0.20	0.06	72-rei/eis(□)	252.11	829.73 ± 0.20	-0.14	88-sun/sch-1(×)
309.17	776.16 ± 0.20	0.07	72-rei/eis(□)	261.62	820.74 ± 0.20	-0.18	88-sun/sch-1(×)
311.32	774.13 ± 0.20	0.09	72-rei/eis(□)	269.38	813.50 ± 0.20	-0.13	88-sun/sch-1(×)
312.17	773.33 ± 0.20	0.11	72-rei/eis(□)	273.27	809.79 ± 0.20	-0.19	88-sun/sch-1 <sup>1)</sup>
317.16	768.56 ± 0.20	0.12	72-rei/eis(□)	281.82	801.87 ± 0.20	-0.08	88-sun/sch-1 <sup>1)</sup>
293.15	791.04 ± 0.20	-0.25	76-hal/ell <sup>1)</sup>	292.38	792.04 ± 0.20	0.03	88-sun/sch-1 <sup>1)</sup>
298.15	786.37 ± 0.20	-0.19	76-hal/ell <sup>1)</sup>	294.36	790.05 ± 0.20	-0.10	88-sun/sch-1 <sup>1)</sup>
303.15	781.65 ± 0.20	-0.17	76-hal/ell <sup>1)</sup>	298.16	786.55 ± 0.20	-0.00	88-sun/sch-1 <sup>1)</sup>
320.00	765.59 ± 0.20	-0.11	76-hal/ell <sup>1)</sup>	303.14	781.79 ± 0.20	-0.04	88-sun/sch-1 <sup>1)</sup>
340.00	745.88 ± 0.20	-0.26	76-hal/ell(×)	313.14	772.23 ± 0.20	-0.06	88-sun/sch-1 <sup>1)</sup>
360.00	725.21 ± 0.20	-0.74	76-hal/ell(×)	323.17	762.58 ± 0.20	-0.05	88-sun/sch-1(×)
380.00	703.03 ± 0.25	-1.90	76-hal/ell(×)	333.15	752.62 ± 0.20	-0.28	88-sun/sch-1(×)
400.00	678.69 ± 0.25	-4.23	76-hal/ell <sup>1)</sup>	203.15	877.08 ± 0.20	0.03	90-sun/sch-1(×)
410.00	665.40 ± 0.25	-3.66	76-hal/ell(×)	213.15	867.09 ± 0.20	-0.10	90-sun/sch-1(×)
420.00	651.27 ± 0.20	-0.95	76-hal/ell(×)	223.15	857.29 ± 0.20	-0.17	90-sun/sch-1(×)
430.00	636.05 ± 0.30	1.40	76-hal/ell(×)	233.15	847.65 ± 0.20	-0.21	90-sun/sch-1(×)
440.00	619.50 ± 0.30	2.03	76-hal/ell(×)	243.15	838.13 ± 0.20	-0.21	90-sun/sch-1(×)
293.15	791.25 ± 0.05	-0.04	84-cer/bou(○)	253.15	828.70 ± 0.20	-0.19	90-sun/sch-1(×)
298.15	786.57 ± 0.03	0.01	86-oga/mur(□)	263.15	819.33 ± 0.20	-0.15	90-sun/sch-1(×)
298.15	786.55 ± 0.06	-0.01	86-tan/toy(◆)	298.15	786.80 ± 0.20	0.24	98-ami/ban(○)
298.15	786.57 ± 0.05	0.01	87-oga/mur(Δ)	303.15	781.80 ± 0.20	-0.02	98-ami/ban(○)
273.15	809.99 ± 0.20	-0.10	88-sun/bis <sup>1)</sup>	308.15	777.10 ± 0.20	0.04	98-ami/ban(○)
283.15	800.70 ± 0.20	-0.00	88-sun/bis <sup>1)</sup>	298.15	786.60 ± 0.20	0.04	98-ami/pat-1(Δ)
293.15	791.32 ± 0.20	0.03	88-sun/bis <sup>1)</sup>	303.15	781.70 ± 0.20	-0.12	98-ami/pat-1(Δ)
303.15	781.86 ± 0.20	0.04	88-sun/bis <sup>1)</sup>	308.15	776.90 ± 0.20	-0.16	98-ami/pat-1(Δ)
313.15	772.32 ± 0.20	0.03	88-sun/bis <sup>1)</sup>				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1848-kop, 1854-kop, 1863-gla/dal, 1864-lan, 1880-pry, 1882-sch-1, 1883-sch-3, 1884-gla, 1884-per, 1884-sch-6, 1884-zan, 1886-tra, 1890-gar, 1891-jah, 1891-sch/kos, 1892-lan/jah, 1896-zel/kra, 1898-kah, 1898-roh, 00-loo, 02-you/for, 03-car/cop, 04-bru/sch, 04-cri, 06-car/fer, 06-kla/nor, 06-wal-1, 07-che-1, 07-tim, 08-get, 08-gyr, 08-ric/mat, 09-dor, 09-hol/sag, 10-daw, 10-dor/pol, 10-fon, 10-tim, 11-dor, 12-kor, 12-mal, 12-tim, 12-tim-1, 12-tyr, 13-atk/wal, 13-bri-1, 13-rom, 13-ste, 14-kre/mei, 14-low, 14-mer/tur, 14-tyr, 15-ric/coo, 16-har-2, 16-ric/shi, 16-sei/alt, 16-wro/rei, 17-jae, 18-her-2, 19-eyk, 20-ric/dav, 21-bar/bir, 21-rei/hic, 22-her/sch, 22-mck/sim, 23-wil/smi, 24-bus-1, 24-dan, 24-mar-1, 24-mil, 25-har/rai, 25-lew, 25-nor/ash, 25-par, 25-per, 25-rak, 26-ewa/rai, 26-gol/aar, 26-mat, 26-mun, 26-ris/hic, 26-sch, 27-arb-2, 28-llo/bro, 29-kel-1, 30-bil/fis-1, 30-rak/fro, 30-tim/hen, 31-bea/mcv, 31-fio/gin, 31-lun/bje, 33-but/tho, 33-koz/koz, 33-nat/bac, 33-vos/con, 34-cor/arc, 34-smi, 34-was/spe, 35-gib, 35-hen, 35-kef/mcl, 36-tom]

cont.

**Methanol** (cont.)**Further references:** (cont.)

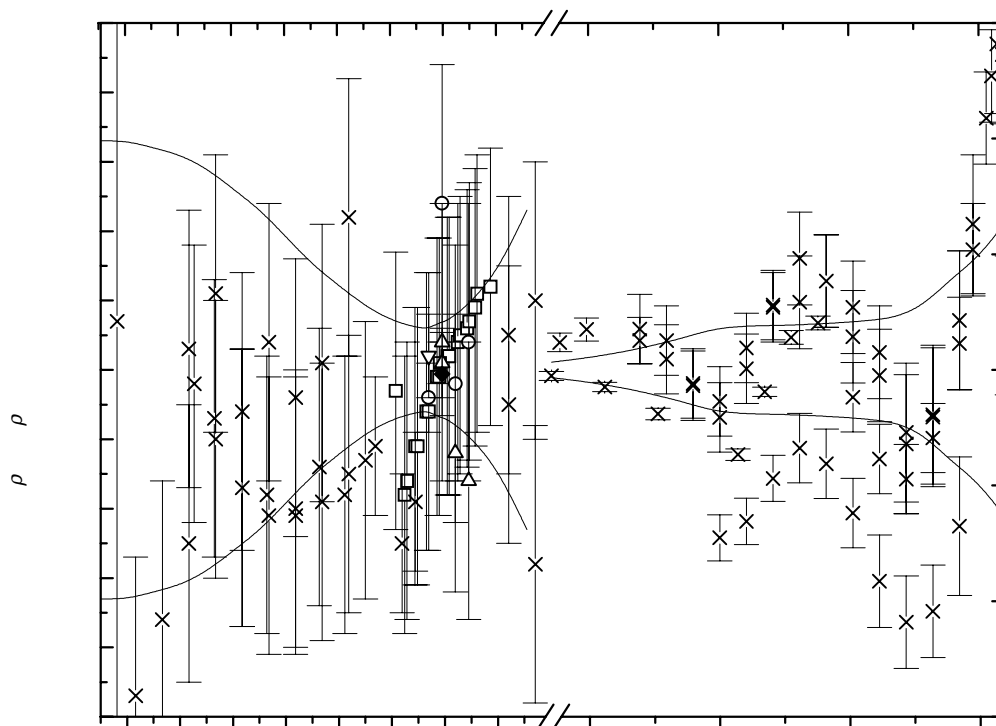
[37-bet/ham, 37-gib/kin, 37-sta/gil, 38-jon/for, 39-lar/hun, 40-pes-1, 40-was/gra, 42-bri/rin, 42-mor/mun, 42-mul, 43-eck/luc, 44-pes/lag, 45-add, 45-dul, 46-kre/now, 46-sca/woo, 46-sca/woo-1, 47-woo, 48-jon/bow, 48-vog-2, 48-wei, 48-wil/ros, 49-gor/gor, 49-gri/buf, 49-hat, 49-sta/gup, 49-tsc/ric, 49-udo/kal, 50-jac, 50-joe/nik, 50-lar/ver, 50-pic/zie, 50-sac/sau, 50-sad/fuo, 50-tei/gor, 50-wol/sau, 51-car/rid, 51-cli/cam, 51-lyu/ter, 51-sie/cru, 51-tei/gor, 52-hug/mal, 52-sca/tic, 52-sta/spi, 53-ame/pax, 53-ani-1, 53-mck/tar, 53-par/cha, 54-col, 54-cro/spi, 54-gri, 54-kre/wie, 54-pur/bow, 54-sad/fuo, 55-den/col, 55-gre/ven, 55-ham/sto, 56-ame/pax, 56-fai/win, 57-gol, 57-mil, 57-tul/chr, 58-ano-5, 58-cos/bow, 58-lin/van, 58-mur/van, 59-ale, 59-yen/ree, 60-cop/fin, 61-mik/kim, 62-bro/smi, 62-chu/tho, 62-mik/kim, 62-nag-4, 62-par/mis, 63-aki/yos, 63-fis, 63-hov/sea, 63-mcc/lai, 63-raj/ran, 64-ma /koh, 65-for/moo, 66-kat/pra-1, 66-kat/shi, 67-cun/vid, 67-fre, 67-han/hac, 67-nak/nak, 67-nak/shi, 67-sum/tho, 68-ano, 68-bek/hal, 68-nak/shi, 68-pfl/pop, 68-sin/ben, 69-bru/gub, 70-iin/sud, 70-kat/kon, 70-kat/kon-1, 70-kon/lya, 70-nak/shi, 70-str/svo, 71-des/bha, 71-des/bha-1, 71-nag/oht, 72-bou/aim, 72-nie/nov, 72-pol/lu, 72-pol/lu -1, 73-khi/ale, 73-svo/ves, 74-dut/mat, 75-mat/fer, 75-mus/ver, 75-nak/wad, 75-tok, 76-kat/nit, 76-mcg/wil, 76-nag/oht, 76-nak/ash, 76-sri/kul, 76-wes, 77-hwa/rob, 77-sch/pla, 77-tre/ben, 78-och/lu, 79-cha/ses-1, 79-cib/hyn, 79-coc/pis, 79-dia/tar, 79-jim/paz, 79-kiy/ben, 80-aim/cip, 80-arc/bla, 80-ben/kiy, 80-edu/boy, 80-kub/tsu, 80-yos/tak, 81-fre/cri, 81-kum/pra, 81-sjo/dyh, 81-tas/ara, 81-won/chu, 82-diz/mar, 82-dom/rat, 82-ort, 83-fuk/ogi, 83-pik-2, 83-rau/ste, 83-tri, 84-sak/nak, 85-dri/ras, 85-kov/svo, 85-mat/ben, 85-mat/ben-1, 85-nag, 85-ort/paz-1, 85-pat/san, 85-sch/pla, 85-tri/rod, 86-bot/bre, 86-cra, 86-hne/cib, 86-kud/str, 86-lep/mat, 86-lin/ber, 86-miy/hay, 86-san/sha, 86-yer/wor, 86-zha/ben-1, 87-ham/als, 87-kub/tan, 87-lin/ber, 87-man/ami, 87-pik, 88-aww/all, 88-bag/gur, 88-ben/van, 88-man/ami, 88-nag-2, 88-ohg/tak, 88-oka/oga, 89-ala/sal, 89-ale/fer, 89-dou/kha, 89-kat/tan, 89-kat/tan-1, 89-nao/sur, 89-raj/ren, 90-arc/dom, 90-cha/kat, 90-jos/ami-1, 90-lee/hon, 90-let/sch-1, 90-rie/sch, 91-cab/bel, 91-gar/her, 91-kat/tan, 91-liu/pus, 91-ram/muk, 92-hia/yam, 92-lee/wei, 92-pap/zio, 92-pla/ste, 93-ami/ara, 94-arc/bla, 94-kim/lee, 94-pap/pan-1, 95-arc/bla, 95-che/kna, 95-red/ram-1, 96-nik/jad, 96-nik/mah, 97-arc/bla, 97-com/fra, 98-arc/mar, 98-arc/nar, 98-bla/ort, 98-igl/org, 98-nik/shi, 98-zie].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
170.00	911.00 ± 0.33	293.15	791.29 ± 0.06	410.00	669.06 ± 1.88
180.00	900.52 ± 0.33	298.15	786.56 ± 0.07	420.00	652.22 ± 1.91
190.00	890.26 ± 0.32	300.00	784.81 ± 0.07	430.00	634.65 ± 1.94
200.00	880.18 ± 0.31	310.00	775.30 ± 0.10	440.00	617.47 ± 1.99
210.00	870.28 ± 0.29	320.00	765.70 ± 0.15	450.00	600.65 ± 2.05
220.00	860.51 ± 0.26	330.00	755.99 ± 0.23	460.00	583.17 ± 2.14
230.00	850.87 ± 0.23	340.00	746.14 ± 0.34	470.00	563.04 ± 2.29
240.00	841.33 ± 0.19	350.00	736.13 ± 0.47	480.00	537.31 ± 2.83
250.00	831.86 ± 0.15	360.00	725.95 ± 0.64	490.00	501.91 ± 3.95
260.00	822.44 ± 0.12	370.00	715.55 ± 0.85	500.00	450.53 ± 4.84
270.00	813.05 ± 0.09	380.00	704.93 ± 1.11	510.00	363.22 ± 6.34
280.00	803.66 ± 0.07	390.00	694.06 ± 1.40		
290.00	794.26 ± 0.06	400.00	682.92 ± 1.75		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Ethanol****[64-17-5]****C<sub>2</sub>H<sub>6</sub>O****MW = 46.07****2**

$$T_c = 514.10 \text{ K [89-tej/lee]}$$

$$\rho_c = 276.00 \text{ kg}\cdot\text{m}^{-3} \text{ [89-tej/lee]}$$

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):

$\sigma_i = 2.7027 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (1.5405 \cdot 10^{-1})$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.5778 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 191.15 \text{ to } 400.00 \text{ K}$	$T = 400.00 \text{ to } 514.10 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$	$\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3$ $+ D(T_c - T)^4]$
<i>A</i>	$1.16239 \cdot 10^3$	1.73318
<i>B</i>	-2.25788	$-3.58319 \cdot 10^{-2}$
<i>C</i>	$5.30621 \cdot 10^{-3}$	$3.19777 \cdot 10^{-4}$
<i>D</i>	$-6.63070 \cdot 10^{-6}$	$-1.03287 \cdot 10^{-6}$

cont.

## Ethanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
<i>crystal</i>				298.15	784.96 ± 0.05	-0.19	80-ben/kiy <sup>1)</sup>
78.15	1021 ± 3.0		30-bilfis-1	303.15	780.67 ± 0.05	-0.15	80-ben/kiy(V)
<i>liquid</i>				308.15	776.38 ± 0.05	-0.08	80-ben/kiy(V)
288.15	793.75 ± 0.08	0.03	13-osb/mck(X)	223.15	848.91 ± 0.10	-0.18	82-sch/pol(X)
298.15	785.03 ± 0.08	-0.12	13-osb/mck <sup>1)</sup>	223.17	848.99 ± 0.10	-0.08	82-sch/pol(X)
273.15	806.28 ± 0.08	-0.14	48-kre/now(◆)	233.15	840.29 ± 0.10	-0.08	82-sch/pol <sup>1)</sup>
298.15	785.04 ± 0.08	-0.11	48-kre/now <sup>1)</sup>	233.15	840.31 ± 0.10	-0.06	82-sch/pol <sup>1)</sup>
353.15	763.12 ± 0.08	28.38	48-kre/now <sup>1)</sup>	233.15	840.39 ± 0.10	0.02	82-sch/pol <sup>1)</sup>
273.15	806.30 ± 0.40	-0.12	58-cos/bow <sup>1)</sup>	233.15	840.28 ± 0.10	-0.09	82-sch/pol <sup>1)</sup>
293.15	789.40 ± 0.40	-0.05	58-cos/bow <sup>1)</sup>	243.13	831.74 ± 0.10	-0.06	82-sch/pol <sup>1)</sup>
313.15	772.20 ± 0.40	0.14	58-cos/bow <sup>1)</sup>	243.15	831.79 ± 0.10	0.01	82-sch/pol <sup>1)</sup>
333.15	754.10 ± 0.40	0.17	58-cos/bow <sup>1)</sup>	243.15	831.71 ± 0.10	-0.07	82-sch/pol <sup>1)</sup>
353.15	734.80 ± 0.50	0.06	58-cos/bow <sup>1)</sup>	243.15	831.73 ± 0.10	-0.05	82-sch/pol <sup>1)</sup>
373.15	715.70 ± 0.50	1.51	58-cos/bow <sup>1)</sup>	253.14	823.28 ± 0.10	-0.01	82-sch/pol(X)
393.15	692.50 ± 0.50	0.57	58-cos/bow(X)	253.14	823.26 ± 0.10	-0.03	82-sch/pol(X)
413.15	663.10 ± 0.60	-2.49	58-cos/bow(X)	253.18	823.25 ± 0.10	-0.01	82-sch/pol(X)
433.15	632.90 ± 0.60	-0.00	58-cos/bow(X)	258.15	819.03 ± 0.10	-0.03	82-sch/pol(X)
453.15	598.40 ± 0.60	0.81	58-cos/bow(X)	258.15	819.04 ± 0.10	-0.02	82-sch/pol(X)
473.15	556.80 ± 0.70	2.22	58-cos/bow(X)	263.15	814.83 ± 0.10	-0.01	82-sch/pol(X)
483.15	518.60 ± 2.00	-7.37	64-ska/kay(X)	263.15	814.82 ± 0.10	-0.02	82-sch/pol(X)
488.15	503.40 ± 2.00	-5.29	64-ska/kay(X)	268.15	810.62 ± 0.10	-0.01	82-sch/pol(X)
493.15	486.30 ± 2.00	-2.43	64-ska/kay(X)	268.15	810.60 ± 0.10	-0.03	82-sch/pol(X)
498.15	466.80 ± 2.00	1.52	64-ska/kay(X)	273.14	806.30 ± 0.10	-0.12	82-sch/pol <sup>1)</sup>
503.15	443.20 ± 3.00	6.26	64-ska/kay(X)	273.15	806.32 ± 0.10	-0.10	82-sch/pol <sup>1)</sup>
508.15	411.30 ± 3.00	10.86	64-ska/kay <sup>1)</sup>	283.15	797.88 ± 0.10	-0.08	82-sch/pol(X)
513.15	339.50 ± 5.00	1.88	64-ska/kay(X)	283.15	797.89 ± 0.10	-0.07	82-sch/pol(X)
293.15	789.20 ± 0.20	-0.25	76-hal/ell <sup>1)</sup>	293.17	789.28 ± 0.10	-0.15	82-sch/pol <sup>1)</sup>
298.15	784.93 ± 0.20	-0.22	76-hal/ell <sup>1)</sup>	293.18	789.26 ± 0.10	-0.16	82-sch/pol <sup>1)</sup>
303.15	780.64 ± 0.20	-0.18	76-hal/ell <sup>1)</sup>	298.15	785.27 ± 0.02	0.12	84-eas/woo(□)
320.00	765.83 ± 0.20	-0.12	76-hal/ell(X)	298.15	785.10 ± 0.02	-0.05	86-oga/mur(O)
340.00	747.47 ± 0.20	-0.02	76-hal/ell(X)	303.15	780.74 ± 0.15	-0.08	87-pik <sup>1)</sup>
360.00	727.80 ± 0.20	-0.07	76-hal/ell(X)	333.15	754.38 ± 0.15	0.45	87-pik(X)
380.00	706.17 ± 0.20	-0.60	76-hal/ell(X)	298.15	784.50 ± 0.08	-0.65	87-rat/sin-3 <sup>1)</sup>
400.00	681.96 ± 0.30	-1.90	76-hal/ell <sup>1)</sup>	308.15	776.30 ± 0.08	-0.16	87-rat/sin-3(X)
420.00	654.27 ± 0.30	-0.49	76-hal/ell(X)	191.15	878.08 ± 0.20	-0.28	88-sun/sch-1(X)
430.00	638.82 ± 0.50	0.60	76-hal/ell(X)	202.34	867.78 ± 0.20	-0.06	88-sun/sch-1(X)
440.00	621.92 ± 0.50	0.76	76-hal/ell(X)	212.98	858.24 ± 0.20	0.10	88-sun/sch-1(X)
450.00	603.52 ± 0.50	0.09	76-hal/ell(X)	222.18	850.13 ± 0.20	0.19	88-sun/sch-1 <sup>1)</sup>
455.00	593.63 ± 0.50	-0.46	76-hal/ell(X)	229.95	843.37 ± 0.20	0.23	88-sun/sch-1 <sup>1)</sup>
298.15	785.13 ± 0.02	-0.02	79-kiy/ben(Δ)	239.35	835.28 ± 0.20	0.25	88-sun/sch-1 <sup>1)</sup>
288.15	793.50 ± 0.05	-0.22	80-ben/kiy(V)	250.85	825.25 ± 0.20	0.02	88-sun/sch-1 <sup>1)</sup>
293.15	789.24 ± 0.05	-0.21	80-ben/kiy(V)	260.49	817.35 ± 0.20	0.27	88-sun/sch-1 <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
268.58	810.46 ± 0.20	0.19	88-sun/sch-1 <sup>1)</sup>	203.15	867.05 ± 0.10	-0.04	91-sun/sch(X)
280.78	800.14 ± 0.20	0.17	88-sun/sch-1 <sup>1)</sup>	213.15	858.06 ± 0.10	0.07	91-sun/sch(X)
292.39	790.25 ± 0.20	0.15	88-sun/sch-1 <sup>1)</sup>	223.15	849.24 ± 0.10	0.15	91-sun/sch(X)
298.15	785.31 ± 0.20	0.16	88-sun/sch-1 <sup>1)</sup>	233.15	840.57 ± 0.10	0.20	91-sun/sch <sup>1)</sup>
303.15	780.93 ± 0.20	0.11	88-sun/sch-1 <sup>1)</sup>	243.15	832.00 ± 0.10	0.22	91-sun/sch <sup>1)</sup>
313.17	772.17 ± 0.20	0.13	88-sun/sch-1 <sup>1)</sup>	253.15	823.50 ± 0.10	0.22	91-sun/sch(X)
323.21	763.20 ± 0.20	0.15	88-sun/sch-1(X)	263.15	815.04 ± 0.10	0.20	91-sun/sch(X)
333.15	754.15 ± 0.20	0.22	88-sun/sch-1(X)	320.00	766.04 ± 0.20	0.09	96-tak/uem(X)
273.15	806.27 ± 0.20	-0.15	88-sun/ten <sup>1)</sup>	380.00	705.92 ± 0.20	-0.85	96-tak/uem(X)
283.15	797.83 ± 0.20	-0.13	88-sun/ten <sup>1)</sup>	400.00	681.80 ± 0.20	-2.06	96-tak/uem <sup>1)</sup>
293.15	789.34 ± 0.20	-0.11	88-sun/ten <sup>1)</sup>	420.00	654.35 ± 0.30	-0.41	96-tak/uem(X)
303.15	780.81 ± 0.20	-0.01	88-sun/ten <sup>1)</sup>	420.00	654.24 ± 0.20	-0.52	96-tak/uem(X)
313.15	772.23 ± 0.20	0.17	88-sun/ten <sup>1)</sup>	440.00	622.02 ± 0.30	0.86	96-tak/uem(X)
323.15	763.61 ± 0.20	0.50	88-sun/ten(X)	460.00	582.79 ± 0.50	-1.47	96-tak/uem(X)
333.15	754.94 ± 0.20	1.01	88-sun/ten(X)	480.00	535.76 ± 1.00	0.02	96-tak/uem(X)
193.15	876.24 ± 0.10	-0.22	91-sun/sch(X)				

<sup>1)</sup> Not included in Fig. 1.

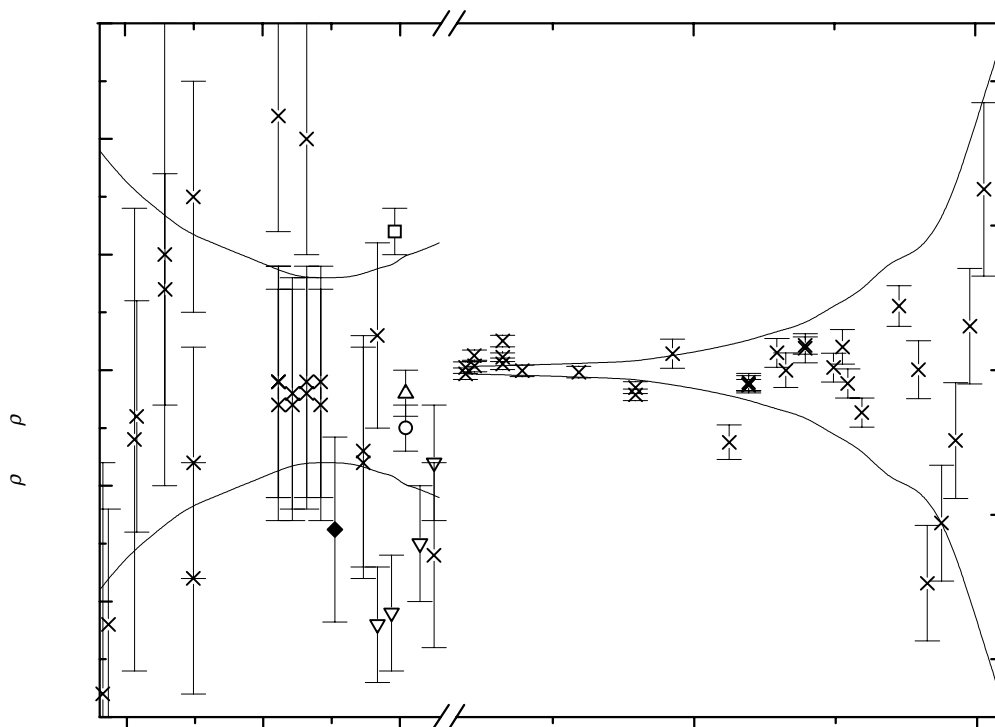
**Further references:** [94-gil, 1811-bra, 1864-lan, 1865-men, 1869-dup/pag, 1882-sch-1, 1883-sch-3, 1884-per, 1884-sch-6, 1888-ket, 1890-gar, 1891-jah, 1891-sch/kos, 1892-lan/jah, 1893-eyk, 1897-zec, 1898-kah, 1898-roh, 00-loo, 01-rud, 02-you, 03-car/cop, 04-bru/sch, 04-cri, 04-dun, 05-win, 06-kla/nor, 06-wal-1, 07-che, 07-dun/tho, 07-tim, 08-and, 08-dor/rak, 08-dun/stu, 08-get, 08-ric/mat, 09-hol/sag, 10-daw, 10-dor/pol, 10-pol, 10-tho, 11-del, 11-dor, 11-kai, 12-kor, 12-mal, 12-osb/mck, 12-sch-1, 12-tyr, 12-wad/mer, 12-wre, 13-bri-1, 13-mer, 13-muc, 13-rob/acr, 13-rom, 13-ste, 14-low, 14-mer/tur, 14-tyr, 15-pea, 15-pri, 15-ric/coo, 16-ric/shi, 16-sei/alt, 16-wro/rei, 17-jae, 18-her-2, 19-eyk, 21-bar/bir, 21-bru/cre, 21-rei/hic, 22-her/sch, 22-mck/sim, 22-sch/reg, 22-tro, 23-moe-1, 23-rii, 23-wil/smi, 24-par/sch, 25-gro/kel, 25-nor/ash, 25-pal/con, 25-par/kel-1, 25-per, 25-rak, 25-ric/cha, 26-bar, 26-gol/aar, 26-mat, 26-mun, 26-sch, 27-arb-2, 27-del, 27-krc/wil, 28-llo/bro, 28-mon, 28-par/nel, 29-ber/reu, 29-ham/and, 29-kel-3, 29-smy/sto, 30-bil/fis-1, 30-fro, 30-mon, 31-bea/mcv, 31-fio/gin, 31-lun/bje, 32-ess/cla, 32-ros, 32-sol/mol, 32-swi/zma, 33-har, 33-vos/con, 34-lal, 35-hen, 36-tom, 37-dol/bri, 37-zep, 38-sca/ray, 39-lar/hun, 40-gos-1, 40-mon/qui, 40-tri/ric, 40-was/gra, 42-mul, 43-bru/bog, 45-add, 45-dul, 46-kre/now, 47-rei/dem, 47-sho/pri, 48-jon/bow, 48-vog-2, 48-wei, 48-zas, 49-dre/mar, 49-gri/chu, 49-hat, 49-hat-1, 49-hat-2, 49-kre/wie-1, 49-tsc/ric, 49-tsv/mar, 49-vve/iva, 50-jac, 50-pic/zie, 50-sac/sau, 50-tei/gor, 50-vie, 50-wol/sau, 51-tei/gor, 52-gri, 52-hug/mal, 52-kip/tes, 52-sta/spi, 53-ame/pax, 53-ani, 53-ani-1, 53-bar-5, 53-bar/bro, 53-cha/mou, 53-kha/kud, 53-mck/tar, 53-ots/wil, 54-gri, 54-pur/bow, 54-smi/otv, 54-tha/row, 55-fle/sau, 55-ham/sto, 56-ame/pax, 56-fai/win, 56-kat/new, 58-ano-5, 58-lin/van, 58-muk/gru, 58-mur/van, 58-oga/tak, 58-wag/web, 59-bar/dod, 59-mck/ski, 59-nie/web, 60-cop/fin, 60-fro/shr, 60-oak/web, 61-bel/web, 62-bro/smi, 62-kae/web, 63-aga/men, 63-hov/sea, 63-kud/sus-1, 63-mcc/lai, 64-sca/sat, 67-kom/man, 67-mis/sub, 68-ano, 68-kaw/min, 68-pfl/pop, 68-sin/ben, 69-fin/cop, 70-kat/kon, 70-kon/lya, 70-min/kaw, 70-nak/shi, 70-sus/hol, 71-bra/joh, 71-nag/oht, 72-nie/nov, 72-pol/lu, 72-pol/lu -1, 73-khi/ale, 74-dut/mat, 74-mye/cle, 75-mat/fer, 75-mus/ver, 75-tok, 76-for/ben, 76-kat/nit, 76-nag/oht, 76-wes, 77-gup/han, 77-hwa/rob, 77-tan/yam, 77-tre/ben, 78-nit/fuj, 79-cha/ses-1, 79-dia/tar, 79-jim/paz, 79-tho/nag, 80-arc/bla, 80-edu/boy, 80-fuk/ogi, 80-mar/ric, 80-oza/ooy, 80-pik, 80-yos/tak, 80-yu /ish, 81-kum/pa, 81-oht/koy, 81-sjo/dyh, 81-tas/ara, 81-won/chu, 82-diz/mar, 82-dom/rat, 82-ort, 83-alb/edg, 83-fuk/ogi, 83-pik-1, 83-pik-2, 83-rau/ste, 83-tri, 84-sak/nak, 85-dri/ras, 85-kov/svo, 85-mat/ben, 85-mat/ben-1, 85-nag, 85-nag-3, 85-ogi/ara, 85-ort/paz-1, 86-lep/mat, 86-miy/hay, 86-ort/pen, 86-san/sha, 86-tan/toy, 86-zha/ben-1, 87-ber-1, 87-ber-8, 87-ber-9, 87-kub/tan, 87-mou, 87-oga/mur, 87-ogi/ara, 87-pap/pap, 88-nag-4, 89-ala/sal, 89-kac/rad]

cont.



**Ethanol** (cont.)**Further references:** (cont.)

[89-kat/tan, 89-kat/tan-1, 89-kou/pan, 89-nao/sur, 89-ort/sus, 89-sol/mar, 89-sus/ort, 90-cha/kat, 90-let/sch-1, 90-siv/rao, 91-cab/bel, 91-gar/her, 91-kat/tan, 91-pap/eva, 91-pap/zia, 91-pap/zio, 91-ram/muk, 91-vro/noo, 92-hia/yam, 92-lee/wei, 93-ami/ara, 94-hia/tak-1, 94-kim/lee, 94-pap/pan, 94-pap/pan-1, 94-sol/bar, 95-arc/bla, 95-hia/tak-1, 96-elb, 96-nik/jad, 96-nik/mah, 97-com/fra, 98-ami/ban, 98-ami/pat-1, 98-arc/mar, 98-arc/nar, 98-igl/org, 98-nik/shi, 98-zie].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
190.00	879.47 ± 0.19	298.15	785.15 ± 0.10	410.00	670.34 ± 0.81
200.00	870.01 ± 0.16	300.00	783.55 ± 0.10	420.00	654.76 ± 1.03
210.00	860.83 ± 0.14	310.00	774.84 ± 0.11	430.00	638.22 ± 1.35
220.00	851.87 ± 0.12	320.00	765.95 ± 0.13	440.00	621.16 ± 1.59
230.00	843.10 ± 0.11	330.00	756.85 ± 0.15	450.00	603.43 ± 2.24
240.00	834.47 ± 0.10	340.00	747.49 ± 0.18	460.00	584.26 ± 2.72
250.00	825.95 ± 0.09	350.00	737.85 ± 0.20	470.00	562.34 ± 3.83
260.00	817.50 ± 0.08	360.00	727.87 ± 0.24	480.00	535.74 ± 4.03
270.00	809.07 ± 0.08	370.00	717.53 ± 0.27	490.00	501.66 ± 5.42
280.00	800.63 ± 0.08	380.00	706.77 ± 0.31	500.00	455.47 ± 8.47
290.00	792.14 ± 0.09	390.00	695.56 ± 0.46	510.00	383.00 ± 11.63
293.15	789.45 ± 0.09	400.00	683.86 ± 0.61		

**1-Propanol****[71-23-8]****C<sub>3</sub>H<sub>8</sub>O****MW = 60.1****3** $T_c = 536.70 \text{ K}$  [89-tej/lee] $\rho_c = 275.00 \text{ kg} \cdot \text{m}^{-3}$  [89-tej/lee]

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_i = 5.7712 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (3.4844 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 2.0066 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 150.00 \text{ to } 410.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 410.00 \text{ to } 536.70 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$1.01077 \cdot 10^3$	1.19032
B	$-3.99649 \cdot 10^{-5}$	$-1.74429 \cdot 10^{-2}$
C	$-6.64923 \cdot 10^{-3}$	$1.13720 \cdot 10^{-4}$
D	$2.16751 \cdot 10^{-5}$	$-2.75663 \cdot 10^{-7}$
E	$-2.46167 \cdot 10^{-8}$	

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	819.28 ± 0.10	-0.08	51-kre(X)	328.20	774.64 ± 1.50	-0.54	51-kre <sup>1)</sup>
288.02	807.55 ± 0.10	-0.09	51-kre <sup>1)</sup>	330.62	772.55 ± 1.50	-0.58	51-kre <sup>1)</sup>
298.12	799.50 ± 0.10	-0.15	51-kre <sup>1)</sup>	333.31	770.22 ± 1.50	-0.62	51-kre <sup>1)</sup>
308.05	791.47 ± 0.10	-0.25	51-kre <sup>1)</sup>	335.56	768.25 ± 1.50	-0.66	51-kre <sup>1)</sup>
318.18	783.12 ± 0.10	-0.38	51-kre(X)	338.23	765.89 ± 1.50	-0.71	51-kre <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

## 1-Propanol (cont.)

Table 2. (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
348.15	756.89 ± 1.50	-0.93	51-kre <sup>1)</sup>	233.15	850.50 ± 0.40	-0.78	67-kom/man(✕)
273.15	819.30 ± 0.50	-0.06	58-cos/bow <sup>1)</sup>	243.15	842.70 ± 0.40	-0.49	67-kom/man(✕)
293.15	803.50 ± 0.50	-0.09	58-cos/bow <sup>1)</sup>	253.15	834.90 ± 0.40	-0.28	67-kom/man(✕)
313.15	787.50 ± 0.50	-0.10	58-cos/bow <sup>1)</sup>	263.15	826.80 ± 0.40	-0.45	67-kom/man <sup>1)</sup>
333.15	770.00 ± 0.50	-0.98	58-cos/bow <sup>1)</sup>	273.15	819.00 ± 0.30	-0.36	67-kom/man <sup>1)</sup>
353.15	752.00 ± 0.50	-1.25	58-cos/bow <sup>1)</sup>	283.15	811.10 ± 0.30	-0.38	67-kom/man <sup>1)</sup>
373.15	732.50 ± 0.50	-1.33	58-cos/bow <sup>1)</sup>	293.15	803.20 ± 0.30	-0.39	67-kom/man <sup>1)</sup>
393.15	711.00 ± 0.60	-1.04	58-cos/bow <sup>1)</sup>	298.15	799.50 ± 0.30	-0.13	67-kom/man <sup>1)</sup>
413.15	687.50 ± 0.60	0.38	58-cos/bow(✕)	303.15	795.96 ± 0.04	0.31	74-rao/nai-1(Δ)
433.15	660.00 ± 0.80	0.73	58-cos/bow(✕)	293.15	803.61 ± 0.20	0.02	76-hal/ell <sup>1)</sup>
453.15	628.50 ± 1.00	-0.43	58-cos/bow(✕)	298.15	799.60 ± 0.20	-0.03	76-hal/ell <sup>1)</sup>
473.15	592.00 ± 1.00	-1.97	58-cos/bow(✕)	303.15	795.61 ± 0.20	-0.04	76-hal/ell <sup>1)</sup>
493.15	548.50 ± 1.00	-0.97	58-cos/bow(✕)	320.00	781.71 ± 0.20	-0.29	76-hal/ell <sup>1)</sup>
273.15	819.47 ± 0.10	0.11	59-mck/ski(✕)	340.00	764.40 ± 0.20	-0.66	76-hal/ell(✕)
293.15	803.50 ± 0.30	-0.09	63-amb/tow <sup>1)</sup>	360.00	745.71 ± 0.20	-1.11	76-hal/ell(✕)
414.80	687.50 ± 0.50	2.59	63-amb/tow(✕)	380.00	725.26 ± 0.20	-1.41	76-hal/ell <sup>1)</sup>
427.33	670.00 ± 0.50	2.39	63-amb/tow(✕)	400.00	702.59 ± 0.20	-1.31	76-hal/ell <sup>1)</sup>
439.00	653.30 ± 0.50	2.60	63-amb/tow(✕)	420.00	677.31 ± 0.30	-0.53	76-hal/ell(✕)
450.08	635.00 ± 0.50	1.19	63-amb/tow(✕)	440.00	648.88 ± 0.30	-0.33	76-hal/ell(✕)
459.44	620.40 ± 0.50	1.79	63-amb/tow(✕)	460.00	616.11 ± 0.40	-1.56	76-hal/ell(✕)
465.92	607.70 ± 0.50	0.31	63-amb/tow(✕)	470.00	597.88 ± 0.50	-2.07	76-hal/ell(✕)
474.16	592.30 ± 0.50	0.29	63-amb/tow(✕)	483.83	571.43 ± 0.50	-0.40	76-hal/ell(✕)
479.55	581.60 ± 0.50	0.51	63-amb/tow(✕)	303.15	795.93 ± 0.10	0.28	78-red/nai-1 <sup>1)</sup>
498.27	537.60 ± 1.00	1.99	63-amb/tow(✕)	313.15	787.62 ± 0.10	0.02	78-red/nai-1(✕)
505.69	516.60 ± 2.00	3.60	63-amb/tow(✕)	298.15	799.91 ± 0.15	0.28	79-dia/tar <sup>1)</sup>
513.26	499.20 ± 2.00	13.23	63-amb/tow <sup>1)</sup>	308.15	791.85 ± 0.15	0.21	79-dia/tar <sup>1)</sup>
518.48	472.40 ± 3.00	8.21	63-amb/tow(✕)	318.15	783.59 ± 0.15	0.07	79-dia/tar <sup>1)</sup>
523.37	449.90 ± 5.00	9.44	63-amb/tow(✕)	333.15	770.80 ± 0.15	-0.18	79-dia/tar(✕)
527.76	426.70 ± 5.00	11.75	63-amb/tow <sup>1)</sup>	298.15	799.57 ± 0.02	-0.06	79-kiy/ben(□)
529.84	412.70 ± 5.00	12.07	63-amb/tow <sup>1)</sup>	288.15	807.40 ± 0.05	-0.14	80-ben/kiy(◆)
323.15	779.50 ± 0.20	0.10	63-brz/har <sup>1)</sup>	293.15	803.49 ± 0.05	-0.10	80-ben/kiy(◆)
333.15	771.30 ± 0.20	0.32	63-brz/har <sup>1)</sup>	298.15	799.35 ± 0.05	-0.28	80-ben/kiy <sup>1)</sup>
343.15	763.70 ± 0.20	1.41	63-brz/har(✕)	303.15	795.47 ± 0.05	-0.18	80-ben/kiy(◆)
153.15	917.00 ± 0.70	-2.12	67-kom/man <sup>1)</sup>	308.15	791.41 ± 0.05	-0.23	80-ben/kiy(◆)
163.15	908.00 ± 0.70	-2.46	67-kom/man <sup>1)</sup>	303.15	796.00 ± 0.05	0.35	81-nar/dha(∇)
173.15	899.60 ± 0.60	-2.21	67-kom/man <sup>1)</sup>	150.00	922.70 ± 0.18	0.85	82-zak(✕)
183.15	890.80 ± 0.60	-2.38	67-kom/man <sup>1)</sup>	150.00	922.70 ± 0.18	0.85	82-zak(✕)
193.15	882.50 ± 0.60	-2.12	67-kom/man <sup>1)</sup>	170.00	903.50 ± 0.18	-1.03	82-zak(✕)
203.15	874.50 ± 0.50	-1.64	67-kom/man(✕)	170.00	903.60 ± 0.18	-0.93	82-zak(✕)
213.15	866.80 ± 0.50	-0.96	67-kom/man <sup>1)</sup>	190.00	886.50 ± 0.18	-0.81	82-zak(✕)
223.15	858.70 ± 0.50	-0.77	67-kom/man(✕)	190.00	886.60 ± 0.18	-0.71	82-zak(✕)

<sup>1)</sup> Not included in Fig. 1.

cont.

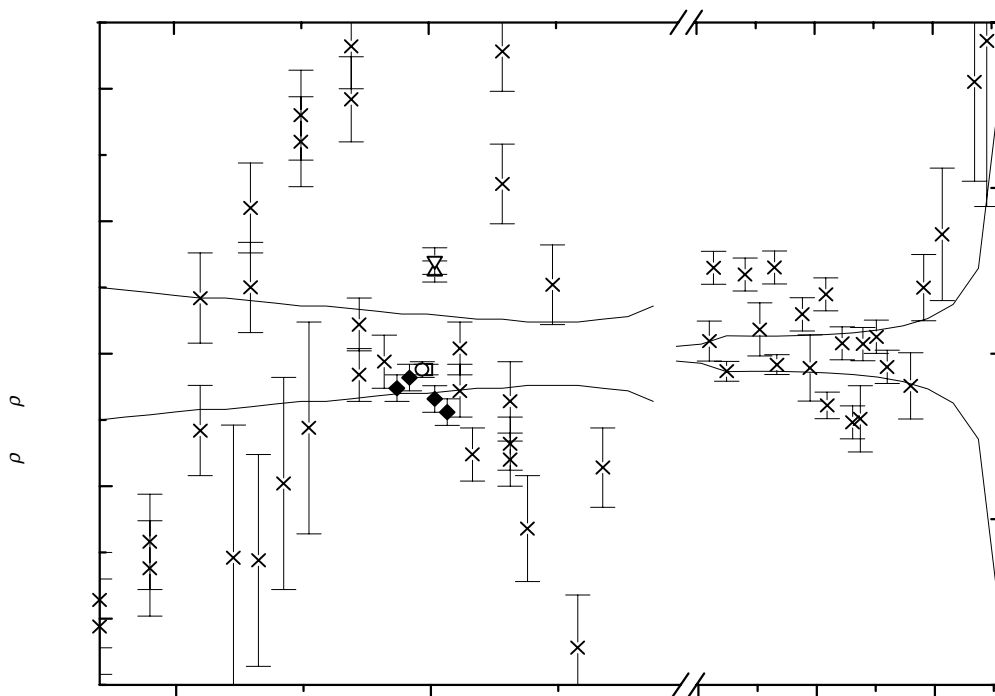
**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
210.00	870.60 ± 0.17	0.21	82-zak(✕)	350.00	757.60 ± 0.15	1.46	82-zak(✕)
210.00	870.10 ± 0.17	-0.29	82-zak(✕)	350.00	756.40 ± 0.15	0.26	82-zak(✕)
230.00	854.40 ± 0.17	0.55	82-zak(✕)	370.00	739.60 ± 0.15	2.57	82-zak <sup>1)</sup>
230.00	854.10 ± 0.17	0.25	82-zak(✕)	370.00	736.60 ± 0.15	-0.43	82-zak(✕)
250.00	838.50 ± 0.17	0.80	82-zak(✕)	283.15	811.45 ± 0.10	-0.03	86-hei/sch(✕)
250.00	838.60 ± 0.17	0.90	82-zak(✕)	298.15	799.63 ± 0.10	-0.00	86-hei/sch <sup>1)</sup>
270.00	823.00 ± 0.16	1.16	82-zak(✕)	313.15	787.46 ± 0.10	-0.14	86-hei/sch(✕)
270.00	822.80 ± 0.16	0.96	82-zak(✕)	298.15	799.57 ± 0.03	-0.06	86-oga/mur(○)
290.00	807.20 ± 0.16	1.12	82-zak <sup>1)</sup>	293.15	803.78 ± 0.10	0.19	86-wag/hei <sup>1)</sup>
290.00	807.30 ± 0.16	1.22	82-zak <sup>1)</sup>	298.15	799.81 ± 0.10	0.18	86-wag/hei <sup>1)</sup>
310.00	791.40 ± 0.16	1.25	82-zak <sup>1)</sup>	333.15	770.58 ± 0.10	-0.40	86-wag/hei(✕)
310.00	791.10 ± 0.16	0.95	82-zak <sup>1)</sup>	303.15	795.61 ± 0.10	-0.04	87-pik <sup>1)</sup>
330.00	774.30 ± 0.15	0.64	82-zak(✕)	333.15	770.64 ± 0.10	-0.34	87-pik(✕)
330.00	774.80 ± 0.15	1.14	82-zak(✕)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1864-lan, 1871-ros, 1872-lin/von, 1879-bru, 1880-bru-3, 1881-nac/pag, 1882-sch-1, 1882-zan, 1883-sch-3, 1884-per, 1884-sch-6, 1884-zan, 1886-tra, 1889-ram/you, 1890-gar, 1891-jah, 1891-sch/kos, 1892-lan/jah, 1892-sch-1, 1893-eyk-1, 1894-sch, 1898-kah, 1898-lou, 1898-roh, 00-loo, 02-you/for, 05-dun, 08-dor/dvo, 08-ric/mat, 09-dor, 09-dor/roz, 09-hol/sag, 10-dor/pol, 10-dor/pol-1, 10-tim, 11-dor, 12-sch-2, 12-wre, 13-atk/wal, 13-bri-1, 14-eng/tur, 14-kre/mei, 14-low, 16-wro/rei, 17-jae, 18-her-2, 19-eyk, 21-bru/cre, 21-rei/hic, 23-bru, 23-tim, 23-wil/smi, 24-par/sch, 25-nor/ash, 25-pal/con, 25-per, 26-han, 26-mun, 26-par/huf, 26-sch, 27-mou/duf, 28-llo/bro, 29-ber, 30-bil/fis-1, 33-azi/bha, 33-but/tho, 33-kil, 33-tre/wat, 33-vos/con, 34-tim/del, 35-bra/fel, 35-cou/hop, 35-hen, 36-spe, 36-tom, 39-lar/hun, 42-mul, 42-was/bro, 45-add, 48-vog-2, 48-wei, 49-hat, 49-tsc/ric, 49-tsv/mar, 50-jac, 50-mum/phi, 50-pic/zie, 50-sac/sau, 50-tei/gor, 51-dim/lan, 51-tei/gor, 52-coo, 53-ani, 53-ani-1, 53-mcc/jon, 54-pur/bow, 55-bak, 57-mal/mal, 57-rom, 58-lin/van, 58-mur/van, 59-ale, 60-cop/fin, 61-ogi/cor, 62-bro/smi, 62-chu/tho, 62-par/mis, 63-gol/bag, 63-hov/sea, 63-mcc/lai, 63-mik/kim, 63-pra/van, 64-ska/kay, 65-fin/kid, 66-gur/raj, 66-kil/che, 67-gol/per, 68-ano, 68-joh, 68-pfl/pop, 69-bro/foc, 69-fin/cop, 69-smi/kur, 70-gur/raj, 70-kri/kom, 70-str/svo, 72-nie/nov, 72-udo/kas, 73-daw/new, 73-svo/ves, 74-dut/mat, 74-rao/nai, 75-mat/fer, 75-tok, 76-for/ben, 76-kat/nit, 76-kow/kas, 76-nag/oht, 76-red/nai, 76-wes-1, 77-hwa/rob, 77-tre/ben, 78-dap/don, 79-cha/ses-1, 79-ern/gli, 79-jim/paz, 80-arc/bla, 80-fuk/ogi, 80-yos/tak, 81-kum/pra, 81-nai/nai, 81-sjo/dyh, 81-tas/ara, 81-won/chu, 82-diz/mar, 82-kar/red, 82-nai/nai, 82-ort, 82-ven/dha, 83-fuk/ogi, 83-pik-1, 83-pik-2, 83-rau/ste, 83-tri, 84-sak/nak, 85-fer/ber, 85-fer/pin, 85-mat/ben, 85-mat/ben-1, 85-nag-2, 85-ort/paz-1, 85-ped/dav, 85-zhu/dur, 86-ash/sri, 86-ber/wec-1, 86-lep/mat, 86-mah/daw, 86-miy/hay, 86-san/sha, 86-tan/toy, 87-ber-2, 87-ber-3, 87-kub/tan, 87-oga/mur, 87-rat/sin-3, 88-jad/fra, 88-nag-2, 88-ort/mat, 89-ala/sal, 89-nao/sur, 89-ort/sus, 89-pae/con, 89-sus/ort, 90-cha/kat, 90-sri/nai, 91-cab/bel, 91-gar/her, 91-kat/tan, 91-ram/muk, 92-kum/sre, 93-ami/ara, 94-hia/tak, 94-hia/tak-1, 94-kim/lee, 94-pap/pan, 94-pap/pan-1, 94-rom/pel, 94-sin/kal, 94-ven/ven, 95-hia/tak, 95-hia/tak-1, 95-red/ram-1, 96-elb, 96-nik/jad, 96-nik/mah, 97-com/fra, 98-ami/ban, 98-ami/pat-1, 98-nik/shi, 98-pal/sha].

cont.

**1-Propanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
150.00	921.85 ± 0.27	290.00	806.08 ± 0.15	410.00	691.28 ± 0.29
160.00	913.19 ± 0.26	293.15	803.59 ± 0.15	420.00	677.84 ± 0.54
170.00	904.53 ± 0.25	298.15	799.63 ± 0.15	430.00	663.81 ± 0.53
180.00	895.89 ± 0.24	300.00	798.16 ± 0.15	440.00	649.21 ± 0.53
190.00	887.31 ± 0.23	310.00	790.15 ± 0.14	450.00	633.93 ± 0.55
200.00	878.81 ± 0.22	320.00	782.00 ± 0.13	460.00	617.67 ± 0.58
210.00	870.39 ± 0.21	330.00	773.66 ± 0.13	470.00	599.95 ± 0.63
220.00	862.07 ± 0.21	340.00	765.06 ± 0.12	480.00	580.14 ± 0.71
230.00	853.85 ± 0.20	350.00	756.14 ± 0.12	490.00	557.41 ± 0.84
240.00	845.73 ± 0.19	360.00	746.82 ± 0.12	500.00	530.62 ± 1.06
250.00	837.70 ± 0.18	370.00	737.03 ± 0.13	510.00	498.18 ± 1.49
260.00	829.74 ± 0.18	380.00	726.67 ± 0.14	520.00	457.21 ± 2.58
270.00	821.84 ± 0.17	390.00	715.66 ± 0.18	530.00	399.44 ± 8.86
280.00	813.96 ± 0.16	400.00	703.90 ± 0.22		

**2- Propanol****[67-63-0]****C<sub>3</sub>H<sub>8</sub>O****MW = 60.1****4** $T_c = 508.00 \text{ K}$  [89-tej/lee] $\rho_c = 273.00 \text{ kg}\cdot\text{m}^{-3}$  [89-tej/lee]**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_T = 9.7228 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (9.9994 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 5.4125 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 213.15 \text{ to } 400.00 \text{ K}$	$T = 400.00 \text{ to } 508.00 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$	$\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$9.93868 \cdot 10^2$	1.42642
B	$-3.40464 \cdot 10^{-5}$	$-2.55851 \cdot 10^{-2}$
C	$-6.95191 \cdot 10^{-3}$	$2.00711 \cdot 10^{-4}$
D	$2.40158 \cdot 10^{-5}$	$-5.71341 \cdot 10^{-7}$
E	$-2.92637 \cdot 10^{-8}$	

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
303.15	$778.60 \pm 0.45$	1.70	33-azi/bha <sup>1)</sup>	443.72	$595.70 \pm 0.50$	-1.33	63-amb/tow(✗)
313.15	$769.80 \pm 0.45$	1.59	33-azi/bha <sup>1)</sup>	450.70	$581.50 \pm 0.50$	-2.04	63-amb/tow(✗)
323.15	$761.70 \pm 0.45$	2.50	33-azi/bha <sup>1)</sup>	458.45	$564.00 \pm 0.50$	-3.06	63-amb/tow(✗)
333.15	$750.90 \pm 0.45$	1.11	33-azi/bha(✗)	465.13	$548.00 \pm 0.50$	-3.12	63-amb/tow(✗)
297.97	$781.04 \pm 0.10$	-0.25	45-kol/bur(Δ)	469.84	$535.70 \pm 0.50$	-2.93	63-amb/tow(✗)
298.15	$781.48 \pm 0.10$	0.34	54-tha/row(∇)	474.89	$522.20 \pm 1.00$	-1.60	63-amb/tow(✗)
293.15	$785.50 \pm 0.20$	0.17	56-tor-1 <sup>1)</sup>	480.40	$505.50 \pm 1.00$	-0.06	63-amb/tow(✗)
313.15	$768.40 \pm 0.20$	0.19	56-tor-1(✗)	486.34	$485.20 \pm 1.00$	2.37	63-amb/tow(✗)
333.15	$749.70 \pm 0.20$	-0.09	56-tor-1(✗)	491.20	$465.80 \pm 1.00$	4.68	63-amb/tow(✗)
213.15	$849.10 \pm 0.50$	-1.08	58-cos/bow(✗)	495.79	$441.80 \pm 1.00$	4.75	63-amb/tow(✗)
233.15	$834.10 \pm 0.50$	0.24	58-cos/bow(✗)	500.43	$416.50 \pm 1.00$	9.31	63-amb/tow(✗)
253.15	$818.30 \pm 0.50$	0.53	58-cos/bow(✗)	504.22	$384.90 \pm 1.00$	10.32	63-amb/tow(✗)
273.15	$802.70 \pm 0.50$	0.99	58-cos/bow(✗)	506.68	$349.30 \pm 1.00$	7.80	63-amb/tow(✗)
293.15	$786.20 \pm 0.40$	0.87	58-cos/bow <sup>1)</sup>	300.00	$779.00 \pm 1.00$	-0.58	64-dan/bah <sup>1)</sup>
313.15	$768.80 \pm 0.40$	0.59	58-cos/bow <sup>1)</sup>	320.00	$763.00 \pm 1.00$	0.92	64-dan/bah <sup>1)</sup>
333.15	$750.20 \pm 0.50$	0.41	58-cos/bow <sup>1)</sup>	340.00	$745.00 \pm 1.00$	1.93	64-dan/bah <sup>1)</sup>
353.15	$730.30 \pm 0.50$	0.88	58-cos/bow(✗)	360.00	$724.00 \pm 1.00$	2.15	64-dan/bah <sup>1)</sup>
373.15	$708.00 \pm 0.60$	1.69	58-cos/bow(✗)	380.00	$702.00 \pm 1.00$	4.39	64-dan/bah <sup>1)</sup>
393.15	$683.00 \pm 0.60$	3.43	58-cos/bow(✗)	400.00	$676.00 \pm 1.50$	6.59	64-dan/bah <sup>1)</sup>
413.15	$656.50 \pm 0.60$	7.69	58-cos/bow(✗)	420.00	$648.00 \pm 1.50$	10.24	64-dan/bah <sup>1)</sup>
433.15	$626.40 \pm 0.60$	10.54	58-cos/bow(✗)	440.00	$619.00 \pm 1.50$	15.16	64-dan/bah(✗)
293.15	$785.11 \pm 0.10$	-0.22	59-bar/dod(○)	460.00	$585.00 \pm 1.50$	21.47	64-dan/bah(✗)
407.35	$660.50 \pm 0.50$	2.49	63-amb/tow(✗)	480.00	$541.00 \pm 2.00$	34.03	64-dan/bah <sup>1)</sup>
422.33	$635.30 \pm 0.50$	1.34	63-amb/tow(✗)	500.00	$470.00 \pm 2.00$	59.70	64-dan/bah <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

## 2- Propanol (cont.)

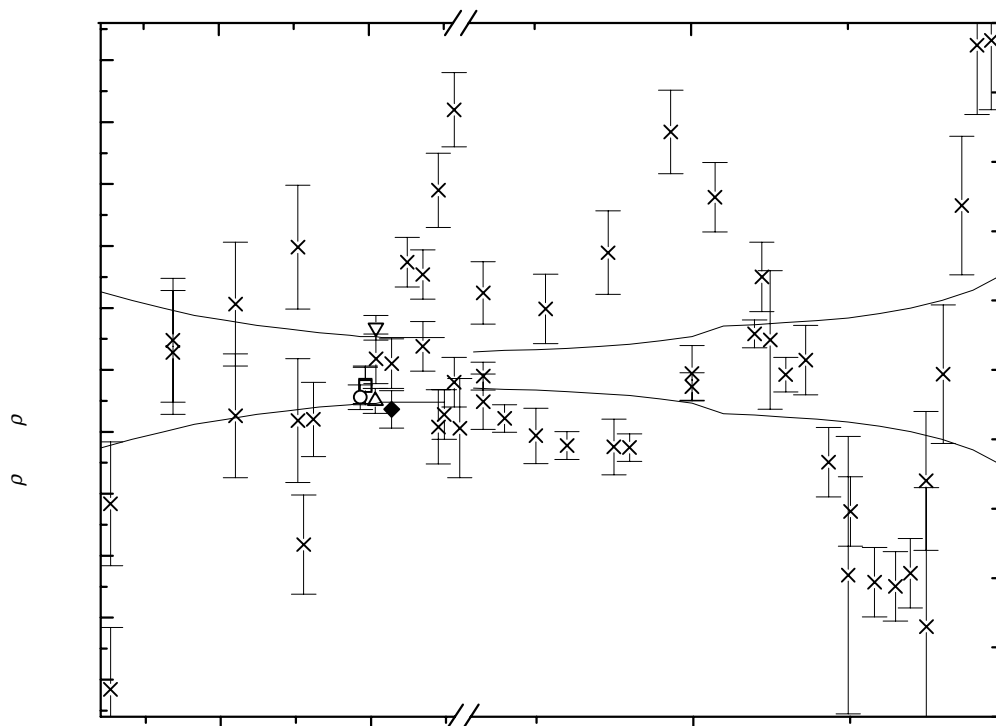
Table 2. (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
436.38	610.40 ± 0.50	0.14	63-amb/tow(✕)	313.15	768.98 ± 0.20	0.77	66-kat/shi(✕)
298.15	780.93 ± 0.20	-0.21	76-hal/ell <sup>1)</sup>	303.15	776.56 ± 0.15	-0.34	83-pik-2(◆)
303.15	776.75 ± 0.20	-0.15	76-hal/ell <sup>1)</sup>	298.15	781.02 ± 0.15	-0.12	83-wec/byl(□)
320.00	761.72 ± 0.20	-0.36	76-hal/ell(✕)	298.15	781.01 ± 0.15	-0.13	83-wec/byl(□)
340.00	742.37 ± 0.20	-0.70	76-hal/ell(✕)	298.15	781.70 ± 0.30	0.56	87-isl/qua <sup>1)</sup>
360.00	720.76 ± 0.20	-1.09	76-hal/ell(✕)	303.15	777.60 ± 0.30	0.70	87-isl/qua <sup>1)</sup>
380.00	696.49 ± 0.20	-1.12	76-hal/ell(✕)	308.15	773.50 ± 0.30	0.91	87-isl/qua <sup>1)</sup>
400.00	669.17 ± 0.20	-0.24	76-hal/ell(✕)	313.15	769.30 ± 0.30	1.09	87-isl/qua <sup>1)</sup>
420.00	638.28 ± 0.20	0.52	76-hal/ell(✕)	318.15	765.20 ± 0.30	1.45	87-isl/qua(✕)
430.00	621.15 ± 0.25	-0.07	76-hal/ell(✕)	323.15	761.30 ± 0.30	2.10	87-isl/qua(✕)
213.15	847.60 ± 0.50	-2.58	76-kat/nit(✕)	303.15	776.59 ± 0.40	-0.31	87-pik <sup>1)</sup>
233.15	834.00 ± 0.50	0.14	76-kat/nit(✕)	333.15	749.33 ± 0.40	-0.46	87-pik(✕)
253.15	817.40 ± 0.50	-0.37	76-kat/nit(✕)	278.15	797.26 ± 0.30	-0.40	88-sak(✕)
273.15	801.30 ± 0.50	-0.41	76-kat/nit(✕)	288.15	798.13 ± 0.30	8.65	88-sak <sup>1)</sup>
275.00	798.80 ± 0.40	-1.41	78-amb/cou-1(✕)	298.15	780.80 ± 0.30	-0.34	88-sak <sup>1)</sup>
300.00	779.55 ± 0.40	-0.03	78-amb/cou-1 <sup>1)</sup>	308.15	772.20 ± 0.30	-0.39	88-sak <sup>1)</sup>
325.00	757.02 ± 0.40	-0.47	78-amb/cou-1(✕)	318.15	763.29 ± 0.30	-0.46	88-sak(✕)
350.00	731.84 ± 0.40	-0.95	78-amb/cou-1(✕)	293.15	785.10 ± 0.30	-0.23	89-pae/con <sup>1)</sup>
375.00	702.89 ± 0.40	-1.11	78-amb/cou-1(✕)	298.15	780.90 ± 0.30	-0.24	89-pae/con <sup>1)</sup>
400.00	669.36 ± 0.40	-0.05	78-amb/cou-1(✕)	303.15	776.70 ± 0.30	-0.20	89-pae/con <sup>1)</sup>
425.00	630.00 ± 1.00	0.43	78-amb/cou-1(✕)	313.15	767.80 ± 0.30	-0.41	89-pae/con <sup>1)</sup>
450.00	581.99 ± 2.00	-2.96	78-amb/cou-1(✕)	323.15	759.10 ± 0.20	-0.10	89-pae/con(✕)
475.00	519.76 ± 2.00	-3.70	78-amb/cou-1(✕)	298.15	781.23 ± 0.20	0.09	98-nik/shi(✕)
500.00	425.22 ± 5.00	14.92	78-amb/cou-1 <sup>1)</sup>	303.15	776.95 ± 0.20	0.05	98-nik/shi(✕)
508.30	273.17 ± 0.00	5.23	78-amb/cou-1 <sup>1)</sup>	308.15	773.46 ± 0.20	0.87	98-nik/shi(✕)

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1880-bru-1, 1883-sch-3, 21-bru/cre, 21-leb, 23-bru, 25-nor/ash, 25-par/kel, 26-mat, 26-mun, 28-par/kel, 29-kel, 35-but/ram, 38-ols/was, 39-lar/hun, 39-par/moo, 44-ira, 46-kre/now, 50-par/gol, 52-cap/mug, 53-ani-1, 53-par/cha, 56-goe/mcc, 58-ano-5, 58-mur/van, 59-bur/can, 61-ogi/cor, 62-chu/tho, 63-pra/van-1, 65-fin/kid, 66-kat/pra-1, 67-fre, 67-gol/per, 68-ano, 68-ver, 69-kom/kri, 69-ver/lau, 70-ver, 71-nag/oht, 73-nag/oht, 74-pur/pol, 75-tok, 76-nag/oht, 76-sri/kul, 80-edu/boy, 80-kas/izy, 80-yos/tak, 82-kar/red, 82-ven/dha, 83-fuk/ogi, 83-tri, 83-wec, 84-ped/sal, 85-dri/ras, 85-mat/ben, 85-mat/ben-1, 85-nag-1, 85-rao/red, 86-ber/wec, 86-hne/cib, 86-mou/nai, 87-ber-1, 87-ber-4, 88-nag-1, 89-kat/tan, 89-nao/sur, 91-ace/ped-1, 91-kat/tan, 92-ard/say-1, 92-kum/sre, 94-hia/tak, 94-sin/kal, 95-hia/tak, 96-nik/jad, 96-nik/mah].

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
210.00	852.78 ± 0.63	300.00	779.58 ± 0.26	410.00	653.83 ± 0.63
220.00	844.56 ± 0.56	310.00	770.98 ± 0.26	420.00	637.76 ± 0.65
230.00	836.41 ± 0.50	320.00	762.08 ± 0.26	430.00	621.22 ± 0.68
240.00	828.33 ± 0.44	330.00	752.80 ± 0.26	440.00	603.84 ± 0.71
250.00	820.30 ± 0.40	340.00	743.07 ± 0.28	450.00	584.95 ± 0.75
260.00	812.28 ± 0.36	350.00	732.79 ± 0.29	460.00	563.53 ± 0.81
270.00	804.25 ± 0.33	360.00	721.85 ± 0.31	470.00	538.18 ± 0.89
280.00	796.15 ± 0.30	370.00	710.16 ± 0.34	480.00	506.97 ± 1.00
290.00	787.95 ± 0.28	380.00	697.61 ± 0.37	490.00	466.79 ± 1.15
293.15	785.33 ± 0.27	390.00	684.06 ± 0.42	500.00	410.30 ± 1.39
298.15	781.14 ± 0.27	400.00	669.41 ± 0.48		



**1-Butanol****[71-36-3]****C<sub>4</sub>H<sub>10</sub>O****MW = 74.12****5** $T_c = 562.40$  K [89-tej/lee] $\rho_c = 270.00$  kg·m<sup>-3</sup> [89-tej/lee]**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_t = 3.7574 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (5.9442 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 4.3091 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 192.35$ to $420.00$ K $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 420.00$ to $562.40$ K $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
<i>A</i>	$1.15309 \cdot 10^3$	1.16613
<i>B</i>	-2.13475	$-1.80981 \cdot 10^{-2}$
<i>C</i>	$5.15573 \cdot 10^{-3}$	$1.25770 \cdot 10^{-4}$
<i>D</i>	$-6.38112 \cdot 10^{-6}$	$-3.17257 \cdot 10^{-7}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
	<i>crystal</i>			197.57	$882.41 \pm 0.30$	-0.95	31-ton/ueh(X)
78.15	$1030.0 \pm 5.0$		30-bilfis-1	204.09	$877.29 \pm 0.30$	-0.62	31-ton/ueh(X)
	<i>liquid</i>			217.71	$866.76 \pm 0.30$	-0.09	31-ton/ueh(X)
273.15	$824.70 \pm 0.20$	0.09	28-tim/mar(X)	217.82	$866.54 \pm 0.30$	-0.23	31-ton/ueh(X)
288.15	$813.35 \pm 0.20$	-0.02	28-tim/mar <sup>1)</sup>	227.45	$859.32 \pm 0.30$	0.14	31-ton/ueh(X)
303.15	$802.04 \pm 0.20$	0.07	28-tim/mar <sup>1)</sup>	233.70	$854.48 \pm 0.20$	0.15	31-ton/ueh(X)
193.15	$887.20 \pm 0.50$	0.08	29-smy/sto(X)	234.79	$853.49 \pm 0.20$	-0.00	31-ton/ueh(X)
203.15	$879.30 \pm 0.50$	0.61	29-smy/sto(X)	235.45	$853.05 \pm 0.20$	0.06	31-ton/ueh(X)
213.15	$871.30 \pm 0.50$	0.79	29-smy/sto(X)	240.28	$849.36 \pm 0.20$	0.07	31-ton/ueh(X)
223.15	$863.40 \pm 0.50$	0.85	29-smy/sto <sup>1)</sup>	249.85	$841.97 \pm 0.20$	-0.07	31-ton/ueh(X)
233.15	$855.60 \pm 0.50$	0.84	29-smy/sto <sup>1)</sup>	255.01	$838.52 \pm 0.20$	0.36	31-ton/ueh(X)
243.15	$847.90 \pm 0.50$	0.79	29-smy/sto <sup>1)</sup>	261.87	$832.64 \pm 0.20$	-0.39	31-ton/ueh(X)
253.15	$840.20 \pm 0.40$	0.64	29-smy/sto(X)	273.15	$823.80 \pm 0.20$	-0.81	31-ton/ueh(X)
263.15	$832.80 \pm 0.40$	0.73	29-smy/sto(X)	273.15	$824.29 \pm 0.20$	-0.32	32-ell/rei(X)
273.15	$825.00 \pm 0.40$	0.39	29-smy/sto <sup>1)</sup>	298.15	$805.61 \pm 0.20$	-0.19	32-ell/rei <sup>1)</sup>
283.15	$817.30 \pm 0.40$	0.17	29-smy/sto <sup>1)</sup>	273.15	$824.60 \pm 0.20$	-0.01	39-jon/chr(X)
293.15	$809.80 \pm 0.40$	0.20	29-smy/sto <sup>1)</sup>	298.15	$805.70 \pm 0.20$	-0.10	39-jon/chr <sup>1)</sup>
303.15	$802.20 \pm 0.40$	0.23	29-smy/sto <sup>1)</sup>	463.15	$625.10 \pm 0.60$	-8.32	55-kay/don(X)
313.15	$794.50 \pm 0.40$	0.28	29-smy/sto <sup>1)</sup>	473.15	$601.90 \pm 0.60$	-16.39	55-kay/don(X)
323.15	$786.70 \pm 0.40$	0.40	29-smy/sto <sup>1)</sup>	483.15	$595.60 \pm 0.60$	-6.95	55-kay/don(X)
333.15	$778.70 \pm 0.40$	0.52	29-smy/sto <sup>1)</sup>	493.15	$575.90 \pm 0.60$	-9.92	55-kay/don(X)
343.15	$770.30 \pm 0.50$	0.49	29-smy/sto <sup>1)</sup>	503.15	$561.80 \pm 0.60$	-5.68	55-kay/don(X)
353.15	$761.60 \pm 0.50$	0.45	29-smy/sto <sup>1)</sup>	513.15	$542.20 \pm 0.70$	-4.54	55-kay/don(X)
363.15	$752.70 \pm 0.50$	0.52	29-smy/sto(X)	523.15	$519.70 \pm 0.70$	-2.83	55-kay/don(X)
192.35	$886.07 \pm 0.30$	-1.74	31-ton/ueh(X)	533.15	$491.70 \pm 0.70$	-1.65	55-kay/don(X)

<sup>1)</sup> Not included in Fig. 1.

cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
543.15	458.50 ± 0.80	1.70	55-kay/don(X)	548.85	436.50 ± 1.00	5.68	63-amb/tow(X)
553.15	414.60 ± 0.90	7.50	55-kay/don(X)	200.00	876.00 ± 1.50	-5.32	64-dan/bah <sup>1)</sup>
562.89	267.00 ± 0.00	? .00	55-kay/don <sup>1)</sup>	220.00	865.00 ± 1.50	-0.03	64-dan/bah <sup>1)</sup>
293.15	809.90 ± 0.30	0.30	55-kus <sup>1)</sup>	240.00	846.00 ± 1.50	-3.51	64-dan/bah <sup>1)</sup>
298.15	806.10 ± 0.30	0.30	55-kus <sup>1)</sup>	260.00	832.00 ± 1.50	-2.43	64-dan/bah <sup>1)</sup>
303.15	802.20 ± 0.30	0.23	55-kus <sup>1)</sup>	280.00	817.00 ± 1.50	-2.49	64-dan/bah <sup>1)</sup>
313.15	794.50 ± 0.30	0.28	55-kus <sup>1)</sup>	300.00	803.00 ± 1.50	-1.39	64-dan/bah <sup>1)</sup>
323.15	786.80 ± 0.30	0.50	55-kus <sup>1)</sup>	320.00	787.00 ± 1.50	-1.82	64-dan/bah <sup>1)</sup>
333.15	778.90 ± 0.30	0.72	55-kus <sup>1)</sup>	340.00	770.00 ± 1.50	-2.47	64-dan/bah <sup>1)</sup>
343.15	770.70 ± 0.40	0.89	55-kus <sup>1)</sup>	360.00	752.00 ± 1.50	-3.04	64-dan/bah <sup>1)</sup>
353.15	762.20 ± 0.40	1.05	55-kus(X)	380.00	732.00 ± 1.50	-4.23	64-dan/bah <sup>1)</sup>
213.15	867.70 ± 0.50	-2.81	58-cos/bow <sup>1)</sup>	400.00	711.00 ± 2.00	-4.71	64-dan/bah <sup>1)</sup>
233.15	852.80 ± 0.50	-1.96	58-cos/bow <sup>1)</sup>	420.00	690.00 ± 2.00	-3.20	64-dan/bah <sup>1)</sup>
253.15	838.20 ± 0.50	-1.36	58-cos/bow <sup>1)</sup>	440.00	663.00 ± 2.00	-4.01	64-dan/bah <sup>1)</sup>
273.15	823.40 ± 0.50	-1.21	58-cos/bow <sup>1)</sup>	460.00	637.00 ± 2.00	-1.11	64-dan/bah <sup>1)</sup>
293.15	808.60 ± 0.40	-1.00	58-cos/bow <sup>1)</sup>	480.00	610.00 ± 2.00	2.40	64-dan/bah <sup>1)</sup>
313.15	793.60 ± 0.40	-0.62	58-cos/bow <sup>1)</sup>	500.00	577.00 ± 2.00	3.52	64-dan/bah <sup>1)</sup>
333.15	779.00 ± 0.50	0.82	58-cos/bow <sup>1)</sup>	520.00	540.00 ± 2.00	9.39	64-dan/bah(X)
353.15	761.60 ± 0.50	0.45	58-cos/bow <sup>1)</sup>	540.00	485.00 ± 2.50	15.67	64-dan/bah(X)
373.15	743.40 ± 0.50	0.55	58-cos/bow(X)	560.00	380.00 ± 6.00	29.03	64-dan/bah <sup>1)</sup>
393.15	723.70 ± 0.50	0.75	58-cos/bow(X)	513.15	548.30 ± 3.00	1.56	64-ska/kay <sup>1)</sup>
413.15	701.60 ± 0.60	0.45	58-cos/bow <sup>1)</sup>	518.15	537.70 ± 3.00	2.55	64-ska/kay <sup>1)</sup>
433.15	678.70 ± 0.60	2.26	58-cos/bow(X)	523.15	526.20 ± 3.00	3.67	64-ska/kay <sup>1)</sup>
443.15	654.50 ± 0.60	-8.07	58-cos/bow(X)	528.15	514.20 ± 3.00	5.52	64-ska/kay <sup>1)</sup>
303.15	802.00 ± 0.30	0.03	58-lin/van <sup>1)</sup>	533.15	501.30 ± 3.00	7.95	64-ska/kay <sup>1)</sup>
328.15	782.90 ± 0.30	0.63	58-lin/van <sup>1)</sup>	538.15	486.80 ± 3.00	10.58	64-ska/kay <sup>1)</sup>
348.15	767.00 ± 0.40	1.48	58-lin/van(X)	543.15	470.00 ± 3.00	13.20	64-ska/kay <sup>1)</sup>
368.15	748.20 ± 0.40	0.64	58-lin/van(X)	548.15	450.00 ± 3.00	15.71	64-ska/kay(X)
273.15	824.59 ± 0.10	-0.02	59-mck/ski(X)	553.15	426.10 ± 3.00	19.00	64-ska/kay(X)
293.15	809.60 ± 0.30	0.00	63-amb/tow <sup>1)</sup>	558.15	391.60 ± 3.00	21.09	64-ska/kay(X)
440.08	669.40 ± 0.50	2.50	63-amb/tow(X)	273.15	826.00 ± 0.50	1.39	66-efr <sup>1)</sup>
451.72	653.80 ± 0.50	3.54	63-amb/tow(X)	293.15	810.00 ± 0.50	0.40	66-efr <sup>1)</sup>
462.05	640.10 ± 0.50	5.04	63-amb/tow(X)	313.15	795.00 ± 0.50	0.78	66-efr <sup>1)</sup>
469.47	627.90 ± 0.50	3.99	63-amb/tow(X)	333.15	779.00 ± 1.00	0.82	66-efr <sup>1)</sup>
475.77	618.20 ± 0.50	3.96	63-amb/tow(X)	353.15	762.00 ± 1.00	0.85	66-efr <sup>1)</sup>
481.90	608.70 ± 1.00	4.13	63-amb/tow(X)	373.15	743.00 ± 1.00	0.15	66-efr <sup>1)</sup>
489.78	595.00 ± 1.00	3.40	63-amb/tow(X)	393.15	723.00 ± 1.00	0.05	66-efr <sup>1)</sup>
499.72	576.40 ± 1.00	2.40	63-amb/tow(X)	413.15	702.00 ± 1.00	0.85	66-efr <sup>1)</sup>
508.23	559.20 ± 1.00	1.89	63-amb/tow(X)	433.15	676.00 ± 1.50	-0.44	66-efr <sup>1)</sup>
515.59	543.70 ± 1.00	2.50	63-amb/tow(X)	453.15	697.00 ± 1.50	48.82	66-efr <sup>1)</sup>
521.20	531.40 ± 1.00	3.81	63-amb/tow(X)	473.15	617.00 ± 1.50	-1.29	66-efr <sup>1)</sup>
530.10	508.00 ± 1.00	5.10	63-amb/tow(X)	493.15	582.00 ± 2.00	-3.82	66-efr <sup>1)</sup>
534.05	489.60 ± 1.00	-0.82	63-amb/tow(X)	513.15	541.00 ± 2.00	-5.74	66-efr <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

## 1-Butanol (cont.)

Table 2. (cont.)

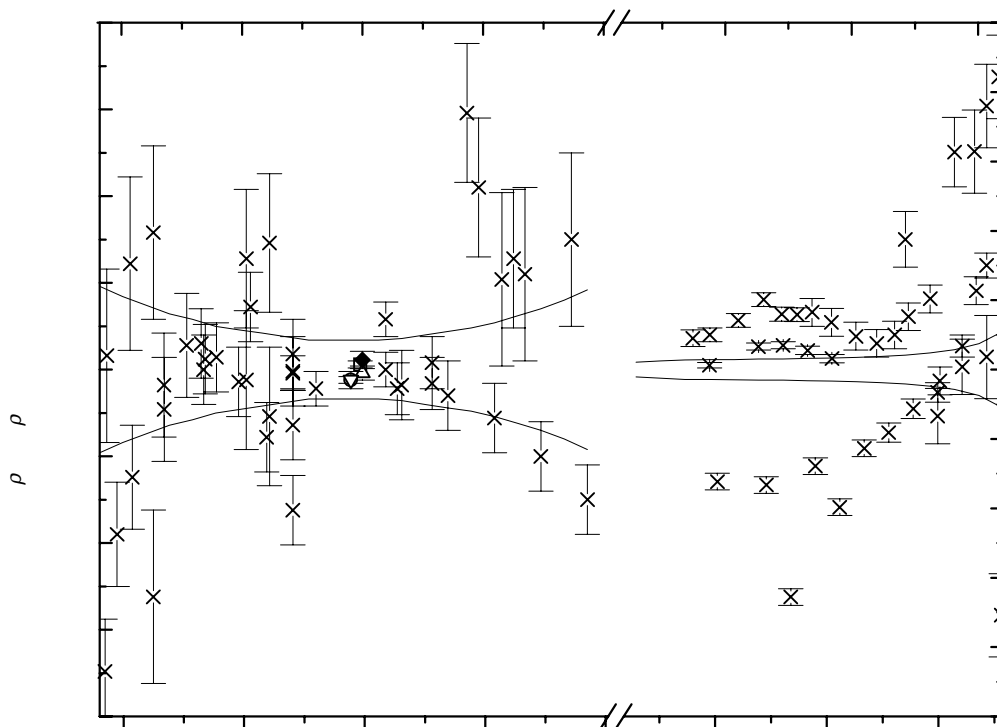
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
533.15	490.00 ± 2.00	-3.35	66-efr(✕)	400.00	714.96 ± 0.20	-0.75	76-hal/ell(✕)
543.15	457.00 ± 2.00	0.20	66-efr(✕)	420.00	692.25 ± 0.20	-0.95	76-hal/ell <sup>1)</sup>
553.15	408.00 ± 3.00	0.90	66-efr(✕)	440.00	667.32 ± 0.20	0.31	76-hal/ell(✕)
559.15	343.00 ± 3.00	-17.71	66-efr(✕)	460.00	639.77 ± 0.25	1.66	76-hal/ell(✕)
560.15	314.00 ± 5.00	-35.06	66-efr <sup>1)</sup>	470.00	624.85 ± 0.25	1.75	76-hal/ell(✕)
186.15	891.20 ± 0.70	-2.00	67-kom/man <sup>1)</sup>	480.00	608.98 ± 0.30	1.38	76-hal/ell(✕)
193.15	885.40 ± 0.70	-1.72	67-kom/man <sup>1)</sup>	490.00	592.03 ± 0.30	0.80	76-hal/ell(✕)
203.15	877.50 ± 0.60	-1.19	67-kom/man <sup>1)</sup>	213.15	869.20 ± 0.50	-1.31	76-kat/nit(✕)
213.15	869.60 ± 0.60	-0.91	67-kom/man <sup>1)</sup>	233.15	853.90 ± 0.50	-0.86	76-kat/nit <sup>1)</sup>
223.15	862.20 ± 0.50	-0.35	67-kom/man <sup>1)</sup>	253.15	839.00 ± 0.50	-0.56	76-kat/nit <sup>1)</sup>
233.15	854.70 ± 0.50	-0.06	67-kom/man <sup>1)</sup>	273.15	824.30 ± 0.50	-0.31	76-kat/nit <sup>1)</sup>
243.15	847.10 ± 0.50	-0.01	67-kom/man <sup>1)</sup>	303.15	802.09 ± 0.10	0.12	78-red/nai-1 <sup>1)</sup>
253.15	839.50 ± 0.40	-0.06	67-kom/man(✕)	313.15	794.51 ± 0.10	0.29	78-red/nai-1(✕)
263.15	831.80 ± 0.40	-0.27	67-kom/man(✕)	298.15	805.84 ± 0.15	0.04	79-dia/tar <sup>1)</sup>
273.15	824.30 ± 0.40	-0.31	67-kom/man <sup>1)</sup>	308.15	798.02 ± 0.15	-0.10	79-dia/tar <sup>1)</sup>
283.15	816.60 ± 0.30	-0.53	67-kom/man <sup>1)</sup>	318.15	790.18 ± 0.15	-0.11	79-dia/tar(✕)
293.15	809.10 ± 0.30	-0.50	67-kom/man <sup>1)</sup>	333.15	778.10 ± 0.15	-0.08	79-dia/tar(✕)
298.15	805.40 ± 0.30	-0.40	67-kom/man <sup>1)</sup>	298.15	805.83 ± 0.02	0.03	79-kiy/ben(□)
303.15	801.95 ± 0.04	-0.02	74-rao/nai-1(Δ)	303.15	802.01 ± 0.05	0.04	81-nar/dha(◆)
293.15	809.56 ± 0.20	-0.04	76-hal/ell <sup>1)</sup>	283.15	817.02 ± 0.10	-0.11	86-hei/sch(✕)
298.15	805.75 ± 0.20	-0.05	76-hal/ell <sup>1)</sup>	298.15	805.76 ± 0.10	-0.04	86-hei/sch <sup>1)</sup>
303.15	801.91 ± 0.20	-0.06	76-hal/ell <sup>1)</sup>	313.15	794.22 ± 0.10	-0.00	86-hei/sch(✕)
320.00	788.73 ± 0.20	-0.09	76-hal/ell(✕)	298.15	805.74 ± 0.02	-0.06	86-oga/mur(○)
340.00	772.32 ± 0.20	-0.15	76-hal/ell(✕)	298.15	805.74 ± 0.05	-0.06	87-oga/mur(∇)
360.00	754.76 ± 0.20	-0.28	76-hal/ell(✕)	303.15	801.91 ± 0.15	-0.06	87-pik <sup>1)</sup>
380.00	735.73 ± 0.20	-0.50	76-hal/ell(✕)	333.15	778.22 ± 0.15	0.04	87-pik(✕)

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1864-lan, 1871-lie/ros, 1880-bru-1, 1881-pri/han, 1883-sch-3, 1884-zan, 1886-tra, 1893-eyk-1, 1898-kah, 00-loo, 06-car/fer, 08-dor/dvo, 08-ric/mat, 13-atk/wal, 14-low, 15-pea, 19-eyk, 19-ort/jon, 19-rei/ral, 21-bru/cre, 21-rei/hic, 22-her/sch, 23-pop, 23-wil/smi, 24-ter, 25-nor/ash, 25-pal/con, 25-per, 26-mat, 26-mun, 27-cla/rob, 27-ver/coo, 28-llo/bro, 29-ber, 29-jon, 29-mah/das, 29-pre, 30-bil/fis-1, 31-smy/wal, 31-sto/hul, 32-ern/lit, 33-azi/bha, 33-but/tho, 33-nev/jat, 33-tre/wat, 33-vos/con, 35-bra/fel, 35-bru/fur, 35-but/ram, 35-hen, 35-kef/mcl, 36-tom, 39-all/lin, 39-lar/hun, 41-hus/age, 42-mul, 42-sny/gil, 43-bru/bog, 44-was/str, 45-add, 46-kre/now, 48-con/elv, 48-jon/bow, 48-laz, 48-vog-2, 48-wei, 49-tsc/ric, 49-tsv/mar, 50-mum/phi, 50-pic/zie, 50-sac/sau, 51-sew, 51-tei/gor, 52-coo, 52-dun/was, 52-von, 53-ani, 53-mcc/jon, 53-par/cha, 54-jon/mcc, 54-pur/bow, 54-skr/mur, 55-bou/cle, 55-dan/col, 55-sin/she, 56-rus/ame, 56-tor-1, 57-mur/las, 57-rao/rao, 57-rom, 58-ano-5, 58-hol/len, 58-lin/tua, 59-ale, 59-ell/raz, 60-cop/fin, 60-tje, 61-bel/shu-1, 62-bro/smi, 62-par/mis, 63-gol/bag, 63-hov/sea, 63-man/she, 63-man/she-1, 63-mcc/lai, 63-sub/rao-1, 64-sta/kor, 65-fin/kid, 65-vij/des, 66-vij/des, 67-dei, 67-gol/per, 67-mur/rao, 67-vij/des-1, 68-ano, 69-fin/cop, 69-smi/kur, 69-sub/nag, 70-gal, 70-kat/kon, 70-kri/kom-1, 71-kat/lob, 72-bon/pik, 73-dak/rao, 73-dak/vee, 73-daw/new, 73-khi/ale, 73-svo/ves, 74-dut/mat, 74-rao/nai, 75-kub/tan, 75-mat/fer]

cont.

[76-bul/pro, 76-kow/kas, 76-red/nai, 77-rat/sal, 77-tre/ben, 78-dap/don, 78-sac/pes, 79-cha/ses-1, 79-jim/paz, 79-kum/pra, 79-sah/hay, 80-arc/bla, 80-fuk/ogi, 80-sue/mul, 81-nai/nai, 81-sjo/dyh, 82-ber/rog-1, 82-kar/red, 82-nai/nai, 82-ort, 82-ven/dha, 83-fuk/ogi, 83-pik-1, 83-pik-2, 83-rau/ste, 83-tri, 84-ber/pen, 84-sak/nak, 85-fer/pin, 85-mat/ben, 85-mat/ben-1, 85-ort/paz-1, 85-sar/paz, 86-ash/sri, 86-gat/woo, 86-gou/tom, 86-lep/mat, 86-mah/daw, 86-miy/hay, 86-san/sha, 86-tan/toy, 87-ber-5, 87-ber-7, 87-fer/ber, 87-kri/cho, 87-kub/tan, 87-nag, 87-ogi/ara, 88-fer/lap, 88-nag-2, 89-ala/sal, 89-mac/fra, 89-nao/sur, 89-ort/sus, 89-vij/nai, 90-cha/kat, 90-sri/nai, 90-vij/nai, 91-cab/bel, 91-fen/wan, 91-gar/her, 91-ram/muk, 92-ban/san, 92-gra/san, 92-tan/mur, 93-ami/ara, 93-ami/rai, 93-sus/ort, 94-kim/lee, 94-pap/pan-1, 94-yu /tsa-1, 95-fra/jim, 95-fra/men, 95-red/ram-1, 96-bha/mak, 96-dej/gon-1, 96-dom/rod, 96-elb, 96-gon/ort, 96-nik/jad, 96-nik/mah, 98-ami/ban, 98-ami/pat-1, 98-nik/shi].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**1-Butanol** (cont.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
190.00	889.84 ± 0.48	310.00	796.68 ± 0.17	450.00	652.75 ± 0.73
200.00	881.32 ± 0.42	320.00	788.82 ± 0.18	460.00	638.11 ± 0.75
210.00	873.06 ± 0.37	330.00	780.76 ± 0.20	470.00	623.10 ± 0.77
220.00	865.03 ± 0.32	340.00	772.47 ± 0.22	480.00	607.60 ± 0.80
230.00	857.19 ± 0.29	350.00	763.91 ± 0.24	490.00	591.23 ± 0.83
240.00	849.51 ± 0.25	360.00	755.04 ± 0.27	500.00	573.48 ± 0.88
250.00	841.93 ± 0.23	370.00	745.83 ± 0.31	510.00	553.60 ± 0.95
260.00	834.43 ± 0.21	380.00	736.23 ± 0.35	520.00	530.61 ± 1.05
270.00	826.96 ± 0.19	390.00	726.20 ± 0.40	530.00	503.20 ± 1.20
280.00	819.49 ± 0.17	400.00	715.71 ± 0.46	540.00	469.33 ± 1.43
290.00	811.98 ± 0.17	410.00	704.73 ± 0.53	550.00	424.91 ± 1.86
293.15	809.60 ± 0.17	420.00	693.20 ± 0.62	560.00	350.97 ± 2.78
298.15	805.80 ± 0.17	430.00	680.65 ± 0.70		
300.00	804.39 ± 0.17	440.00	667.01 ± 0.71		

**d-2-Butanol**

[4221-99-2]

C<sub>4</sub>H<sub>10</sub>O

MW = 74.12

6

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 1.8025 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 4.7605 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 348.95 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.60370 \cdot 10^2$
B	$4.37482 \cdot 10^{-1}$
C	$-2.11090 \cdot 10^{-3}$

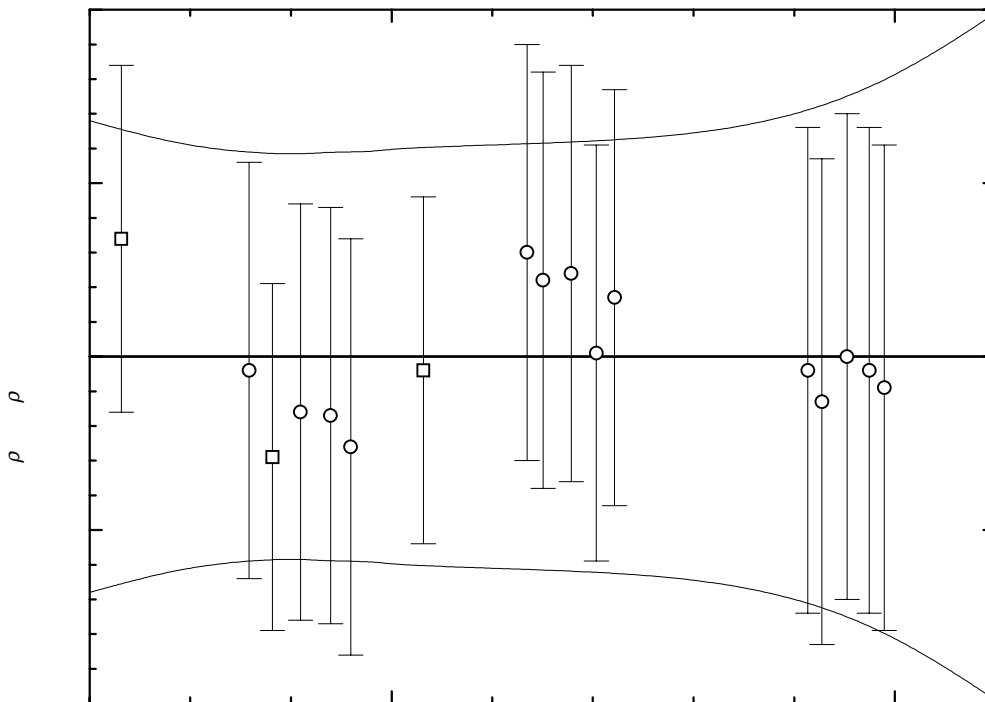
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
285.85	812.90 ± 0.60	-0.04	14-smi(O)	341.35	763.70 ± 0.70	-0.04	14-smi(O)
290.95	808.80 ± 0.60	-0.16	14-smi(O)	342.75	762.20 ± 0.70	-0.13	14-smi(O)
293.95	806.40 ± 0.60	-0.17	14-smi(O)	345.25	759.80 ± 0.70	0.00	14-smi(O)
295.95	804.70 ± 0.60	-0.26	14-smi(O)	347.45	757.50 ± 0.70	-0.04	14-smi(O)
313.45	790.40 ± 0.60	0.30	14-smi(O)	348.95	755.90 ± 0.70	-0.09	14-smi(O)
315.05	788.90 ± 0.60	0.22	14-smi(O)	273.15	822.71 ± 0.50	0.34	28-tim/mar(□)
317.85	786.40 ± 0.60	0.24	14-smi(O)	288.15	810.87 ± 0.50	-0.29	28-tim/mar(□)
320.35	783.90 ± 0.60	0.01	14-smi(O)	303.15	798.96 ± 0.50	-0.04	28-tim/mar(□)
322.15	782.40 ± 0.60	0.17	14-smi(O)				

<sup>1)</sup> Not included in Fig. 1.

cont.

Further references: [48-kor/pat].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	824.61 ± 0.68	298.15	803.16 ± 0.59	330.00	774.86 ± 0.64
280.00	817.37 ± 0.60	300.00	801.63 ± 0.60	340.00	765.09 ± 0.69
290.00	809.71 ± 0.58	310.00	793.13 ± 0.61	350.00	754.90 ± 0.80
293.15	807.21 ± 0.59	320.00	784.21 ± 0.62	360.00	744.29 ± 0.99

***l*-2-Butanol**

[14898-79-4]

C<sub>4</sub>H<sub>10</sub>O

MW = 74.12

7

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	804.2 ± 0.5	51-ler/luc

**(RS)-2-Butanol****[78-92-2]****C<sub>4</sub>H<sub>10</sub>O****MW = 74.12****8** $T_c = 536.18 \text{ K}$  [89-tej/lee] $\rho_c = 276.00 \text{ kg}\cdot\text{m}^{-3}$  [89-tej/lee]**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_t = 2.1049$  (low temperature range),  $\sigma_{c,w} = (1.9422 \text{ combined temperature ranges, weighted})$ ,  $\sigma_{c,uw} = 8.1750 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 200.00 \text{ to } 410.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 410.00 \text{ to } 536.18 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$1.16218 \cdot 10^3$	$4.61818 \cdot 10^{-1}$
B	-2.35615	$1.78871 \cdot 10^{-3}$
C	$6.45589 \cdot 10^{-3}$	$-6.92823 \cdot 10^{-5}$
D	$-8.71602 \cdot 10^{-6}$	$3.07819 \cdot 10^{-7}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg}\cdot\text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg}\cdot\text{m}^{-3}$	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg}\cdot\text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg}\cdot\text{m}^{-3}$	Ref. (Symbol in Fig. 1)
273.15	$822.61 \pm 0.20$	-0.04	22-tim(◆)	433.15	$667.70 \pm 0.60$	18.32	58-cos/bow(X)
273.15	$822.73 \pm 0.15$	0.08	28-tim/mar(Δ)	453.15	$636.50 \pm 0.60$	16.34	58-cos/bow(X)
288.15	$810.86 \pm 0.15$	0.10	28-tim/mar(Δ)	293.15	$812.90 \pm 0.30$	6.20	63-amb/tow <sup>1)</sup>
303.15	$798.93 \pm 0.15$	0.54	28-tim/mar(Δ)	407.23	$694.40 \pm 0.50$	9.71	63-amb/tow <sup>1)</sup>
293.15	$806.50 \pm 0.20$	-0.20	29-ber(X)	424.02	$670.10 \pm 0.50$	8.62	63-amb/tow(X)
298.15	$802.50 \pm 0.15$	-0.08	45-kol/bur(∇)	444.77	$637.70 \pm 0.50$	4.59	63-amb/tow(X)
293.15	$807.30 \pm 0.40$	0.60	55-kus <sup>1)</sup>	453.55	$623.30 \pm 0.50$	3.79	63-amb/tow(X)
298.15	$803.30 \pm 0.40$	0.72	55-kus <sup>1)</sup>	461.35	$609.20 \pm 0.50$	3.07	63-amb/tow(X)
303.15	$799.10 \pm 0.40$	0.71	55-kus <sup>1)</sup>	473.25	$587.10 \pm 1.00$	4.22	63-amb/tow(X)
313.15	$790.60 \pm 0.40$	0.82	55-kus <sup>1)</sup>	478.56	$575.80 \pm 1.00$	4.53	63-amb/tow(X)
323.15	$781.70 \pm 0.40$	0.87	55-kus(X)	494.70	$539.00 \pm 2.00$	8.35	63-amb/tow(X)
333.15	$772.30 \pm 0.50$	0.82	55-kus <sup>1)</sup>	504.39	$513.20 \pm 3.00$	11.41	63-amb/tow(X)
343.15	$762.20 \pm 0.50$	0.52	55-kus(X)	302.75	$798.80 \pm 0.40$	0.07	63-tho/mea <sup>1)</sup>
353.15	$752.10 \pm 0.50$	0.73	55-kus(X)	318.25	$785.70 \pm 0.40$	0.44	63-tho/mea(X)
213.15	$866.80 \pm 0.60$	-2.07	58-cos/bow(X)	332.35	$772.10 \pm 0.40$	-0.14	63-tho/mea(X)
233.15	$851.70 \pm 0.60$	-1.62	58-cos/bow(X)	347.75	$756.70 \pm 0.50$	-0.30	63-tho/mea(X)
253.15	$837.20 \pm 0.60$	-0.85	58-cos/bow(X)	362.15	$740.90 \pm 0.50$	-0.73	63-tho/mea(X)
273.15	$822.10 \pm 0.50$	-0.55	58-cos/bow <sup>1)</sup>	200.00	$875.00 \pm 1.50$	-4.46	64-dan/bah(X)
293.15	$806.00 \pm 0.50$	-0.70	58-cos/bow <sup>1)</sup>	220.00	$862.00 \pm 1.50$	-1.49	64-dan/bah(X)
313.15	$789.40 \pm 0.50$	-0.38	58-cos/bow <sup>1)</sup>	240.00	$846.00 \pm 1.50$	-2.08	64-dan/bah(X)
333.15	$771.40 \pm 0.50$	-0.08	58-cos/bow <sup>1)</sup>	260.00	$830.00 \pm 1.50$	-2.81	64-dan/bah(X)
353.15	$753.90 \pm 0.50$	2.53	58-cos/bow(X)	280.00	$814.00 \pm 1.50$	-3.27	64-dan/bah <sup>1)</sup>
373.15	$735.60 \pm 0.60$	6.56	58-cos/bow(X)	300.00	$798.00 \pm 1.50$	-3.04	64-dan/bah <sup>1)</sup>
393.15	$716.90 \pm 0.60$	12.83	58-cos/bow <sup>1)</sup>	320.00	$781.00 \pm 1.50$	-2.69	64-dan/bah <sup>1)</sup>
413.15	$695.50 \pm 0.60$	19.33	58-cos/bow(X)	340.00	$761.00 \pm 1.50$	-3.82	64-dan/bah <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
360.00	742.00 ± 1.50	-2.00	64-dan/bah <sup>1)</sup>	420.00	667.41 ± 0.20	0.60	76-hal/ell(✕)
380.00	717.00 ± 1.50	-3.81	64-dan/bah <sup>1)</sup>	440.00	637.44 ± 0.20	-2.54	76-hal/ell(✕)
400.00	693.00 ± 1.50	-1.84	64-dan/bah <sup>1)</sup>	460.00	604.02 ± 0.25	-4.52	76-hal/ell(✕)
420.00	667.00 ± 1.70	0.19	64-dan/bah <sup>1)</sup>	483.83	557.48 ± 0.30	-1.44	76-hal/ell(✕)
440.00	638.00 ± 1.70	-1.98	64-dan/bah <sup>1)</sup>	490.00	543.63 ± 0.30	0.27	76-hal/ell(✕)
460.00	607.00 ± 2.00	-1.54	64-dan/bah <sup>1)</sup>	293.15	807.70 ± 0.50	1.00	81-kor/kov <sup>1)</sup>
480.00	572.00 ± 2.00	4.02	64-dan/bah(✕)	293.15	807.80 ± 0.50	1.10	81-kor/kov <sup>1)</sup>
500.00	532.00 ± 2.00	16.66	64-dan/bah(✕)	353.15	755.80 ± 0.50	4.43	81-kor/kov(✕)
520.00	465.00 ± 3.00	20.36	64-dan/bah(✕)	353.15	755.80 ± 0.50	4.43	81-kor/kov(✕)
293.15	806.61 ± 0.20	-0.09	76-hal/ell(✕)	298.15	802.50 ± 0.30	-0.08	85-ogi/ara <sup>1)</sup>
298.15	802.44 ± 0.20	-0.14	76-hal/ell <sup>1)</sup>	313.15	790.00 ± 0.30	0.22	85-ogi/ara(✕)
303.15	798.25 ± 0.20	-0.14	76-hal/ell(✕)	293.15	806.66 ± 0.10	-0.04	86-cha/lam(○)
320.00	783.42 ± 0.20	-0.27	76-hal/ell(✕)	313.15	789.66 ± 0.10	-0.12	86-cha/lam(○)
340.00	764.17 ± 0.20	-0.65	76-hal/ell(✕)	323.15	780.46 ± 0.15	-0.37	86-cha/lam(○)
360.00	742.98 ± 0.20	-1.02	76-hal/ell(✕)	333.15	770.78 ± 0.15	-0.70	86-cha/lam(○)
380.00	719.83 ± 0.20	-0.98	76-hal/ell(✕)	298.15	802.49 ± 0.06	-0.09	88-oka/oga(□)
400.00	694.75 ± 0.20	-0.09	76-hal/ell(✕)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1869-lie, 06-car/fer, 11-pic/ken, 13-pic/ken, 14-smi, 14-vav, 16-wil/bru, 19-beh, 19-eyk, 21-bru/cre, 21-rei/hic, 23-bru, 23-clo/joh, 25-fai, 25-nor/ash, 26-mun, 33-huc/ack, 33-nev/jat, 35-but/ram, 35-mah-1, 39-all/lin, 39-bar/atk, 39-lar/hun, 42-boe/han-1, 48-wei, 49-ber/ped, 50-pic/zie, 51-ami/wei, 51-bot, 52-coo, 52-dun/was, 56-rus/ame, 62-bro/smi, 63-mcc/lai, 65-fin/kid, 67-gol/per, 68-ano, 68-eva/lin, 69-bro/foc, 78-sac/pes, 80-cha/ses, 80-kas/izy, 80-rig/ube, 83-fuk/ogi, 85-rao/red, 86-kar/cam, 87-kri/cho, 88-nag-2, 89-nao/sur, 92-tan/mur, 94-ben/car, 96-bha/mak, 96-dej/gon-1, 98-fen/cho].

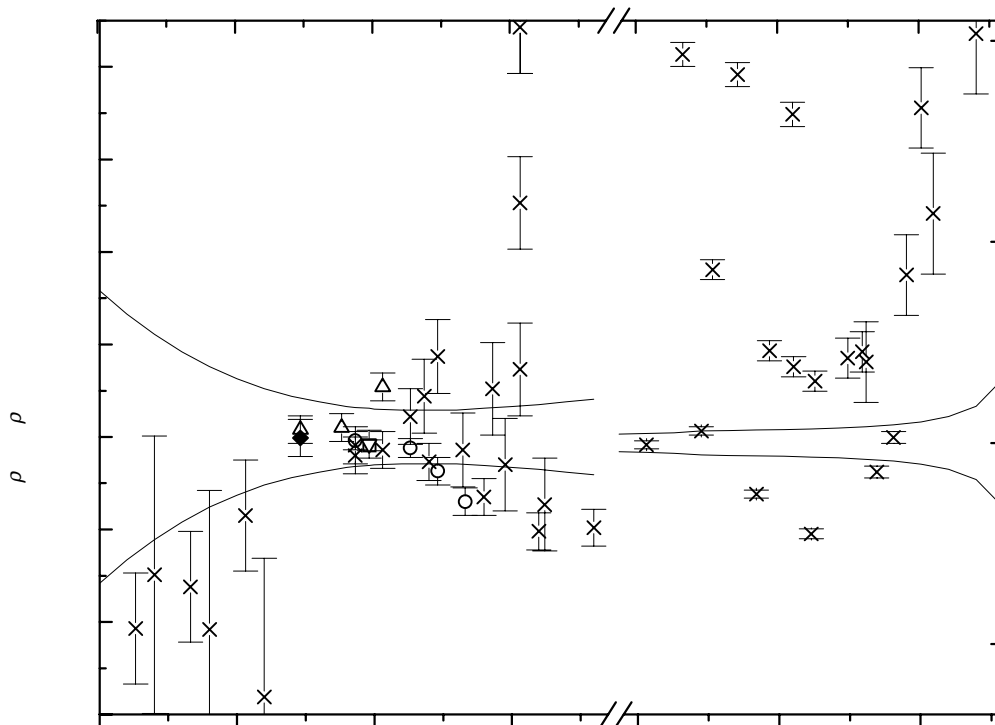
**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
200.00	879.46 ± 1.58	300.00	801.04 ± 0.30	420.00	666.81 ± 0.60
210.00	871.38 ± 1.33	310.00	792.53 ± 0.29	430.00	653.58 ± 0.62
220.00	863.49 ± 1.11	320.00	783.69 ± 0.29	440.00	639.98 ± 0.64
230.00	855.74 ± 0.92	330.00	774.47 ± 0.29	450.00	625.17 ± 0.66
240.00	848.08 ± 0.76	340.00	764.82 ± 0.31	460.00	608.54 ± 0.70
250.00	840.45 ± 0.63	350.00	754.68 ± 0.33	470.00	589.60 ± 0.74
260.00	832.81 ± 0.52	360.00	744.00 ± 0.35	480.00	567.98 ± 0.81
270.00	825.10 ± 0.44	370.00	732.73 ± 0.38	490.00	543.36 ± 0.90
280.00	817.27 ± 0.38	380.00	720.81 ± 0.41	500.00	515.34 ± 1.05
290.00	809.27 ± 0.33	390.00	708.20 ± 0.44	510.00	483.12 ± 1.31
293.15	806.70 ± 0.32	400.00	694.84 ± 0.47	520.00	444.64 ± 1.82
298.15	802.58 ± 0.31	410.00	680.68 ± 0.51	530.00	391.57 ± 3.20

cont.



**(RS)-2-Butanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**2-Methyl-1-propanol****[78-83-1]****C<sub>4</sub>H<sub>10</sub>O****MW = 74.12****9** $T_c = 547.74$  K [63-amb/bro] $\rho_c = 272.20$  kg·m<sup>-3</sup> [63-amb/bro]**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction): $\sigma_i = 1.9234$  (low temperature range),  $\sigma_{c,w} = (1.4721$  combined temperature ranges, weighted), $\sigma_{c,uw} = 8.2141 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 213.15$ to $440.00$ K $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 440.00$ to $547.74$ K $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3$ $+ D(T_c - T)^4]$
<i>A</i>	$1.16796 \cdot 10^3$	$8.96238 \cdot 10^{-1}$
<i>B</i>	$-2.41227$	$-1.28076 \cdot 10^{-2}$
<i>C</i>	$6.24427 \cdot 10^{-3}$	$9.68824 \cdot 10^{-5}$
<i>D</i>	$-7.77901 \cdot 10^{-6}$	$-2.95139 \cdot 10^{-7}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	816.22 ± 0.70	-0.18	1881-ber <sup>1)</sup>	273.15	819.60 ± 0.60	3.20	22-mic(X)
280.71	810.50 ± 0.70	-0.28	1881-ber <sup>1)</sup>	273.15	817.00 ± 0.60	0.60	26-han(X)
281.64	809.80 ± 0.70	-0.29	1881-ber <sup>1)</sup>	380.15	726.00 ± 0.60	0.04	27-arb-2(X)
287.65	805.20 ± 0.70	-0.39	1881-ber <sup>1)</sup>	380.15	726.00 ± 0.60	0.04	27-arb-2(X)
290.95	802.70 ± 0.70	-0.40	1881-ber <sup>1)</sup>	273.15	817.03 ± 0.60	0.63	28-tim/mar(X)
292.15	801.80 ± 0.70	-0.40	1881-ber <sup>1)</sup>	288.15	805.74 ± 0.60	0.53	28-tim/mar <sup>1)</sup>
292.25	801.70 ± 0.70	-0.42	1881-ber <sup>1)</sup>	303.15	794.35 ± 0.60	0.54	28-tim/mar <sup>1)</sup>
303.86	792.70 ± 0.70	-0.56	1881-ber <sup>1)</sup>	303.15	795.00 ± 0.45	1.19	33-azi/bha <sup>1)</sup>
304.40	792.30 ± 0.70	-0.54	1881-ber <sup>1)</sup>	313.15	788.90 ± 0.45	2.89	33-azi/bha <sup>1)</sup>
310.44	787.20 ± 0.70	-0.94	1881-ber <sup>1)</sup>	323.15	778.80 ± 0.45	0.81	33-azi/bha(X)
319.71	780.00 ± 0.70	-0.78	1881-ber <sup>1)</sup>	333.15	770.70 ± 0.45	0.98	33-azi/bha(X)
319.86	779.90 ± 0.70	-0.75	1881-ber <sup>1)</sup>	348.15	754.50 ± 0.45	-2.22	33-azi/bha(X)
333.85	768.00 ± 0.70	-1.13	1881-ber <sup>1)</sup>	273.15	817.20 ± 0.30	0.80	45-alb/was(♦)
342.12	760.80 ± 1.00	-1.24	1881-ber <sup>1)</sup>	298.15	798.09 ± 0.30	0.45	45-alb/was <sup>1)</sup>
354.01	749.70 ± 1.00	-1.72	1881-ber <sup>1)</sup>	293.15	802.10 ± 0.60	0.66	48-vog-2 <sup>1)</sup>
372.43	731.80 ± 1.00	-2.02	1881-ber(X)	315.85	785.20 ± 0.60	1.34	48-vog-2 <sup>1)</sup>
372.63	731.50 ± 1.00	-2.12	1881-ber(X)	334.65	769.90 ± 0.60	1.45	48-vog-2(X)
375.12	729.50 ± 1.00	-1.61	1881-ber(X)	358.15	750.10 ± 0.60	2.51	48-vog-2(X)
379.75	726.50 ± 1.00	0.12	1883-sch-3(X)	493.15	555.50 ± 0.50	-2.98	55-kay/don(X)
379.55	726.50 ± 1.00	-0.08	1884-sch-6(X)	503.15	533.80 ± 0.50	-1.35	55-kay/don(X)
283.15	809.90 ± 0.50	0.94	1890-gar <sup>1)</sup>	513.15	503.20 ± 0.50	-5.19	55-kay/don(X)
293.15	801.90 ± 0.50	0.46	1890-gar <sup>1)</sup>	523.15	478.90 ± 0.60	2.36	55-kay/don(X)
303.15	794.00 ± 0.50	0.19	1890-gar <sup>1)</sup>	533.15	441.20 ± 2.00	4.89	55-kay/don(X)
313.15	786.50 ± 0.50	0.49	1890-gar <sup>1)</sup>	543.15	283.00 ± 3.00	-92.91	55-kay/don <sup>1)</sup>
323.15	779.20 ± 0.50	1.21	1890-gar(X)	547.74	269.00 ± 5.00	-3.20	55-kay/don(X)
273.15	816.96 ± 0.60	0.56	02-you/for(X)	293.15	802.30 ± 0.50	0.86	55-kus <sup>1)</sup>
289.50	804.59 ± 0.60	0.39	02-you/for <sup>1)</sup>	298.15	798.30 ± 0.50	0.66	55-kus <sup>1)</sup>
289.40	806.78 ± 0.50	2.51	12-sch-3 <sup>1)</sup>	303.15	794.30 ± 0.50	0.49	55-kus <sup>1)</sup>
304.95	794.21 ± 0.50	1.79	12-sch-3 <sup>1)</sup>	313.15	786.30 ± 0.50	0.29	55-kus <sup>1)</sup>
326.15	776.49 ± 0.50	0.95	12-sch-3(X)	323.15	778.50 ± 0.50	0.51	55-kus(X)
347.80	758.27 ± 0.70	1.24	12-sch-3(X)	333.15	770.20 ± 0.50	0.48	55-kus(X)
289.40	806.78 ± 0.50	2.51	15-sch-1 <sup>1)</sup>	343.15	761.60 ± 0.50	0.46	55-kus(X)
304.95	794.21 ± 0.50	1.79	15-sch-1 <sup>1)</sup>	353.15	752.70 ± 0.50	0.49	55-kus(X)
326.15	776.49 ± 0.50	0.95	15-sch-1(X)	293.15	801.60 ± 0.50	0.16	56-tor-1 <sup>1)</sup>
347.80	758.27 ± 0.70	1.24	15-sch-1(X)	313.15	786.20 ± 0.50	0.19	56-tor-1 <sup>1)</sup>
201.65	885.00 ± 1.50	13.35	17-jae <sup>1)</sup>	333.15	769.60 ± 0.50	-0.12	56-tor-1(X)
261.15	828.00 ± 1.50	2.70	17-jae(X)	213.15	861.30 ± 0.60	-0.85	58-cos/bow(X)
273.45	817.00 ± 1.50	0.82	17-jae <sup>1)</sup>	233.15	846.40 ± 0.60	0.02	58-cos/bow(X)
283.55	807.00 ± 1.50	-1.66	17-jae <sup>1)</sup>	253.15	831.40 ± 0.60	0.14	58-cos/bow(X)
298.25	794.00 ± 1.50	-3.57	17-jae <sup>1)</sup>	273.15	816.70 ± 0.50	0.30	58-cos/bow(X)
308.25	785.00 ± 1.50	-4.85	17-jae <sup>1)</sup>	293.15	802.10 ± 0.50	0.66	58-cos/bow <sup>1)</sup>
322.85	771.00 ± 1.50	-7.24	17-jae <sup>1)</sup>	313.15	785.80 ± 0.50	-0.21	58-cos/bow <sup>1)</sup>
342.75	753.00 ± 1.50	-8.49	17-jae <sup>1)</sup>	333.15	769.20 ± 0.50	-0.52	58-cos/bow(X)
374.15	731.00 ± 1.50	-1.09	17-jae <sup>1)</sup>	353.15	751.00 ± 0.50	-1.21	58-cos/bow(X)

<sup>1)</sup> Not included in Fig. 1.

cont.

## 2-Methyl-1-propanol (cont.)

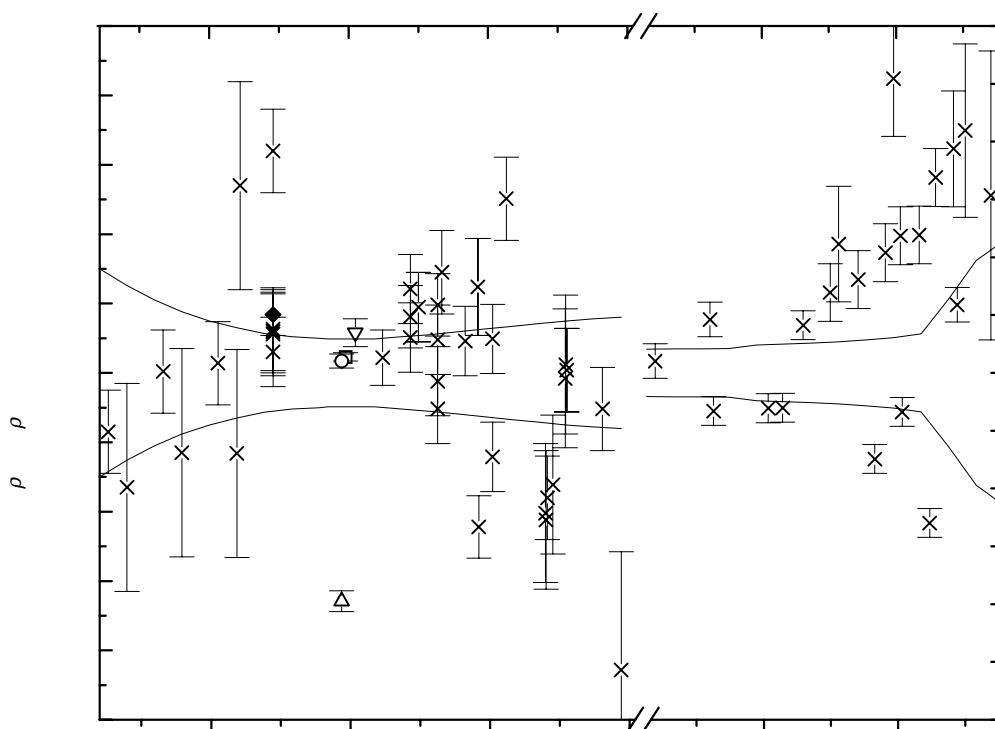
Table 2. (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
373.15	731.30 ± 0.60	-1.80	58-cos/bow(X)	280.00	810.00 ± 1.50	-1.31	64-dan/bah <sup>1)</sup>
393.15	711.50 ± 0.60	-0.52	58-cos/bow(X)	300.00	795.00 ± 1.50	-1.23	64-dan/bah <sup>1)</sup>
413.15	689.00 ± 0.60	0.41	58-cos/bow(X)	320.00	778.00 ± 1.50	-2.54	64-dan/bah <sup>1)</sup>
433.15	664.30 ± 0.60	1.85	58-cos/bow(X)	340.00	762.00 ± 1.50	-1.88	64-dan/bah <sup>1)</sup>
293.15	802.20 ± 0.40	0.76	63-amb/tow <sup>1)</sup>	360.00	743.00 ± 1.50	-2.86	64-dan/bah <sup>1)</sup>
421.16	667.50 ± 0.50	-10.97	63-amb/tow <sup>1)</sup>	380.00	722.00 ± 1.50	-4.12	64-dan/bah <sup>1)</sup>
434.40	659.40 ± 0.50	-1.32	63-amb/tow(X)	400.00	700.00 ± 1.70	-4.28	64-dan/bah(X)
454.31	629.70 ± 0.50	-1.22	63-amb/tow(X)	420.00	676.00 ± 1.70	-3.96	64-dan/bah <sup>1)</sup>
459.55	621.10 ± 0.50	-1.21	63-amb/tow(X)	440.00	650.00 ± 2.00	-2.80	64-dan/bah <sup>1)</sup>
467.04	611.10 ± 0.50	1.65	63-amb/tow(X)	460.00	620.00 ± 2.00	-1.55	64-dan/bah <sup>1)</sup>
476.88	594.30 ± 1.00	2.78	63-amb/tow(X)	480.00	590.00 ± 2.00	4.46	64-dan/bah(X)
487.09	574.60 ± 1.00	3.23	63-amb/tow(X)	500.00	553.00 ± 2.00	10.18	64-dan/bah(X)
497.04	553.90 ± 1.00	4.16	63-amb/tow(X)	520.00	510.00 ± 2.50	22.74	64-dan/bah(X)
502.46	541.60 ± 1.00	4.74	63-amb/tow(X)	540.00	440.00 ± 6.00	40.84	64-dan/bah(X)
509.32	523.90 ± 1.00	4.77	63-amb/tow(X)	298.15	794.35 ± 0.15	-3.29	80-kas/izy(Δ)
515.30	508.80 ± 1.00	6.76	63-amb/tow(X)	303.15	794.39 ± 0.20	0.58	86-mou/nai(∇)
521.85	488.80 ± 2.00	7.75	63-amb/tow(X)	298.15	797.87 ± 0.06	0.23	88-oka/oga(□)
526.06	474.30 ± 3.00	8.38	63-amb/tow(X)	298.15	797.81 ± 0.10	0.17	96-dom/rod(○)
535.44	431.30 ± 5.00	6.14	63-amb/tow(X)	298.15	798.30 ± 0.40	0.66	98-nik/shi <sup>1)</sup>
200.00	868.00 ± 1.50	-5.04	64-dan/bah <sup>1)</sup>	303.15	794.31 ± 0.40	0.50	98-nik/shi <sup>1)</sup>
220.00	855.00 ± 1.50	-1.65	64-dan/bah(X)	308.15	790.26 ± 0.40	0.33	98-nik/shi <sup>1)</sup>
240.00	840.00 ± 1.50	-1.15	64-dan/bah(X)	313.15	786.23 ± 0.40	0.22	98-nik/shi(X)
260.00	825.00 ± 1.50	-1.16	64-dan/bah(X)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1872-lin/von-2, 1872-pie/puc, 1884-gla, 1884-per, 1891-jah, 1891-sch/kos, 1892-lan/jah, 1894-jah/mol, 1898-kah, 08-dor/dvo, 11-dor, 13-rom, 14-eng/tur, 14-gas, 14-wor, 15-pea, 15-ric/coo, 16-wro/rei, 19-eyk, 21-bru/cre, 21-rei/hic, 23-pop, 23-wil/smi, 25-nor/ash, 26-mat, 26-mun, 31-sto/hul, 32-byl, 33-huc/ack, 33-tre/wat, 33-vos/con, 34-smi, 35-but/ram, 35-mah-1, 39-all/lin, 39-lar/hun, 42-sny/gil, 43-boh, 46-fri/sto, 47-sho/pri, 48-wei, 50-cro/van, 50-mum/phi, 50-pic/zie, 51-hau, 51-tei/gor, 52-coo, 52-dun/was, 53-ani, 53-ani-1, 53-hag/dec, 53-par/cha, 55-dan/col, 56-rus/ame, 58-ano-5, 62-bro/smi, 63-mcc/lai, 67-gol/per, 67-nat/rao, 68-ano, 69-bro/foc, 69-smi/kur, 70-sus/hol, 82-ber/rog-1, 82-kar/red, 82-ven/dha, 83-fuk/ogi, 83-lin, 84-ber/pen, 85-mat/ben, 85-mat/ben-1, 85-rao/red, 87-ber-1, 87-kri/cho, 88-nag, 88-nag-1, 90-mal/rao, 92-kum/sre, 93-ami/rai, 95-red/ram-1, 96-bha/mak, 96-nik/jad, 96-nik/mah, 98-art/dom, 98-sen].

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
210.00	864.71 ± 1.50	310.00	788.48 ± 0.49	430.00	666.76 ± 0.83
220.00	856.65 ± 1.26	320.00	780.54 ± 0.52	440.00	652.80 ± 0.84
230.00	848.81 ± 1.05	330.00	772.36 ± 0.55	450.00	637.78 ± 0.97
240.00	841.15 ± 0.88	340.00	763.88 ± 0.59	460.00	621.55 ± 1.00
250.00	833.61 ± 0.75	350.00	755.06 ± 0.63	470.00	604.19 ± 1.03
260.00	826.16 ± 0.65	360.00	745.86 ± 0.67	480.00	585.54 ± 1.08
270.00	818.74 ± 0.57	370.00	736.23 ± 0.71	490.00	565.28 ± 1.14
280.00	811.31 ± 0.52	380.00	726.12 ± 0.75	500.00	542.82 ± 1.22
290.00	803.82 ± 0.50	390.00	715.48 ± 0.78	510.00	517.27 ± 1.35
293.15	801.44 ± 0.49	400.00	704.28 ± 0.80	520.00	487.26 ± 2.55
298.15	797.64 ± 0.49	410.00	692.45 ± 0.82	530.00	450.24 ± 3.89
300.00	796.23 ± 0.49	420.00	679.96 ± 0.83	540.00	399.16 ± 4.57

**2-Methyl-2-propanol****[75-65-0]****C<sub>4</sub>H<sub>10</sub>O****MW = 74.12****10** $T_c = 506.20$  K [89-tej/lee] $\rho_c = 270.00$  kg·m<sup>-3</sup> [89-tej/lee]**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_\tau = 4.8919$  (low temperature range),  $\sigma_{c,w} = (1.7560$  combined temperature ranges, weighted),  $\sigma_{c,uw} = 4.6459 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $400.00$ K $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 400.00$ to $506.20$ K $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$9.06345 \cdot 10^2$	1.32387
B	$1.53910 \cdot 10^{-1}$	$-2.89194 \cdot 10^{-2}$
C	$-1.93019 \cdot 10^{-3}$	$2.93882 \cdot 10^{-4}$
D		$-1.07285 \cdot 10^{-6}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	$807.40 \pm 1.00$	3.03	1872-but(X)	447.23	$575.40 \pm 0.50$	2.89	63-amb/tow(X)
303.15	$775.40 \pm 1.00$	-0.22	1872-but <sup>1)</sup>	456.20	$556.10 \pm 0.50$	2.63	63-amb/tow(X)
303.15	$777.50 \pm 0.50$	1.88	31-smy/dor-1 <sup>1)</sup>	465.81	$533.00 \pm 0.50$	2.08	63-amb/tow(X)
323.15	$756.30 \pm 0.50$	1.78	31-smy/dor-1 <sup>1)</sup>	473.52	$512.80 \pm 1.00$	2.70	63-amb/tow(X)
343.15	$734.30 \pm 0.50$	2.42	31-smy/dor-1(X)	480.56	$490.50 \pm 1.00$	2.68	63-amb/tow(X)
293.15	$786.68 \pm 0.50$	1.09	34-tim/del(◆)	300.00	$776.00 \pm 1.50$	-2.80	64-dan/bah <sup>1)</sup>
303.15	$776.18 \pm 0.50$	0.56	34-tim/del <sup>1)</sup>	320.00	$756.00 \pm 1.50$	-1.94	64-dan/bah <sup>1)</sup>
308.15	$770.88 \pm 0.50$	0.39	34-tim/del <sup>1)</sup>	340.00	$736.00 \pm 1.50$	0.46	64-dan/bah <sup>1)</sup>
313.15	$765.58 \pm 0.50$	0.32	34-tim/del <sup>1)</sup>	360.00	$712.00 \pm 1.50$	0.40	64-dan/bah <sup>1)</sup>
298.15	$781.60 \pm 0.40$	0.95	55-kus <sup>1)</sup>	380.00	$686.00 \pm 1.50$	-0.11	64-dan/bah <sup>1)</sup>
303.15	$776.60 \pm 0.40$	0.98	55-kus <sup>1)</sup>	400.00	$654.00 \pm 1.50$	-5.08	64-dan/bah <sup>1)</sup>
313.15	$766.50 \pm 0.40$	1.24	55-kus <sup>1)</sup>	420.00	$618.00 \pm 1.70$	-7.60	64-dan/bah <sup>1)</sup>
323.15	$755.90 \pm 0.40$	1.38	55-kus <sup>1)</sup>	440.00	$580.00 \pm 1.70$	-7.09	64-dan/bah <sup>1)</sup>
333.15	$741.50 \pm 0.50$	-1.89	55-kus <sup>1)</sup>	460.00	$536.00 \pm 2.00$	-8.90	64-dan/bah <sup>1)</sup>
343.15	$734.20 \pm 0.50$	2.32	55-kus(X)	480.00	$476.00 \pm 2.50$	-13.74	64-dan/bah <sup>1)</sup>
353.15	$722.60 \pm 0.50$	2.63	55-kus(X)	500.00	$380.00 \pm 6.00$	-11.52	64-dan/bah(X)
313.15	$765.20 \pm 0.50$	-0.06	58-cos/bow <sup>1)</sup>	300.65	$778.10 \pm 0.12$	-0.05	83-hal/gun(V)
333.15	$742.90 \pm 0.50$	-0.49	58-cos/bow <sup>1)</sup>	303.15	$775.43 \pm 0.12$	-0.19	83-hal/gun(V)
353.15	$721.20 \pm 0.50$	1.23	58-cos/bow(X)	308.15	$770.23 \pm 0.12$	-0.26	83-hal/gun(V)
373.15	$697.40 \pm 0.50$	2.38	58-cos/bow(X)	313.15	$757.60 \pm 0.15$	-7.66	83-hal/gun(V)
393.15	$671.50 \pm 0.60$	2.99	58-cos/bow(X)	340.00	$735.05 \pm 0.15$	-0.49	83-hal/gun(V)
413.15	$645.00 \pm 0.60$	6.98	58-cos/bow(X)	360.00	$710.82 \pm 0.17$	-0.78	83-hal/gun(V)
300.15	$779.20 \pm 0.40$	0.55	63-amb/tow <sup>1)</sup>	380.00	$684.41 \pm 0.17$	-1.70	83-hal/gun(V)
419.82	$628.10 \pm 0.50$	2.16	63-amb/tow(X)	400.00	$655.47 \pm 0.17$	-3.61	83-hal/gun(V)
433.61	$603.50 \pm 0.50$	3.85	63-amb/tow(X)	420.00	$623.36 \pm 0.20$	-2.24	83-hal/gun(V)

<sup>1)</sup> Not included in Fig. 1.

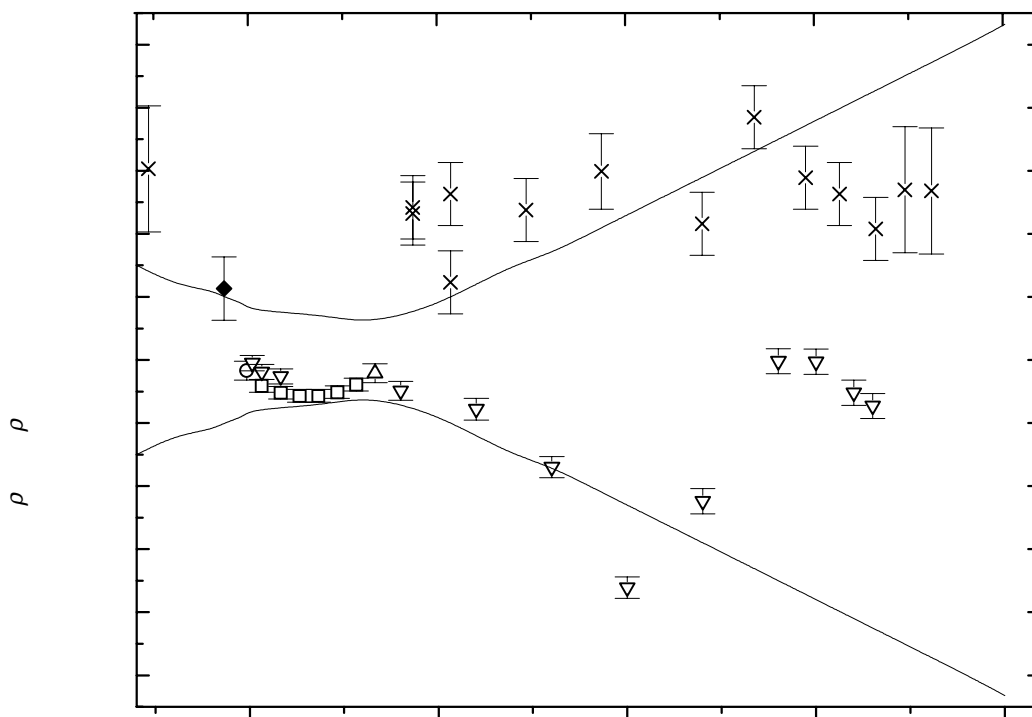
cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
440.00	587.07 ± 0.20	-0.02	83-hal/gun(∇)	308.15	769.97 ± 0.10	-0.52	88-kim/mar(□)
450.00	566.74 ± 0.20	-0.03	83-hal/gun(∇)	313.15	764.69 ± 0.10	-0.57	88-kim/mar(□)
460.00	544.38 ± 0.20	-0.52	83-hal/gun(∇)	318.15	759.37 ± 0.10	-0.57	88-kim/mar(□)
465.00	532.21 ± 0.20	-0.73	83-hal/gun(∇)	323.15	754.01 ± 0.10	-0.51	88-kim/mar(□)
303.15	775.46 ± 0.15	-0.16	87-pik <sup>1)</sup>	328.15	748.61 ± 0.10	-0.39	88-kim/mar(□)
333.15	743.18 ± 0.15	-0.21	87-pik(Δ)	299.15	779.48 ± 0.15	-0.17	88-oka/oga(○)
303.15	775.21 ± 0.10	-0.41	88-kim/mar(□)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1872-lin/von-2, 1880-bru-1, 1884-per, 1893-tho/jon, 02-you/for, 06-car/fer, 08-ric/mat, 11-dor-1, 19-beh, 19-eyk, 25-nor/ash, 26-mun, 29-pre, 29-swa, 33-gin/her, 33-nev/jat, 35-hen, 36-ipa/cor, 36-spe, 39-owe/qua, 44-ira, 46-sim/was, 48-wei, 49-dre/mar, 50-pic/zie, 52-dun/was, 54-wes/aud, 55-bou/cle, 55-wes, 56-rus/ame, 62-bro/smi, 63-mcc/lai, 69-bro/foc, 70-sus/hol, 71-des/bha-1, 76-tri/kri, 77-gov/and-1, 80-kas/izy, 83-pik-2, 85-rao/red, 87-kri/cho, 88-cac/cos, 95-red/ram-1, 96-bha/mak, 96-nik/mah, 98-nik/shi].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**2-Methyl-2-propanol** (cont.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  
 $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	807.19 ± 1.50	340.00	735.54 ± 0.72	430.00	606.64 ± 3.20
280.00	798.11 ± 1.20	350.00	723.77 ± 0.90	440.00	587.09 ± 3.53
290.00	788.65 ± 1.13	360.00	711.60 ± 1.22	450.00	566.77 ± 3.80
293.15	785.59 ± 1.00	370.00	699.05 ± 1.51	460.00	544.90 ± 4.10
298.15	780.65 ± 0.91	380.00	686.11 ± 1.74	470.00	519.99 ± 4.40
300.00	778.80 ± 0.80	390.00	672.79 ± 2.00	480.00	489.74 ± 4.70
310.00	768.57 ± 0.75	400.00	659.08 ± 2.30	490.00	450.24 ± 5.00
320.00	757.94 ± 0.70	410.00	643.47 ± 2.60	500.00	391.52 ± 5.32
330.00	746.94 ± 0.60	420.00	625.60 ± 2.90		

2.1.2 Alkanols, C<sub>5</sub> - C<sub>6</sub>

**2,2-Dimethyl-1-propanol** [75-84-3] C<sub>5</sub>H<sub>12</sub>O MW = 88.15 11

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
303.15	799.0 ± 0.3	74-mye/cle

**2-Methyl-1-butanol** [137-32-6] C<sub>5</sub>H<sub>12</sub>O MW = 88.15 12

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 7.9216 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 1.8175 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $390.65$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.00094 \cdot 10^3$
B	$-4.27416 \cdot 10^{-1}$
C	$-6.53533 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

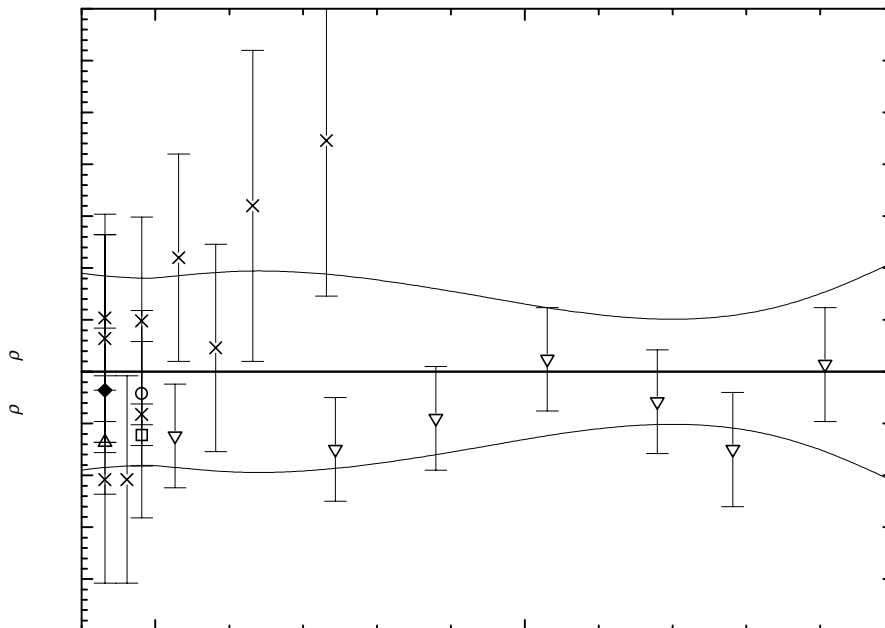
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
298.15	815.20 ± 0.50	-0.21	27-nor/cor(○)	367.95	754.90 ± 0.50	-0.29	63-tho/mea(∇)
296.15	816.00 ± 1.00	-1.04	31-lev/mar-4(×)	378.15	745.10 ± 0.55	-0.75	63-tho/mea(∇)
293.15	819.30 ± 0.60	-0.18	37-bra(◆)	390.65	734.30 ± 0.55	0.07	63-tho/mea(∇)
293.15	818.44 ± 1.00	-1.04	38-whi/ole(×)	293.15	818.80 ± 0.50	-0.68	68-ano(Δ)
308.15	807.40 ± 1.00	0.23	46-haf/lov(×)	298.15	814.80 ± 0.30	-0.61	82-dap/don(□)
293.15	820.00 ± 1.00	0.52	51-lyu/ter(×)	293.15	819.80 ± 1.00	0.32	83-fuk/ogi(×)
293.15	819.80 ± 1.00	0.32	52-coo(×)	298.15	815.90 ± 1.00	0.49	83-fuk/ogi(×)
298.15	815.00 ± 1.00	-0.41	56-ike/kep(×)	303.15	812.40 ± 1.00	1.10	83-fuk/ogi(×)
302.65	811.10 ± 0.50	-0.62	63-tho/mea(∇)	313.15	804.60 ± 1.50	1.60	83-fuk/ogi(×)
324.35	792.80 ± 0.50	-0.75	63-tho/mea(∇)	323.15	796.80 ± 1.50	2.23	83-fuk/ogi(×)
337.95	781.40 ± 0.50	-0.45	63-tho/mea(∇)	333.15	788.80 ± 1.50	2.79	83-fuk/ogi <sup>1)</sup>
353.05	768.70 ± 0.50	0.12	63-tho/mea(∇)	343.15	780.10 ± 1.50	2.79	83-fuk/ogi <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1884-per, 01-mar/mck, 16-wil/bru, 33-tre/wat, 35-gui, 37-gin/bau, 39-bar/atc, 48-bro/bro, 48-wei, 50-pic/zie, 52-hel, 63-mcc/lai]

cont.



**2-Methyl-1-butanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	822.02 ± 0.95	320.00	797.24 ± 0.97	370.00	753.32 ± 0.49
293.15	819.48 ± 0.92	330.00	788.72 ± 0.89	380.00	744.15 ± 0.54
298.15	815.41 ± 0.90	340.00	780.07 ± 0.78	390.00	734.84 ± 0.73
300.00	813.89 ± 0.90	350.00	771.28 ± 0.65	400.00	725.40 ± 1.06
310.00	805.63 ± 0.98	360.00	762.37 ± 0.54		

**(S)-(-)-2-Methyl-1-butanol****[1565-80-6]****C<sub>5</sub>H<sub>12</sub>O****MW = 88.15****13**

**Table 1.** Fit with estimated *B* coefficient for 7 accepted points. Deviation  $\sigma_w = 0.464$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1047.24
<i>B</i>	-0.780

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	818.9 ± 0.5	0.32	38-whi/ole	293.15	818.3 ± 1.0	-0.29	38-whi/ole-1
293.15	818.8 ± 0.6	0.18	38-whi/ole-1	296.15	814.0 ± 1.5	-2.24	52-hel
300.65	813.0 ± 2.0	0.27	38-whi/ole-1	289.15	821.6 ± 0.5	-0.10	59-pin/lar
293.15	818.4 ± 1.0	-0.16	38-whi/ole-1				

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	828.8 ± 1.6
290.00	821.0 ± 1.0
293.15	818.6 ± 1.0
298.15	814.7 ± 1.2
310.00	805.4 ± 2.1

**2-Methyl-2-butanol**

[75-85-4]

C<sub>5</sub>H<sub>12</sub>O

MW = 88.15

14

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 1.1040$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 2.1679 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 268.15$ to $453.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.31063 \cdot 10^2$
B	$6.74937 \cdot 10^{-2}$
C	$-1.64419 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
374.75	724.10 ± 1.00	-1.35	1883-sch-3(X)	298.15	801.80 ± 2.00	-3.23	39-owe/qua <sup>1)</sup>
375.15	724.10 ± 1.00	-0.88	1884-sch-6(X)	308.15	792.30 ± 2.00	-3.44	39-owe/qua <sup>1)</sup>
273.15	827.00 ± 0.60	0.18	10-ric(X)	318.15	782.70 ± 2.00	-3.41	39-owe/qua <sup>1)</sup>
288.15	813.80 ± 0.50	-0.19	27-nor/reu(X)	328.15	773.10 ± 2.00	-3.06	39-owe/qua(X)
298.15	804.73 ± 0.50	-0.30	27-nor/reu <sup>1)</sup>	328.15	773.10 ± 2.00	-3.06	39-owe/qua <sup>1)</sup>
273.15	827.16 ± 0.60	0.34	32-tim/hen(X)	338.15	762.40 ± 0.50	-3.48	39-owe/qua <sup>1)</sup>
288.15	813.44 ± 0.60	-0.55	32-tim/hen(X)	273.15	825.00 ± 0.50	-1.82	58-cos/bow(X)
303.15	799.72 ± 0.60	-0.70	32-tim/hen <sup>1)</sup>	293.15	808.40 ± 0.50	-1.15	58-cos/bow <sup>1)</sup>
298.15	805.99 ± 0.60	0.96	35-but/ram(□)	313.15	790.00 ± 0.50	-0.96	58-cos/bow(X)
273.15	826.20 ± 2.00	-0.62	39-owe/qua <sup>1)</sup>	333.15	771.30 ± 0.50	0.24	58-cos/bow(X)
273.15	826.20 ± 0.50	-0.62	39-owe/qua(X)	353.15	750.40 ± 0.50	0.56	58-cos/bow(X)
298.15	801.80 ± 0.50	-3.23	39-owe/qua <sup>1)</sup>	373.15	728.10 ± 0.50	0.79	58-cos/bow(X)

<sup>1)</sup> Not included in Fig.

cont.

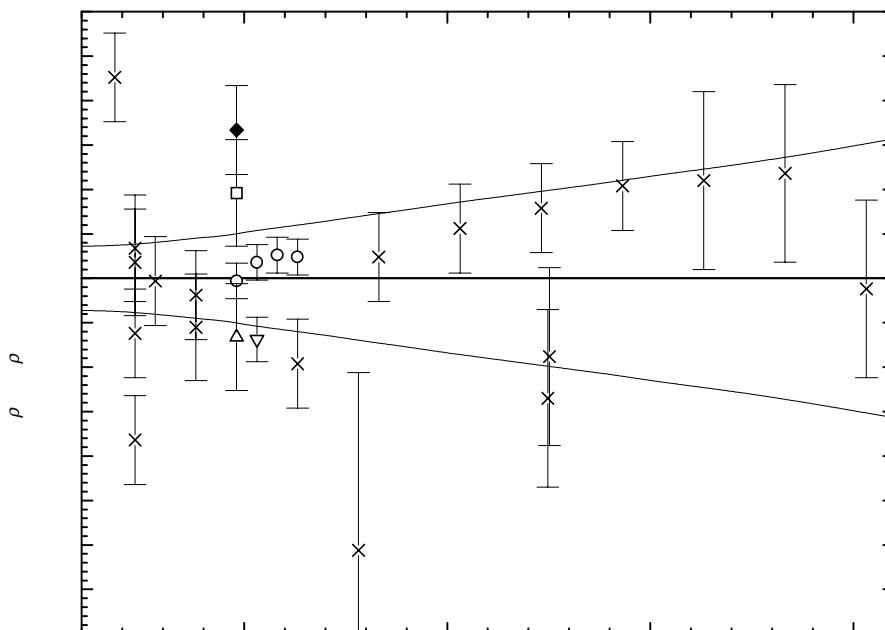
## 2-Methyl-2-butanol (cont.)

Table 2. (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
393.15	704.50 ± 0.50	1.04	58-cos/bow(✕)	298.15	806.90 ± 0.50	1.87	85-dap/don <sup>1)</sup>
413.15	679.40 ± 1.00	1.10	58-cos/bow(✕)	308.15	796.20 ± 0.50	0.46	85-dap/don <sup>1)</sup>
433.15	653.00 ± 1.00	1.18	58-cos/bow(✕)	298.15	804.37 ± 0.60	-0.66	85-tre/ben(Δ)
453.15	623.90 ± 1.00	-0.12	58-cos/bow(✕)	298.15	805.00 ± 0.20	-0.03	86-rig/mar(O)
303.15	799.73 ± 0.25	-0.69	75-hsu/cle(∇)	303.15	800.60 ± 0.20	0.18	86-rig/mar(O)
298.15	806.70 ± 0.50	1.67	82-dap/don(◆)	308.15	796.00 ± 0.20	0.26	86-rig/mar(O)
268.15	833.20 ± 0.50	2.26	85-dap/don(✕)	313.15	791.20 ± 0.20	0.24	86-rig/mar(O)
278.15	822.60 ± 0.50	-0.03	85-dap/don(✕)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1878-wis, 1884-per, 1893-tho/jon, 19-eyk, 26-mun, 33-nev/jat, 35-mah-1, 36-par, 37-gin/bau, 48-wei, 50-pic/zie, 51-lev/fai, 52-coo, 55-soe/fre, 57-pet/sus, 58-pan/osi, 63-mcc/lai, 67-gol/per, 76-tri/kri, 88-cab/bar, 96-nik/jad, 98-pai/che, 98-sen].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)]^{1/3} + 0.75(1 - T/T_c)[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
260.00	837.46 ± 0.36	320.00	784.30 ± 0.64	400.00	694.99 ± 1.15
270.00	829.43 ± 0.37	330.00	774.28 ± 0.71	410.00	682.35 ± 1.21
280.00	821.06 ± 0.41	340.00	763.94 ± 0.77	420.00	669.38 ± 1.27
290.00	812.36 ± 0.46	350.00	753.27 ± 0.84	430.00	656.07 ± 1.34
293.15	809.55 ± 0.47	360.00	742.27 ± 0.90	440.00	642.45 ± 1.41
298.15	805.03 ± 0.50	370.00	730.95 ± 0.96	450.00	628.49 ± 1.49
300.00	803.33 ± 0.52	380.00	719.29 ± 1.02	460.00	614.20 ± 1.57
310.00	793.98 ± 0.58	390.00	707.30 ± 1.08		

**3-Methyl-1-butanol****[123-51-3]****C<sub>5</sub>H<sub>12</sub>O****MW = 88.15****15****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 9.8281 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.2532 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 347.85 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.89389 \cdot 10^2$
B	$1.88877 \cdot 10^{-1}$
C	$-1.56150 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

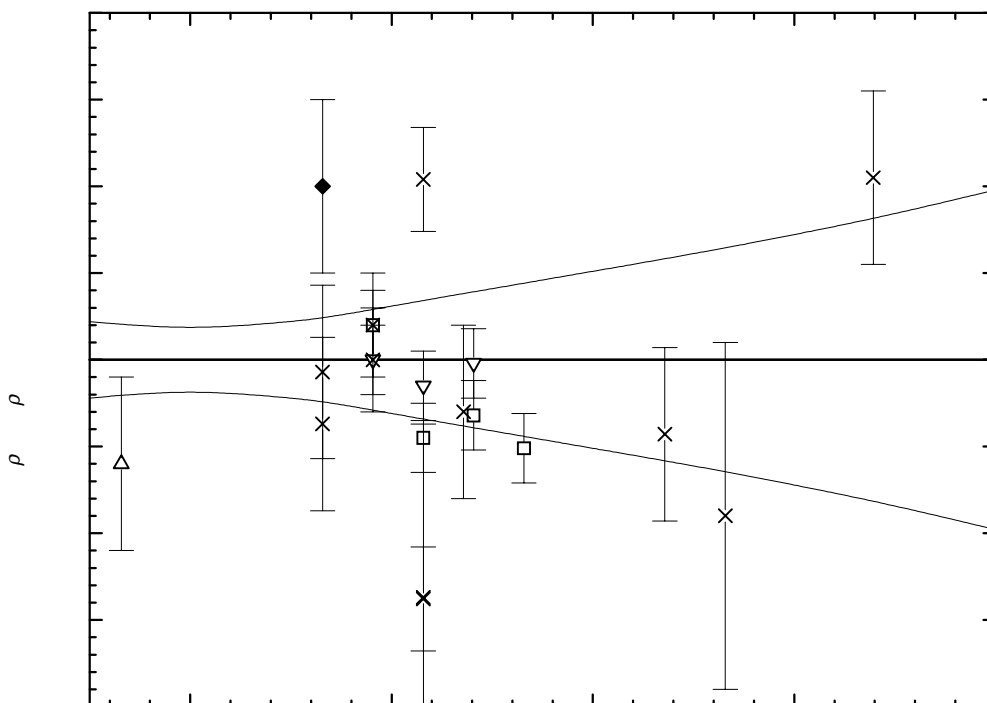
$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
285.45	815.83 ± 0.00	-0.24	11-sch <sup>1)</sup>	303.15	804.19 ± 0.30	1.04	85-rao/red(✗)
307.15	799.79 ± 0.50	-0.30	11-sch(✗)	303.15	801.77 ± 0.30	-1.38	86-mou/nai(✗)
327.15	783.63 ± 0.50	-0.43	11-sch(✗)	298.15	807.10 ± 0.20	0.20	86-rig/mar(□)
347.85	767.20 ± 0.50	1.05	11-sch(✗)	303.15	802.70 ± 0.20	-0.45	86-rig/mar(□)
293.15	810.50 ± 0.50	-0.07	26-mat(✗)	308.15	799.00 ± 0.20	-0.32	86-rig/mar(□)
293.15	810.20 ± 0.50	-0.37	28-mon(✗)	313.15	794.90 ± 0.20	-0.51	86-rig/mar(□)
273.15	823.88 ± 0.50	-0.60	29-tim/hen(Δ)	303.15	801.78 ± 1.00	-1.37	92-kum/sre(✗)
288.15	812.87 ± 1.00	-1.29	29-tim/hen <sup>1)</sup>	298.15	806.90 ± 0.20	0.00	92-tan/mur(✗)
303.15	801.73 ± 1.00	-1.42	29-tim/hen <sup>1)</sup>	298.15	806.90 ± 0.20	0.00	93-ami/rai(∇)
293.15	808.60 ± 2.00	-1.97	56-tor-1 <sup>1)</sup>	303.15	803.00 ± 0.20	-0.15	93-ami/rai(∇)
313.15	793.80 ± 2.00	-1.61	56-tor-1 <sup>1)</sup>	308.15	799.30 ± 0.20	-0.02	93-ami/rai(∇)
333.15	778.10 ± 1.00	-0.90	56-tor-1(✗)	298.15	807.10 ± 0.30	0.20	98-sen(✗)
293.15	811.57 ± 0.50	1.00	81-joo/ar(◆)				

<sup>1)</sup> Not included in Fig. 1.

cont.

**3-Methyl-1-butanol** (cont.)

**Further references:** [1876-bal, 1884-per, 1884-sch-6, 1886-tra, 1891-sch/kos, 1893-tho/jon, 1898-kah, 04-bru/sch, 07-che-1, 08-ric/mat, 13-muc, 14-eng/tur, 16-wro/rei, 21-rei/hic, 23-pop, 26-han, 26-mun, 27-krc/wil, 27-nor/cor, 28-har-2, 28-llo/bro, 33-nev/jat, 35-but/ram, 35-cou/hop, 35-mah-1, 36-spe, 36-tom, 37-gin/bau, 41-hus/age, 42-boh, 42-mul, 43-boh, 45-add, 48-vog-2, 48-wei, 49-udo/kal, 50-pic/zie, 52-coo, 53-par/cha, 56-ike/kep, 57-ano-1, 57-pet/sus, 57-rom-1, 58-arn/was, 60-ter/kep, 63-mcc/lai, 63-raj/ran, 65-red/rao, 67-gol/per, 68-ana/rao, 68-ano, 71-abr/ber, 71-tha/rao, 79-sub/rao, 82-dap/don, 82-kar/red, 87-isl/qua].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	826.55 ± 0.22	298.15	806.90 ± 0.29	330.00	781.67 ± 0.61
280.00	819.85 ± 0.17	300.00	805.52 ± 0.31	340.00	773.10 ± 0.72
290.00	812.84 ± 0.22	310.00	797.88 ± 0.41	350.00	764.21 ± 0.84
293.15	810.57 ± 0.24	320.00	789.93 ± 0.51	360.00	755.01 ± 0.98

## 3-Methyl-2-butanol

[598-75-4]

C<sub>5</sub>H<sub>12</sub>O

MW = 88.15

16

**Table 1.** Coefficients of the polynomial expansion equation.

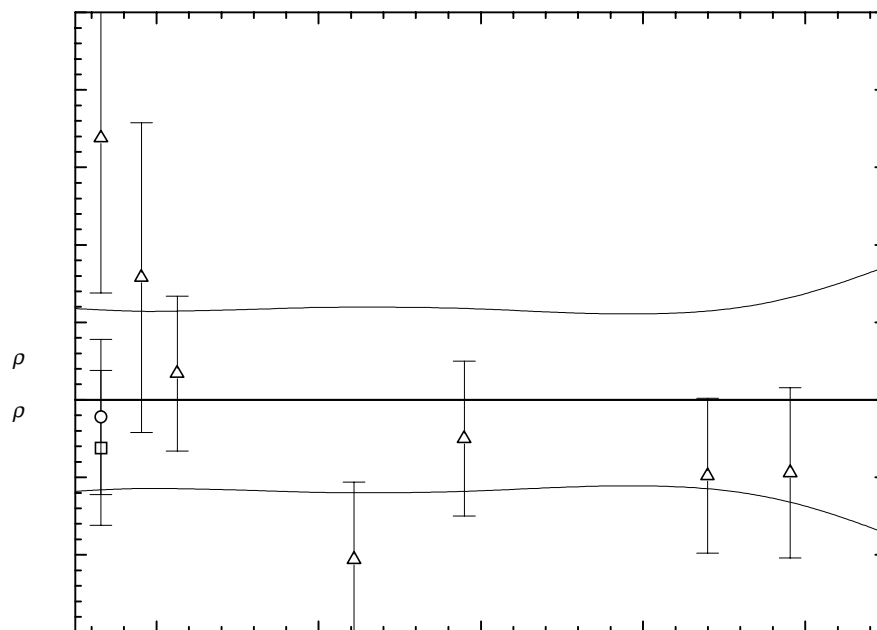
Standard deviations (see introduction):

 $\sigma_{c,w} = 7.5344 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.8698 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $378.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.82581 \cdot 10^2$
B	$3.69971 \cdot 10^{-1}$
C	$-2.00997 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	$818.00 \pm 0.50$	-0.31	12-pic/ken(□)	324.35	$790.10 \pm 0.50$	-1.03	63-tho/mea(Δ)
293.15	$818.20 \pm 0.50$	-0.11	50-pic/zie(O)	337.95	$777.80 \pm 0.50$	-0.25	63-tho/mea(Δ)
293.15	$820.00 \pm 1.00$	1.69	63-tho/mea(Δ)	353.05	$759.80 \pm 0.50$	-2.87	63-tho/mea <sup>1)</sup>
298.15	$815.00 \pm 1.00$	0.79	63-tho/mea(Δ)	367.95	$746.10 \pm 0.50$	-0.49	63-tho/mea(Δ)
302.55	$810.70 \pm 0.50$	0.17	63-tho/mea(Δ)	378.15	$734.60 \pm 0.55$	-0.47	63-tho/mea(Δ)

<sup>1)</sup> Not included in Fig. 1.**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**3-Methyl-2-butanol** (cont.)

**Further references:** [1876-mun, 1878-win, 1878-wis, 33-ste, 37-gin/bau, 38-whi/joh, 48-mcm/rop, 52-coo, 63-mcc/lai].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	820.83 ± 0.59	320.00	795.15 ± 0.60	370.00	744.31 ± 0.57
293.15	818.31 ± 0.58	330.00	785.79 ± 0.60	380.00	732.93 ± 0.67
298.15	814.21 ± 0.57	340.00	776.02 ± 0.59	390.00	721.15 ± 0.86
300.00	812.68 ± 0.57	350.00	765.85 ± 0.56		
310.00	804.11 ± 0.58	360.00	755.28 ± 0.55		

**(S)-3-Methyl-2-butanol** [500029-41-4] C<sub>5</sub>H<sub>12</sub>O MW = 88.15 17

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	810.0 ± 2.0	33-ste

**1-Pentanol** [71-41-0] C<sub>5</sub>H<sub>12</sub>O MW = 88.15 18

$T_c = 588.00 \text{ K}$  [89-tej/lee]

$\rho_c = 270.00 \text{ kg} \cdot \text{m}^{-3}$  [89-tej/lee]

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_l = 7.5696 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (6.3480 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 3.3635 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 213.15 \text{ to } 470.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 470.00 \text{ to } 588.00 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$1.10034 \cdot 10^3$	$1.06991 \cdot 10^0$
B	$-1.58026 \cdot 10^0$	$-1.91438 \cdot 10^{-2}$
C	$3.34384 \cdot 10^{-3}$	$1.56345 \cdot 10^{-4}$
D	$-4.34342 \cdot 10^{-6}$	$-4.63597 \cdot 10^{-7}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	829.60 ± 0.50	-0.06	26-han(✕)	400.00	724.98 ± 0.20	-0.29	76-hal/ell(✕)
273.15	829.61 ± 0.20	-0.05	32-ell/rei(✕)	420.00	704.25 ± 0.20	-0.44	76-hal/ell(✕)
298.15	811.59 ± 0.20	0.28	32-ell/rei <sup>1)</sup>	440.00	681.80 ± 0.25	-0.60	76-hal/ell(✕)
213.15	873.00 ± 1.00	-0.36	58-cos/bow(✕)	460.00	657.53 ± 0.25	-0.67	76-hal/ell <sup>1)</sup>
233.15	858.10 ± 1.00	-0.52	58-cos/bow(✕)	470.00	644.61 ± 0.30	-0.71	76-hal/ell <sup>1)</sup>
253.15	843.00 ± 1.00	-1.12	58-cos/bow(✕)	480.00	631.11 ± 0.30	-0.40	76-hal/ell(✕)
273.15	827.80 ± 1.00	-1.86	58-cos/bow <sup>1)</sup>	490.00	616.92 ± 0.30	0.14	76-hal/ell(✕)
293.15	813.30 ± 1.00	-1.72	58-cos/bow <sup>1)</sup>	288.15	818.20 ± 0.30	-0.51	78-dap/don(✕)
313.15	798.10 ± 1.00	-1.91	58-cos/bow <sup>1)</sup>	298.15	810.90 ± 0.30	-0.41	78-dap/don <sup>1)</sup>
333.15	783.40 ± 1.00	-1.00	58-cos/bow <sup>1)</sup>	308.15	803.90 ± 0.30	0.09	78-dap/don <sup>1)</sup>
353.15	768.00 ± 1.00	0.00	58-cos/bow <sup>1)</sup>	318.15	796.00 ± 0.30	-0.17	78-dap/don <sup>1)</sup>
373.15	751.50 ± 1.00	0.91	58-cos/bow <sup>1)</sup>	303.15	807.58 ± 0.20	0.00	78-red/nai-1 <sup>1)</sup>
393.15	735.60 ± 2.00	3.64	58-cos/bow(✕)	313.15	799.92 ± 0.20	-0.09	78-red/nai-1(✕)
413.15	718.40 ± 2.00	6.48	58-cos/bow <sup>1)</sup>	298.15	810.97 ± 0.15	-0.34	79-dia/tar(V)
433.15	698.30 ± 2.00	8.06	58-cos/bow <sup>1)</sup>	308.15	803.61 ± 0.15	-0.20	79-dia/tar(V)
453.15	675.40 ± 2.00	8.68	58-cos/bow <sup>1)</sup>	318.15	796.05 ± 0.15	-0.12	79-dia/tar(V)
273.15	830.83 ± 0.10	1.17	59-mck/ski(Δ)	333.15	784.44 ± 0.15	0.04	79-dia/tar(V)
273.15	831.00 ± 1.50	1.34	66-efr <sup>1)</sup>	278.15	825.34 ± 0.20	-0.68	83-dap/del(◆)
293.15	815.00 ± 1.50	-0.02	66-efr <sup>1)</sup>	288.15	818.21 ± 0.20	-0.50	83-dap/del(◆)
313.15	800.00 ± 1.50	-0.01	66-efr <sup>1)</sup>	298.15	811.34 ± 0.20	0.03	83-dap/del <sup>1)</sup>
333.15	780.00 ± 1.50	-4.40	66-efr <sup>1)</sup>	308.15	803.50 ± 0.20	-0.31	83-dap/del(◆)
353.15	784.00 ± 1.50	16.00	66-efr <sup>1)</sup>	318.15	795.83 ± 0.20	-0.34	83-dap/del(◆)
373.15	752.00 ± 1.50	1.41	66-efr <sup>1)</sup>	298.15	810.86 ± 0.10	-0.45	84-sak/nak(O)
393.15	732.00 ± 1.50	0.04	66-efr <sup>1)</sup>	268.15	839.00 ± 0.50	5.72	85-dap/don(✕)
413.15	712.00 ± 1.50	0.08	66-efr(✕)	278.15	825.30 ± 0.50	-0.72	85-dap/don(✕)
433.15	690.00 ± 1.50	-0.24	66-efr(✕)	298.15	810.90 ± 0.50	-0.41	85-dap/don <sup>1)</sup>
453.15	665.00 ± 1.50	-1.72	66-efr(✕)	308.15	803.90 ± 0.50	0.09	85-dap/don <sup>1)</sup>
473.15	640.00 ± 1.50	-1.11	66-efr(✕)	298.15	811.00 ± 0.20	-0.31	86-rig/mar <sup>1)</sup>
493.15	612.00 ± 1.50	-0.01	66-efr(✕)	303.15	807.30 ± 0.20	-0.28	86-rig/mar <sup>1)</sup>
513.15	581.00 ± 1.50	0.43	66-efr(✕)	308.15	803.90 ± 0.20	0.09	86-rig/mar(✕)
533.15	545.00 ± 1.50	-0.47	66-efr(✕)	313.15	799.90 ± 0.20	-0.11	86-rig/mar(✕)
553.15	500.00 ± 2.00	-0.71	66-efr(✕)	323.15	792.18 ± 0.10	-0.11	93-gar/ban-1(□)
563.15	471.00 ± 2.00	-0.02	66-efr(✕)	328.15	788.92 ± 0.10	0.55	93-gar/ban-1(□)
568.15	454.00 ± 2.00	0.84	66-efr(✕)	333.15	784.39 ± 0.10	-0.01	93-gar/ban-1(□)
573.15	434.00 ± 3.00	1.63	66-efr(✕)	338.15	780.59 ± 0.10	0.21	93-gar/ban-1(□)
578.15	410.00 ± 3.00	2.82	66-efr(✕)	343.15	776.19 ± 0.10	-0.12	93-gar/ban-1(□)
583.15	365.00 ± 5.00	-8.61	66-efr(✕)	348.15	771.92 ± 0.10	-0.27	93-gar/ban-1(□)
584.15	350.00 ± 5.00	-14.84	66-efr(✕)	353.15	768.08 ± 0.10	0.08	93-gar/ban-1(□)
585.15	324.00 ± 5.00	-30.71	66-efr <sup>1)</sup>	358.15	763.64 ± 0.10	-0.11	93-gar/ban-1(□)
293.15	814.45 ± 0.20	-0.57	76-hal/ell(✕)	363.15	759.36 ± 0.10	-0.07	93-gar/ban-1(□)
298.15	810.80 ± 0.20	-0.51	76-hal/ell <sup>1)</sup>	373.15	750.46 ± 0.10	-0.13	93-gar/ban-1(□)
303.15	807.12 ± 0.20	-0.46	76-hal/ell <sup>1)</sup>	278.15	825.34 ± 0.40	-0.68	94-rom/pel(✕)
320.00	794.46 ± 0.20	-0.28	76-hal/ell(✕)	288.15	818.10 ± 0.40	-0.61	94-rom/pel <sup>1)</sup>
340.00	778.81 ± 0.20	-0.07	76-hal/ell(✕)	298.15	810.87 ± 0.40	-0.44	94-rom/pel <sup>1)</sup>
360.00	762.11 ± 0.20	-0.05	76-hal/ell(✕)	308.15	803.40 ± 0.40	-0.41	94-rom/pel <sup>1)</sup>
380.00	744.25 ± 0.20	-0.11	76-hal/ell(✕)				

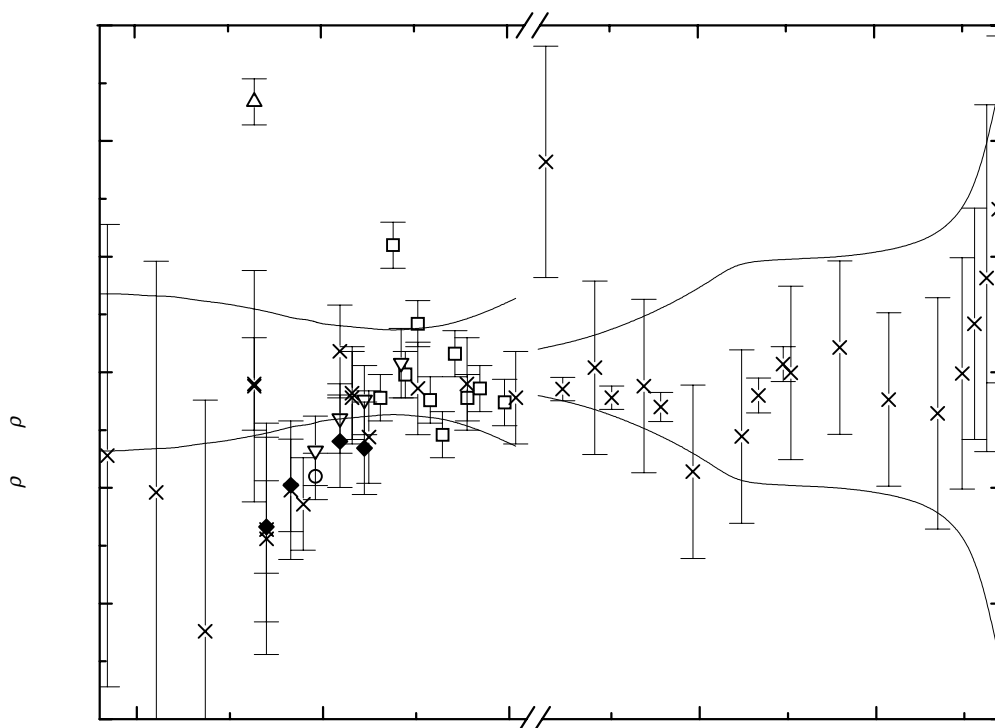
<sup>1)</sup> Not included in Fig. 1..

cont.



**1-Pentanol** (cont.)

**Further references:** [1854-kop, 1864-lan, 1871-lie/ros-3, 1880-bru-1, 1883-sch-3, 1884-zan, 1886-gar, 1892-lan/jah, 1894-jah/mol, 13-kis-3, 13-rom, 23-pop, 24-bou, 24-bus-1, 24-lie, 27-ver/coo, 28-llo/bro, 29-sim, 30-err/she, 30-she, 32-tim/hen, 33-but/tho, 35-but/ram, 39-lar/hun, 45-add, 48-jon/bow, 48-lad/smi, 48-vog-2, 48-wei, 49-tsc/ric, 50-mum/phi, 50-pic/zie, 50-sac/sau, 52-coo, 52-von, 54-dub/luf, 59-ale, 59-lis/kor, 63-hov/sea, 63-tho/mea, 67-gol/per, 68-ano, 70-mye/cle, 73-khi/ale, 73-min/rue, 74-rao/nai, 74-rao/nai-1, 75-mat/fer, 76-kow/kas, 76-red/nai, 78-ast, 78-paz/gar, 78-tre/ben, 79-gyl/apa, 79-kiy/ben, 81-joo/ar1, 81-nai/nai, 81-sjo/dyh, 82-kar/red, 82-nai/nai, 82-ort, 82-ven/dha, 83-fuk/ogi, 85-fer/pin, 85-ort/paz-1, 85-sar/paz, 86-ash/sri, 86-ort/paz-1, 86-san/sha, 86-tan/toy, 87-fer/ber, 89-ala/sal, 89-ort/sus, 89-vij/nai, 90-sri/nai, 90-vij/nai, 91-gar/her, 91-ram/muk, 91-yos/kat, 93-ami/ara, 93-ami/rai, 94-kim/lee, 94-kum/nai, 94-kum/nai-1, 94-ven/ven, 94-yu /tsa-1, 95-org/igl, 95-red/ram-1, 96-elb, 98-ami/ban, 98-ami/pat-1, 98-pai/che].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**1-Pentanol** (cont.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
210.00	875.72 ± 0.34	330.00	786.91 ± 0.18	470.00	645.32 ± 1.86
220.00	868.27 ± 0.34	340.00	778.88 ± 0.19	480.00	631.51 ± 1.93
230.00	860.92 ± 0.33	350.00	770.64 ± 0.20	490.00	616.78 ± 1.95
240.00	853.64 ± 0.33	360.00	762.16 ± 0.23	500.00	601.48 ± 1.97
250.00	846.40 ± 0.31	370.00	753.41 ± 0.27	510.00	585.68 ± 1.99
260.00	839.17 ± 0.30	380.00	744.36 ± 0.32	520.00	569.16 ± 2.03
270.00	831.94 ± 0.28	390.00	734.99 ± 0.40	530.00	551.43 ± 2.09
280.00	824.68 ± 0.26	400.00	725.27 ± 0.49	540.00	531.69 ± 2.18
290.00	817.35 ± 0.23	410.00	715.18 ± 0.60	550.00	508.81 ± 2.33
293.15	815.02 ± 0.23	420.00	704.69 ± 0.74	560.00	481.13 ± 2.62
298.15	811.31 ± 0.22	430.00	693.77 ± 0.91	570.00	445.87 ± 3.28
300.00	809.93 ± 0.21	440.00	682.40 ± 1.10	580.00	396.14 ± 5.29
310.00	802.41 ± 0.20	450.00	670.55 ± 1.32		
320.00	794.74 ± 0.19	460.00	658.20 ± 1.57		

**d-2-Pentanol**

[31087-44-2]

C<sub>5</sub>H<sub>12</sub>O

MW = 88.15

19

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.785$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1039.28
<i>B</i>	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	810.1 ± 1.0	-0.52	43-bra
298.15	807.9 ± 1.5	1.18	56-ike/kep
298.15	816.1 ± 3.0	9.38	60-ter/kep <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	813.1 ± 1.2
293.15	810.6 ± 1.1
298.15	806.7 ± 1.1

## 2-Pentanol

[6032-29-7]

C<sub>5</sub>H<sub>12</sub>O

MW = 88.15

20

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 5.1481 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 9.2505 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 233.15$ to $381.35$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.37043 \cdot 10^2$
B	$-5.69541 \cdot 10^{-2}$
C	$-1.29071 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	$824.79 \pm 0.50$	-0.39	32-ell/rei(X)	293.25	$806.90 \pm 0.50$	-2.45	63-tho/mea <sup>1)</sup>
298.15	$805.26 \pm 0.50$	-0.07	32-ell/rei <sup>1)</sup>	303.25	$801.50 \pm 0.50$	0.42	63-tho/mea <sup>1)</sup>
273.15	$824.68 \pm 0.50$	-0.50	32-tim/hen(X)	314.45	$792.30 \pm 0.50$	0.79	63-tho/mea(X)
288.15	$813.17 \pm 0.50$	-0.29	32-tim/hen(X)	323.95	$783.60 \pm 0.60$	0.46	63-tho/mea(X)
303.15	$801.18 \pm 0.50$	0.02	32-tim/hen <sup>1)</sup>	347.75	$761.70 \pm 0.60$	0.55	63-tho/mea(X)
298.15	$805.25 \pm 0.30$	-0.08	35-but/ram(♦)	366.65	$742.80 \pm 0.60$	0.15	63-tho/mea(X)
293.15	$808.80 \pm 0.40$	-0.63	50-pic/zie(X)	381.35	$727.40 \pm 0.70$	-0.22	63-tho/mea(X)
293.15	$809.70 \pm 0.30$	0.27	52-coo(O)	298.15	$805.60 \pm 0.30$	0.27	82-dap/don(V)
293.15	$809.80 \pm 0.40$	0.37	54-pom/foo-1(X)	298.15	$805.16 \pm 0.30$	-0.17	86-ort/paz-1(Δ)
233.15	$854.90 \pm 1.00$	1.30	58-cos/bow(X)	303.15	$800.97 \pm 0.30$	-0.19	86-ort/paz-1(Δ)
253.15	$840.20 \pm 0.60$	0.29	58-cos/bow(X)	308.15	$796.97 \pm 0.30$	0.04	86-ort/paz-1(Δ)
273.15	$824.60 \pm 0.60$	-0.58	58-cos/bow(X)	318.15	$788.26 \pm 0.30$	-0.02	86-ort/paz-1(Δ)
293.15	$808.90 \pm 0.60$	-0.53	58-cos/bow <sup>1)</sup>	323.15	$783.75 \pm 0.30$	-0.10	86-ort/paz-1(Δ)
313.15	$791.90 \pm 0.60$	-0.74	58-cos/bow <sup>1)</sup>	298.15	$805.50 \pm 0.20$	0.17	86-rig/mar(□)
333.15	$774.20 \pm 0.60$	-0.61	58-cos/bow(X)	303.15	$801.00 \pm 0.20$	-0.16	86-rig/mar(□)
353.15	$755.10 \pm 0.70$	-0.86	58-cos/bow(X)	308.15	$796.90 \pm 0.20$	-0.03	86-rig/mar(□)
373.15	$730.40 \pm 0.70$	-5.67	58-cos/bow <sup>1)</sup>	313.15	$792.80 \pm 0.20$	0.16	86-rig/mar(□)

<sup>1)</sup> Not included in Fig. 1.**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

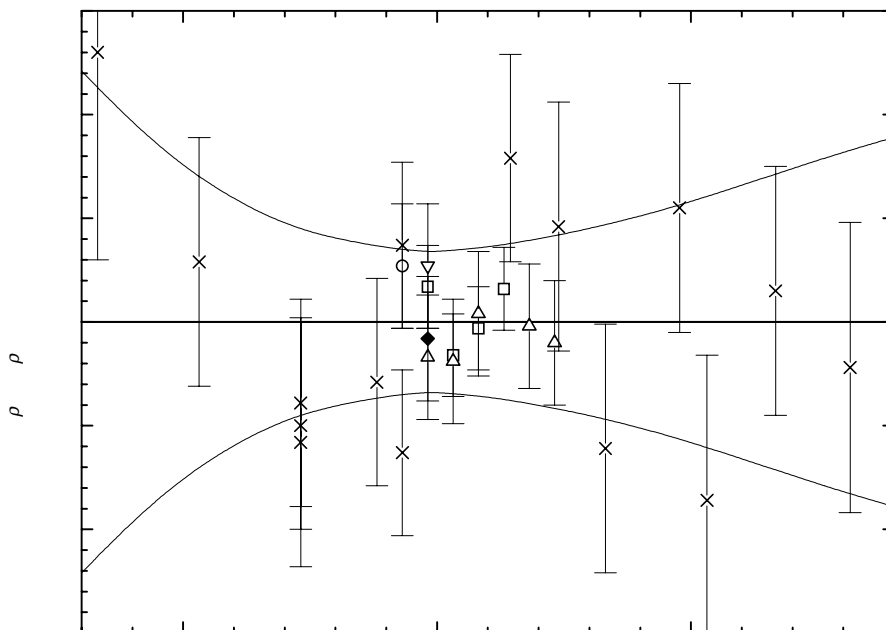
$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
230.00	$855.66 \pm 1.21$	293.15	$809.43 \pm 0.35$	350.00	$759.00 \pm 0.58$
240.00	$849.03 \pm 0.96$	298.15	$805.33 \pm 0.34$	360.00	$749.26 \pm 0.66$
250.00	$842.13 \pm 0.75$	300.00	$803.79 \pm 0.34$	370.00	$739.27 \pm 0.74$
260.00	$834.98 \pm 0.59$	310.00	$795.35 \pm 0.36$	380.00	$729.02 \pm 0.82$
270.00	$827.57 \pm 0.47$	320.00	$786.65 \pm 0.40$	390.00	$718.51 \pm 0.89$
280.00	$819.90 \pm 0.40$	330.00	$777.69 \pm 0.45$		
290.00	$811.98 \pm 0.36$	340.00	$768.47 \pm 0.51$		

cont.

**2-Pentanol** (cont.)

**Further references:** [1876-lin, 11-pic/ken, 14-vav, 19-eyk, 23-bru, 23-clo/joh, 25-fai, 26-mun, 27-nor/cor, 30-err/she, 36-nor/has, 37-gin/bau, 56-goe/mcc, 63-mcc/lai].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3-Pentanol**

[584-02-1]

C<sub>5</sub>H<sub>12</sub>O

MW = 88.15

21

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviation (see introduction):

$\sigma_{c,w} = 1.0029$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.4273 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $381.35$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.59951 \cdot 10^2$
B	$-9.37135 \cdot 10^{-2}$
C	$-1.30516 \cdot 10^{-3}$

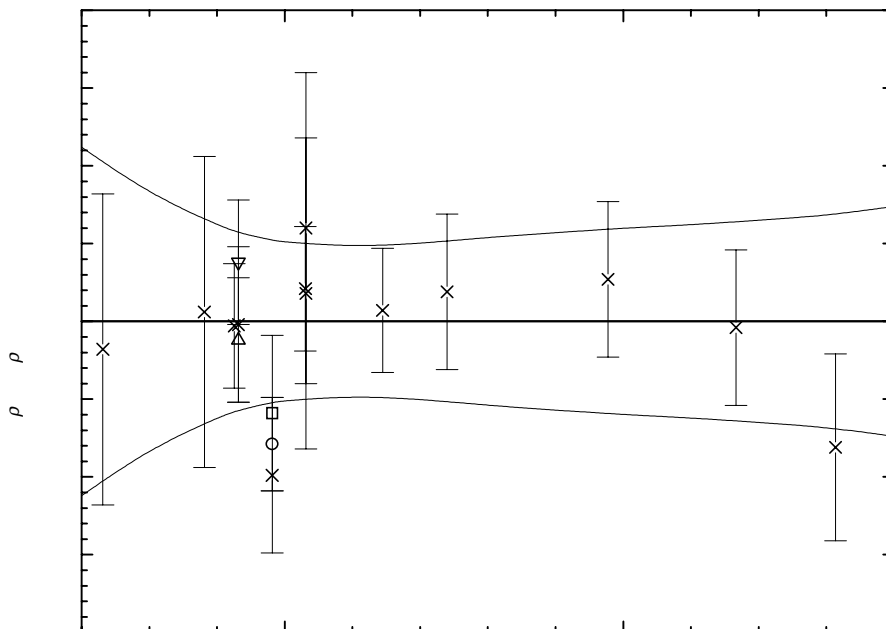
cont.

## 3-Pentanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
298.15	815.40 ± 0.50	-0.59	23-bru(□)	292.55	820.80 ± 0.40	-0.03	63-tho/mea(×)
273.15	836.79 ± 1.00	-0.18	32-tim/hen(×)	303.05	811.90 ± 0.40	0.21	63-tho/mea(×)
288.15	824.64 ± 1.00	0.06	32-tim/hen(×)	314.45	801.50 ± 0.40	0.07	63-tho/mea(×)
303.15	811.78 ± 1.00	0.18	32-tim/hen(×)	323.97	792.80 ± 0.50	0.19	63-tho/mea(×)
303.15	812.20 ± 1.00	0.60	33-nev/jat(×)	347.75	769.80 ± 0.50	0.27	63-tho/mea(×)
293.15	820.20 ± 0.40	-0.12	50-lad/smi(Δ)	366.65	750.10 ± 0.50	-0.04	63-tho/mea(×)
293.15	820.30 ± 0.50	-0.02	50-pic/zie(×)	381.35	733.60 ± 0.60	-0.81	63-tho/mea(×)
293.15	820.70 ± 0.40	0.38	54-pom/foo-1(∇)	298.15	815.20 ± 0.30	-0.79	82-dap/don(O)
298.15	815.00 ± 0.50	-0.99	63-mcc/lai(×)				

**Further references:** [1875-wag/say, 13-pic/ken, 14-vav, 19-eyk, 27-nor/cor, 30-err/she, 35-les/lom, 36-spe, 37-gin/bau, 37-she/mat, 40-whi/sur, 48-wei, 52-coo, 53-ano-1, 56-goe/mcc, 56-shu/bel].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	839.50 ± 1.12	300.00	814.37 ± 0.51	350.00	767.27 ± 0.60
280.00	831.39 ± 0.82	310.00	805.47 ± 0.48	360.00	757.07 ± 0.62
290.00	823.01 ± 0.62	320.00	796.31 ± 0.50	370.00	746.60 ± 0.65
293.15	820.32 ± 0.57	330.00	786.89 ± 0.54	380.00	735.87 ± 0.68
298.15	815.99 ± 0.52	340.00	777.21 ± 0.57	390.00	724.89 ± 0.74

**2,2-Dimethyl-1-butanol****[1185-33-7]****C<sub>6</sub>H<sub>14</sub>O****MW = 102.18****22****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 3.0286 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 9.4262 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 278.15$ to $408.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.76530 \cdot 10^2$
B	$-2.16929 \cdot 10^{-1}$
C	$-9.82641 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
278.15	841.01 ± 0.40	0.84	40-hov/lan-2(□)	368.15	763.86 ± 0.40	0.37	40-hov/lan-2(□)
288.15	832.37 ± 0.40	-0.06	40-hov/lan-2(□)	378.15	754.30 ± 0.40	0.32	40-hov/lan-2(□)
298.15	824.27 ± 0.40	-0.23	40-hov/lan-2(□)	388.15	744.38 ± 0.40	0.10	40-hov/lan-2(□)
308.15	816.20 ± 0.40	-0.18	40-hov/lan-2(□)	398.15	734.38 ± 0.40	-0.01	40-hov/lan-2(□)
318.15	807.90 ± 0.40	-0.15	40-hov/lan-2(□)	408.15	724.02 ± 0.40	-0.28	40-hov/lan-2(□)
328.15	799.47 ± 0.40	-0.06	40-hov/lan-2(□)	293.15	828.30 ± 0.60	-0.19	50-pic/zie(O)
338.15	790.97 ± 0.40	0.16	40-hov/lan-2(□)	293.15	827.50 ± 1.00	-0.99	64-blo/hag(Δ)
348.15	782.03 ± 0.40	0.13	40-hov/lan-2(□)	293.15	828.50 ± 1.00	0.01	65-shu/puz(V)
358.15	773.02 ± 0.40	0.23	40-hov/lan-2(□)				

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

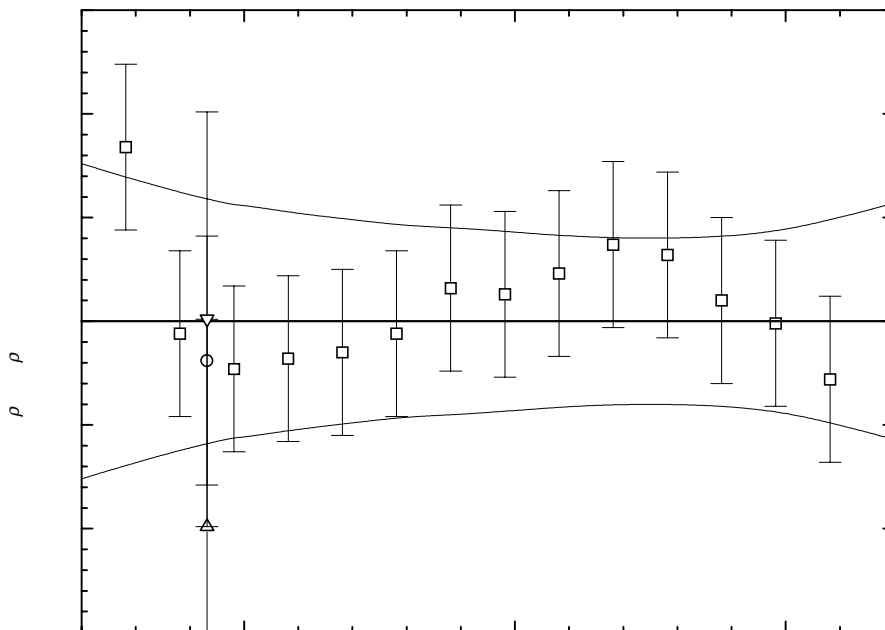
$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	846.32 ± 0.76	310.00	814.85 ± 0.52	370.00	761.74 ± 0.40
280.00	838.75 ± 0.68	320.00	806.49 ± 0.49	380.00	752.20 ± 0.40
290.00	830.98 ± 0.61	330.00	797.93 ± 0.46	390.00	742.47 ± 0.41
293.15	828.49 ± 0.59	340.00	789.18 ± 0.45	400.00	732.54 ± 0.44
298.15	824.50 ± 0.56	350.00	780.23 ± 0.43	410.00	722.41 ± 0.50
300.00	823.01 ± 0.56	360.00	771.09 ± 0.41	420.00	712.08 ± 0.57

cont.

**2,2-Dimethyl-1-butanol** (cont.)

**Further references:** [04-bou/bla-2, 38-gin/web].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**2,3-Dimethyl-1-butanol**

[19550-30-2]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

23

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	823.7 ± 2.0	59-tsu/hay <sup>1)</sup>	293.15	830.1 ± 0.6	50-pic/zie
293.65	829.7 ± 0.6	13-gor	293.15	830.6 ± 1.0	52-coo
298.15	823.0 ± 2.0	35-lev/mar <sup>1)</sup>	293.15	830.0 ± 0.6	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**(R)-2,3-Dimethyl-1-butanol**

[15019-27-9]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

24

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	823.7 ± 0.8	59-tsu/hay

## 2,3-Dimethyl-2-butanol

[594-60-5]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

25

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 6.3478 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.4692 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $388.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.39911 \cdot 10^2$
B	$6.32414 \cdot 10^{-2}$
C	$-1.58086 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	$838.60 \pm 1.00$	-0.64	1879-pav(∇)	348.15	$770.02 \pm 0.20$	-0.29	41-hov/lan(□)
292.15	$821.90 \pm 1.00$	-1.56	1879-pav(∇)	358.15	$759.67 \pm 0.20$	-0.11	41-hov/lan(□)
278.15	$835.11 \pm 0.20$	-0.08	41-hov/lan(□)	368.15	$748.92 \pm 0.20$	-0.01	41-hov/lan(□)
288.15	$826.76 \pm 0.20$	-0.11	41-hov/lan(□)	378.15	$738.04 \pm 0.20$	0.27	41-hov/lan(□)
298.15	$818.59 \pm 0.20$	0.35	41-hov/lan(□)	388.15	$726.36 \pm 0.20$	0.07	41-hov/lan(□)
308.15	$809.51 \pm 0.20$	0.22	41-hov/lan(□)	293.15	$823.60 \pm 0.40$	1.00	47-hov/mea(○)
318.15	$799.84 \pm 0.20$	-0.18	41-hov/lan(□)	298.15	$819.30 \pm 0.40$	1.06	47-hov/mea(○)
328.15	$790.56 \pm 0.20$	0.13	41-hov/lan(□)	293.15	$822.30 \pm 0.60$	-0.30	50-pic/zie(Δ)
338.15	$780.70 \pm 0.20$	0.17	41-hov/lan(□)				

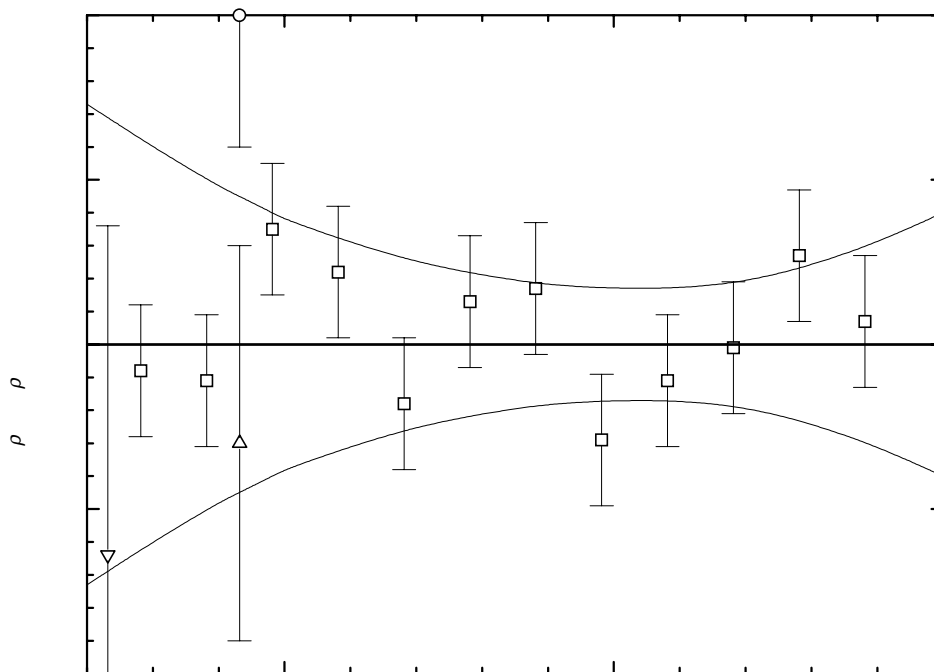
**Further references:** [1873-fri/sil, 52-lev/tan, 52-ove/ber].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	$841.74 \pm 0.73$	310.00	$807.60 \pm 0.31$	370.00	$746.89 \pm 0.19$
280.00	$833.68 \pm 0.60$	320.00	$798.27 \pm 0.25$	380.00	$735.67 \pm 0.24$
290.00	$825.30 \pm 0.48$	330.00	$788.62 \pm 0.21$	390.00	$724.13 \pm 0.31$
293.15	$822.60 \pm 0.45$	340.00	$778.67 \pm 0.18$	400.00	$712.27 \pm 0.40$
298.15	$818.24 \pm 0.40$	350.00	$768.39 \pm 0.17$		
300.00	$816.61 \pm 0.38$	360.00	$757.80 \pm 0.17$		

cont.



**2,3-Dimethyl-2-butanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3,3-Dimethyl-1-butanol**

[624-95-3]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

26

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
297.15	814.0 ± 2.0	41-hus/age
288.15	844.0 ± 10.0	49-mal/vol
298.15	809.7 ± 2.0	56-sar/new

**3,3-Dimethyl-2-butanol**

[464-07-3]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

27

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	818.5 ± 1.0	14-low	298.15	812.2 ± 2.0	56-sar/new <sup>1)</sup>
298.15	810.0 ± 3.0	33-ste <sup>1)</sup>	293.15	816.7 ± 1.0	50-pic/zie
298.15	815.7 ± 2.0	38-gin/web <sup>1)</sup>	293.15	817.9 ± 1.2	Recommended
293.15	818.4 ± 1.0	50-mos/lac			

<sup>1)</sup> Not included in calculation of recommended value.

**(S)-3,3-Dimethyl-2-butanol** [1517-67-5] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 28

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	810.0 ± 2.0	33-ste

**2-Ethyl-1-butanol** [97-95-0] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 29

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 2.6167 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 5.9806 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 288.15 \text{ to } 418.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.36526 \cdot 10^2$
B	$1.79278 \cdot 10^{-2}$
C	$-1.26674 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	832.60 ± 1.00	-0.32	38-whi/kar(✕)	368.15	771.39 ± 0.50	-0.05	40-hov/lan-2(Δ)
293.15	832.80 ± 0.50	-0.12	39-gol/tay(◆)	378.15	762.31 ± 0.50	0.15	40-hov/lan-2(Δ)
278.15	845.04 ± 0.50	1.53	40-hov/lan-2 <sup>1)</sup>	388.15	752.47 ± 0.50	-0.17	40-hov/lan-2(Δ)
288.15	837.33 ± 0.50	0.82	40-hov/lan-2(Δ)	398.15	742.87 ± 0.50	0.01	40-hov/lan-2(Δ)
298.15	829.53 ± 0.50	0.26	40-hov/lan-2(Δ)	408.15	732.74 ± 0.50	-0.08	40-hov/lan-2(Δ)
308.15	822.03 ± 0.50	0.27	40-hov/lan-2(Δ)	418.15	722.29 ± 0.50	-0.24	40-hov/lan-2(Δ)
318.15	814.11 ± 0.50	0.10	40-hov/lan-2(Δ)	293.15	833.10 ± 0.60	0.18	52-coo(✕)
328.15	805.93 ± 0.50	-0.07	40-hov/lan-2(Δ)	293.15	832.90 ± 0.50	-0.02	68-ano(V)
338.15	797.38 ± 0.50	-0.36	40-hov/lan-2(Δ)	298.15	829.11 ± 0.20	-0.16	84-kim/ben(□)
348.15	789.18 ± 0.50	-0.05	40-hov/lan-2(Δ)	298.15	829.07 ± 0.20	-0.20	85-ort/paz-2(O)
358.15	780.51 ± 0.50	0.05	40-hov/lan-2(Δ)				

<sup>1)</sup> Not included in Fig. 1.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

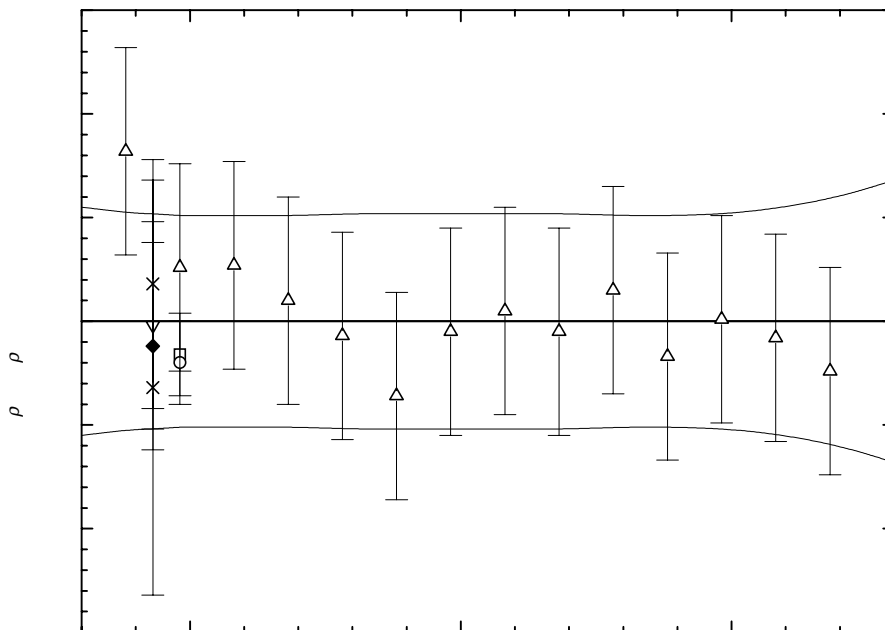
$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
280.00	842.23 ± 0.55	320.00	812.55 ± 0.51	380.00	760.42 ± 0.51
290.00	835.19 ± 0.52	330.00	804.49 ± 0.52	390.00	750.85 ± 0.51
293.15	832.92 ± 0.52	340.00	796.19 ± 0.52	400.00	741.02 ± 0.52
298.15	829.27 ± 0.51	350.00	787.62 ± 0.52	410.00	730.94 ± 0.55
300.00	827.90 ± 0.51	360.00	778.81 ± 0.52	420.00	720.60 ± 0.60
310.00	820.35 ± 0.51	370.00	769.74 ± 0.52	430.00	710.01 ± 0.68

cont.

**2-Ethyl-1-butanol** (cont.)

**Further references:** [48-wei, 50-pic/zie, 53-ano-1, 58-ano-5, 58-cos/bow].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**1-Hexanol**

[111-27-3]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

30

$$T_c = 611.00 \text{ K [89-tej/lee]}$$

$$\rho_c = 268.00 \text{ kg}\cdot\text{m}^{-3} \text{ [89-tej/lee]}$$

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):

$\sigma_T = 7.2858 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (4.6480 \cdot 10^{-1})$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 2.7537 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 235.72 \text{ to } 500.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 500.00 \text{ to } 611.00 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3$ $+ D(T_c - T)^4]$
A	$1.01544 \cdot 10^3$	$8.35316 \cdot 10^{-1}$
B	$-7.78875 \cdot 10^{-1}$	$-1.13272 \cdot 10^{-2}$
C	$8.80075 \cdot 10^{-4}$	$8.40546 \cdot 10^{-5}$
D	$-1.73223 \cdot 10^{-6}$	$-2.64908 \cdot 10^{-7}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

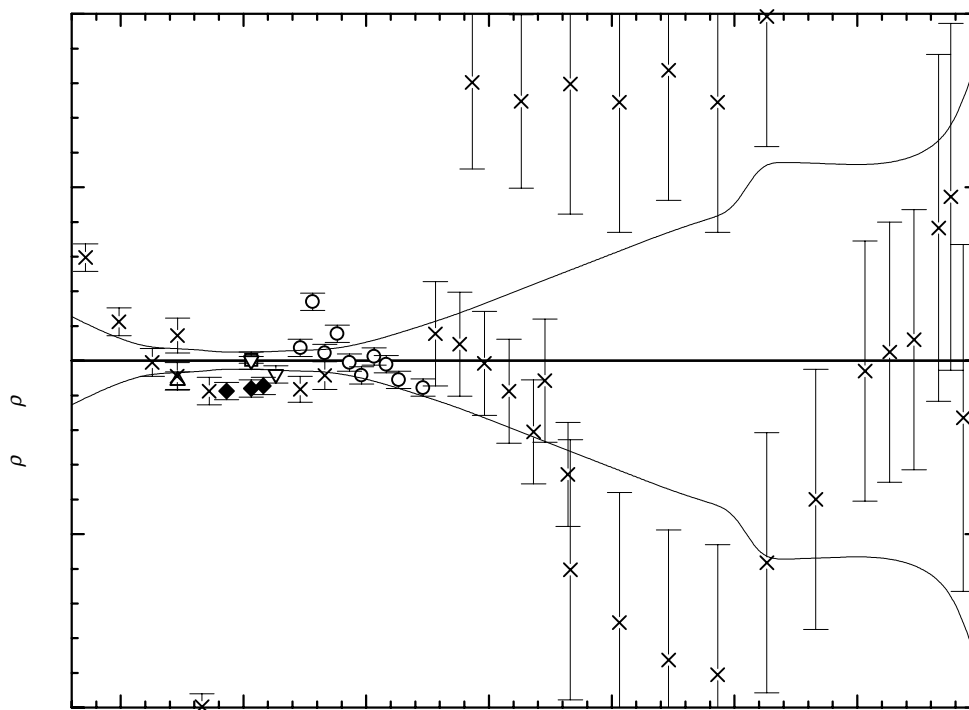
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	833.34 ± 0.20	0.29	32-ell/rei(X)	553.15	545.00 ± 1.50	-0.12	66-efr(X)
298.15	815.79 ± 0.20	0.25	32-ell/rei <sup>1)</sup>	563.15	524.00 ± 1.50	0.10	66-efr(X)
278.15	829.83 ± 0.50	0.23	38-hov/lan <sup>1)</sup>	573.15	500.00 ± 1.50	0.24	66-efr(X)
288.15	822.67 ± 0.50	0.04	38-hov/lan <sup>1)</sup>	583.15	473.00 ± 2.00	1.53	66-efr(X)
298.15	815.54 ± 0.50	0.00	38-hov/lan <sup>1)</sup>	588.15	457.00 ± 2.00	1.89	66-efr(X)
308.15	808.34 ± 0.50	0.03	38-hov/lan <sup>1)</sup>	593.15	436.00 ± 2.00	-0.66	66-efr(X)
318.15	801.03 ± 0.50	0.09	38-hov/lan <sup>1)</sup>	598.15	410.00 ± 3.00	-5.23	66-efr(X)
328.15	793.56 ± 0.50	0.15	38-hov/lan <sup>1)</sup>	603.15	385.00 ± 5.00	-3.80	66-efr(X)
338.15	785.34 ± 0.50	-0.37	38-hov/lan <sup>1)</sup>	605.15	370.00 ± 5.00	-5.74	66-efr(X)
348.15	778.20 ± 0.50	0.35	38-hov/lan <sup>1)</sup>	607.15	347.00 ± 5.00	-12.95	66-efr <sup>1)</sup>
358.15	770.22 ± 0.50	0.43	38-hov/lan <sup>1)</sup>	235.72	859.24 ± 0.16	1.19	73-fin(X)
368.15	762.12 ± 0.50	0.58	38-hov/lan <sup>1)</sup>	249.28	849.58 ± 0.16	0.45	73-fin(X)
378.15	753.39 ± 0.60	0.31	38-hov/lan(X)	262.88	840.02 ± 0.16	-0.02	73-fin(X)
388.15	744.60 ± 0.60	0.19	38-hov/lan(X)	273.00	832.97 ± 0.16	-0.18	73-fin(X)
398.15	735.48 ± 0.60	-0.03	38-hov/lan(X)	286.10	823.72 ± 0.16	-0.35	73-fin(X)
408.15	726.02 ± 0.60	-0.35	38-hov/lan(X)	293.12	818.88 ± 0.16	-0.24	73-fin <sup>1)</sup>
418.15	716.16 ± 0.60	-0.82	38-hov/lan(X)	293.14	818.80 ± 0.16	-0.31	73-fin <sup>1)</sup>
432.15	702.09 ± 0.60	-1.31	38-hov/lan(X)	303.16	811.63 ± 0.16	-0.30	73-fin <sup>1)</sup>
253.15	850.30 ± 1.00	3.74	58-cos/bow <sup>1)</sup>	313.13	804.42 ± 0.16	-0.24	73-fin <sup>1)</sup>
273.15	835.90 ± 1.00	2.85	58-cos/bow <sup>1)</sup>	323.08	797.04 ± 0.16	-0.20	73-fin <sup>1)</sup>
293.15	821.70 ± 1.00	2.60	58-cos/bow <sup>1)</sup>	333.14	789.42 ± 0.16	-0.17	73-fin(X)
313.15	807.00 ± 1.00	2.36	58-cos/bow <sup>1)</sup>	303.15	811.95 ± 0.04	0.01	74-rao/nai-1(□)
333.15	792.40 ± 1.00	2.82	58-cos/bow <sup>1)</sup>	293.15	818.75 ± 0.10	-0.35	78-jel/leo(◆)
353.15	776.60 ± 1.00	2.76	58-cos/bow <sup>1)</sup>	298.15	815.34 ± 0.10	-0.20	78-jel/leo <sup>1)</sup>
373.15	759.90 ± 1.00	2.56	58-cos/bow <sup>1)</sup>	303.15	811.62 ± 0.10	-0.32	78-jel/leo(◆)
393.15	743.20 ± 1.00	3.21	58-cos/bow(X)	308.15	808.02 ± 0.10	-0.29	78-jel/leo(◆)
413.15	724.70 ± 1.00	2.99	58-cos/bow(X)	303.15	811.94 ± 0.10	-0.00	78-red/nai-1(V)
433.15	705.60 ± 1.50	3.19	58-cos/bow(X)	313.15	804.48 ± 0.10	-0.16	78-red/nai-1(V)
453.15	685.00 ± 1.50	2.98	58-cos/bow(X)	290.10	820.00 ± 0.82	-1.26	79-gyl/apa <sup>1)</sup>
473.15	663.80 ± 1.50	3.35	58-cos/bow(X)	305.90	807.50 ± 0.81	-2.45	79-gyl/apa <sup>1)</sup>
493.15	640.60 ± 1.50	2.98	58-cos/bow(X)	350.80	743.40 ± 0.74	-32.33	79-gyl/apa <sup>1)</sup>
513.15	616.30 ± 1.50	3.97	58-cos/bow(X)	380.90	744.00 ± 0.74	-6.72	79-gyl/apa <sup>1)</sup>
273.15	832.82 ± 0.10	-0.23	59-mck/ski(Δ)	422.80	712.30 ± 0.71	-0.23	79-gyl/apa(X)
273.15	834.00 ± 1.50	0.95	66-efr <sup>1)</sup>	283.15	822.14 ± 0.15	-3.99	86-hei/sch(X)
293.15	819.00 ± 1.50	-0.10	66-efr <sup>1)</sup>	298.15	815.12 ± 0.15	-0.42	86-hei/sch <sup>1)</sup>
313.15	804.00 ± 1.50	-0.64	66-efr <sup>1)</sup>	308.15	807.93 ± 0.15	-0.38	86-hei/sch <sup>1)</sup>
333.15	788.00 ± 1.50	-1.58	66-efr <sup>1)</sup>	323.15	796.86 ± 0.15	-0.33	86-hei/sch(X)
353.15	773.00 ± 1.50	-0.84	66-efr <sup>1)</sup>	323.15	797.34 ± 0.10	0.15	93-gar/ban-1(O)
373.15	757.00 ± 1.50	-0.34	66-efr <sup>1)</sup>	328.15	794.09 ± 0.10	0.68	93-gar/ban-1(O)
393.15	739.00 ± 1.50	-0.99	66-efr <sup>1)</sup>	333.15	789.67 ± 0.10	0.09	93-gar/ban-1(O)
413.15	720.00 ± 1.50	-1.71	66-efr <sup>1)</sup>	338.15	786.02 ± 0.10	0.31	93-gar/ban-1(O)
433.15	700.00 ± 1.50	-2.41	66-efr(X)	343.15	781.78 ± 0.10	-0.02	93-gar/ban-1(O)
453.15	679.00 ± 1.50	-3.02	66-efr(X)	348.15	777.68 ± 0.10	-0.17	93-gar/ban-1(O)
473.15	657.00 ± 1.50	-3.45	66-efr(X)	353.15	773.89 ± 0.10	0.05	93-gar/ban-1(O)
493.15	634.00 ± 1.50	-3.62	66-efr(X)	358.15	769.75 ± 0.10	-0.04	93-gar/ban-1(O)
513.15	610.00 ± 1.50	-2.33	66-efr(X)	363.15	765.47 ± 0.10	-0.22	93-gar/ban-1(O)
533.15	580.00 ± 1.50	-1.60	66-efr(X)	373.15	757.03 ± 0.10	-0.31	93-gar/ban-1(O)

<sup>1)</sup> Not included in Fig. 1.

cont.

## 1-Hexanol (cont.)

**Further references:** [1877-lie/jan, 1883-fre, 1884-zan, 1886-gar, 18-bro/hum, 19-beh, 27-nor/cor, 27-ver/coo, 29-kel-3, 29-mah/das, 30-wal/ros, 33-but/tho, 35-bil/gis, 35-but/ram, 39-gol/tay, 41-hus/age, 45-add, 48-jon/bow, 48-lad/smi, 48-vog-2, 48-wei, 50-gor, 50-mum/phi, 50-pic/zie, 50-sac/sau, 52-coo, 52-eri-1, 53-ano-1, 53-par/cha, 54-naz/kak-2, 56-shu/bel, 57-col/fal, 58-ano-5, 58-lin/tua, 62-bro/smi, 63-nik, 68-ano, 68-pfl/pop, 68-rao/chi, 69-kat/pat, 70-mye/cle, 70-puz/bul, 74-moo/wel, 74-rao/nai, 75-hsu/cle, 75-mat/fer, 76-kow/kas, 76-red/nai, 78-ast, 78-dap/don, 78-paz/gar, 78-tre/ben, 79-dia/tar, 79-kiy/ben, 80-tre/ben, 81-han/hal, 81-kim/ben, 81-kor/kov, 81-nai/nai, 81-sjo/dyh, 82-nai/nai, 82-ort, 82-sin/sin, 82-ven/dha, 83-fuk/ogi, 83-kim/ben, 84-bra/pin, 84-ort/ang, 84-sak/nak, 85-fer/pin, 85-ort, 85-ort/paz-1, 85-sar/paz, 85-sin/sin, 85-sin/sin-1, 86-ash/sri, 86-dew/meh, 86-sin/sin, 86-tan/toy, 86-wag/hei, 87-dew/meh, 88-ort/gar, 89-ala/sal, 89-dew/gup, 89-mat/mak-1, 89-sin/sin, 89-vij/nai, 90-vij/nai, 91-fen/wan, 91-ram/muk, 92-lie/sen-1, 93-ami/ara, 93-ami/rai, 93-yan/mae, 94-kim/lee, 94-kum/nai, 94-kum/nai-1, 94-ven/ven, 94-yu /tsa, 94-yu /tsa-1, 95-fra/jim, 95-fra/men, 96-elb, 98-ami/ban, 98-ami/pat-1].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)]^{1/3} + 0.75(1 - T/T_c)[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
230.00	861.78 ± 0.51	350.00	776.37 ± 0.21	490.00	641.30 ± 1.64
240.00	855.25 ± 0.37	360.00	768.28 ± 0.29	500.00	629.49 ± 1.73
250.00	848.66 ± 0.25	370.00	759.99 ± 0.38	510.00	616.68 ± 2.28
260.00	841.98 ± 0.16	380.00	751.50 ± 0.47	520.00	602.39 ± 2.29
270.00	835.20 ± 0.14	390.00	742.78 ± 0.57	530.00	586.79 ± 2.28
280.00	828.32 ± 0.13	400.00	733.84 ± 0.68	540.00	569.84 ± 2.27
290.00	821.33 ± 0.10	410.00	724.65 ± 0.79	550.00	551.33 ± 2.26
293.15	819.10 ± 0.10	420.00	715.22 ± 0.90	560.00	530.85 ± 2.27
298.15	815.54 ± 0.10	430.00	705.52 ± 1.01	570.00	507.74 ± 2.32
300.00	814.21 ± 0.10	440.00	695.56 ± 1.12	580.00	480.94 ± 2.44
310.00	806.96 ± 0.10	450.00	685.31 ± 1.23	590.00	448.56 ± 2.72
320.00	799.56 ± 0.12	460.00	674.77 ± 1.34	600.00	406.21 ± 3.58
330.00	792.00 ± 0.12	470.00	663.93 ± 1.45	610.00	324.59 ± 9.90
340.00	784.27 ± 0.15	480.00	652.78 ± 1.55		

**2-Hexanol****[626-93-7]****C<sub>6</sub>H<sub>14</sub>O****MW = 102.18****31****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 4.6999 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 8.6236 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 413.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.26903 \cdot 10^2$
B	$-3.13386 \cdot 10^{-3}$
C	$-1.30510 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	828.70 ± 0.60	0.03	08-zel/prz(✕)	298.15	810.34 ± 0.50	0.39	38-hov/lan(✕)
293.15	814.10 ± 0.60	0.27	08-zel/prz(✕)	308.15	802.21 ± 0.50	0.20	38-hov/lan(✕)
293.15	815.00 ± 0.60	1.17	11-pic/ken(✕)	318.15	794.01 ± 0.50	0.20	38-hov/lan(✕)
371.65	744.40 ± 1.00	-1.07	12-pic/ken(✕)	328.15	785.49 ± 0.50	0.15	38-hov/lan(✕)
393.15	726.30 ± 1.00	2.35	12-pic/ken <sup>1)</sup>	338.15	776.74 ± 0.50	0.13	38-hov/lan(✕)
273.15	828.30 ± 0.50	-0.37	26-van(✕)	348.15	767.76 ± 0.50	0.14	38-hov/lan(✕)
288.15	817.10 ± 0.50	-0.54	26-van(✕)	358.15	758.01 ± 0.50	-0.36	38-hov/lan(✕)
298.15	809.75 ± 0.20	-0.20	32-ell/rei(○)	368.15	749.26 ± 0.50	0.40	38-hov/lan(✕)
298.15	810.80 ± 0.50	0.85	38-gin/web(◆)	378.15	738.95 ± 0.60	-0.14	38-hov/lan(✕)
278.15	825.80 ± 0.50	0.74	38-hov/lan(✕)	388.15	728.80 ± 0.60	-0.26	38-hov/lan(✕)
288.15	818.12 ± 0.50	0.48	38-hov/lan(✕)	398.15	718.43 ± 0.60	-0.34	38-hov/lan(✕)

<sup>1)</sup> Not included in Fig. 1

cont.

## 2-Hexanol (cont.)

Table 2. (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
408.15	707.72 ± 0.60	-0.49	38-hov/lan(×)	300.15	808.05 ± 0.50	-0.34	85-ort(×)
413.15	702.22 ± 0.60	-0.62	38-hov/lan(×)	302.15	806.46 ± 0.50	-0.35	85-ort(×)
293.15	815.00 ± 0.60	1.17	42-air/bal(×)	304.15	804.85 ± 0.50	-0.37	85-ort(×)
293.15	814.20 ± 0.60	0.37	50-pic/zie(×)	306.15	803.27 ± 0.50	-0.35	85-ort(×)
293.15	814.30 ± 0.50	0.47	52-coo(∇)	308.15	801.89 ± 0.50	-0.12	85-ort(×)
293.15	813.56 ± 0.50	-0.27	85-ort(×)	298.15	809.69 ± 0.10	-0.26	86-ort/paz(□)
298.15	809.61 ± 0.50	-0.34	85-ort(×)	298.15	809.61 ± 0.50	-0.34	94-tar/jun(Δ)

Further references: [23-clo/joh, 27-nor/cor, 35-les/lom, 39-bar/atk].

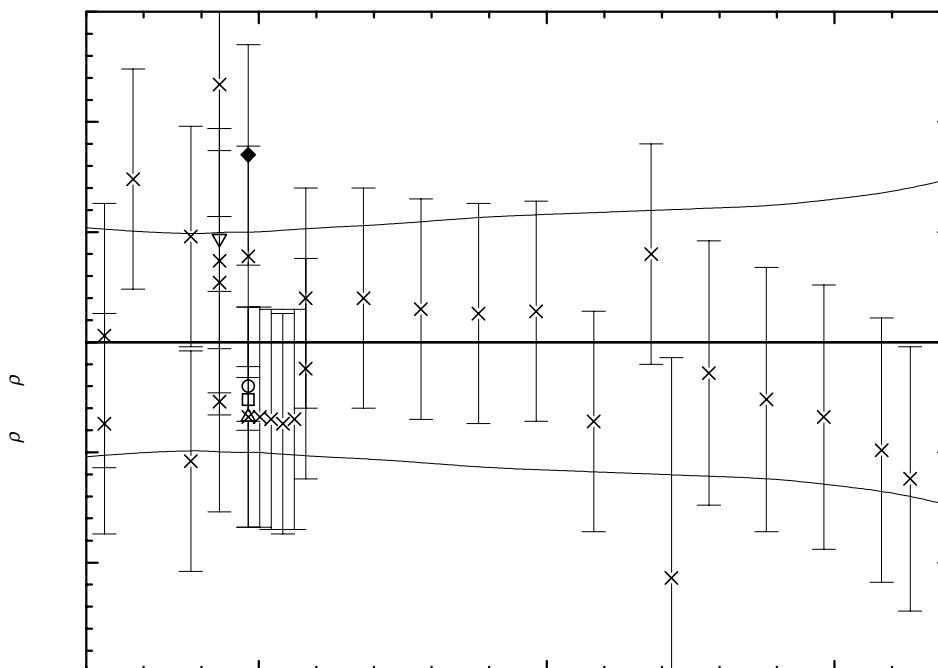


Fig. 1. The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)]^{1/3} + 0.75(1 - T/T_c)[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	830.92 ± 0.52	310.00	800.51 ± 0.52	370.00	747.08 ± 0.60
280.00	823.71 ± 0.50	320.00	792.26 ± 0.53	380.00	737.26 ± 0.61
290.00	816.24 ± 0.49	330.00	783.74 ± 0.55	390.00	727.18 ± 0.62
293.15	813.83 ± 0.50	340.00	774.97 ± 0.57	400.00	716.83 ± 0.65
298.15	809.95 ± 0.50	350.00	765.93 ± 0.58	410.00	706.23 ± 0.68
300.00	808.50 ± 0.50	360.00	756.63 ± 0.59	420.00	695.37 ± 0.74

**(RS)-2-Hexanol** [20281-86-1] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 32

**Table 1.** Experimental value with uncertainty.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	810.0 ± 0.2	88-tan/luo

**3-Hexanol** [623-37-0] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 33

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.6198 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 7.2518 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $409.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.66285 \cdot 10^2$
B	$-1.77415 \cdot 10^{-1}$
C	$-1.11253 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	833.50 ± 1.00	-1.32	1875-lie <sup>1)</sup>	338.15	779.06 ± 0.50	-0.02	38-hov/lan(O)
293.15	818.80 ± 1.00	0.13	1875-lie(X)	348.15	769.72 ± 0.50	0.05	38-hov/lan(O)
273.15	833.50 ± 1.00	-1.32	1875-lie/vol <sup>1)</sup>	358.15	759.69 ± 0.50	-0.35	38-hov/lan(O)
293.15	818.80 ± 1.00	0.13	1875-lie/vol(X)	368.15	750.40 ± 0.50	0.22	38-hov/lan(O)
273.15	834.31 ± 1.00	-0.51	1876-dec(V)	378.15	740.13 ± 0.50	0.02	38-hov/lan(O)
293.15	818.23 ± 1.00	-0.44	1876-dec(V)	388.15	730.34 ± 0.50	0.53	38-hov/lan(O)
298.15	814.30 ± 0.50	-0.19	38-gin/web(Δ)	398.15	719.18 ± 0.50	-0.11	38-hov/lan(O)
278.15	830.96 ± 0.50	0.10	38-hov/lan(O)	409.15	707.06 ± 0.50	-0.39	38-hov/lan(O)
288.15	822.73 ± 0.50	-0.06	38-hov/lan(O)	293.15	819.30 ± 1.00	0.63	42-air/bal(◆)
298.15	814.26 ± 0.50	-0.23	38-hov/lan(O)	293.15	819.50 ± 1.00	0.83	44-hen/mat(X)
308.15	805.80 ± 0.50	-0.17	38-hov/lan(O)	293.15	818.60 ± 0.50	-0.07	50-pic/zie(□)
318.15	796.97 ± 0.50	-0.26	38-hov/lan(O)	293.15	819.00 ± 1.00	0.33	52-coo(X)
328.15	788.10 ± 0.50	-0.17	38-hov/lan(O)				

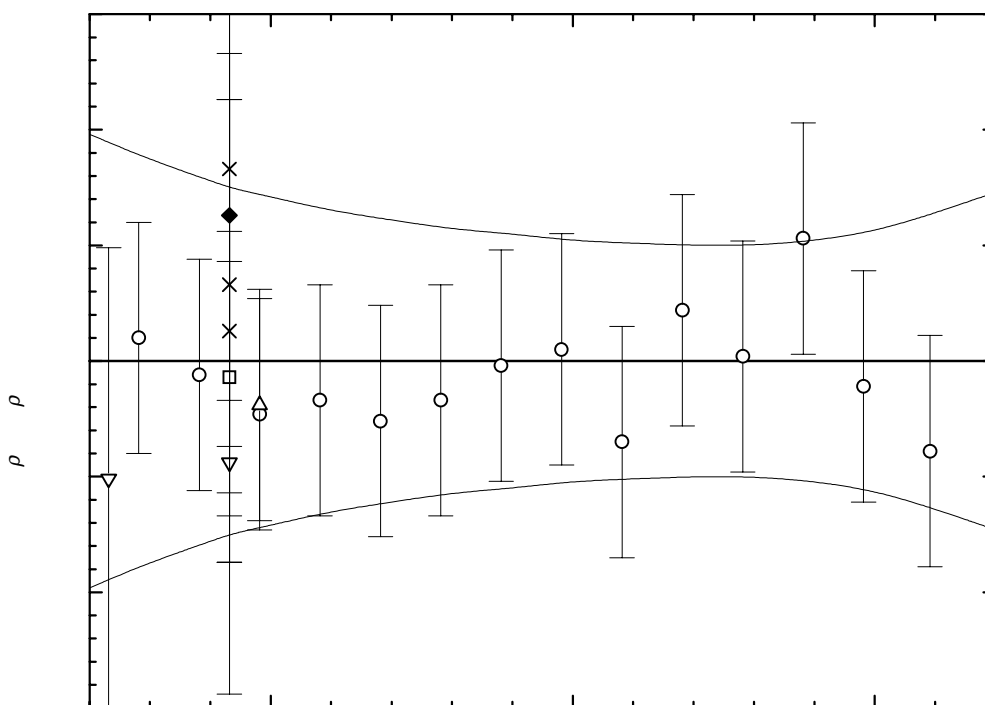
<sup>1)</sup> Not included in Fig. 1.

cont.



**3-Hexanol** (cont.)

**Further references:** [13-pic/ken, 34-les/lom, 35-les/lom, 39-spi/tin-1, 54-naz/kak-3, 56-shu/bel].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	837.28 ± 0.98	310.00	804.37 ± 0.65	370.00	748.34 ± 0.50
280.00	829.39 ± 0.87	320.00	795.59 ± 0.61	380.00	738.22 ± 0.50
290.00	821.27 ± 0.78	330.00	786.58 ± 0.57	390.00	727.88 ± 0.52
293.15	818.67 ± 0.75	340.00	777.36 ± 0.55	400.00	717.31 ± 0.56
298.15	814.49 ± 0.72	350.00	767.91 ± 0.52	410.00	706.53 ± 0.64
300.00	812.93 ± 0.71	360.00	758.23 ± 0.51	420.00	695.52 ± 0.73

**2-Methyl-1-pentanol** [105-30-6] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 34**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 3.6425 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 7.9675 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $408.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.25662 \cdot 10^2$
B	$1.79466 \cdot 10^{-2}$
C	$-1.24362 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	$839.50 \pm 1.50$	1.72	1883-lie/zei <sup>1)</sup>	338.15	$789.50 \pm 0.50$	-0.03	38-hov/lan( $\Delta$ )
273.15	$837.40 \pm 1.50$	-0.38	1883-lie/zei( $\nabla$ )	348.15	$781.19 \pm 0.50$	0.02	38-hov/lan( $\Delta$ )
290.75	$824.60 \pm 1.50$	-1.15	1883-lie/zei( $\nabla$ )	358.15	$772.69 \pm 0.50$	0.12	38-hov/lan( $\Delta$ )
296.85	$821.40 \pm 1.50$	-0.00	1883-lie/zei( $\nabla$ )	368.15	$764.13 \pm 0.50$	0.41	38-hov/lan( $\Delta$ )
278.15	$834.70 \pm 0.50$	0.26	38-hov/lan( $\Delta$ )	378.15	$754.77 \pm 0.50$	0.16	38-hov/lan( $\Delta$ )
288.15	$827.99 \pm 0.50$	0.42	38-hov/lan( $\Delta$ )	388.15	$745.34 \pm 0.50$	0.08	38-hov/lan( $\Delta$ )
298.15	$820.63 \pm 0.50$	0.17	38-hov/lan( $\Delta$ )	398.15	$735.69 \pm 0.50$	0.03	38-hov/lan( $\Delta$ )
308.15	$813.07 \pm 0.50$	-0.03	38-hov/lan( $\Delta$ )	408.15	$725.74 \pm 0.50$	-0.08	38-hov/lan( $\Delta$ )
318.15	$805.48 \pm 0.50$	-0.01	38-hov/lan( $\Delta$ )	293.15	$824.30 \pm 0.50$	0.25	50-pic/zie( $\circ$ )
328.15	$797.55 \pm 0.50$	-0.08	38-hov/lan( $\Delta$ )	293.15	$824.00 \pm 0.50$	-0.05	68-ano( $\square$ )

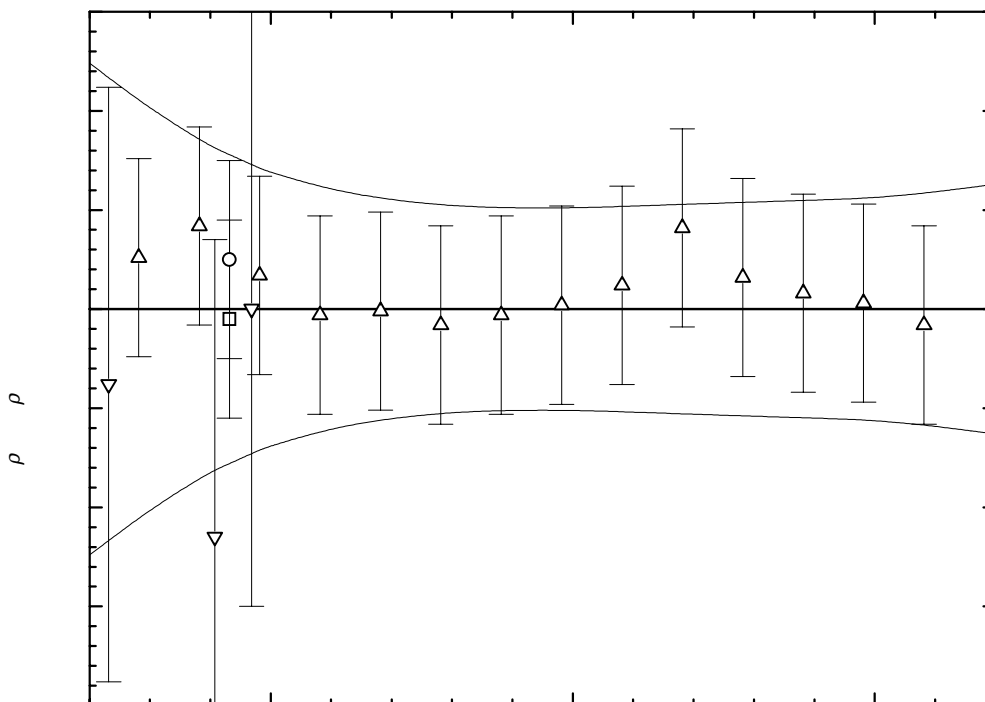
<sup>1)</sup> Not included in Fig. 1.**Further references:** [24-ter, 27-nor/cor, 36-oli, 51-hau, 52-coo, 53-ano-1, 56-ano-1, 84-bra/pin, 85-ort, 94-tar/jun].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	$839.85 \pm 1.24$	310.00	$811.71 \pm 0.60$	370.00	$762.05 \pm 0.53$
280.00	$833.19 \pm 1.01$	320.00	$804.06 \pm 0.55$	380.00	$752.90 \pm 0.54$
290.00	$826.28 \pm 0.82$	330.00	$796.15 \pm 0.52$	390.00	$743.51 \pm 0.55$
293.15	$824.05 \pm 0.78$	340.00	$788.00 \pm 0.51$	400.00	$733.86 \pm 0.56$
298.15	$820.46 \pm 0.71$	350.00	$779.60 \pm 0.51$	410.00	$723.97 \pm 0.59$
300.00	$819.12 \pm 0.69$	360.00	$770.95 \pm 0.52$	420.00	$713.82 \pm 0.63$

cont.

## 2-Methyl-1-pentanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

## 2-Methyl-2-pentanol

[590-36-3]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

35

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 2.6940 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.0135 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

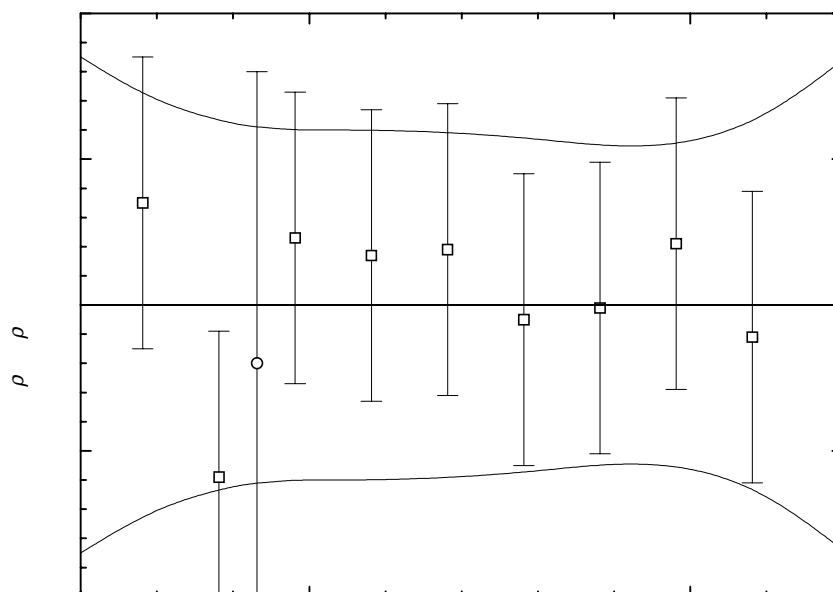
Coefficient	$T = 278.15 \text{ to } 358.15 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.36813 \cdot 10^2$
B	$-1.65836 \cdot 10^{-2}$
C	$-1.37719 \cdot 10^{-3}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
278.15	826.00 ± 0.50	0.35	33-hov/lan(□)	328.15	783.02 ± 0.50	-0.05	33-hov/lan(□)
288.15	817.10 ± 0.50	-0.59	33-hov/lan(□)	338.15	773.72 ± 0.50	-0.01	33-hov/lan(□)
298.15	809.68 ± 0.50	0.23	33-hov/lan(□)	348.15	764.32 ± 0.50	0.21	33-hov/lan(□)
308.15	801.10 ± 0.50	0.17	33-hov/lan(□)	358.15	754.11 ± 0.50	-0.11	33-hov/lan(□)
318.15	792.33 ± 0.50	0.19	33-hov/lan(□)	293.15	813.40 ± 1.00	-0.20	50-pic/zie(○)

**Further references:** [36-nor/has, 38-gin/web, 38-whi/joh, 39-owe/qua, 52-lev/tan, 85-ort, 94-tar/jun].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	831.94 ± 0.85	300.00	807.89 ± 0.60	350.00	762.30 ± 0.55
280.00	824.20 ± 0.69	310.00	799.32 ± 0.60	360.00	752.36 ± 0.64
290.00	816.18 ± 0.62	320.00	790.48 ± 0.59	370.00	742.14 ± 0.84
293.15	813.60 ± 0.61	330.00	781.36 ± 0.57		
298.15	809.45 ± 0.60	340.00	771.97 ± 0.54		

## 2-Methyl-3-pentanol

[565-67-3]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

36

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 6.8420 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.7852 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 278.15$ to $398.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.13614 \cdot 10^2$
B	$2.23285 \cdot 10^{-1}$
C	$-1.80054 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	$824.70 \pm 1.00$	0.36	12-pic/ken(✕)	338.15	$783.78 \pm 0.60$	0.55	40-hov/lan-1(○)
288.95	$826.90 \pm 1.00$	-0.90	28-kro/see(✕)	348.15	$773.60 \pm 0.60$	0.49	40-hov/lan-1(○)
298.15	$819.30 \pm 1.00$	-0.83	36-nor/has(Δ)	358.15	$762.93 \pm 0.60$	0.30	40-hov/lan-1(○)
298.15	$818.60 \pm 1.00$	-1.53	38-gin/web(✕)	368.15	$751.71 \pm 0.60$	-0.07	40-hov/lan-1(○)
293.15	$824.00 \pm 1.00$	-0.34	38-whi/joh(∇)	378.15	$739.85 \pm 0.60$	-0.73	40-hov/lan-1(○)
278.15	$837.11 \pm 0.60$	0.69	40-hov/lan-1(○)	388.15	$727.85 \pm 0.60$	-1.16	40-hov/lan-1(○)
288.15	$829.09 \pm 0.60$	0.64	40-hov/lan-1(○)	398.15	$718.58 \pm 0.60$	1.49	40-hov/lan-1(○)
298.15	$820.62 \pm 0.60$	0.49	40-hov/lan-1(○)	293.15	$823.00 \pm 1.00$	-1.34	44-hen/mat(✕)
308.15	$811.80 \pm 0.60$	0.35	40-hov/lan-1(○)	293.15	$824.90 \pm 1.00$	0.56	50-pic/zie(◆)
318.15	$802.98 \pm 0.60$	0.58	40-hov/lan-1(○)	298.15	$820.08 \pm 0.40$	-0.05	85-ort/paz-2(□)
328.15	$793.44 \pm 0.60$	0.44	40-hov/lan-1(○)				

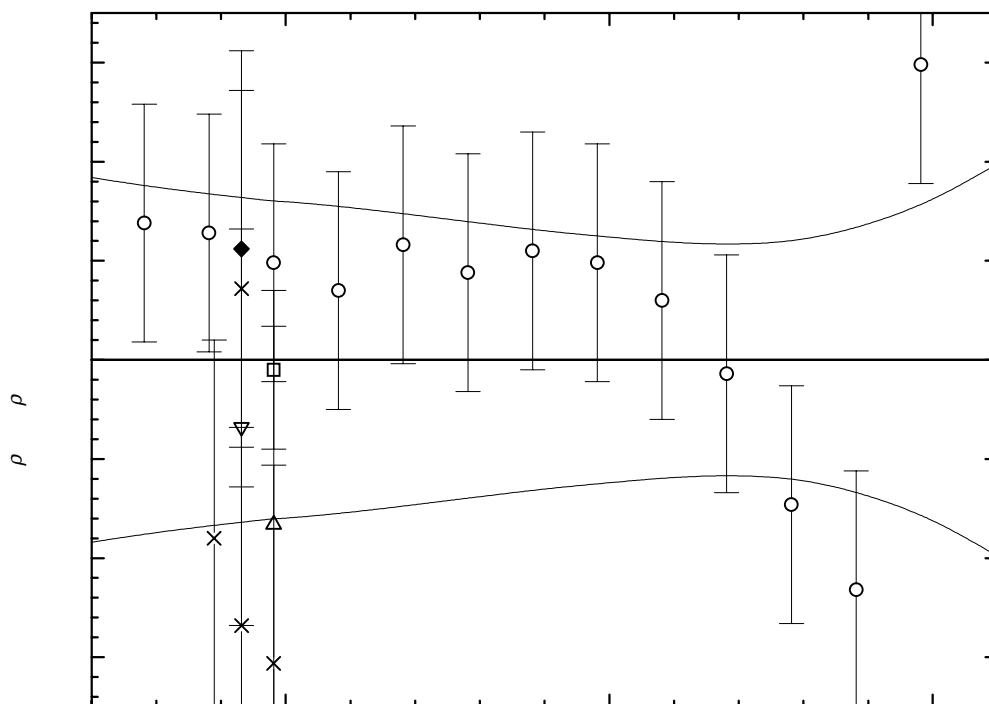
Further references: [19-beh].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	$842.64 \pm 0.92$	310.00	$809.80 \pm 0.77$	370.00	$749.74 \pm 0.58$
280.00	$834.97 \pm 0.87$	320.00	$800.69 \pm 0.73$	380.00	$738.46 \pm 0.60$
290.00	$826.94 \pm 0.83$	330.00	$791.22 \pm 0.69$	390.00	$726.83 \pm 0.68$
293.15	$824.34 \pm 0.82$	340.00	$781.39 \pm 0.65$	400.00	$714.84 \pm 0.80$
298.15	$820.13 \pm 0.80$	350.00	$771.20 \pm 0.62$	410.00	$702.49 \pm 0.99$
300.00	$818.55 \pm 0.80$	360.00	$760.65 \pm 0.59$		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

### 3-Methyl-1-pentanol

[589-35-5]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

37

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 8.2830 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 2.1862 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 278.15$ to $423.15$ K
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.12528 \cdot 10^2$
B	$7.80681 \cdot 10^{-2}$
C	$-1.29987 \cdot 10^{-3}$

cont.

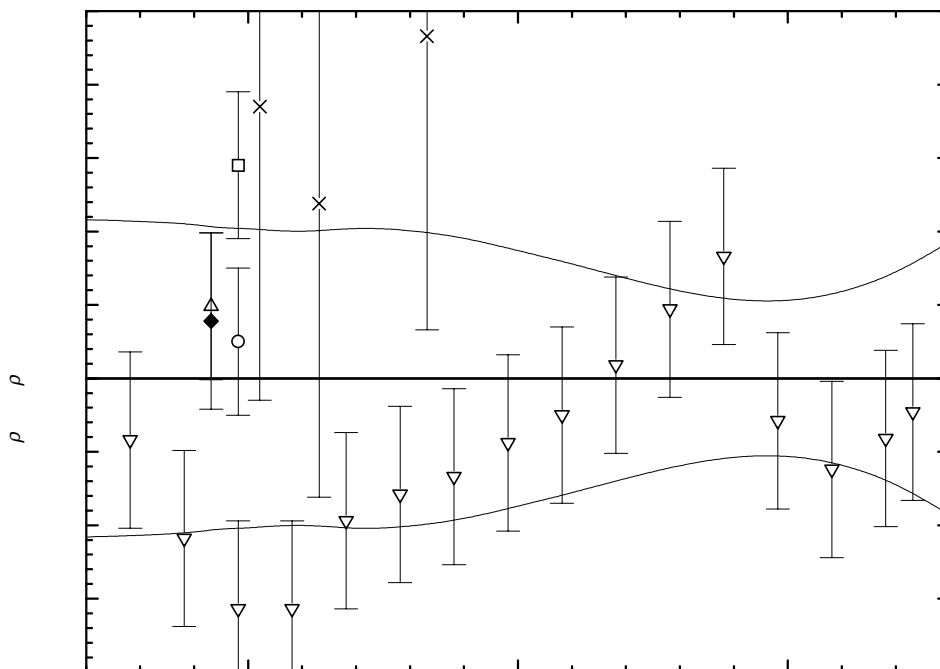
## 3-Methyl-1-pentanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.65	826.20 ± 2.00	2.84	08-har <sup>1)</sup>	338.15	789.62 ± 0.60	-0.67	40-hov/lan(∇)
302.15	819.30 ± 2.00	1.85	08-har(×)	348.15	781.71 ± 0.60	-0.44	40-hov/lan(∇)
313.15	810.70 ± 2.00	1.19	08-har(×)	358.15	773.50 ± 0.60	-0.25	40-hov/lan(∇)
333.15	796.60 ± 2.00	2.33	08-har(×)	368.15	765.18 ± 0.60	0.09	40-hov/lan(∇)
353.15	781.20 ± 2.00	3.22	08-har <sup>1)</sup>	378.15	756.64 ± 0.60	0.47	40-hov/lan(∇)
298.15	820.50 ± 0.50	0.25	27-nor/cor(O)	388.15	747.82 ± 0.60	0.83	40-hov/lan(∇)
293.15	824.20 ± 0.50	0.49	36-oli(Δ)	398.15	737.26 ± 0.60	-0.29	40-hov/lan(∇)
278.15	833.26 ± 0.60	-0.42	40-hov/lan(∇)	408.15	727.23 ± 0.60	-0.62	40-hov/lan(∇)
288.15	826.00 ± 0.60	-1.09	40-hov/lan(∇)	418.15	717.48 ± 0.60	-0.41	40-hov/lan(∇)
298.15	818.68 ± 0.60	-1.57	40-hov/lan(∇)	423.15	712.58 ± 0.60	-0.23	40-hov/lan(∇)
308.15	811.58 ± 0.60	-1.57	40-hov/lan(∇)	293.15	824.10 ± 0.60	0.39	52-coo(◆)
318.15	804.82 ± 0.60	-0.97	40-hov/lan(∇)	298.15	821.70 ± 0.50	1.45	59-pin/lar(□)
328.15	797.38 ± 0.60	-0.79	40-hov/lan(∇)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [12-ipa, 41-boh, 41-hus/age, 43-boh, 50-pic/zie].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)  
cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	838.85 ± 1.08	320.00	804.40 ± 1.03	390.00	745.26 ± 0.53
280.00	832.48 ± 1.07	330.00	796.73 ± 1.01	400.00	735.78 ± 0.52
290.00	825.85 ± 1.05	340.00	788.81 ± 0.96	410.00	726.03 ± 0.58
293.15	823.71 ± 1.03	350.00	780.62 ± 0.87	420.00	716.02 ± 0.71
298.15	820.25 ± 1.02	360.00	772.17 ± 0.78	430.00	705.75 ± 0.93
300.00	818.96 ± 1.02	370.00	763.46 ± 0.68		
310.00	811.81 ± 0.99	380.00	754.49 ± 0.59		

**(R)-3-Methyl-1-pentanol** [70224-28-1] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 38

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.020$ .

Coefficient	$\rho = A + BT$
$A$	1060.34
$B$	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
292.95	826.0 ± 0.5	0.02	59-pin/lar
298.15	821.8 ± 0.5	-0.02	59-pin/lar

**Table 3.** Recommended values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	828.3 ± 0.5
293.15	825.8 ± 0.5
298.15	821.8 ± 0.5

**3-Methyl-2-pentanol** [565-60-6] C<sub>6</sub>H<sub>14</sub>O MW = 102.18 39

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.8542 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.6563 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 278.15$ to $398.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
$A$	$9.72247 \cdot 10^2$
$B$	$-1.48421 \cdot 10^{-1}$
$C$	$-1.16182 \cdot 10^{-3}$

cont.

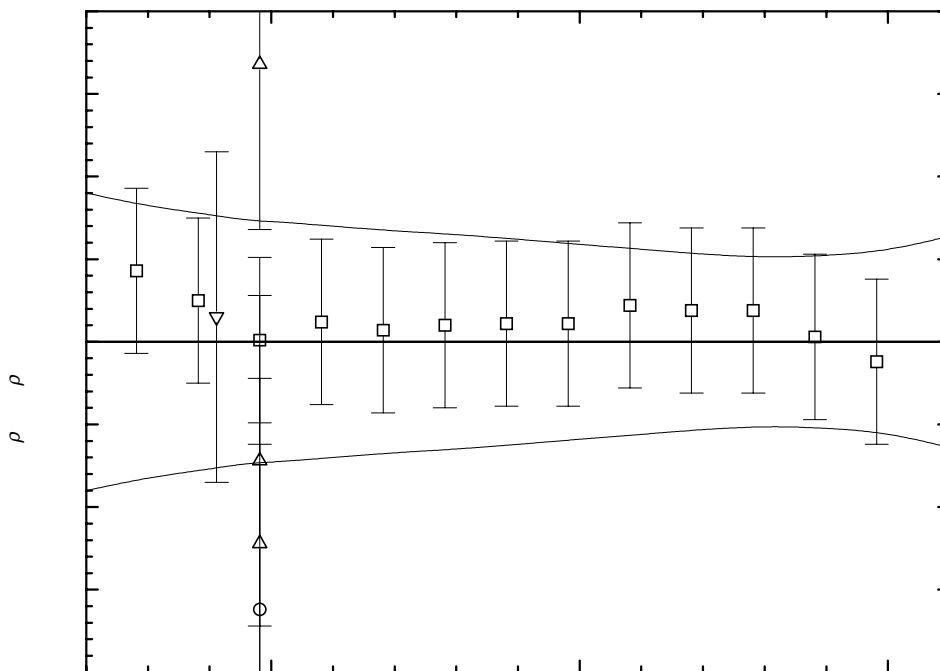


## 3-Methyl-2-pentanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
291.15	830.70 ± 1.00	0.15	1883-wis(∇)	318.15	807.50 ± 0.50	0.07	41-hov/lan(□)
298.15	824.00 ± 1.00	-0.72	36-nor/has(Δ)	328.15	798.53 ± 0.50	0.10	41-hov/lan(□)
298.15	826.40 ± 1.00	1.68	36-nor/has(Δ)	338.15	789.32 ± 0.50	0.11	41-hov/lan(□)
298.15	823.50 ± 1.00	-1.22	36-nor/has(Δ)	348.15	779.86 ± 0.50	0.11	41-hov/lan(□)
298.15	823.10 ± 1.00	-1.62	38-gin/web(○)	358.15	770.28 ± 0.50	0.22	41-hov/lan(□)
278.15	841.51 ± 0.50	0.43	41-hov/lan(□)	368.15	760.33 ± 0.50	0.19	41-hov/lan(□)
288.15	833.26 ± 0.50	0.25	41-hov/lan(□)	378.15	750.17 ± 0.50	0.19	41-hov/lan(□)
298.15	824.73 ± 0.50	0.01	41-hov/lan(□)	388.15	739.63 ± 0.50	0.03	41-hov/lan(□)
308.15	816.31 ± 0.50	0.12	41-hov/lan(□)	398.15	728.86 ± 0.50	-0.12	41-hov/lan(□)

**Further references:** [01-zel/zel, 50-pic/zie, 84-bra/pin, 85-ort, 94-tar/jun].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	847.48 ± 0.90	310.00	814.59 ± 0.70	370.00	758.28 ± 0.53
280.00	839.60 ± 0.82	320.00	805.78 ± 0.67	380.00	748.08 ± 0.51
290.00	831.50 ± 0.77	330.00	796.75 ± 0.65	390.00	737.65 ± 0.52
293.15	828.89 ± 0.75	340.00	787.48 ± 0.62	400.00	726.99 ± 0.55
298.15	824.72 ± 0.73	350.00	777.98 ± 0.59	410.00	716.09 ± 0.64
300.00	823.16 ± 0.73	360.00	768.24 ± 0.56		

**3-Methyl-3-pentanol**

[77-74-7]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

40

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 5.7626 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.1588 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.06284 \cdot 10^2$
B	$3.36695 \cdot 10^{-1}$
C	$-2.05718 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

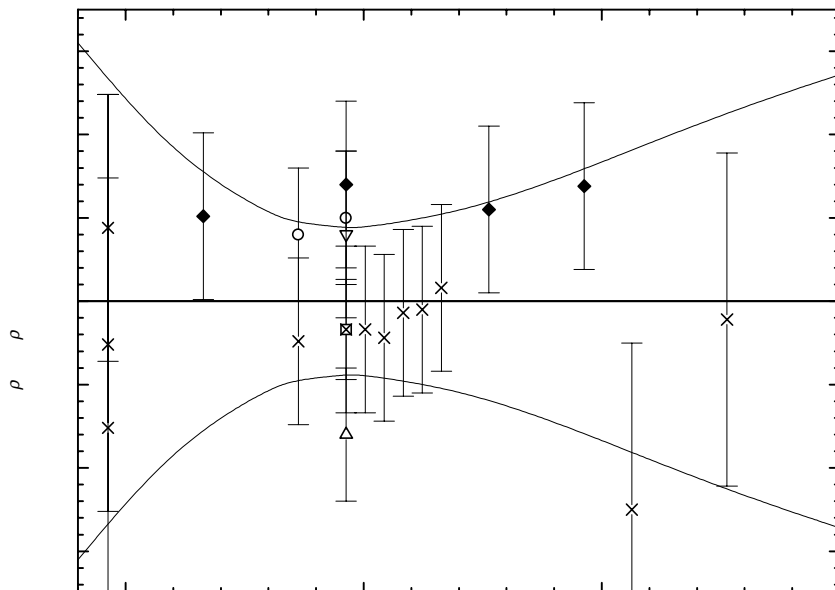
$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	845.20 ± 0.80	0.44	21-par/sim(×)	298.15	823.00 ± 0.40	-0.80	84-bra/pin(Δ)
298.15	824.20 ± 0.50	0.40	38-gin/web(∇)	293.15	827.96 ± 0.50	-0.24	85-ort(×)
273.15	844.50 ± 1.00	-0.26	39-owe/qua(×)	298.15	823.63 ± 0.50	-0.17	85-ort(×)
298.15	821.50 ± 1.00	-2.30	39-owe/qua <sup>1)</sup>	300.15	821.84 ± 0.50	-0.17	85-ort(×)
308.15	812.20 ± 1.00	-2.49	39-owe/qua <sup>1)</sup>	302.15	819.99 ± 0.50	-0.22	85-ort(×)
318.15	803.10 ± 1.00	-2.08	39-owe/qua <sup>1)</sup>	304.15	818.32 ± 0.50	-0.07	85-ort(×)
328.15	794.00 ± 1.00	-1.25	39-owe/qua(×)	306.15	816.50 ± 0.50	-0.05	85-ort(×)
338.15	784.80 ± 1.00	-0.11	39-owe/qua(×)	308.15	814.77 ± 0.50	0.08	85-ort(×)
293.15	828.60 ± 0.40	0.40	47-how/mea(○)	283.15	837.20 ± 0.50	0.51	88-cac/cos(◆)
298.15	824.30 ± 0.40	0.50	47-how/mea(○)	298.15	824.50 ± 0.50	0.70	88-cac/cos(◆)
273.15	844.00 ± 2.00	-0.76	48-zal(×)	313.15	810.54 ± 0.50	0.55	88-cac/cos(◆)
280.15	837.10 ± 2.00	-2.05	48-zal <sup>1)</sup>	323.15	800.95 ± 0.50	0.69	88-cac/cos(◆)
293.15	827.90 ± 2.00	-0.30	48-zal <sup>1)</sup>	298.15	823.63 ± 0.30	-0.17	94-tar/jun(□)

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1887-ref, 19-eyk, 27-nor/cor, 35-sav, 36-nor/has, 40-hov/lan-1, 50-pic/zie, 52-van, 55-soe/fre, 56-sok/fed].

cont.

## 3-Methyl-3-pentanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4).$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	847.22 ± 1.55	298.15	823.80 ± 0.44	330.00	793.37 ± 0.95
280.00	839.28 ± 0.87	300.00	822.15 ± 0.44	340.00	782.95 ± 1.17
290.00	830.92 ± 0.52	310.00	812.96 ± 0.53	350.00	772.12 ± 1.36
293.15	828.20 ± 0.47	320.00	803.37 ± 0.72		

## 4-Methyl-1-pentanol

[626-89-1]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

41

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.9343 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 8.2317 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

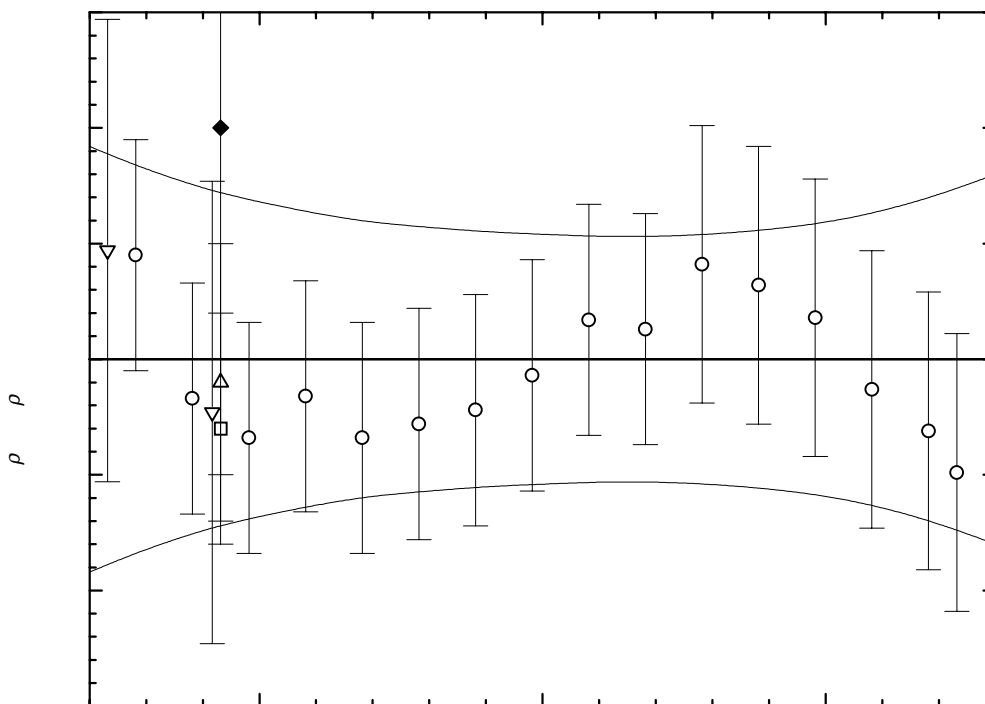
Coefficient	$T = 273.15 \text{ to } 423.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.17775 \cdot 10^2$
B	$-2.40364 \cdot 10^{-2}$
C	$-1.13490 \cdot 10^{-3}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)
273.15	$827.00 \pm 1.00$	0.47	19-beh( $\nabla$ )	358.15	$763.76 \pm 0.50$	0.17	40-hov/lan( $\circ$ )
291.65	$814.00 \pm 1.00$	-0.23	19-beh( $\nabla$ )	368.15	$755.24 \pm 0.50$	0.13	40-hov/lan( $\circ$ )
293.15	$813.10 \pm 0.60$	-0.10	36-oli( $\Delta$ )	378.15	$746.81 \pm 0.60$	0.41	40-hov/lan( $\circ$ )
278.15	$823.74 \pm 0.50$	0.45	40-hov/lan( $\circ$ )	388.15	$737.78 \pm 0.60$	0.32	40-hov/lan( $\circ$ )
288.15	$816.45 \pm 0.50$	-0.17	40-hov/lan( $\circ$ )	398.15	$728.48 \pm 0.60$	0.18	40-hov/lan( $\circ$ )
298.15	$809.38 \pm 0.50$	-0.34	40-hov/lan( $\circ$ )	408.15	$718.78 \pm 0.60$	-0.13	40-hov/lan( $\circ$ )
308.15	$802.44 \pm 0.50$	-0.16	40-hov/lan( $\circ$ )	418.15	$708.98 \pm 0.60$	-0.31	40-hov/lan( $\circ$ )
318.15	$794.91 \pm 0.50$	-0.34	40-hov/lan( $\circ$ )	423.15	$703.90 \pm 0.60$	-0.49	40-hov/lan( $\circ$ )
328.15	$787.40 \pm 0.50$	-0.28	40-hov/lan( $\circ$ )	293.15	$812.90 \pm 0.50$	-0.30	50-pic/zie( $\square$ )
338.15	$779.66 \pm 0.50$	-0.22	40-hov/lan( $\circ$ )	293.15	$814.20 \pm 1.50$	1.00	52-coo( $\blacklozenge$ )
348.15	$771.78 \pm 0.50$	-0.07	40-hov/lan( $\circ$ )				

**Further references:** [02-gri/tis, 27-nor/cor, 41-hus/age].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**4-Methyl-1-pentanol** (cont.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	828.55 ± 0.92	320.00	793.87 ± 0.59	390.00	735.78 ± 0.56
280.00	822.07 ± 0.82	330.00	786.25 ± 0.57	400.00	726.58 ± 0.59
290.00	815.36 ± 0.74	340.00	778.41 ± 0.55	410.00	717.14 ± 0.64
293.15	813.20 ± 0.72	350.00	770.34 ± 0.54	420.00	707.48 ± 0.71
298.15	809.72 ± 0.69	360.00	762.04 ± 0.53	430.00	697.60 ± 0.80
300.00	808.42 ± 0.68	370.00	753.51 ± 0.53		
310.00	801.26 ± 0.63	380.00	744.76 ± 0.54		

**4-Methyl-2-pentanol**

[108-11-2]

C<sub>6</sub>H<sub>14</sub>O

MW = 102.18

42

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 3.2132 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 4.5436 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

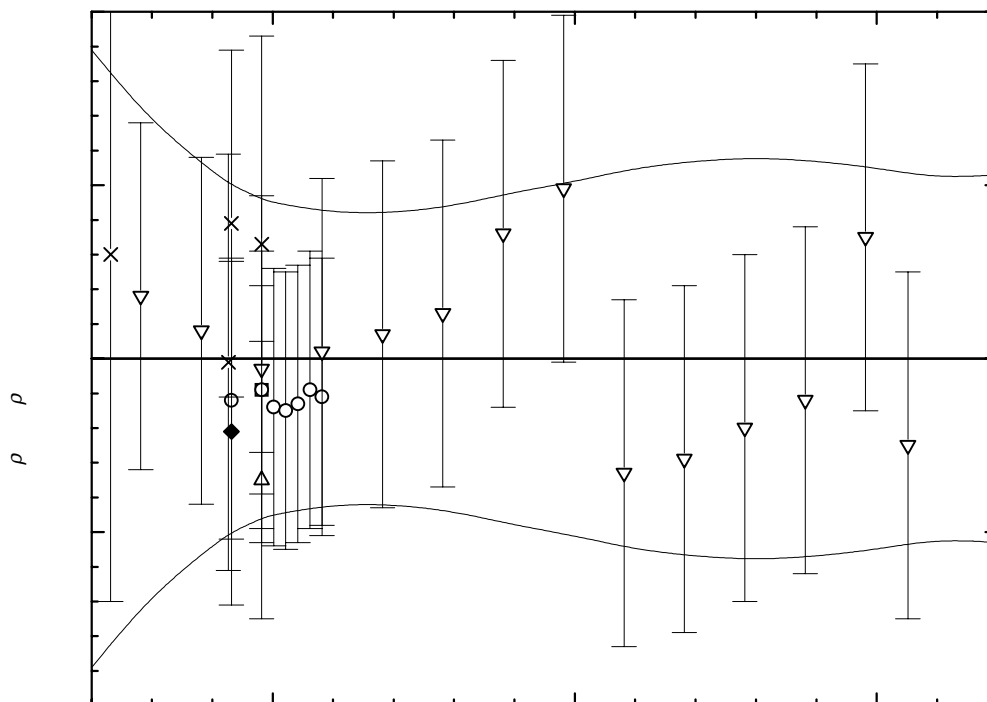
Coefficient	$T = 273.15 \text{ to } 405.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.40784 \cdot 10^2$
B	$-1.09111 \cdot 10^{-1}$
C	$-1.18327 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	823.00 ± 1.00	0.30	09-gue(✕)	398.15	710.12 ± 0.50	0.35	38-hov/lan(∇)
298.15	803.40 ± 0.60	0.33	38-gin/web(✕)	405.15	702.10 ± 0.50	-0.25	38-hov/lan(∇)
278.15	819.07 ± 0.50	0.18	38-hov/lan(∇)	293.15	807.50 ± 0.50	0.39	44-hen/mat(✕)
288.15	811.18 ± 0.50	0.08	38-hov/lan(∇)	292.65	807.50 ± 0.60	-0.01	49-ken/str(✕)
298.15	803.04 ± 0.50	-0.03	38-hov/lan(∇)	293.15	806.90 ± 0.50	-0.21	68-ano(◆)
308.15	794.82 ± 0.50	0.02	38-hov/lan(∇)	298.15	802.72 ± 0.40	-0.35	84-bra/pin(Δ)
318.15	786.37 ± 0.50	0.07	38-hov/lan(∇)	293.15	806.99 ± 0.40	-0.12	85-ort(○)
328.15	777.69 ± 0.50	0.13	38-hov/lan(∇)	298.15	802.98 ± 0.40	-0.09	85-ort(○)
338.15	768.95 ± 0.50	0.36	38-hov/lan(∇)	300.15	801.29 ± 0.40	-0.14	85-ort(○)
348.15	759.87 ± 0.50	0.49	38-hov/lan(∇)	302.15	799.64 ± 0.40	-0.15	85-ort(○)
358.15	749.60 ± 0.50	-0.33	38-hov/lan(∇)	304.15	798.01 ± 0.40	-0.13	85-ort(○)
368.15	739.95 ± 0.50	-0.29	38-hov/lan(∇)	306.15	796.38 ± 0.40	-0.09	85-ort(○)
378.15	730.12 ± 0.50	-0.20	38-hov/lan(∇)	308.15	794.69 ± 0.40	-0.11	85-ort(○)
388.15	720.04 ± 0.50	-0.12	38-hov/lan(∇)	298.15	802.98 ± 0.30	-0.09	94-tar/jun(□)

cont.

**Further references:** [11-pic/ken, 12-gue, 14-vav, 19-beh, 21-bru/cre, 23-bru, 33-van, 38-whi/joh, 39-dup/dar, 47-tuo/guy, 48-wei, 50-pic/zie, 53-ano-1, 58-ano-5, 58-rao/ram].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	825.06 ± 0.89	310.00	793.25 ± 0.42	370.00	738.42 ± 0.57
280.00	817.46 ± 0.68	320.00	784.70 ± 0.42	380.00	728.46 ± 0.58
290.00	809.63 ± 0.54	330.00	775.92 ± 0.44	390.00	718.26 ± 0.57
293.15	807.11 ± 0.50	340.00	766.90 ± 0.48	400.00	707.82 ± 0.55
298.15	803.07 ± 0.46	350.00	757.64 ± 0.51	410.00	697.14 ± 0.52
300.00	801.56 ± 0.45	360.00	748.15 ± 0.55	420.00	686.23 ± 0.53



2.1.3 Alkanols, C<sub>7</sub>

**2,2-Dimethyl-1-pentanol** [2370-12-9] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 43

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	837.9 ± 1.0	65-shu/puz

**2,2-Dimethyl-3-pentanol** [3970-62-5] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 44

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.493$ .

Coefficient	$\rho = A + BT$
$A$	1060.34
$B$	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	824.6 ± 2.0	-1.22	13-fav <sup>1)</sup>	293.15	825.4 ± 0.6	-0.42	49-boo/gre
293.15	824.0 ± 2.0	-1.82	29-edg/cal <sup>1)</sup>	293.15	826.4 ± 1.0	0.58	50-pic/zie
298.15	822.4 ± 1.0	0.58	38-gin/hau	293.15	828.1 ± 2.0	2.28	55-gay/cau <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	828.3 ± 0.8
293.15	825.8 ± 0.6
298.15	821.8 ± 0.7

**2,3-Dimethyl-1-pentanol** [10143-23-4] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 45

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
296.15	836.0 ± 2.0	31-lev/mar-2

**2,3-Dimethyl-2-pentanol** [4911-70-0] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 46

**Table 1.** Fit with estimated  $B$  coefficient for 5 accepted points. Deviation  $\sigma_w = 0.857$ .

Coefficient	$\rho = A + BT$
$A$	1060.84
$B$	-0.780

cont.



**2,3-Dimethyl-2-pentanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	803.0 ± 5.0	-29.18	29-edg/cal <sup>1)</sup>	298.15	830.7 ± 2.0	2.42	38-gin/hau
298.15	828.5 ± 1.0	0.22	36-nor/has	293.15	832.4 ± 1.0	0.22	43-jam
298.15	827.6 ± 1.0	-0.68	36-nor/has	293.15	830.7 ± 2.0	-1.48	50-pic/zie

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	834.6 ± 1.5
293.15	832.2 ± 1.4
298.15	828.3 ± 1.4

**1-2,3-Dimethyl-2-pentanol** [28357-68-8] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 47**Table 1.** Experimental value with uncertainty.

$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	836.0 ± 1.0	57-luk/lan

**2,3-Dimethyl-3-pentanol** [595-41-5] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 48**Table 1.** Fit with estimated *B* coefficient for 6 accepted points. Deviation  $\sigma_w = 0.901$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1075.79
<i>B</i>	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
273.15	858.6 ± 1.0	1.33	21-par/sim	298.15	838.2 ± 1.0	0.93	36-nor/has
293.15	841.5 ± 1.0	0.23	21-par/sim	298.15	836.5 ± 1.0	-0.77	38-gin/hau
293.15	833.0 ± 4.0	-8.27	33-whi/eve <sup>1)</sup>	293.15	840.2 ± 1.0	-1.07	50-pic/zie
298.15	836.6 ± 1.0	-0.67	36-nor/has	293.15	832.0 ± 4.0	-9.27	56-sok/fed <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	859.8 ± 1.6	293.15	841.3 ± 1.1
280.00	851.8 ± 1.3	298.15	837.3 ± 1.2
290.00	843.8 ± 1.1		

**2,4-Dimethyl-1-pentanol** [6305-71-1] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 49**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.500$ .

Coefficient	$\rho = A + BT$
A	1054.02
B	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	793.0 ± 15.0	-26.50	31-chu/mar <sup>1)</sup>
298.15	821.0 ± 5.0	5.50	32-mor/har <sup>1)</sup>
298.15	816.0 ± 2.0	0.50	35-lev/mar
293.15	819.0 ± 2.0	-0.50	39-gol/tay

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	822.0 ± 1.2
293.15	819.5 ± 1.1
298.15	815.5 ± 1.1

**2,4-Dimethyl-2-pentanol** [625-06-9] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 50**Table 1.** Fit with estimated *B* coefficient for 7 accepted points. Deviation  $\sigma_w = 0.680$ .

Coefficient	$\rho = A + BT$
A	1034.29
B	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	815.7 ± 3.0	4.20	09-kho <sup>1)</sup>	293.15	811.0 ± 1.0	-0.50	38-whi/joh
273.15	832.5 ± 3.0	5.80	09-kho <sup>1)</sup>	293.15	812.2 ± 1.0	0.70	50-pic/zie
293.15	812.2 ± 1.0	0.70	24-cha/deg	293.15	811.9 ± 1.0	0.40	57-pet/sus
293.15	810.3 ± 1.0	-1.20	31-deg	293.15	811.9 ± 1.0	0.40	59-pet/zak-1
288.15	814.8 ± 1.0	-0.50	31-deg	293.15	814.6 ± 2.0	3.10	66-are/tav <sup>1)</sup>
298.15	810.0 ± 2.0	2.30	38-gin/hau <sup>1)</sup>				

<sup>1)</sup> Not included in calculation of linear coefficients.

cont.

**2,4-Dimethyl-2-pentanol** (cont.)**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	821.5 ± 1.5
290.00	813.9 ± 0.9
293.15	811.5 ± 0.9
298.15	807.7 ± 1.1

**2,4-Dimethyl-3-pentanol**

[600-36-2]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

51

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 1.0054$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 2.2149 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 290.15$ to $394.75$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.11751 \cdot 10^3$
B	$-9.81289 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

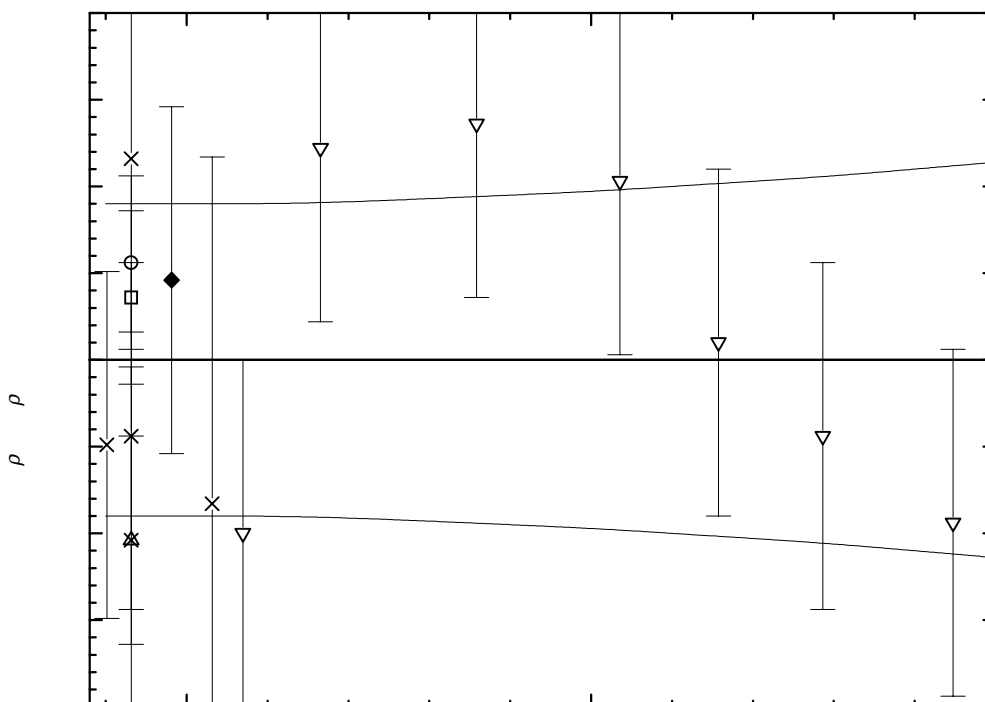
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
290.15	832.30 ± 1.00	-0.49	1876-mun(✕)	293.15	830.20 ± 0.50	0.36	53-raz/old(□)
293.15	828.80 ± 1.00	-1.04	1891-pol(✕)	306.95	815.30 ± 1.00	-1.00	63-tho/mea(∇)
298.15	825.40 ± 1.00	0.46	38-gin/hau(◆)	316.55	808.10 ± 1.00	1.22	63-tho/mea(∇)
293.15	831.00 ± 1.00	1.16	38-whi/joh(✕)	335.85	789.30 ± 1.00	1.36	63-tho/mea(∇)
293.15	828.80 ± 0.60	-1.04	39-gol/tay(Δ)	353.55	771.60 ± 1.00	1.03	63-tho/mea(∇)
303.15	819.20 ± 2.00	-0.83	48-wei(✕)	365.75	758.70 ± 1.00	0.10	63-tho/mea(∇)
293.15	829.40 ± 1.00	-0.44	50-pic/zie(✕)	378.65	745.50 ± 1.00	-0.44	63-tho/mea(∇)
293.15	830.40 ± 0.50	0.56	52-coo(O)	394.75	729.20 ± 1.00	-0.94	63-tho/mea(∇)

**Further references:** [44-hus/awu, 49-naz/pin].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	832.93 ± 0.90	320.00	803.50 ± 0.91	370.00	754.43 ± 1.03
293.15	829.84 ± 0.90	330.00	793.68 ± 0.93	380.00	744.62 ± 1.06
298.15	824.94 ± 0.90	340.00	783.87 ± 0.95	390.00	734.81 ± 1.10
300.00	823.12 ± 0.90	350.00	774.06 ± 0.97	400.00	724.99 ± 1.14
310.00	813.31 ± 0.90	360.00	764.24 ± 1.00		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3,3-Dimethyl-1-pentanol** [19264-94-9] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 52

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	832.0 ± 1.0	45-sch

**3,3-Dimethyl-2-pentanol** [19781-24-9] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 53

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	827.0 ± 1.5	29-edg/cal

**3,4-Dimethyl-1-pentanol** [6570-87-2] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 54**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
297.15	819.0 ± 2.0	41-hus/age
293.15	834.5 ± 2.0	47-det/cra
325.15	803.5 ± 2.0	60-tsu/kis

**3,4-Dimethyl-2-pentanol** [64502-86-9] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 55**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
294.15	836.0 ± 2.0	19-wil/hat

**4,4-Dimethyl-1-pentanol** [3121-79-7] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 56**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.15	820.0 ± 2.0	49-mal/vol <sup>1)</sup>
293.15	815.2 ± 1.0	31-hom
293.15	815.0 ± 1.0	33-whi/hom-1
293.15	815.1 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**4,4-Dimethyl-2-pentanol** [6144-93-0] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 57**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	811.5 ± 1.0	33-whi/hom	293.15	811.3 ± 1.0	52-coo
293.15	812.0 ± 1.0	33-whi/hom-1	293.15	813.3 ± 1.0	55-gay/cau
293.15	811.5 ± 1.0	33-whi/kru	293.15	811.9 ± 1.2	Recommended

**2-Ethyl-2-methyl-1-butanol** [18371-13-6] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 58**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 1.550$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1055.31
<i>B</i>	-0.780

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	828.2 ± 1.0	1.55	25-fav/zal
273.15	840.7 ± 1.0	-1.55	25-fav/zal

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	844.7 ± 1.9
280.00	836.9 ± 1.8
290.00	829.1 ± 1.8
293.15	826.7 ± 1.9
298.15	822.7 ± 1.9

**2-Ethyl-3-methyl-1-butanol** [32444-34-1] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 59

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	832.7 ± 1.0	56-sar/new
298.15	832.6 ± 0.8	59-tsu/hay
298.15	832.6 ± 1.0	60-tsu/kis
298.15	832.6 ± 0.8	Recommended

**2-Ethyl-1-pentanol** [27522-11-8] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 60

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	832.0 ± 3.0	32-mor/har <sup>1)</sup>
298.15	828.0 ± 2.0	36-lev/rot-1
298.15	829.6 ± 2.0	50-ada/van
298.15	828.8 ± 2.1	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Ethyl-2-pentanol** [609-27-8] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 61

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.200$ .

Coefficient	$\rho = A + BT$
$A$	1071.82
$B$	-0.800

cont.

**3-Ethyl-2-pentanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
273.15	853.1 ± 2.0	-0.20	07-fou/tif
298.15	833.5 ± 2.0	0.20	29-luc

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	855.8 ± 2.4
280.00	847.8 ± 1.9
290.00	839.8 ± 1.9
293.15	837.3 ± 2.0
298.15	833.3 ± 2.2

**3-Ethyl-3-pentanol**

[597-49-9]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

62

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 5.5395 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 3.5871 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

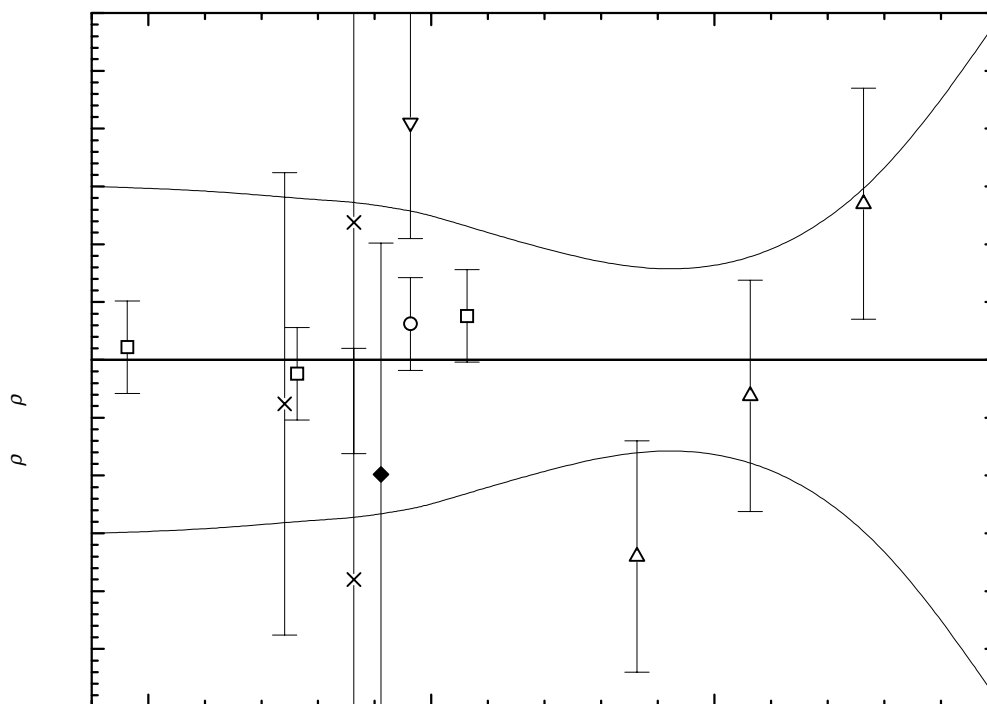
Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.65425 \cdot 10^2$
B	$7.69225 \cdot 10^{-1}$
C	$-2.87450 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
287.05	849.00 ± 2.00	-0.38	19-eyk(✕)	338.15	798.20 ± 1.00	1.35	39-owe/qua(Δ)
298.15	841.30 ± 1.00	2.05	29-luc(∇)	293.15	842.00 ± 2.00	-1.90	53-gru/ost(✕)
295.54	840.70 ± 2.00	-0.99	32-boe/wil(◆)	273.15	861.18 ± 0.40	0.11	55-tim/hen(□)
273.15	860.30 ± 1.00	-0.77	39-owe/qua <sup>1)</sup>	288.15	848.29 ± 0.40	-0.12	55-tim/hen(□)
298.15	836.70 ± 1.00	-2.55	39-owe/qua <sup>1)</sup>	303.15	834.83 ± 0.40	0.38	55-tim/hen(□)
308.15	827.30 ± 1.00	-2.21	39-owe/qua <sup>1)</sup>	293.15	845.09 ± 2.00	1.19	56-lib/lap-1(✕)
318.15	817.50 ± 1.00	-1.70	39-owe/qua(Δ)	298.15	839.56 ± 0.40	0.31	88-cac/cos(○)
328.15	808.00 ± 1.00	-0.31	39-owe/qua(Δ)				

<sup>1)</sup> Not included in Fig. 1.**Further references:** [29-edg/cal, 50-pic/zie, 55-soe/fre, 62-and/kuk-1].

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	$863.57 \pm 1.50$	298.15	$839.25 \pm 1.29$	330.00	$806.24 \pm 0.87$
280.00	$855.45 \pm 1.47$	300.00	$837.49 \pm 1.25$	340.00	$794.67 \pm 1.54$
290.00	$846.76 \pm 1.38$	310.00	$827.65 \pm 0.95$	350.00	$782.53 \pm 2.94$
293.15	$843.90 \pm 1.37$	320.00	$817.23 \pm 0.73$		



## 1-Heptanol

[111-70-6]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

63

 $T_c = 632.50$  K [89-tej/lee] $\rho_c = 267.00$  kg·m<sup>-3</sup> [89-tej/lee]

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_T = 7.2440 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (2.0233 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 3.3667 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $510.00$ K	$T = 510.00$ to $632.50$ K
	$\rho = A + BT + CT^2 + DT^3 + \dots$	$\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$9.98526 \cdot 10^2$	$9.10034 \cdot 10^{-1}$
B	$-6.23212 \cdot 10^{-1}$	$-1.32340 \cdot 10^{-2}$
C	$4.74025 \cdot 10^{-4}$	$8.23480 \cdot 10^{-5}$
D	$-1.34624 \cdot 10^{-6}$	$-1.83963 \cdot 10^{-7}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	$836.20 \pm 0.50$	-0.03	31-def(X)	533.15	$600.00 \pm 1.50$	2.80	66-efr(X)
273.15	$836.20 \pm 1.00$	-0.03	31-def <sup>1)</sup>	553.15	$574.00 \pm 1.50$	3.18	66-efr(X)
288.15	$825.99 \pm 0.50$	-0.11	31-def <sup>1)</sup>	573.15	$540.00 \pm 1.50$	0.23	66-efr(X)
288.15	$825.99 \pm 1.00$	-0.11	31-def <sup>1)</sup>	593.15	$496.00 \pm 1.50$	-3.22	66-efr(X)
303.15	$815.81 \pm 0.50$	0.15	31-def <sup>1)</sup>	603.15	$470.00 \pm 1.50$	-2.90	66-efr(X)
303.15	$818.81 \pm 1.00$	3.15	31-def <sup>1)</sup>	613.15	$440.00 \pm 2.00$	-0.03	66-efr(X)
273.15	$836.32 \pm 0.20$	0.09	32-ell/rei(◆)	618.15	$420.00 \pm 2.00$	0.20	66-efr(X)
298.15	$819.13 \pm 0.20$	-0.04	32-ell/rei <sup>1)</sup>	623.15	$400.00 \pm 5.00$	4.68	66-efr(X)
273.15	$836.04 \pm 0.30$	-0.19	35-bil/gis(X)	628.15	$370.00 \pm 5.00$	7.80	66-efr(X)
288.15	$825.80 \pm 0.30$	-0.30	35-bil/gis(X)	298.15	$819.30 \pm 0.25$	0.13	76-kow/kas <sup>1)</sup>
303.15	$815.57 \pm 0.30$	-0.09	35-bil/gis <sup>1)</sup>	298.15	$819.29 \pm 0.25$	0.12	76-kow/kas <sup>1)</sup>
273.15	$836.50 \pm 0.10$	0.27	59-mck/ski(Δ)	313.15	$810.47 \pm 0.25$	1.96	76-kow/kas(X)
273.15	$839.00 \pm 1.50$	2.77	66-efr <sup>1)</sup>	298.15	$819.42 \pm 0.20$	0.25	79-dia/tar <sup>1)</sup>
293.15	$824.00 \pm 1.50$	1.35	66-efr <sup>1)</sup>	308.15	$812.28 \pm 0.20$	0.18	79-dia/tar(X)
313.15	$809.00 \pm 1.50$	0.49	66-efr <sup>1)</sup>	318.15	$805.10 \pm 0.20$	0.22	79-dia/tar(X)
333.15	$794.00 \pm 1.50$	0.26	66-efr <sup>1)</sup>	333.15	$794.05 \pm 0.20$	0.31	79-dia/tar(X)
353.15	$778.00 \pm 1.50$	-0.26	66-efr <sup>1)</sup>	293.15	$822.10 \pm 0.30$	-0.55	82-ort <sup>1)</sup>
373.15	$762.00 \pm 1.50$	-0.03	66-efr <sup>1)</sup>	298.15	$819.50 \pm 0.30$	0.33	82-ort <sup>1)</sup>
393.15	$745.00 \pm 1.50$	0.03	66-efr <sup>1)</sup>	303.15	$815.70 \pm 0.30$	0.04	82-ort <sup>1)</sup>
413.15	$726.00 \pm 1.50$	-1.02	66-efr(X)	308.15	$812.10 \pm 0.30$	-0.00	82-ort <sup>1)</sup>
433.15	$707.00 \pm 1.50$	-1.11	66-efr(X)	313.15	$811.20 \pm 0.30$	2.69	82-ort <sup>1)</sup>
453.15	$688.00 \pm 1.50$	-0.19	66-efr(X)	318.15	$804.80 \pm 0.30$	-0.08	82-ort(X)
473.15	$669.00 \pm 1.50$	1.83	66-efr(X)	298.15	$818.24 \pm 0.10$	-0.93	84-sak/nak(O)
493.15	$648.00 \pm 1.50$	2.99	66-efr <sup>1)</sup>	303.15	$815.72 \pm 0.20$	0.06	89-vij/nai(V)
513.15	$626.00 \pm 1.50$	4.36	66-efr(X)	323.15	$801.09 \pm 0.10$	-0.12	93-gar/ban-I(□)

<sup>1)</sup> Not included in Fig. 1.

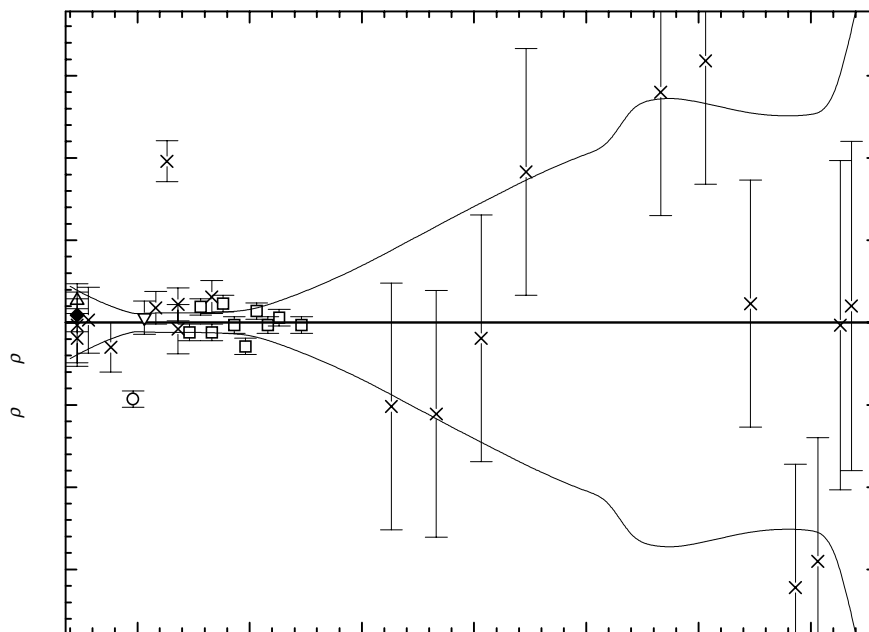
cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
328.15	797.68 ± 0.10	0.19	93-gar/ban-1(□)	363.15	770.31 ± 0.10	0.06	93-gar/ban-1(□)
333.15	793.62 ± 0.10	-0.12	93-gar/ban-1(□)	373.15	762.00 ± 0.10	-0.03	93-gar/ban-1(□)
338.15	790.17 ± 0.10	0.23	93-gar/ban-1(□)	278.15	832.91 ± 0.40	0.03	94-rom/pel(✕)
343.15	786.06 ± 0.10	-0.03	93-gar/ban-1(□)	288.15	825.96 ± 0.40	-0.14	94-rom/pel <sup>1)</sup>
348.15	781.91 ± 0.10	-0.29	93-gar/ban-1(□)	298.15	819.06 ± 0.40	-0.11	94-rom/pel <sup>1)</sup>
353.15	778.40 ± 0.10	0.14	93-gar/ban-1(□)	308.15	811.99 ± 0.40	-0.11	94-rom/pel <sup>1)</sup>
358.15	774.25 ± 0.10	-0.03	93-gar/ban-1(□)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1877-cro, 1877-cro-1, 1880-bru-1, 1884-per, 1884-zan, 1886-gar, 1890-gar, 1893-eyk, 06-car/fer, 09-fal-1, 14-low, 18-lev/tay, 19-beh, 19-eyk, 25-fai-1, 27-nor/cor, 27-ver/coo, 28-har-2, 30-bin/for, 30-err/she, 30-she, 33-ano, 33-but/tho, 34-bur/adk, 34-car/jon, 35-but/ram, 35-mah-1, 37-oli, 41-hus/age, 42-mul, 44-app/dob, 45-add, 48-jon/bow, 48-vog-2, 49-pra/dra, 50-mum/phi, 50-pic/zie, 50-sac/sau, 52-coo, 52-eri-1, 66-rob/edm, 67-gol/per, 70-puz/bul, 73-min/rue, 74-moo/wel, 75-mat/fer, 81-sjo/dyh, 82-ven/dha, 83-fuk/ogi, 83-rau/ste, 85-fer/pin, 85-ogi/ara, 85-ort-1, 85-ort/paz-1, 85-sar/paz, 85-zhu, 86-ash/sri, 86-dew/meh, 87-dew/meh, 88-ort/gar, 89-ala/sal, 89-dew/gup, 90-vij/nai, 91-ram/muk, 93-ami/ara, 93-yan/mae, 94-kum/nai, 94-kum/nai-1, 94-yu /tsa-1, 95-cas/cal, 96-elbj].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**1-Heptanol** (cont.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	838.32 ± 0.44	380.00	756.28 ± 0.44	510.00	625.40 ± 2.14
280.00	831.64 ± 0.29	390.00	747.72 ± 0.56	520.00	613.39 ± 2.64
290.00	824.83 ± 0.18	400.00	738.93 ± 0.69	530.00	601.13 ± 2.72
293.15	822.65 ± 0.15	410.00	729.91 ± 0.83	540.00	588.48 ± 2.73
298.15	819.17 ± 0.11	420.00	720.65 ± 0.98	550.00	575.19 ± 2.68
300.00	817.88 ± 0.11	430.00	711.16 ± 1.12	560.00	560.90 ± 2.62
310.00	810.78 ± 0.12	440.00	701.41 ± 1.27	570.00	545.14 ± 2.56
320.00	803.52 ± 0.12	450.00	691.39 ± 1.41	580.00	527.28 ± 2.52
330.00	796.11 ± 0.12	460.00	681.11 ± 1.55	590.00	506.52 ± 2.51
340.00	788.52 ± 0.13	470.00	670.56 ± 1.69	600.00	481.77 ± 2.52
350.00	780.75 ± 0.15	480.00	659.72 ± 1.82	610.00	451.29 ± 2.59
360.00	772.79 ± 0.23	490.00	648.58 ± 1.94	620.00	411.37 ± 3.78
370.00	764.64 ± 0.33	500.00	637.15 ± 2.05	630.00	344.48 ± 5.46

**2-Heptanol**

[543-49-7]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

64

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 8.0415 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.7660 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

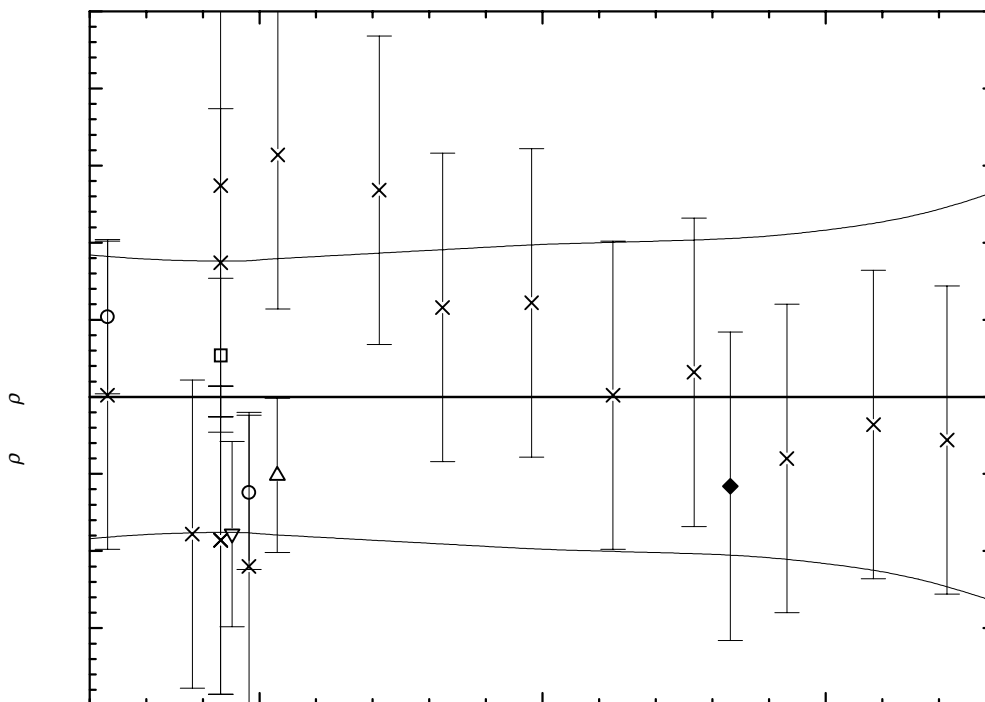
Coefficient	$T = 273.15 \text{ to } 421.45 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.15825 \cdot 10^2$
B	$4.92881 \cdot 10^{-2}$
C	$-1.31078 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	818.50 ± 1.00	0.87	11-pic/ken(×)	293.15	816.70 ± 1.00	-0.93	52-pom(×)
383.15	741.70 ± 1.00	-0.58	12-pic/ken(◆)	298.15	812.90 ± 1.00	-1.10	52-pom(×)
295.15	815.30 ± 0.60	-0.89	30-err/she(∇)	303.25	811.80 ± 1.00	1.57	63-tho/mea(×)
273.15	831.50 ± 1.00	0.01	30-she(×)	321.15	797.80 ± 1.00	1.34	63-tho/mea(×)
288.15	820.30 ± 1.00	-0.89	30-she(×)	332.35	788.00 ± 1.00	0.58	63-tho/mea(×)
293.15	816.70 ± 1.00	-0.93	30-she(×)	348.05	774.80 ± 1.00	0.61	63-tho/mea(×)
273.15	832.01 ± 0.50	0.52	32-ell/rei(○)	362.45	761.50 ± 1.00	0.01	63-tho/mea(×)
298.15	813.38 ± 0.50	-0.62	32-ell/rei(○)	376.75	748.50 ± 1.00	0.16	63-tho/mea(×)
303.15	809.80 ± 0.50	-0.51	48-wei(Δ)	393.15	732.20 ± 1.00	-0.40	63-tho/mea(×)
293.15	819.00 ± 1.50	1.37	50-pic/zie(×)	408.45	717.10 ± 1.00	-0.18	63-tho/mea(×)
293.15	817.90 ± 0.50	0.27	52-coo(□)	421.45	703.50 ± 1.00	-0.28	63-tho/mea(×)

cont.

**Further references:** [09-hen, 09-mas, 13-tho, 49-mal/vol, 62-cuv/nor].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	833.58 ± 0.92	320.00	797.37 ± 0.93	390.00	735.68 ± 1.04
280.00	826.86 ± 0.89	330.00	789.35 ± 0.95	400.00	725.82 ± 1.08
290.00	819.88 ± 0.88	340.00	781.06 ± 0.97	410.00	715.69 ± 1.13
293.15	817.63 ± 0.88	350.00	772.51 ± 0.99	420.00	705.30 ± 1.21
298.15	814.00 ± 0.88	360.00	763.69 ± 1.00	430.00	694.66 ± 1.33
300.00	812.64 ± 0.89	370.00	754.62 ± 1.01		
310.00	805.14 ± 0.91	380.00	745.28 ± 1.02		

## 3-Heptanol

[589-82-2]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

65

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 5.5943 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.3013 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $416.55$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.65814 \cdot 10^2$
B	$-1.88467 \cdot 10^{-1}$
C	$-1.04313 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

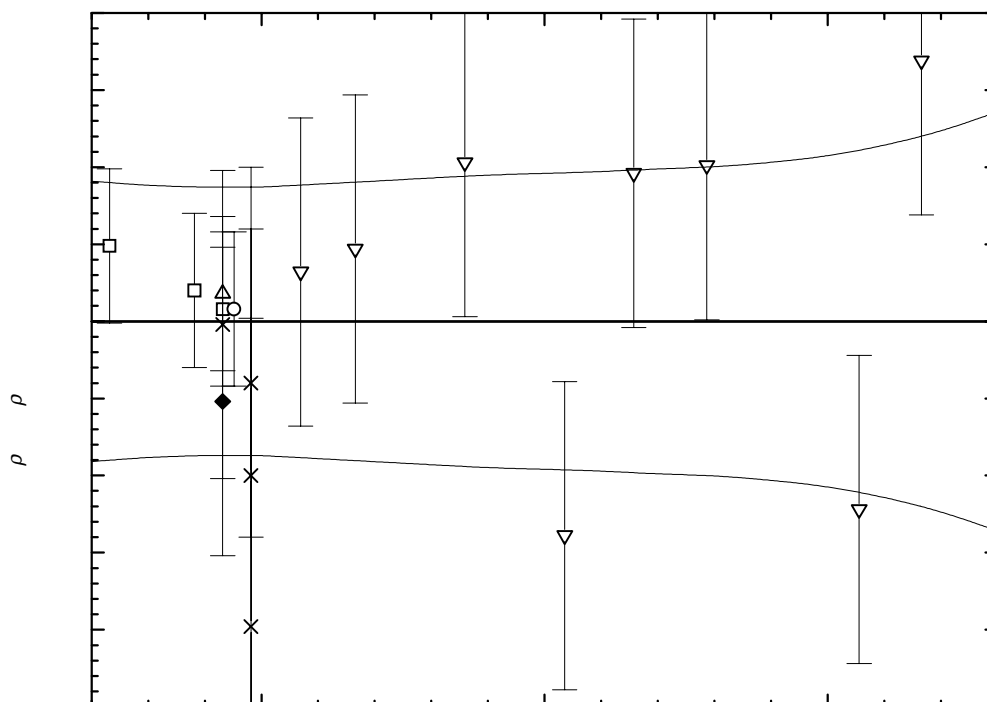
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
298.15	$815.90 \pm 2.00$	-1.00	28-dil/luc(✕)	306.95	$810.00 \pm 1.00$	0.32	63-tho/mea(∇)
295.15	$819.40 \pm 0.50$	0.08	30-err/she(○)	316.55	$802.10 \pm 1.00$	0.47	63-tho/mea(∇)
273.15	$837.00 \pm 0.50$	0.49	30-she(□)	335.95	$785.80 \pm 1.00$	1.03	63-tho/mea(∇)
288.15	$825.10 \pm 0.50$	0.20	30-she(□)	353.55	$767.40 \pm 1.00$	-1.39	63-tho/mea(∇)
293.15	$821.00 \pm 0.50$	0.08	30-she(□)	365.75	$758.30 \pm 1.00$	0.96	63-tho/mea(∇)
298.15	$816.50 \pm 1.00$	-0.40	50-ada/van(✕)	378.65	$745.90 \pm 1.00$	1.01	63-tho/mea(∇)
293.15	$820.40 \pm 1.00$	-0.52	50-pic/zie(◆)	405.55	$716.60 \pm 1.00$	-1.22	63-tho/mea(∇)
293.15	$821.10 \pm 0.50$	0.18	52-coo(Δ)	416.55	$708.00 \pm 1.00$	1.69	63-tho/mea(∇)
293.15	$820.90 \pm 1.00$	-0.02	53-ano-1(✕)	298.15	$814.92 \pm 2.00$	-1.98	88-tan/luo(✕)

**Further references:** [13-pic/ken, 61-tis/sta].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	$838.88 \pm 0.91$	320.00	$798.69 \pm 0.91$	390.00	$733.65 \pm 1.03$
280.00	$831.26 \pm 0.88$	330.00	$790.02 \pm 0.93$	400.00	$723.53 \pm 1.07$
290.00	$823.43 \pm 0.87$	340.00	$781.15 \pm 0.95$	410.00	$713.19 \pm 1.14$
293.15	$820.92 \pm 0.87$	350.00	$772.07 \pm 0.96$	420.00	$702.65 \pm 1.23$
298.15	$816.90 \pm 0.87$	360.00	$762.78 \pm 0.97$	430.00	$691.90 \pm 1.36$
300.00	$815.39 \pm 0.87$	370.00	$753.28 \pm 0.99$		
310.00	$807.14 \pm 0.89$	380.00	$743.57 \pm 1.00$		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**4-Heptanol**

[589-55-9]

**C<sub>7</sub>H<sub>16</sub>O****MW = 116.2****66****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 1.1547$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.3522 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $416.05$ K
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.10927 \cdot 10^2$
B	$9.60428 \cdot 10^{-2}$
C	$-1.40301 \cdot 10^{-3}$

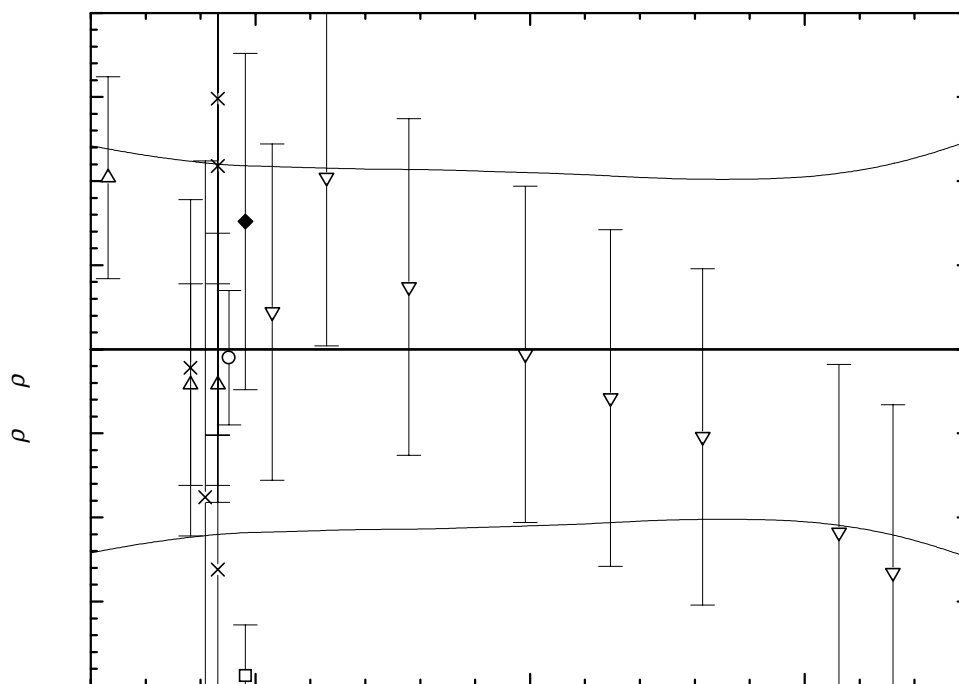
cont.

## 4-Heptanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
288.15	822.00 ± 1.00	-0.11	14-vav(×)	293.15	817.20 ± 2.00	-1.31	52-coo(×)
293.15	820.00 ± 2.00	1.49	19-beh(×)	293.15	819.60 ± 2.00	1.09	56-shu/bel(×)
290.85	819.30 ± 2.00	-0.88	19-eyk(×)	303.05	811.40 ± 1.00	0.22	63-tho/mea(∇)
298.15	812.90 ± 0.30	-1.94	23-bru(□)	312.95	804.60 ± 1.00	1.02	63-tho/mea(∇)
298.15	815.60 ± 1.00	0.76	27-nor/cor(◆)	327.95	791.90 ± 1.00	0.37	63-tho/mea(∇)
295.15	817.00 ± 0.40	-0.05	30-err/she(○)	349.15	773.40 ± 1.00	-0.03	63-tho/mea(∇)
273.15	833.50 ± 0.60	1.02	30-she(Δ)	364.65	759.10 ± 1.00	-0.29	63-tho/mea(∇)
288.15	821.90 ± 0.60	-0.21	30-she(Δ)	381.45	742.90 ± 1.00	-0.52	63-tho/mea(∇)
293.15	818.30 ± 0.60	-0.21	30-she(Δ)	406.25	717.30 ± 1.00	-1.09	63-tho/mea(∇)
293.15	820.00 ± 2.00	1.49	39-gol/tay(×)	416.05	706.70 ± 1.00	-1.33	63-tho/mea(∇)

**Further references:** [28-dil/luc, 36-tuo, 42-boe/han, 50-pic/zie].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	834.58 ± 1.21	320.00	797.99 ± 1.07	390.00	734.99 ± 1.01
280.00	827.82 ± 1.15	330.00	789.83 ± 1.07	400.00	724.86 ± 1.02
290.00	820.79 ± 1.11	340.00	781.39 ± 1.06	410.00	714.46 ± 1.06
293.15	818.51 ± 1.10	350.00	772.67 ± 1.05	420.00	703.77 ± 1.13
298.15	814.84 ± 1.09	360.00	763.67 ± 1.04	430.00	692.81 ± 1.24
300.00	813.47 ± 1.09	370.00	754.39 ± 1.02		
310.00	805.87 ± 1.08	380.00	744.83 ± 1.01		

**2-Methyl-1-hexanol**

[624-22-6]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

67

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.583$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1054.84
<i>B</i>	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
286.15	831.3 ± 1.0	-0.34	08-zel/prz
293.15	827.0 ± 1.0	0.82	08-zel/prz
293.15	825.7 ± 1.0	-0.48	50-pic/zie
293.15	829.0 ± 2.0	2.82	54-naz/kak-1 <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
280.00	836.4 ± 1.4	293.15	826.2 ± 0.9
290.00	828.6 ± 0.9	298.15	822.3 ± 1.2

**2-Methyl-2-hexanol**

[625-23-0]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

68

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 4.8651 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.2332 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 388.25 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
<i>A</i>	$9.60129 \cdot 10^2$
<i>B</i>	$-1.73590 \cdot 10^{-1}$
<i>C</i>	$-1.10338 \cdot 10^{-3}$

cont.

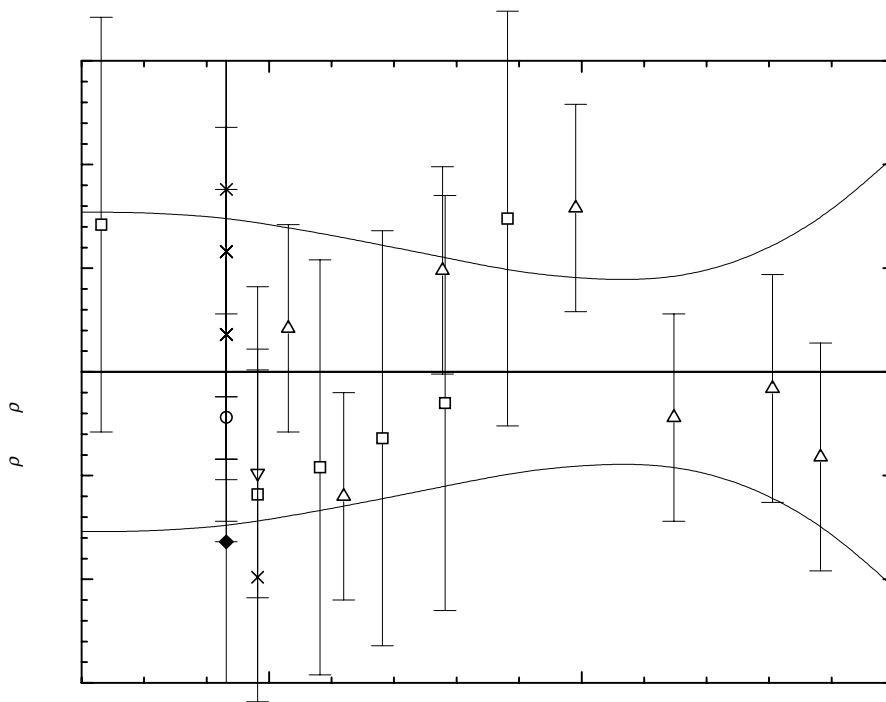


## 2-Methyl-2-hexanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
298.15	809.30 ± 1.00	-0.99	38-gin/hau(×)	293.15	814.60 ± 1.00	0.18	54-naz/kak-2(×)
293.15	814.60 ± 0.70	0.18	38-whi/ore(×)	293.15	815.00 ± 1.00	0.58	54-naz/kak-2(×)
273.15	831.10 ± 1.00	0.71	39-owe/qua(□)	293.15	815.00 ± 1.00	0.58	57-pet/sus(×)
298.15	809.70 ± 1.00	-0.59	39-owe/qua(□)	293.15	815.30 ± 1.00	0.88	59-pet/zak-1(×)
308.15	801.40 ± 1.00	-0.46	39-owe/qua(□)	303.05	806.40 ± 0.50	0.21	63-tho/mea(Δ)
318.15	792.90 ± 1.00	-0.32	39-owe/qua(□)	311.95	798.00 ± 0.50	-0.60	63-tho/mea(Δ)
328.15	784.20 ± 1.00	-0.15	39-owe/qua(□)	327.75	785.20 ± 0.50	0.49	63-tho/mea(Δ)
338.15	776.00 ± 1.00	0.74	39-owe/qua(□)	349.05	765.90 ± 0.50	0.79	63-tho/mea(Δ)
293.15	814.20 ± 0.50	-0.22	50-pic/zie(○)	364.75	749.80 ± 0.50	-0.22	63-tho/mea(Δ)
293.15	813.60 ± 0.70	-0.82	52-lev/tan(◆)	380.55	734.20 ± 0.55	-0.08	63-tho/mea(Δ)
298.15	809.80 ± 0.60	-0.49	53-sut(∇)	388.25	726.00 ± 0.55	-0.41	63-tho/mea(Δ)

**Further references:** [09-hen, 29-edg/cal, 33-whi/woo, 38-whi/joh].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	832.82 ± 0.77	310.00	800.28 ± 0.66	370.00	744.85 ± 0.48
280.00	825.02 ± 0.77	320.00	791.59 ± 0.60	380.00	734.84 ± 0.59
290.00	816.99 ± 0.75	330.00	782.69 ± 0.54	390.00	724.60 ± 0.77
293.15	814.42 ± 0.74	340.00	773.56 ± 0.48	400.00	714.15 ± 1.04
298.15	810.29 ± 0.72	350.00	764.21 ± 0.45		
300.00	808.75 ± 0.71	360.00	754.64 ± 0.44		

**2-Methyl-3-hexanol**

[617-29-8]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

69

**Table 1.** Fit with estimated *B* coefficient for 6 accepted points. Deviation  $\sigma_w = 0.661$ .

Coefficient	$\rho = A + BT$
A	1052.32
B	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
290.15	821.0 ± 6.0	-5.01	06-mus <sup>1)</sup>	284.15	830.3 ± 2.0	-0.39	48-mal/kon
293.15	825.0 ± 2.0	1.33	12-pic/ken	293.15	823.9 ± 0.6	0.23	50-pic/zie
293.15	822.0 ± 2.0	-1.67	38-whi/joh	289.15	825.8 ± 2.0	-0.99	54-naz/kak-1
293.15	822.8 ± 2.0	-0.87	43-geo				

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
280.00	833.9 ± 1.9	293.15	823.7 ± 1.5
290.00	826.1 ± 1.5	298.15	819.8 ± 1.6

**3-Methyl-1-hexanol**

[13231-81-7]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

70

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	825.8 ± 1.0	24-dew/wec	297.15	817.0 ± 5.0	41-hus/age <sup>1)</sup>
298.15	824.5 ± 2.0	27-nor/cor <sup>1)</sup>	293.15	825.8 ± 1.0	50-pic/zie
302.15	820.8 ± 2.0	31-lev/mar-5 <sup>1)</sup>	293.15	825.8 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Methyl-2-hexanol** [2313-65-7] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 71

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	822.0 ± 0.8	12-bje-0

**3-Methyl-3-hexanol** [597-96-6] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 72

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 8.4017 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 2.5702 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.09518 \cdot 10^3$
B	$-9.22352 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
296.75	819.90 ± 2.00	-1.57	19-eyk(✕)	318.15	801.60 ± 1.00	-0.13	39-owe/qua(∇)
288.15	829.60 ± 1.00	0.20	25-deg(Δ)	328.15	792.50 ± 1.00	-0.01	39-owe/qua(∇)
293.15	825.40 ± 1.00	0.61	25-deg(Δ)	338.15	783.50 ± 1.00	0.21	39-owe/qua(∇)
298.15	820.20 ± 1.00	0.02	38-gin/hau(✕)	290.15	829.40 ± 1.00	1.84	46-shi(◆)
273.15	841.50 ± 1.00	-1.74	39-owe/qua(∇)	293.15	825.40 ± 0.60	0.61	50-pic/zie(□)
298.15	819.80 ± 1.00	-0.38	39-owe/qua(∇)	293.15	825.40 ± 0.60	0.61	55-soe/fre(○)
308.15	810.70 ± 1.00	-0.26	39-owe/qua(∇)				

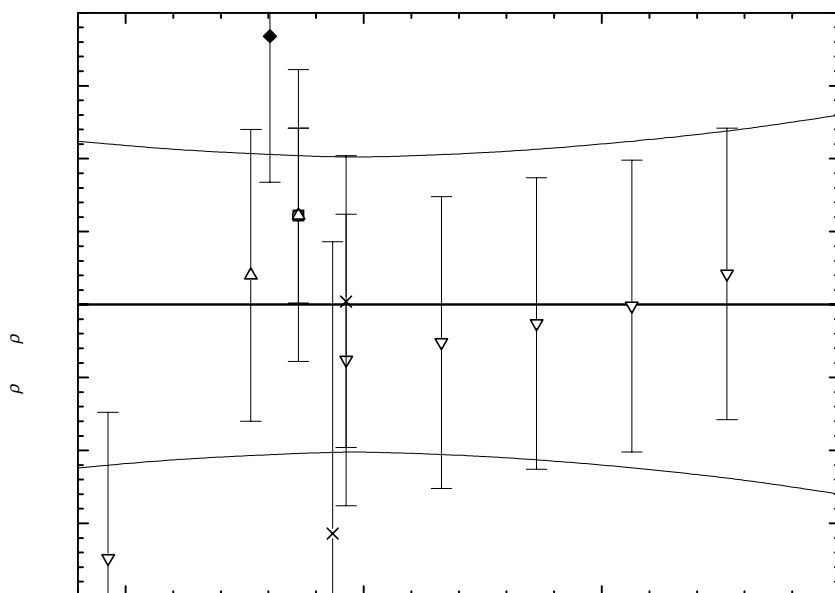
**Further references:** [07-fou/tif, 14-hal, 29-edg/cal].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	846.14 ± 1.12	298.15	820.18 ± 1.01	330.00	790.80 ± 1.13
280.00	836.92 ± 1.06	300.00	818.47 ± 1.01	340.00	781.58 ± 1.20
290.00	827.70 ± 1.03	310.00	809.25 ± 1.03	350.00	772.36 ± 1.30
293.15	824.79 ± 1.02	320.00	800.03 ± 1.07		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

#### 4-Methyl-1-hexanol

[818-49-5]

C<sub>7</sub>H<sub>16</sub>O

MW = 116.2

73

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_v = 0.104$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1052.63
<i>B</i>	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	823.9 ± 1.0	-0.07	24-dew/wec
297.15	821.0 ± 1.0	0.15	41-hus/age
293.15	823.9 ± 1.0	-0.07	50-pic/zie

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	826.4 ± 0.9
293.15	824.0 ± 0.9
298.15	820.1 ± 0.9

**4-Methyl-2-hexanol** [2313-61-3] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 74

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	817.7 ± 2.0	30-dav/dix
295.15	816.0 ± 2.0	31-lev/mar-4
293.15	810.0 ± 8.0	53-ner/hen

**5-Methyl-1-hexanol** [627-98-5] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 75

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	819.2 ± 6.0	16-lev/all <sup>1)</sup>
297.15	819.0 ± 5.0	41-hus/age <sup>1)</sup>
293.15	822.6 ± 3.0	54-naz/kak-2 <sup>1)</sup>
293.15	815.7 ± 1.0	52-coo
293.15	815.7 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**5-Methyl-2-hexanol** [627-59-8] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 76

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 1.301$ .

Coefficient	$\rho = A + BT$
$A$	1049.27
$B$	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
290.65	818.5 ± 2.0	1.75	1878-roh	293.15	814.0 ± 2.0	-0.75	38-whi/joh
290.65	817.4 ± 2.0	0.65	1878-roh	277.15	822.0 ± 4.0	-5.55	49-mal/vol <sup>1)</sup>
293.15	813.1 ± 2.0	-1.65	36-tuo				

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	817.3 ± 1.9
293.15	814.7 ± 1.9
298.15	810.7 ± 2.0

**5-Methyl-3-hexanol** [623-55-2] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 77

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	833.1 ± 1.0	57-shu/bel

**2,2,3-Trimethyl-1-butanol** [55505-23-2] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 78

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	846.6 ± 1.0	41-gle

**2,3,3-Trimethyl-1-butanol** [36794-64-6] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 79

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	823.8 ± 2.0	56-sar/new
293.15	837.2 ± 2.0	66-far/per

**2,3,3-Trimethyl-2-butanol** [594-83-2] C<sub>7</sub>H<sub>16</sub>O MW = 116.2 80

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.081$ .

Coefficient	$\rho = A + BT$
$A$	1116.79
$B$	-0.950

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
298.15	838.0 ± 3.0	4.46	38-gin/hau <sup>1)</sup>	298.15	833.5 ± 0.5	-0.03	88-sip/wie
298.15	833.5 ± 0.5	-0.03	85-wie/sip	303.15	828.9 ± 0.5	0.14	88-sip/wie
293.15	838.2 ± 0.5	-0.07	88-sip/wie	308.15	819.2 ± 2.0	-4.87	88-sip/wie <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	841.3 ± 0.5
293.15	838.3 ± 0.4
298.15	833.5 ± 0.3
310.00	822.3 ± 0.7



2.1.4 Alkanols, C<sub>8</sub>

**3,3-Dimethyl-2-ethyl-1-butanol** [66576-56-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 81

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	842.5 ± 1.0	56-sar/new

**2,2-Dimethyl-1-hexanol** [2370-13-0] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 82

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	826.5 ± 2.0	64-blo/hag
293.15	839.8 ± 2.0	65-shu/puz

**2,2-Dimethyl-3-hexanol** [4209-90-9] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 83

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.15	830.0 ± 5.0	21-ler <sup>1)</sup>
293.15	834.2 ± 2.0	44-hen/mat
293.15	834.2 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,3-Dimethyl-2-hexanol** [19550-03-9] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 84

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	831.0 ± 2.0	43-ste/gre <sup>1)</sup>
293.15	836.5 ± 1.0	41-hus/gui
293.15	836.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,3-Dimethyl-3-hexanol** [4166-46-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 85

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	837.1 ± 2.0	26-sta



**2,4-Dimethyl-2-hexanol****[42328-76-7****C<sub>8</sub>H<sub>18</sub>O****MW = 130.23****86****Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
294.15	827.0 ± 10.0	31-lev/mar-2 <sup>1)</sup>
293.15	809.9 ± 2.0	41-hus/gui <sup>1)</sup>
301.15	806.5 ± 1.0	60-tha/vas
301.15	806.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**2,5-Dimethyl-1-hexanol****[6886-16-4]****C<sub>8</sub>H<sub>18</sub>O****MW = 130.23****87****Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction): $\sigma_{c,w} = 1.3629 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 3.8771 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.26323 \cdot 10^2$
B	$-1.60894 \cdot 10^{-3}$
C	$-1.13959 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

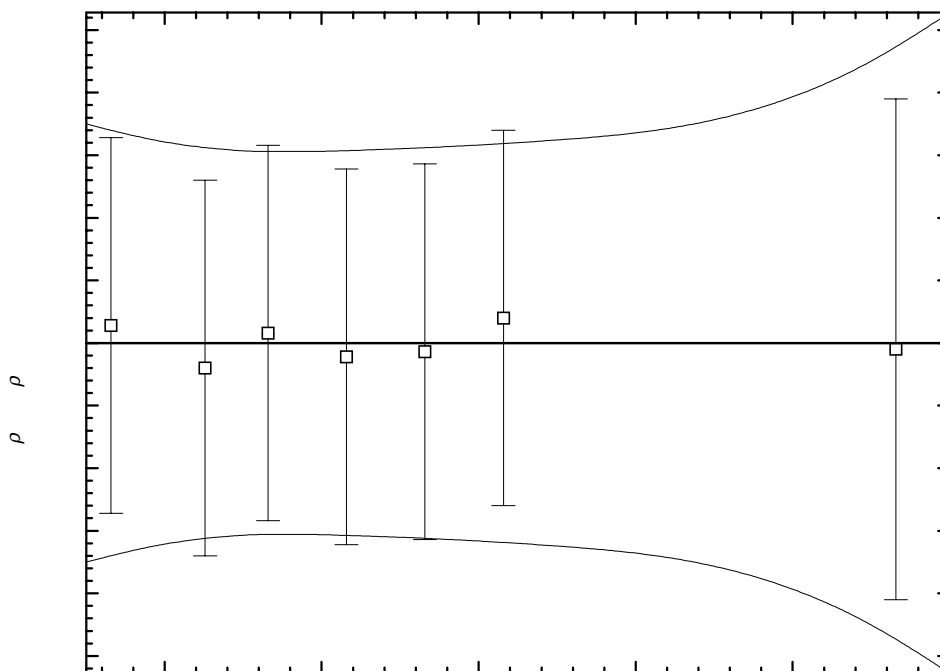
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	841.00 ± 1.50	0.14	1879-car(□)	313.15	814.00 ± 1.50	-0.07	1879-car(□)
285.15	833.00 ± 1.50	-0.20	1879-car(□)	323.15	807.00 ± 1.50	0.20	1879-car(□)
293.15	828.00 ± 1.50	0.08	1879-car(□)	373.15	767.00 ± 2.00	-0.05	1879-car(□)
303.15	821.00 ± 1.50	-0.11	1879-car(□)				

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	842.81 ± 1.75	300.00	823.28 ± 1.53	350.00	786.16 ± 1.77
280.00	836.53 ± 1.59	310.00	816.31 ± 1.55	360.00	778.05 ± 1.95
290.00	830.02 ± 1.53	320.00	809.11 ± 1.58	370.00	769.72 ± 2.23
293.15	827.92 ± 1.53	330.00	801.69 ± 1.62	380.00	761.15 ± 2.64
298.15	824.54 ± 1.53	340.00	794.04 ± 1.67		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

### 2,5-Dimethyl-2-hexanol

[3730-60-7]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

88

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_v = 0.390$ .

Coefficient	$\rho = A + BT$
$A$	1044.07
$B$	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	822.8 ± 5.0	7.39	02-kon <sup>1)</sup>
293.15	810.5 ± 3.0	-4.91	33-mey/tuo <sup>1)</sup>
293.15	815.8 ± 1.0	0.39	41-hus/gui
302.15	808.0 ± 1.0	-0.39	56-woo/vio

<sup>1)</sup> Not included in calculation of linear coefficients.

cont.

**2,5-Dimethyl-2-hexanol** (cont.)**Table 3.** Recommended values.

$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	817.9 ± 0.7
293.15	815.4 ± 0.6
298.15	811.5 ± 0.6
310.00	802.3 ± 0.9

**2,5-Dimethyl-3-hexanol**

[19550-07-3]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

89

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 8.1519 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 3.4359 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $323.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.97260 \cdot 10^2$
B	$2.17973 \cdot 10^{-1}$
C	$-1.67297 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

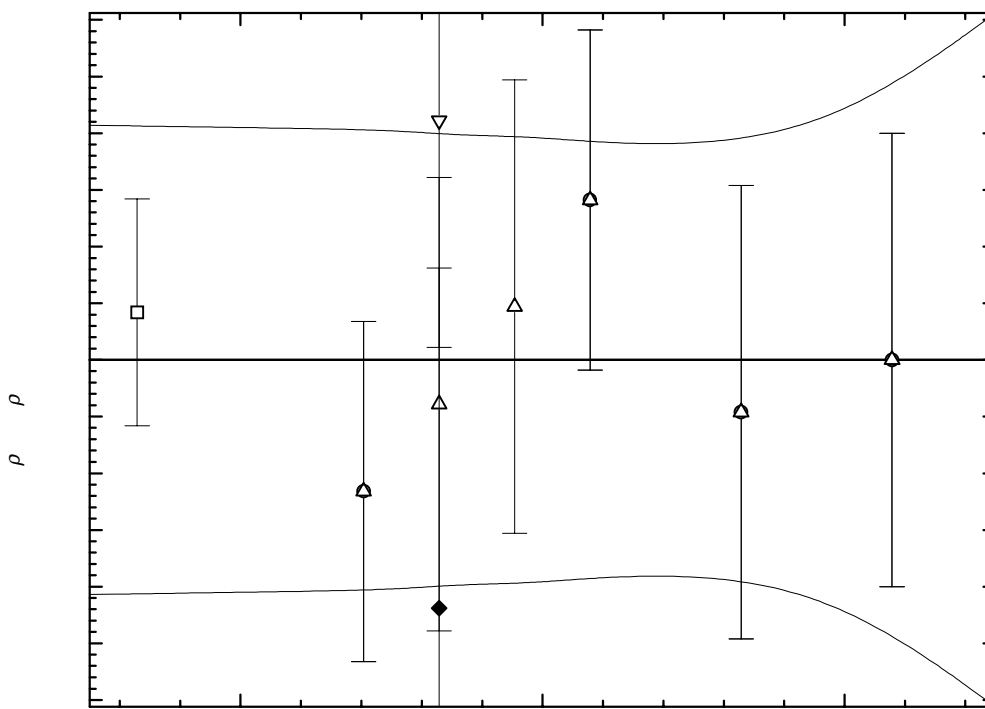
$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
288.15	820.00 ± 1.50	-1.16	1879-car(Δ)	303.15	811.00 ± 1.50	1.41	00-car-1(O)
293.15	817.00 ± 2.00	-0.39	1879-car(Δ)	313.15	801.00 ± 2.00	-0.46	00-car-1(O)
298.15	814.00 ± 2.00	0.47	1879-car(Δ)	323.15	793.00 ± 2.00	0.00	00-car-1(O)
303.15	811.00 ± 1.50	1.41	1879-car(Δ)	273.15	832.40 ± 1.00	0.42	13-fav(□)
313.15	801.00 ± 2.00	-0.46	1879-car(Δ)	293.15	822.10 ± 4.00	4.71	13-fav <sup>1)</sup>
323.15	793.00 ± 2.00	0.00	1879-car(Δ)	293.15	819.50 ± 2.00	2.11	43-geo(V)
288.15	820.00 ± 1.50	-1.16	00-car-1(O)	293.15	815.20 ± 3.00	-2.19	53-sok(◆)

<sup>1)</sup> Not included in Fig. 1.**Further references:** [12-mic, 36-tuo, 48-mal/kon].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$T$ K	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$T$ K	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	834.15 ± 2.07	293.15	817.39 ± 1.99	310.00	804.06 ± 1.86
280.00	827.13 ± 2.05	298.15	813.53 ± 1.97	320.00	795.70 ± 2.10
290.00	819.78 ± 2.03	300.00	812.08 ± 1.96	330.00	787.00 ± 3.06

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3,3-Dimethyl-1-hexanol** [10524-70-6] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 90

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	839.0 ± 2.0	64-sta-1

**3,3-Dimethyl-2-hexanol** [22025-20-3] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 91

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	845.7 ± 1.0	57-bol/ego-1
273.15	880.8 ± 10.	57-bol/ego-1 <sup>1)</sup>
293.15	845.9 ± 1.0	58-ego
293.15	845.9 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,4-Dimethyl-3-hexanol** [19550-08-4] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 92

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	834.5 ± 2.0	48-hus/goe

**3,5-Dimethyl-1-hexanol** [13501-73-0] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 93

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	828.2 ± 2.0	59-hos/nis

**3,5-Dimethyl-3-hexanol** [4209-91-0] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 94

**Table 2.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	830.0 ± 3.0	09-bod/tab <sup>1)</sup>	293.15	826.1 ± 2.0	59-pet/zak
293.15	822.8 ± 3.0	33-mey/tuo <sup>1)</sup>	293.15	826.1 ± 2.0	59-pet/zak-1
288.15	830.0 ± 3.0	50-doe/zei <sup>1)</sup>	293.15	827.2 ± 2.0	61-sok/she
298.15	827.0 ± 3.0	56-woo/vio <sup>1)</sup>	293.15	827.0 ± 2.0	Recommended
293.15	828.8 ± 2.0	58-pan/osi			

<sup>1)</sup> Not included in calculation of recommended value.

**4,4-Dimethyl-3-hexanol** [19550-09-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 95

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	834.1 ± 2.0	51-lev/fai

**5,5-Dimethyl-3-hexanol** [66576-31-6] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 96

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	833.9 ± 1.0	41-whi/whi

## 2-Ethyl-1-hexanol

[104-76-7]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

97

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 8.7629 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.8894 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.64$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.00464 \cdot 10^3$
B	$-4.24121 \cdot 10^{-1}$
C	$-5.58140 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

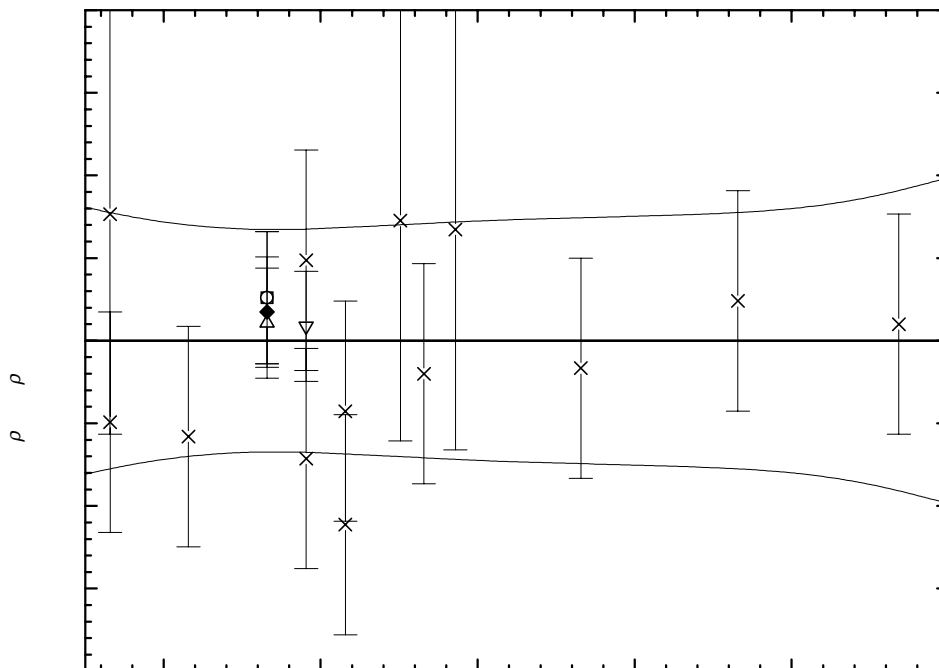
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	$848.30 \pm 2.00$	1.15	01-gue-1(✕)	293.15	$832.60 \pm 0.40$	0.26	56-ano-1(○)
273.19	$846.38 \pm 1.00$	-0.74	30-bin/dar(✕)	293.15	$832.50 \pm 0.50$	0.16	58-ano-5(Δ)
283.15	$838.93 \pm 1.00$	-0.87	30-bin/dar(✕)	293.15	$832.60 \pm 0.40$	0.26	61-dyk/sep(□)
293.15	$831.60 \pm 1.00$	-0.74	30-bin/dar <sup>1)</sup>	293.15	$832.60 \pm 0.50$	0.26	68-ano(◆)
303.15	$824.13 \pm 1.00$	-0.64	30-bin/dar(✕)	293.15	$832.10 \pm 1.00$	-0.24	85-chi/lin <sup>1)</sup>
313.15	$816.79 \pm 1.00$	-0.30	30-bin/dar(✕)	298.15	$827.50 \pm 1.00$	-1.07	85-chi/lin(✕)
333.15	$801.15 \pm 1.00$	-0.25	30-bin/dar(✕)	303.15	$823.10 \pm 1.00$	-1.67	85-chi/lin(✕)
353.15	$785.61 \pm 1.00$	0.36	30-bin/dar(✕)	308.15	$818.50 \pm 0.00$	-2.45	85-chi/lin <sup>1)</sup>
373.64	$768.40 \pm 1.00$	0.15	30-bin/dar(✕)	313.15	$812.40 \pm 0.00$	-4.69	85-chi/lin <sup>1)</sup>
298.15	$829.30 \pm 1.00$	0.73	36-lev/rot-1(✕)	318.15	$807.30 \pm 0.00$	-5.91	85-chi/lin <sup>1)</sup>
292.15	$834.20 \pm 2.00$	1.11	39-ken/pla <sup>1)</sup>	323.15	$801.80 \pm 0.00$	-7.50	85-chi/lin <sup>1)</sup>
293.15	$833.40 \pm 2.00$	1.06	39-ken/pla <sup>1)</sup>	328.15	$795.20 \pm 0.00$	-10.16	85-chi/lin <sup>1)</sup>
310.15	$820.50 \pm 2.00$	1.09	39-ken/pla(✕)	333.15	$790.70 \pm 0.00$	-10.70	85-chi/lin <sup>1)</sup>
317.15	$815.00 \pm 2.00$	1.01	39-ken/pla(✕)	298.15	$828.70 \pm 0.50$	0.13	88-cab/bar(∇)
367.15	$777.00 \pm 2.00$	3.31	39-ken/pla <sup>1)</sup>				

<sup>1)</sup> Not included in Fig. 1.**Further references:** [22-lev/tay-1, 34-von/man, 37-mas, 38-mas, 39-gol/tay, 51-hau, 58-kut/lyu, 58-lyu, 58-lyu/bel, 60-tje, 63-lyu/mer].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	$849.44 \pm 1.21$	300.00	$827.17 \pm 1.02$	350.00	$787.82 \pm 1.15$
280.00	$842.13 \pm 1.06$	310.00	$819.52 \pm 1.05$	360.00	$779.62 \pm 1.19$
290.00	$834.70 \pm 1.01$	320.00	$811.77 \pm 1.09$	370.00	$771.30 \pm 1.29$
293.15	$832.34 \pm 1.01$	330.00	$803.90 \pm 1.11$	380.00	$762.88 \pm 1.48$
298.15	$828.57 \pm 1.01$	340.00	$795.92 \pm 1.13$		

cont.

**2-Ethyl-1-hexanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3-Ethyl-1-hexanol** [41065-95-6] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 98

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
301.15	829.0 ± 3.0	31-lev/mar-3

**3-Ethyl-3-hexanol** [597-76-2] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 99

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 8.6240 \cdot 10^{-1}$  (combined temperature ranges, weighted),

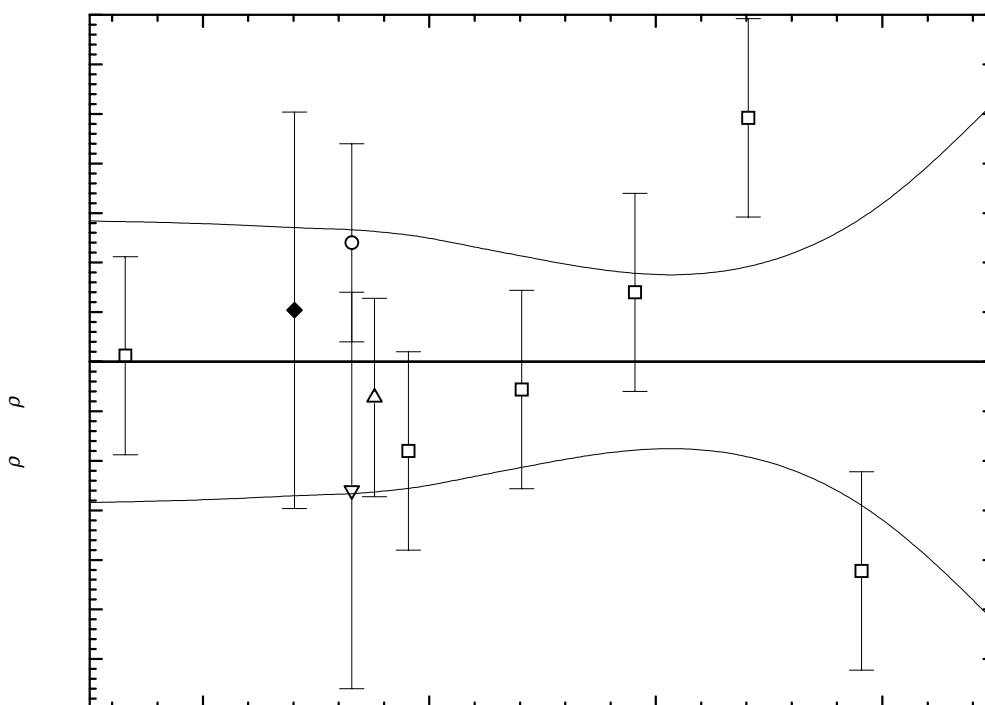
$\sigma_{c,uw} = 4.3902 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.03283 \cdot 10^2$
B	1.10512
C	$-3.35884 \cdot 10^{-3}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
295.15	836.50 ± 1.00	-0.36	14-hal(Δ)	308.15	824.60 ± 1.00	-0.28	39-owe/qua(□)
288.10	843.40 ± 2.00	0.52	19-eyk(◆)	318.15	815.60 ± 1.00	0.70	39-owe/qua(□)
293.15	837.30 ± 2.00	-1.30	22-bae(∇)	328.15	806.70 ± 1.00	2.46	39-owe/qua(□)
273.15	854.60 ± 1.00	0.06	39-owe/qua(□)	338.15	790.80 ± 1.00	-2.11	39-owe/qua(□)
298.15	833.30 ± 1.00	-0.90	39-owe/qua(□)	293.15	839.80 ± 1.00	1.20	55-ano(○)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	856.81 ± 1.42	298.15	834.20 ± 1.28	330.00	802.19 ± 0.94
280.00	849.38 ± 1.40	300.00	832.52 ± 1.25	340.00	790.74 ± 1.50
290.00	841.29 ± 1.34	310.00	823.09 ± 1.02	350.00	778.62 ± 2.63
293.15	838.60 ± 1.34	320.00	812.98 ± 0.83		



**4-Ethyl-3-hexanol** [19780-44-0] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 100

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	835.0 ± 3.0	07-fou/tif

**2-Ethyl-4-methyl-1-pentanol** [106-67-2] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 101

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	830.0 ± 2.0	58-ano-3
293.15	827.3 ± 0.6	61-dyk/sep

**3-Ethyl-2-methyl-2-pentanol** [19780-63-3] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 102

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.150$ .

Coefficient	$\rho = A + BT$
$A$	1067.01
$B$	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	838.2 ± 1.0	-0.15	41-hus/gui
298.15	834.6 ± 1.	0.15	54-ski/flo

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	840.8 ± 0.9
293.15	838.4 ± 0.9
298.15	834.5 ± 0.9

**3-Ethyl-2-methyl-3-pentanol** [597-05-7] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 103

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.200$ .

Coefficient	$\rho = A + BT$
$A$	1070.08
$B$	-0.820

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
273.15	846.3 ± 2.0	0.20	1891-gri/paw
293.15	829.5 ± 2.0	-0.20	1891-gri/paw

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	848.7 ± 2.2
280.00	840.5 ± 1.8
290.00	832.3 ± 1.9
293.15	829.7 ± 2.1
298.15	825.6 ± 2.3

**3-Ethyl-3-methyl-2-pentanol** [66576-22-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 104

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	857.6 ± 1.0	57-bol/ego
293.15	857.6 ± 1.0	58-ego

**2-Methyl-1-heptanol** [60435-70-3] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 105

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 2.1063 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 9.7608 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 372.82 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.49326 \cdot 10^2$
B	$-2.66559 \cdot 10^{-1}$
C	$-8.01222 \cdot 10^{-4}$

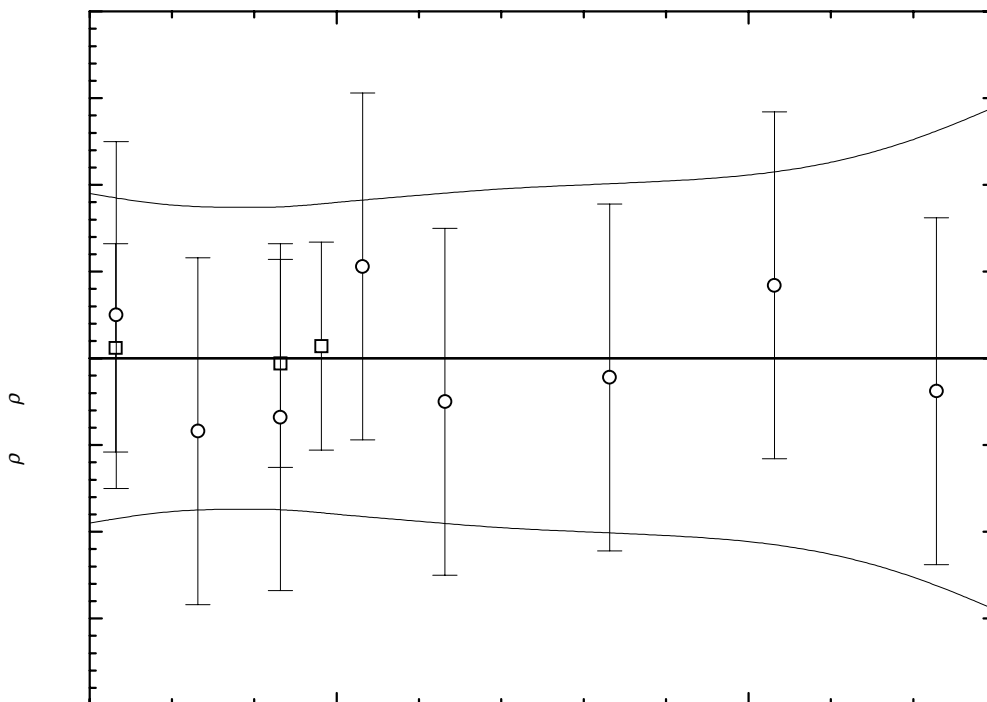
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.23	816.93 ± 1.00	0.25	30-bin/dar(○)	353.15	755.69 ± 1.00	0.42	30-bin/dar(○)
283.15	809.19 ± 1.00	-0.42	30-bin/dar(○)	372.82	738.39 ± 1.00	-0.19	30-bin/dar(○)
293.15	801.99 ± 1.00	-0.34	30-bin/dar(○)	273.15	816.80 ± 0.60	0.06	41-dor/gla(□)
303.15	795.42 ± 1.00	0.53	30-bin/dar(○)	293.15	802.30 ± 0.60	-0.03	41-dor/gla(□)
313.15	787.03 ± 1.00	-0.25	30-bin/dar(○)	298.15	798.70 ± 0.60	0.07	41-dor/gla(□)
333.15	771.49 ± 1.00	-0.11	30-bin/dar(○)				

<sup>1)</sup> Not included in Fig. 1.

cont.

## 2-Methyl-1-heptanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	818.95 ± 0.95	300.00	797.25 ± 0.90	350.00	757.88 ± 1.05
280.00	811.87 ± 0.87	310.00	789.70 ± 0.94	360.00	749.53 ± 1.12
290.00	804.64 ± 0.87	320.00	781.98 ± 0.98	370.00	741.01 ± 1.25
293.15	802.33 ± 0.87	330.00	774.11 ± 1.00	380.00	732.34 ± 1.45
298.15	798.63 ± 0.89	340.00	766.07 ± 1.02		

## 2-Methyl-2-heptanol

[625-25-2]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

106

**Table 1.** Coefficients of the polynomial expansion equation.

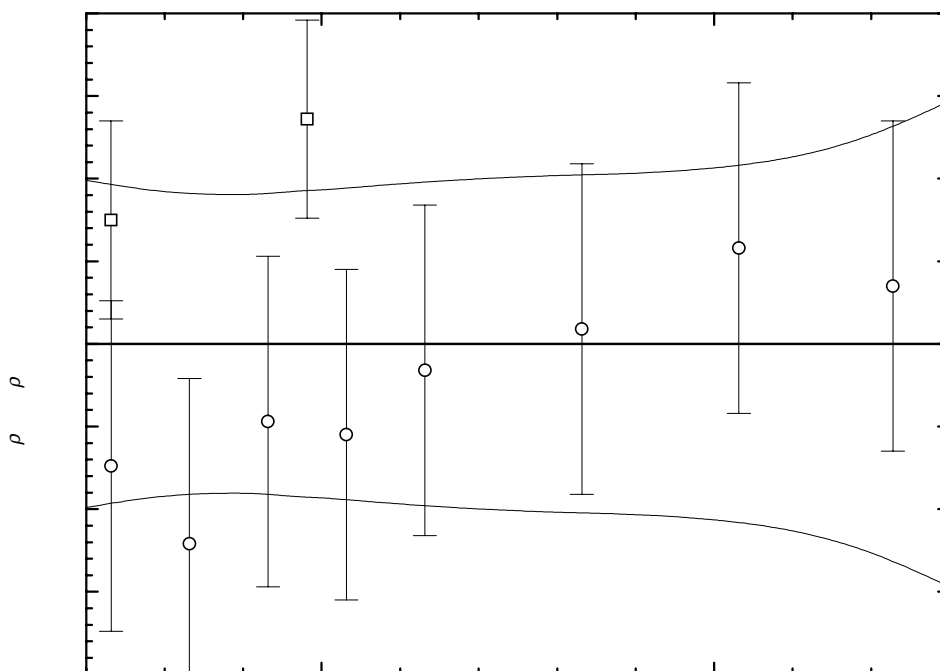
Standard deviations (see introduction):

 $\sigma_{c,w} = 7.1719 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.6066 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $372.77$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.54283 \cdot 10^2$
B	$-1.78842 \cdot 10^{-1}$
C	$-1.09478 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.19	$822.98 \pm 1.00$	-0.74	30-bin/dar(O)	333.15	$773.28 \pm 1.00$	0.09	30-bin/dar(O)
283.15	$814.66 \pm 1.00$	-1.21	30-bin/dar(O)	353.15	$755.17 \pm 1.00$	0.58	30-bin/dar(O)
293.15	$807.30 \pm 1.00$	-0.47	30-bin/dar(O)	372.77	$735.84 \pm 1.00$	0.35	30-bin/dar(O)
303.15	$798.91 \pm 1.00$	-0.55	30-bin/dar(O)	273.15	$824.50 \pm 0.60$	0.75	41-dor/gla(□)
313.15	$790.76 \pm 1.00$	-0.16	30-bin/dar(O)	298.15	$805.00 \pm 0.60$	1.36	41-dor/gla(□)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**2-Methyl-2-heptanol** (cont.)**Further references:** [06-mus, 33-whi/wil, 41-hus/gui, 44-qua/sma, 57-col/fal].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	826.19 ± 0.99	300.00	802.10 ± 0.93	350.00	757.58 ± 1.06
280.00	818.38 ± 0.91	310.00	793.63 ± 0.97	360.00	748.02 ± 1.12
290.00	810.35 ± 0.90	320.00	784.95 ± 1.00	370.00	738.24 ± 1.25
293.15	807.77 ± 0.91	330.00	776.04 ± 1.02	380.00	728.24 ± 1.47
298.15	803.64 ± 0.93	340.00	766.92 ± 1.03		

**2-Methyl-3-heptanol****[18720-62-2]****C<sub>8</sub>H<sub>18</sub>O****MW = 130.23****107****Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction): $\sigma_{c,w} = 2.3940 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.0583 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.52$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.51750 \cdot 10^2$
B	$-8.19206 \cdot 10^{-2}$
C	$-1.19870 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	825.00 ± 1.00	0.28	06-mus(X)	333.15	791.26 ± 1.00	-0.16	30-bin/dar(◆)
293.15	823.50 ± 1.00	-1.22	12-pic/ken(Δ)	353.15	773.57 ± 1.00	0.25	30-bin/dar(◆)
298.15	821.00 ± 1.00	0.23	13-tho(X)	373.52	753.98 ± 1.00	0.07	30-bin/dar(◆)
273.21	840.19 ± 1.00	0.30	30-bin/dar(◆)	273.15	840.00 ± 0.60	0.06	41-dor/gla(□)
283.15	832.09 ± 1.00	-0.36	30-bin/dar(◆)	298.15	821.00 ± 0.60	0.23	41-dor/gla(□)
293.15	824.67 ± 1.00	-0.05	30-bin/dar(◆)	293.15	825.10 ± 1.00	0.38	43-geo(∇)
303.15	816.66 ± 1.00	-0.10	30-bin/dar(◆)	284.15	831.60 ± 1.00	-0.09	48-mal/kon(O)
313.15	808.73 ± 1.00	0.18	30-bin/dar(◆)				

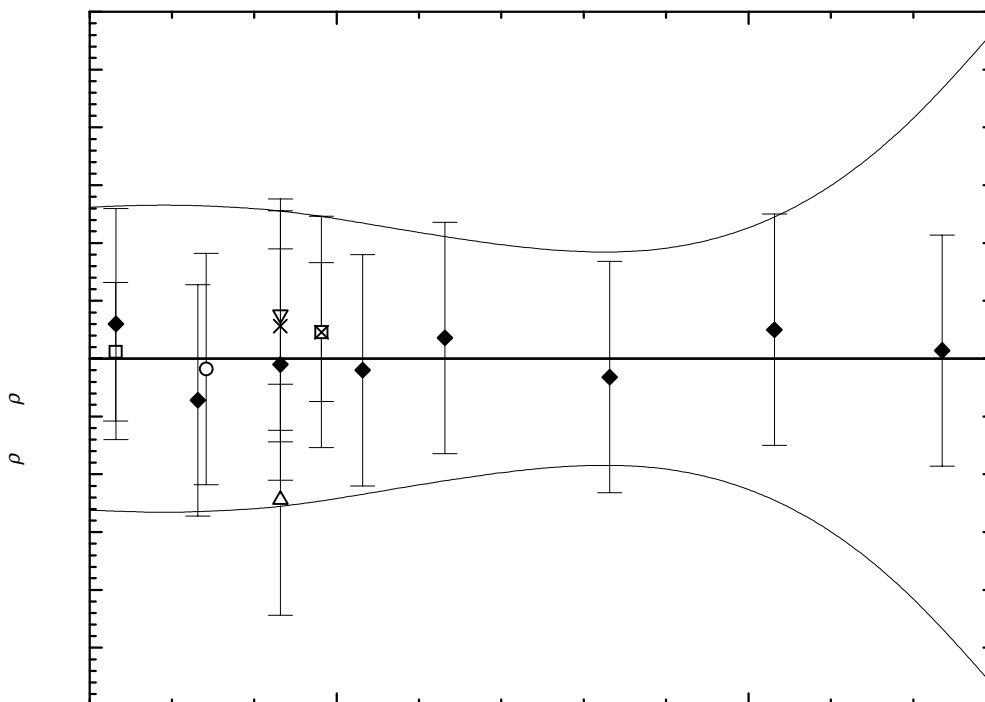
**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	842.25 ± 1.31	300.00	819.29 ± 1.21	350.00	776.24 ± 1.10
280.00	834.83 ± 1.34	310.00	811.16 ± 1.09	360.00	766.91 ± 1.46
290.00	827.18 ± 1.30	320.00	802.79 ± 0.98	370.00	757.34 ± 2.04
293.15	824.72 ± 1.28	330.00	794.18 ± 0.91	380.00	747.53 ± 2.85
298.15	820.77 ± 1.23	340.00	785.33 ± 0.93		

cont.

Further references: [14-wal-1, 33-bri, 36-tuo].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

### 2-Methyl-4-heptanol

[21570-35-4]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

108

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 1.1397 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 5.7770 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.54$ K
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.33558 \cdot 10^2$
B	$-7.11104 \cdot 10^{-2}$
C	$-1.15359 \cdot 10^{-3}$

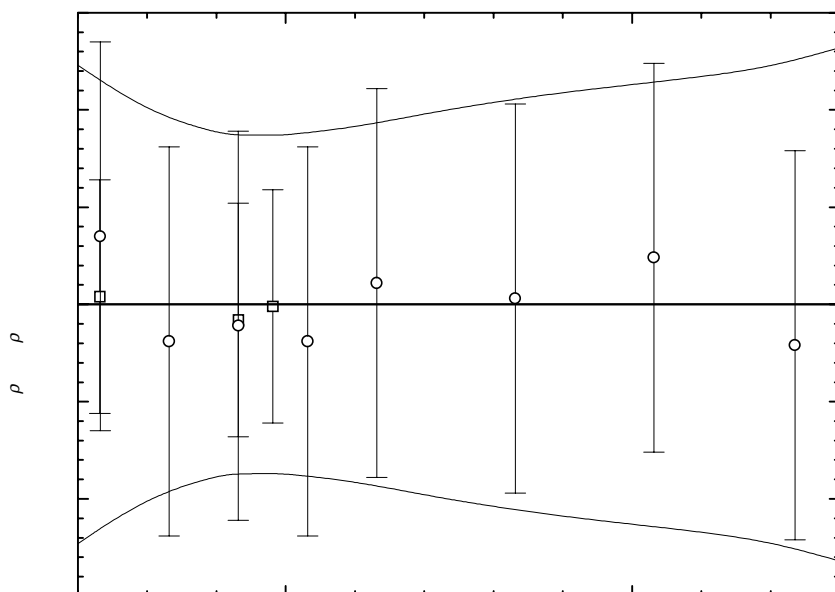
cont.

## 2-Methyl-4-heptanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.23	828.36 ± 1.00	0.35	30-bin/dar(O)	353.15	764.82 ± 1.00	0.24	30-bin/dar(O)
283.15	820.75 ± 1.00	-0.19	30-bin/dar(O)	373.54	745.82 ± 1.00	-0.21	30-bin/dar(O)
293.15	813.47 ± 1.00	-0.11	30-bin/dar(O)	273.15	828.10 ± 0.60	0.04	41-dor/gla(□)
303.15	805.80 ± 1.00	-0.19	30-bin/dar(O)	293.15	813.50 ± 0.60	-0.08	41-dor/gla(□)
313.15	798.28 ± 1.00	0.11	30-bin/dar(O)	298.15	809.80 ± 0.60	-0.01	41-dor/gla(□)
333.15	781.86 ± 1.00	0.03	30-bin/dar(O)				

**Further references:** [06-mus, 36-tuo, 57-shu/bel].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	830.26 ± 1.23	300.00	808.40 ± 0.87	350.00	767.35 ± 1.13
280.00	823.21 ± 0.99	310.00	800.65 ± 0.91	360.00	758.45 ± 1.17
290.00	815.92 ± 0.88	320.00	792.68 ± 0.98	370.00	749.32 ± 1.22
293.15	813.58 ± 0.87	330.00	784.47 ± 1.04	380.00	739.96 ± 1.32
298.15	809.81 ± 0.87	340.00	776.03 ± 1.09		

## 3-Methyl-1-heptanol

[1070-32-2]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

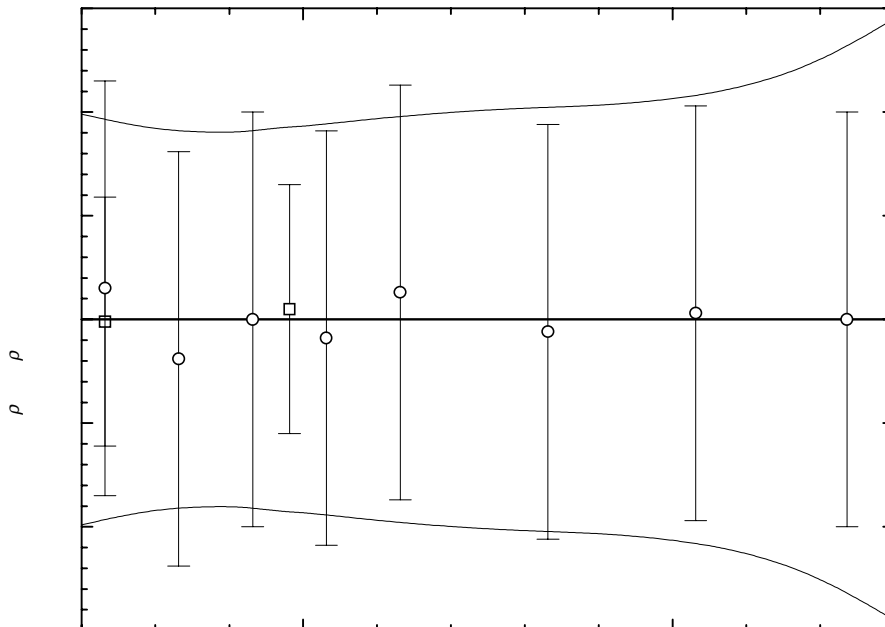
109

**Table 1.** Coefficients of the polynomial expansion equation.  
Standard deviations (see introduction): $\sigma_{c,w} = 7.0802 \cdot 10^{-2}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 3.3702 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.62$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.62326 \cdot 10^2$
B	$-4.50758 \cdot 10^{-1}$
C	$-4.89103 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.19	$802.83 \pm 1.00$	0.15	30-bin/dar(○)	333.15	$757.81 \pm 1.00$	-0.06	30-bin/dar(○)
283.15	$795.29 \pm 1.00$	-0.19	30-bin/dar(○)	353.15	$742.17 \pm 1.00$	0.03	30-bin/dar(○)
293.15	$788.15 \pm 1.00$	-0.00	30-bin/dar(○)	373.62	$725.64 \pm 1.00$	0.00	30-bin/dar(○)
303.15	$780.64 \pm 1.00$	-0.09	30-bin/dar(○)	273.15	$802.70 \pm 0.60$	-0.01	41-dor/gla(□)
313.15	$773.34 \pm 1.00$	0.13	30-bin/dar(○)	298.15	$784.50 \pm 0.60$	0.05	41-dor/gla(□)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.



**3-Methyl-1-heptanol** (cont.)**Further references:** [31-lev/mar-5, 33-bri, 41-hus/age, 56-lic/dur].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	804.97 ± 0.99	300.00	783.08 ± 0.93	350.00	744.65 ± 1.06
280.00	797.77 ± 0.91	310.00	775.59 ± 0.97	360.00	736.67 ± 1.12
290.00	790.47 ± 0.90	320.00	768.00 ± 1.00	370.00	728.59 ± 1.24
293.15	788.15 ± 0.91	330.00	760.31 ± 1.02	380.00	720.41 ± 1.45
298.15	784.45 ± 0.93	340.00	752.53 ± 1.03		

**3-Methyl-2-heptanol****[31367-46-1]****C<sub>8</sub>H<sub>18</sub>O****MW = 130.23****110****Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.094$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1056.15
<i>B</i>	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
286.15	827.2 ± 2.00	-0.03	24-pow <sup>1)</sup>	303.15	781.5 ± 10.00	-32.14	30-bin/dar <sup>1)</sup>
273.15	837.5 ± 1.00	-0.13	41-dor/gla	313.15	773.7 ± 10.00	-31.88	30-bin/dar <sup>1)</sup>
298.15	817.7 ± 1.00	0.07	41-dor/gla	333.15	756.0 ± 10.00	-33.60	30-bin/dar <sup>1)</sup>
293.15	821.7 ± 1.00	0.07	41-dor/gla	353.15	738.4 ± 10.00	-35.19	30-bin/dar <sup>1)</sup>
283.15	797.6 ± 10.00	-32.05	30-bin/dar <sup>1)</sup>	373.44	723.5 ± 10.00	-33.92	30-bin/dar <sup>1)</sup>
293.15	790.0 ± 10.00	-31.62	30-bin/dar <sup>1)</sup>	273.20	806.3 ± 10.00	-31.27	30-bin/dar <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	840.2 ± 0.9
280.00	832.2 ± 0.5
290.00	824.2 ± 0.3
293.15	821.6 ± 0.3
298.15	817.6 ± 0.6

## 3-Methyl-3-heptanol

[5582-82-1]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

111

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 9.7126 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.4649 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.54$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.00165 \cdot 10^3$
B	$-3.47181 \cdot 10^{-1}$
C	$-8.23886 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.23	$845.31 \pm 1.00$	0.03	30-bin/dar( $\Delta$ )	293.15	$828.20 \pm 2.00$	-0.87	33-whi/woo( $\times$ )
283.15	$837.17 \pm 1.00$	-0.12	30-bin/dar( $\Delta$ )	298.15	$824.90 \pm 2.00$	0.00	33-whi/woo( $\times$ )
293.15	$829.19 \pm 1.00$	0.12	30-bin/dar( $\Delta$ )	273.15	$847.10 \pm 1.00$	1.75	41-dor/gla( $\nabla$ )
303.15	$821.02 \pm 1.00$	0.33	30-bin/dar( $\Delta$ )	298.15	$827.10 \pm 1.00$	2.20	41-dor/gla( $\nabla$ )
313.15	$812.61 \pm 1.00$	0.47	30-bin/dar( $\Delta$ )	298.15	$825.20 \pm 1.00$	0.30	44-qua/sma( $\circ$ )
333.15	$794.47 \pm 1.00$	-0.07	30-bin/dar( $\Delta$ )	318.15	$808.30 \pm 1.00$	0.50	44-qua/sma( $\circ$ )
353.15	$776.10 \pm 1.00$	-0.19	30-bin/dar( $\Delta$ )	328.15	$799.90 \pm 1.00$	0.90	44-qua/sma( $\circ$ )
373.54	$757.17 \pm 1.00$	0.17	30-bin/dar( $\Delta$ )	298.15	$823.00 \pm 2.00$	-1.90	61-wib/fos( $\times$ )
273.15	$844.60 \pm 2.00$	-0.75	30-van( $\blacklozenge$ )	293.15	$826.90 \pm 1.00$	-2.17	66-are/tav( $\square$ )
288.15	$832.50 \pm 2.00$	-0.70	30-van( $\blacklozenge$ )				

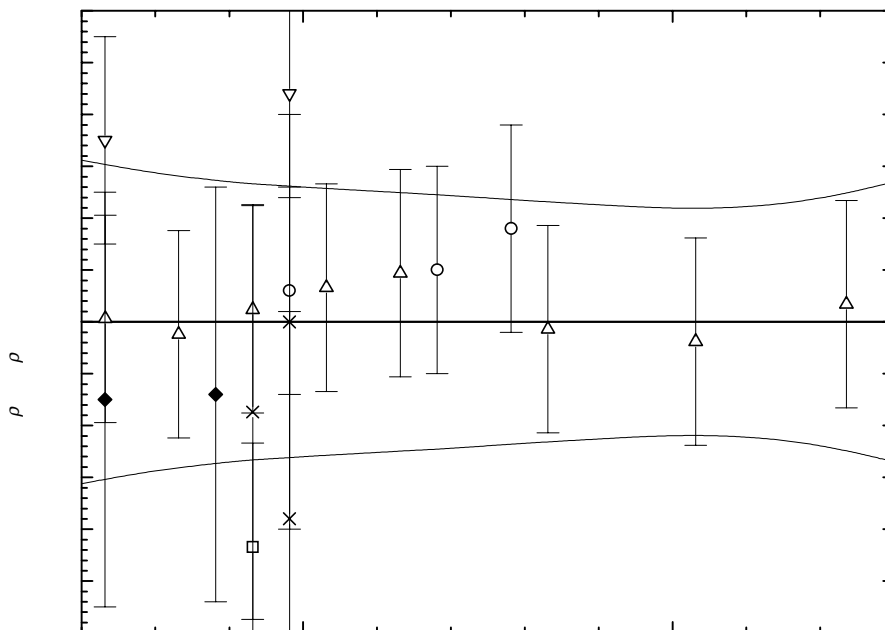
**Further references:** [02-kon, 65-col/des].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	$847.85 \pm 1.56$	300.00	$823.35 \pm 1.30$	350.00	$779.21 \pm 1.09$
280.00	$839.85 \pm 1.43$	310.00	$814.85 \pm 1.26$	360.00	$769.89 \pm 1.10$
290.00	$831.68 \pm 1.35$	320.00	$806.19 \pm 1.22$	370.00	$760.40 \pm 1.18$
293.15	$829.07 \pm 1.33$	330.00	$797.36 \pm 1.17$	380.00	$750.75 \pm 1.35$
298.15	$824.90 \pm 1.31$	340.00	$788.37 \pm 1.13$		

cont.

## 3-Methyl-3-heptanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

## 3-Methyl-4-heptanol

[1838-73-9]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

112

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 5.5178 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 2.7388 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

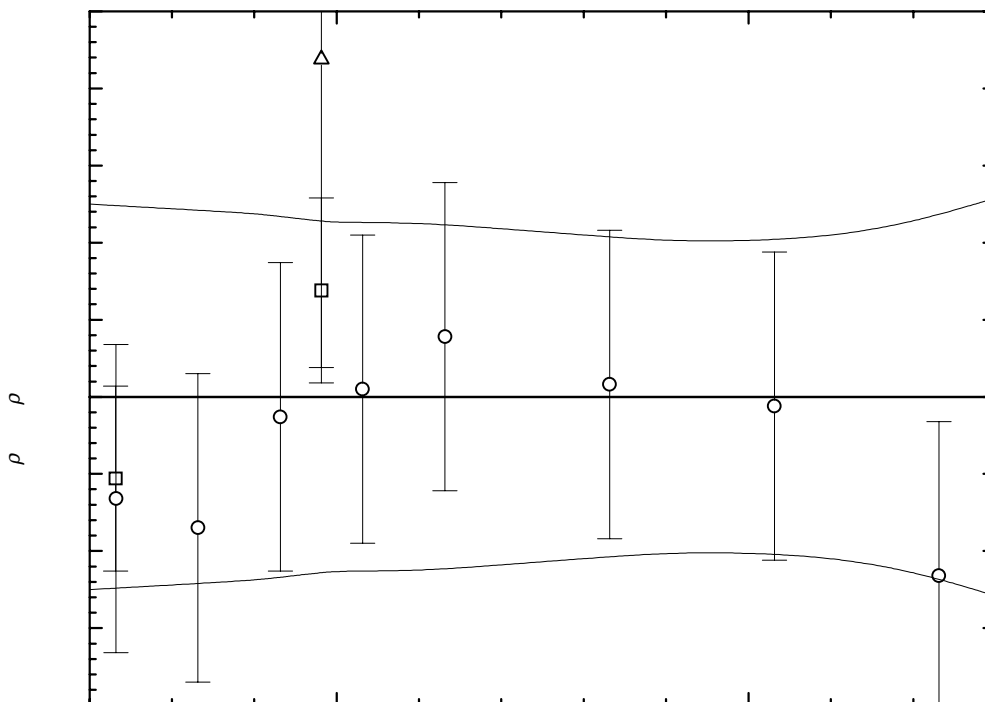
Coefficient	$T = 273.15$ to $373.12$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.08833 \cdot 10^3$
B	$-8.57031 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.20	$853.53 \pm 1.00$	-0.66	30-bin/dar(O)	353.15	$785.61 \pm 1.00$	-0.06	30-bin/dar(O)
283.15	$844.81 \pm 1.00$	-0.85	30-bin/dar(O)	373.12	$767.40 \pm 1.00$	-1.16	30-bin/dar(O)
293.15	$836.96 \pm 1.00$	-0.13	30-bin/dar(O)	273.15	$853.70 \pm 0.60$	-0.53	41-dor/gla(□)
303.15	$828.57 \pm 1.00$	0.05	30-bin/dar(O)	298.15	$833.50 \pm 0.60$	0.69	41-dor/gla(□)
313.15	$820.34 \pm 1.00$	0.39	30-bin/dar(O)	298.15	$835.00 \pm 2.00$	2.19	65-col/des(Δ)
333.15	$802.89 \pm 1.00$	0.08	30-bin/dar(O)				

cont.

Further references: [33-bri].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	856.93 ± 1.25	300.00	831.22 ± 1.13	350.00	788.37 ± 1.01
280.00	848.36 ± 1.22	310.00	822.65 ± 1.13	360.00	779.80 ± 1.04
290.00	839.79 ± 1.19	320.00	814.08 ± 1.09	370.00	771.23 ± 1.13
293.15	837.09 ± 1.17	330.00	805.51 ± 1.05	380.00	762.66 ± 1.29
298.15	832.81 ± 1.14	340.00	796.94 ± 1.01		

## 4-Methyl-1-heptanol

[817-91-4]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

113

**Table 1.** Coefficients of the polynomial expansion equation.

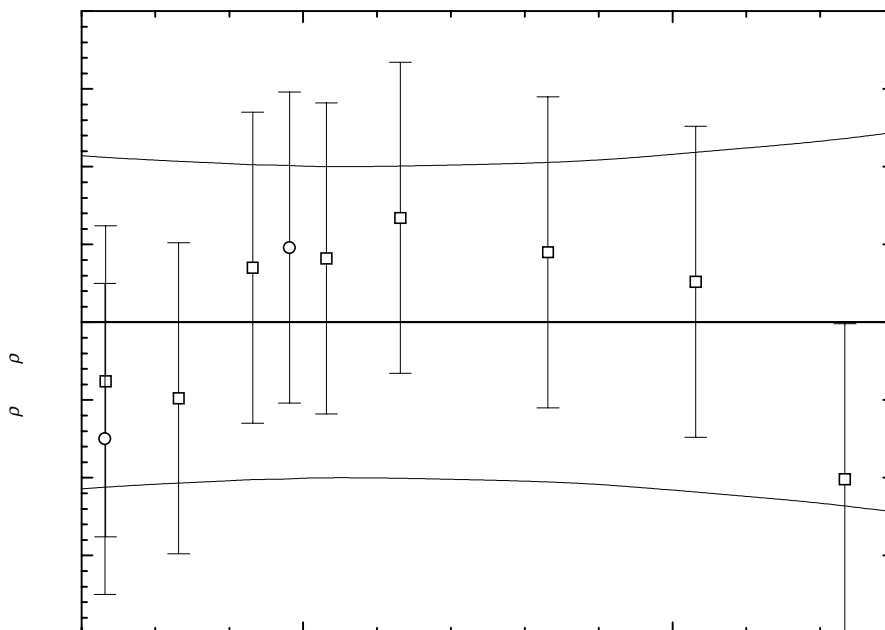
Standard deviations (see introduction):

 $\sigma_{c,w} = 5.6667 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.8889 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.35$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.03650 \cdot 10^3$
B	$-7.73026 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.27	$824.88 \pm 1.00$	-0.38	30-bin/dar(□)	333.15	$779.42 \pm 1.00$	0.45	30-bin/dar(□)
283.15	$817.13 \pm 1.00$	-0.49	30-bin/dar(□)	353.15	$763.77 \pm 1.00$	0.26	30-bin/dar(□)
293.15	$810.24 \pm 1.00$	0.35	30-bin/dar(□)	373.35	$746.88 \pm 1.00$	-1.01	30-bin/dar(□)
303.15	$802.57 \pm 1.00$	0.41	30-bin/dar(□)	273.15	$824.60 \pm 1.00$	-0.75	41-dor/gla(O)
313.15	$795.10 \pm 1.00$	0.67	30-bin/dar(□)	298.15	$806.50 \pm 1.00$	0.48	41-dor/gla(O)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	827.78 ± 1.07	300.00	804.59 ± 1.00	350.00	765.94 ± 1.08
280.00	820.05 ± 1.04	310.00	796.86 ± 1.00	360.00	758.21 ± 1.12
290.00	812.32 ± 1.02	320.00	789.13 ± 1.01	370.00	750.48 ± 1.16
293.15	809.89 ± 1.01	330.00	781.40 ± 1.02	380.00	742.75 ± 1.22
298.15	806.02 ± 1.01	340.00	773.67 ± 1.04		

**4-Methyl-2-heptanol** [56298-90-9] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 114

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 1.0278 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 5.1187 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 373.13 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.32872 \cdot 10^2$
B	$-1.40659 \cdot 10^{-1}$
C	$-1.03498 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.20	817.33 ± 1.00	0.13	30-bin/dar(O)	333.15	771.31 ± 1.00	0.17	30-bin/dar(O)
283.15	809.78 ± 1.00	-0.29	30-bin/dar(O)	353.15	755.23 ± 1.00	1.11	30-bin/dar <sup>1)</sup>
293.15	802.57 ± 1.00	-0.13	30-bin/dar(O)	373.13	736.27 ± 1.00	-0.02	30-bin/dar(O)
303.15	795.04 ± 1.00	-0.08	30-bin/dar(O)	273.15	817.30 ± 0.60	0.07	41-dor/gla(□)
313.15	787.40 ± 1.00	0.07	30-bin/dar(O)	298.15	799.00 ± 0.60	0.07	41-dor/gla(□)

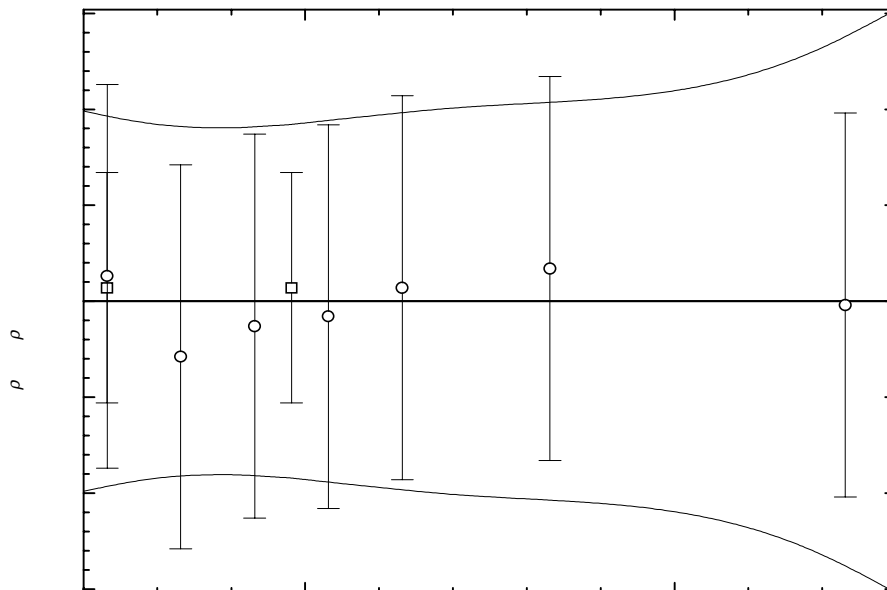
<sup>1)</sup> Not included in Fig. 1.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	819.44 ± 0.99	300.00	797.53 ± 0.93	350.00	756.86 ± 1.09
280.00	812.35 ± 0.91	310.00	789.81 ± 0.97	360.00	748.10 ± 1.17
290.00	805.04 ± 0.90	320.00	781.88 ± 1.01	370.00	739.14 ± 1.31
293.15	802.70 ± 0.91	330.00	773.75 ± 1.03	380.00	729.97 ± 1.52
298.15	798.93 ± 0.92	340.00	765.40 ± 1.05		

cont.

## 4-Methyl-2-heptanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

## 4-Methyl-3-heptanol

[14979-39-6]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

115

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 2.8281 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.0734 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

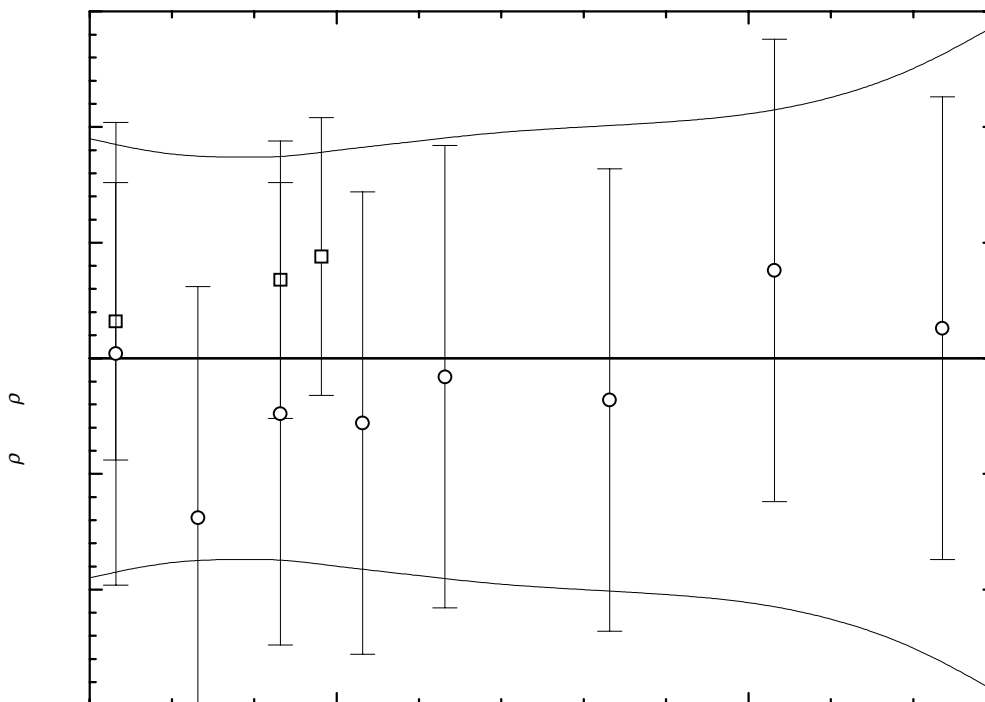
Coefficient	$T = 273.15$ to $373.56$ K
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.85558 \cdot 10^2$
B	$-4.61789 \cdot 10^{-1}$
C	$-6.04236 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.18	$814.33 \pm 1.00$	0.02	30-bin/dar(O)	353.15	$747.50 \pm 1.00$	0.38	30-bin/dar(O)
283.15	$805.67 \pm 1.00$	-0.69	30-bin/dar(O)	373.56	$728.86 \pm 1.00$	0.13	30-bin/dar(O)
293.15	$798.02 \pm 1.00$	-0.24	30-bin/dar(O)	273.15	$814.50 \pm 0.60$	0.16	41-dor/gla(□)
303.15	$789.76 \pm 1.00$	-0.28	30-bin/dar(O)	293.15	$798.60 \pm 0.60$	0.34	41-dor/gla(□)
313.15	$781.62 \pm 1.00$	-0.08	30-bin/dar(O)	298.15	$794.60 \pm 0.60$	0.44	41-dor/gla(□)
333.15	$764.47 \pm 1.00$	-0.18	30-bin/dar(O)				

cont.

Further references: [12-bje].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	816.83 ± 0.95	300.00	792.64 ± 0.90	350.00	749.91 ± 1.05
280.00	808.89 ± 0.87	310.00	784.34 ± 0.94	360.00	741.01 ± 1.12
290.00	800.82 ± 0.87	320.00	775.91 ± 0.98	370.00	731.98 ± 1.24
293.15	798.26 ± 0.87	330.00	767.37 ± 1.00	380.00	722.83 ± 1.44
298.15	794.16 ± 0.89	340.00	758.70 ± 1.02		



## 4-Methyl-4-heptanol

[598-01-6]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

116

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 5.8580 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.7570 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.42$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.96959 \cdot 10^2$
B	$-3.50068 \cdot 10^{-1}$
C	$-8.24303 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

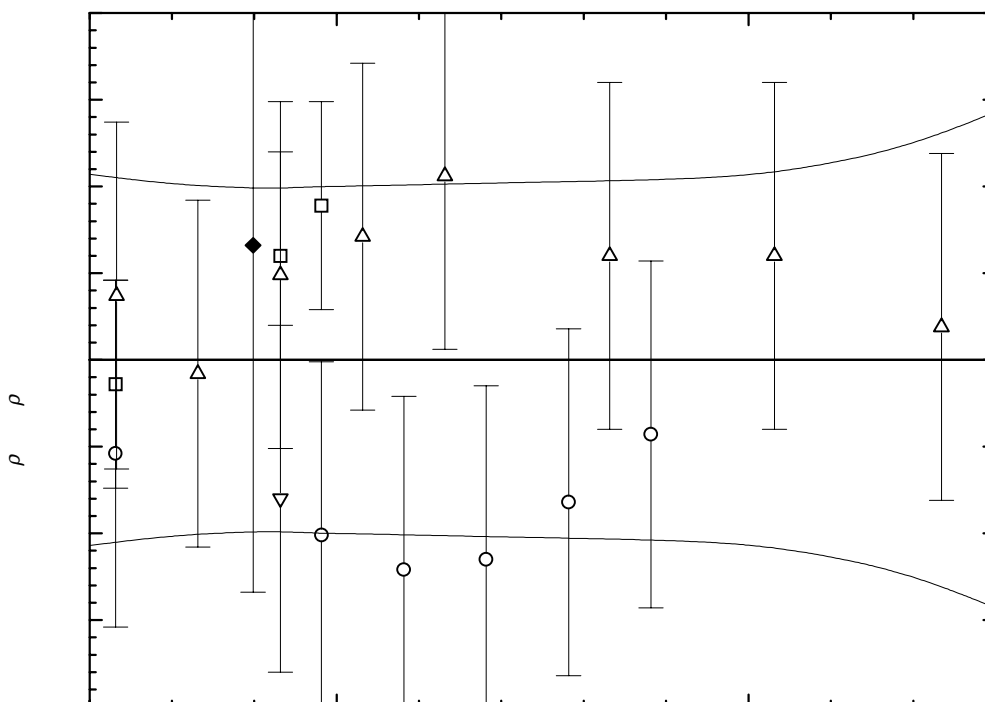
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
289.85	$826.90 \pm 2.00$	0.66	19-eyk(◆)	298.15	$818.30 \pm 1.00$	-1.01	39-owe/qua(○)
273.26	$840.12 \pm 1.00$	0.37	30-bin/dar(Δ)	308.15	$809.60 \pm 1.00$	-1.21	39-owe/qua(○)
283.15	$831.67 \pm 1.00$	-0.08	30-bin/dar(Δ)	318.15	$801.00 \pm 1.00$	-1.15	39-owe/qua(○)
293.15	$823.99 \pm 1.00$	0.49	30-bin/dar(Δ)	328.15	$792.50 \pm 1.00$	-0.82	39-owe/qua(○)
303.15	$815.79 \pm 1.00$	0.71	30-bin/dar(Δ)	338.15	$783.90 \pm 1.00$	-0.43	39-owe/qua(○)
313.15	$807.56 \pm 1.00$	1.06	30-bin/dar(Δ)	273.15	$839.70 \pm 0.60$	-0.14	41-dor/gla(□)
333.15	$789.45 \pm 1.00$	0.60	30-bin/dar(Δ)	293.15	$824.10 \pm 0.60$	0.60	41-dor/gla(□)
353.15	$771.13 \pm 1.00$	0.60	30-bin/dar(Δ)	298.15	$820.20 \pm 0.60$	0.89	41-dor/gla(□)
373.42	$751.48 \pm 1.00$	0.19	30-bin/dar(Δ)	293.15	$822.70 \pm 1.00$	-0.80	59-yur/bel(∇)
273.15	$839.30 \pm 1.00$	-0.54	39-owe/qua(○)				

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	$842.35 \pm 1.07$	300.00	$817.75 \pm 1.00$	350.00	$773.46 \pm 1.06$
280.00	$834.31 \pm 1.01$	310.00	$809.22 \pm 1.01$	360.00	$764.10 \pm 1.13$
290.00	$826.12 \pm 0.99$	320.00	$800.53 \pm 1.02$	370.00	$754.59 \pm 1.24$
293.15	$823.50 \pm 0.99$	330.00	$791.67 \pm 1.03$	380.00	$744.90 \pm 1.43$
298.15	$819.31 \pm 1.00$	340.00	$782.65 \pm 1.04$		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

### 5-Methyl-1-heptanol

[7212-53-5]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

117

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 2.1134 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 9.5153 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

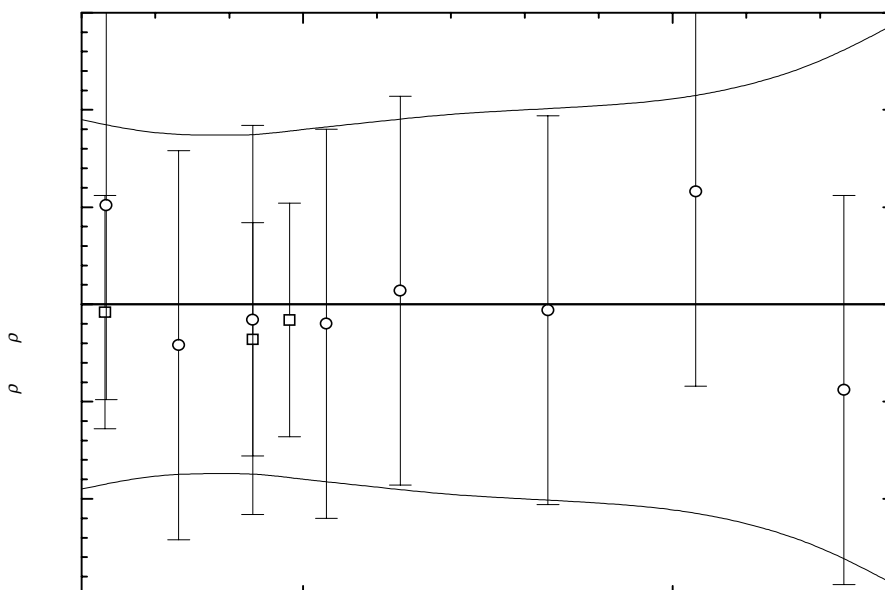
Coefficient	$T = 273.15$ to $373.22$ K
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.74236 \cdot 10^2$
B	$-3.44128 \cdot 10^{-1}$
C	$-6.33911 \cdot 10^{-4}$

cont.

## 5-Methyl-1-heptanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.32	833.33 ± 1.00	0.51	30-bin/dar(○)	353.15	774.23 ± 1.00	0.58	30-bin/dar(○)
283.15	825.76 ± 1.00	-0.21	30-bin/dar(○)	373.22	757.06 ± 1.00	-0.44	30-bin/dar(○)
293.15	818.80 ± 1.00	-0.08	30-bin/dar(○)	273.15	832.90 ± 0.60	-0.04	41-dor/gla(□)
303.15	811.56 ± 1.00	-0.10	30-bin/dar(○)	293.15	818.70 ± 0.60	-0.18	41-dor/gla(□)
313.15	804.38 ± 1.00	0.07	30-bin/dar(○)	298.15	815.20 ± 0.60	-0.08	41-dor/gla(□)
333.15	789.20 ± 1.00	-0.03	30-bin/dar(○)				

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	835.11 ± 0.95	300.00	813.94 ± 0.90	350.00	776.14 ± 1.05
280.00	828.18 ± 0.87	310.00	806.64 ± 0.94	360.00	768.19 ± 1.12
290.00	821.13 ± 0.87	320.00	799.20 ± 0.98	370.00	760.13 ± 1.24
293.15	818.88 ± 0.87	330.00	791.64 ± 1.00	380.00	751.93 ± 1.44
298.15	815.28 ± 0.89	340.00	783.95 ± 1.02		

**L(+)-5-Methyl-1-heptanol** [500006-90-6] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 118

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	825.9 ± 0.6	62-lar/sal

**5-Methyl-2-heptanol** [54630-50-1] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 119

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 3.6541 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 1.7122 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 373.50 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.98516 \cdot 10^2$
B	$2.01122 \cdot 10^{-1}$
C	$-1.67280 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.20	828.78 ± 1.00	0.17	30-bin/dar(O)	353.15	764.06 ± 1.00	3.14	30-bin/dar <sup>1)</sup>
283.15	820.55 ± 1.00	-0.80	30-bin/dar(O)	373.50	740.14 ± 1.00	-0.13	30-bin/dar(O)
293.15	813.34 ± 1.00	-0.38	30-bin/dar(O)	273.15	829.00 ± 0.60	0.36	41-dor/gla(□)
303.15	805.22 ± 1.00	-0.54	30-bin/dar(O)	293.15	813.80 ± 0.60	0.08	41-dor/gla(□)
313.15	797.45 ± 1.00	-0.01	30-bin/dar(O)	298.15	810.00 ± 0.60	0.22	41-dor/gla(□)
333.15	780.88 ± 1.00	1.02	30-bin/dar(O)				

<sup>1)</sup> Not included in Fig. 1.

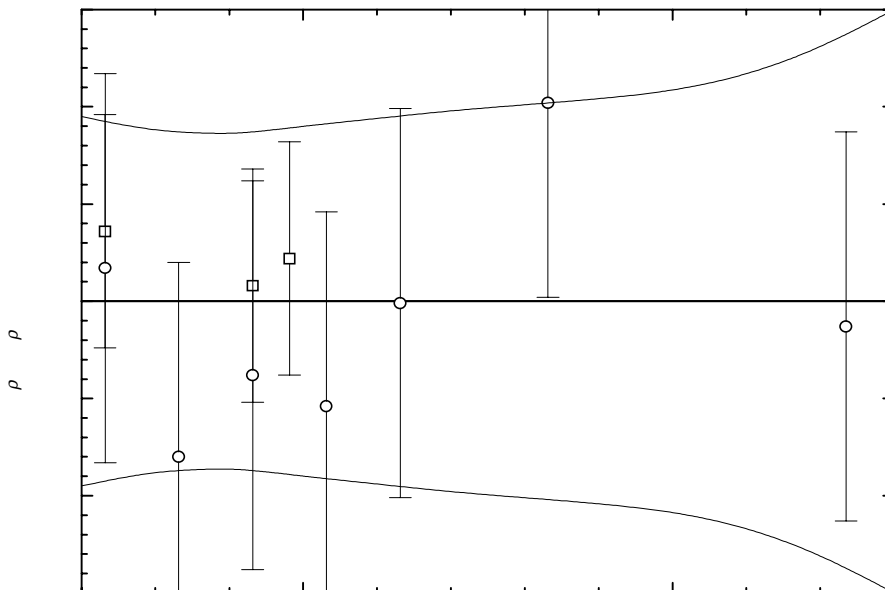
**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	830.87 ± 0.95	300.00	808.30 ± 0.90	350.00	763.99 ± 1.08
280.00	823.68 ± 0.87	310.00	800.11 ± 0.94	360.00	754.12 ± 1.16
290.00	816.16 ± 0.86	320.00	791.58 ± 0.98	370.00	743.92 ± 1.30
293.15	813.72 ± 0.87	330.00	782.72 ± 1.01	380.00	733.39 ± 1.50
298.15	809.78 ± 0.89	340.00	773.52 ± 1.04		

cont.

## 5-Methyl-2-heptanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

## 5-Methyl-3-heptanol

[18720-65-5]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

120

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 9.4864 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 2.9572 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

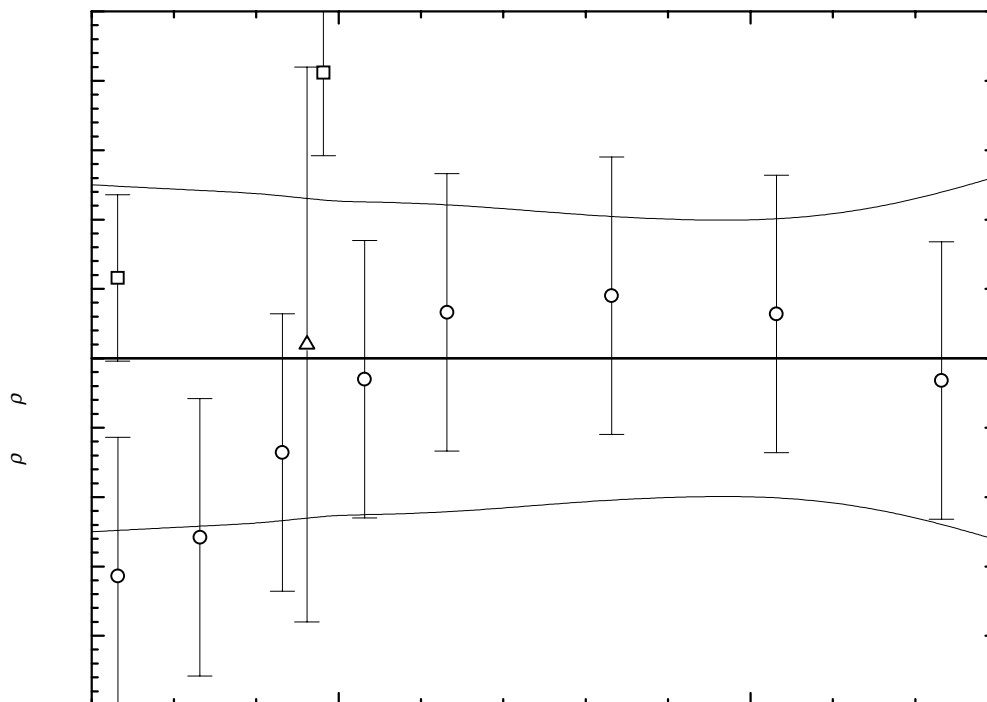
Coefficient	$T = 273.15 \text{ to } 373.20 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.07627 \cdot 10^3$
B	$-8.79191 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.19	$834.52 \pm 1.00$	-1.57	30-bin/dar(O)	353.15	$766.11 \pm 1.00$	0.32	30-bin/dar(O)
283.15	$826.04 \pm 1.00$	-1.29	30-bin/dar(O)	373.20	$748.00 \pm 1.00$	-0.16	30-bin/dar(O)
293.15	$817.86 \pm 1.00$	-0.68	30-bin/dar(O)	296.15	$816.00 \pm 2.00$	0.10	31-lev/mar-4(Δ)
303.15	$809.59 \pm 1.00$	-0.15	30-bin/dar(O)	273.15	$836.70 \pm 0.60$	0.58	41-dor/gla(□)
313.15	$801.28 \pm 1.00$	0.33	30-bin/dar(O)	298.15	$816.20 \pm 0.60$	2.06	41-dor/gla(□)
333.15	$783.82 \pm 1.00$	0.45	30-bin/dar(O)				

cont.

**Further references:** [12-gue, 31-pow/sec, 59-mac/bar].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	838.89 ± 1.25	300.00	812.51 ± 1.13	350.00	768.55 ± 0.99
280.00	830.10 ± 1.22	310.00	803.72 ± 1.12	360.00	759.76 ± 1.03
290.00	821.31 ± 1.19	320.00	794.93 ± 1.08	370.00	750.97 ± 1.14
293.15	818.54 ± 1.17	330.00	786.14 ± 1.03	380.00	742.18 ± 1.31
298.15	814.14 ± 1.14	340.00	777.35 ± 1.00		

**6-Methyl-1-heptanol**

[1653-40-3]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

121

**Table 1.** Coefficients of the polynomial expansion equation.

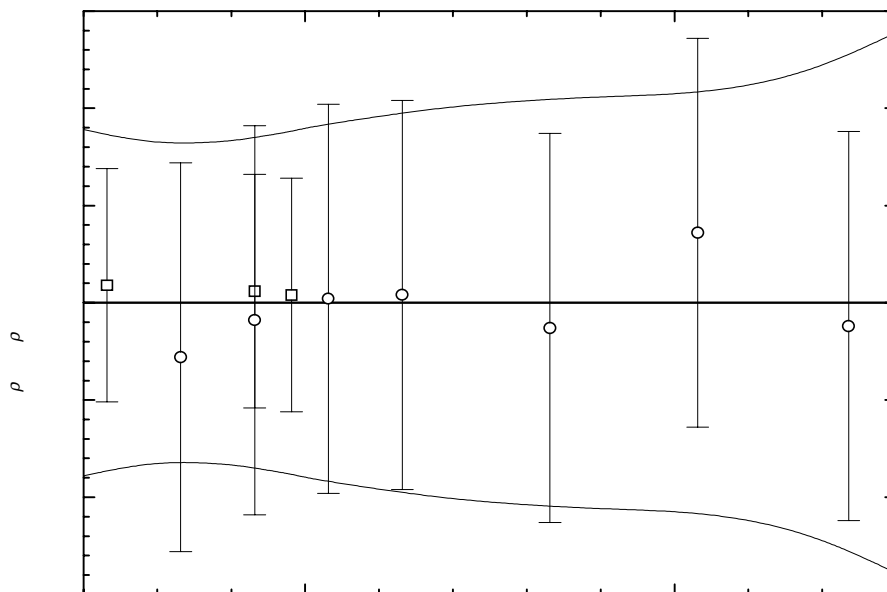
Standard deviations (see introduction):

 $\sigma_{c,w} = 1.1940 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 5.7073 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.57$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.65307 \cdot 10^2$
B	$-2.92230 \cdot 10^{-1}$
C	$-6.81907 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.37	$839.14 \pm 3.00$	4.68	30-bin/dar <sup>1)</sup>	353.15	$777.42 \pm 1.00$	0.36	30-bin/dar(O)
283.15	$827.61 \pm 1.00$	-0.28	30-bin/dar(O)	373.57	$760.86 \pm 1.00$	-0.12	30-bin/dar(O)
293.15	$820.95 \pm 1.00$	-0.09	30-bin/dar(O)	273.15	$834.70 \pm 0.60$	0.09	41-dor/gla(□)
303.15	$814.07 \pm 1.00$	0.02	30-bin/dar(O)	293.15	$821.10 \pm 0.60$	0.06	41-dor/gla(□)
313.15	$806.97 \pm 1.00$	0.04	30-bin/dar(O)	298.15	$817.60 \pm 0.60$	0.04	41-dor/gla(□)
333.15	$792.14 \pm 1.00$	-0.13	30-bin/dar(O)				

<sup>1)</sup> Not included in Fig. 1.**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Further references:** [16-lev/all].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	836.69 ± 0.89	300.00	816.27 ± 0.90	350.00	779.49 ± 1.07
280.00	830.02 ± 0.81	310.00	809.18 ± 0.96	360.00	771.73 ± 1.11
290.00	823.21 ± 0.83	320.00	801.97 ± 1.01	370.00	763.83 ± 1.21
293.15	821.04 ± 0.85	330.00	794.61 ± 1.04	380.00	755.79 ± 1.39
298.15	817.56 ± 0.88	340.00	787.12 ± 1.06		

### 6-Methyl-2-heptanol

[4730-22-7]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

122

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$$\sigma_{c,w} = 1.6961 \cdot 10^{-1} \text{ (combined temperature ranges, weighted),}$$

$$\sigma_{c,uw} = 8.6825 \cdot 10^{-2} \text{ (combined temperature ranges, unweighted).}$$

Coefficient	$T = 273.15 \text{ to } 373.37 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.63426 \cdot 10^2$
B	$-3.06269 \cdot 10^{-1}$
C	$-7.74629 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
284.15	814.10 ± 2.00	0.24	28-esc(Δ)	333.15	775.43 ± 1.00	0.01	30-bin/dar(O)
273.17	822.37 ± 1.00	0.41	30-bin/dar(O)	353.15	759.07 ± 1.00	0.41	30-bin/dar(O)
283.15	814.46 ± 1.00	-0.14	30-bin/dar(O)	373.37	740.47 ± 1.00	-0.62	30-bin/dar(O)
293.15	807.04 ± 1.00	-0.03	30-bin/dar(O)	273.15	821.90 ± 0.60	-0.07	41-dor/gla(□)
303.15	799.17 ± 1.00	-0.22	30-bin/dar(O)	293.15	807.10 ± 0.60	0.03	41-dor/gla(□)
313.15	791.39 ± 1.00	-0.17	30-bin/dar(O)	298.15	803.40 ± 0.60	0.15	41-dor/gla(□)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

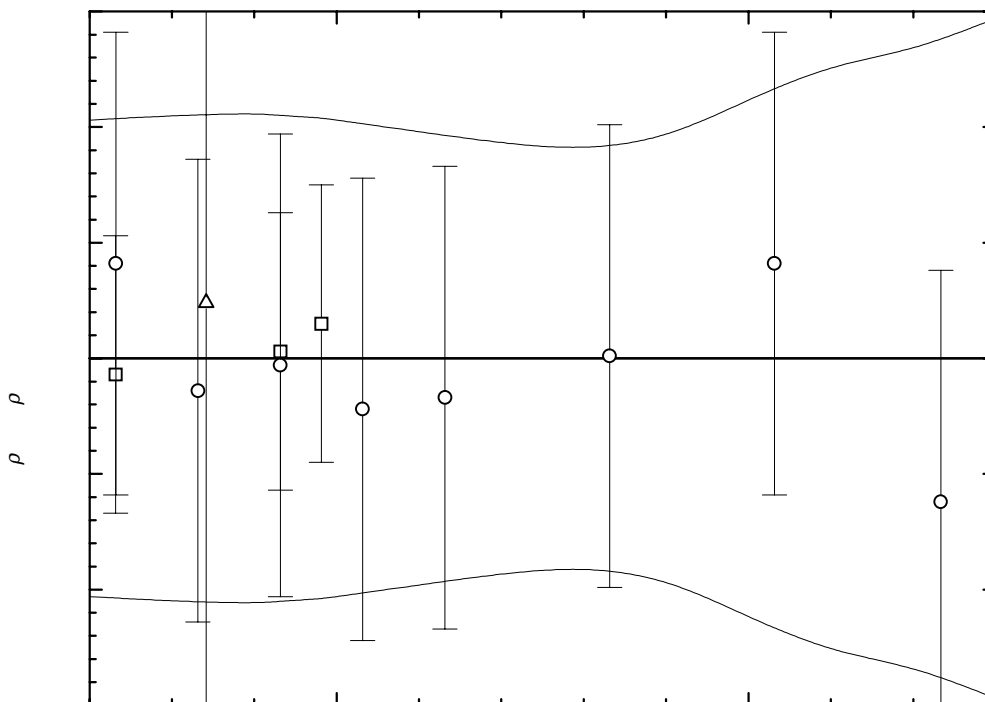
$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	824.26 ± 1.03	300.00	801.83 ± 1.03	350.00	761.34 ± 1.12
280.00	816.94 ± 1.05	310.00	794.04 ± 0.98	360.00	752.78 ± 1.27
290.00	809.46 ± 1.06	320.00	786.10 ± 0.93	370.00	744.06 ± 1.33
293.15	807.07 ± 1.05	330.00	778.00 ± 0.90	380.00	735.19 ± 1.47
298.15	803.25 ± 1.04	340.00	769.75 ± 0.95		

cont.



**6-Methyl-2-heptanol** (cont.)

**Further references:** [08-bue, 08-bue-1, 12-gue-2, 14-wal-1, 52-her/zao, 53-her/zao, 62-mir/fed].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**6-Methyl-3-heptanol**

[18720-66-6]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

123

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 7.5441 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 3.0306 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

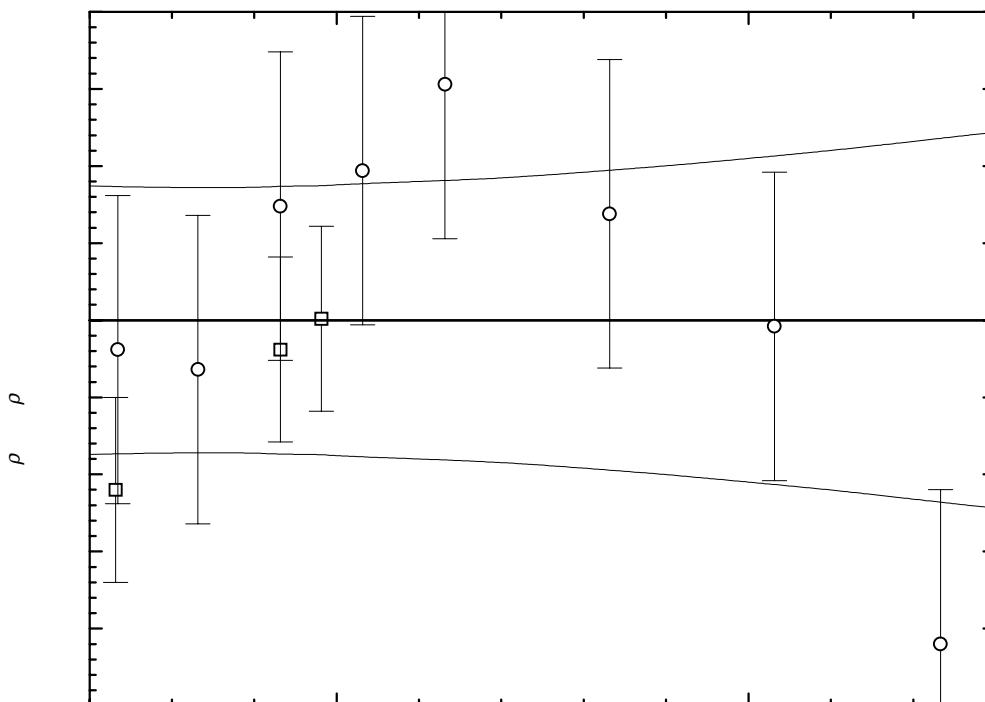
Coefficient	$T = 273.15 \text{ to } 373.32 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.02123 \cdot 10^3$
B	$-8.20546 \cdot 10^{-1}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)
273.42	$796.69 \pm 1.00$	-0.19	30-bin/dar(O)	353.15	$731.42 \pm 1.00$	-0.04	30-bin/dar(O)
283.15	$788.58 \pm 1.00$	-0.32	30-bin/dar(O)	373.32	$712.81 \pm 1.00$	-2.10	30-bin/dar(O)
293.15	$781.43 \pm 1.00$	0.74	30-bin/dar(O)	273.15	$796.00 \pm 0.60$	-1.10	41-dor/gla(□)
303.15	$773.46 \pm 1.00$	0.97	30-bin/dar(O)	293.15	$780.50 \pm 0.60$	-0.19	41-dor/gla(□)
313.15	$765.81 \pm 1.00$	1.53	30-bin/dar(O)	298.15	$776.60 \pm 0.60$	0.01	41-dor/gla(□)
333.15	$748.56 \pm 1.00$	0.69	30-bin/dar(O)				

**Further references:** [08-bue-1, 33-bri, 44-hen/mat].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**6-Methyl-3-heptanol** (cont.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	799.69 ± 0.87	300.00	775.07 ± 0.88	350.00	734.04 ± 1.05
280.00	791.48 ± 0.86	310.00	766.87 ± 0.90	360.00	725.84 ± 1.10
290.00	783.28 ± 0.86	320.00	758.66 ± 0.92	370.00	717.63 ± 1.16
293.15	780.69 ± 0.87	330.00	750.45 ± 0.96	380.00	709.43 ± 1.22
298.15	776.59 ± 0.87	340.00	742.25 ± 1.00		

**3-Methyl-2-(1-methylethyl)-1-butanol** [18593-92-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 124**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	842.5 ± 1.0	56-sar/new

**1-Octanol** [111-87-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 125

$$T_c = 652.60 \text{ K [89-tej/lee]} \quad \rho_c = 266.00 \text{ kg} \cdot \text{m}^{-3} \text{ [89-tej/lee]}$$

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_i = 3.5218 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (2.6366 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 3.0252 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 258.08 \text{ to } 530.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 530.00 \text{ to } 652.60 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$1.02020 \cdot 10^3$	1.11884
B	$-7.81865 \cdot 10^{-1}$	$-1.68799 \cdot 10^{-2}$
C	$8.70573 \cdot 10^{-4}$	$8.96699 \cdot 10^{-5}$
D	$-1.61006 \cdot 10^{-6}$	$-1.31742 \cdot 10^{-7}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
<i>crystal</i>				303.15	818.60 ± 0.60	0.27	29-smy/sto <sup>1)</sup>
78.15	1023.0 ± 3.0		30-bil/fis-1	303.15	818.60 ± 0.40	0.27	29-smy/sto <sup>1)</sup>
194.15	1001.0 ± 3.0		30-bil/fis-1	313.15	811.50 ± 0.40	0.21	29-smy/sto <sup>1)</sup>
<i>liquid</i>				323.15	804.20 ± 0.50	0.08	29-smy/sto <sup>1)</sup>
263.15	846.10 ± 0.50	0.70	29-smy/sto(✗)	333.15	797.00 ± 0.50	0.19	29-smy/sto <sup>1)</sup>
273.15	839.10 ± 0.50	0.33	29-smy/sto <sup>1)</sup>	273.15	838.46 ± 0.20	-0.31	32-ell/rei(✗)
283.15	832.20 ± 0.50	0.14	29-smy/sto <sup>1)</sup>	298.15	821.35 ± 0.20	-0.45	32-ell/rei <sup>1)</sup>
293.15	825.30 ± 0.40	0.05	29-smy/sto <sup>1)</sup>	273.15	837.50 ± 0.50	-1.27	58-cos/bow <sup>1)</sup>
293.15	825.30 ± 0.60	0.05	29-smy/sto <sup>1)</sup>	293.15	822.70 ± 0.52	-2.55	58-cos/bow <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

**Table 2.** (cont.)

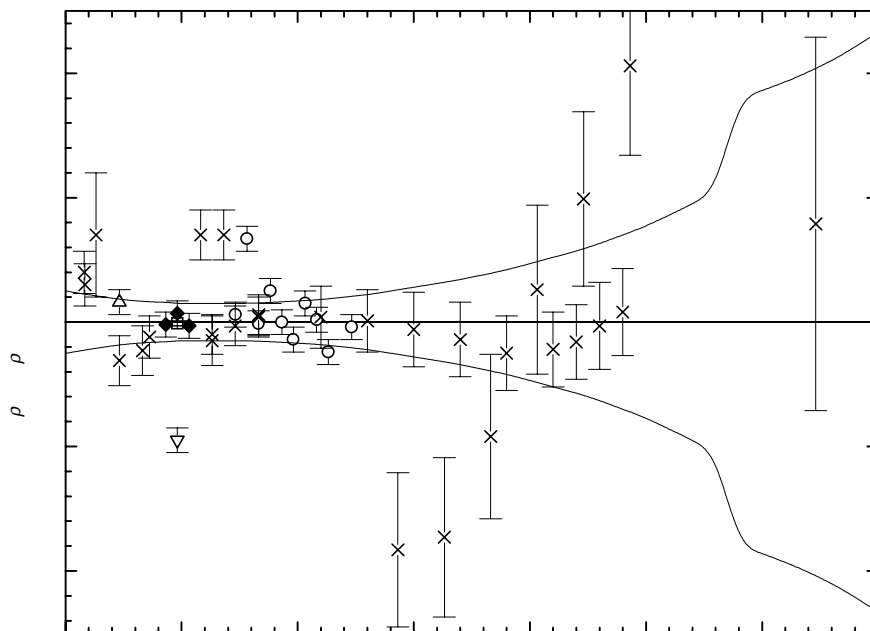
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
313.15	809.10 ± 0.54	-2.19	58-cos/bow <sup>1)</sup>	323.07	804.15 ± 0.16	-0.03	73-fin(✕)
333.15	794.80 ± 0.56	-2.01	58-cos/bow <sup>1)</sup>	333.12	796.87 ± 0.16	0.04	73-fin(✕)
353.15	780.40 ± 0.58	-1.34	58-cos/bow <sup>1)</sup>	333.18	796.85 ± 0.16	0.06	73-fin(✕)
373.15	764.30 ± 0.60	-1.71	58-cos/bow <sup>1)</sup>	293.15	824.99 ± 0.25	-0.26	76-hal/ell <sup>1)</sup>
393.15	747.70 ± 0.62	-1.83	58-cos/bow(✕)	298.15	821.57 ± 0.25	-0.23	76-hal/ell <sup>1)</sup>
413.15	730.50 ± 0.64	-1.73	58-cos/bow(✕)	303.15	818.11 ± 0.25	-0.22	76-hal/ell <sup>1)</sup>
433.15	713.10 ± 0.66	-0.92	58-cos/bow(✕)	320.00	806.27 ± 0.25	-0.12	76-hal/ell <sup>1)</sup>
453.15	695.10 ± 0.68	0.26	58-cos/bow(✕)	340.00	791.73 ± 0.25	0.01	76-hal/ell <sup>1)</sup>
473.15	675.60 ± 0.70	0.99	58-cos/bow(✕)	360.00	776.47 ± 0.25	0.04	76-hal/ell(✕)
493.15	655.30 ± 0.72	2.06	58-cos/bow(✕)	380.00	760.46 ± 0.25	0.01	76-hal/ell(✕)
513.15	635.10 ± 1.50	4.43	58-cos/bow <sup>1)</sup>	400.00	743.64 ± 0.30	-0.06	76-hal/ell(✕)
533.15	613.70 ± 1.50	6.81	58-cos/bow(✕)	420.00	725.96 ± 0.30	-0.14	76-hal/ell(✕)
553.15	590.00 ± 2.00	4.73	58-cos/bow(✕)	440.00	707.32 ± 0.30	-0.25	76-hal/ell(✕)
273.15	838.93 ± 0.10	0.16	59-mck/ski(Δ)	460.00	687.82 ± 0.30	-0.22	76-hal/ell(✕)
273.15	843.00 ± 1.50	4.23	66-efr <sup>1)</sup>	470.00	677.71 ± 0.30	-0.16	76-hal/ell(✕)
293.15	827.00 ± 1.50	1.75	66-efr <sup>1)</sup>	480.00	667.39 ± 0.35	-0.03	76-hal/ell(✕)
313.15	812.00 ± 1.50	0.71	66-efr <sup>1)</sup>	490.00	656.77 ± 0.35	0.08	76-hal/ell(✕)
333.15	797.00 ± 1.50	0.19	66-efr <sup>1)</sup>	293.15	825.23 ± 0.10	-0.02	78-jel/leo(◆)
353.15	782.00 ± 1.50	0.26	66-efr <sup>1)</sup>	298.15	821.87 ± 0.10	0.07	78-jel/leo(◆)
373.15	767.00 ± 1.50	0.99	66-efr <sup>1)</sup>	303.15	818.30 ± 0.10	-0.03	78-jel/leo(◆)
393.15	750.00 ± 1.50	0.47	66-efr <sup>1)</sup>	298.15	822.60 ± 0.20	0.80	79-dia/tar <sup>1)</sup>
413.15	733.00 ± 1.50	0.77	66-efr <sup>1)</sup>	308.15	815.52 ± 0.20	0.70	79-dia/tar(✕)
433.15	714.00 ± 1.50	-0.02	66-efr <sup>1)</sup>	318.15	808.42 ± 0.20	0.70	79-dia/tar(✕)
453.15	696.00 ± 1.50	1.16	66-efr <sup>1)</sup>	333.15	797.58 ± 0.20	0.77	79-dia/tar <sup>1)</sup>
473.15	677.00 ± 1.50	2.39	66-efr <sup>1)</sup>	298.15	821.79 ± 0.02	-0.01	79-kiy/ben(□)
493.15	657.00 ± 1.50	3.76	66-efr <sup>1)</sup>	298.15	820.85 ± 0.10	-0.95	84-sak/nak(∇)
513.15	637.00 ± 1.50	6.33	66-efr <sup>1)</sup>	283.15	831.83 ± 0.20	-0.23	86-hei/sch(✕)
533.15	615.00 ± 1.50	8.11	66-efr(✕)	298.15	821.59 ± 0.20	-0.21	86-hei/sch <sup>1)</sup>
553.15	592.00 ± 1.50	6.73	66-efr(✕)	313.15	811.14 ± 0.20	-0.15	86-hei/sch(✕)
573.15	565.00 ± 1.50	0.79	66-efr(✕)	323.15	804.18 ± 0.10	0.06	93-gar/ban-1(O)
593.15	534.00 ± 1.50	-4.26	66-efr(✕)	328.15	801.15 ± 0.10	0.67	93-gar/ban-1(O)
613.15	500.00 ± 2.00	-0.69	66-efr(✕)	333.15	796.80 ± 0.10	-0.01	93-gar/ban-1(O)
633.15	444.00 ± 2.00	2.66	66-efr(✕)	338.15	793.35 ± 0.10	0.25	93-gar/ban-1(O)
643.15	400.00 ± 3.00	4.51	66-efr(✕)	343.15	789.36 ± 0.10	0.00	93-gar/ban-1(O)
258.08	849.12 ± 0.17	0.40	73-fin(✕)	348.15	785.43 ± 0.10	-0.14	93-gar/ban-1(O)
258.33	848.86 ± 0.17	0.30	73-fin(✕)	353.15	781.89 ± 0.10	0.15	93-gar/ban-1(O)
286.14	829.91 ± 0.17	-0.12	73-fin(✕)	358.15	777.90 ± 0.10	0.02	93-gar/ban-1(O)
293.15	825.10 ± 0.17	-0.15	73-fin <sup>1)</sup>	363.15	773.73 ± 0.10	-0.24	93-gar/ban-1(O)
303.15	818.18 ± 0.16	-0.15	73-fin <sup>1)</sup>	373.15	765.97 ± 0.10	-0.04	93-gar/ban-1(O)
313.15	811.19 ± 0.16	-0.10	73-fin(✕)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1869-zin, 1884-per, 1884-zan, 1886-gar, 1890-gar, 13-har, 14-low, 19-beh, 19-eyk, 27-ver/coo, 29-mah/das, 31-def, 32-kom/tal, 33-ano, 33-but/tho, 33-nev/jat, 35-but/ram, 35-saw, 37-oli, 41-dor/gla, 41-hus/age, 45-add, 48-jon/bow, 48-vog-2, 48-wei, 49-dre/mar, 49-tsv/mar, 50-mum/phi, 50-sac/sau, 52-coo, 52-eri-1, 53-par/cha, 56-goe/mcc, 56-goe/mcc-1, 62-bro/smi, 62-gei/fru, 62-par/mis, 64-blo/hag, 67-gol/per, 69-kat/pat, 73-min/rue, 75-mat/fer, 78-ast, 78-tre/ben, 80-sue/mul.] cont.

**1-Octanol** (cont.)**Further references** (cont.)

[81-sjo/dyh, 82-aww/pet, 82-kat/wat, 82-ort, 82-ven/dha, 83-rau/ste, 85-fer/pin, 85-ort/paz-1, 85-sar/paz, 85-zhu, 86-ash/sri, 86-dew/meh, 86-wag/hei, 87-dew/meh, 88-ort/gar, 89-ala/sal, 89-dew/gup, 89-mat/mak-1, 89-vij/nai, 90-vij/nai, 91-ram/muk, 92-lie/sen-1, 93-yan/mae, 94-yu /tsa-1, 95-arc/bla, 95-cas/cal, 95-fra/jim, 95-fra/men, 95-sen/say, 96-elb].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
250.00	853.99 ± 0.25	298.15	821.80 ± 0.15	350.00	784.16 ± 0.17
260.00	847.47 ± 0.22	300.00	820.52 ± 0.15	360.00	776.43 ± 0.18
270.00	840.87 ± 0.19	310.00	813.52 ± 0.15	370.00	768.54 ± 0.20
280.00	834.18 ± 0.17	320.00	806.39 ± 0.15	380.00	760.45 ± 0.22
290.00	827.40 ± 0.16	330.00	799.13 ± 0.15	390.00	752.18 ± 0.25
293.15	825.25 ± 0.16	340.00	791.72 ± 0.16	400.00	743.70 ± 0.28

cont.

**Table 3.** (cont.)

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
410.00	735.01 ± 0.31	500.00	645.65 ± 0.77	590.00	542.93 ± 2.21
420.00	726.10 ± 0.34	510.00	634.31 ± 0.86	600.00	527.10 ± 2.33
430.00	716.95 ± 0.38	520.00	622.64 ± 0.95	610.00	507.71 ± 2.47
440.00	707.57 ± 0.42	530.00	610.65 ± 1.05	620.00	483.56 ± 2.64
450.00	697.93 ± 0.47	540.00	599.13 ± 1.80	630.00	452.84 ± 3.85
460.00	688.04 ± 0.52	550.00	588.51 ± 1.86	640.00	411.94 ± 4.10
470.00	677.87 ± 0.57	560.00	578.25 ± 1.93	650.00	344.17 ± 5.40
480.00	667.42 ± 0.63	570.00	567.70 ± 2.01		
490.00	656.69 ± 0.70	580.00	556.18 ± 2.10		

**2-Octanol****[123-96-6]****C<sub>8</sub>H<sub>18</sub>O****MW = 130.23****126****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 1.9507 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.1763 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 452.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.55354 \cdot 10^2$
B	$-1.73168 \cdot 10^{-1}$
C	$-9.75788 \cdot 10^{-4}$

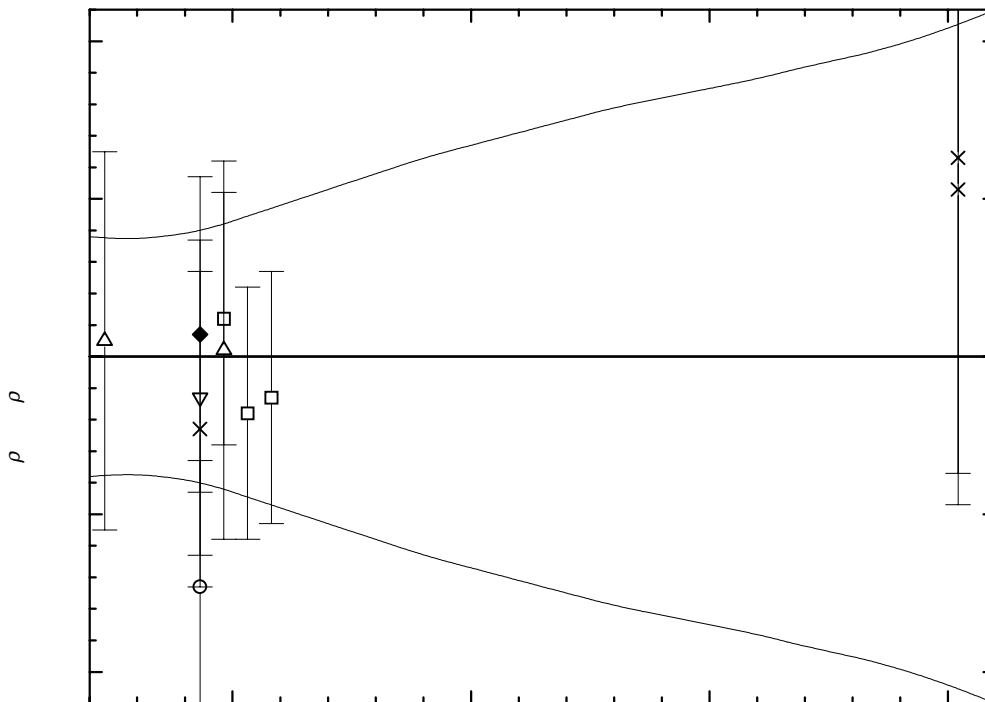
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
452.15	678.10 ± 1.00	0.53	1883-sch-3(✕)	293.15	820.60 ± 0.50	-0.13	62-gei/fru(∇)
452.15	678.20 ± 1.00	0.63	1883-sch-3(✕)	293.15	820.00 ± 0.40	-0.73	90-bar/paz(○)
273.15	835.30 ± 0.60	0.05	41-dor/gla(Δ)	298.15	817.10 ± 0.40	0.12	93-ami/rai(□)
298.15	817.00 ± 0.60	0.02	41-dor/gla(Δ)	303.15	813.00 ± 0.40	-0.18	93-ami/rai(□)
293.15	820.50 ± 0.50	-0.23	46-bra(✕)	308.15	809.20 ± 0.40	-0.13	93-ami/rai(□)
293.15	820.80 ± 0.50	0.07	52-coo(◆)				

**Further references:** [1863-gla/dal, 1880-bru-1, 1884-per, 11-pic/ken, 19-beh, 19-eyk, 33-whi/her, 36-par, 37-zep, 42-mul, 45-add, 50-naz/fis, 53-ani-1, 57-tra/bat, 70-puz/bul].

cont.

## 2-Octanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	837.46 ± 0.38	330.00	791.95 ± 0.58	410.00	720.33 ± 0.88
280.00	830.37 ± 0.37	340.00	783.68 ± 0.63	420.00	710.49 ± 0.92
290.00	823.07 ± 0.39	350.00	775.21 ± 0.67	430.00	700.47 ± 0.95
293.15	820.73 ± 0.40	360.00	766.55 ± 0.71	440.00	690.25 ± 0.99
298.15	816.98 ± 0.42	370.00	757.70 ± 0.75	450.00	679.83 ± 1.04
300.00	815.58 ± 0.43	380.00	748.65 ± 0.79	460.00	669.22 ± 1.10
310.00	807.90 ± 0.48	390.00	739.40 ± 0.82		
320.00	800.02 ± 0.53	400.00	729.96 ± 0.85		

**(R)-(-)-2-Octanol** [5978-70-1] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 127

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	815.2 ± 1.0	55-ber/sch
298.15	816.0 ± 2.0	56-goe/mcc
298.15	815.4 ± 1.0	Recommended

**(RS)-2-Octanol** [4128-31-8] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 128

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.189$ .

Coefficient	$\rho = A + BT$
$A$	1043.06
$B$	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	820.2 ± 1.0	-0.07	39-cop/gos
293.15	820.2 ± 1.0	-0.07	47-kor/lic
298.15	817.0 ± 2.0	0.53	56-goe/mcc

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	822.7 ± 1.3
293.15	820.3 ± 1.2
298.15	816.5 ± 1.3

**(S)-(+)-2-Octanol** [6169-06-8] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 129

**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction):

$\sigma_{c,w} = 4.6275 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.8230 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

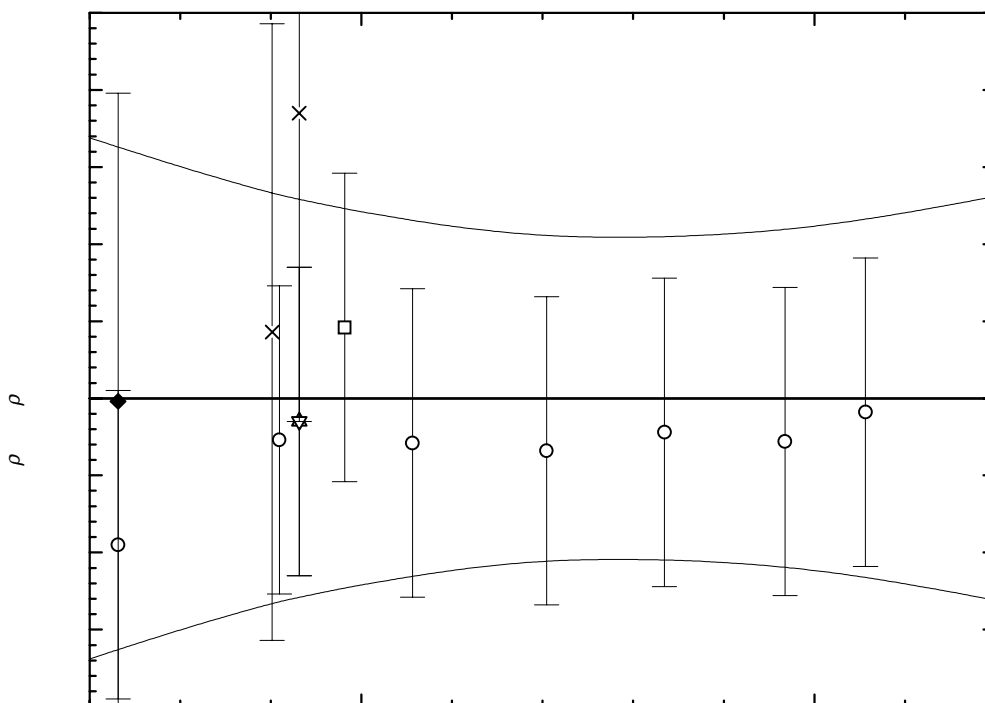
Coefficient	$T = 273.15 \text{ to } 355.65 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
$A$	$1.03721 \cdot 10^3$
$B$	$-7.40112 \cdot 10^{-1}$

cont.



**(S)-(+)-2-Octanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
290.15	822.90 ± 2.00	0.43	07-pic/ken(×)	320.45	799.70 ± 1.00	-0.34	37-pat/hol(○)
293.15	822.10 ± 2.00	1.85	07-pic/ken(×)	333.45	790.20 ± 1.00	-0.22	37-pat/hol(○)
273.15	835.03 ± 2.00	-0.02	32-ell/rei(◆)	346.75	780.30 ± 1.00	-0.28	37-pat/hol(○)
298.15	823.01 ± 2.00	6.47	32-ell/rei <sup>1)</sup>	355.65	773.90 ± 1.00	-0.09	37-pat/hol(○)
273.15	834.10 ± 1.00	-0.95	37-pat/hol(○)	293.15	820.10 ± 1.00	-0.15	39-cop/gos(Δ)
290.95	821.60 ± 1.00	-0.27	37-pat/hol(○)	293.15	820.10 ± 1.00	-0.15	47-kor/lic(∇)
305.65	810.70 ± 1.00	-0.29	37-pat/hol(○)	298.15	817.00 ± 1.00	0.46	56-goe/mcc(□)

<sup>1)</sup> Not included in Fig. 1.**Further references:** [12-pic/ken].**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	837.38 ± 1.69	300.00	815.18 ± 1.21	350.00	778.17 ± 1.11
280.00	829.98 ± 1.50	310.00	807.77 ± 1.11	360.00	770.77 ± 1.20
290.00	822.58 ± 1.33	320.00	800.37 ± 1.05	370.00	763.37 ± 1.31
293.15	820.25 ± 1.29	330.00	792.97 ± 1.04		
298.15	816.54 ± 1.23	340.00	785.57 ± 1.06		

**3-Octanol****[589-98-0]****C<sub>8</sub>H<sub>18</sub>O****MW = 130.23****130****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 5.3499 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 4.6865 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 373.01 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.61167 \cdot 10^2$
B	$-1.85752 \cdot 10^{-1}$
C	$-9.98691 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	824.70 ± 3.00	3.81	13-pic/ken(∇)	333.15	787.53 ± 1.00	-0.91	30-bin/dar(○)
353.15	771.10 ± 3.00	0.08	13-pic/ken(∇)	353.15	770.12 ± 1.00	-0.90	30-bin/dar(○)
273.32	835.49 ± 1.00	-0.30	30-bin/dar(○)	373.01	751.09 ± 1.00	-1.84	30-bin/dar(○)
283.15	827.47 ± 1.00	-1.03	30-bin/dar(○)	273.15	836.10 ± 0.60	0.18	41-dor/gla(□)
293.15	820.88 ± 1.00	-0.01	30-bin/dar(○)	298.15	816.00 ± 0.60	-1.01	41-dor/gla(□)
303.15	812.61 ± 1.00	-0.47	30-bin/dar(○)	293.15	823.90 ± 2.00	3.01	69-nav/tul(Δ)
313.15	804.44 ± 1.00	-0.62	30-bin/dar(○)				

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

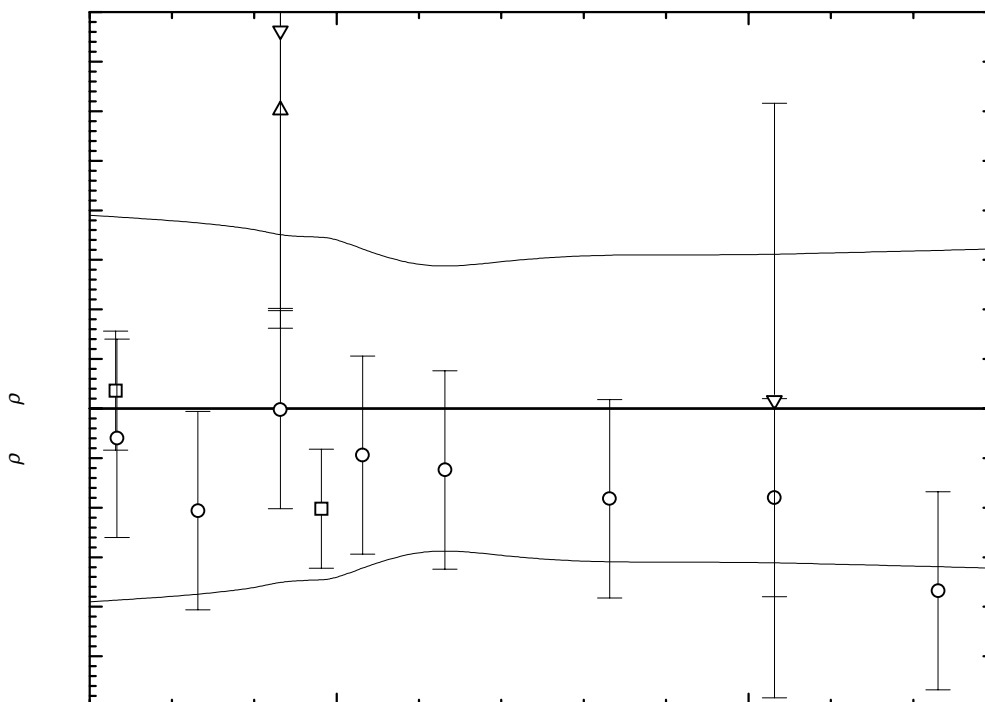
$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	838.21 ± 1.95	300.00	815.56 ± 1.72	350.00	773.81 ± 1.55
280.00	830.86 ± 1.90	310.00	807.61 ± 1.38	360.00	764.87 ± 1.57
290.00	823.31 ± 1.82	320.00	799.46 ± 1.49	370.00	755.72 ± 1.59
293.15	820.89 ± 1.74	330.00	791.11 ± 1.55	380.00	746.37 ± 1.67
298.15	817.01 ± 1.73	340.00	782.56 ± 1.55		

cont.

**3-Octanol** (cont.)

**Further references:** [56-woo/vio, 62-gei/fru].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**(RS)-3-Octanol** [20296-29-1] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 131

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.35	817.7 ± 0.8	33-bri

**(S)-(+)-3-Octanol** [22658-92-0] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 132

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	834.4 ± 1.0	57-shu/bel

## 4-Octanol

[589-62-8]

C<sub>8</sub>H<sub>18</sub>O

MW = 130.23

133

**Table 1.** Coefficients of the polynomial expansion equation.

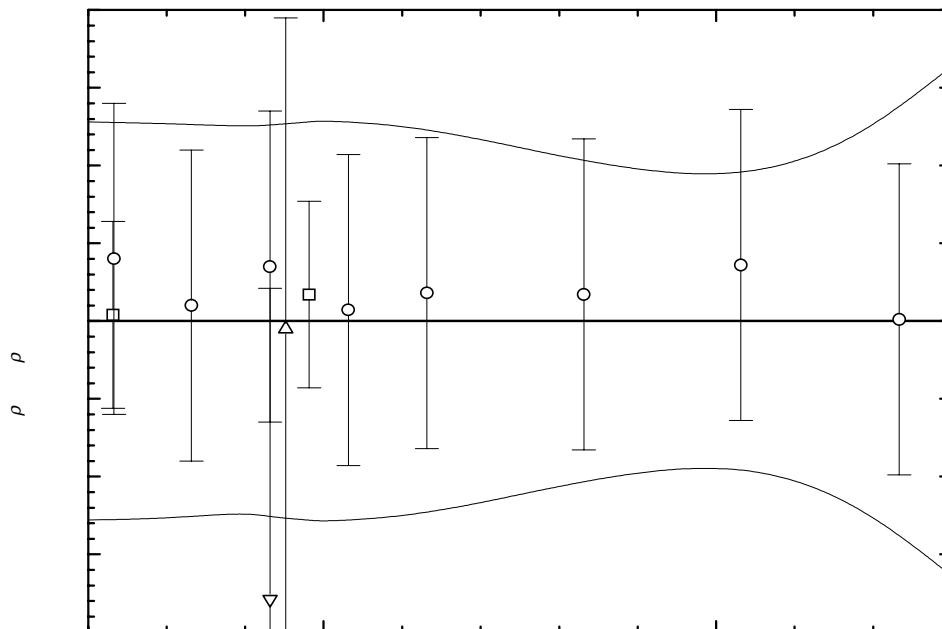
Standard deviations (see introduction):

 $\sigma_{c,w} = 2.5809 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.7589 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $373.32$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.65289 \cdot 10^2$
B	$-2.26785 \cdot 10^{-1}$
C	$-9.21832 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.29	$834.86 \pm 1.00$	0.40	30-bin/dar(O)	353.15	$770.59 \pm 1.00$	0.36	30-bin/dar(O)
283.15	$827.27 \pm 1.00$	0.10	30-bin/dar(O)	373.32	$752.16 \pm 1.00$	0.01	30-bin/dar(O)
293.15	$819.94 \pm 1.00$	0.35	30-bin/dar(O)	295.15	$818.00 \pm 2.00$	-0.05	31-lev/mar-2( $\Delta$ )
303.15	$811.89 \pm 1.00$	0.07	30-bin/dar(O)	293.15	$817.80 \pm 2.00$	-1.79	36-tuo( $\nabla$ )
313.15	$804.05 \pm 1.00$	0.18	30-bin/dar(O)	273.15	$834.60 \pm 0.60$	0.04	41-dor/gla( $\square$ )
333.15	$787.59 \pm 1.00$	0.17	30-bin/dar(O)	298.15	$815.90 \pm 0.60$	0.17	41-dor/gla( $\square$ )

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**4-Octanol** (cont.)**Further references:** [06-bou/loc, 50-naz/fis, 62-gei/fru].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	836.86 ± 1.28	300.00	814.29 ± 1.29	350.00	772.99 ± 0.93
280.00	829.52 ± 1.27	310.00	806.40 ± 1.26	360.00	764.18 ± 1.00
290.00	822.00 ± 1.25	320.00	798.32 ± 1.17	370.00	755.18 ± 1.24
293.15	819.59 ± 1.26	330.00	790.06 ± 1.06	380.00	746.00 ± 1.64
298.15	815.73 ± 1.28	340.00	781.62 ± 0.97		

**2-Propyl-1-pentanol** [58175-57-8] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 134**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
294.15	900.0 ± 10.0	58-wie/thu

**2,2,3-Trimethyl-3-pentanol** [7294-05-5] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 135**Table 1.** Fit with estimated *B* coefficient for 5 accepted points. Deviation  $\sigma_w = 0.823$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1075.47
<i>B</i>	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	849.0 ± 2.00	2.19	33-whi/lau	298.15	842.0 ± 1.00	-0.91	39-gin/col
298.15	842.3 ± 1.00	-0.61	36-nor/has	293.15	831.0 ± 10.00	-15.81	57-pet/sus <sup>1)</sup>
298.15	843.4 ± 1.00	0.49	36-nor/has	293.15	847.3 ± 1.00	0.49	62-gei/fru

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	849.3 ± 1.4
293.15	846.8 ± 1.3
298.15	842.9 ± 1.2

**2,2,4-Trimethyl-1-pentanol** [123-44-4] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 136

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	823.2 ± 10.0	25-ter <sup>1)</sup>
293.15	838.4 ± 1.0	58-ano-3
293.15	838.4 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,2,4-Trimethyl-3-pentanol** [5162-48-1] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 137

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	832.2 ± 1.0	51-smi/cre
293.15	832.6 ± 1.0	62-gei/fru
293.15	832.4 ± 1.0	Recommended

**2,3,3-Trimethyl-2-pentanol** [23171-85-9] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 138

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	861.0 ± 2.0	33-whi/lau
298.15	815.1 ± 5.0	36-nor/has
293.15	851.7 ± 2.0	41-hus/gui

**2,3,4-Trimethyl-1-pentanol** [6570-88-3] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 139

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	849.8 ± 1.0	58-per/can

**2,3,4-Trimethyl-2-pentanol** [66576-26-9] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 140

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	808.1 ± 2.0	39-hus/gui
293.15	808.0 ± 2.0	41-hus/gui
293.15	843.2 ± 2.0	48-hus/kra

**2,3,4-Trimethyl-3-pentanol** [3054-92-0] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 141

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	849.2 ± 2.0	26-sta

**2,4,4-Trimethyl-1-pentanol** [16325-63-6] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 142

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	833.0 ± 2.0	40-sut

**2,4,4-Trimethyl-2-pentanol** [690-37-9] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 143

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
296.65	830.9 ± 6.0	48-rit <sup>1)</sup>
293.15	822.5 ± 2.0	41-hus/gui
293.15	825.0 ± 2.0	41-whi/wil
293.15	823.7 ± 2.2	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,3,4-Trimethyl-2-pentanol** [19411-41-7] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 144

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	812.8 ± 4.0	08-bue <sup>1)</sup>
293.15	855.7 ± 1.0	55-mes/pet
293.15	855.7 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,4,4-Trimethyl-2-pentanol** [10575-56-1] C<sub>8</sub>H<sub>18</sub>O MW = 130.23 145

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	840.8 ± 1.0	41-whe

2.1.5 Alkanols, C<sub>9</sub>

**2,2-Dimethyl-3-ethyl-3-pentanol** [66793-96-2] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 146

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.250$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1097.33
<i>B</i>	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	852.4 ± 3.0	-4.55	38-whi/mey <sup>1)</sup>
293.15	857.2 ± 1.0	0.25	47-how/mea
298.15	852.6 ± 1.0	-0.25	47-how/mea

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	859.5 ± 0.9
293.15	857.0 ± 0.7
298.15	852.9 ± 0.7

**2,4-Dimethyl-2-ethyl-1-pentanol** [66793-98-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 147

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	837.0 ± 1.5	52-doe/far

**2,4-Dimethyl-3-ethyl-3-pentanol** [3970-59-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 148

**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 0.542$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1081.51
<i>B</i>	-0.760

cont.



**2,4-Dimethyl-3-ethyl-3-pentanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
273.15	877.3 ± 2.0	3.38	26-sta <sup>1)</sup>	293.15	858.8 ± 0.6	0.08	47-how/mea
293.15	860.8 ± 2.0	2.08	26-sta <sup>1)</sup>	298.15	854.3 ± 0.6	-0.62	47-how/mea
303.15	853.2 ± 2.0	2.08	26-sta <sup>1)</sup>	293.15	858.8 ± 0.6	0.08	51-smi/cre
293.15	860.0 ± 1.0	1.28	43-geo				

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	861.1 ± 0.8
293.15	858.7 ± 0.7
298.15	854.9 ± 0.7

**2,2-Dimethyl-3-heptanol**

[19549-70-3]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

149

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.020$ .

Coefficient	$\rho = A + BT$
$A$	1050.33
$B$	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
295.15	826.0 ± 1.0	-0.02	49-col/lag
299.15	823.0 ± 1.0	0.02	59-fol/wel

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	829.9 ± 1.1
293.15	827.5 ± 1.0
298.15	823.7 ± 0.9

**2,3-Dimethyl-2-heptanol**

[66794-00-1]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

150

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	839.6 ± 1.0	48-naz/tor

**2,3-Dimethyl-3-heptanol** [19549-71-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 151

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	839.5 ± 2.0	33-whi/eve
294.15	838.3 ± 2.0	33-whi/eve
293.15	834.9 ± 3.0	50-naz/bak

**2,4-Dimethyl-2-heptanol** [65822-93-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 152

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	828.0 ± 1.0	59-col/gau

**2,4-Dimethyl-4-heptanol** [19549-77-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 153

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	826.0 ± 1.0	09-bod/tab	293.15	824.2 ± 1.0	59-pet/zak
293.15	821.5 ± 3.0	33-mey/tuo <sup>1)</sup>	293.15	824.2 ± 1.0	59-pet/zak-1
293.15	825.4 ± 1.0	42-hen/all	293.15	824.8 ± 1.0	Recommended
293.15	824.2 ± 1.0	54-naz/kak-3			

<sup>1)</sup> Not included in calculation of recommended value.

**2,5-Dimethyl-2-heptanol** [1561-18-8] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 154

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.15	830.0 ± 2.0	31-lev/mar-2

**2,6-Dimethyl-2-heptanol** [13254-34-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 155

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	818.6 ± 2.0	26-pas/zam
283.65	816.2 ± 2.0	28-esc

**2,6-Dimethyl-3-heptanol** [19549-73-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 156

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	821.2 ± 4.0	12-mic <sup>1)</sup>
293.15	814.8 ± 2.0	36-tuo
293.15	814.8 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,6-Dimethyl-4-heptanol**

[108-82-7]

C<sub>9</sub>H<sub>20</sub>O

MW =144.26

157

**Table 1.** Fit with estimated *B* coefficient for 8 accepted points. Deviation  $\sigma_w = 0.427$ .

Coefficient	$\rho = A + BT$
A	1033.02
B	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
294.15	809.0 ± 1.0	-0.47	14-vav	333.15	779.9 ± 0.4	0.05	47-str/gab
293.15	811.4 ± 1.0	1.17	36-tuo	293.15	810.6 ± 1.0	0.37	53-ano-5
293.15	809.7 ± 0.4	-0.56	47-str/gab	293.15	810.7 ± 1.0	0.47	58-ano-5
313.15	795.2 ± 0.4	0.17	47-str/gab	293.15	810.7 ± 1.0	0.47	68-ano

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	812.6 ± 1.3	310.00	797.4 ± 0.8	330.00	782.2 ± 1.3
293.15	810.2 ± 1.1	320.00	789.8 ± 1.0	340.00	774.6 ± 1.8
298.15	806.4 ± 1.0				

**3,5-Dimethyl-3-heptanol**

[19549-74-7]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

158

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 1.930$ .

Coefficient	$\rho = A + BT$
A	1066.31
B	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
298.15	817.7 ± 3.0	-4.13	30-dav/dix <sup>1)</sup>
297.15	834.0 ± 8.0	11.35	48-bro/bro <sup>1)</sup>
301.15	831.0 ± 8.0	11.63	48-bro/bro <sup>1)</sup>
293.15	824.0 ± 2.0	-1.93	59-mac/bar
301.15	821.3 ± 2.0	1.93	60-tha/vas

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	828.5 ± 2.1
293.15	825.9 ± 2.1
298.15	821.8 ± 2.1
310.00	812.1 ± 2.2

**3,5-Dimethyl-4-heptanol** [19549-79-2] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 159**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
291.15	836.0 ± 10.0	23-vav/iva <sup>1)</sup>
293.15	859.2 ± 1.0	52-lev/shu
293.15	859.2 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**3,6-Dimethyl-1-heptanol** [1573-33-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 160**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
300.15	823.0 ± 2.0	32-lev/mar

**3,6-Dimethyl-3-heptanol** [1573-28-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 161**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
289.15	828.5 ± 2.0	04-kon

**4,6-Dimethyl-2-heptanol** [51079-52-8] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 162**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	878.7 ± 2.0	09-gue <sup>1)</sup>
273.15	880.1 ± 2.0	12-gue <sup>1)</sup>
298.15	822.0 ± 1.5	64-hin/dre
298.15	822.0 ± 1.5	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**5,6-Dimethyl-2-heptanol** [58795-24-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 163**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
291.15	835.0 ± 2.0	11-wal

**6,6-Dimethyl-1-heptanol** [65769-10-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 164

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	843.9 ± 1.0	56-gol/kon

**3-Ethyl-1-heptanol** [3525-25-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 165

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
296.15	834.0 ± 2.0	31-lev/mar-3

**3-Ethyl-3-heptanol** [19780-41-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 166

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.4886 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.4242 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.07793 \cdot 10^3$
B	$-8.33559 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	832.90 ± 1.00	-0.67	38-whi/ore(□)	318.15	812.60 ± 1.00	-0.14	39-owe/qua(○)
273.15	850.50 ± 1.00	0.25	39-owe/qua(○)	328.15	804.30 ± 1.00	-0.10	39-owe/qua(○)
298.15	829.90 ± 1.00	0.49	39-owe/qua(○)	338.15	796.30 ± 1.00	0.24	39-owe/qua(○)
308.15	821.00 ± 1.00	-0.07	39-owe/qua(○)				

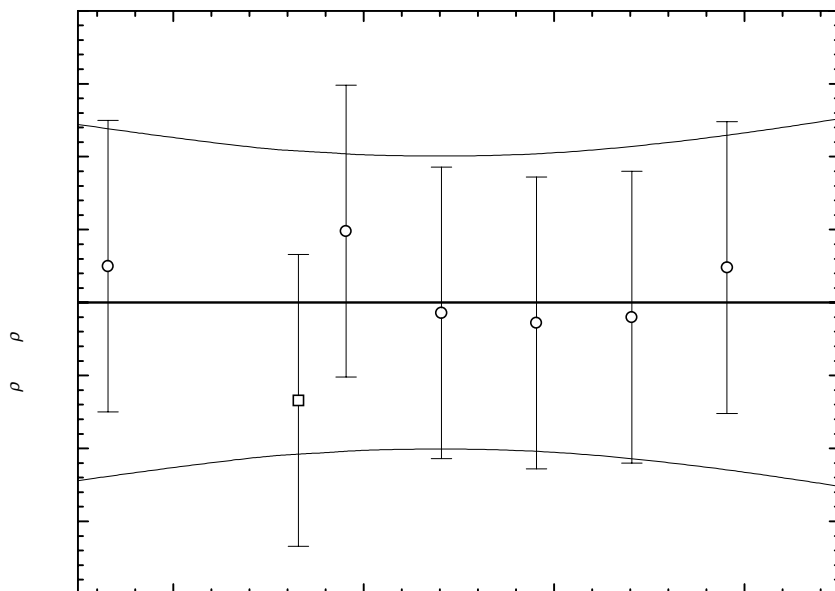
**Further references:** [29-con/bla, 33-whi/woo].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	852.87 ± 1.22	298.15	829.41 ± 1.02	330.00	802.86 ± 1.08
280.00	844.54 ± 1.13	300.00	827.86 ± 1.01	340.00	794.52 ± 1.16
290.00	836.20 ± 1.05	310.00	819.53 ± 1.00	350.00	786.19 ± 1.26
293.15	833.57 ± 1.04	320.00	811.19 ± 1.02		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**5-Ethyl-1-heptanol** [998-65-2] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 167

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	848.0 ± 1.0	62-col/des

**2-Ethyl-3-methyl-1-hexanol** [66794-04-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 168

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	835.8 ± 1.0	32-con/adk

**2-Ethyl-4-methyl-1-hexanol** [66794-06-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 169

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	828.8 ± 1.0	58-hag/hud

**2-Ethyl-5-methyl-1-hexanol** [66794-07-8] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 170

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	820.8 ± 1.0	32-con/adk

**3-Ethyl-2-methyl-1-hexanol** [66794-01-2] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 171

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.15	848.0 ± 2.0	54-naz/kak-4 <sup>1)</sup>
293.15	851.2 ± 1.0	54-naz/kak-4
293.15	851.2 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Ethyl-2-methyl-2-hexanol** [66794-02-3] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 172

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	833.4 ± 1.0	54-ski/flo

**3-Ethyl-2-methyl-3-hexanol** [66794-03-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 173

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	850.6 ± 2.0	26-sta <sup>1)</sup>
295.15	845.2 ± 2.0	54-naz/kak-4 <sup>1)</sup>
298.15	844.5 ± 1.0	54-ski/flo
298.15	844.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Ethyl-4-methyl-3-hexanol** [51200-80-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 174

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
288.15	861.0 ± 1.0	44-pre/zal

**3-Ethyl-5-methyl-3-hexanol** [597-77-3] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 175

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
295.15	839.6 ± 2.0	14-hal

**4-Ethyl-2-methyl-3-hexanol** [33943-21-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 176

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	827.5 ± 1.0	43-geo

**4-Ethyl-3-methyl-3-hexanol** [66794-05-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 177

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	899.4 ± 1.0	54-ski/flo

**1-Ethyl-1-propyl-1-butanol** [597-90-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 178

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.464$ .

Coefficient	$\rho = A + BT$
$A$	1074.08
$B$	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>		K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
289.15	838.4 ± 2.0	1.42	19-eyk <sup>1)</sup>	298.15	829.9 ± 1.0	0.30	39-owe/qua
293.15	833.7 ± 1.5	0.00	26-sta	328.15	804.3 ± 1.0	-0.70	39-owe/qua
273.15	850.5 ± 1.0	0.40	39-owe/qua	293.15	836.4 ± 2.0	2.70	54-naz/kak-3 <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>	K	kg · m <sup>-3</sup>	K	kg · m <sup>-3</sup>
270.00	852.7 ± 1.9	293.15	833.7 ± 0.9	320.00	811.7 ± 1.5
280.00	844.5 ± 1.4	298.15	829.6 ± 0.8	330.00	803.5 ± 2.0
290.00	836.3 ± 1.0	310.00	819.9 ± 1.1		



**2-Methyl-1-octanol** [818-81-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 179

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
277.15	841.8 ± 1.0	04-bou/bla-2

**2-Methyl-2-octanol** [628-44-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 180

**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction):

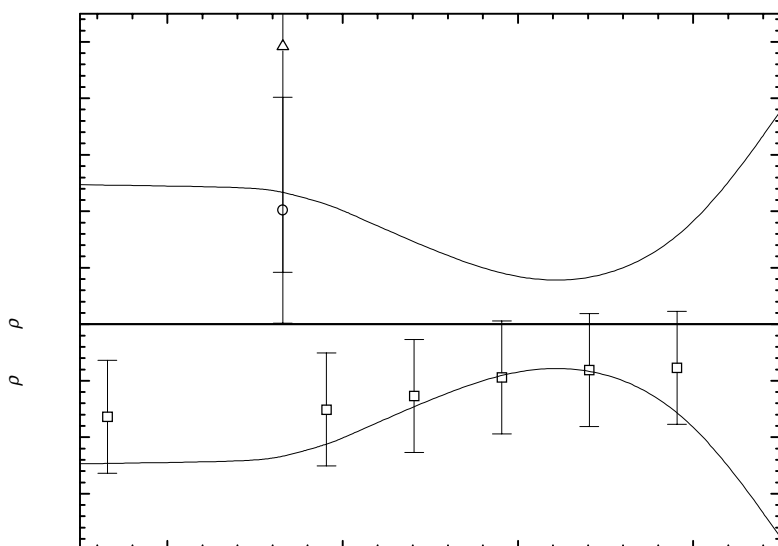
$\sigma_{\text{c,w}} = 1.2926$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 8.1386 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.05740 \cdot 10^3$
B	$-8.13336 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	821.00 ± 2.00	2.02	38-whi/ore(○)	318.15	797.70 ± 1.00	-0.94	39-owe/qua(□)
273.15	833.60 ± 1.00	-1.64	39-owe/qua(□)	328.15	789.70 ± 1.00	-0.81	39-owe/qua(□)
298.15	813.40 ± 1.00	-1.51	39-owe/qua(□)	338.15	781.60 ± 1.00	-0.77	39-owe/qua(□)
308.15	805.50 ± 1.00	-1.27	39-owe/qua(□)	293.15	823.90 ± 4.00	4.92	56-tar/tai(Δ)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)  
cont.

**Further references:** [59-her].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	837.80 ± 2.47	298.15	814.91 ± 2.13	330.00	789.00 ± 0.76
280.00	829.67 ± 2.45	300.00	813.40 ± 2.02	340.00	780.87 ± 1.60
290.00	821.54 ± 2.42	310.00	805.27 ± 1.32	350.00	772.74 ± 3.78
293.15	818.98 ± 2.35	320.00	797.14 ± 0.75		

**2-Methyl-3-octanol** [26533-34-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 181

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	827.0 ± 3.0	12-pic/ken <sup>1)</sup>
293.15	833.1 ± 2.0	31-lev/mar-4
293.15	833.1 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Methyl-4-octanol** [40575-41-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 182

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	815.0 ± 3.0	06-mal-1 <sup>1)</sup>
293.15	813.0 ± 4.0	36-tuo <sup>1)</sup>
298.15	815.0 ± 2.0	54-dub/luf
298.15	815.0 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Methyl-1-octanol** [38514-02-2] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 183

**Table 1.** Experimental values with uncertainties.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
297.15	827.0 ± 2.0	31-lev/mar-1
297.15	827.0 ± 2.0	31-lev/mar-5

**3-Methyl-2-octanol** [27644-49-1] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 184**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
300.15	831.0 ± 2.0	33-pow/mur

**3-Methyl-3-octanol** [5340-36-3] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 185**Table 1.** Fit with estimated  $B$  coefficient for 6 accepted points. Deviation  $\sigma_w = 0.605$ .

Coefficient	$\rho = A + BT$
$A$	1072.01
$B$	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
298.15	825.8 ± 2.0	-1.73	33-whi/wil	328.15	802.9 ± 1.0	-0.03	44-qua/sma
293.15	821.6 ± 8.0	-10.03	34-gre <sup>1)</sup>	293.15	833.1 ± 2.0	1.47	54-pom/foo-1
298.15	827.5 ± 1.0	-0.03	44-qua/sma	293.15	832.2 ± 2.0	0.57	61-sok/she
318.15	811.1 ± 1.0	-0.03	44-qua/sma				

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	834.2 ± 2.5	298.15	827.5 ± 1.8	320.00	809.6 ± 1.6
293.15	831.6 ± 2.2	310.00	817.8 ± 1.3	330.00	801.4 ± 2.3

**3-Methyl-4-octanol** [26533-35-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 186**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
291.15	834.0 ± 2.0	23-vav/iva

**4-Methyl-1-octanol** [38514-03-3] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 187**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
300.65	820.0 ± 2.0	31-lev/mar-5

**4-Methyl-3-octanol** [66793-80-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 188**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	843.7 ± 2.0	34-gre

**4-Methyl-4-octanol** [23418-37-3] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 189**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 0.328$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1069.04
<i>B</i>	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	826.7 ± 2.0	-1.96	33-whi/woo <sup>1)</sup>	328.15	799.9 ± 1.0	-0.06	44-qua/sma
298.15	823.7 ± 2.0	-0.86	33-whi/woo <sup>1)</sup>	293.15	828.4 ± 0.6	-0.26	54-pom/foo-1
298.15	825.2 ± 1.0	0.64	44-qua/sma	293.15	822.7 ± 4.0	-5.96	59-yur/bel-1 <sup>1)</sup>
318.15	808.3 ± 1.0	0.14	44-qua/sma				

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	831.2 ± 0.9	298.15	824.6 ± 0.6	320.00	806.6 ± 1.0
293.15	828.7 ± 0.8	310.00	814.8 ± 0.6	330.00	798.4 ± 1.4

**5-Methyl-1-octanol** [38514-04-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 190**Table 1.** Experimental value with uncertainty.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
297.15	828.0 ± 2.0	33-lev/mar-1

**5-Methyl-2-octanol** [66793-81-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 191**Table 1.** Experimental value with uncertainty.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	821.0 ± 2.0	31-lev/mar-4

**5-Methyl-4-octanol** [59734-23-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 192**Table 1.** Experimental value with uncertainty.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	815.6 ± 0.8	12-bje

**(S)-6-Methyl-1-octanol** [110453-78-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 193

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
297.15	828.0 ± 2.0	33-lev/mar-1

**6-Methyl-3-octanol** [40225-75-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 194

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
301.15	832.0 ± 1.0	36 -pow/bal -0

**6-Methyl-4-octanol** [66793-82-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 195

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
296.15	822.0 ± 2.0	31-lev/mar-4

**7-Methyl-1-octanol** [2430-22-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 196

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	826.0 ± 2.0	16-lev/all

**7-Methyl-3-octanol** [66793-84-8] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 197

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
285.15	840.2 ± 2.0	25-tho/kah

**7-Methyl-4-octanol** [33933-77-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 198

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	813.6 ± 1.0	36-tuo

**4-Methyl-2-propyl-1-pentanol** [54004-41-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 199

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	825.6 ± 1.0	58-hag/hud

## 1-Nonanol

[143-08-8]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

200

 $T_c = 670.50 \text{ K}$  [89-tej/lee] $\rho_c = 264.00 \text{ kg}\cdot\text{m}^{-3}$  [89-tej/lee]

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_T = 9.8705 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (5.4570 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 4.0529 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 540.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 540.00 \text{ to } 670.50 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$9.49744 \cdot 10^2$	2.41155
B	$-7.07347 \cdot 10^{-2}$	$-5.85206 \cdot 10^{-2}$
C	$-1.43841 \cdot 10^{-3}$	$5.31779 \cdot 10^{-4}$
D	$8.99651 \cdot 10^{-7}$	$-1.62241 \cdot 10^{-6}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg}\cdot\text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg}\cdot\text{m}^{-3}$	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg}\cdot\text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg}\cdot\text{m}^{-3}$	Ref. (Symbol in Fig. 1)
273.15	$841.50 \pm 1.00$	0.06	1886-kra(X)	288.15	$831.00 \pm 1.70$	-0.45	71-gol/dob <sup>1)</sup>
273.15	$841.50 \pm 0.60$	0.06	1886-kra(X)	288.45	$831.00 \pm 1.70$	-0.25	71-gol/dob <sup>1)</sup>
283.15	$834.60 \pm 0.60$	-0.22	1886-kra(X)	293.15	$827.80 \pm 1.70$	-0.26	71-gol/dob <sup>1)</sup>
283.15	$834.60 \pm 1.00$	-0.22	1886-kra <sup>1)</sup>	298.85	$822.30 \pm 1.60$	-1.85	71-gol/dob <sup>1)</sup>
293.15	$827.90 \pm 0.60$	-0.16	1886-kra <sup>1)</sup>	298.95	$822.30 \pm 1.60$	-1.78	71-gol/dob <sup>1)</sup>
293.15	$827.90 \pm 1.00$	-0.16	1886-kra <sup>1)</sup>	303.15	$821.80 \pm 1.60$	0.63	71-gol/dob <sup>1)</sup>
273.15	$840.00 \pm 0.30$	-1.44	32-ell/rei(V)	313.15	$815.50 \pm 1.60$	1.33	71-gol/dob <sup>1)</sup>
298.15	$823.01 \pm 0.30$	-1.62	32-ell/rei(V)	322.85	$809.50 \pm 1.60$	2.25	71-gol/dob <sup>1)</sup>
273.15	$827.00 \pm 1.50$	-14.44	66-efr <sup>1)</sup>	323.15	$809.20 \pm 1.60$	2.16	71-gol/dob <sup>1)</sup>
293.15	$827.00 \pm 1.50$	-1.06	66-efr <sup>1)</sup>	323.45	$809.10 \pm 1.60$	2.28	71-gol/dob <sup>1)</sup>
313.15	$813.00 \pm 1.50$	-1.17	66-efr <sup>1)</sup>	333.15	$802.80 \pm 1.60$	3.00	71-gol/dob <sup>1)</sup>
333.15	$800.00 \pm 1.50$	0.20	66-efr <sup>1)</sup>	343.15	$796.10 \pm 1.60$	3.65	71-gol/dob <sup>1)</sup>
353.15	$786.00 \pm 1.50$	1.00	66-efr <sup>1)</sup>	347.75	$793.20 \pm 1.60$	4.17	71-gol/dob <sup>1)</sup>
373.15	$771.00 \pm 1.50$	1.19	66-efr <sup>1)</sup>	347.75	$793.10 \pm 1.60$	4.07	71-gol/dob <sup>1)</sup>
393.15	$755.00 \pm 1.50$	0.73	66-efr(X)	347.85	$792.90 \pm 1.60$	3.94	71-gol/dob <sup>1)</sup>
413.15	$739.00 \pm 1.50$	0.56	66-efr(X)	353.15	$789.20 \pm 1.60$	4.20	71-gol/dob <sup>1)</sup>
433.15	$722.00 \pm 1.50$	-0.34	66-efr(X)	363.15	$782.20 \pm 1.60$	4.75	71-gol/dob <sup>1)</sup>
453.15	$704.00 \pm 1.50$	-2.03	66-efr(X)	369.95	$777.50 \pm 1.60$	5.24	71-gol/dob <sup>1)</sup>
473.15	$686.00 \pm 1.50$	-3.55	66-efr(X)	370.25	$777.20 \pm 1.60$	5.17	71-gol/dob <sup>1)</sup>
493.15	$667.00 \pm 1.50$	-5.94	66-efr(X)	370.35	$776.80 \pm 1.60$	4.84	71-gol/dob <sup>1)</sup>
513.15	$648.00 \pm 1.50$	-8.24	66-efr(X)	373.15	$775.00 \pm 1.60$	5.19	71-gol/dob <sup>1)</sup>
533.15	$629.00 \pm 1.50$	-10.50	66-efr <sup>1)</sup>	383.15	$767.10 \pm 1.50$	5.02	71-gol/dob(X)
553.15	$607.00 \pm 1.50$	-10.86	66-efr(X)	393.15	$759.40 \pm 1.50$	5.13	71-gol/dob(X)
573.15	$585.00 \pm 1.50$	-1.41	66-efr(X)	403.15	$751.20 \pm 1.50$	4.81	71-gol/dob(X)
593.15	$560.00 \pm 1.50$	0.90	66-efr(X)	413.15	$742.80 \pm 1.50$	4.36	71-gol/dob(X)
613.15	$541.00 \pm 1.50$	4.05	66-efr(X)	423.15	$734.10 \pm 1.50$	3.68	71-gol/dob(X)
633.15	$500.00 \pm 2.00$	-7.88	66-efr(X)	424.35	$733.20 \pm 1.50$	3.75	71-gol/dob(X)
653.15	$450.00 \pm 2.00$	2.95	66-efr(X)	424.75	$732.80 \pm 1.50$	3.67	71-gol/dob(X)
663.15	$420.00 \pm 3.00$	30.57	66-efr <sup>1)</sup>	424.85	$732.30 \pm 1.50$	3.25	71-gol/dob(X)

<sup>1)</sup> Not included in Fig. 1.

cont.

## 1-Nonanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
433.15	725.00 ± 1.50	2.66	71-gol/dob(✕)	298.15	824.60 ± 0.30	-0.03	82-ort(◆)
443.15	715.50 ± 1.40	1.29	71-gol/dob(✕)	303.15	821.60 ± 0.30	0.43	82-ort(◆)
453.15	705.80 ± 1.40	-0.23	71-gol/dob(✕)	308.15	818.10 ± 0.30	0.41	82-ort(◆)
463.15	695.00 ± 1.40	-2.81	71-gol/dob(✕)	313.15	814.70 ± 0.30	0.53	82-ort(◆)
473.15	685.00 ± 1.40	-4.55	71-gol/dob(✕)	318.15	811.00 ± 0.30	0.38	82-ort(◆)
473.15	685.80 ± 1.40	-3.75	71-gol/dob(✕)	288.15	831.00 ± 0.40	-0.45	83-rau/ste(✕)
474.45	683.10 ± 1.40	-5.38	71-gol/dob(✕)	298.15	824.40 ± 0.40	-0.23	83-rau/ste <sup>1)</sup>
483.15	673.60 ± 1.30	-7.66	71-gol/dob <sup>1)</sup>	308.15	817.70 ± 0.40	0.01	83-rau/ste <sup>1)</sup>
300.45	823.39 ± 0.40	0.34	73-nay/kud <sup>1)</sup>	318.15	811.10 ± 0.50	0.48	83-rau/ste <sup>1)</sup>
310.27	816.77 ± 0.40	0.57	73-nay/kud(✕)	328.15	804.30 ± 0.50	0.87	83-rau/ste <sup>1)</sup>
320.89	809.11 ± 0.40	0.45	73-nay/kud(✕)	298.15	824.72 ± 0.20	0.09	85-fer/pin(□)
330.83	802.40 ± 0.40	0.91	73-nay/kud <sup>1)</sup>	323.15	806.92 ± 0.10	-0.12	93-gar/ban-1(✕)
340.81	794.57 ± 0.40	0.39	73-nay/kud <sup>1)</sup>	328.15	803.98 ± 0.10	0.55	93-gar/ban-1(✕)
350.02	788.06 ± 0.40	0.72	73-nay/kud <sup>1)</sup>	333.15	799.70 ± 0.10	-0.10	93-gar/ban-1(✕)
359.78	780.30 ± 0.40	0.30	73-nay/kud <sup>1)</sup>	338.15	796.32 ± 0.10	0.19	93-gar/ban-1(✕)
369.70	772.24 ± 0.40	-0.21	73-nay/kud(✕)	343.15	792.34 ± 0.10	-0.11	93-gar/ban-1(✕)
293.15	828.10 ± 0.30	0.04	76-hon/sin(Δ)	348.15	788.36 ± 0.10	-0.37	93-gar/ban-1(✕)
298.15	824.47 ± 0.20	-0.16	79-dia/tar(O)	353.15	785.08 ± 0.10	0.08	93-gar/ban-1(✕)
308.15	817.58 ± 0.20	-0.11	79-dia/tar(O)	358.15	781.10 ± 0.10	-0.13	93-gar/ban-1(✕)
318.15	810.62 ± 0.20	0.00	79-dia/tar(O)	363.15	777.09 ± 0.10	-0.36	93-gar/ban-1(✕)
333.15	799.91 ± 0.20	0.11	79-dia/tar(O)	373.15	769.58 ± 0.10	-0.23	93-gar/ban-1(✕)
293.15	827.70 ± 0.30	-0.36	82-ort(◆)				

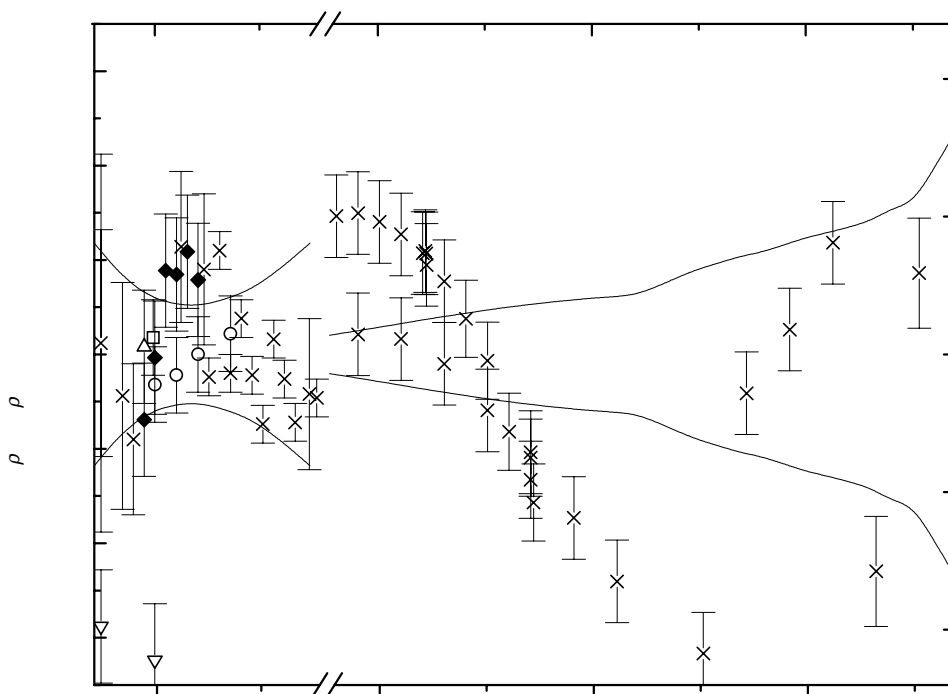
<sup>1)</sup> Not included in Fig. 1.**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	843.49 ± 0.59	400.00	748.88 ± 0.95	550.00	622.37 ± 3.08
280.00	836.92 ± 0.45	410.00	740.95 ± 1.08	560.00	607.28 ± 3.32
290.00	830.20 ± 0.35	420.00	732.95 ± 1.21	570.00	591.31 ± 3.56
293.15	828.06 ± 0.33	430.00	724.89 ± 1.34	580.00	576.25 ± 3.71
298.15	824.63 ± 0.30	440.00	716.78 ± 1.46	590.00	562.92 ± 3.96
300.00	823.36 ± 0.29	450.00	708.62 ± 1.58	600.00	551.28 ± 4.23
310.00	816.39 ± 0.26	460.00	700.41 ± 1.69	610.00	540.44 ± 4.41
320.00	809.30 ± 0.26	470.00	692.16 ± 1.79	620.00	528.74 ± 4.61
330.00	802.09 ± 0.29	480.00	683.88 ± 1.88	630.00	513.76 ± 4.83
340.00	794.77 ± 0.33	490.00	675.56 ± 1.96	640.00	492.33 ± 5.29
350.00	787.35 ± 0.40	500.00	667.23 ± 2.03	650.00	460.27 ± 5.49
360.00	779.84 ± 0.49	510.00	658.88 ± 2.09	660.00	410.90 ± 6.75
370.00	772.22 ± 0.59	520.00	650.51 ± 2.14	670.00	307.42 ± 8.10
380.00	764.52 ± 0.70	530.00	642.14 ± 2.40		
390.00	756.74 ± 0.82	540.00	633.77 ± 2.76		

cont.

**Further references:** [00-ste, 19-beh, 27-ver/coo, 29-mah/das, 33-ano, 37-oli, 42-mul, 48-vog-2, 50-sac/sau, 52-coo, 52-eri-1, 57-gol/kon, 81-sjo/dyh, 85-ort/paz-1, 88-ort/gar, 90-klo/pal, 93-ami/rai, 93-yan/mae, 94-yu /tsa-1].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

## 2-Nonanol

[628-99-9]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

201

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.974$ .

Coefficient	$\rho = A + BT$
$A$	1045.94
$B$	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	847.1 ± 20.0	23.93	06-van <sup>1)</sup>	403.15	730.4 ± 3.0	-9.15	12-pic/ken <sup>1)</sup>
273.15	839.9 ± 1.0	1.55	09-mas	273.15	837.2 ± 1.0	-1.14	32-ell/rei
298.15	823.0 ± 4.0	3.65	10-hal/las <sup>1)</sup>	298.15	819.1 ± 1.0	-0.27	32-ell/rei
293.15	823.0 ± 1.0	-0.15	11-pic/ken				

<sup>1)</sup> Not included in calculation of linear coefficients.

cont.



**2-Nonanol** (cont.)**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	840.7 ± 1.8	293.15	823.1 ± 1.4
280.00	833.1 ± 1.2	298.15	819.3 ± 1.8
290.00	825.5 ± 1.2		

**3-Nonanol**

[624-51-1]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

202

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 1.150$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1068.03
<i>B</i>	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	826.5 ± 2.0	-1.15	13-pic/ken
353.15	779.6 ± 2.0	1.15	13-pic/ken
293.15	819.6 ± 4.0	-8.05	36-tuo <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	830.2 ± 2.9	310.00	813.8 ± 1.9	340.00	789.2 ± 2.0
293.15	827.6 ± 2.7	320.00	805.6 ± 1.7	350.00	781.0 ± 2.5
298.15	823.5 ± 2.4	330.00	797.4 ± 1.7	360.00	772.8 ± 3.1

**4-Nonanol**

[5932-79-6]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

203

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	826.3 ± 1.0	57-shu/bel

**5-nonanol**

[623-93-8]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

204

**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 0.293$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1044.87
<i>B</i>	-0.760

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	823.0 ± 1.0	0.92	06-mal-1	293.15	825.7 ± 2.0	3.62	47-tuo/guy <sup>1)</sup>
289.15	824.4 ± 2.0	-0.72	19-eyk <sup>1)</sup>	293.15	822.0 ± 0.4	-0.08	50-mea/foo
291.15	823.0 ± 1.0	-0.60	23-vav/iva	298.15	818.3 ± 0.4	0.02	50-mea/foo
293.65	835.6 ± 10.0	13.90	42-boe/han <sup>1)</sup>				

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	824.5 ± 0.5
293.15	822.1 ± 0.5
298.15	818.3 ± 0.5

**2,2,3,4-Tetramethyl-3-pentanol**

[29772-39-2]

C<sub>9</sub>H<sub>20</sub>O

MW = 144.26

205

**Table 1.** Fit with estimated  $B$  coefficient for 5 accepted points. Deviation  $\sigma_w = 0.468$ .

Coefficient	$\rho = A + BT$
$A$	1096.61
$B$	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	856.4 ± 1.0	0.18	29-con/bla	293.15	856.5 ± 0.6	0.28	47-how/mea
293.15	856.0 ± 1.0	-0.22	33-whi/lau	298.15	852.3 ± 0.6	0.18	47-how/mea
288.15	862.2 ± 2.0	1.88	36-naz <sup>1)</sup>	293.15	855.0 ± 1.0	-1.22	48-cad/foo

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	858.8 ± 0.8
293.15	856.2 ± 0.8
298.15	852.1 ± 0.8

**2,2,3-Trimethyl-3-hexanol** [5340-41-0] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 206

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	846.4 ± 1.0	43-geo
293.15	848.5 ± 2.0	48-ruo <sup>1)</sup>
293.15	846.3 ± 1.0	55-pet/sus
293.15	846.0 ± 1.0	61-mar/pet
293.15	846.2 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,3,4-Trimethyl-2-hexanol** [21102-13-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 207

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	835.3 ± 1.0	35-col-1

**2,3,5-Trimethyl-3-hexanol** [65927-60-8] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 208

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	825.6 ± 3.0	33-mey/tuo <sup>1)</sup>
293.15	831.2 ± 2.0	59-pet/zak-1
293.15	831.2 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,4,4-Trimethyl-2-hexanol** [66793-91-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 209

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	847.5 ± 1.0	40-mos

**2,4,4-Trimethyl-3-hexanol** [66793-92-8] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 210

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	848.8 ± 1.0	48-ruo

**2,5,5-Trimethyl-3-hexanol** [66793-72-4] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 211

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	825.0 ± 1.0	42-whi/for

**3,4,4-Trimethyl-3-hexanol** [66793-74-6] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 212

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
294.15	832.3 ± 2.0	06-kon/mil

**3,5,5-Trimethyl-1-hexanol** [3452-97-9] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 213

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	823.6 ± 1.0	49-bru

**3,5,5-Trimethyl-3-hexanol** [66810-87-5] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 214

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	835.0 ± 0.5	47-how/mea

**4,5,5-Trimethyl-1-hexanol** [66793-75-7] C<sub>9</sub>H<sub>20</sub>O MW = 144.26 215

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	846.0 ± 1.0	61-mar/pet



2.1.6 Alkanols, C<sub>10</sub>

**2-Butyl-1-hexanol** [2768-15-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 216

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
289.15	836.0 ± 3.0	16-lev/all

**1-Decanol** [112-30-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 217

$$T_c = 687.10 \text{ K [89-tej/lee]} \quad \rho_c = 264.00 \text{ kg}\cdot\text{m}^{-3} \text{ [89-tej/lee]}$$

**Table 1.** Coefficients for the polynomial expansion equations. Standard deviations (see introduction):  $\sigma_T = 4.3461 \cdot 10^{-1}$  (low temperature range),  $\sigma_{c,w} = (2.6342 \cdot 10^{-1})$  (combined temperature ranges, weighted),  $\sigma_{c,uw} = 3.3635 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 279.63 \text{ to } 550.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$	$T = 550.00 \text{ to } 687.10 \text{ K}$ $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)]$ $[\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$
A	$1.01735 \cdot 10^3$	1.30964
B	$-6.79957 \cdot 10^{-1}$	$-1.59285 \cdot 10^{-2}$
C	$3.98783 \cdot 10^{-4}$	$5.30923 \cdot 10^{-5}$
D	$-8.88242 \cdot 10^{-7}$	$7.66905 \cdot 10^{-9}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
280.15	838.90 ± 1.00	0.27	1883-kra <sup>1)</sup>	413.15	738.70 ± 0.64	-3.16	58-cos/bow(X)
293.15	829.70 ± 1.00	-0.22	1883-kra <sup>1)</sup>	433.15	722.40 ± 0.66	-3.06	58-cos/bow(X)
371.85	773.40 ± 1.00	-0.58	1883-kra(X)	453.15	705.30 ± 0.68	-3.17	58-cos/bow(X)
293.10	830.10 ± 0.29	0.15	55-kus <sup>1)</sup>	473.15	688.30 ± 0.70	-2.52	58-cos/bow(X)
298.10	826.90 ± 0.30	0.33	55-kus <sup>1)</sup>	493.15	670.80 ± 0.72	-1.69	58-cos/bow(X)
303.10	823.50 ± 0.30	0.34	55-kus <sup>1)</sup>	513.15	653.50 ± 1.00	0.08	58-cos/bow(X)
313.10	816.80 ± 0.32	0.51	55-kus <sup>1)</sup>	533.15	635.00 ± 1.00	1.42	58-cos/bow(X)
323.10	810.00 ± 0.34	0.67	55-kus <sup>1)</sup>	553.15	612.70 ± 1.00	-0.35	58-cos/bow(X)
333.10	802.70 ± 0.36	0.42	55-kus <sup>1)</sup>	293.15	829.70 ± 1.50	-0.22	66-efr <sup>1)</sup>
343.10	795.40 ± 0.38	0.27	55-kus(X)	313.15	816.20 ± 1.50	-0.05	66-efr <sup>1)</sup>
353.10	788.10 ± 0.39	0.22	55-kus(X)	333.15	802.20 ± 1.50	-0.04	66-efr <sup>1)</sup>
358.10	784.20 ± 0.40	-0.01	55-kus(X)	353.15	787.60 ± 1.50	-0.24	66-efr <sup>1)</sup>
293.15	826.00 ± 0.52	-3.92	58-cos/bow <sup>1)</sup>	373.15	772.40 ± 1.50	-0.60	66-efr <sup>1)</sup>
313.15	812.70 ± 0.54	-3.55	58-cos/bow <sup>1)</sup>	393.15	757.20 ± 1.50	-0.49	66-efr(X)
333.15	799.80 ± 0.56	-2.44	58-cos/bow <sup>1)</sup>	413.15	741.40 ± 1.50	-0.46	66-efr(X)
353.15	785.80 ± 0.58	-2.04	58-cos/bow <sup>1)</sup>	433.15	727.50 ± 1.50	2.04	66-efr <sup>1)</sup>
373.15	770.50 ± 0.60	-2.50	58-cos/bow(X)	453.15	707.20 ± 1.50	-1.27	66-efr <sup>1)</sup>
393.15	755.00 ± 0.62	-2.69	58-cos/bow(X)	473.15	694.00 ± 1.50	3.18	66-efr <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

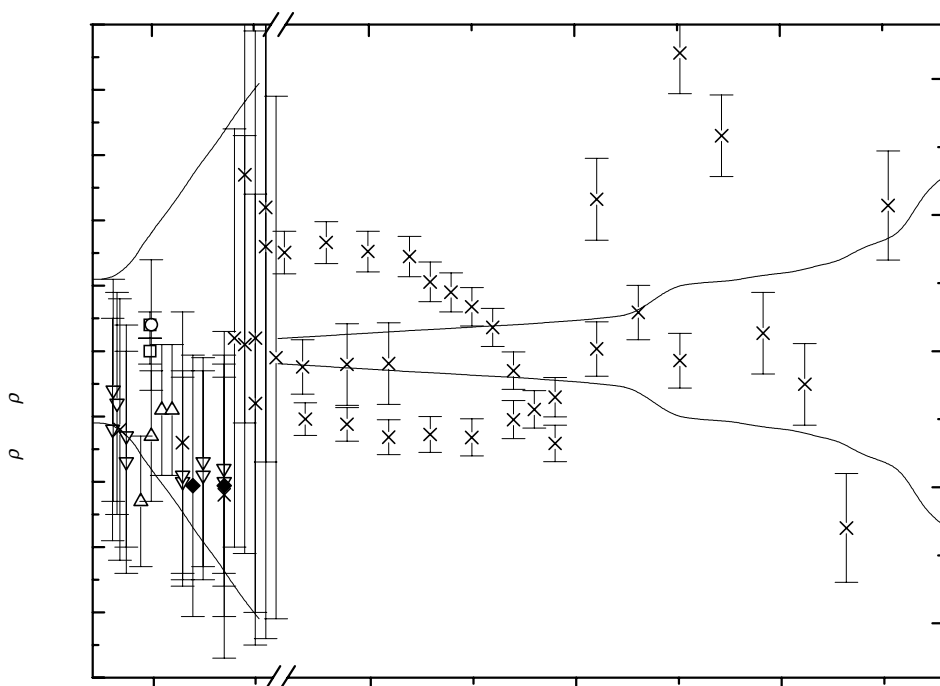
cont.

**1-Decanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
493.15	675.00 ± 1.50	2.51	66-efr <sup>1)</sup>	303.15	823.20 ± 0.33	0.07	89-mat/mak-1 <sup>1)</sup>
513.15	659.00 ± 1.50	5.58	66-efr(×)	308.15	819.70 ± 0.33	-0.00	89-mat/mak-1 <sup>1)</sup>
533.15	643.00 ± 1.50	9.42	66-efr <sup>1)</sup>	313.15	816.30 ± 0.33	0.05	89-mat/mak-1 <sup>1)</sup>
553.15	624.00 ± 1.50	10.95	66-efr(×)	318.15	812.80 ± 0.33	0.01	89-mat/mak-1 <sup>1)</sup>
573.15	605.00 ± 1.50	7.91	66-efr(×)	323.15	809.30 ± 0.32	0.01	89-mat/mak-1 <sup>1)</sup>
593.15	584.00 ± 1.50	0.66	66-efr(×)	323.15	809.40 ± 0.49	0.11	89-mat/mak-1 <sup>1)</sup>
613.15	564.00 ± 1.50	-1.22	66-efr(×)	328.15	805.90 ± 0.32	0.12	89-mat/mak-1 <sup>1)</sup>
633.15	530.00 ± 2.00	-6.50	66-efr(×)	333.15	802.30 ± 0.32	0.06	89-mat/mak-1 <sup>1)</sup>
653.15	496.00 ± 2.00	5.35	66-efr(×)	338.15	798.70 ± 0.32	0.02	89-mat/mak-1(×)
673.15	450.00 ± 3.00	33.09	66-efr <sup>1)</sup>	343.15	795.10 ± 0.32	0.01	89-mat/mak-1(×)
279.63	838.86 ± 0.17	-0.12	73-fin(∇)	348.15	791.50 ± 0.47	0.02	89-mat/mak-1(×)
279.85	838.77 ± 0.17	-0.06	73-fin(∇)	348.15	791.40 ± 0.32	-0.08	89-mat/mak-1(×)
281.69	837.53 ± 0.17	-0.08	73-fin(∇)	283.15	834.30 ± 0.83	-2.33	90-apa/gyl <sup>1)</sup>
286.12	834.51 ± 0.17	-0.13	73-fin(∇)	293.15	828.40 ± 0.83	-1.52	90-apa/gyl <sup>1)</sup>
286.15	834.45 ± 0.17	-0.17	73-fin(∇)	303.15	822.60 ± 0.82	-0.53	90-apa/gyl <sup>1)</sup>
293.15	829.73 ± 0.17	-0.19	73-fin <sup>1)</sup>	323.15	811.10 ± 0.81	1.81	90-apa/gyl <sup>1)</sup>
293.16	829.73 ± 0.17	-0.18	73-fin <sup>1)</sup>	343.15	798.20 ± 0.80	3.11	90-apa/gyl <sup>1)</sup>
303.14	822.94 ± 0.16	-0.19	73-fin <sup>1)</sup>	363.15	784.10 ± 0.78	3.62	90-apa/gyl(×)
313.13	816.07 ± 0.16	-0.20	73-fin(∇)	383.15	769.40 ± 0.77	3.99	90-apa/gyl(×)
313.15	816.06 ± 0.16	-0.19	73-fin(∇)	403.15	753.50 ± 0.75	3.66	90-apa/gyl(×)
323.08	809.17 ± 0.16	-0.17	73-fin(∇)	423.15	737.20 ± 0.74	3.47	90-apa/gyl(×)
323.09	809.15 ± 0.16	-0.19	73-fin(∇)	433.15	728.00 ± 0.73	2.54	90-apa/gyl(×)
333.14	802.07 ± 0.16	-0.18	73-fin(∇)	443.15	719.20 ± 0.72	2.16	90-apa/gyl(×)
333.16	802.04 ± 0.16	-0.20	73-fin(∇)	453.15	710.10 ± 0.71	1.63	90-apa/gyl(×)
293.15	829.69 ± 0.10	-0.23	78-jel/leo(Δ)	463.15	700.60 ± 0.70	0.87	90-apa/gyl(×)
298.15	826.40 ± 0.10	-0.13	78-jel/leo(Δ)	473.15	690.10 ± 0.69	-0.72	90-apa/gyl(×)
303.15	823.04 ± 0.10	-0.09	78-jel/leo(Δ)	483.15	679.60 ± 0.68	-2.14	90-apa/gyl(×)
308.15	819.61 ± 0.10	-0.09	78-jel/leo(Δ)	493.15	669.10 ± 0.67	-3.39	90-apa/gyl(×)
298.15	826.23 ± 0.20	-0.30	79-dia/tar <sup>1)</sup>	288.15	833.90 ± 0.60	0.62	92-lie/sen-1 <sup>1)</sup>
308.15	819.46 ± 0.20	-0.24	79-dia/tar <sup>1)</sup>	293.15	830.20 ± 0.60	0.28	92-lie/sen-1 <sup>1)</sup>
318.15	812.58 ± 0.20	-0.21	79-dia/tar(◆)	298.15	827.00 ± 0.60	0.47	92-lie/sen-1 <sup>1)</sup>
333.15	802.03 ± 0.20	-0.21	79-dia/tar(◆)	303.15	823.70 ± 0.60	0.57	92-lie/sen-1 <sup>1)</sup>
298.15	826.57 ± 0.02	0.04	79-kiy/ben(×)	308.15	820.10 ± 0.60	0.40	92-lie/sen-1 <sup>1)</sup>
298.15	826.53 ± 0.02	-0.00	81-ben/han(□)	313.15	816.40 ± 0.60	0.15	92-lie/sen-1 <sup>1)</sup>
298.15	826.57 ± 0.10	0.04	85-kum/ben(O)	318.15	812.90 ± 0.60	0.11	92-lie/sen-1 <sup>1)</sup>
283.15	836.51 ± 0.20	-0.12	86-hei/sch(×)	323.15	809.50 ± 0.60	0.21	92-lie/sen-1 <sup>1)</sup>
298.15	826.40 ± 0.20	-0.13	86-hei/sch <sup>1)</sup>	328.15	805.80 ± 0.60	0.02	92-lie/sen-1 <sup>1)</sup>
313.15	816.11 ± 0.20	-0.14	86-hei/sch(×)	333.15	802.40 ± 0.60	0.16	92-lie/sen-1 <sup>1)</sup>
293.15	829.82 ± 0.25	-0.10	86-wag/hei <sup>1)</sup>	338.15	798.80 ± 0.60	0.12	92-lie/sen-1 <sup>1)</sup>
298.15	826.44 ± 0.25	-0.09	86-wag/hei <sup>1)</sup>	343.15	795.20 ± 0.60	0.11	92-lie/sen-1 <sup>1)</sup>
333.15	802.02 ± 0.25	-0.22	86-wag/hei(×)	348.15	791.60 ± 0.60	0.12	92-lie/sen-1 <sup>1)</sup>
298.15	826.60 ± 0.33	0.07	89-mat/mak-1 <sup>1)</sup>	353.15	788.00 ± 0.60	0.16	92-lie/sen-1(×)
298.15	826.80 ± 0.50	0.27	89-mat/mak-1 <sup>1)</sup>				

<sup>1)</sup> Not included in Fig. 1.

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	845.35 ± 0.11	400.00	752.33 ± 0.64	550.00	616.23 ± 2.38
280.00	838.73 ± 0.11	410.00	744.39 ± 0.69	560.00	606.90 ± 2.49
290.00	832.04 ± 0.14	420.00	736.31 ± 0.74	570.00	599.28 ± 2.54
293.15	829.92 ± 0.16	430.00	728.09 ± 0.78	580.00	592.47 ± 2.60
298.15	826.53 ± 0.18	440.00	719.71 ± 0.82	590.00	585.63 ± 2.76
300.00	825.27 ± 0.19	450.00	711.19 ± 0.87	600.00	577.94 ± 2.84
310.00	818.43 ± 0.23	460.00	702.50 ± 0.91	610.00	568.62 ± 2.94
320.00	811.50 ± 0.28	470.00	693.64 ± 0.95	620.00	556.89 ± 3.16
330.00	804.47 ± 0.32	480.00	684.62 ± 1.00	630.00	541.98 ± 3.30
340.00	797.36 ± 0.37	490.00	675.42 ± 1.05	640.00	523.10 ± 3.79
350.00	790.14 ± 0.41	500.00	666.04 ± 1.11	650.00	499.33 ± 4.03
360.00	782.81 ± 0.46	510.00	656.47 ± 1.17	660.00	469.47 ± 4.35
370.00	775.37 ± 0.51	520.00	646.71 ± 1.25	670.00	431.35 ± 5.79
380.00	767.81 ± 0.55	530.00	636.76 ± 1.34	680.00	378.50 ± 6.41
390.00	760.14 ± 0.60	540.00	626.60 ± 1.85		

cont.



**1-Decanol** (cont.)

**Further references:** [09-sch-1, 27-ver/coo, 48-jon/bow, 48-vog-2, 48-wei, 50-sac/sau, 56-rat/cur, 68-pfl/pop, 68-sin/ben, 69-smi/kur, 78-ast, 78-tre/ben, 81-kiy/ben, 81-sjo/dyh, 81-tre/kiy, 82-ort, 82-tre/han, 83-gop/rao, 83-rau/ste, 84-kum/ben, 85-fer/pin, 85-ort/paz-1, 86-dew/meh, 87-dew/meh, 88-ort/gar, 89-dew/gup, 93-yan/mae, 94-yu /tsa-1].

**2-Decanol** [1120-06-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 218

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	825.0 ± 1.0	11-pic/ken
293.15	824.9 ± 1.0	59-asi/gei
293.15	825.6 ± 1.0	60-kor/pet
293.15	825.2 ± 1.0	Recommended

**3-Decanol** [1565-81-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 219

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.283$ .

Coefficient	$\rho = A + BT$
A	1055.46
B	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	827.2 ± 1.0	0.40	13-pic/ken
353.15	779.8 ± 1.0	-0.20	13-pic/ken
293.15	826.6 ± 1.0	-0.20	59-asi/gei

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	829.3 ± 1.5	310.00	813.7 ± 1.0	340.00	790.3 ± 1.6
293.15	826.8 ± 1.4	320.00	805.9 ± 1.0	350.00	782.5 ± 2.1
298.15	822.9 ± 1.2	330.00	798.1 ± 1.3	360.00	774.7 ± 2.5

**4-Decanol** [2051-31-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 220

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	826.2 ± 2.0	57-pet/nef-1
293.15	823.8 ± 2.0	59-asi/gei
293.15	825.0 ± 2.2	Recommended

**5-Decanol** [5205-34-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 221

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.221$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1047.15
<i>B</i>	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	827.6 ± 3.0	3.29	56-gol/kon <sup>1)</sup>
293.15	823.8 ± 1.0	-0.55	59-asi/gei
298.15	820.6 ± 0.4	0.09	88-cac/cos

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	826.7 ± 0.6
293.15	824.4 ± 0.5
298.15	820.6 ± 0.5

**2,2-Dimethyl-4-ethyl-3-hexanol** [66719-47-9] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 222

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	833.9 ± 1.0	41-whi/whi

**2,4-Dimethyl-4-ethyl-3-hexanol** [66719-48-0] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 223

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	860.6 ± 2.0	53-sok

**5,5-Dimethyl-2-ethyl-1-hexanol** [66719-49-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 224

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	838.6 ± 1.0	56-gol/kon

**5,5-Dimethyl-3-ethyl-3-hexanol** [5340-62-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 225

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	842.2 ± 1.0	34-sta
293.15	845.0 ± 2.0	42-whi/for
293.15	842.8 ± 1.4	Recommended

**2,4-Dimethyl-3-(1-methylethyl)-3-pentanol** [51200-83-0] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 226

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.050$ .

Coefficient	$\rho = A + BT$
$A$	1097.67
$B$	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	874.0 ± 2.0	10.85	44-you/rob <sup>1)</sup>
292.15	861.6 ± 2.0	-2.35	46-vav/col <sup>1)</sup>
293.15	863.2 ± 0.6	0.05	47-how/mea
298.15	859.1 ± 0.6	-0.05	47-how/mea

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	865.7 ± 0.4
293.15	863.1 ± 0.3
298.15	859.1 ± 0.3

**2,4-Dimethyl-3-propyl-3-pentanol** [500001-19-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 227

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.262$ .

Coefficient	$\rho = A + BT$
$A$	1088.19
$B$	-0.800

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	853.9 ± 1.0	0.23	26-sta
273.15	869.3 ± 1.0	-0.37	26-sta
303.15	845.8 ± 1.0	0.13	26-sta

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	872.2 ± 2.2	290.00	856.2 ± 0.9	298.15	849.7 ± 1.3
280.00	864.2 ± 1.4	293.15	853.7 ± 1.0	310.00	840.2 ± 2.2

**1,1-Dimethyl-1-octanol** [10297-57-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 228

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	807.8 ± 1.0	64-tis/sta

**2,2-Dimethyl-1-octanol** [2370-14-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 229

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	830.0 ± 1.0	64-blo/hag
293.15	843.0 ± 2.0	65-shu/puz <sup>1)</sup>
293.15	830.0 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,2-Dimethyl-4-octanol** [66719-52-6] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 230

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	821.2 ± 1.0	38-whi/pop-1

**2,3-Dimethyl-3-octanol** [19781-10-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 231

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.150$ .

Coefficient	$\rho = A + BT$
$A$	1069.53
$B$	-0.820

cont.

**2,3-Dimethyl-3-octanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	840.1 ± 6.0	10.95	33-whi/eve <sup>1)</sup>
293.15	829.3 ± 0.6	0.15	50-mea/foo
298.15	824.9 ± 0.6	-0.15	50-mea/foo

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	831.7 ± 0.7
293.15	829.2 ± 0.5
298.15	825.1 ± 0.5

**2,4-Dimethyl-2-octanol** [18675-20-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 232**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	825.7 ± 2.0	48-naz/tor

**2,4-Dimethyl-4-octanol** [33933-79-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 233**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	823.8 ± 1.0	33-mey/tuo	293.15	822.7 ± 1.0	59-pet/zak
293.15	823.6 ± 1.0	58-sok/kra	293.15	822.7 ± 1.0	59-pet/zak-1
293.15	832.8 ± 6.0	59-nog/dza <sup>1)</sup>	293.15	823.2 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**2,5-Dimethyl-4-octanol** [66719-53-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 234**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	821.5 ± 0.8	12-bje

**2,6-Dimethyl-1-octanol** [62417-08-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 235**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
291.15	830.0 ± 2.0	14-vav

**2,6-Dimethyl-2-octanol** [18479-57-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 236**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	802.3 ± 10.0	53-sut <sup>1)</sup>
293.15	833.5 ± 5.0	57-naz/kra <sup>1)</sup>
293.15	826.0 ± 2.0	59-hou/lev <sup>1)</sup>
293.15	827.3 ± 1.0	64-ohl/sei
293.15	827.3 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**2,7-Dimethyl-1-octanol** [15250-22-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 237**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
288.15	830.3 ± 1.0	40-pal

**2,7-Dimethyl-2-octanol** [42007-73-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 238**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 7.1829 \cdot 10^{-2}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 1.9108 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

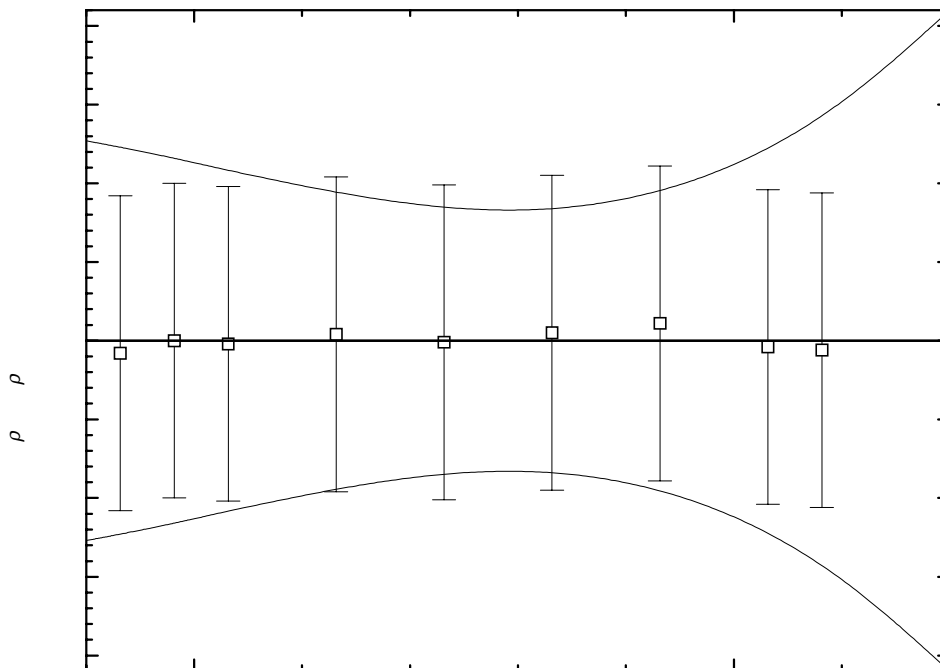
Coefficient	$T = 293.15$ to $358.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.06429 \cdot 10^3$
B	$-8.15665 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	825.10 ± 1.00	-0.08	55-kus(□)	333.15	792.60 ± 1.00	0.05	55-kus(□)
298.15	821.10 ± 1.00	0.00	55-kus(□)	343.15	784.50 ± 1.00	0.11	55-kus(□)
303.15	817.00 ± 1.00	-0.02	55-kus(□)	353.15	776.20 ± 1.00	-0.04	55-kus(□)
313.15	808.90 ± 1.00	0.04	55-kus(□)	358.15	772.10 ± 1.00	-0.06	55-kus(□)
323.15	800.70 ± 1.00	-0.01	55-kus(□)				

cont.

## 2,7-Dimethyl-2-octanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	827.75 ± 1.27	310.00	811.43 ± 0.98	350.00	778.81 ± 1.09
293.15	825.18 ± 1.23	320.00	803.28 ± 0.86	360.00	770.65 ± 1.48
298.15	821.10 ± 1.16	330.00	795.12 ± 0.81	370.00	762.49 ± 2.10
300.00	819.59 ± 1.13	340.00	786.96 ± 0.88		

## 2,7-Dimethyl-3-octanol

[66719-55-9]

C<sub>10</sub>H<sub>22</sub>O

MW = 158.28

239

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	815.2 ± 2.0	12-mic

**2,7-Dimethyl-4-octanol** [19781-11-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 240

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	814.0 ± 2.0	36-tuo <sup>1)</sup>
293.15	818.3 ± 1.0	44-pow/hag
293.15	818.3 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,5-Dimethyl-3-octanol** [56065-42-0] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 241

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	837.0 ± 2.0	59-col/gau

**3,6-Dimethyl-3-octanol** [151-19-9] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 242

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.15	834.7 ± 2.0	13-dup

**3,7-Dimethyl-1-octanol** [106-21-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 243

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
291.15	838.0 ± 2.0	23-von/kai <sup>1)</sup>	296.15	828.1 ± 3.0	54-rin/ari <sup>1)</sup>
293.15	831.0 ± 3.0	24-lon/mar <sup>1)</sup>	293.15	840.2 ± 1.5	58-leb/kuk
284.15	837.4 ± 3.0	28-esc <sup>1)</sup>	293.15	828.6 ± 3.0	60-por/far <sup>1)</sup>
288.15	830.0 ± 6.0	40-pal <sup>1)</sup>	294.15	840.0 ± 2.0	61-yeh <sup>1)</sup>
293.15	835.7 ± 3.0	51-sor/suc <sup>1)</sup>	293.15	840.9 ± 1.5	63-yeh
291.15	837.0 ± 3.0	52-ino <sup>1)</sup>	293.15	840.6 ± 1.5	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,7-Dimethyl-2-octanol** [15340-96-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 244

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	829.1 ± 1.0	56-nav/des



**3,7-Dimethyl-3-octanol** [78-69-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 245**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	828.0 ± 2.0	14-wal-1
298.15	864.7 ± 20.0	39-ste/mcn <sup>1)</sup>
292.15	833.9 ± 3.0	40-pal <sup>1)</sup>
293.15	829.5 ± 2.0	58-naz/gus
293.15	828.7 ± 2.1	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**4,6-Dimethyl-4-octanol** [56065-43-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 246**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
301.15	825.8 ± 1.0	60-tha/vas

**4,7-Dimethyl-4-octanol** [19781-13-6] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 247**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
273.15	842.1 ± 2.0	12-gue-1

**3-Ethyl-2-methyl-3-heptanol** [66719-37-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 248**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	845.5 ± 2.0	15-wal-3

**3-Ethyl-6-methyl-3-heptanol** [66719-40-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 249**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 0.056$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1065.11
<i>B</i>	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
273.15	852.0 ± 1.5	-0.06	04-gri
283.55	844.0 ± 1.5	0.06	04-gri
273.15	852.0 ± 1.5	-0.06	04-gri-1
283.55	844.0 ± 1.5	0.06	04-gri-1

cont.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	854.5 ± 1.5
280.00	846.7 ± 1.3
290.00	838.9 ± 1.6

**5-Ethyl-4-methyl-3-heptanol** [66731-94-0] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 250

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.15	865.0 ± 2.0	43-col/jol

**1-3-Ethyl-1-octanol** [90002-57-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 251

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
295.15	833.0 ± 2.0	31-lev/mar-3

**3-Ethyl-3-octanol** [2051-32-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 252

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	836.1 ± 1.0	33-whi/wil

**4-Ethyl-4-octanol** [38395-42-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 253

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 2.1329 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 9.5387 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.07866 \cdot 10^3$
B	$-8.43628 \cdot 10^{-1}$

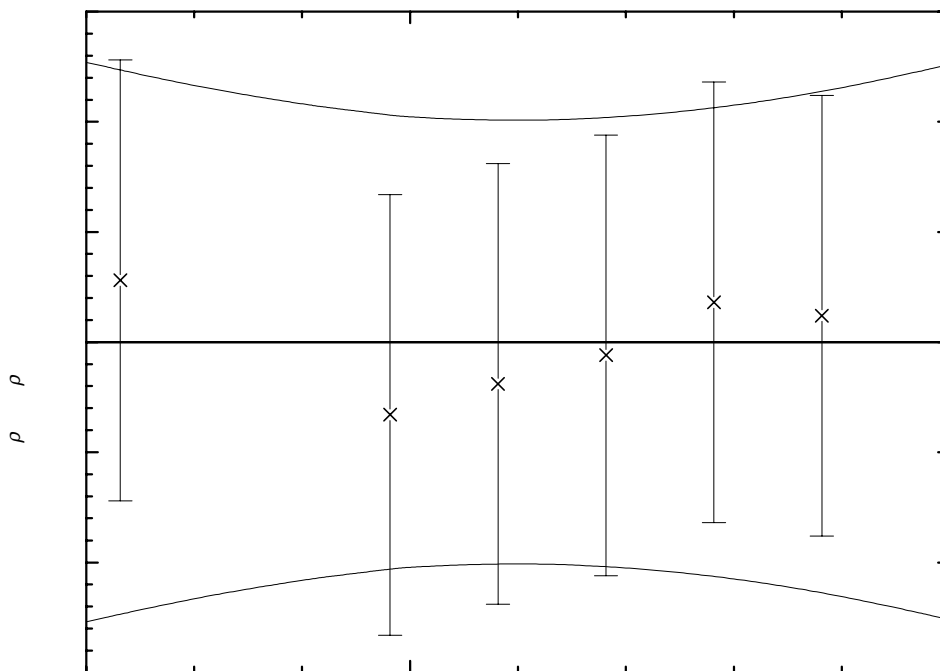
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	848.50 ± 1.00	0.28	39-owe/qua(✗)	318.15	810.20 ± 1.00	-0.06	39-owe/qua(✗)
298.15	826.80 ± 1.00	-0.33	39-owe/qua(✗)	328.15	802.00 ± 1.00	0.18	39-owe/qua(✗)
308.15	818.50 ± 1.00	-0.19	39-owe/qua(✗)	338.15	793.50 ± 1.00	0.12	39-owe/qua(✗)

cont.

**4-Ethyl-4-octanol** (cont.)

Further references: [33-whi/woo].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	850.88 ± 1.27	298.15	827.13 ± 1.03	330.00	800.26 ± 1.07
280.00	842.44 ± 1.16	300.00	825.57 ± 1.02	340.00	791.82 ± 1.15
290.00	834.00 ± 1.08	310.00	817.13 ± 1.00	350.00	783.39 ± 1.26
293.15	831.35 ± 1.06	320.00	808.70 ± 1.02		

**6-Ethyl-3-octanol**

[19781-27-2]

C<sub>10</sub>H<sub>22</sub>O

MW = 158.28

254

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
297.65	839.6 ± 0.5	36-pow/bal

**3-Ethyl-2,2,4-trimethyl-3-pentanol** [66256-41-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 255

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
292.15	862.8 ± 1.5	36-naz <sup>1)</sup>
293.15	862.0 ± 1.0	51-smi/cre
293.15	862.8 ± 1.0	54-mos/cox
293.15	862.4 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Methyl-3-(1-methylethyl)-3-hexanol** [51200-81-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 256

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	853.7 ± 2.0	26-sta
293.15	855.4 ± 3.0	43-geo <sup>1)</sup>
293.15	850.4 ± 1.0	48-cad/foo
293.15	851.1 ± 1.2	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**5-Methyl-2-(1-methylethyl)-1-hexanol** [2051-33-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 257

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	832.2 ± 2.0	25-ter <sup>1)</sup>
290.15	836.6 ± 1.0	47-sch/sch
290.15	836.6 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**4-Methyl-2-(2-methylpropyl)-1-pentanol** [22417-45-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 258

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
277.15	846.0 ± 2.0	04-bou/bla
273.15	846.0 ± 2.0	10-fre

**2-Methyl-1-nonanol** [40589-14-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 259

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.350$ .

Coefficient	$\rho = A + BT$
$A$	1058.41
$B$	-0.780

cont.

**2-Methyl-1-nonanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
273.15	845.7 ± 2.0	0.35	02-gue
288.15	833.3 ± 2.0	-0.35	02-gue

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	847.8 ± 2.1
280.00	840.0 ± 1.8
290.00	832.2 ± 2.0

**2-Methyl-3-nonanol**

[26533-33-5]

C<sub>10</sub>H<sub>22</sub>O

MW = 158.28

260

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.309$ .

Coefficient	$\rho = A + BT$
$A$	1051.17
$B$	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	829.0 ± 1.0	0.63	12-pic/ken
293.15	828.7 ± 1.0	0.33	48-pet/old
293.15	828.1 ± 0.6	-0.27	50-mea/foo
298.15	824.5 ± 0.6	-0.07	50-mea/foo

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	830.8 ± 0.8
293.15	828.4 ± 0.8
298.15	824.6 ± 0.8

**2-Methyl-4-nonanol**

[26533-31-3]

C<sub>10</sub>H<sub>22</sub>O

MW = 158.28

261

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	820.0 ± 2.0	54-dub/luf

**2-Methyl-5-nonanol** [29843-62-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 262

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	821.5 ± 1.0	44-pow/hag

**3-Methyl-1-nonanol** [22663-64-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 263

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	834.2 ± 3.0	22-lev/tay-1 <sup>1)</sup>
296.15	837.0 ± 2.0	31-lev/mar-5
296.15	837.0 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**(R)-3-Methyl-1-nonanol** [86414-45-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 264

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	829.0 ± 2.0	58-leg/ulr

**3-Methyl-2-nonanol** [60671-32-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 265

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.15	845.0 ± 3.0	35-gre-2 <sup>1)</sup>
293.15	835.3 ± 2.0	57-pet/nef-1
293.15	835.3 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Methyl-3-nonanol** [21078-72-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 266

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 1.0876$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 6.1414 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

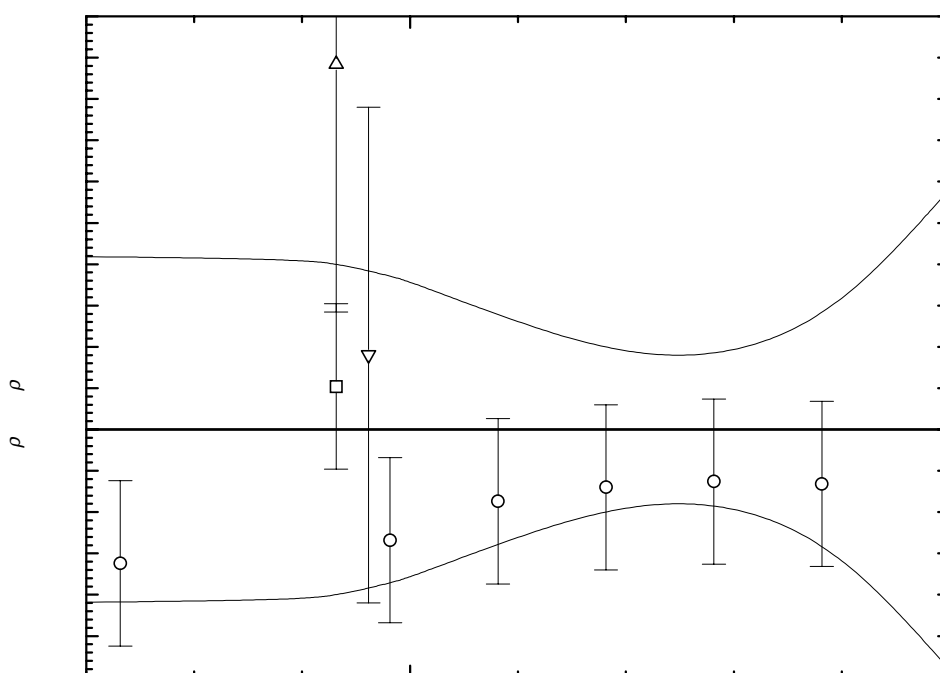
Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.07303 \cdot 10^3$
B	$-8.27037 \cdot 10^{-1}$

cont.

## 3-Methyl-3-nonanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
296.15	829.00 ± 3.00	0.90	35-gre-2(∇)	318.15	809.20 ± 1.00	-0.70	39-owe/qua(○)
293.15	831.10 ± 1.00	0.52	38-whi/ore(□)	328.15	801.00 ± 1.00	-0.63	39-owe/qua(○)
273.15	845.50 ± 1.00	-1.62	39-owe/qua(○)	338.15	792.70 ± 1.00	-0.66	39-owe/qua(○)
298.15	825.10 ± 1.00	-1.34	39-owe/qua(○)	293.15	835.00 ± 3.00	4.42	61-sok/she(Δ)
308.15	817.30 ± 1.00	-0.87	39-owe/qua(○)				

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	849.73 ± 2.09	298.15	826.44 ± 1.86	330.00	800.10 ± 0.87
280.00	841.46 ± 2.08	300.00	824.91 ± 1.79	340.00	791.83 ± 1.44
290.00	833.19 ± 2.05	310.00	816.64 ± 1.29	350.00	783.56 ± 2.91
293.15	830.58 ± 2.01	320.00	808.37 ± 0.89		

***d*-3-Methyl-5-nonanol** [500021-26-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 267

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	821.0 ± 2.0	50-let/tra

**4-Methyl-1-nonanol** [1489-47-0] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 268

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
300.15	826.0 ± 2.0	31-lev/mar-5

**4-Methyl-4-nonanol** [23418-38-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 269

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.047$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1071.65
<i>B</i>	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
298.15	824.5 ± 2.0	-2.67	33-whi/wil <sup>1)</sup>
298.15	827.1 ± 1.0	-0.07	44-qua/sma
318.15	810.8 ± 1.0	0.03	44-qua/sma
328.15	802.6 ± 1.0	0.03	44-qua/sma

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	833.8 ± 1.4	298.15	827.2 ± 1.1	320.00	809.2 ± 0.7
293.15	831.3 ± 1.3	310.00	817.4 ± 0.7	330.00	801.0 ± 1.0

**5-Methyl-1-nonanol** [2768-16-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 270

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
297.15	831.0 ± 2.0	33-lev/mar-1



**5-Methyl-4-nonanol** [66719-44-6] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 271

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
300.15	826.0 ± 2.0	48-pow/nie

**5-Methyl-5-nonanol** [33933-78-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 272

**Table 1.** Fit with estimated  $B$  coefficient for 5 accepted points. Deviation  $\sigma_w = 0.264$ .

Coefficient	$\rho = A + BT$
$A$	1063.90
$B$	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg·m <sup>-3</sup>	kg·m <sup>-3</sup>		K	kg·m <sup>-3</sup>	kg·m <sup>-3</sup>	
293.15	829.0 ± 1.0	-0.38	33-whi/woo	328.15	801.3 ± 1.0	-0.08	44-qua/sma
298.15	825.3 ± 1.0	-0.08	33-whi/woo	318.15	809.5 ± 1.0	0.12	44-qua/sma
298.15	825.8 ± 1.0	0.42	44-qua/sma	293.15	830.5 ± 2.0	1.12	59-yur/bel <sup>1)</sup>

<sup>1)</sup> Not included in calculation of recommended value.

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg·m <sup>-3</sup>	K	kg·m <sup>-3</sup>	K	kg·m <sup>-3</sup>
290.00	831.9 ± 1.2	298.15	825.4 ± 0.9	320.00	807.9 ± 1.0
293.15	829.4 ± 1.1	310.00	815.9 ± 0.8	330.00	799.9 ± 1.4

**6-Methyl-2-nonanol** [66256-60-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 273

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	833.2 ± 1.0	61-shv/pet

**7-Methyl-1-nonanol** [33234-93-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 274

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	828.2 ± 1.0	62-lar/sal

**L(+)-7-Methyl-1-nonanol** [500006-91-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 275

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	828.2 ± 0.6	62-lar/sal

**3-(1-Methylethyl)-1-heptanol** [38514-15-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 276

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
303.15	834.1 ± 1.0	57-kit

**4-(1-Methylethyl)-4-heptanol** [51200-82-9] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 277

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.713$ .

Coefficient	$\rho = A + BT$
$A$	1067.93
$B$	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	844.9 ± 2.0	-0.23	26-sta
273.15	859.6 ± 2.0	-0.73	26-sta
303.15	838.5 ± 2.0	0.97	26-sta
293.15	847.1 ± 3.0	1.97	54-naz/kak-3 <sup>1)</sup>

<sup>1)</sup> Not included in calculation of recommended value.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	862.7 ± 2.5	290.00	847.5 ± 1.5	298.15	841.3 ± 1.7
280.00	855.1 ± 1.8	293.15	845.1 ± 1.6	310.00	832.3 ± 2.5

**2-(1-Methylpropyl)-3-methyl-1-pentanol** [91717-78-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 278

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
295.15	835.0 ± 2.0	62-thi

**2-Propyl-1-heptanol** [10042-59-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 279

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	832.2 ± 0.4	56-ano-4

**4-Propyl-4-heptanol**

[2198-72-3]

C<sub>10</sub>H<sub>22</sub>O

MW = 158.28

280

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.630$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1067.17
<i>B</i>	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
294.15	833.7 ± 2.0	1.85	02-kon <sup>1)</sup>
290.35	835.0 ± 1.0	0.11	19-eyk
293.15	834.0 ± 1.0	1.35	61-mes/erz
298.15	828.3 ± 0.5	-0.37	88-cac/cos

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	835.2 ± 1.0
293.15	832.6 ± 0.9
298.15	828.6 ± 0.9

**2,2,3,4-Tetramethyl-3-hexanol**

[66256-63-1]

C<sub>10</sub>H<sub>22</sub>O

MW = 158.28

281

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.080$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1104.69
<i>B</i>	-0.840

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
283.15	867.0 ± 2.0	0.16	37-naz
293.15	858.4 ± 1.0	-0.04	50-ste/coo

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	869.5 ± 1.7
290.00	861.1 ± 1.3
293.15	858.4 ± 1.4
298.15	854.2 ± 1.5

**2,2,3,5-Tetramethyl-3-hexanol** [66256-64-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 282

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	839.3 ± 1.0	55-pet
293.15	839.3 ± 1.0	55-pet/sus

**2,2,4,4-Tetramethyl-3-hexanol** [66256-65-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 283

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	854.9 ± 1.0	34-sta

**2,3,4,4-Tetramethyl-3-hexanol** [66256-67-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 284

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
289.15	876.0 ± 2.0	37-naz <sup>1)</sup>
293.15	869.4 ± 3.0	40-mos <sup>1)</sup>
293.15	874.5 ± 1.0	50-ste/coo
293.15	874.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,3,5,5-Tetramethyl-3-hexanol** [5396-09-8] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 285

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	837.8 ± 2.0	42-moe

**3,4,4,5-Tetramethyl-3-hexanol** [66256-39-1] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 286

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	874.2 ± 1.0	50-ste/coo

**3,4,5,5-Tetramethyl-3-hexanol** [66256-40-4] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 287

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	862.3 ± 1.0	50-ste/coo

**2,2,3-Trimethyl-3-heptanol** [29772-40-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 288

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	848.7 ± 1.0	29-con/bla

**2,2,4-Trimethyl-4-heptanol** [57233-31-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 289

**Table 1.** Experimental values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	833.0 ± 2.0	42-moe
293.15	833.0 ± 2.0	49-moe/whi

**2,2,5-Trimethyl-4-heptanol** [66256-42-6] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 290

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	751.3 ± 1.0	39-pet/sum

**2,2,6-Trimethyl-3-heptanol** [66256-43-7] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 291

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	823.6 ± 1.0	38-whi/mey

**2,3,6-Trimethyl-3-heptanol** [58046-40-5] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 292

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	839.8 ± 1.0	63-tho/pal

**2,4,6-Trimethyl-4-heptanol** [60836-07-9] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 293

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
294.15	823.0 ± 2.0	09-bod/tab <sup>1)</sup>
293.15	818.6 ± 3.0	33-mey/tuo <sup>1)</sup>
293.15	824.1 ± 1.0	59-pet/zak-1
293.15	824.1 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,5,5-Trimethyl-4-heptanol** [66256-49-3] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 294

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	838.0 ± 2.0	57-tak/nak

**2,5,6-Trimethyl-2-heptanol** [66256-48-2] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 295

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.15	833.0 ± 2.0	11-wal

**3,5,5-Trimethyl-3-heptanol** [66256-50-6] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 296

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	851.3 ± 2.0	40-mos
293.15	851.3 ± 2.0	41-whi/mos
293.15	855.8 ± 1.0	50-ste/coo
293.15	854.3 ± 1.6	Recommended

**4,6,6-Trimethyl-2-heptanol** [51079-79-9] C<sub>10</sub>H<sub>22</sub>O MW = 158.28 297

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	826.5 ± 2.0	46-dou-1



2.1.7 Alkanols, C<sub>11</sub> - C<sub>12</sub>

**3-Butyl-2,4-dimethyl-3-pentanol** [90002-65-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 298

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	860.0 ± 2.0	44-you/rob

**3-Butyl-2-heptanol** [115667-95-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 299

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.05	839.2 ± 1.0	25-hes/bap

**2,6-Dimethyl-4-ethyl-4-heptanol** [54460-99-0] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 300

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	825.2 ± 0.8	56-kru/cho

**3,3-Dimethyl-5-ethyl-4-heptanol** [500000-48-6] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 301

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	849.6 ± 1.0	41-whi/whi

**1-2,4-Dimethyl-3-(1-methylethyl)-3-hexanol** [28357-71-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 302

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	868.0 ± 2.0	44-you/rob

**2,5-Dimethyl-3-(1-methylethyl)-3-hexanol** [57233-26-8] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 303

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	847.0 ± 2.0	43-geo
293.15	848.6 ± 1.0	48-cad/foo
293.15	848.3 ± 1.0	Recommended



**2,2-Dimethyl-1-nonanol** [14250-80-7] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 304

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	839.2 ± 1.0	65-shu/puz

**2,2-Dimethyl-4-nonanol** [38206-58-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 305

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	822.5 ± 1.0	38-whi/pop-1

**2,4-Dimethyl-4-nonanol** [74356-31-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 306

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	828.5 ± 2.0	59-pet/zak

**2,6-Dimethyl-5-nonanol** [500001-10-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 307

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	821.6 ± 0.8	12-bje

**3,5-Dimethyl-5-nonanol** [106593-61-7] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 308

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
301.15	826.4 ± 1.0	60-tha/vas

**4,8-Dimethyl-1-nonanol** [33933-80-1] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 309

**Table 1.** Experimental values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
292.15	834.0 ± 2.0	23-von/kai
291.15	833.0 ± 2.0	23-von/kai

**4,8-Dimethyl-4-nonanol** [91337-13-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 310

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
284.15	845.8 ± 2.0	28-esc

**2,2-Dimethyl-3-propyl-3-hexanol** [900002-63-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 311

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.15	853.0 ± 2.0	21-ler

**4,4-Dimethyl-3-(1,1-dimethylethyl)-1-pentanol** [79802-55-4] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 312

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	866.1 ± 2.0	60-pet/sok

**5-Ethyl-2-nonanol** [103-08-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 313

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.150$ .

Coefficient	$\rho = A + BT$
$A$	1063.31
$B$	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
303.15	826.7 ± 1.0	-0.15	48-wei
293.15	834.8 ± 1.0	0.15	58-ano-13

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>	K	kg · m <sup>-3</sup>
290.00	837.1 ± 1.0	298.15	830.7 ± 0.9
293.15	834.7 ± 0.9	310.00	821.5 ± 1.1

**5-Ethyl-3-nonanol** [19780-71-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 314

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	834.9 ± 1.0	58-ano-5

**5-Ethyl-4-nonanol** [19780-73-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 315

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	837.0 ± 2.0	48-pow/nie

**5-Ethyl-5-nonanol** [5340-51-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 316

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.150$ .

Coefficient	$\rho = A + BT$
$A$	1037.09
$B$	-0.680

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
293.15	837.6 ± 1.0	-0.15	33-whi/woo
298.15	834.5 ± 1.0	0.15	33-whi/woo

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>
290.00	839.9 ± 1.1
293.15	837.8 ± 0.9
298.15	834.4 ± 0.9

***d*-6-Ethyl-3-nonanol** [900002-60-0] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 317

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
295.15	830.0 ± 2.0	31-lev/mar-3

**3-Ethyl-2,2,4,4-tetramethyl-3-pentanol** [32579-68-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 318

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	811.9 ± 1.5	60-pet/sok

**4-Ethyl-2,2,3-trimethyl-3-hexanol** [91337-10-9] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 319

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	862.0 ± 2.0	37-naz

**2-Methyl-4-decanol** [25564-57-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 320

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	816.8 ± 1.0	38-wer/bog

**2-Methyl-5-decanol** [500001-13-8] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 321

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	826.6 ± 1.0	44-pow/hag

**3-Methyl-2-decanol** [500001-16-1] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 322

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
296.15	834.0 ± 2.0	33-pow/mur

**4-Methyl-3-decanol** [500001-14-9] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 323

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
296.15	829.0 ± 2.0	35-gre-2

**4-Methyl-4-decanol** [26209-94-9] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 324

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 4.1396 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 2.6273 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 338.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.06090 \cdot 10^3$
B	$-7.94286 \cdot 10^{-1}$

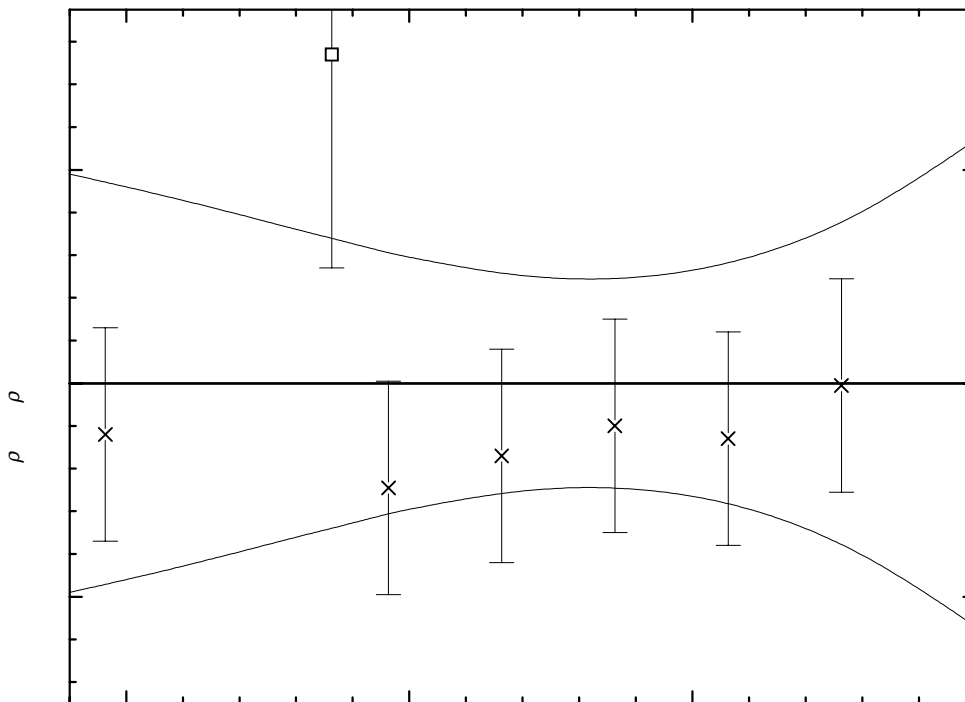
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	829.60 ± 1.00	1.54	38-whi/ore(□)	318.15	808.00 ± 0.50	-0.20	39-owe/qua(×)
273.15	843.70 ± 0.50	-0.24	39-owe/qua(×)	328.15	800.00 ± 0.50	-0.26	39-owe/qua(×)
298.15	823.60 ± 0.50	-0.49	39-owe/qua(×)	338.15	792.30 ± 0.50	-0.01	39-owe/qua(×)
308.15	815.80 ± 0.50	-0.34	39-owe/qua(×)				

<sup>1)</sup> Not included in Fig. 1.

cont.

## 4-Methyl-4-decanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	846.44 ± 0.98	298.15	824.09 ± 0.61	330.00	798.79 ± 0.57
280.00	838.50 ± 0.86	300.00	822.62 ± 0.59	340.00	790.84 ± 0.78
290.00	830.56 ± 0.72	310.00	814.67 ± 0.49	350.00	782.90 ± 1.14
293.15	828.06 ± 0.68	320.00	806.73 ± 0.48		

**L-5-Methyl-1-decanol****[500001-17-2]****C<sub>11</sub>H<sub>24</sub>O****MW = 172.31****325****Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
297.15	840.0 ± 2.0	33-lev/mar-1

**5-Methyl-5-decanol** [87258-26-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 326

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	826.2 ± 1.0	33-whi/wil

**l-6-Methyl-3-decanol** [900002-59-7] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 327

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
297.15	829.0 ± 2.0	31-lev/mar-4

**2-Methyl-3-(1-methylethyl)-3-heptanol** [5340-35-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 328

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	848.7 ± 1.0	29-con/bla
293.15	855.7 ± 3.0	43-geo <sup>1)</sup>
293.15	849.0 ± 1.0	49-naz/pin
293.15	848.9 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**5-Methyl-3-(2-methylpropyl)-2-hexanol** [900002-62-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 329

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
277.15	844.0 ± 2.0	10-fre

**2-Methyl-4-propyl-4-heptanol** [56065-39-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 330

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
295.15	831.1 ± 2.0	14-hal

**4-Methyl-2-propyl-1-hexanol** [66256-62-0] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 331

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	828.6 ± 1.0	58-hag/hud

**4-(1-Methylethyl)-4-octanol** [900002-61-1] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 332

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	840.0 ± 2.0	54-naz/kak-4

**2,2,3,4,4-Pentamethyl-3-hexanol** [500000-99-7] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 333

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	886.0 ± 2.0	37-naz

**2,2,3,4,5-Pentamethyl-3-hexanol** [500000-98-6] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 334

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
285.15	868.0 ± 2.0	37-naz

**2,2,4,5,5-Pentamethyl-4-hexanol** [900002-64-4] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 335

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	841.0 ± 2.0	49-moe/whi

**3,4,4,5,5-Pentamethyl-3-hexanol** [536-91-2] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 336

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	877.8 ± 2.0	60-pet/kao

**3-Propyl-2-octanol** [500001-08-1] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 337

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
290.15	831.0 ± 2.0	12-gue-2

**4-Propyl-4-octanol** [6632-94-6] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 338**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.100$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1034.54
<i>B</i>	-0.680

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	835.1 ± 1.0	-0.10	33-whi/woo
298.15	831.9 ± 1.0	0.10	33-whi/woo

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	837.3 ± 1.1
293.15	835.2 ± 0.9
298.15	831.8 ± 0.9

**2,2,3,4-Tetramethyl-3-heptanol** [91337-08-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 339**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	866.0 ± 2.0	37-naz

**2,2,3,6-Tetramethyl-3-heptanol** [106593-59-3] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 340**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	850.6 ± 1.0	57-pet/sus

**2,2,4,6-Tetramethyl-4-heptanol** [106593-60-6] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 341**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	828.0 ± 2.0	49-moe/whi

**2,3,4,4-Tetramethyl-3-heptanol** [91337-09-6] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 342**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	874.0 ± 2.0	37-naz



**2,2,4-Trimethyl-3-(1-methylethyl)-3-pentanol** [5457-41-0] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 343

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
292.15	870.0 ± 2.0	46-vav/col <sup>1)</sup>
293.15	875.8 ± 1.0	51-smi/cre
293.15	875.8 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,2,4-Trimethyl-4-octanol** [5340-54-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 344

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	835.0 ± 1.0	49-moe/whi

**2,4,7-Trimethyl-4-octanol** [42842-13-7] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 345

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	825.0 ± 1.0	33-mey/tuo

**1-Undecanol** [112-42-5] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 346

**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 2.5713 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 1.0106 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.10$ to $358.10$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.03691 \cdot 10^3$
B	$-6.95763 \cdot 10^{-1}$

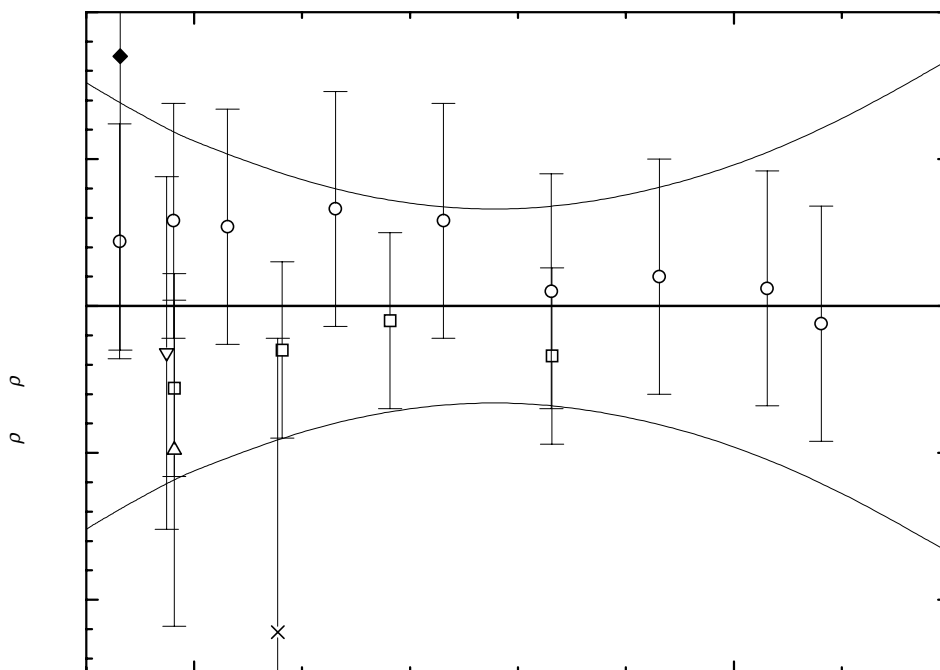
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
307.75	821.68 ± 1.00	-1.11	27-ver/coo(×)	343.10	798.30 ± 0.40	0.10	55-kus(O)
293.15	833.80 ± 1.00	0.85	42-mul(◆)	353.10	791.30 ± 0.40	0.06	55-kus(O)
297.45	829.80 ± 0.60	-0.16	50-sac/sau(∇)	358.10	787.70 ± 0.40	-0.06	55-kus(O)
293.10	833.20 ± 0.40	0.22	55-kus(O)	298.15	829.19 ± 0.30	-0.28	79-dia/tar(□)
298.10	829.80 ± 0.40	0.29	55-kus(O)	308.15	822.36 ± 0.30	-0.15	79-dia/tar(□)
303.10	826.30 ± 0.40	0.27	55-kus(O)	318.15	815.51 ± 0.30	-0.05	79-dia/tar(□)
313.10	819.40 ± 0.40	0.33	55-kus(O)	333.15	804.95 ± 0.30	-0.17	79-dia/tar(□)
323.10	812.40 ± 0.40	0.29	55-kus(O)	298.15	828.98 ± 0.60	-0.49	90-klo/pal(Δ)
333.10	805.20 ± 0.40	0.05	55-kus(O)				

<sup>1)</sup> Not included in Fig. 1.

cont.

**Further references:** [03-bla/gue, 29-mah/das, 48-vog-2, 56-gol/kon, 63-vil/gav].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	835.14 ± 0.76	310.00	821.23 ± 0.42	350.00	793.40 ± 0.47
293.15	832.95 ± 0.69	320.00	814.27 ± 0.34	360.00	786.44 ± 0.63
298.15	829.47 ± 0.59	330.00	807.31 ± 0.32	370.00	779.48 ± 0.84
300.00	828.18 ± 0.56	340.00	800.35 ± 0.37		

## 2-Undecanol

[1653-30-1]

C<sub>11</sub>H<sub>24</sub>O

MW = 172.31

347

**Table 1.** Fit with estimated  $B$  coefficient for 5 accepted points. Deviation  $\sigma_w = 1.587$ .

Coefficient	$\rho = A + BT$
$A$	1044.22
$B$	-0.740

cont.

**2-Undecanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
292.15	826.8 ± 2.0	-1.23	1870-gie	293.15	827.0 ± 1.0	-0.29	11-pic/ken
291.15	826.3 ± 2.0	-2.47	03-tho/man	405.15	739.3 ± 3.0	-5.11	12-pic/ken <sup>1)</sup>
296.15	827.0 ± 2.0	1.93	10-hal/las	293.15	830.2 ± 2.0	2.91	42-mul

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	829.6 ± 2.1
293.15	827.3 ± 2.1
298.15	823.6 ± 2.1

**3-Undecanol** [6929-08-4] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 348**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	829.5 ± 2.0	13-pic/ken
353.15	782.7 ± 2.0	13-pic/ken

**4-Undecanol** [4272-06-4] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 349**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	821.5 ± 1.0	65-das/mae

**6-Undecanol** [23708-56-7] C<sub>11</sub>H<sub>24</sub>O MW = 172.31 350**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	833.4 ± 2.0	25-hes/bap
294.95	827.2 ± 2.0	25-hes/bap

**3-Butyl-3-methyl-2-heptanol** [500001-77-4] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 351**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	850.0 ± 2.0	33-whi/kru

**2-Butyl-1-octanol** [3913-02-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 352

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.255$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1051.19
<i>B</i>	-0.740

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
289.65	837.1 ± 1.0	0.25	38-mas
293.15	834.0 ± 1.0	-0.26	53-ano-15

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	844.0 ± 1.1
290.00	836.6 ± 0.9
293.15	834.3 ± 0.9
298.15	830.6 ± 1.0

**4-Butyl-1-octanol** [500001-73-0] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 353

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
289.15	841.0 ± 2.0	16-lev/all

**2,4-Diethyl-1-octanol** [55514-25-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 354

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	840.0 ± 1.0	61-mil/ben

**2,2-Dimethyl-1-decanol** [2370-15-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 355

**Table 1.** Experimental values with uncertainties.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	834.5 ± 2.0	64-blo/hag
293.15	839.0 ± 2.0	65-shu/puz

**2,4-Dimethyl-4-decanol** [106652-28-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 356

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	828.4 ± 2.0	59-pet/zak

**3,5-Dimethyl-5-decanol** [105900-70-7] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 357

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
301.15	827.0 ± 1.0	60-tha/vas

**5,9-Dimethyl-5-decanol** [900002-66-6] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 358

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
284.15	852.6 ± 2.0	28-esc

**6,6-Dimethyl-5-decanol** [500001-68-3] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 359

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	845.0 ± 2.0	33-who/kru

**2,2-Dimethyl-3-(1,1-dimethylethyl)-3-hexanol** [32579-69-4] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 360

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>		K	kg · m <sup>-3</sup>	
293.15	859.5 ± 1.0	48-cad/foo	293.15	865.2 ± 3.0	57-pet/sok <sup>1)</sup>
293.15	895.5 ± 3.0	51-smi/cre <sup>1)</sup>	293.15	859.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**5,5-Dimethyl-4-(1,1-dimethylethyl)-1-hexanol** [900002-67-7] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 361

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	865.2 ± 2.0	60-pet/sok

**2,2-Dimethyl-4-ethyl-3-octanol** [124154-63-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 362

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	840.9 ± 1.0	41-whi/whi

**2,2-Dimethyl-3-(1-methylethyl)-3-heptanol** [500001-78-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 363

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	856.5 ± 1.0	50-naz/kot-1

**2,6-Dimethyl-3-(1-methylethyl)-3-heptanol** [5340-82-9] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 364

**Table 1.** Experimental values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	860.6 ± 2.0	14-mur/amo
273.15	871.7 ± 2.0	14-mur/amo

**2,2-Dimethyl-4-propyl-4-heptanol** [500001-79-6] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 365

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	837.6 ± 1.0	8 -whi/pop -1
293.15	838.6 ± 1.0	2 -whi/for -0
293.15	838.1 ± 1.1	Recommended

**1-Dodecanol** [112-53-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 366

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 2.7829 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 9.5525 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 296.90$ to $533.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.42675 \cdot 10^2$
B	$-4.51517 \cdot 10^{-2}$
C	$-1.31349 \cdot 10^{-3}$
D	$6.54515 \cdot 10^{-7}$

cont.

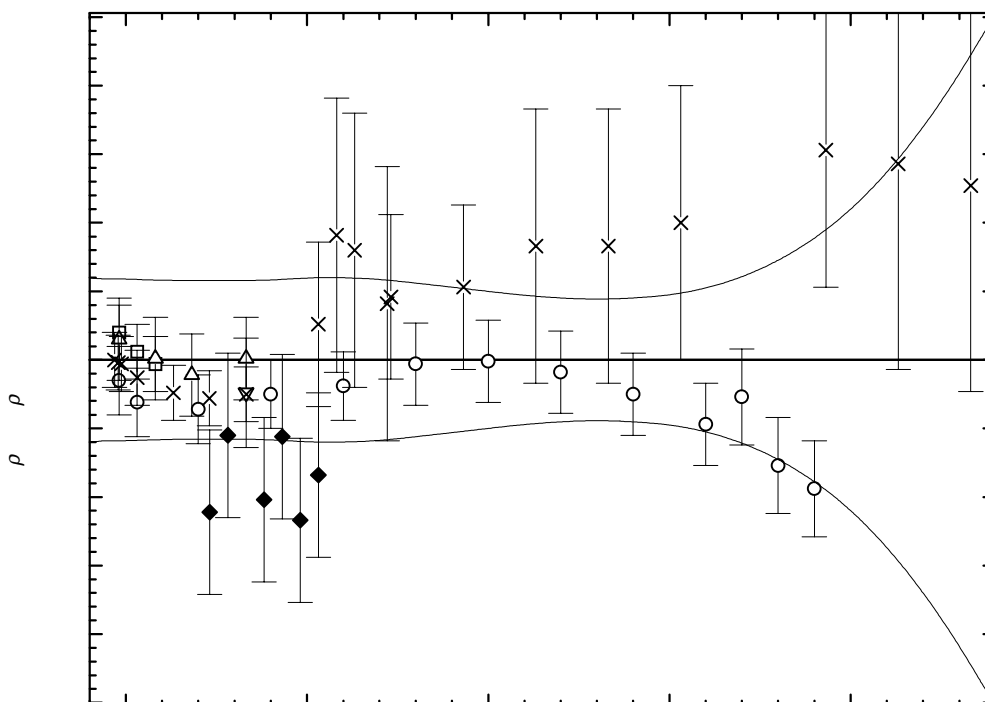
## 1-Dodecanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
<i>crystal</i>				303.14	826.39 ± 0.20	-0.13	73-fin(×)
78.15	1017.0 ± 3.0		30-bil/fis-1	313.13	819.60 ± 0.20	-0.24	73-fin(×)
194.15	981.0 ± 3.0		30-bil/fis-1	323.07	812.78 ± 0.20	-0.28	73-fin(×)
<i>liquid</i>				333.20	805.77 ± 0.20	-0.25	73-fin(×)
297.15	830.90 ± 1.00	0.45	1883-kra <sup>1)</sup>	298.15	829.65 ± 0.25	-0.15	76-hal/ell(O)
313.15	820.10 ± 1.00	0.27	1883-kra <sup>1)</sup>	303.15	826.20 ± 0.25	-0.31	76-hal/ell(O)
372.15	778.10 ± 1.00	0.41	1883-kra(×)	320.00	814.81 ± 0.25	-0.36	76-hal/ell(O)
313.15	819.60 ± 0.60	-0.23	58-cos/bow <sup>1)</sup>	340.00	800.96 ± 0.25	-0.25	76-hal/ell(O)
333.15	805.70 ± 0.60	-0.35	58-cos/bow <sup>1)</sup>	360.00	786.54 ± 0.25	-0.19	76-hal/ell(O)
353.15	792.00 ± 0.60	0.26	58-cos/bow(×)	380.00	771.73 ± 0.30	-0.03	76-hal/ell(O)
373.15	777.40 ± 0.60	0.46	58-cos/bow(×)	400.00	756.33 ± 0.30	-0.01	76-hal/ell(O)
393.15	762.20 ± 0.60	0.53	58-cos/bow(×)	420.00	740.41 ± 0.30	-0.09	76-hal/ell(O)
413.15	746.80 ± 1.00	0.83	58-cos/bow(×)	440.00	724.02 ± 0.30	-0.25	76-hal/ell(O)
433.15	730.70 ± 1.00	0.83	58-cos/bow(×)	460.00	707.21 ± 0.30	-0.47	76-hal/ell(O)
453.15	714.40 ± 1.00	1.00	58-cos/bow(×)	470.00	698.99 ± 0.35	-0.27	76-hal/ell(O)
473.15	698.20 ± 1.00	1.61	58-cos/bow <sup>1)</sup>	480.00	689.99 ± 0.35	-0.77	76-hal/ell(O)
493.15	681.00 ± 1.00	1.53	58-cos/bow(×)	490.00	681.24 ± 0.35	-0.94	76-hal/ell(O)
513.15	663.50 ± 1.50	1.43	58-cos/bow(×)	298.15	830.00 ± 0.20	0.20	78-jel/leo(□)
533.15	645.70 ± 1.50	1.27	58-cos/bow(×)	303.15	826.57 ± 0.20	0.06	78-jel/leo(□)
553.15	627.50 ± 1.50	0.92	58-cos/bow <sup>1)</sup>	308.15	823.16 ± 0.20	-0.03	78-jel/leo(□)
573.15	609.70 ± 1.50	1.16	58-cos/bow <sup>1)</sup>	298.15	829.95 ± 0.30	0.15	79-dia/tar(Δ)
293.15	834.60 ± 1.00	1.55	62-gei/qui <sup>1)</sup>	308.15	823.20 ± 0.30	0.01	79-dia/tar(Δ)
298.15	831.20 ± 1.00	1.40	62-gei/qui <sup>1)</sup>	318.15	816.33 ± 0.30	-0.11	79-dia/tar(Δ)
303.15	827.80 ± 1.00	1.29	62-gei/qui <sup>1)</sup>	333.15	806.06 ± 0.30	0.01	79-dia/tar(Δ)
308.15	824.40 ± 1.00	1.21	62-gei/qui <sup>1)</sup>	298.15	823.00 ± 0.40	-6.80	86-wag/hei <sup>1)</sup>
313.15	821.10 ± 1.00	1.27	62-gei/qui <sup>1)</sup>	333.15	805.81 ± 0.40	-0.24	86-wag/hei(∇)
318.15	817.80 ± 1.00	1.36	62-gei/qui <sup>1)</sup>	298.15	828.50 ± 0.60	-1.30	92-lie/sen-1 <sup>1)</sup>
323.15	814.40 ± 1.00	1.39	62-gei/qui <sup>1)</sup>	303.15	825.50 ± 0.60	-1.01	92-lie/sen-1 <sup>1)</sup>
328.15	811.00 ± 1.00	1.45	62-gei/qui <sup>1)</sup>	308.15	822.50 ± 0.60	-0.69	92-lie/sen-1 <sup>1)</sup>
333.15	807.50 ± 1.00	1.45	62-gei/qui <sup>1)</sup>	313.15	818.20 ± 0.60	-1.63	92-lie/sen-1 <sup>1)</sup>
338.15	804.00 ± 1.00	1.48	62-gei/qui <sup>1)</sup>	318.15	815.20 ± 0.60	-1.24	92-lie/sen-1 <sup>1)</sup>
343.15	800.20 ± 1.00	1.24	62-gei/qui <sup>1)</sup>	323.15	811.90 ± 0.60	-1.11	92-lie/sen-1(◆)
348.15	796.50 ± 1.00	1.13	62-gei/qui <sup>1)</sup>	328.15	809.00 ± 0.60	-0.55	92-lie/sen-1(◆)
353.15	792.80 ± 1.00	1.06	62-gei/qui <sup>1)</sup>	333.15	804.70 ± 0.60	-1.35	92-lie/sen-1 <sup>1)</sup>
358.15	789.00 ± 1.00	0.91	62-gei/qui(×)	338.15	801.50 ± 0.60	-1.02	92-lie/sen-1(◆)
363.15	785.20 ± 1.00	0.80	62-gei/qui(×)	343.15	798.40 ± 0.60	-0.56	92-lie/sen-1(◆)
296.90	830.62 ± 0.20	0.00	73-fin(×)	348.15	794.20 ± 0.60	-1.17	92-lie/sen-1(◆)
297.89	829.95 ± 0.20	-0.02	73-fin(×)	353.15	790.90 ± 0.60	-0.84	92-lie/sen-1(◆)
298.78	829.36 ± 0.20	-0.03	73-fin(×)				

<sup>1)</sup> Not included in Fig. 1.**Further references:** [27-ver/coo, 29-mah/das, 31-zaa, 36-pal/sab, 42-mul, 43-hsu, 44-sto/rou, 46-par/row, 48-wei, 49-tsv/mar, 50-sac/sau, 55-pet/sus, 56-rat/cur, 63-vil/gav, 67-seu/mor, 93-yan/mae].

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	835.08 ± 0.60	370.00	779.30 ± 0.59	470.00	699.26 ± 0.60
293.15	833.05 ± 0.59	380.00	771.76 ± 0.56	480.00	690.76 ± 0.72
298.15	829.80 ± 0.59	390.00	764.11 ± 0.53	490.00	682.18 ± 0.88
300.00	828.59 ± 0.59	400.00	756.34 ± 0.50	500.00	673.54 ± 1.09
310.00	821.95 ± 0.58	410.00	748.47 ± 0.47	510.00	664.83 ± 1.36
320.00	815.17 ± 0.58	420.00	740.50 ± 0.45	520.00	656.06 ± 1.69
330.00	808.26 ± 0.58	430.00	732.43 ± 0.44	530.00	647.23 ± 2.08
340.00	801.21 ± 0.58	440.00	724.27 ± 0.45	540.00	638.34 ± 2.53
350.00	794.03 ± 0.60	450.00	716.02 ± 0.47		
360.00	786.73 ± 0.60	460.00	707.68 ± 0.52		



**2-Dodecanol****[10203-28-8]****C<sub>12</sub>H<sub>26</sub>O****MW = 186.34****367****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 1.0204 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.8302 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $363.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.76605 \cdot 10^2$
B	$-3.16820 \cdot 10^{-1}$
C	$-6.34131 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

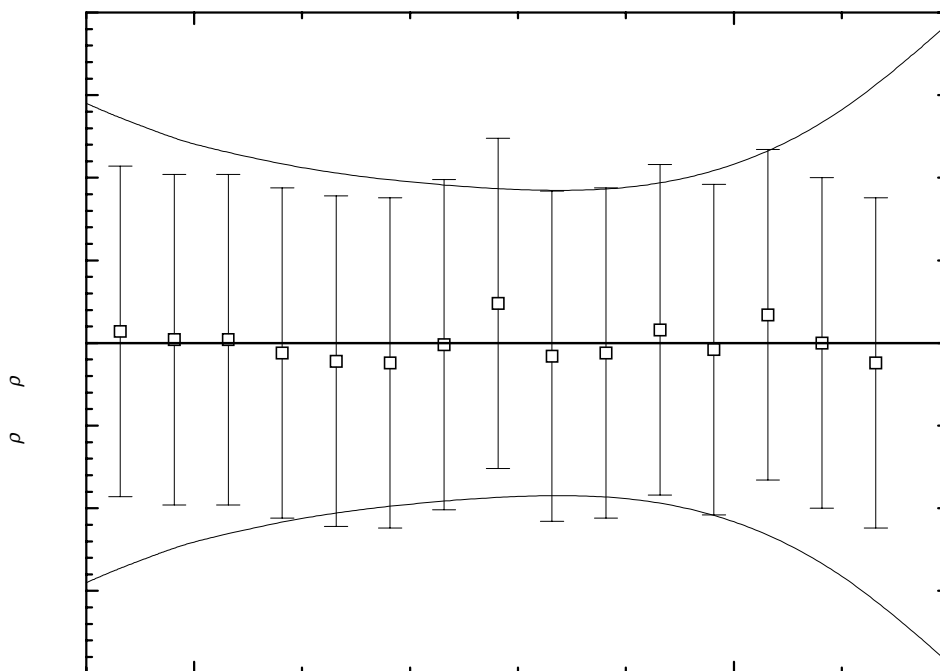
$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	$829.30 \pm 1.00$	0.07	62-gei/qui(□)	333.15	$800.60 \pm 1.00$	-0.08	62-gei/qui(□)
298.15	$825.80 \pm 1.00$	0.02	62-gei/qui(□)	338.15	$796.90 \pm 1.00$	-0.06	62-gei/qui(□)
303.15	$822.30 \pm 1.00$	0.02	62-gei/qui(□)	343.15	$793.30 \pm 1.00$	0.08	62-gei/qui(□)
308.15	$818.70 \pm 1.00$	-0.06	62-gei/qui(□)	348.15	$789.40 \pm 1.00$	-0.04	62-gei/qui(□)
313.15	$815.10 \pm 1.00$	-0.11	62-gei/qui(□)	353.15	$785.80 \pm 1.00$	0.17	62-gei/qui(□)
318.15	$811.50 \pm 1.00$	-0.12	62-gei/qui(□)	358.15	$781.80 \pm 1.00$	0.00	62-gei/qui(□)
323.15	$808.00 \pm 1.00$	-0.01	62-gei/qui(□)	363.15	$777.80 \pm 1.00$	-0.12	62-gei/qui(□)
328.15	$804.60 \pm 1.00$	0.24	62-gei/qui(□)				

**Further references:** [11-pic/ken].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	$831.40 \pm 1.45$	310.00	$817.45 \pm 1.05$	350.00	$788.04 \pm 1.05$
293.15	$829.23 \pm 1.36$	320.00	$810.29 \pm 0.97$	360.00	$780.37 \pm 1.37$
298.15	$825.78 \pm 1.24$	330.00	$803.00 \pm 0.92$	370.00	$772.57 \pm 1.94$
300.00	$824.49 \pm 1.20$	340.00	$795.58 \pm 0.92$		

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3-Dodecanol**

[10203-30-2]

C<sub>12</sub>H<sub>26</sub>O

MW = 186.34

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**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 3.8100 \cdot 10^{-2}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.0998 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15 \text{ to } 363.15 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.00182 \cdot 10^3$
B	$-4.39256 \cdot 10^{-1}$
C	$-4.82504 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	$831.60 \pm 1.00$	0.01	62-gei/qui(□)	308.15	$820.60 \pm 1.00$	-0.05	62-gei/qui(□)
298.15	$828.00 \pm 1.00$	0.03	62-gei/qui(□)	313.15	$816.90 \pm 1.00$	-0.05	62-gei/qui(□)
303.15	$824.30 \pm 1.00$	-0.02	62-gei/qui(□)	318.15	$813.30 \pm 1.00$	0.06	62-gei/qui(□)

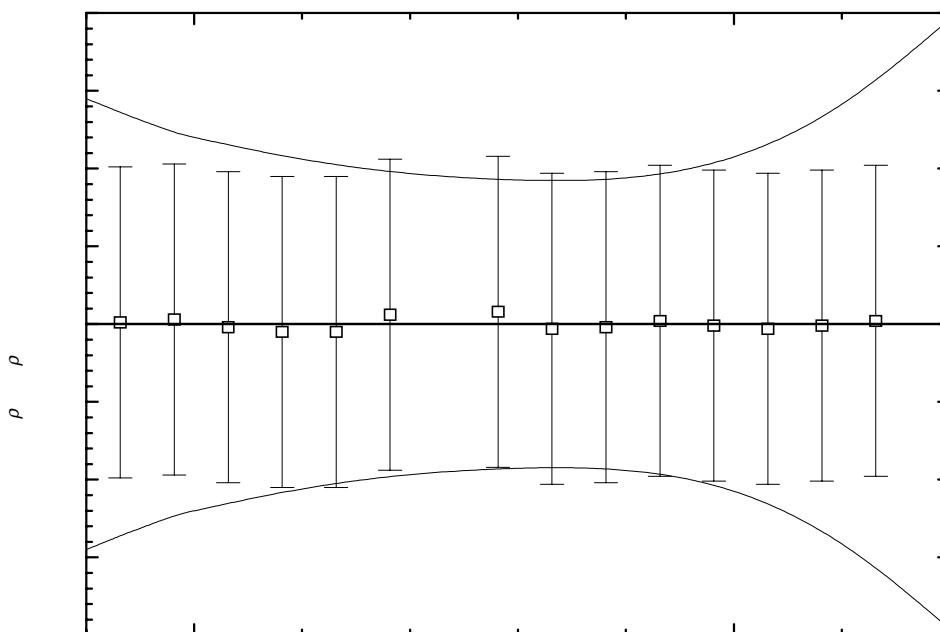
cont.

**3-Dodecanol** (cont.)**Table 2.** (cont.)

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
323.15	809.70 ± 1.00	0.21	62-gei/qui <sup>1)</sup>	348.15	790.40 ± 1.00	-0.01	62-gei/qui(□)
328.15	805.80 ± 1.00	0.08	62-gei/qui(□)	353.15	786.50 ± 1.00	-0.03	62-gei/qui(□)
333.15	801.90 ± 1.00	-0.03	62-gei/qui(□)	358.15	782.60 ± 1.00	-0.01	62-gei/qui(□)
338.15	798.10 ± 1.00	-0.02	62-gei/qui(□)	363.15	778.70 ± 1.00	0.02	62-gei/qui(□)
343.15	794.30 ± 1.00	0.02	62-gei/qui(□)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [13-pic/ken].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	833.86 ± 1.45	310.00	819.29 ± 1.05	350.00	788.98 ± 1.04
293.15	831.59 ± 1.36	320.00	811.85 ± 0.96	360.00	781.16 ± 1.37
298.15	827.97 ± 1.23	330.00	804.32 ± 0.92	370.00	773.24 ± 1.96
300.00	826.62 ± 1.20	340.00	796.70 ± 0.92		

**4-Dodecanol****[10203-32-4]****C<sub>12</sub>H<sub>26</sub>O****MW = 186.34****369****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 4.1061 \cdot 10^{-2}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.1853 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $363.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.85212 \cdot 10^2$
B	$-3.51028 \cdot 10^{-1}$
C	$-6.18755 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	$829.20 \pm 1.00$	0.07	62-gei/qui(□)	333.15	$799.60 \pm 1.00$	0.01	62-gei/qui(□)
298.15	$825.50 \pm 1.00$	-0.05	62-gei/qui(□)	338.15	$795.70 \pm 1.00$	-0.06	62-gei/qui(□)
303.15	$821.90 \pm 1.00$	-0.03	62-gei/qui(□)	343.15	$791.90 \pm 1.00$	0.00	62-gei/qui(□)
308.15	$818.30 \pm 1.00$	0.01	62-gei/qui(□)	348.15	$788.10 \pm 1.00$	0.10	62-gei/qui(□)
313.15	$814.60 \pm 1.00$	-0.01	62-gei/qui(□)	353.15	$784.10 \pm 1.00$	0.02	62-gei/qui(□)
318.15	$810.90 \pm 1.00$	-0.00	62-gei/qui(□)	358.15	$780.10 \pm 1.00$	-0.02	62-gei/qui(□)
323.15	$807.30 \pm 1.00$	0.14	62-gei/qui <sup>1)</sup>	363.15	$776.10 \pm 1.00$	-0.04	62-gei/qui(□)
328.15	$803.40 \pm 1.00$	0.01	62-gei/qui(□)				

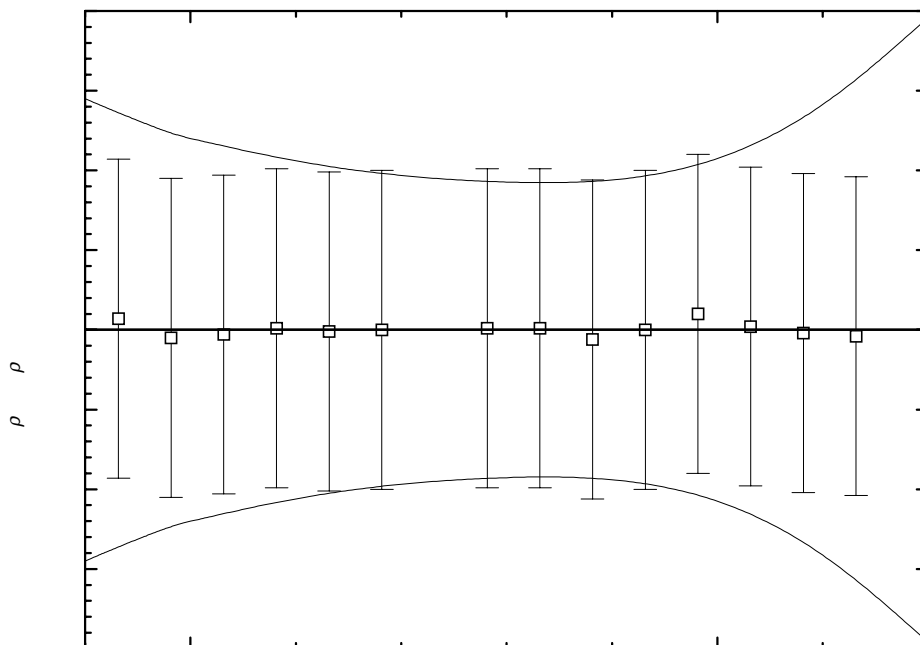
<sup>1)</sup> Not included in Fig. 1.**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	$831.38 \pm 1.45$	310.00	$816.93 \pm 1.05$	350.00	$786.55 \pm 1.04$
293.15	$829.13 \pm 1.36$	320.00	$809.52 \pm 0.96$	360.00	$778.65 \pm 1.37$
298.15	$825.55 \pm 1.23$	330.00	$801.99 \pm 0.92$	370.00	$770.62 \pm 1.96$
300.00	$824.22 \pm 1.20$	340.00	$794.33 \pm 0.92$		

cont.

## 4-Dodecanol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

## 5-Dodecanol

[10203-33-5]

C<sub>12</sub>H<sub>26</sub>O

MW = 186.34

370

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 7.5305 \cdot 10^{-2}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 2.1739 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15 \text{ to } 363.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.59772 \cdot 10^2$
B	$-1.92462 \cdot 10^{-1}$
C	$-8.58906 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

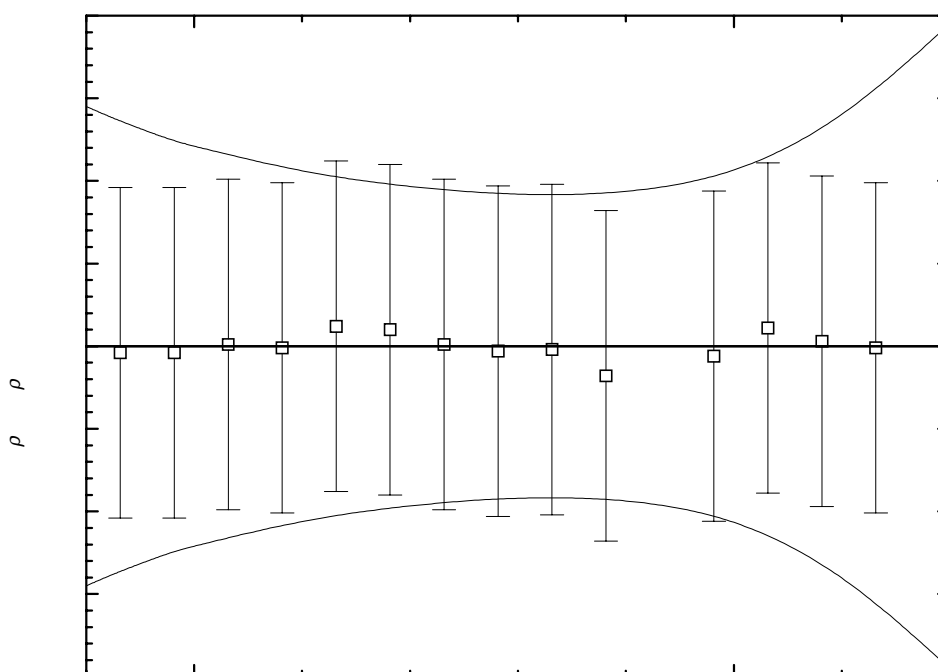
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	$829.50 \pm 1.00$	-0.04	62-gei/qui(□)	308.15	$818.90 \pm 1.00$	-0.01	62-gei/qui(□)
298.15	$826.00 \pm 1.00$	-0.04	62-gei/qui(□)	313.15	$815.40 \pm 1.00$	0.12	62-gei/qui(□)
303.15	$822.50 \pm 1.00$	0.01	62-gei/qui(□)	318.15	$811.70 \pm 1.00$	0.10	62-gei/qui(□)

cont.

**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
323.15	807.90 ± 1.00	0.01	62-gei/qui(□)	348.15	788.60 ± 1.00	-0.06	62-gei/qui(□)
328.15	804.10 ± 1.00	-0.03	62-gei/qui(□)	353.15	784.80 ± 1.00	0.11	62-gei/qui(□)
333.15	800.30 ± 1.00	-0.02	62-gei/qui(□)	358.15	780.70 ± 1.00	0.03	62-gei/qui(□)
338.15	796.30 ± 1.00	-0.18	62-gei/qui(□)	363.15	776.60 ± 1.00	-0.01	62-gei/qui(□)
343.15	792.30 ± 1.00	-0.29	62-gei/qui <sup>1)</sup>				

<sup>1)</sup> Not included in Fig. 1.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	831.72 ± 1.45	310.00	817.57 ± 1.05	350.00	787.19 ± 1.03
293.15	829.54 ± 1.36	320.00	810.23 ± 0.96	360.00	779.17 ± 1.36
298.15	826.04 ± 1.24	330.00	802.73 ± 0.91	370.00	770.98 ± 1.95
300.00	824.73 ± 1.21	340.00	795.05 ± 0.92		

**6-Dodecanol**

[6836-38-0]

C<sub>12</sub>H<sub>26</sub>O

MW = 186.34

371

**Table 1.** Coefficients of the polynomial expansion equation.

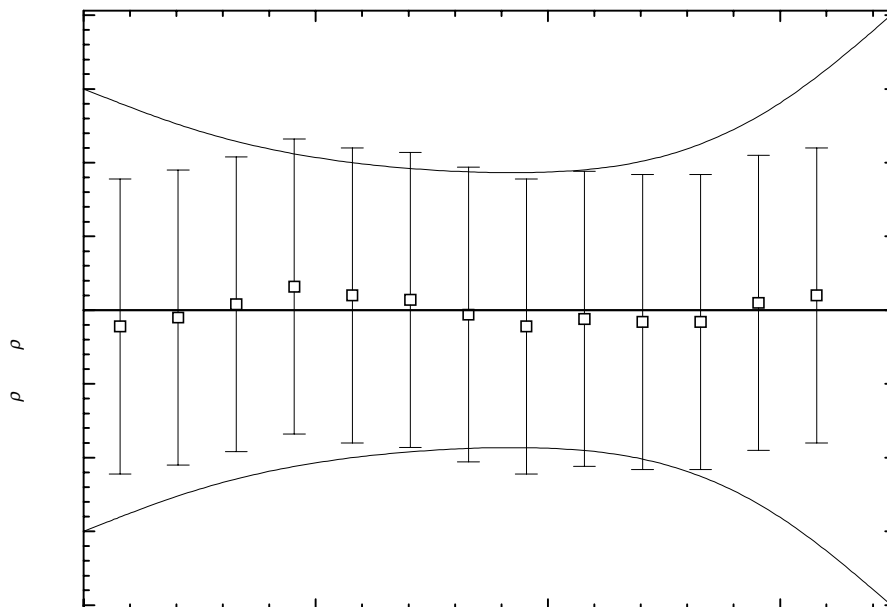
Standard deviations (see introduction):

 $\sigma_{c,w} = 8.7855 \cdot 10^{-2}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.6489 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 303.15 \text{ to } 363.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.92440 \cdot 10^2$
B	$-4.06419 \cdot 10^{-1}$
C	$-5.33467 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
303.15	$820.10 \pm 1.00$	-0.11	62-gei/qui(□)	338.15	$793.90 \pm 1.00$	-0.11	62-gei/qui(□)
308.15	$816.50 \pm 1.00$	-0.05	62-gei/qui(□)	343.15	$790.10 \pm 1.00$	-0.06	62-gei/qui(□)
313.15	$812.90 \pm 1.00$	0.04	62-gei/qui(□)	348.15	$786.20 \pm 1.00$	-0.08	62-gei/qui(□)
318.15	$809.30 \pm 1.00$	0.16	62-gei/qui(□)	353.15	$782.30 \pm 1.00$	-0.08	62-gei/qui(□)
323.15	$805.50 \pm 1.00$	0.10	62-gei/qui(□)	358.15	$778.50 \pm 1.00$	0.05	62-gei/qui(□)
328.15	$801.70 \pm 1.00$	0.07	62-gei/qui(□)	363.15	$774.60 \pm 1.00$	0.10	62-gei/qui(□)
333.15	$797.80 \pm 1.00$	-0.03	62-gei/qui(□)				



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.).

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
300.00	822.50 ± 1.50	330.00	800.23 ± 0.94	360.00	776.99 ± 1.35
310.00	815.18 ± 1.19	340.00	792.59 ± 0.92	370.00	769.03 ± 2.03
320.00	807.76 ± 1.02	350.00	784.84 ± 1.00		

**5-Ethyl-5-decanol** [91635-39-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 372

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 1.122$ .

Coefficient	$\rho = A + BT$
$A$	1054.83
$B$	-0.740

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	835.7 ± 1.0	1.50	44-qua/sma
318.15	819.1 ± 1.0	-0.30	44-qua/sma
328.15	810.8 ± 1.0	-1.20	44-qua/sma

**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	840.2 ± 1.9	298.15	834.2 ± 1.7	320.00	818.0 ± 1.5
293.15	837.9 ± 1.8	310.00	825.4 ± 1.5	330.00	810.6 ± 1.6

**6-Ethyl-3-decanol** [19780-31-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 373

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
301.15	836.4 ± 1.0	36-pow/bal

**4-Ethyl-2-methyl-3-(1-methylethyl)-3-hexanol** [500001-86-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 374

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	852.8 ± 1.0	43-geo



**5-Ethyl-2-methyl-3-nonanol** [105902-95-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 375

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	847.1 ± 2.0	57-pet/nef-1

**5-Ethyl-7-methyl-3-nonanol** [66634-87-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 376

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
273.15	921.0 ± 2.0	12-gue

**4-Ethyl-2,2,3,4-tetramethyl-3-hexanol** [91635-45-9] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 377

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.15	892.0 ± 2.0	37-naz

**3-Ethyl-3,4,5-trimethyl-4-heptanol** [500002-61-9] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 378

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
286.15	885.0 ± 2.0	37-naz

**2,2,3,4,4,5-Hexamethyl-3-hexanol** [500002-63-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 379

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
286.15	893.0 ± 2.0	37-naz

**2,2,4,4,5,5-Hexamethyl-3-hexanol** [500001-88-7] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 380

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.245$ .

Coefficient	$\rho = A + BT$
$A$	1065.31
$B$	-0.700

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
288.15	848.1 ± 4.0	-15.50	33-fav/naz <sup>1)</sup>
293.15	860.4 ± 0.6	0.30	53-per/wag
303.15	853.1 ± 0.6	-0.00	53-per/wag
313.15	845.8 ± 0.6	-0.30	53-per/wag

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	862.3 ± 0.8
293.15	860.1 ± 0.7
298.15	856.6 ± 0.5
310.00	848.3 ± 0.6
320.00	841.3 ± 1.0

**2,3,4,4,5,5-Hexamethyl-3-hexanol** [100392-68-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 381

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	888.6 ± 2.0	60-pet/kao

**5-Methyl-2-(3-methylbutyl)-1-hexanol** [500001-82-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 382

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	834.0 ± 1.0	37-bra/kur

**2-Methyl-3-(1-methylethyl)-3-octanol** [19965-71-0] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 383

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	853.7 ± 1.0	43-geo

**5-Methyl-5-propyl-4-octanol** [500001-75-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 384

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
289.65	845.5 ± 1.0	21-ler

**2-Methyl-2-undecanol** [32836-42-3] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 385**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.410$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1046.24
<i>B</i>	-0.740

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
273.15	843.7 ± 1.0	-0.41	19-beh
286.15	834.9 ± 1.0	0.41	19-beh

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	846.4 ± 1.1
280.00	839.0 ± 1.0
290.00	831.6 ± 1.1

**2-Methyl-3-undecanol** [60671-36-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 386**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	832.7 ± 2.0	12-pic/ken

**2-Methyl-5-undecanol** [33978-71-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 387**Table 1.** Experimental values with uncertainties.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	826.6 ± 1.0	44-pow/hag
293.15	825.1 ± 2.0	48-pet/old

**3-Methyl-1-undecanol** [71526-27-7] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 388**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 0.817$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1039.61
<i>B</i>	-0.700

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	834.1 ± 1.0	-0.30	48-pro/cas
298.15	830.9 ± 1.0	-0.00	48-pro/cas
303.15	827.5 ± 1.0	0.10	48-pro/cas
308.15	824.1 ± 1.0	0.20	48-pro/cas

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	836.6 ± 1.1
293.15	834.4 ± 1.0
298.15	830.9 ± 0.9
310.00	822.6 ± 1.0

**[S-(R\*,R\*)]-3-Methyl-5-undecanol** [82749-56-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 389

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
297.15	827.2 ± 2.0	35-lev/har

**5-Methyl-5-undecanol** [21078-80-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 390

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 3.2352 \cdot 10^{-1}$  (combined temperature ranges, weighted),

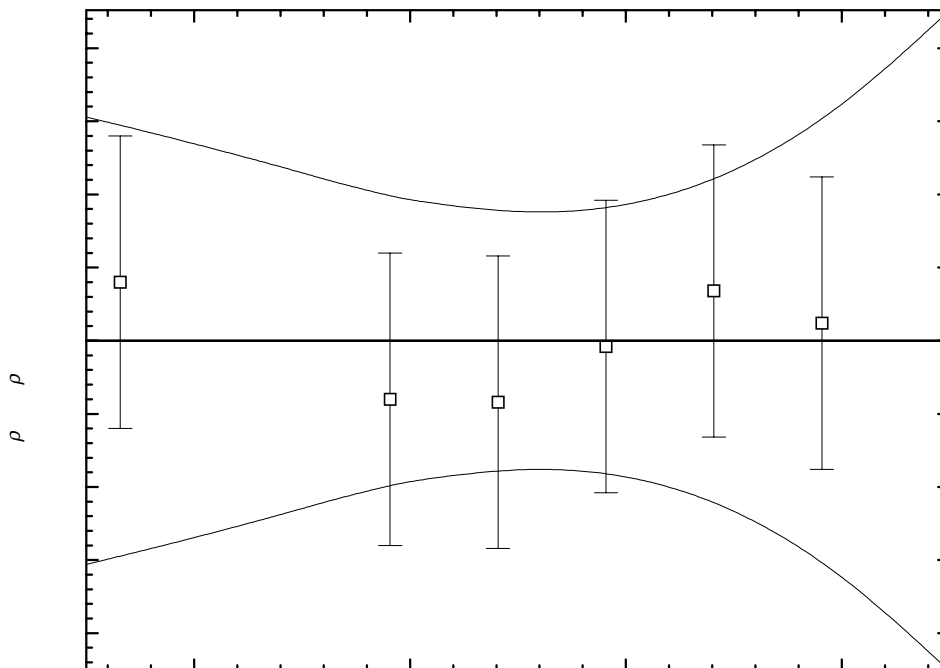
$\sigma_{\text{c,uw}} = 1.4468 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $338.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.05408 \cdot 10^3$
B	$-7.68000 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	844.70 ± 1.00	0.40	39-owe/qua(□)	318.15	809.70 ± 1.00	-0.04	39-owe/qua(□)
298.15	824.70 ± 1.00	-0.40	39-owe/qua(□)	328.15	802.40 ± 1.00	0.34	39-owe/qua(□)
308.15	817.00 ± 1.00	-0.42	39-owe/qua(□)	338.15	794.50 ± 1.00	0.12	39-owe/qua(□)

cont.

**5-Methyl-5-undecanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	846.72 ± 1.53	298.15	825.10 ± 0.99	330.00	800.64 ± 1.13
280.00	839.04 ± 1.35	300.00	823.68 ± 0.96	340.00	792.96 ± 1.58
290.00	831.36 ± 1.15	310.00	816.00 ± 0.86	350.00	785.28 ± 2.26
293.15	828.94 ± 1.08	320.00	808.32 ± 0.90		

**6-Methyl-6-undecanol**

[5340-31-8]

C<sub>12</sub>H<sub>26</sub>O

MW = 186.34

391

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	827.1 ± 1.0	33-whi/wil

**9-Methyl-1-undecanol** [91635-46-0] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 392

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	831.6 ± 1.0	62-lar/sal

**L(+)-9-Methyl-1-undecanol** [500006-92-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 393

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	831.6 ± 0.6	62-lar/sal

**5-(1-Methylethyl)-5-nonanol** [76144-88-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 394

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	844.0 ± 2.0	33-whi/kru

**3-(1-Methylethyl)-2,2,4,4-tetramethyl-3-pentanol** [5457-42-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 395

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	888.9 ± 1.0	51-smi/cre
293.15	885.3 ± 2.0	57-pet/sok
293.15	888.2 ± 1.6	Recommended

**3-(1-Methylethyl)-2,2,5-trimethyl-3-hexanol** [500001-89-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 396

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	855.2 ± 2.0	57-pet/sus

**2,2,3,3,4-Pentamethyl-4-heptanol** [500001-81-0] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 397

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	877.2 ± 2.0	60-pet/kao

**2,2,4,6,6-Pentamethyl-3-heptanol** [105902-93-0] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 398

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	838.0 ± 1.0	41-whi/whi

**4-Propyl-4-nonanol** [5340-77-2] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 399

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
297.65	832.4 ± 2.0	33-whi/wil

**5-Propyl-5-nonanol** [5340-52-3] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 400

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 1.052$ .

Coefficient	$\rho = A + BT$
$A$	1066.88
$B$	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
293.15	837.0 ± 2.0	-1.23	33-whi/woo
298.15	834.0 ± 2.0	-0.33	33-whi/woo
288.15	842.0 ± 2.0	-0.13	37-pet/mal
293.15	839.9 ± 2.0	1.67	61-mes/erz

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>
280.00	848.5 ± 2.5
290.00	840.7 ± 2.1
293.15	838.2 ± 2.1
298.15	834.3 ± 2.1

**2,2,3,4,4-Pentamethyl-3-heptanol** [500002-60-8] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 401

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
286.15	885.0 ± 2.0	37-naz

**2,2,5,6,6-Pentamethyl-3-heptanol** [500002-65-3] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 402

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	845.0 ± 2.0	35-col

**3,3,4,5,5-Pentamethyl-4-heptanol** [500002-62-0] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 403

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.15	900.4 ± 1.0	37-naz

**2,5,8-Trimethyl-5-nonanol** [64029-94-3] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 404

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	828.9 ± 1.0	59-yur/bel

**2,6,8-Trimethyl-4-nonanol** [123-17-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 405

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	817.9 ± 1.0	53-ano-15
293.15	817.9 ± 1.0	58-ano-5
293.15	817.9 ± 1.0	68-ano

**3,4,8-Trimethyl-1-nonanol** [18352-71-1] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 406

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	846.3 ± 1.0	67-min/che

**3,4,8-Trimethyl-3-nonanol** [18352-67-5] C<sub>12</sub>H<sub>26</sub>O MW = 186.34 407

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	836.6 ± 1.0	67-min/che





2.1.8 Alkanols, C<sub>13</sub> - C<sub>22</sub>

**3-Butyl-2,2-dimethyl-3-heptanol** [90002-68-8] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 408

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	849.8 ± 1.0	38-whi/pop

**2-Butyl-1-nonanol** [51655-57-3] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 409

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	835.9 ± 2.0	22-lev/tay-1

**5-Butyl-5-nonanol** [597-93-3] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 410

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.85	835.3 ± 2.0	19-eyk <sup>1)</sup>	293.15	844.2 ± 2.0	61-mes/erz <sup>1)</sup>
351.85	768.9 ± 3.0	19-eyk <sup>1)</sup>	298.15	835.0 ± 0.7	88-cac/cos
293.15	840.8 ± 2.0	33-whi/woo <sup>1)</sup>	298.15	835.0 ± 0.7	Recommended
298.15	836.8 ± 2.0	33-whi/woo <sup>1)</sup>			

<sup>1)</sup> Not included in calculation of recommended value.

**4,4-Diethyl-2,2,3-trimethyl-3-hexanol** [500045-00-1] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 411

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
283.15	906.0 ± 2.0	37-naz

**2,2-Dimethyl-3-(1,1-dimethylethyl)-3-heptanol** [42930-67-6] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 412

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	860.6 ± 1.0	54-mos/cox
293.15	859.6 ± 1.0	60-pet/sok
293.15	860.1 ± 1.1	Recommended

**5,5-Dimethyl-2-neopentyl-1-hexanol** [109509-73-1] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 413

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	847.0 ± 2.0	56-gol/kon

**2,8-Dimethyl-5-ethyl-5-nonanol** [500001-93-4] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 414

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	867.7 ± 2.0	14-hal

**3,3-Dimethyl-5-ethyl-4-nonanol** [500000-49-7] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 415

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	851.2 ± 1.0	41-whi/whi

**2,4-Dimethyl-4-undecanol** [500045-01-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 416

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	825.2 ± 1.5	59-pet/zak

**3,5-Dimethyl-5-undecanol** [107618-96-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 417

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
301.15	827.2 ± 1.0	60-tha/vas

**3-(1,1-Dimethylethyl)-2,2,5-trimethyl-3-hexanol** [32579-70-7] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 418

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	866.8 ± 1.0	54-mos/cox
293.15	867.6 ± 1.0	60-pet/sok
293.15	867.2 ± 1.0	Recommended

**2-Ethyl-1-undecanol** [54381-03-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 419

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	840.4 ± 2.0	47-sto

**6-Ethyl-6-undecanol** [5340-50-1] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 420

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	834.8 ± 2.0	33-whi/wil

**4-Ethyl-3,3,5,5-tetramethyl-4-heptanol** [900002-19-9] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 421

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	892.8 ± 1.0	54-mos/cox

**2-Methyl-1-dodecanol** [22663-61-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 422

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	844.0 ± 2.0	29-lev/mik

**6-Methyl-6-dodecanol** [62958-40-1] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 423

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.0037 \cdot 10^{-1}$  (combined temperature ranges, weighted),

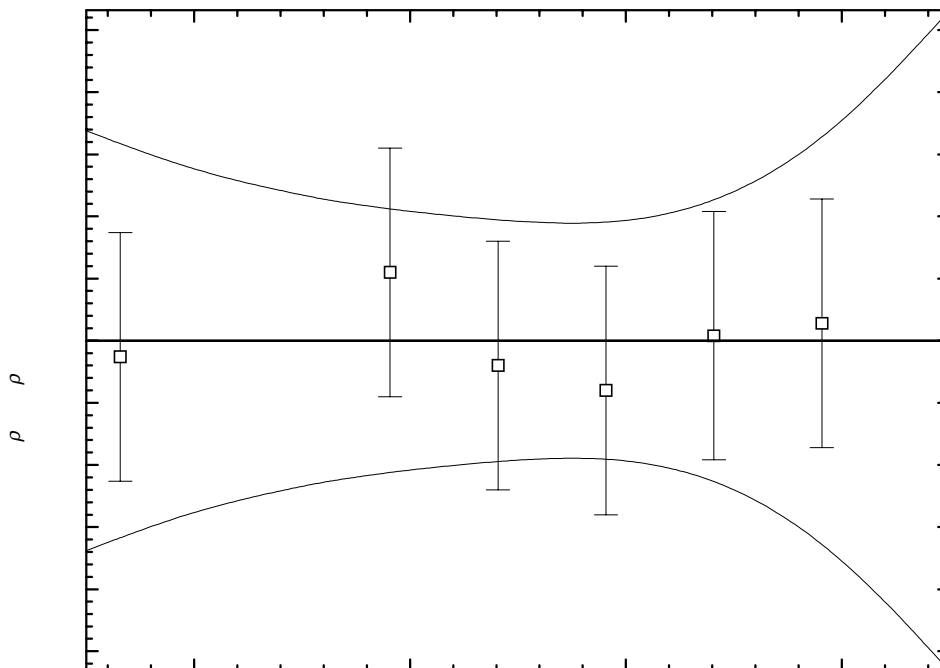
$\sigma_{c,uw} = 1.5019 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 338.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$9.86877 \cdot 10^2$
B	$-3.15853 \cdot 10^{-1}$
C	$-7.40820 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref. (Symbol in Fig. 1)	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref. (Symbol in Fig. 1)
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>		K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
273.15	845.20 ± 1.00	-0.13	39-owe/qua(□)	318.15	811.00 ± 1.00	-0.40	39-owe/qua(□)
298.15	827.40 ± 1.00	0.55	39-owe/qua(□)	328.15	803.50 ± 1.00	0.04	39-owe/qua(□)
308.15	819.00 ± 1.00	-0.20	39-owe/qua(□)	338.15	795.50 ± 1.00	0.14	39-owe/qua(□)

cont.

**6-Methyl-6-dodecanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	847.59 ± 1.69	298.15	826.85 ± 1.06	330.00	801.97 ± 1.14
280.00	840.36 ± 1.36	300.00	825.45 ± 1.04	340.00	793.85 ± 1.71
290.00	832.98 ± 1.17	310.00	817.77 ± 0.95	350.00	785.58 ± 2.66
293.15	830.62 ± 1.12	320.00	809.94 ± 0.93		

**4-(1-Methylethyl)-3,3,6-trimethyl-4-heptanol**

[900002-20-2]

C<sub>13</sub>H<sub>28</sub>O

MW = 200.36

424

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	864.8 ± 1.0	54-mos/cox

**5-(2-Methylpropyl)-5-nonanol** [500013-26-3] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 425

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
288.15	843.8 ± 1.5	37-pet/mal

**2,2,3,3,4-Pentamethyl-4-octanol** [100799-11-9] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 426

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	876.3 ± 2.0	60-pet/kao

**5-Propyl-5-decanol** [62958-41-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 427

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	832.0 ± 2.0	44-qua/sma

**4-Propyl-3,3,6-trimethyl-4-heptanol** [900002-21-3] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 428

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	859.8 ± 1.0	54-mos/cox

**1-Tridecanol** [112-70-9] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 429

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.476$ .

Coefficient	$\rho = A + BT$
$A$	1022.21
$B$	-0.640

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
323.15	816.5 ± 1.0	1.10	63-vil/gav
313.15	821.5 ± 0.6	-0.30	77-bel/bub
333.15	808.9 ± 0.6	-0.10	77-bel/bub

cont.

**1-Tridecanol** (cont.)**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
310.00	823.8 ± 1.0	330.00	811.0 ± 0.9
320.00	817.4 ± 0.8	340.00	804.6 ± 1.2

**2-Tridecanol**

[1653-31-2]

C<sub>13</sub>H<sub>28</sub>O

MW = 200.36

430

**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 0.944$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1035.14
<i>B</i>	-0.700

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
307.25	821.5 ± 2.0	1.43	11-pic/ken
320.45	810.9 ± 2.0	0.07	11-pic/ken
333.75	801.2 ± 2.0	-0.32	11-pic/ken
287.65	832.6 ± 2.0	-1.19	12-pic/ken

**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
280.00	839.1 ± 3.8	298.15	826.4 ± 2.5	330.00	804.1 ± 2.7
290.00	832.1 ± 3.0	310.00	818.1 ± 2.0	340.00	797.1 ± 3.4
293.15	829.9 ± 2.8	320.00	811.1 ± 2.2		

**3-Tridecanol**

[10289-68-6]

C<sub>13</sub>H<sub>28</sub>O

MW = 200.36

431

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
353.15	786.5 ± 3.0	13-pic/ken

**4-Tridecanol**

[26215-92-9]

C<sub>13</sub>H<sub>28</sub>O

MW = 200.36

432

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	823.4 ± 2.0	48-pet/old

**2,2,3-Trimethyl-4-propyl-3-heptanol** [500002-64-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 433

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
285.15	859.0 ± 2.0	37-naz

**2,3,6-Trimethyl-1-decanol** [500002-12-0] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 434

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	835.1 ± 2.0	38-wer/bog

**2,5,9-Trimethyl-5-decanol** [500001-91-2] C<sub>13</sub>H<sub>28</sub>O MW = 200.36 435

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
284.15	844.4 ± 2.0	28-esc

**5-Butyl-5-decanol** [5340-34-1] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 436

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.926$ .

Coefficient	$\rho = A + BT$
$A$	1048.44
$B$	-0.720

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
298.15	834.5 ± 2.0	0.73	33-whi/wil
298.15	834.8 ± 2.0	1.03	44-qua/sma
318.15	818.9 ± 2.0	-0.47	44-qua/sma
328.15	810.9 ± 2.0	-1.27	44-qua/sma
293.15	845.4 ± 6.0	8.03	61-mes/erz <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>	K	kg · m <sup>-3</sup>	K	kg · m <sup>-3</sup>
290.00	839.6 ± 2.7	298.15	833.8 ± 2.1	320.00	818.0 ± 1.9
293.15	837.4 ± 2.4	310.00	825.2 ± 1.7	330.00	810.8 ± 2.6



**2,2-Dimethyl-3-(1,1-dimethylethyl)-3-octanol** [500045-08-9] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 437

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	861.4 ± 1.5	60-pet/sok

**3,3-Dimethyl-4-(1,1-dimethylethyl)-4-octanol** [900002-34-8] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 438

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	873.4 ± 1.0	54-mos/cox

**2,2-Dimethyl-1-dodecanol** [92318-63-3] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 439

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	836.3 ± 2.0	64-blo/hag

**3,3-Dimethyl-4-(2-methylpropyl)-4-octanol** [900002-22-4] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 440

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	856.8 ± 1.0	54-mos/cox

**4-(1,1-Dimethylethyl)-3,3,6-trimethyl-4-heptanol** [900002-25-7] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 441

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	879.4 ± 1.0	54-mos/cox

**5-(2,2-Dimethylpropyl)-5-nonanol** [5340-38-5] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 442

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	832.0 ± 3.0	38-whi/pop-1 <sup>1)</sup>
293.15	840.3 ± 2.0	42-whi/for
293.15	840.3 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**7-Ethyl-2-methyl-4-undecanol** [103-20-8] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 443

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
20.00	834.1 ± 1.0	58-ano-5

**2-Methyl-3-(1-methylethyl)-3-decanol** [57233-27-9] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 444

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	856.2 ± 2.0	62-pet/kap

**2-Methyl-2-tridecanol** [32836-44-5] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 445

**Table 1.** Experimental values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
289.75	832.0 ± 2.0	19-eyk
354.95	784.1 ± 4.0	19-eyk

**2-Methyl-3-tridecanol** [98930-89-3] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 446

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	839.0 ± 2.0	12-pic/ken

**4-Methyl-4-tridecanol** [116436-16-9] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 447

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
297.15	829.2 ± 2.0	19-eyk

**11-Methyl-1-tridecanol** [20194-46-1] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 448

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	834.4 ± 1.0	62-lar/sal

**L(+)-11-Methyl-1-tridecanol** [500006-93-9] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 449

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	834.4 ± 0.6	62-lar/sal

**6-(1-Methylethyl)-6-undecanol** [500002-69-7] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 450

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	842.5 ± 1.0	46-hus/bai

**4-(2-Methylpropyl)-2,2,6-trimethyl-4-heptanol** [500002-08-4] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 451

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	831.7 ± 2.0	42-whi/for

**4-(2-Methylpropyl)-3,3,6-trimethyl-4-heptanol** [900002-24-6] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 452

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	853.0 ± 1.0	54-mos/cox

**2,2,3,3,4-Pentamethyl-4-nonanol** [108272-61-3] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 453

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	875.1 ± 2.0	60-pet/kao

**4,4,5,6,6-Pentamethyl-5-nonanol** [500002-06-2] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 454

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	887.6 ± 2.0	37-naz

**2-Pentyl-1-nonanol** [5333-48-2] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 455

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	840.5 ± 2.0	01-gue
297.15	837.7 ± 2.0	38-mas

**4-Propyl-3,3,5,5-tetramethyl-4-heptanol** [900002-88-2] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 456

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	888.2 ± 1.0	54-mos/cox

**6-Propyl-6-undecanol** [500002-03-9] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 457

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	833.6 ± 2.0	33-whi/wil

**1-Tetradecanol** [112-72-1] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 458

**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 8.9110 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 1.2677 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $573.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.01416 \cdot 10^3$
B	$-5.58592 \cdot 10^{-1}$
C	$-1.11840 \cdot 10^{-4}$
D	$-2.07120 \cdot 10^{-7}$

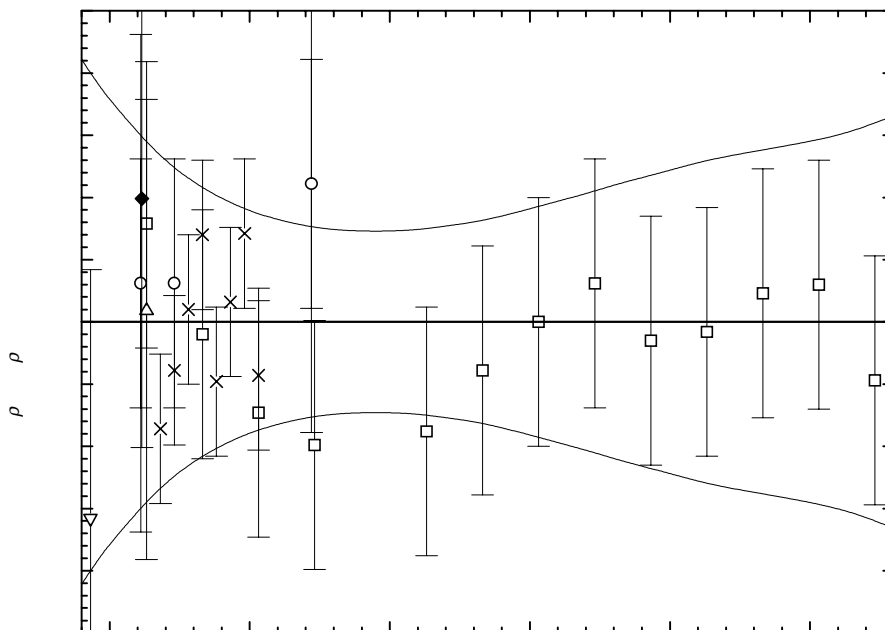
**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
311.15	823.60 ± 2.00	0.31	1883-kra(○)	433.15	734.00 ± 1.00	-0.39	58-cos/bow(□)
311.15	823.60 ± 1.00	0.31	1883-kra(○)	453.15	718.80 ± 1.00	0.00	58-cos/bow(□)
323.15	815.30 ± 1.00	0.31	1883-kra(○)	473.15	703.20 ± 1.00	0.31	58-cos/bow(□)
323.15	815.30 ± 2.00	0.31	1883-kra <sup>1)</sup>	493.15	686.50 ± 1.00	-0.15	58-cos/bow(□)
372.05	781.30 ± 1.00	1.11	1883-kra(○)	513.15	670.00 ± 1.00	-0.08	58-cos/bow(□)
372.05	781.30 ± 2.00	1.11	1883-kra(○)	533.15	653.40 ± 1.00	0.23	58-cos/bow(□)
311.55	824.00 ± 2.00	0.99	49-tsv/mar(◆)	553.15	636.20 ± 1.00	0.30	58-cos/bow(□)
313.15	822.00 ± 2.00	0.09	56-rat/cur(Δ)	573.15	617.80 ± 1.00	-0.47	58-cos/bow(□)
333.15	807.00 ± 2.00	-1.00	56-rat/cur <sup>1)</sup>	318.15	817.60 ± 0.60	-0.86	92-lie/sen-1(X)
353.15	794.00 ± 2.00	0.17	56-rat/cur <sup>1)</sup>	323.15	814.60 ± 0.60	-0.39	92-lie/sen-1(X)
293.15	834.00 ± 2.00	-1.58	58-ano-3(∇)	328.15	811.60 ± 0.60	0.10	92-lie/sen-1(X)
313.15	822.70 ± 1.00	0.79	58-cos/bow(□)	333.15	808.70 ± 0.60	0.70	92-lie/sen-1(X)
333.15	807.90 ± 1.00	-0.10	58-cos/bow(□)	338.15	804.00 ± 0.60	-0.48	92-lie/sen-1(X)
353.15	793.10 ± 1.00	-0.73	58-cos/bow(□)	343.15	801.10 ± 0.60	0.16	92-lie/sen-1(X)
373.15	778.40 ± 1.00	-0.99	58-cos/bow(□)	348.15	798.10 ± 0.60	0.71	92-lie/sen-1(X)
393.15	766.60 ± 1.00	1.92	58-cos/bow <sup>1)</sup>	353.15	793.40 ± 0.60	-0.43	92-lie/sen-1(X)
413.15	748.80 ± 1.00	-0.88	58-cos/bow(□)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [60-pet/kao, 60-pet/sok, 63-vil/gav].

cont.

**1-Tetradecanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	837.71 ± 2.11	380.00	774.38 ± 0.74	490.00	689.23 ± 1.16
293.15	835.58 ± 2.00	390.00	767.01 ± 0.73	500.00	681.02 ± 1.22
298.15	832.19 ± 1.84	400.00	759.58 ± 0.73	510.00	672.72 ± 1.28
300.00	830.93 ± 1.79	410.00	752.06 ± 0.74	520.00	664.33 ± 1.33
310.00	824.08 ± 1.52	420.00	744.48 ± 0.77	530.00	655.86 ± 1.37
320.00	817.17 ± 1.29	430.00	736.82 ± 0.80	540.00	647.30 ± 1.41
330.00	810.20 ± 1.12	440.00	729.09 ± 0.85	550.00	638.65 ± 1.45
340.00	803.17 ± 0.99	450.00	721.27 ± 0.91	560.00	629.90 ± 1.50
350.00	796.07 ± 0.89	460.00	713.38 ± 0.97	570.00	621.07 ± 1.57
360.00	788.91 ± 0.82	470.00	705.42 ± 1.03	580.00	612.14 ± 1.66
370.00	781.68 ± 0.77	480.00	697.36 ± 1.10		

**3-Tetradecanol** [1653-32-3] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 459

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
353.15	788.5 ± 2.0	13-pic/ken

**4-Tetradecanol** [1653-33-4] C<sub>14</sub>H<sub>30</sub>O MW = 214.39 460

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
305.15	823.1 ± 3.0	48-pet/old

**4-Butyl-3,3,5,5-tetramethyl-4-heptanol** [900002-89-3] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 461

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	884.9 ± 1.0	54-mos/cox

**6-Butyl-6-undecanol** [5396-08-7] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 462

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	834.4 ± 2.0	33-whi/wil

**2,2-Dimethyl-3-(1,1-dimethylethyl)-3-nonanol** [101082-11-5] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 463

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	860.3 ± 2.0	57-pet/sok
293.15	860.3 ± 2.0	60-pet/sok

**2,8-Dimethyl-5-(2-methylpropyl)-5-nonanol** [500002-16-4] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 464

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.060$ .

Coefficient	$\rho = A + BT$
$A$	1068.38
$B$	-0.800

cont.

**2,8-Dimethyl-5-(2-methylpropyl)-5-nonanol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
273.15	849.8 ± 2.0	-0.06	04-gri
283.55	841.6 ± 2.0	0.06	04-gri
273.15	849.8 ± 2.0	-0.06	04-gri-1
283.55	841.6 ± 2.0	0.06	04-gri-1

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	852.4 ± 1.8
280.00	844.4 ± 1.8
290.00	836.4 ± 1.9

**6,10-Dimethyl-2-tridecanol**

[101082-12-6]

C<sub>15</sub>H<sub>32</sub>O

MW = 228.42

465

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	830.3 ± 1.0	49-naz/zar-1
293.15	888.2 ± 2.0	61-shv/pet <sup>1)</sup>
293.15	830.3 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**2-Methyl-2-tetradecanol**

[27570-83-8]

C<sub>15</sub>H<sub>32</sub>O

MW = 228.42

466

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	836.0 ± 2.0	42-pet/che
293.15	838.0 ± 2.0	57-for/lan
293.15	837.0 ± 2.1	Recommended

**6-(2-Methylpropyl)-6-undecanol**

[500002-70-0]

C<sub>15</sub>H<sub>32</sub>O

MW = 228.42

467

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	836.7 ± 2.0	46-hus/bai

**1-Pentadecanol** [629-76-5] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 468

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.350$ .

Coefficient	$\rho = A + BT$
A	1025.57
B	-0.640

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
295.55	836.4 ± 2.0	-0.01	47-sto <sup>1)</sup>
323.15	819.2 ± 2.0	0.45	63-vil/gav <sup>1)</sup>
313.15	824.8 ± 0.6	-0.35	77-bel/bub
333.15	812.7 ± 0.6	0.35	77-bel/bub

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
310.00	827.2 ± 0.8
320.00	820.8 ± 0.5
330.00	814.4 ± 0.6
340.00	808.0 ± 1.0

**3-Pentadecanol** [53346-71-7] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 469

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
353.15	792.1 ± 3.0	13-pic/ken

**3,7,11-Trimethyl-3-dodecanol** [7278-65-1] C<sub>15</sub>H<sub>32</sub>O MW = 228.42 470

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	838.7 ± 2.0	58-naz/gus



**2-Butyl-1-dodecanol****[21078-85-3]****C<sub>16</sub>H<sub>34</sub>O****MW = 242.45****471****Table 1.** Coefficients of the polynomial expansion equation.

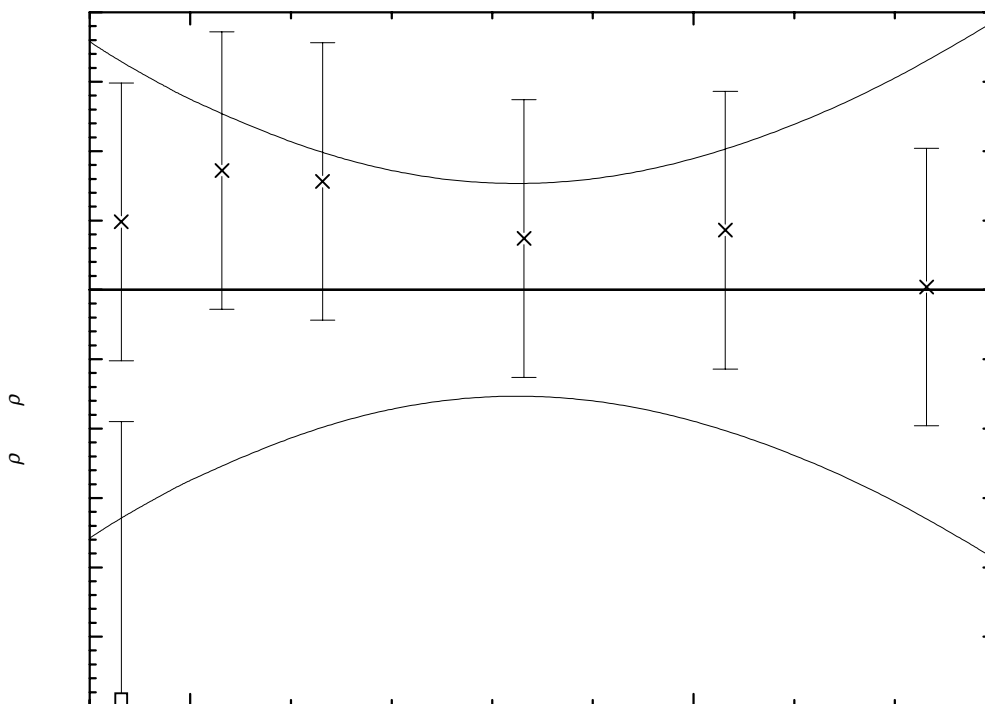
Standard deviations (see introduction):

 $\sigma_{c,w} = 7.9175 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 5.0211 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	T = 293.15 to 373.15 K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.03807 \cdot 10^3$
B	$-6.84381 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	$837.94 \pm 1.00$	0.49	33-bin/ste(✕)	353.15	$796.81 \pm 1.00$	0.43	33-bin/ste(✕)
303.15	$831.46 \pm 1.00$	0.86	33-bin/ste(✕)	373.15	$782.72 \pm 1.00$	0.02	33-bin/ste(✕)
313.15	$824.54 \pm 1.00$	0.78	33-bin/ste(✕)	293.15	$834.50 \pm 2.00$	-2.95	35-cox/rei(□)
333.15	$810.44 \pm 1.00$	0.37	33-bin/ste(✕)				

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  
 $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	839.60 ± 1.79	310.00	825.92 ± 1.05	350.00	798.54 ± 0.93
293.15	837.45 ± 1.64	320.00	819.07 ± 0.84	360.00	791.70 ± 1.18
298.15	834.03 ± 1.44	330.00	812.23 ± 0.75	370.00	784.85 ± 1.51
300.00	832.76 ± 1.37	340.00	805.38 ± 0.78	380.00	778.01 ± 1.94

**5-Butyl-5-dodecanol** [93314-38-6] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 472

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	841.5 ± 1.0	37-pet/and

**2,2-Dimethyl-3-(1,1-dimethylethyl)-3-decanol** [93314-37-5] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 473

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	865.6 ± 2.0	62-pet/kap

**2,2-Dimethyl-1-tetradecanol** [5286-18-0] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 474

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	840.0 ± 2.0	64-blo/hag

**2,2-Dimethyl-3-tetradecanol** [500000-42-0] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 475

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	835.6 ± 1.0	41-whi/whi

**2-Ethyl-1-tetradecanol** [25354-99-8] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 476

**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction):

$\sigma_{c,w} = 8.6253 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 5.4877 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

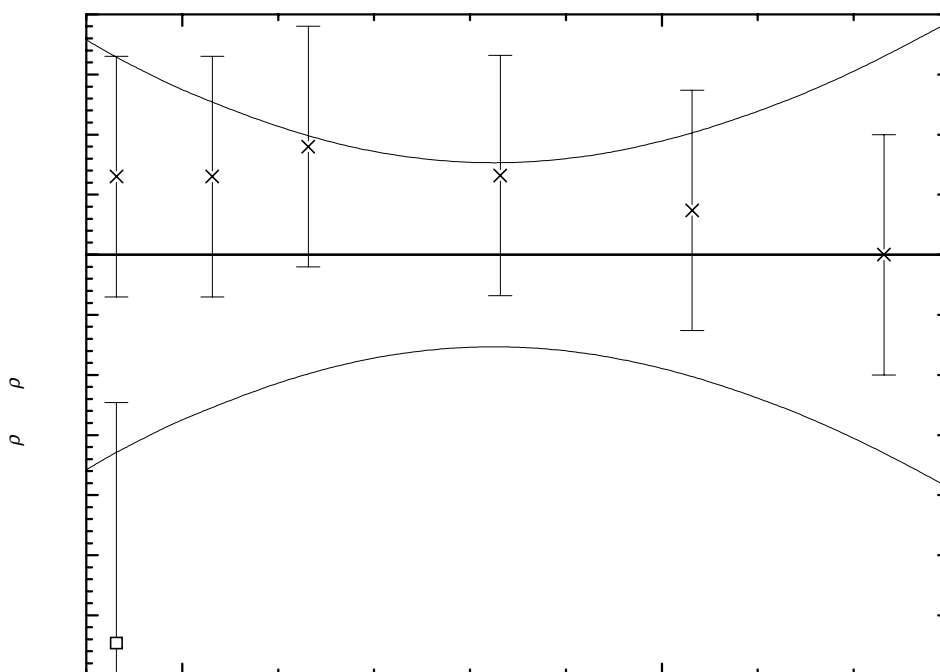
Coefficient	$T = 293.15$ to $373.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.04120 \cdot 10^3$
B	$-6.86917 \cdot 10^{-1}$

cont.

## 2-Ethyl-1-tetradecanol (cont.)

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
293.15	840.48 ± 1.00	0.65	33-bin/ste(X)	353.15	798.98 ± 1.00	0.37	33-bin/ste(X)
303.15	833.61 ± 1.00	0.65	33-bin/ste(X)	373.15	784.87 ± 1.00	-0.00	33-bin/ste(X)
313.15	826.99 ± 1.00	0.90	33-bin/ste(X)	293.15	836.60 ± 2.00	-3.23	35-cox/rei(□)
333.15	813.01 ± 1.00	0.66	33-bin/ste(X)				

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	841.99 ± 1.79	310.00	828.25 ± 1.05	350.00	800.78 ± 0.93
293.15	839.83 ± 1.64	320.00	821.38 ± 0.84	360.00	793.91 ± 1.18
298.15	836.39 ± 1.44	330.00	814.51 ± 0.75	370.00	787.04 ± 1.51
300.00	835.12 ± 1.37	340.00	807.65 ± 0.78	380.00	780.17 ± 1.94

**3-Ethyl-3-tetradecanol** [101433-18-5] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 477

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
288.45	846.0 ± 3.0	19-eyk

**2-Heptyl-1-nonanol** [25355-03-7] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 478

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 1.3014 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 6.5072 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	T = 293.15 to 373.15 K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	1.00360 · 10 <sup>3</sup>
B	-4.62418 · 10 <sup>-1</sup>
C	-3.53389 · 10 <sup>-4</sup>

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	837.59 ± 1.00	-0.09	33-bin/ste(□)	333.15	810.24 ± 1.00	-0.09	33-bin/ste(□)
303.15	830.91 ± 1.00	-0.04	33-bin/ste(□)	353.15	796.11 ± 1.00	-0.12	33-bin/ste(□)
313.15	824.40 ± 1.00	0.26	33-bin/ste(□)	373.15	781.92 ± 1.00	0.07	33-bin/ste(□)

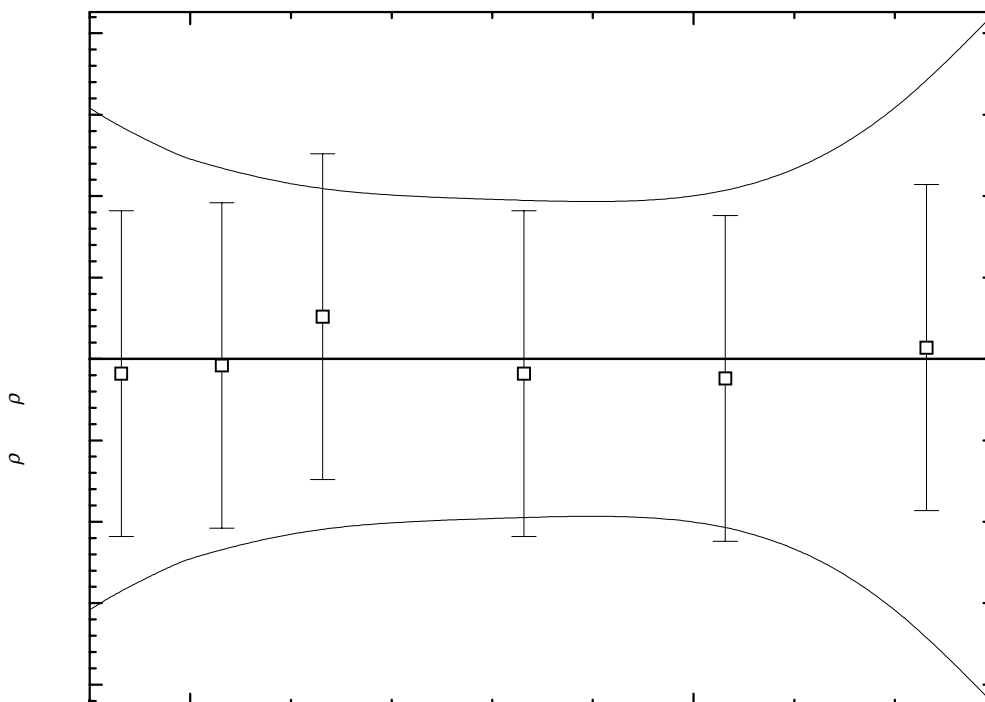
**Further references:** [35-cox/rei].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	839.78 ± 1.54	310.00	826.29 ± 1.06	350.00	798.47 ± 0.98
293.15	837.68 ± 1.42	320.00	819.44 ± 1.00	360.00	791.33 ± 1.13
298.15	834.32 ± 1.27	330.00	812.52 ± 0.98	370.00	784.13 ± 1.50
300.00	833.07 ± 1.22	340.00	805.53 ± 0.96	380.00	776.86 ± 2.13

cont.

**2-Heptyl-1-nonanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**1-Hexadecanol**

[36653-82-4]

C<sub>16</sub>H<sub>34</sub>O

MW = 242.45

479

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 2.9130 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 5.8696 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 321.15 \text{ to } 573.15 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$
<i>A</i>	$9.25311 \cdot 10^2$
<i>B</i>	$1.01083 \cdot 10^{-1}$
<i>C</i>	$-1.68710 \cdot 10^{-3}$
<i>D</i>	$1.06172 \cdot 10^{-6}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

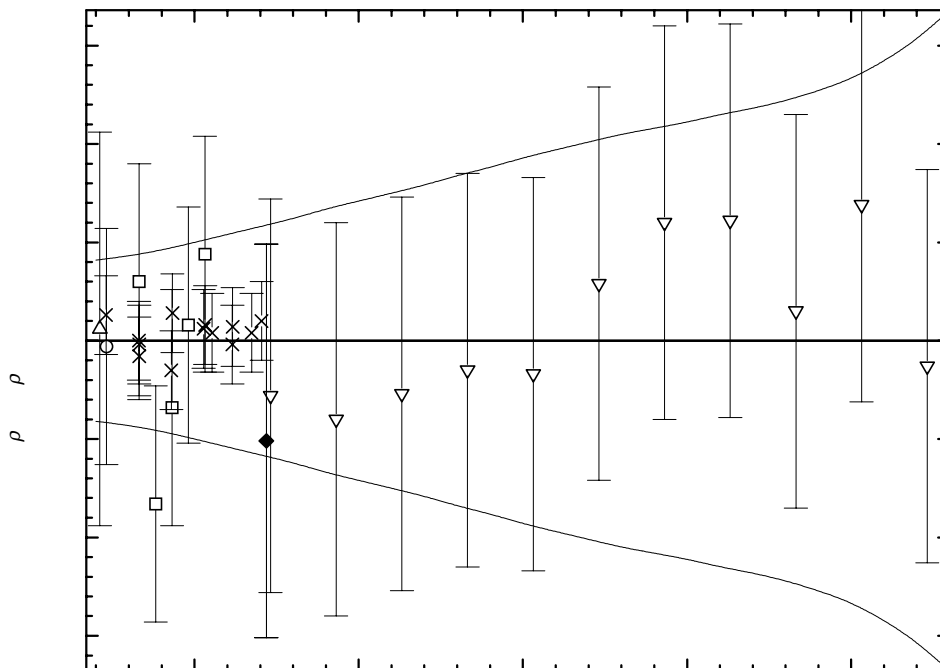
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
<i>crystal</i>				513.15	677.00 ± 1.00	0.61	58-cos/bow(∇)
78.15	1000.0 ± 3.0		30-bil/fis-1	533.15	660.70 ± 1.00	0.15	58-cos/bow(∇)
194.15	974.0 ± 3.0		30-bil/fis-1	553.15	645.40 ± 1.00	0.69	58-cos/bow(∇)
<i>liquid</i>				573.15	628.80 ± 1.00	-0.13	58-cos/bow(∇)
322.65	817.60 ± 1.00	-0.36	1883-kra <sup>1)</sup>	323.08	817.80 ± 0.20	0.13	73-fin(×)
322.65	817.60 ± 1.00	-0.36	1883-kra <sup>1)</sup>	333.09	811.04 ± 0.20	0.00	73-fin(×)
333.15	810.50 ± 1.00	-0.50	1883-kra <sup>1)</sup>	333.14	810.98 ± 0.20	-0.02	73-fin(×)
333.15	810.50 ± 1.00	-0.50	1883-kra <sup>1)</sup>	333.15	810.92 ± 0.20	-0.08	73-fin(×)
371.85	783.70 ± 1.00	-0.51	1883-kra(◆)	342.95	804.23 ± 0.20	-0.15	73-fin(×)
371.85	783.70 ± 1.00	-0.51	1883-kra(◆)	343.26	804.30 ± 0.20	0.14	73-fin(×)
298.15	888.60 ± 0.60	54.98	38-bak/smy <sup>1)</sup>	352.77	797.69 ± 0.20	0.06	73-fin(×)
323.15	817.60 ± 0.60	-0.03	38-bak/smy(○)	353.19	797.42 ± 0.20	0.08	73-fin(×)
321.15	819.00 ± 1.00	0.06	53-kre-1(Δ)	355.38	795.85 ± 0.20	0.04	73-fin(×)
323.15	817.60 ± 1.00	-0.03	53-kre-1 <sup>1)</sup>	361.46	791.54 ± 0.20	-0.02	73-fin(×)
333.15	810.50 ± 1.00	-0.50	58-cos/bow <sup>1)</sup>	361.61	791.53 ± 0.20	0.07	73-fin(×)
353.15	797.10 ± 1.00	-0.26	58-cos/bow <sup>1)</sup>	367.39	787.42 ± 0.20	0.04	73-fin(×)
373.15	783.00 ± 1.00	-0.28	58-cos/bow(∇)	370.40	785.34 ± 0.20	0.10	73-fin(×)
393.15	768.40 ± 1.00	-0.40	58-cos/bow(∇)	333.15	811.30 ± 0.60	0.30	92-lie/sen-1(□)
413.15	753.70 ± 1.00	-0.27	58-cos/bow(∇)	338.15	806.80 ± 0.60	-0.83	92-lie/sen-1(□)
433.15	738.70 ± 1.00	-0.15	58-cos/bow(∇)	343.15	803.90 ± 0.60	-0.34	92-lie/sen-1(□)
453.15	723.30 ± 1.00	-0.17	58-cos/bow(∇)	348.15	800.90 ± 0.60	0.08	92-lie/sen-1(□)
473.15	708.20 ± 1.00	0.29	58-cos/bow(∇)	353.15	797.80 ± 0.60	0.44	92-lie/sen-1(□)
493.15	692.80 ± 1.00	0.60	58-cos/bow(∇)				

<sup>1)</sup> Not included in Fig. 1.**Further references:** [1893-eyk, 22-tro, 31-del, 49-hos/ste, 50-boe/ned, 56-rat/cur, 63-vil/gav, 69-kat/pat].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
320.00	819.69 ± 0.41	410.00	756.33 ± 0.75	500.00	686.79 ± 1.11
330.00	813.10 ± 0.43	420.00	748.82 ± 0.79	510.00	678.89 ± 1.15
340.00	806.38 ± 0.46	430.00	741.25 ± 0.84	520.00	670.97 ± 1.18
350.00	799.54 ± 0.50	440.00	733.61 ± 0.88	530.00	663.04 ± 1.22
360.00	792.59 ± 0.54	450.00	725.91 ± 0.93	540.00	655.12 ± 1.27
370.00	785.53 ± 0.58	460.00	718.16 ± 0.97	550.00	647.20 ± 1.33
380.00	778.36 ± 0.62	470.00	710.37 ± 1.01	560.00	639.30 ± 1.42
390.00	771.11 ± 0.67	480.00	702.54 ± 1.05	570.00	631.41 ± 1.53
400.00	763.76 ± 0.71	490.00	694.68 ± 1.08	580.00	623.55 ± 1.68

cont.

**1-Hexadecanol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3-Hexadecanol** [593-03-3] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 480

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
353.15	790.7 ± 2.0	13-pic/ken

**2-Hexyl-1-decanol** [2425-77-6] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 481

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 1.1013$  (combined temperature ranges, weighted),

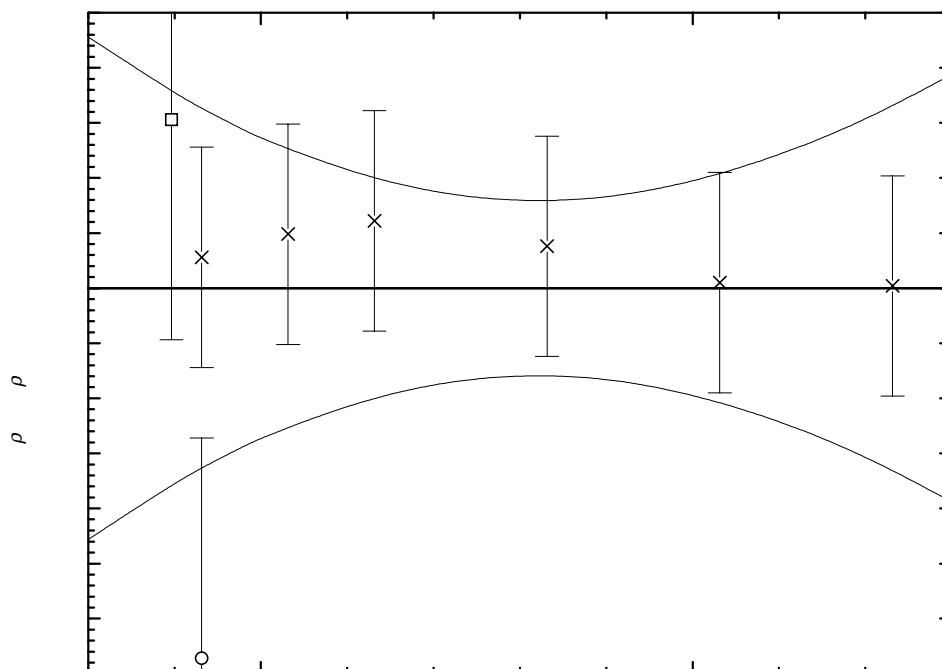
$\sigma_{\text{c,uw}} = 5.0818 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 289.65$ to $373.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.03893 \cdot 10^3$
B	$-6.88973 \cdot 10^{-1}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	837.24 ± 1.00	0.28	33-bin/ste(×)	353.15	795.67 ± 1.00	0.05	33-bin/ste(×)
303.15	830.56 ± 1.00	0.49	33-bin/ste(×)	373.15	781.86 ± 1.00	0.02	33-bin/ste(×)
313.15	823.79 ± 1.00	0.61	33-bin/ste(×)	293.15	833.60 ± 2.00	-3.36	35-cox/rei(O)
333.15	809.78 ± 1.00	0.38	33-bin/ste(×)	289.65	840.90 ± 2.00	1.53	38-mas(□)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
280.00	846.02 ± 2.28	310.00	825.35 ± 1.06	360.00	790.90 ± 1.20
290.00	839.13 ± 1.77	320.00	818.46 ± 0.86	370.00	784.01 ± 1.52
293.15	836.96 ± 1.63	330.00	811.57 ± 0.78	380.00	777.12 ± 1.94
298.15	833.51 ± 1.43	340.00	804.68 ± 0.81		
300.00	832.24 ± 1.36	350.00	797.79 ± 0.96		



**2-Methyl-1-pentadecanol** [25354-98-7] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 482

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	832.0 ± 1.0	35-cox/rei

**2-Methyl-2-pentadecanol** [60129-23-9] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 483

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.35	826.5 ± 2.0	19-eyk
353.95	764.0 ± 2.0	19-eyk

**6-Methyl-6-pentadecanol** [108836-86-8] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 484

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	831.6 ± 2.0	30-dav/dix

**9-Methyl-7-pentadecanol** [500002-20-0] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 485

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	835.1 ± 2.0	12-gue

**2-Pentyl-1-undecanol** [25355-02-6] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 486

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 7.9132 \cdot 10^{-1}$  (combined temperature ranges, weighted),

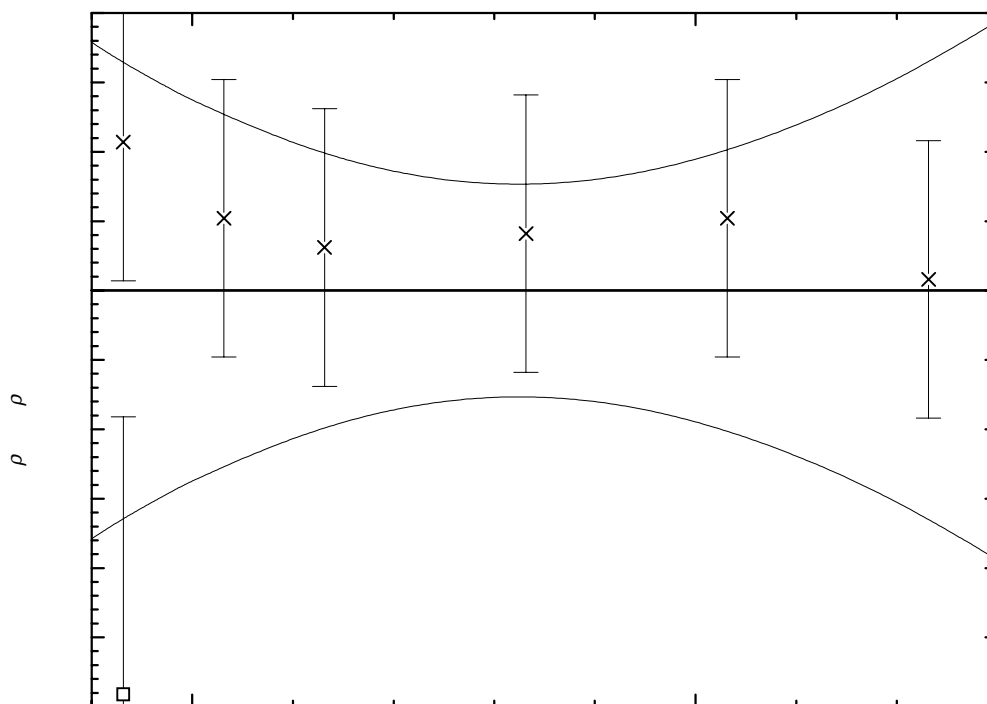
$\sigma_{\text{c,uw}} = 4.9799 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $373.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.03716 \cdot 10^3$
B	$-6.82767 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	838.08 ± 1.00	1.07	33-bin/ste(✕)	353.15	796.56 ± 1.00	0.52	33-bin/ste(✕)
303.15	830.70 ± 1.00	0.52	33-bin/ste(✕)	373.15	782.47 ± 1.00	0.08	33-bin/ste(✕)
313.15	823.66 ± 1.00	0.31	33-bin/ste(✕)	293.15	834.10 ± 2.00	-2.91	35-cox/rei(□)
333.15	810.11 ± 1.00	0.41	33-bin/ste(✕)				

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	839.16 ± 1.79	310.00	825.50 ± 1.05	350.00	798.19 ± 0.93
293.15	837.01 ± 1.64	320.00	818.68 ± 0.84	360.00	791.37 ± 1.18
298.15	833.59 ± 1.44	330.00	811.85 ± 0.75	370.00	784.54 ± 1.51
300.00	832.33 ± 1.37	340.00	805.02 ± 0.78	380.00	777.71 ± 1.94

### 6-Pentyl-6-undecanol

[5331-63-5]

C<sub>16</sub>H<sub>34</sub>O

MW = 242.45

487

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	829.3 ± 2.0	33 -whi/wil -0

**2-Propyl-1-tridecanol****[25355-00-4]****C<sub>16</sub>H<sub>34</sub>O****MW = 242.45****488****Table 1.** Coefficients of the polynomial expansion equation.

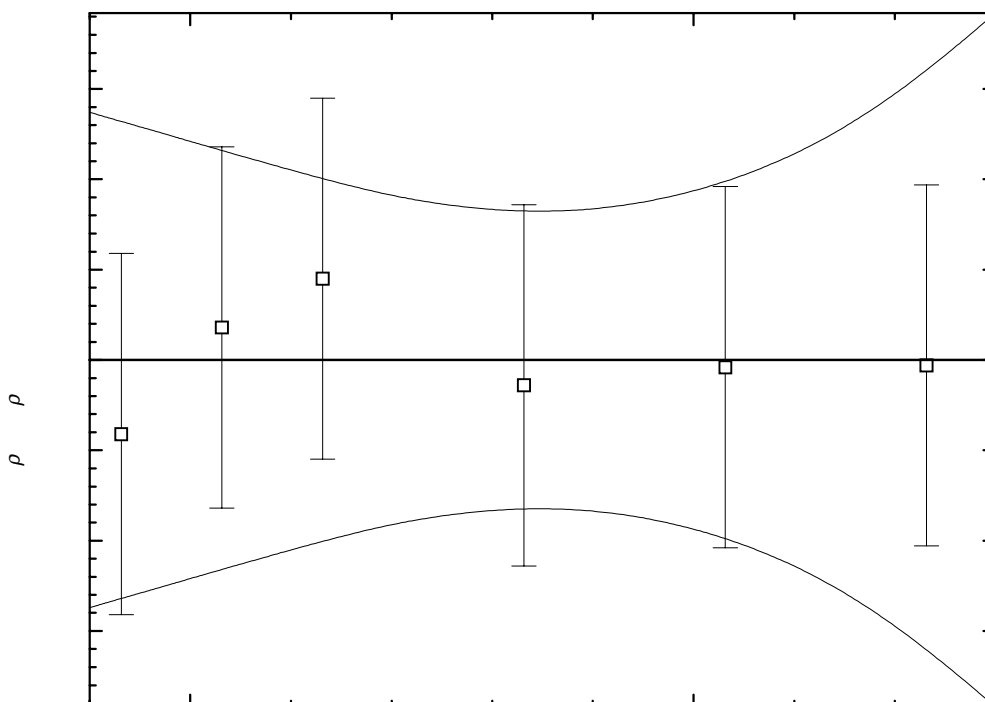
Standard deviations (see introduction):

 $\sigma_{c,w} = 2.6674 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.1929 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $373.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.04215 \cdot 10^3$
B	$-6.93516 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	$838.43 \pm 1.00$	-0.41	33-bin/ste(□)	333.15	$810.96 \pm 1.00$	-0.14	33-bin/ste(□)
303.15	$832.09 \pm 1.00$	0.18	33-bin/ste(□)	353.15	$797.19 \pm 1.00$	-0.04	33-bin/ste(□)
313.15	$825.42 \pm 1.00$	0.45	33-bin/ste(□)	373.15	$783.33 \pm 1.00$	-0.03	33-bin/ste(□)

**Further references:** [35-cox/rei].**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	841.03 ± 1.37	310.00	827.16 ± 1.05	350.00	799.42 ± 0.92
293.15	838.84 ± 1.32	320.00	820.22 ± 0.90	360.00	792.48 ± 1.12
298.15	835.38 ± 1.24	330.00	813.29 ± 0.82	370.00	785.55 ± 1.45
300.00	834.09 ± 1.21	340.00	806.35 ± 0.82	380.00	778.61 ± 1.92

**5-Propyl-4-tridecanol** [500002-21-1] C<sub>16</sub>H<sub>34</sub>O MW = 242.45 489

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
288.15	831.0 ± 2.0	48-pet/old

**3,9-Diethyl-6-tridecanol** [123-24-0] C<sub>17</sub>H<sub>36</sub>O MW = 256.47 490

**Table 1.** Experimental values with uncertainties.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	846.0 ± 1.0	53-ano-15
293.15	846.1 ± 1.0	58-ano-5

**1-Heptadecanol** [1454-85-9] C<sub>17</sub>H<sub>36</sub>O MW = 256.47 491

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
323.15	815.3 ± 2.0	63-vil/gav

**2-Heptadecanol** [16813-18-6] C<sub>17</sub>H<sub>36</sub>O MW = 256.47 492

**Table 1.** Experimental values with uncertainties.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	837.0 ± 2.0	19-wil/sch
273.15	847.0 ± 2.0	19-wil/sch

**8-Methyl-8-(2-methylpropyl)-6-dodecanol** [500002-24-4] C<sub>17</sub>H<sub>36</sub>O MW = 256.47 493

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	846.1 ± 2.0	61-des/del

**3-Ethyl-3-hexadecanol** [90002-70-2] C<sub>18</sub>H<sub>38</sub>O MW = 270.5 494

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
295.95	840.5 ± 2.0	19-eyk

**2-Heptyl-1-undecanol** [5333-44-8] C<sub>18</sub>H<sub>38</sub>O MW = 270.5 495

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
288.15	844.6 ± 2.0	38-mas

**1-Octadecanol** [112-92-5] C<sub>18</sub>H<sub>38</sub>O MW = 270.5 496

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 7.8077 \cdot 10^{-1}$  (combined temperature ranges, weighted),

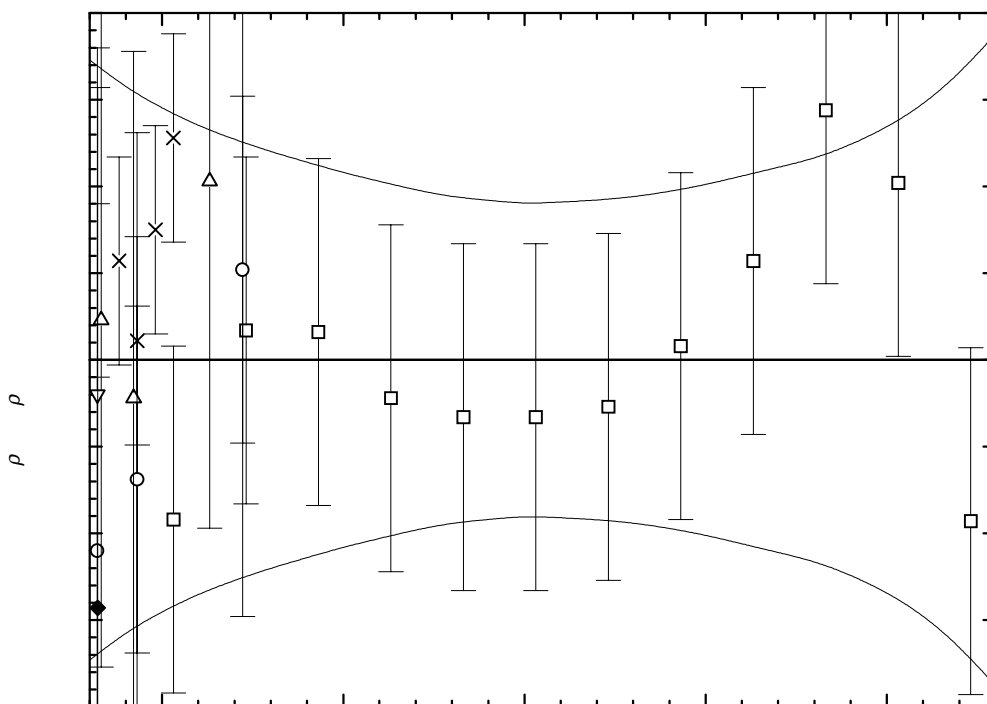
$\sigma_{\text{c,uw}} = 1.5346 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 332.15 \text{ to } 573.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.10078 \cdot 10^3$
B	-1.09517
C	$9.79822 \cdot 10^{-4}$
D	$-8.62705 \cdot 10^{-7}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref. (Symbol in Fig. 1)	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref. (Symbol in Fig. 1)
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>		K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
332.15	812.40 ± 1.00	-1.10	1883-kra(○)	413.15	754.50 ± 1.00	-0.22	58-cos/bow(□)
332.15	812.40 ± 2.00	-1.10	1883-kra(○)	433.15	739.80 ± 1.00	-0.33	58-cos/bow(□)
343.15	804.80 ± 2.00	-0.69	1883-kra(○)	453.15	725.10 ± 1.00	-0.33	58-cos/bow(□)
343.15	804.80 ± 1.00	-0.69	1883-kra(○)	473.15	710.30 ± 1.00	-0.27	58-cos/bow(□)
372.25	784.90 ± 2.00	0.52	1883-kra(○)	493.15	695.60 ± 1.00	0.08	58-cos/bow(□)
372.25	784.90 ± 1.00	0.52	1883-kra(○)	513.15	680.80 ± 1.00	0.57	58-cos/bow(□)
332.15	813.30 ± 2.00	-0.20	1884-kra(∇)	533.15	666.10 ± 1.00	1.44	58-cos/bow(□)
332.25	812.00 ± 3.00	-1.43	49-tsv/mar(◆)	553.15	649.80 ± 1.00	1.02	58-cos/bow(□)
333.15	813.00 ± 2.00	0.23	56-rat/cur(Δ)	573.15	631.60 ± 1.00	-0.93	58-cos/bow(□)
342.15	806.00 ± 2.00	-0.22	56-rat/cur(Δ)	338.15	809.70 ± 0.60	0.57	92-lie/sen-1(×)
363.15	792.00 ± 2.00	1.03	56-rat/cur(Δ)	343.15	805.60 ± 0.60	0.11	92-lie/sen-1(×)
353.15	797.30 ± 1.00	-0.92	58-cos/bow(□)	348.15	802.60 ± 0.60	0.75	92-lie/sen-1(×)
373.15	783.90 ± 1.00	0.17	58-cos/bow(□)	353.15	799.50 ± 0.60	1.28	92-lie/sen-1(×)
393.15	769.40 ± 1.00	0.16	58-cos/bow(□)				

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
330.00	815.07 ± 1.73	420.00	749.73 ± 0.98	510.00	682.66 ± 1.06
340.00	807.78 ± 1.57	430.00	742.44 ± 0.94	520.00	674.93 ± 1.11
350.00	800.51 ± 1.45	440.00	735.11 ± 0.92	530.00	667.14 ± 1.16
360.00	793.25 ± 1.35	450.00	727.75 ± 0.90	540.00	659.26 ± 1.24
370.00	786.01 ± 1.27	460.00	720.36 ± 0.91	550.00	651.30 ± 1.34
380.00	778.76 ± 1.20	470.00	712.92 ± 0.92	560.00	643.25 ± 1.47
390.00	771.52 ± 1.14	480.00	705.44 ± 0.94	570.00	635.11 ± 1.65
400.00	764.27 ± 1.08	490.00	697.91 ± 0.97	580.00	626.87 ± 1.88
410.00	757.01 ± 1.03	500.00	690.31 ± 1.01		

**3-Octadecanol** [26762-44-7] C<sub>18</sub>H<sub>38</sub>O MW = 270.5 497

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
353.15	785.8 ± 2.0	13-pic/ken

**2,2-Dimethyl-3-(1,1-dimethylethyl)-3-tridecanol** [500045-09-0] C<sub>19</sub>H<sub>40</sub>O MW = 284.53 498

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	869.8 ± 1.5	60-pet/sok

**7-Hexyl-7-tridecanol** [5340-59-0] C<sub>19</sub>H<sub>40</sub>O MW = 284.53 499

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	840.8 ± 2.0	61-mes/erz

**4-Methyl-4-octadecanol** [54892-13-6] C<sub>19</sub>H<sub>40</sub>O MW = 284.53 500

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	839.4 ± 1.0	48-sor/sor

**5-Methyl-5-octadecanol** [500020-99-5] C<sub>19</sub>H<sub>40</sub>O MW = 284.53 501

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	837.4 ± 0.6	48-sor/sor

**6-Methyl-6-octadecanol** [500021-00-1] C<sub>19</sub>H<sub>40</sub>O MW = 284.53 502

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	838.5 ± 1.0	48-sor/sor

**9-Methyl-9-octadecanol** [500021-01-2] C<sub>19</sub>H<sub>40</sub>O MW = 284.53 503

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	835.5 ± 1.0	48-sor/sor

**1-Eicosanol** [629-96-9] C<sub>20</sub>H<sub>42</sub>O MW = 298.55 504

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.189$ .

Coefficient	$\rho = A + BT$
$A$	1056.70
$B$	-0.720

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
348.15	805.9 ± 0.50	-0.13	69-pat/kat
358.15	798.7 ± 0.50	-0.13	69-pat/kat
368.15	791.9 ± 0.50	0.27	69-pat/kat

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>
340.00	811.9 ± 1.0
350.00	804.7 ± 0.6
360.00	797.5 ± 0.5
370.00	790.3 ± 0.8

**3-Ethyl-3-octadecanol** [35185-53-6] C<sub>20</sub>H<sub>42</sub>O MW = 298.55 505

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
353.25	778.8 ± 3.0	19-eyk

**2-Methyl-2-nonadecanol** [76695-48-2] C<sub>20</sub>H<sub>42</sub>O MW = 298.55 506

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
352.95	771.7 ± 3.0	19-eyk



**2-Octyl-1-dodecanol** [5333-42-6] C<sub>20</sub>H<sub>42</sub>O MW = 298.55 507

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
292.15	846.3 ± 2.0	38-mas

**2,6,11,15-Tetramethyl-8-hexadecanol** [50002-33-5] C<sub>20</sub>H<sub>42</sub>O MW = 298.55 508

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
292.15	892.0 ± 2.0	23-von/kai

**1-Docosanol** [661-19-8] C<sub>22</sub>H<sub>46</sub>O MW = 326.61 509

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.094$ .

Coefficient	$\rho = A + BT$
$A$	1074.44
$B$	-0.770

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
348.15	806.3 ± 0.5	-0.07	69-pat/kat
358.15	798.6 ± 0.5	-0.07	69-pat/kat
368.15	791.1 ± 0.5	0.13	69-pat/kat

**Table 3.** Recommended values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$
K	kg · m <sup>-3</sup>	K	kg · m <sup>-3</sup>
340.00	812.6 ± 1.0	360.00	797.2 ± 0.5
350.00	804.9 ± 0.6	370.00	789.5 ± 0.7

**3-Ethyl-3-eicosanol** [95287-47-1] C<sub>22</sub>H<sub>46</sub>O MW = 326.61 510

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
353.20	780.0 ± 3.0	19-eyk

**2-Nonyl-1-tridecanol** [54439-52-0] C<sub>22</sub>H<sub>46</sub>O MW = 326.61 511

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
290.65	847.6 ± 2.0	38-mas

## 2.2 Unsaturated Monoalcohols

### 2.2.1 Alcohols of General Formula C<sub>n</sub>H<sub>2n</sub>O

**2-Propenol****[107-18-6]****C<sub>3</sub>H<sub>6</sub>O****MW = 58.08****512****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 8.0998 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.6309 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 440.00 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
<i>A</i>	$1.05862 \cdot 10^3$
<i>B</i>	$-1.61233$
<i>C</i>	$4.16485 \cdot 10^{-3}$
<i>D</i>	$-6.30190 \cdot 10^{-6}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

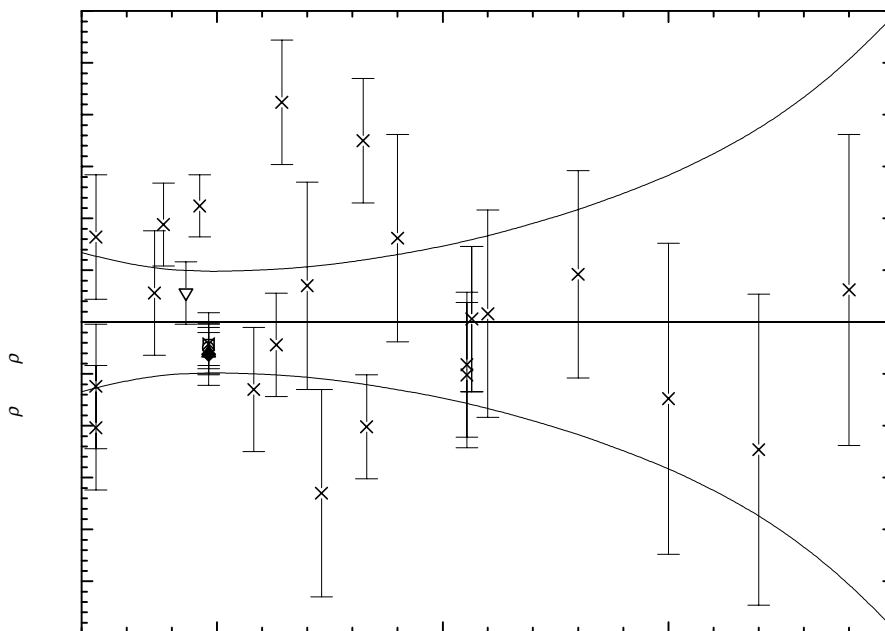
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.15	799.50 ± 0.60	-1.02	1882-zan(✕)	293.15	786.00 ± 0.40	0.88	52-cap/mug <sup>1)</sup>
290.15	785.10 ± 0.60	-2.39	1882-zan <sup>1)</sup>	298.15	781.50 ± 0.40	0.39	52-cap/mug <sup>1)</sup>
283.15	794.00 ± 1.00	1.06	1890-gar <sup>1)</sup>	298.15	780.89 ± 0.20	-0.22	52-wil/sim(□)
293.15	785.40 ± 1.00	0.28	1890-gar <sup>1)</sup>	298.15	780.80 ± 0.30	-0.31	54-bre(◆)
303.15	776.50 ± 1.00	-0.52	1890-gar <sup>1)</sup>	298.15	780.81 ± 0.20	-0.30	54-kre/wie(Δ)
313.15	767.50 ± 1.00	-1.12	1890-gar <sup>1)</sup>	298.15	780.86 ± 0.20	-0.25	54-pur/bow(O)
323.15	758.20 ± 1.00	-1.65	1890-gar(✕)	293.15	785.50 ± 0.50	0.38	56-tor-1 <sup>1)</sup>
286.15	790.90 ± 0.60	0.28	19-eyk(✕)	313.15	768.40 ± 0.50	-0.22	56-tor-1(✕)
273.15	799.90 ± 0.60	-0.62	25-pal/con(✕)	333.15	749.70 ± 0.50	-1.01	56-tor-1(✕)
355.35	728.30 ± 0.70	-0.51	27-arb-2(✕)	298.15	780.90 ± 0.30	-0.21	58-arn/was(✕)
355.35	728.40 ± 0.70	-0.41	27-arb-2(✕)	293.15	785.40 ± 0.30	0.28	63-amb/tow(V)
356.45	727.70 ± 0.70	0.03	27-arb-2(✕)	300.00	779.00 ± 1.00	-0.61	64-dan/bah <sup>1)</sup>
356.45	727.70 ± 0.70	0.03	27-arb-2(✕)	320.00	763.00 ± 1.00	0.35	64-dan/bah(✕)
273.15	801.34 ± 0.60	0.82	34-tim/del(✕)	340.00	745.00 ± 1.00	0.81	64-dan/bah(✕)
288.15	789.14 ± 0.60	0.08	34-tim/del <sup>1)</sup>	360.00	724.00 ± 1.00	0.08	64-dan/bah(✕)
303.15	776.88 ± 0.60	-0.14	34-tim/del <sup>1)</sup>	380.00	702.00 ± 1.00	0.46	64-dan/bah(✕)
308.15	772.21 ± 0.60	-0.65	43-lan/key(✕)	400.00	676.00 ± 1.50	-0.74	64-dan/bah(✕)
293.15	786.40 ± 0.60	1.28	48-vog-2 <sup>1)</sup>	420.00	648.00 ± 1.50	-1.23	64-dan/bah(✕)
314.35	769.70 ± 0.60	2.12	48-vog-2(✕)	440.00	619.00 ± 1.50	0.31	64-dan/bah(✕)
332.35	753.20 ± 0.60	1.75	48-vog-2(✕)	460.00	585.00 ± 1.50	0.17	64-dan/bah <sup>1)</sup>
296.15	783.84 ± 0.30	1.12	51-dim/lan(✕)	480.00	541.00 ± 2.00	-6.34	64-dan/bah <sup>1)</sup>
288.15	790.00 ± 0.40	0.94	52-cap/mug(✕)	500.00	470.00 ± 2.00	-35.93	64-dan/bah <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

**2-Propenol** (cont.)

**Further references:** [1872-lin/von, 1880-bru-1, 1880-bru-3, 1880-tho, 1881-pri/han, 1882-sch-1, 1883-sch-3, 1884-gla, 1884-per, 1884-sch-6, 1897-tho, 02-you/for, 08-dor/dvo, 13-atk/wal, 14-vav, 21-leb, 23-clo/joh, 25-nor/ash, 25-par/kel, 25-par/kel-1, 25-rak, 27-par/cha, 28-par/bar, 28-par/nel, 29-ber, 29-ber/reu, 29-swa, 31-ton/ueh, 33-tre/wat, 35-hen, 35-mah-1, 35-ols/was, 37-zep, 38-dol/gre, 40-mil/bli, 40-was/beg, 40-was/gra, 42-sch/hun, 42-was/bro, 43-bru/bog, 43-dur/roe, 48-wei, 49-hat, 50-jac, 50-par/gol, 50-pic/zie, 52-coo, 53-ani, 53-ani-1, 57-rom-1, 58-hil/hay, 61-ogi/cor, 62-bro/smi, 63-lab].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	802.87 ± 0.67	320.00	762.65 ± 0.53	390.00	689.46 ± 1.24
280.00	795.35 ± 0.56	330.00	753.63 ± 0.58	400.00	676.74 ± 1.41
290.00	787.61 ± 0.50	340.00	744.19 ± 0.65	410.00	663.34 ± 1.62
293.15	785.12 ± 0.50	350.00	734.30 ± 0.73	420.00	649.23 ± 1.86
298.15	781.11 ± 0.49	360.00	723.92 ± 0.83	430.00	634.35 ± 2.16
300.00	779.61 ± 0.49	370.00	713.02 ± 0.95	440.00	618.69 ± 2.52
310.00	771.30 ± 0.50	380.00	701.54 ± 1.08	450.00	602.19 ± 2.96

**1-Buten-3-ol** [598-32-3] C<sub>4</sub>H<sub>8</sub>O MW = 72.11 513

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	830.0 ± 2.0	52-wib

**(Z)-2-Buten-1-ol** [4088-60-2] C<sub>4</sub>H<sub>8</sub>O MW = 72.11 514

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	895.0 ± 3.0	58-hil/hay

**2-Methyl-3-buten-2-ol** [115-18-4] C<sub>5</sub>H<sub>10</sub>O MW = 86.13 515

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.3193 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.9173 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$8.68886 \cdot 10^2$
B	$5.71276 \cdot 10^{-1}$
C	$-2.47190 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

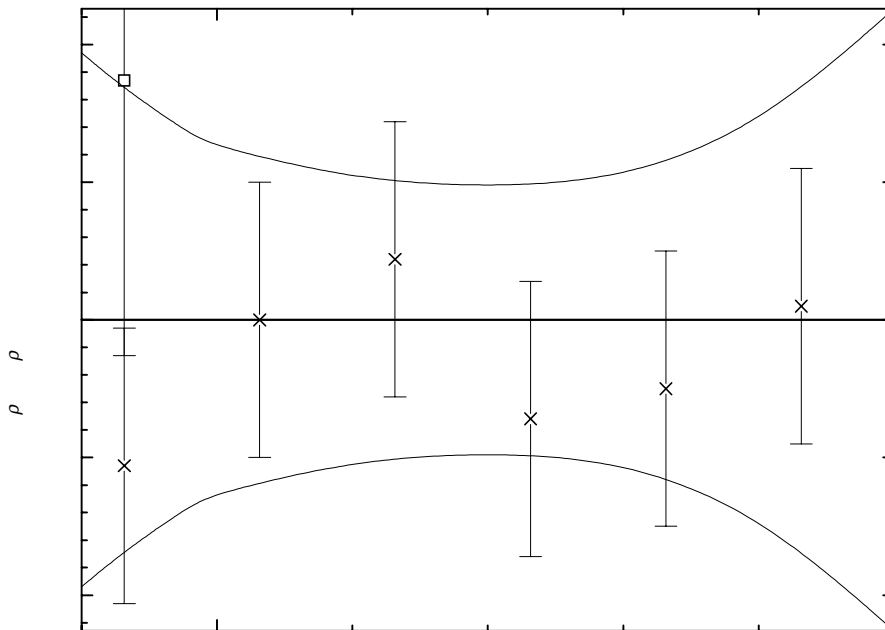
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	824.80 ± 1.00	0.87	41-cam/eby-1(□)	323.15	795.00 ± 0.50	-0.36	88-bag/gur(×)
293.15	823.40 ± 0.50	-0.53	88-bag/gur(×)	333.15	784.60 ± 0.50	-0.25	88-bag/gur(×)
303.15	814.90 ± 0.50	-0.00	88-bag/gur(×)	343.15	773.90 ± 0.50	0.05	88-bag/gur(×)
313.15	805.60 ± 0.50	0.22	88-bag/gur(×)				

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg · m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg · m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg · m <sup>-3</sup>
290.00	826.67 ± 0.97	300.00	817.80 ± 0.63	330.00	788.22 ± 0.51
293.15	823.93 ± 0.84	310.00	808.43 ± 0.51	340.00	777.37 ± 0.70
298.15	819.48 ± 0.67	320.00	798.57 ± 0.48	350.00	766.02 ± 1.13

cont.

**2-Methyl-3-buten-2-ol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**1-Penten-3-ol** [616-25-1]  $C_5H_{10}O$  MW = 86.13 516

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$833.0 \pm 0.6$	63-lab

**3-Penten-1-ol** [39161-19-8]  $C_5H_{10}O$  MW = 86.13 517

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$849.2 \pm 1.0$	48-goe/cr

**4-Penten-1-ol** [821-09-0]  $C_5H_{10}O$  MW = 86.13 518

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
298.15	$839.5 \pm 1.0$	45-sch/gel

**(E)-3,3-Dimethyl-2-buten-1-ol** [500029-65-2] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 519

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.047$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1037.77
<i>B</i>	-0.700

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	832.5 ± 0.7	-0.07	61-hat/wei
298.15	829.1 ± 0.7	0.03	61-hat/wei
303.15	825.6 ± 0.7	0.03	61-hat/wei

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	834.8 ± 0.7
293.15	832.6 ± 0.7
298.15	829.1 ± 0.6
310.00	820.8 ± 0.9

**(Z)-3,3-Dimethyl-2-buten-1-ol** [500029-64-1] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 520

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.094$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1041.21
<i>B</i>	-0.680

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	841.8 ± 0.7	-0.07	61-hat/wei
298.15	838.4 ± 0.7	-0.07	61-hat/wei
303.15	835.2 ± 0.7	0.13	61-hat/wei

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	844.0 ± 0.8
293.15	841.9 ± 0.7
298.15	838.5 ± 0.6
310.00	830.4 ± 0.9

**1-Hexen-3-ol** [4798-44-1] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 521

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	835.7 ± 0.6	63-lab

**2-Hexen-1-ol** [500026-97-1] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 522

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	850.8 ± 1.0	30-wal/ros

**(E)-2-Hexen-1-ol** [928-95-0] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 523

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_{\text{v}} = 0.094$ .

Coefficient	$\rho = A + BT$
$A$	1039.35
$B$	-0.640

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	851.6 ± 0.7	-0.13	61-hat/wei
298.15	848.6 ± 0.7	0.07	61-hat/wei
303.15	845.4 ± 0.7	0.07	61-hat/wei

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	853.7 ± 0.8
293.15	851.7 ± 0.7
298.15	848.5 ± 0.6
310.00	840.9 ± 0.9

**2-Hexen-4-ol** [4798-58-7] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 524

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	836.7 ± 1.0	54-gay/cro <sup>1)</sup>
293.15	841.6 ± 0.6	63-lab
293.15	841.6 ± 0.6	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**5-Hexen-2-ol** [626-94-8] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 525

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
297.15	838.0 ± 2.0	49-col/lag

**2-Methyl-1-penten-3-ol** [2088-07-5] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 526

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	840.0 ± 2.0	65-col/des

**2-Methyl-2-penten-1-ol** [1610-29-3] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 527

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	851.0 ± 2.0	65-col/des

**3-Methyl-1-penten-3-ol** [918-85-4] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 528

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	833.4 ± 0.5	52-mye/col

**3-Methyl-2-penten-1-ol** [500060-37-7] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 529

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.380$ .

Coefficient	$\rho = A + BT$
$A$	1078.78
$B$	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
273.15	866.1 ± 1.5	0.38	50-fav/fri
291.15	851.3 ± 1.5	-0.38	50-fav/fri

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	868.2 ± 1.5	293.15	850.1 ± 1.5
280.00	860.4 ± 1.4	298.15	846.2 ± 1.6
290.00	852.6 ± 1.4		



**3-Methyl-4-penten-3-ol** [500060-36-6] C<sub>6</sub>H<sub>12</sub>O MW = 100.16 530**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 2.090$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1096.92
<i>B</i>	-0.860

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
273.15	864.1 ± 1.5	2.09	50-fav/fri
295.15	841.0 ± 1.5	-2.09	50-fav/fri

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	864.7 ± 2.9
280.00	856.1 ± 2.5
290.00	847.5 ± 2.6
293.15	844.8 ± 2.6
298.15	840.5 ± 2.9

**2-Hepten-4-ol** [4798-59-8] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 531**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	844.5 ± 0.6	63-lab

**(Z)-3-Hepten-1-ol** [1708-81-2] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 532**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 0.249$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1064.56
<i>B</i>	-0.740

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	847.9 ± 0.7	0.27	61-hat/wei
298.15	843.6 ± 0.7	-0.33	61-hat/wei
303.15	840.3 ± 0.7	0.07	61-hat/wei

cont.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	850.0 ± 0.8
293.15	847.6 ± 0.7
298.15	843.9 ± 0.7
310.00	835.2 ± 0.9

**4-Hepten-1-ol** [20851-55-2] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 533

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	844.3 ± 2.0	64-ber/vav

**5-Hepten-1-ol** [89794-36-5] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 534

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
291.15	846.1 ± 1.0	56-gla/gau

**2-Methyl-1-hexen-3-ol** [500029-09-4] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 535

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	842.0 ± 2.0	65-col/des

**2-Methyl-2-hexen-1-ol** [500029-07-2] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 536

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	846.0 ± 2.0	65-col/des

**3-Methyl-1-hexen-3-ol** [55145-28-3] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 537

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.15	836.7 ± 1.0	46-shi

**4-Methyl-1-hexen-4-ol** [500005-96-9] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 538

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	827.0 ± 0.6	63-lab

**4-Methyl-4-hexen-3-ol** [101084-24-6] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 539

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	856.0 ± 2.0	50-pau/tch

**5-Methyl-2-hexen-4-ol** [500025-43-4] C<sub>7</sub>H<sub>14</sub>O MW = 114.19 540

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	842.0 ± 0.6	63-lab

**1,1-Dimethyl-5-hexen-1-ol** [77437-98-0] C<sub>8</sub>H<sub>16</sub>O MW = 128.21 541

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	842.3 ± 1.0	55-che/che

**3,5-Dimethyl-4-hexen-3-ol** [1569-43-3] C<sub>8</sub>H<sub>16</sub>O MW = 128.21 542

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.298$ .

Coefficient	$\rho = A + BT$
$A$	1098.38
$B$	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref.
K	kg · m <sup>-3</sup>	kg · m <sup>-3</sup>	
273.15	874.7 ± 2.0	0.30	34-jac-6
290.35	860.0 ± 2.0	-0.30	34-jac-6

cont.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	877.0 ± 1.9
280.00	868.8 ± 1.8
290.00	860.6 ± 1.9
293.15	858.0 ± 1.9
298.15	853.9 ± 2.0

**3-Ethyl-5-hexen-2-ol** [60091-37-4] C<sub>8</sub>H<sub>16</sub>O MW = 128.21 543

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
289.45	854.0 ± 2.0	47-col/lag
289.15	854.0 ± 2.0	49-col/lag

**6-Methyl-3-hepten-2-ol** [51500-48-2] C<sub>8</sub>H<sub>16</sub>O MW = 128.21 544

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	830.1 ± 2.0	62-mir/fed

**6-Methyl-5-hepten-2-ol** [1569-60-4] C<sub>8</sub>H<sub>16</sub>O MW = 128.21 545

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	858.8 ± 2.0	62-mir/fed

**2-Octen-4-ol** [4798-61-2] C<sub>8</sub>H<sub>16</sub>O MW = 128.21 546

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	847.5 ± 0.6	63-lab

**2,2-Dimethyl-6-hepten-3-ol** [54525-85-8] C<sub>9</sub>H<sub>18</sub>O MW = 142.24 547

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
294.15	843.0 ± 2.0	47-col/lag
297.15	843.0 ± 2.0	49-col/lag

**2,4-Dimethyl-2-hepten-4-ol** [59673-20-0]  $C_9H_{18}O$  MW = 142.24 548

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.176$ .

Coefficient	$\rho = A + BT$
$A$	1076.98
$B$	-0.780

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
273.15	$864.1 \pm 2.0$	0.18	34-jac-6
289.75	$850.8 \pm 2.0$	-0.18	34-jac-6

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$
270.00	$866.4 \pm 1.9$
280.00	$858.6 \pm 1.8$
290.00	$850.8 \pm 1.8$

**(E)-2-Methyl-3-octen-2-ol** [18521-06-7]  $C_9H_{18}O$  MW = 142.24 549

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$830.1 \pm 0.5$	41-cam/eby-1

**(Z)-2-Methyl-3-octen-2-ol** [18521-07-8]  $C_9H_{18}O$  MW = 142.24 550

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$837.8 \pm 0.5$	41-cam/eby-1

**4-Methyl-3-octen-5-ol** [500025-37-6]  $C_9H_{18}O$  MW = 142.24 551

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
298.15	$846.8 \pm 0.8$	12-bje

**4-Methyl-4-octen-1-ol** [500000-06-6]  $C_9H_{18}O$  MW = 142.24 552

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
298.15	$852.0 \pm 2.0$	50-pau/tch

**2,4-Dimethyl-2-octen-4-ol** [76008-28-1] C<sub>10</sub>H<sub>20</sub>O MW = 156.27 553

**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.120$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1078.70
<i>B</i>	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
273.15	860.3 ± 2.0	0.12	34-jac-6
292.35	844.7 ± 2.0	-0.12	34-jac-6

**Table 3.** Recommended values.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	862.7 ± 1.9
280.00	854.7 ± 1.8
290.00	846.7 ± 1.8
293.15	844.2 ± 1.9
298.15	840.2 ± 2.0

**3,5-Dimethyl-6-octen-2-ol** [57785-04-3] C<sub>10</sub>H<sub>20</sub>O MW = 156.27 554

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	864.00 ± 1.00	75-lee/che

**3,7-Dimethyl-6-octen-1-ol** [106-22-9] C<sub>10</sub>H<sub>20</sub>O MW = 156.27 555

**Table 1.** Experimental and recommended values with uncertainties.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	890.0 ± 6.0	1884-gla <sup>1)</sup>
293.15	865.3 ± 1.0	54-ser/voi-1
293.15	865.3 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,2,3-Trimethyl-6-hepten-3-ol** [85924-69-2] C<sub>10</sub>H<sub>20</sub>O MW = 156.27 556

**Table 1.** Experimental value with uncertainty.

<i>T</i> K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
294.15	862.0 ± 2.0	49-col/lag

**2,3,4-Trimethyl-5-hepten-2-ol** [57785-05-4] C<sub>10</sub>H<sub>20</sub>O MW = 156.27 557

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	875.0 ± 1.0	75-lee/che

**3-Ethyl-1-nonen-4-ol** [10544-97-5] C<sub>11</sub>H<sub>22</sub>O MW = 170.30 558

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	843.0 ± 2.0	65-mig/mig

**3,4,8-Trimethyl-1-nonen-3-ol** [18352-66-4] C<sub>12</sub>H<sub>24</sub>O MW = 184.32 559

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	852.1 ± 1.0	67-min/che

**(E)-9-Octadecen-1-ol** [506-42-3] C<sub>18</sub>H<sub>36</sub>O MW = 268.48 560

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
313.15	833.8 ± 1.0	26-boe/bel

**(Z)-9-Octadecen-1-ol** [143-28-2] C<sub>18</sub>H<sub>36</sub>O MW = 268.48 561

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
313.15	836.7 ± 1.0	26-boe/bel

**3,7,11-Trimethyl-2-hexadecen-1-ol** [102013-46-7] C<sub>19</sub>H<sub>38</sub>O MW = 282.51 562

**Table 1.** Experimental value with uncertainty.

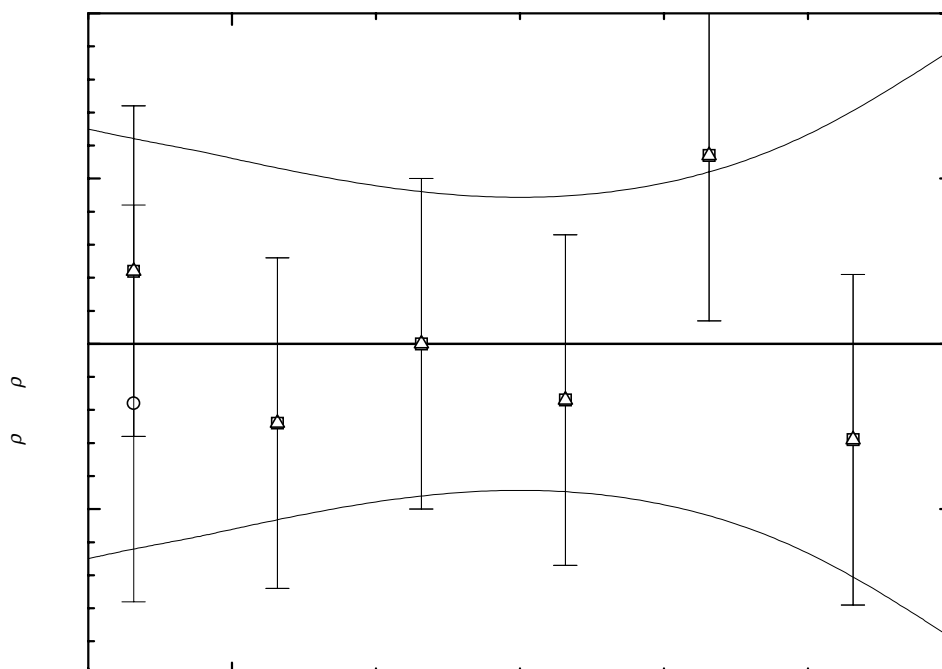
$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	856.1 ± 2.0	60-naz/mak

**3,7,11,15-Tetramethyl-1-hexadecen-3-ol** [60046-87-9] C<sub>20</sub>H<sub>40</sub>O MW = 296.54 563**Table 1.** Coefficients of the polynomial expansion equation.  
Standard deviations (see introduction): $\sigma_{c,w} = 2.9464 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 8.4869 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.06651 \cdot 10^3$
B	$-7.53664 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	$845.40 \pm 0.60$	-0.18	62-mau/smi(O)	293.15	$845.80 \pm 0.50$	0.22	88-bag/gur(□)
293.15	$845.80 \pm 0.50$	0.22	85-bel/ber(Δ)	303.15	$837.80 \pm 0.50$	-0.24	88-bag/gur(□)
303.15	$837.80 \pm 0.50$	-0.24	85-bel/ber(Δ)	313.15	$830.50 \pm 0.50$	-0.00	88-bag/gur(□)
313.15	$830.50 \pm 0.50$	-0.00	85-bel/ber(Δ)	323.15	$822.80 \pm 0.50$	-0.17	88-bag/gur(□)
323.15	$822.80 \pm 0.50$	-0.17	85-bel/ber(Δ)	333.15	$816.00 \pm 0.50$	0.57	88-bag/gur(□)
333.15	$816.00 \pm 0.50$	0.57	85-bel/ber(Δ)	343.15	$807.60 \pm 0.50$	-0.29	88-bag/gur(□)
343.15	$807.60 \pm 0.50$	-0.29	85-bel/ber(Δ)				

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.



**3,7,11,15-Tetramethyl-1-hexadecen-3-ol** (cont.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	847.95 ± 0.65	300.00	840.41 ± 0.56	330.00	817.80 ± 0.47
293.15	845.58 ± 0.62	310.00	832.88 ± 0.47	340.00	810.27 ± 0.61
298.15	841.81 ± 0.58	320.00	825.34 ± 0.43	350.00	802.73 ± 0.89

**3,7,11,15-Tetramethyl-2-heptadecen-1-ol,**

[114161-31-8]

C<sub>21</sub>H<sub>42</sub>O

MW = 310.56

564

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	858.6 ± 2.0	60-naz/mak

**3,7,11,15,16,16-Hexamethyl-1-heptadecen-3-ol**

[113058-51-8]

C<sub>23</sub>H<sub>46</sub>O

MW = 338.62

565

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	851.9 ± 2.0	60-naz/mak

**3,7,11,15,16,16-Hexamethyl-2-heptadecen-1-ol**

[113057-97-9]

C<sub>23</sub>H<sub>46</sub>O

MW = 338.62

566

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	862.8 ± 2.0	60-naz/mak

2.2.2 Alcohols of General Formula C<sub>n</sub>H<sub>2n-2</sub>O

**2-Propyn-1-ol** [107-19-7] C<sub>3</sub>H<sub>4</sub>O MW = 56.06 567

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	971.5 ± 5.00	1880-bru-3 <sup>1)</sup>	293.15	983.5 ± 5.00	1880-bru-3 <sup>1)</sup>
291.95	971.0 ± 5.00	1880-bru-3 <sup>1)</sup>	293.15	947.6 ± 1.00	45-hen/gre <sup>1)</sup>
294.15	972.8 ± 5.00	1880-bru-3 <sup>1)</sup>	298.15	945.2 ± 0.60	95-kum/rao-1
293.15	983.5 ± 5.00	1880-bru-3 <sup>1)</sup>	298.15	945.2 ± 0.60	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Butyn-1-ol** [927-74-2] C<sub>4</sub>H<sub>6</sub>O MW = 70.09 568

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	925.5 ± 0.5	45-hen/gre

**2-Methyl-3-butyn-2-ol** [115-19-5] C<sub>5</sub>H<sub>8</sub>O MW = 84.12 569

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	861.3 ± 0.6	41-cam/eby-1
293.15	861.2 ± 0.6	45-hen/gre
293.15	865.8 ± 2.0	62-mau/smi <sup>1)</sup>
293.15	861.3 ± 0.6	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,4-Pentadien-2-ol** [17615-19-9] C<sub>5</sub>H<sub>8</sub>O MW = 84.12 570

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	901.4 ± 2.0	62-ber/leg-1

**2-Pentyn-1-ol** [6261-22-9] C<sub>5</sub>H<sub>8</sub>O MW = 84.12 571

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	907.7 ± 1.0	64-zak/sta

**4-Pentyn-1-ol** [5390-04-5] C<sub>5</sub>H<sub>8</sub>O MW = 84.12 572

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	913.2 ± 2.0	55-mos

**(RS)-4-Pentyn-2-ol** [2117-11-5] C<sub>5</sub>H<sub>8</sub>O MW = 84.12 573

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	895.7 ± 0.6	54-pom/foo
293.15	905.0 ± 2.0	62-ber/leg-1 <sup>1)</sup>
293.15	895.7 ± 0.6	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3,3-Dimethyl-2-butyn-1-ol** [500029-63-0] C<sub>6</sub>H<sub>10</sub>O MW = 98.14 574

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.047$ .

Coefficient	$\rho = A + BT$
$A$	1074.80
$B$	-0.740

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	857.8 ± 0.7	-0.07	61-hat/wei
298.15	854.2 ± 0.7	0.03	61-hat/wei
303.15	850.5 ± 0.7	0.03	61-hat/wei

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	860.2 ± 0.7	298.15	854.2 ± 0.6
293.15	857.9 ± 0.7	310.00	845.4 ± 0.9

**4,5-Hexadien-3-ol** [4376-43-6] C<sub>6</sub>H<sub>10</sub>O MW = 98.14 575

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	880.7 ± 2.0	62-ber/leg-1

**5-Hexyn-1-ol** [928-90-5] C<sub>6</sub>H<sub>10</sub>O MW = 98.14 576

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	902.0 ± 1.0	64-zak/sta

**5-Hexyn-3-ol** [19780-84-8] C<sub>6</sub>H<sub>10</sub>O MW = 98.14 577

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	893.1 ± 2.0	62-ber/leg-1

**3-Ethyl-1-pentyn-3-ol** [6285-06-9] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 578

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	871.7 ± 0.6	45-hen/gre

**1,2-Heptadien-4-ol** [4376-46-9] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 579

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
294.15	868.8 ± 2.0	62-ber/leg-1

**1-Heptyn-4-ol** [22127-83-9] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 580

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.15	886.7 ± 2.0	62-ber/leg-1

**2-Heptyn-1-ol** [1002-36-4] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 581

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.062$ .

Coefficient	$\rho = A + BT$
$A$	1106.75
$B$	-0.750

cont.

**2-Heptyn-1-ol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	886.8 ± 0.7	-0.08	61-hat/wei
298.15	883.2 ± 0.7	0.07	61-hat/wei
303.15	879.4 ± 0.7	0.02	61-hat/wei
293.15	885.8 ± 1.0	-1.08	64-zak/sta <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	889.2 ± 0.6
293.15	886.9 ± 0.5
298.15	883.1 ± 0.5
310.00	874.2 ± 0.8

**2-Methyl-3,5-hexadien-2-ol** [926-38-5] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 582

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	864.9 ± 2.0	64-bog/kug

**2-Methyl-4,5-hexadien-3-ol** [4376-49-2] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 583

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
294.15	872.2 ± 2.0	62-ber/leg-1

**5-Methyl-3,5-hexadien-1-ol** [19764-79-5] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 584

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	889.9 ± 1.0	67-min/che

**2-Methyl-5-hexyn-3-ol** [54838-77-6] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 585

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	874.9 ± 2.0	62-ber/leg-1

**3-Methyl-1-hexyn-3-ol** [4339-05-3] C<sub>7</sub>H<sub>12</sub>O MW = 112.17 586

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
290.15	867.1 ± 1.0	46-shi

**3,5-Dimethyl-1-hexyn-3-ol** [107-54-0] C<sub>8</sub>H<sub>14</sub>O MW = 126.2 587

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	858.2 ± 1.0	57-hic/ken

**2-Methyl-2,3-heptadien-1-ol** [14270-80-5] C<sub>8</sub>H<sub>14</sub>O MW = 126.20 588

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	875.1 ± 1.0	66-per/bal

**3-Methyl-1,6-heptadien-4-ol** [1838-74-0] C<sub>8</sub>H<sub>14</sub>O MW = 126.20 589

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	868.0 ± 1.0	65-col/des

**5-Methyl-3,5-heptadien-1-ol** [19756-78-6] C<sub>8</sub>H<sub>14</sub>O MW = 126.20 590

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	898.2 ± 1.0	67-min/che

**2,6-Dimethyl-3-heptyn-5-ol** [5923-00-2] C<sub>9</sub>H<sub>16</sub>O MW = 140.23 591

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	848.2 ± 2.0	65-fav/nik

**3-Methyl-3,4-octadien-2-ol** [14270-81-6] C<sub>9</sub>H<sub>16</sub>O MW = 140.23 592

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	860.2 ± 1.0	66-per/bal

**5-Methyl-3,5-octadien-1-ol** [19756-79-7]  $C_9H_{16}O$  MW = 140.23 593

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$890.2 \pm 1.0$	67-min/che

**6-Methyl-2,6-octadien-8-ol** [90002-84-8]  $C_9H_{16}O$  MW = 140.23 594

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$877.0 \pm 2.0$	60-naz/mak

**2-Methyl-3-octyn-2-ol** [20599-16-0]  $C_9H_{16}O$  MW = 140.23 595

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$850.6 \pm 0.5$	41-cam/eby-1

**2-Methyl-3-octyn-5-ol** [5922-99-6]  $C_9H_{16}O$  MW = 140.23 596

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$851.8 \pm 2.0$	65-fav/nik

**5,8-Nonadien-2-ol** [13175-61-6]  $C_9H_{16}O$  MW = 140.23 597

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
298.15	$1086.5 \pm 2.0$	63-col/bue

**4-Nonyl-3-ol** [999-70-2]  $C_9H_{16}O$  MW = 140.23 598

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$866.1 \pm 0.7$	63-lab

**2,3-Dimethyl-3,4-octadien-2-ol** [14129-51-2]  $C_{10}H_{18}O$  MW = 154.25 599

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$867.8 \pm 1.0$	66-per/bal

**(E)-3,7-Dimethyl-2,6-octadien-1-ol** [106-24-1] C<sub>10</sub>H<sub>18</sub>O MW = 154.25 600

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	879.2 ± 0.7	65-rum

**(Z)-3,7-Dimethyl-2,6-octadien-1-ol** [106-25-2] C<sub>10</sub>H<sub>18</sub>O MW = 154.25 601

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	873.3 ± 0.7	65-rum

**3,7-Dimethyl-1-octyn-3-ol** [1604-26-8] C<sub>10</sub>H<sub>18</sub>O MW = 154.25 602

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	852.1 ± 2.0	62-mau/smi

**8-Methyl-5,8-nonadien-2-ol** [13175-62-7] C<sub>10</sub>H<sub>18</sub>O MW = 154.25 603

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
298.15	882.0 ± 2.0	63-col/bue

**3-Propyl-1,2-heptadien-4-ol** [900002-85-9] C<sub>10</sub>H<sub>18</sub>O MW = 154.25 604

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
297.15	863.2 ± 2.0	62-ber/leg-1

**3,5-Diethyl-1,6-heptadine-4-ol** [10545-05-8] C<sub>11</sub>H<sub>20</sub>O MW = 168.28 605

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	892.0 ± 2.0	65-mig/mig

**3,7-Dimethyl-2,6-nonadien-1-ol** [41865-30-9] C<sub>11</sub>H<sub>20</sub>O MW = 168.28 606

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg·m <sup>-3</sup>	
293.15	881.0 ± 2.0	60-naz/mak



**3-Ethenyl-1-nonen-4-ol** [13014-73-8] C<sub>11</sub>H<sub>20</sub>O MW = 168.28 607

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	854.0 ± 2.0	65-mig/mig

**10-Undecyn-1-ol** [2774-84-7] C<sub>11</sub>H<sub>20</sub>O MW = 168.28 608

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	873.3 ± 1.0	62-ber/mol

**3,4,8-Trimethyl-1-nonyn-3-ol** [18352-64-2] C<sub>12</sub>H<sub>22</sub>O MW = 182.31 609

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	858.6 ± 1.0	67-min/che

**3,7,8-Trimethyl-2,6-nonadien-1-ol** [105906-02-3] C<sub>12</sub>H<sub>22</sub>O MW = 182.31 610

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	879.5 ± 2.0	60-naz/mak

**2,8-Dimethyl-3-ethyl-3,4-nonadien-2-ol** [14270-84-9] C<sub>13</sub>H<sub>24</sub>O MW = 196.33 611

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	830.0 ± 1.0	66-per/bal

**3-(1,1-Dimethylethyl)-2-methyl-3,4-octadien-2-ol** [14129-52-3] C<sub>13</sub>H<sub>24</sub>O MW = 196.33 612

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	833.9 ± 1.0	66-per/bal

**3-Ethyl-2,7,7-trimethyl-3,4-octadien-2-ol** [14270-83-8] C<sub>13</sub>H<sub>24</sub>O MW = 196.33 613

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	849.3 ± 1.0	66-per/bal

**5-Tridecyn-7-ol** [1846-65-7] C<sub>13</sub>H<sub>24</sub>O MW = 196.33 614

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	854.6 ± 0.6	63-lab

**5-Pentadecyn-7-ol** [92857-08-4] C<sub>15</sub>H<sub>28</sub>O MW = 224.39 615

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	853.6 ± 0.7	63-lab

**3,7,11-Trimethyl-1-dodecyn-3-ol** [1604-35-9] C<sub>15</sub>H<sub>28</sub>O MW = 224.39 616

**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction):

$$\sigma_{c,w} = 3.7211 \cdot 10^{-1} \text{ (combined temperature ranges, weighted),}$$

$$\sigma_{c,uw} = 1.5548 \cdot 10^{-1} \text{ (combined temperature ranges, unweighted).}$$

Coefficient	$T = 293.00 \text{ to } 343.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.07542 \cdot 10^3$
B	$-7.63342 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

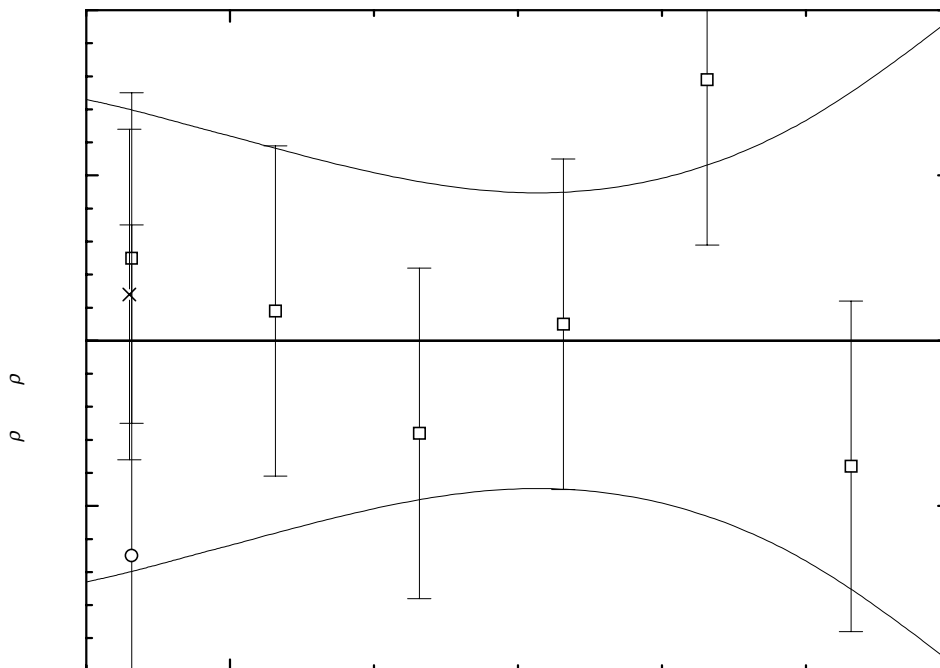
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	851.00 ± 1.00	-0.65	62-mau/smi(O)	313.15	836.10 ± 0.50	-0.28	88-bag/gur(□)
293.00	851.90 ± 0.50	0.14	86-bae(X)	323.15	828.80 ± 0.50	0.05	88-bag/gur(□)
293.15	851.90 ± 0.50	0.25	88-bag/gur(□)	333.15	821.90 ± 0.50	0.79	88-bag/gur(□)
303.15	844.10 ± 0.50	0.09	88-bag/gur(□)	343.15	813.10 ± 0.50	-0.38	88-bag/gur(□)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg · m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg · m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg · m <sup>-3</sup>
290.00	854.05 ± 0.73	300.00	846.42 ± 0.62	330.00	823.52 ± 0.47
293.15	851.65 ± 0.70	310.00	838.79 ± 0.50	340.00	815.89 ± 0.64
298.15	847.83 ± 0.64	320.00	831.15 ± 0.43	350.00	808.25 ± 0.97

cont.

**3,7,11-Trimethyl-1-dodecyn-3-ol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**9,12-Octadecadien-1-ol** [1577-52-2]  $C_{18}H_{34}O$  MW = 266.47 617

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	$861.2 \pm 1.0$	38-tur

**3,7,11,15-Tetramethyl-1-hexadecyn-3-ol** [29171-23-1]  $C_{20}H_{38}O$  MW = 294.52 618

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 4.5296 \cdot 10^{-1}$  (combined temperature ranges, weighted),

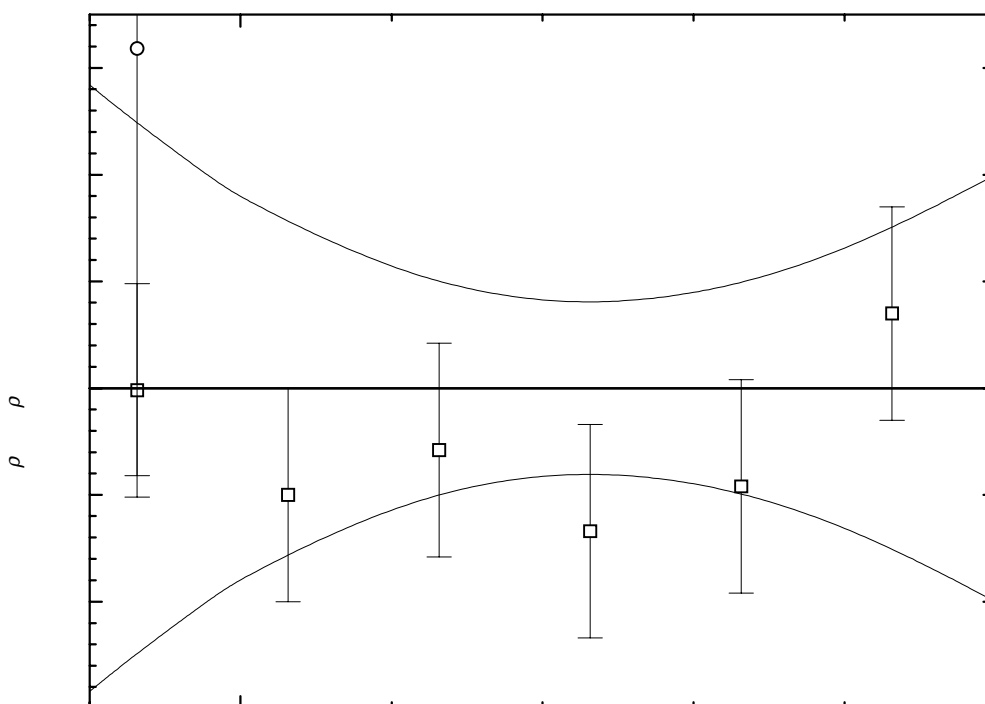
$\sigma_{c,uw} = 2.9444 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.06610 \cdot 10^3$
B	$-7.31308 \cdot 10^{-1}$

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	853.30 ± 2.00	1.59	62-mau/smi(O)	323.15	829.10 ± 0.50	-0.67	88-bag/gur(□)
293.15	851.70 ± 0.50	-0.01	88-bag/gur(□)	333.15	822.00 ± 0.50	-0.46	88-bag/gur(□)
303.15	843.90 ± 0.50	-0.50	88-bag/gur(□)	343.15	815.50 ± 0.50	0.35	88-bag/gur(□)
313.15	836.80 ± 0.50	-0.29	88-bag/gur(□)				

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	854.02 ± 1.42	300.00	846.70 ± 0.89	330.00	824.77 ± 0.42
293.15	851.71 ± 1.24	310.00	839.39 ± 0.54	340.00	817.45 ± 0.63
298.15	848.06 ± 0.98	320.00	832.08 ± 0.38	350.00	810.14 ± 1.00



2.2.3 Alcohols of General Formula C<sub>n</sub>H<sub>2n-4</sub>O

**1-Hexen-5-yn-3-ol** [1573-66-6] C<sub>6</sub>H<sub>8</sub>O MW = 96.13 619

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	919.0 ± 0.7	63-lab

**(RS)-1-Hexen-5-yn-3-ol** [126110-03-0] C<sub>6</sub>H<sub>8</sub>O MW = 96.13 620

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	915.5 ± 1.0	65-alb/bry

**2-Hepten-6-yn-4-ol** [500025-44-5] C<sub>7</sub>H<sub>10</sub>O MW = 110.16 621

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	925.6 ± 0.7	63-lab

**3-Methyl-1-hexen-5-yn-3-ol** [1573-67-7] C<sub>7</sub>H<sub>10</sub>O MW = 110.16 622

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	906.6 ± 1.0	65-alb/bry

**4-Methyl-1,2,6-heptatrien-4-ol** [90198-78-0] C<sub>8</sub>H<sub>12</sub>O MW = 124.18 623

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
294.15	900.6 ± 2.0	62-ber/leg

**6-Methyl-1,3,4-heptatrien-6-ol** [500025-52-5] C<sub>8</sub>H<sub>12</sub>O MW = 124.18 624

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	882.5 ± 0.7	63-lab

**4-Ethyl-1,2,6-heptatrien-4-ol** [90611-15-7]  $C_9H_{14}O$  MW = 138.21 625

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$895.4 \pm 2.0$	62-ber/leg

**6-Methyl-1,3,4-octatrien-6-ol** [500025-51-4]  $C_9H_{14}O$  MW = 138.21 626

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$885.5 \pm 0.7$	63-lab

**2,4,5-Nonatrien-7-ol** [500025-50-3]  $C_9H_{14}O$  MW = 138.21 627

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$891.8 \pm 0.7$	63-lab

**3,7-Dimethyl-6-octen-1-yn-3-ol** [29171-20-8]  $C_{10}H_{16}O$  MW = 152.2 628

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 5.4842 \cdot 10^{-1}$  (combined temperature ranges, weighted),

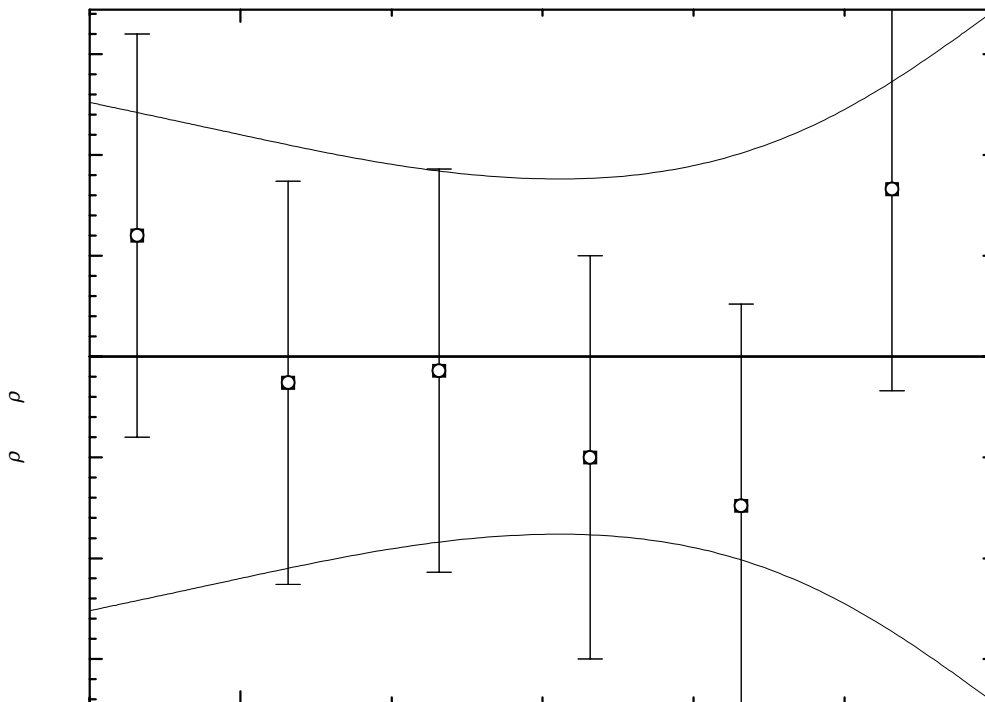
$\sigma_{\text{c,uw}} = 1.6817 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
$A$	$1.12321 \cdot 10^3$
$B$	$-8.36474 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref. (Symbol in Fig. 1)	$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$	Ref. (Symbol in Fig. 1)
K	$\text{kg} \cdot \text{m}^{-3}$	$\text{kg} \cdot \text{m}^{-3}$		K	$\text{kg} \cdot \text{m}^{-3}$	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$878.60 \pm 1.00$	0.60	85-bel/ber(□)	293.15	$878.60 \pm 1.00$	0.60	88-bag/gur(O)
303.15	$869.50 \pm 1.00$	-0.13	85-bel/ber(□)	303.15	$869.50 \pm 1.00$	-0.13	88-bag/gur(O)
313.15	$861.20 \pm 1.00$	-0.07	85-bel/ber(□)	313.15	$861.20 \pm 1.00$	-0.07	88-bag/gur(O)
323.15	$852.40 \pm 1.00$	-0.50	85-bel/ber(□)	323.15	$852.40 \pm 1.00$	-0.50	88-bag/gur(O)
333.15	$843.80 \pm 1.00$	-0.74	85-bel/ber(□)	333.15	$843.80 \pm 1.00$	-0.74	88-bag/gur(O)
343.15	$837.00 \pm 1.00$	0.83	85-bel/ber(□)	343.15	$837.00 \pm 1.00$	0.83	88-bag/gur(O)

cont.

**3,7-Dimethyl-6-octen-1-yn-3-ol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	880.63 ± 1.26	300.00	872.27 ± 1.10	330.00	847.17 ± 0.91
293.15	878.00 ± 1.21	310.00	863.90 ± 0.94	340.00	838.81 ± 1.18
298.15	873.81 ± 1.13	320.00	855.54 ± 0.86	350.00	830.44 ± 1.72

**3-Methyl-2-nonen-4-yn-6-ol**

[500025-47-8]

C<sub>10</sub>H<sub>16</sub>O

MW = 152.24

629

**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	881.3 ± 0.6	63-lab



**4-(1-Methylethyl)-1,2,6-heptatrien-4-ol** [91055-94-6]  $C_{10}H_{16}O$  MW = 152.24 630

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
295.15	$885.1 \pm 2.0$	62-ber/leg

**4-Propyl-1,2,6-heptatrien-4-ol** [91055-95-7]  $C_{10}H_{16}O$  MW = 152.24 631

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
294.15	$882.1 \pm 2.0$	62-ber/leg

**3-Ethenyl-1-nonyl-4-ol** [900002-83-7]  $C_{11}H_{18}O$  MW = 166.26 632

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$879.0 \pm 2.0$	65-mig/mig

**5-Methyl-2,5,6-decatrien-4-ol** [14129-53-4]  $C_{11}H_{18}O$  MW = 166.26 633

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$871.5 \pm 1.0$	66-per/bal

**3-(Methylethenyl)-3,4-octadien-2-ol** [14129-70-5]  $C_{11}H_{18}O$  MW = 166.26 634

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$874.3 \pm 1.0$	66-per/bal

**2-Methyl-3-(1-methylethenyl)-3,4-octadien-2-ol** [14270-82-7]  $C_{12}H_{20}O$  MW = 180.29 635

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$855.5 \pm 1.0$	66-per/bal

**2,7-Dimethyl-3-(1-methylethenyl)-3,4-octadien-2-ol** [14270-85-0]  $C_{13}H_{22}O$  MW = 194.32 636

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$855.8 \pm 1.0$	66-per/bal

**5-Ethyl-9-methyl-2,5,6-decatrien-4-ol** [14129-71-6]  $C_{13}H_{22}O$  MW = 194.32 637

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$867.1 \pm 1.0$	66-per/bal



2.2.4 Alcohols of General Formula C<sub>n</sub>H<sub>2n-6</sub>O

**1,6-Heptadiyn-4-ol** [21972-06-5] C<sub>7</sub>H<sub>8</sub>O MW = 108.14 638

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	967.2 ± 1.0	63-lab

**4-Methyl-1,6-heptadiyn-4-ol** [41005-07-6] C<sub>8</sub>H<sub>10</sub>O MW = 122.17 639

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	959.5 ± 1.0	63-lab

**1,7-Octadien-5-yn-3-ol** [1573-68-8] C<sub>8</sub>H<sub>10</sub>O MW = 122.17 640

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	922.5 ± 1.0	65-alb/bry

**3-Methyl-1,7-octadien-5-yn-3-ol** [1573-69-9] C<sub>9</sub>H<sub>12</sub>O MW = 136.19 641

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	910.5 ± 1.0	65-alb/bry

**2-Methyl-3,5-octadiyn-2-ol** [500025-48-9] C<sub>9</sub>H<sub>12</sub>O MW = 136.19 642

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	870.0 ± 1.0	63-lab

**2-Methyl-3,5-decadiyn-2-ol** [500025-49-0] C<sub>11</sub>H<sub>16</sub>O MW = 164.25 643

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	897.3 ± 1.0	63-lab

## 3 Tabulated Data on Density - Diols

### 3.1 Alkanediols

#### 3.1.1 Alkanediols C<sub>1</sub> - C<sub>6</sub>

1,2-Ethanediol

[107-21-1]

C<sub>2</sub>H<sub>6</sub>O<sub>2</sub>

MW = 62.07

644

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 6.0901 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.3696 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 250.25$ to $513.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.31971 \cdot 10^3$
B	$-8.26843 \cdot 10^{-1}$
C	$8.03242 \cdot 10^{-4}$
D	$-1.30719 \cdot 10^{-6}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

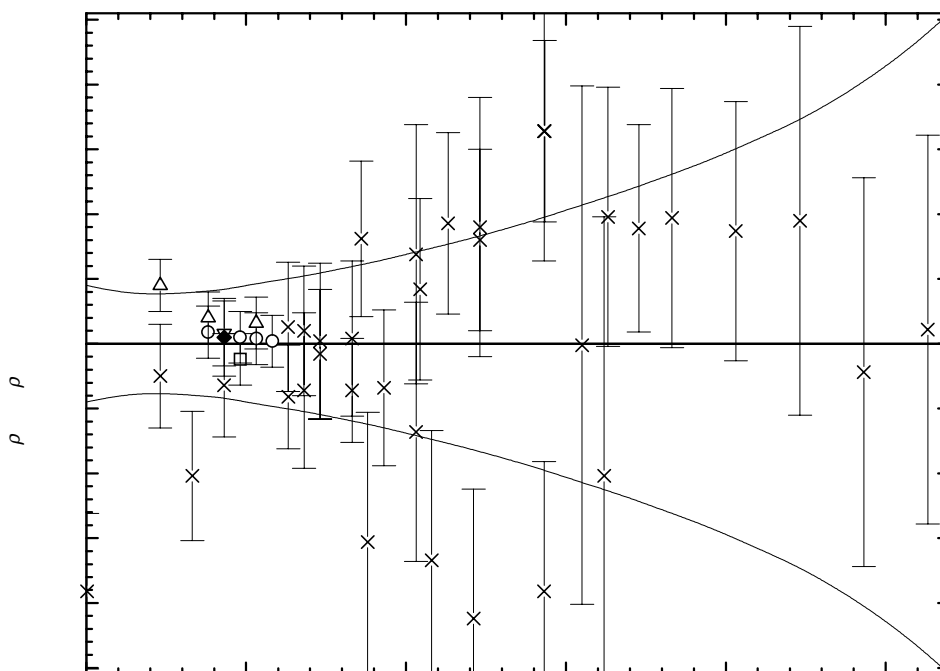
$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$T$ K	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
289.95	$1118.00 \pm 2.00$	2.37	1893-ram/shi-3 <sup>1)</sup>	343.15	$1077.40 \pm 0.60$	-0.34	57-ket/van(X)
319.25	$1091.20 \pm 2.00$	-3.87	1893-ram/shi-3 <sup>1)</sup>	273.15	$1126.00 \pm 1.00$	-1.15	58-cos/bow <sup>1)</sup>
351.35	$1068.00 \pm 2.00$	-3.66	1893-ram/shi-3 <sup>1)</sup>	293.15	$1113.00 \pm 1.00$	-0.42	58-cos/bow <sup>1)</sup>
405.05	$1029.70 \pm 2.00$	-0.01	1893-ram/shi-3(X)	313.15	$1100.00 \pm 1.00$	0.59	58-cos/bow <sup>1)</sup>
292.45	$1113.40 \pm 1.00$	-0.50	1895-eyk <sup>1)</sup>	333.15	$1086.00 \pm 1.00$	0.94	58-cos/bow <sup>1)</sup>
411.95	$1023.00 \pm 2.00$	-1.02	1895-eyk(X)	353.15	$1071.00 \pm 1.00$	0.69	58-cos/bow(X)
293.15	$1112.72 \pm 1.00$	-0.70	30-bin/for <sup>1)</sup>	373.15	$1056.00 \pm 1.00$	0.90	58-cos/bow(X)
303.15	$1105.58 \pm 1.00$	-0.87	30-bin/for <sup>1)</sup>	393.15	$1041.00 \pm 1.00$	1.64	58-cos/bow(X)
313.15	$1098.78 \pm 1.00$	-0.63	30-bin/for <sup>1)</sup>	413.15	$1024.00 \pm 1.00$	0.98	58-cos/bow(X)
333.15	$1084.13 \pm 1.00$	-0.93	30-bin/for <sup>1)</sup>	433.15	$1007.00 \pm 1.00$	0.97	58-cos/bow(X)
353.15	$1069.63 \pm 1.00$	-0.68	30-bin/for(X)	453.15	$989.20 \pm 1.00$	0.87	58-cos/bow(X)
371.15	$1054.52 \pm 1.00$	-2.12	30-bin/for(X)	473.15	$970.80 \pm 1.50$	0.95	58-cos/bow(X)
393.15	$1037.45 \pm 1.00$	-1.91	30-bin/for(X)	493.15	$950.30 \pm 1.50$	-0.22	58-cos/bow(X)
298.15	$1109.90 \pm 0.60$	-0.04	31-smy/wal <sup>1)</sup>	513.15	$930.40 \pm 1.50$	0.11	58-cos/bow(X)
323.15	$1092.30 \pm 0.60$	0.02	31-smy/wal(X)	533.15	$910.30 \pm 1.50$	1.20	58-cos/bow <sup>1)</sup>
273.15	$1127.60 \pm 0.20$	0.45	35-tim/hen( $\Delta$ )	553.15	$889.20 \pm 1.50$	2.33	58-cos/bow <sup>1)</sup>
288.15	$1117.07 \pm 0.20$	0.20	35-tim/hen( $\Delta$ )	250.25	$1140.70 \pm 0.60$	-1.91	59-kom/ros(X)
303.15	$1106.61 \pm 0.20$	0.16	35-tim/hen( $\Delta$ )	366.25	$1067.80 \pm 0.60$	7.40	59-kom/ros <sup>1)</sup>
293.15	$1113.10 \pm 0.60$	-0.32	53-dan/fad <sup>1)</sup>	293.10	$1113.96 \pm 0.50$	0.51	75-khi/gri <sup>1)</sup>
333.15	$1085.10 \pm 0.60$	0.04	53-dan/fad(X)	298.10	$1110.28 \pm 0.50$	0.30	75-khi/gri <sup>1)</sup>
293.15	$1113.10 \pm 0.60$	-0.32	57-ket/van <sup>1)</sup>	303.10	$1106.72 \pm 0.50$	0.23	75-khi/gri <sup>1)</sup>
318.15	$1095.50 \pm 0.60$	-0.36	57-ket/van(X)	308.10	$1103.06 \pm 0.50$	0.08	75-khi/gri <sup>1)</sup>

<sup>1)</sup> Not included in Fig. 1.

cont.

**1,2-Ethandiol** (cont.)**Table 2.** (cont.)

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
313.10	1099.58 ± 0.50	0.13	75-khi/gri(✕)	393.40	1040.80 ± 0.70	1.64	89-taw/tej(✕)
318.10	1095.99 ± 0.50	0.10	75-khi/gri(✕)	422.80	1015.80 ± 0.80	0.89	89-taw/tej(✕)
323.10	1092.24 ± 0.50	-0.08	75-khi/gri(✕)	283.15	1119.29 ± 0.50	-1.02	90-lee/hon(✕)
293.15	1113.50 ± 0.25	0.08	81-joo/arl(∇)	293.15	1112.02 ± 0.50	-1.40	90-lee/hon <sup>1)</sup>
298.00	1094.00 ± 1.00	-16.05	84-idr/fre <sup>1)</sup>	303.15	1105.82 ± 0.50	-0.63	90-lee/hon <sup>1)</sup>
318.00	1109.00 ± 1.00	13.04	84-idr/fre <sup>1)</sup>	288.15	1116.96 ± 0.20	0.09	91-dou/pal(○)
338.00	1080.00 ± 1.00	-1.53	84-idr/fre(✕)	298.15	1109.99 ± 0.20	0.05	91-dou/pal(○)
358.00	1065.00 ± 1.00	-1.67	84-idr/fre(✕)	303.15	1106.49 ± 0.20	0.04	91-dou/pal(○)
298.15	1109.82 ± 0.20	-0.12	88-dou/pal(□)	308.15	1102.96 ± 0.20	0.02	91-dou/pal(○)
303.15	1105.90 ± 0.60	-0.55	89-taw/tej <sup>1)</sup>	293.15	1113.47 ± 0.30	0.05	93-chi/pro(◆)
313.30	1099.90 ± 0.60	0.60	89-taw/tej <sup>1)</sup>	273.15	1126.90 ± 0.40	-0.25	93-kum/moc(✕)
336.00	1083.80 ± 0.60	0.81	89-taw/tej(✕)	293.15	1113.10 ± 0.40	-0.32	93-kum/moc(✕)
354.40	1069.80 ± 0.70	0.42	89-taw/tej(✕)	313.15	1099.00 ± 0.40	-0.41	93-kum/moc(✕)
363.15	1063.70 ± 0.70	0.93	89-taw/tej(✕)	333.15	1084.70 ± 0.40	-0.36	93-kum/moc(✕)
373.15	1055.90 ± 0.70	0.80	89-taw/tej(✕)				

<sup>1)</sup> Not included in Fig. 1.

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)  
cont.

**Further references:** [1859-wur, 1864-lan, 1884-gla, 1884-per, 01-def-1, 05-dun, 06-wal-1, 07-wal-4, 09-sch-2, 14-low, 18-kar, 19-eyk, 25-rii/soe, 26-tay/rin, 27-kai/mel, 29-ber/reu, 32-bri-2, 35-sch/sta, 36-rom, 37-ewe, 37-gib/kin, 37-mou/dod, 37-puk, 41-gib/loe, 43-ish/kat, 44-ira, 48-lad/smi, 48-wei, 52-cur/joh, 53-ish/kat, 55-fog/hix, 56-koi/han, 57-cru/jos, 60-rab/mur, 61-lut/obu, 62-mel, 65-por/pli, 66-gar/kom, 66-koz/rab, 67-dav/fin, 67-sho/ata, 68-ano, 68-naz/tsy, 69-ada, 70-kun/cha, 70-paz/paz, 70-ras/gaz, 72-gla/gha, 74-jim/paz, 74-wol/ska, 75-esp/man, 77-zhu/zhu-2, 78-fro/ers-1, 78-mus/kan, 79-jim/paz, 79-sah/hay, 79-sin/siv, 82-diz/mar, 82-man/les, 85-zhu, 91-fen/wan, 98-pal/sha].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
250.00	1142.78 ± 0.45	330.00	1087.35 ± 0.58	430.00	1008.76 ± 1.28
260.00	1136.05 ± 0.40	340.00	1080.06 ± 0.63	440.00	1000.05 ± 1.37
270.00	1129.29 ± 0.38	350.00	1072.67 ± 0.69	450.00	991.17 ± 1.47
280.00	1122.47 ± 0.39	360.00	1065.16 ± 0.75	460.00	982.09 ± 1.58
290.00	1115.60 ± 0.41	370.00	1057.53 ± 0.81	470.00	972.81 ± 1.69
293.15	1113.42 ± 0.42	380.00	1049.77 ± 0.88	480.00	963.33 ± 1.82
298.15	1109.94 ± 0.44	390.00	1041.87 ± 0.95	490.00	953.63 ± 1.97
300.00	1108.65 ± 0.45	400.00	1033.83 ± 1.03	500.00	943.70 ± 2.14
310.00	1101.64 ± 0.49	410.00	1025.64 ± 1.11	510.00	933.54 ± 2.33
320.00	1094.54 ± 0.53	420.00	1017.28 ± 1.19	520.00	923.15 ± 2.55

### 1,2-Propanediol

[57-55-6]

C<sub>3</sub>H<sub>8</sub>O<sub>2</sub>

MW = 76.1

645

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 3.0002 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 4.9012 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 323.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.25088 \cdot 10^3$
B	$-7.32395 \cdot 10^{-1}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

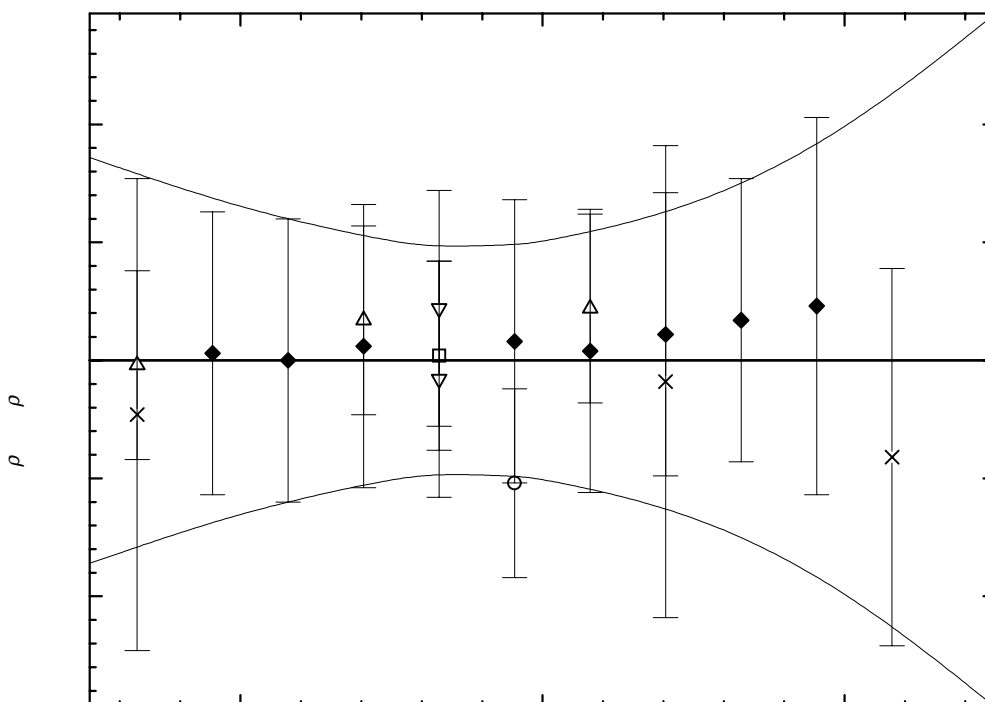
$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
298.15	1032.80 ± 0.80	0.28	31-smy/wal <sup>1)</sup>	296.15	1035.40 ± 0.50	1.42	62-mel <sup>1)</sup>
323.15	1013.80 ± 0.80	-0.41	31-smy/wal(✕)	278.15	1047.20 ± 0.60	0.03	70-kun/cha(◆)
293.15	1038.10 ± 1.00	1.92	51-mac/tho <sup>1)</sup>	283.15	1043.50 ± 0.60	-0.00	70-kun/cha(◆)
308.15	1025.10 ± 1.00	-0.09	51-mac/tho(✕)	288.15	1039.90 ± 0.60	0.06	70-kun/cha(◆)
273.15	1050.60 ± 1.00	-0.23	51-van-1(✕)	293.15	1036.30 ± 0.60	0.12	70-kun/cha <sup>1)</sup>
293.15	1037.60 ± 1.00	1.42	51-van-1 <sup>1)</sup>	298.15	1032.60 ± 0.60	0.08	70-kun/cha(◆)
273.15	1050.81 ± 0.40	-0.02	55-tim/hen(Δ)	303.15	1028.90 ± 0.60	0.04	70-kun/cha(◆)
288.15	1040.01 ± 0.40	0.17	55-tim/hen(Δ)	308.15	1025.30 ± 0.60	0.11	70-kun/cha(◆)
303.15	1029.08 ± 0.40	0.22	55-tim/hen(Δ)	313.15	1021.70 ± 0.60	0.17	70-kun/cha(◆)
293.15	1036.20 ± 0.40	0.02	57-ano(□)	318.15	1018.10 ± 0.80	0.23	70-kun/cha(◆)
293.15	1036.10 ± 0.50	-0.08	62-mel(∇)	298.15	1032.00 ± 0.40	-0.52	85-les/eic(O)
293.15	1036.40 ± 0.50	0.22	62-mel(∇)				

<sup>1)</sup> Not included in Fig. 1.

cont.

**1,2-Propanediol** (cont.)

**Further references:** [1857-wur-1, 1859-wur, 1879-bel, 1882-zan, 1890-gar, 27-tro/luk, 32-bri-2, 35-sch/sta, 36-dup-1, 37-puk, 46-puc/wis, 50-cle/mac, 52-cur/joh, 53-ano-5, 55-ano-2, 61-sch-3, 62-deg/lad, 65-wei/lan, 66-mil-1, 68-ano, 70-gar/kom, 73-gar/paz, 74-wol/ska, 78-mus/kan, 82-man/les].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	1053.14 ± 0.86	293.15	1036.18 ± 0.48	310.00	1023.84 ± 0.64
280.00	1045.81 ± 0.64	298.15	1032.52 ± 0.49	320.00	1016.52 ± 0.96
290.00	1038.49 ± 0.50	300.00	1031.16 ± 0.50	330.00	1009.19 ± 1.47



**1,3-Propanediol****[504-63-2]****C<sub>3</sub>H<sub>8</sub>O<sub>2</sub>****MW = 76.1****646****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 8.3438 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 1.6142 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15 \text{ to } 343.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.13576 \cdot 10^3$
B	$2.29954 \cdot 10^{-2}$
C	$-1.03995 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

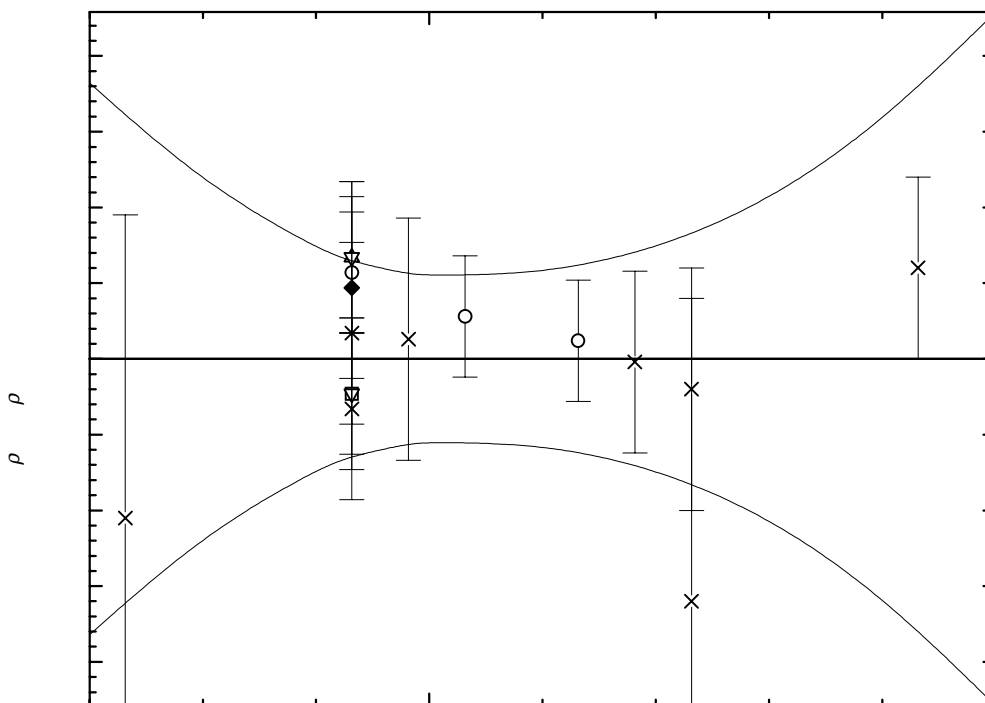
$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
273.15	$1063.40 \pm 2.00$	-1.05	1874-reb-2(✕)	343.15	$1021.80 \pm 0.60$	0.60	57-ket/van(✕)
292.15	$1053.00 \pm 2.00$	-0.72	1874-reb-2 <sup>1)</sup>	293.15	$1053.80 \pm 0.50$	0.67	62-mel(∇)
298.15	$1050.30 \pm 0.80$	0.13	31-smy/wal(✕)	293.15	$1052.90 \pm 0.50$	-0.23	62-mel(∇)
323.15	$1034.40 \pm 0.80$	-0.20	31-smy/wal(✕)	298.15	$1049.00 \pm 2.00$	-1.17	80-bru <sup>1)</sup>
293.15	$1052.80 \pm 0.60$	-0.33	32-bri-2(✕)	323.15	$1033.00 \pm 2.00$	-1.60	80-bru(✕)
293.15	$1053.80 \pm 0.50$	0.67	35-sch/sta(Δ)	373.15	$1003.00 \pm 2.00$	3.46	80-bru <sup>1)</sup>
293.15	$1053.60 \pm 0.60$	0.47	52-cur/joh(◆)	293.15	$1053.70 \pm 0.40$	0.57	88-cze/zyw(○)
293.15	$1052.90 \pm 0.40$	-0.23	53-ano-6(□)	303.15	$1047.44 \pm 0.40$	0.28	88-cze/zyw(○)
293.15	$1053.30 \pm 0.60$	0.17	57-ket/van(✕)	313.15	$1041.10 \pm 0.40$	0.12	88-cze/zyw(○)
318.15	$1037.80 \pm 0.60$	-0.02	57-ket/van(✕)				

<sup>1)</sup> Not included in Fig. 1.**Further references:** [1874-reb-1, 1882-zan, 18-kar, 26-ray, 36-sto/rou, 50-cle/mac, 59-ale, 72-rak/isa, 74-paz/rom, 74-rak/mel, 74-rak/zlo, 75-nak/kom, 78-mus/kan].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	$1066.16 \pm 1.82$	298.15	$1050.17 \pm 0.56$	330.00	$1030.10 \pm 1.04$
280.00	$1060.67 \pm 1.16$	300.00	$1049.07 \pm 0.55$	340.00	$1023.36 \pm 1.56$
290.00	$1054.97 \pm 0.73$	310.00	$1042.95 \pm 0.56$	350.00	$1016.42 \pm 2.29$
293.15	$1053.13 \pm 0.64$	320.00	$1036.63 \pm 0.72$		

cont.

**1,3-Propanediol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**R-(-)-1,2-Propanediol** [4254-14-2] C<sub>3</sub>H<sub>8</sub>O<sub>2</sub> MW = 76.1 647

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	1004.3 ± 3.0	18-abd/eic
299.15	1025.3 ± 3.0	56-pri/osg

**(S)-(+)-1,2-Propanediol** [4254-15-3] C<sub>3</sub>H<sub>8</sub>O<sub>2</sub> MW = 76.1 648

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	1040.0 ± 3.0	48-bae/fis
295.15	1041.0 ± 3.0	62-kuh/kuh

**1,2-Butanediol** [584-03-2] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 649

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 1.1759$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.4556 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15 \text{ to } 454.70 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.09605 \cdot 10^3$
B	$2.45483 \cdot 10^{-2}$
C	$-1.17159 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

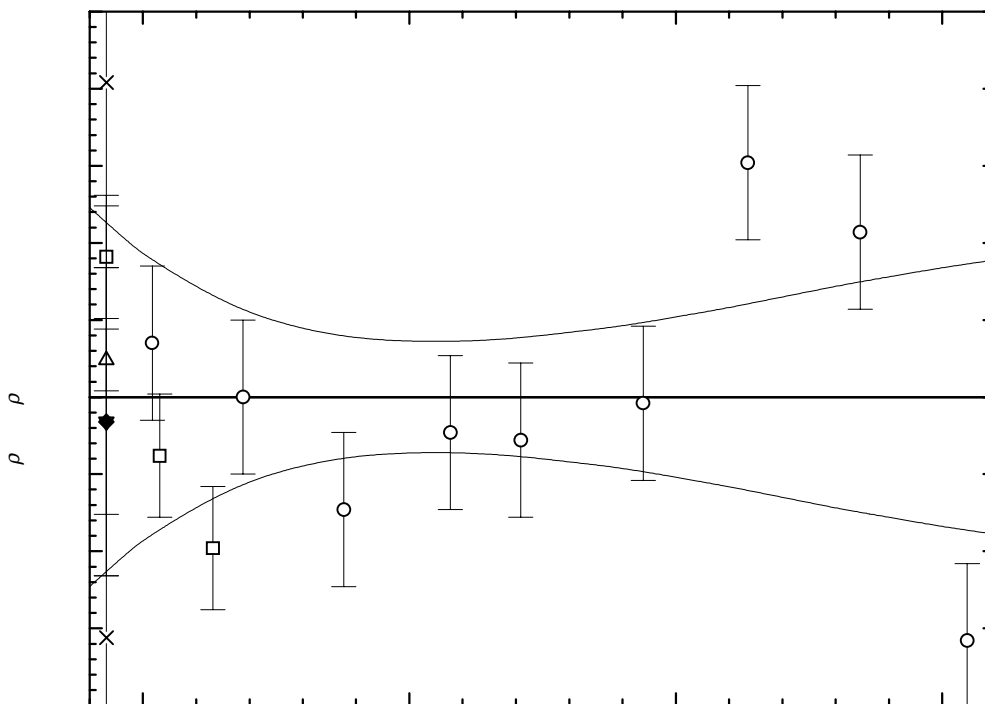
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	1004.60 ± 2.00	2.04	37-tis(✕)	318.80	984.80 ± 0.50	-0.00	92-sun/dig(O)
293.15	1001.00 ± 2.00	-1.56	37-tis/chu(✕)	337.70	970.00 ± 0.50	-0.73	92-sun/dig(O)
293.15	1002.40 ± 1.00	-0.16	50-cle/mac(◆)	357.70	954.70 ± 0.50	-0.23	92-sun/dig(O)
293.15	1002.40 ± 1.00	-0.16	62-mel(∇)	370.90	943.70 ± 0.50	-0.28	92-sun/dig(O)
293.15	1002.80 ± 1.00	0.24	65-wei/lan(Δ)	393.90	923.90 ± 0.50	-0.04	92-sun/dig(O)
293.15	1003.47 ± 0.40	0.91	88-cze/zyw(□)	413.50	907.40 ± 0.50	1.52	92-sun/dig(O)
303.15	995.44 ± 0.40	-0.38	88-cze/zyw(□)	434.60	886.50 ± 0.50	1.07	92-sun/dig(O)
313.15	987.87 ± 0.40	-0.98	88-cze/zyw(□)	454.70	863.40 ± 0.50	-1.58	92-sun/dig(O)
301.80	997.10 ± 0.50	0.35	92-sun/dig(O)				

**Further references:** [1886-hen, 73-sza/mys].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	1004.64 ± 1.23	340.00	968.96 ± 0.38	410.00	909.17 ± 0.58
293.15	1002.56 ± 1.13	350.00	961.12 ± 0.36	420.00	899.69 ± 0.65
298.15	999.22 ± 0.98	360.00	953.05 ± 0.36	430.00	889.98 ± 0.72
300.00	997.97 ± 0.93	370.00	944.74 ± 0.38	440.00	880.03 ± 0.78
310.00	991.07 ± 0.71	380.00	936.20 ± 0.42	450.00	869.85 ± 0.84
320.00	983.93 ± 0.54	390.00	927.43 ± 0.46	460.00	859.43 ± 0.89
330.00	976.57 ± 0.44	400.00	918.42 ± 0.52		

cont.

**1,2-Butanediol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**(RS)-1,2-Butanediol**

[26171-83-5]

C<sub>4</sub>H<sub>10</sub>O<sub>2</sub>

MW = 90.12

650

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

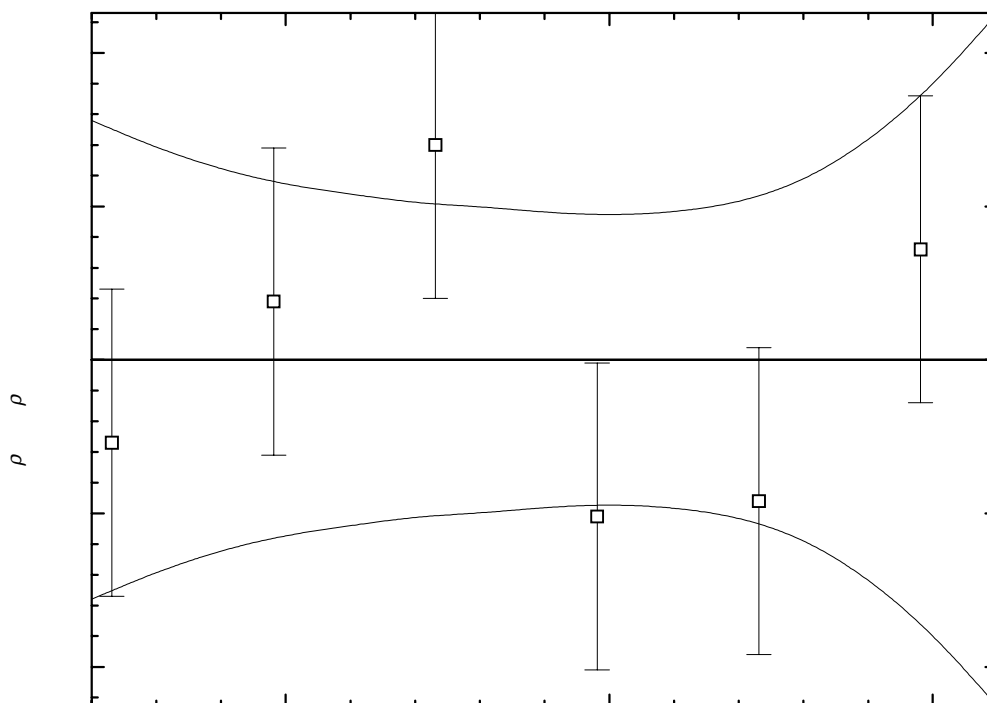
 $\sigma_{c,w} = 4.4743 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.2372 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 323.14$ to $448.11$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.11932 \cdot 10^3$
B	$-1.05834 \cdot 10^{-1}$
C	$-1.01373 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
323.14	$979.00 \pm 0.50$	-0.27	96-ste/chi(□)	398.12	$916.00 \pm 0.50$	-0.51	96-ste/chi(□)
348.14	$959.80 \pm 0.50$	0.19	96-ste/chi(□)	423.11	$892.60 \pm 0.50$	-0.46	96-ste/chi(□)
373.12	$939.40 \pm 0.50$	0.70	96-ste/chi(□)	448.11	$868.70 \pm 0.50$	0.36	96-ste/chi(□)

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
320.00	981.65 ± 0.78	370.00	941.38 ± 0.51	420.00	896.05 ± 0.51
330.00	974.00 ± 0.69	380.00	932.72 ± 0.50	430.00	886.38 ± 0.58
340.00	966.15 ± 0.62	390.00	923.86 ± 0.48	440.00	876.50 ± 0.71
350.00	958.10 ± 0.57	400.00	914.79 ± 0.47	450.00	866.42 ± 0.89
360.00	949.84 ± 0.54	410.00	905.52 ± 0.48	460.00	856.13 ± 1.13

**1,3-Butanediol****[107-88-0]****C<sub>4</sub>H<sub>10</sub>O<sub>2</sub>****MW = 90.12****651****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 8.4552 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.2006 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15 \text{ to } 458.90 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.09606 \cdot 10^3$
B	$-8.02845 \cdot 10^{-3}$
C	$-1.03339 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref. (Symbol in Fig. 1)
298.15	$1000.20 \pm 1.00$	-1.60	48-adk/bil(∇)	323.10	$986.10 \pm 0.60$	0.52	92-sun/dig(O)
293.15	$1003.50 \pm 0.60$	-1.40	62-mel(Δ)	342.90	$970.80 \pm 0.60$	-1.00	92-sun/dig(O)
293.15	$1002.00 \pm 1.00$	-2.90	62-mel <sup>1)</sup>	363.00	$957.20 \pm 0.60$	0.23	92-sun/dig(O)
293.15	$1003.70 \pm 0.60$	-1.20	62-mel(Δ)	383.20	$941.50 \pm 0.60$	0.27	92-sun/dig(O)
293.15	$1005.30 \pm 0.70$	0.40	62-mel(Δ)	400.90	$927.00 \pm 0.60$	0.25	92-sun/dig(O)
293.15	$1005.79 \pm 0.40$	0.89	88-cze/zyw(□)	420.30	$910.40 \pm 0.60$	0.27	92-sun/dig(O)
303.15	$999.04 \pm 0.40$	0.39	88-cze/zyw(□)	439.60	$893.10 \pm 0.60$	0.27	92-sun/dig(O)
313.15	$992.39 \pm 0.40$	0.19	88-cze/zyw(□)	458.90	$874.80 \pm 0.60$	0.05	92-sun/dig(O)
302.40	$1000.60 \pm 0.60$	1.47	92-sun/dig(O)				

<sup>1)</sup> Not included in Fig. 1.

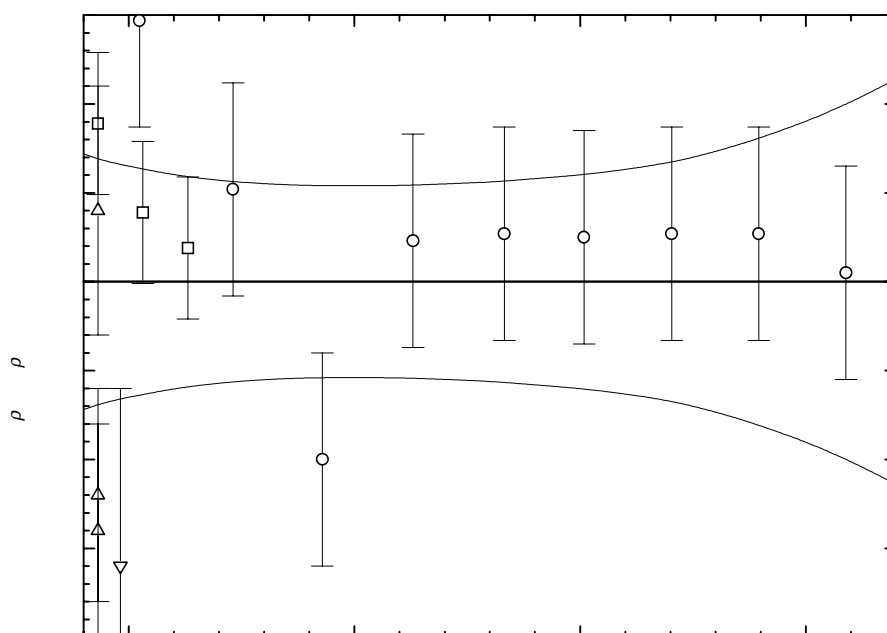
**Further references:** [29-ber/mie, 35-sch/sta, 37-tis/chu, 43-gre/kel, 48-bou/nic, 48-mic/hop, 50-cle/mac, 52-cur/joh, 54-ros, 55-ser, 56-far/she, 67-pis/gas, 72-rak/isa, 74-rak/mak, 74-rak/mel, 74-wol/ska, 78-mus/kan, 82-man/les].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
290.00	$1006.82 \pm 0.72$	340.00	$973.87 \pm 0.54$	410.00	$919.05 \pm 0.63$
293.15	$1004.90 \pm 0.69$	350.00	$966.66 \pm 0.54$	420.00	$910.39 \pm 0.67$
298.15	$1001.80 \pm 0.66$	360.00	$959.24 \pm 0.54$	430.00	$901.53 \pm 0.73$
300.00	$1000.64 \pm 0.65$	370.00	$951.61 \pm 0.55$	440.00	$892.46 \pm 0.81$
310.00	$994.26 \pm 0.60$	380.00	$943.78 \pm 0.56$	450.00	$883.18 \pm 0.90$
320.00	$987.67 \pm 0.57$	390.00	$935.75 \pm 0.58$	460.00	$873.70 \pm 1.01$
330.00	$980.87 \pm 0.55$	400.00	$927.50 \pm 0.60$	470.00	$864.01 \pm 1.14$

cont.



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**(RS)-1,3-Butanediol**

[18826-95-4]

C<sub>4</sub>H<sub>10</sub>O<sub>2</sub>

MW = 90.12

652

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 4.2923 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.1462 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

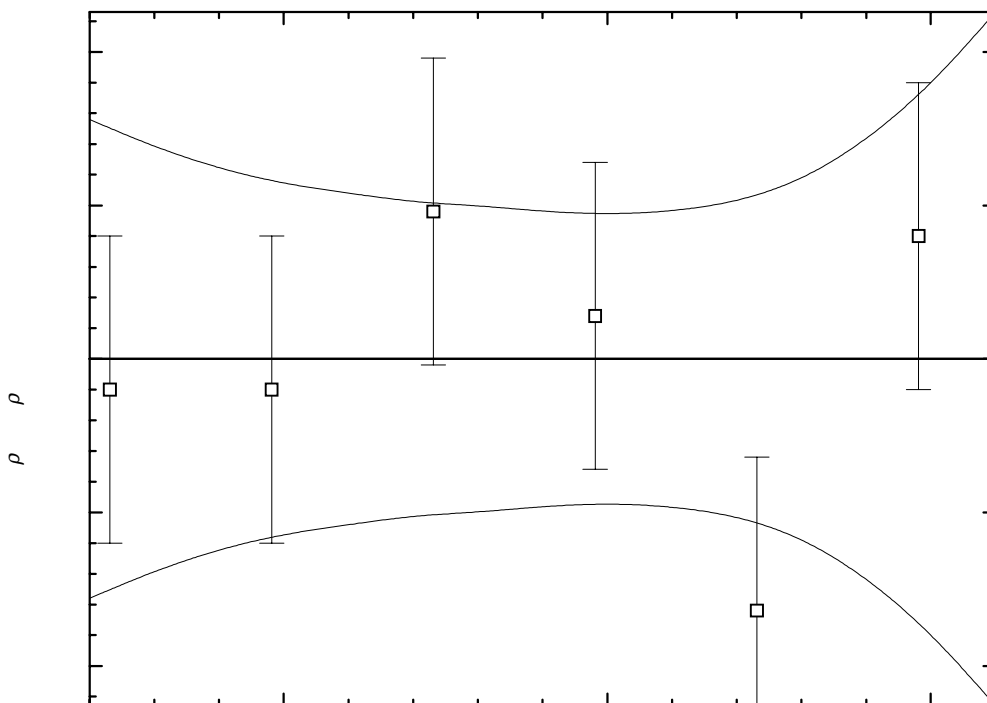
Coefficient	$T = 323.14 \text{ to } 448.11 \text{ K}$
	$\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.07840 \cdot 10^3$
B	$8.73975 \cdot 10^{-2}$
C	$-1.18509 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
323.14	$982.80 \pm 0.50$	-0.10	96-ste/chi(□)	448.11	$880.00 \pm 0.50$	0.40	96-ste/chi(□)
348.13	$965.10 \pm 0.50$	-0.10	96-ste/chi(□)	672.80	$391.30 \pm 0.00$	-209.46	96-ste/chi <sup>1)</sup>
373.12	$946.50 \pm 0.50$	0.48	96-ste/chi(□)	674.50	$348.90 \pm 0.00$	-249.29	96-ste/chi <sup>1)</sup>
398.12	$925.50 \pm 0.50$	0.14	96-ste/chi(□)	675.40	$316.00 \pm 0.00$	-280.83	96-ste/chi <sup>1)</sup>
423.11	$902.40 \pm 0.50$	-0.82	96-ste/chi(□)				

<sup>1)</sup> Not included in Fig. 1.

cont.

**(RS)-1,3-Butanediol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
320.00	985.02 ± 0.78	370.00	948.50 ± 0.51	420.00	906.06 ± 0.51
330.00	978.19 ± 0.69	380.00	940.49 ± 0.50	430.00	896.86 ± 0.58
340.00	971.12 ± 0.62	390.00	932.23 ± 0.48	440.00	887.42 ± 0.71
350.00	963.82 ± 0.57	400.00	923.75 ± 0.47	450.00	877.75 ± 0.89
360.00	956.28 ± 0.54	410.00	915.02 ± 0.48	460.00	867.84 ± 1.13



**1,4-Butanediol****[110-63-4]****C<sub>4</sub>H<sub>10</sub>O<sub>2</sub>****MW = 90.12****653****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{c,w} = 1.0892$  (combined temperature ranges, weighted), $\sigma_{c,uw} = 2.6052 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15 \text{ to } 493.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.12256 \cdot 10^3$
B	$-1.72321 \cdot 10^{-1}$
C	$-5.89027 \cdot 10^{-4}$
D	$-1.76600 \cdot 10^{-7}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

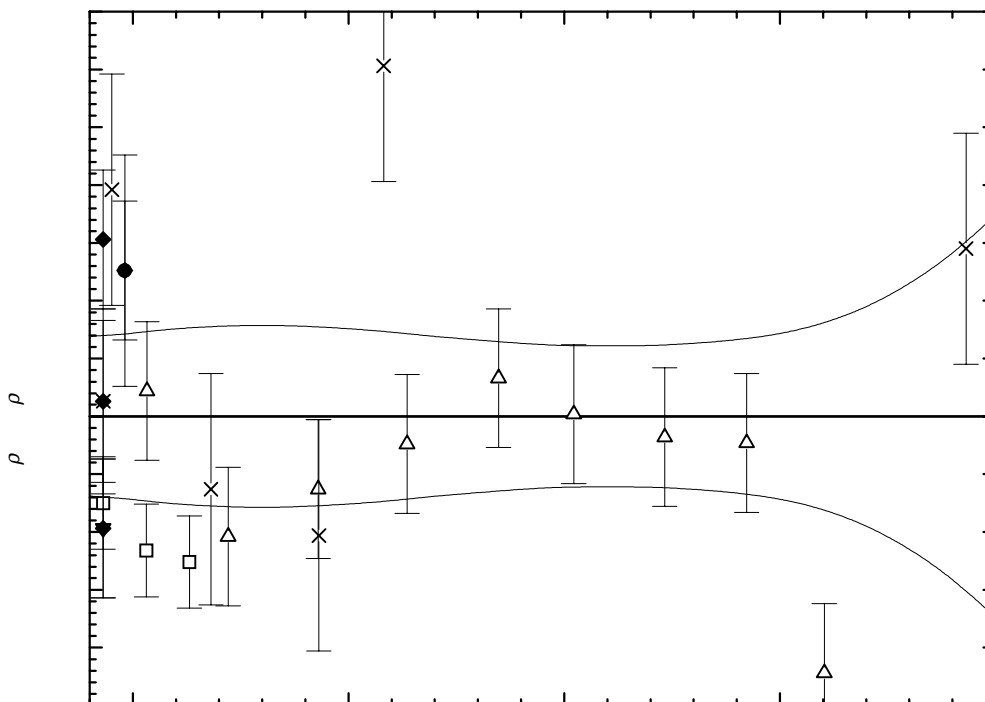
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	1017.10 ± 0.80	0.13	29-kir/tric(×)	493.15	874.60 ± 1.00	1.45	78-apa/ker-2(×)
293.15	1016.00 ± 0.60	-0.97	48-bou/nic(∇)	293.15	1016.22 ± 0.40	-0.75	88-cze/zyw(□)
293.15	1017.30 ± 1.00	0.33	57-ket/van <sup>1)</sup>	303.15	1010.11 ± 0.40	-1.16	88-cze/zyw(□)
318.15	1001.80 ± 1.00	-0.63	57-ket/van(×)	313.15	1004.15 ± 0.40	-1.26	88-cze/zyw(□)
343.15	985.90 ± 1.00	-1.03	57-ket/van(×)	303.30	1011.40 ± 0.60	0.22	92-sun/dig(Δ)
293.15	1017.10 ± 0.70	0.13	62-mel(◆)	322.10	999.00 ± 0.60	-1.04	92-sun/dig(Δ)
293.15	1016.00 ± 0.60	-0.97	62-mel(◆)	343.00	986.40 ± 0.60	-0.63	92-sun/dig(Δ)
293.15	1018.50 ± 0.60	1.53	62-mel(◆)	363.60	973.30 ± 0.60	-0.24	92-sun/dig(Δ)
298.15	1015.40 ± 1.00	1.26	62-mel(◆)	384.80	959.30 ± 0.60	0.33	92-sun/dig(Δ)
298.15	1015.40 ± 0.60	1.26	66-fre/hor(○)	402.20	946.50 ± 0.60	0.02	92-sun/dig(Δ)
295.15	1017.80 ± 1.00	1.96	78-apa/ker-2(×)	423.30	930.50 ± 0.60	-0.18	92-sun/dig(Δ)
358.16	980.20 ± 1.00	3.03	78-apa/ker-2(×)	442.30	915.60 ± 0.60	-0.23	92-sun/dig(Δ)
451.11	913.00 ± 1.00	4.26	78-apa/ker-2 <sup>1)</sup>	460.30	899.00 ± 0.60	-2.22	92-sun/dig(Δ)

<sup>1)</sup> Not included in Fig. 1.**Further references:** [1890-dek, 01-ham, 32-hun, 50-cle/mac, 52-cur/joh, 54-ros, 60-kun/sak, 63-shu/bar, 66-mya/pya, 68-naz/tsy, 70-are/tav, 78-mus/kan, 82-man/les].**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	1018.74 ± 0.69	350.00	982.52 ± 0.76	430.00	925.51 ± 0.63
293.15	1016.97 ± 0.70	360.00	975.95 ± 0.73	440.00	917.66 ± 0.66
298.15	1014.14 ± 0.71	370.00	969.22 ± 0.69	450.00	909.64 ± 0.71
300.00	1013.08 ± 0.72	380.00	962.33 ± 0.66	460.00	901.46 ± 0.80
310.00	1007.27 ± 0.76	390.00	955.29 ± 0.63	470.00	893.12 ± 0.94
320.00	1001.31 ± 0.78	400.00	948.08 ± 0.61	480.00	884.60 ± 1.14
330.00	995.20 ± 0.79	410.00	940.72 ± 0.61	490.00	875.92 ± 1.40
340.00	988.94 ± 0.78	420.00	933.20 ± 0.61	500.00	867.07 ± 1.74

cont.

**1,4-Butanediol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**2,3-Butanediol (isomer not specified)** [513-85-9] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 654

**Table 1.** Fit with estimated *B* coefficient for 5 accepted points. Deviation  $\sigma_w = 0.509$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1238.27
<i>B</i>	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	1007.6 ± 3.0	3.85	62-mel <sup>1)</sup>	293.15	1005.0 ± 2.0	1.25	65-wei/lan
293.15	1003.3 ± 1.0	-0.45	64-mys/zie	293.15	1003.3 ± 1.0	-0.45	35-sch/sta
298.15	1000.3 ± 1.0	0.55	64-mys/zie	298.15	999.8 ± 1.0	0.05	46-cle-1

<sup>1)</sup> Not included in calculation of linear coefficients.

cont.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	1006.3 ± 1.1
293.15	1003.8 ± 1.0
298.15	999.8 ± 1.0

**D-(-)-2,3-Butanediol** [24347-58-8] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 655

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	987.2 ± 0.5	46-kno/sch

**dl-2,3-Butanediol** [6982-25-8] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 656

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 7.3545 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 1.9800 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $452.20$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.16268 \cdot 10^3$
B	$-3.59946 \cdot 10^{-1}$
C	$-7.45938 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
298.15	990.00 ± 1.00	0.94	44-mor/ae(Δ)	381.20	917.70 ± 0.60	0.62	92-sun/dig(□)
293.15	993.00 ± 1.00	-0.06	75-nak/kom(O)	400.60	899.80 ± 0.60	1.02	92-sun/dig(□)
303.30	984.90 ± 0.60	0.01	92-sun/dig(□)	419.50	880.20 ± 0.60	-0.22	92-sun/dig(□)
322.90	968.50 ± 0.60	-0.18	92-sun/dig(□)	439.70	860.00 ± 0.60	-0.20	92-sun/dig(□)
343.60	950.20 ± 0.60	-0.74	92-sun/dig(□)	452.20	847.10 ± 0.60	-0.28	92-sun/dig(□)
361.70	934.00 ± 0.60	-0.90	92-sun/dig(□)				

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

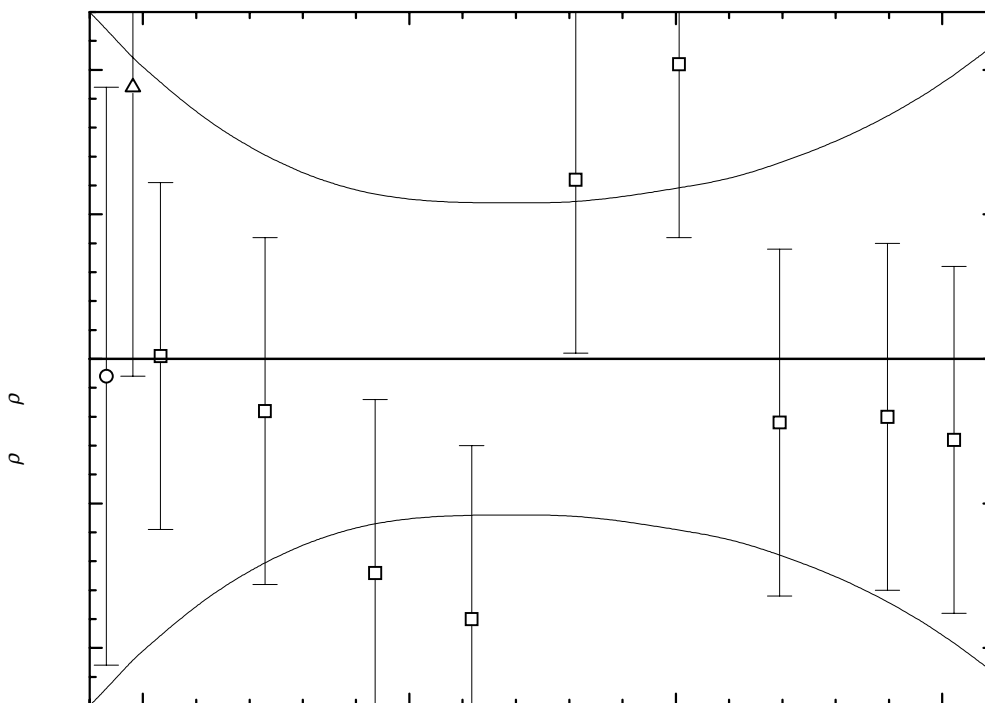
$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	995.57 ± 1.20	340.00	954.07 ± 0.58	410.00	889.71 ± 0.62
293.15	993.06 ± 1.14	350.00	945.33 ± 0.55	420.00	879.92 ± 0.68
298.15	989.06 ± 1.04	360.00	936.43 ± 0.54	430.00	869.98 ± 0.75
300.00	987.57 ± 1.01	370.00	927.39 ± 0.54	440.00	859.89 ± 0.84
310.00	979.42 ± 0.85	380.00	918.19 ± 0.54	450.00	849.66 ± 0.95
320.00	971.12 ± 0.73	390.00	908.85 ± 0.56	460.00	839.27 ± 1.09
330.00	962.67 ± 0.64	400.00	899.36 ± 0.59		

cont.

*dl*-2,3-Butanediol (cont.)

Further references: [1859-wur, 51-wat/coo, 52-cur/joh].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

***L*-(+)-2,3-Butanediol** [19132-06-0] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 657

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	986.9 ± 0.5	46-kno/sch

**(*R*\*, *S*\*)-2,3-Butanediol** [5341-95-7] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 658

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	993.9 ± 2.0	46-kno/sch

**2-Methyl-1,2-propanediol** [558-43-0] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 659**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	1002.4 ± 3.0	37-dob/gut <sup>1)</sup>	293.15	996.7 ± 2.0	54-vor/tit
287.15	999.0 ± 3.0	37-mou/dod <sup>1)</sup>	293.15	997.0 ± 2.0	65-wei/lan
293.15	1003.0 ± 3.0	41-hea/tam <sup>1)</sup>	293.15	996.9 ± 2.0	Recommended
298.15	989.6 ± 3.0	48-adk/bil <sup>1)</sup>			

<sup>1)</sup> Not included in calculation of recommended value.**2-Methyl-1,3-propanediol** [2163-42-0] C<sub>4</sub>H<sub>10</sub>O<sub>2</sub> MW = 90.12 660**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
273.15	1029.7 ± 3.0	07-fav/sok-3 <sup>1)</sup>	293.15	1009.0 ± 3.0	65-bar/koz <sup>1)</sup>
273.15	1029.7 ± 3.0	07-sok <sup>1)</sup>	293.15	1020.0 ± 2.0	65-wei/lan
293.15	1029.0 ± 3.0	35-has/mcb <sup>1)</sup>	293.15	1020.0 ± 2.0	Recommended
293.15	1027.3 ± 3.0	42-pum/hah <sup>1)</sup>			

<sup>1)</sup> Not included in calculation of recommended value.**2,2-Dimethyl-1,3-propanediol** [126-30-7] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 661**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
<i>crystal</i>		
298.15	1066.0 ± 5.0	57-ano-10
298.15	1066.0 ± 5.0	60-ano-13

**2-Ethyl-1,3-propanediol** [2612-29-5] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 662**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	997.0 ± 1.0	48-adk/bil

**2-Methyl-1,3-butanediol** [684-84-4] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 663**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	994.0 ± 1.5	58-far/spe <sup>1)</sup>	293.15	991.5 ± 1.0	64-hel/dav
293.15	991.9 ± 1.0	56-far/she	293.15	991.7 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Methyl-2,3-butanediol** [5396-58-7] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 664

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	968.8 ± 1.0	58-hen/wat

**3-Methyl-1,2-butanediol** [50468-22-9] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 665

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	998.8 ± 2.0	1875-fla
294.65	984.2 ± 2.0	1875-fla

**3-Methyl-1,3-butanediol** [2568-33-4] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 666

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	983.3 ± 3.0	07-kut <sup>1)</sup>	293.15	976.3 ± 2.0	56-far/she
273.15	995.4 ± 3.0	07-kut <sup>1)</sup>	293.15	977.7 ± 2.0	62-esa/shi
293.15	964.5 ± 6.0	55-sar/mor <sup>1)</sup>	293.15	977.0 ± 2.1	Recommended
293.15	986.7 ± 3.0	57-far/rot <sup>1)</sup>			

<sup>1)</sup> Not included in calculation of recommended value.

**1,2-Pentanediol** [5343-92-0] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 667

**Table 1.** Fit with estimated *B* coefficient for 6 accepted points. Deviation  $\sigma_w = 0.167$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1194.93
<i>B</i>	-0.760

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
273.15	987.0 ± 1.0	-0.34	1859-wur	293.15	972.3 ± 1.0	0.16	50-cle/mac
293.15	978.5 ± 3.0	6.36	23-kau/ada <sup>1)</sup>	293.15	970.7 ± 2.0	-1.39	51-cop/fie <sup>1)</sup>
297.15	969.1 ± 1.0	0.00	45-len/dup	293.15	972.3 ± 1.0	0.16	62-mel
297.15	969.1 ± 1.0	0.00	45-sch/gel	297.15	969.1 ± 1.0	0.00	62-mel

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
270.00	989.7 ± 2.3	293.15	972.1 ± 0.7
280.00	982.1 ± 1.4	298.15	968.3 ± 0.9
290.00	974.5 ± 0.7		

**1,3-Pentanediol** [3174-67-2] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 668

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	981.0 ± 1.0	64-hel/dav

**1,4-Pentanediol** [626-95-9] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 669

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
273.00	1000.1 ± 2.0	1889-lip <sup>1)</sup>	293.15	988.6 ± 1.0	63-shu/bar
293.15	990.3 ± 1.0	57-fav/ser	293.15	989.5 ± 1.2	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**1,5-Pentanediol** [111-29-5] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 670

**Table 1.** Fit with estimated  $B$  coefficient for 20 accepted points. Deviation  $\sigma_w = 0.834$ .

Coefficient	$\rho = A + BT$
$A$	1174.56
$B$	-0.620

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
284.65	987.0 ± 6.0	-11.08	1893-eyk-1 <sup>1)</sup>	318.15	978.5 ± 2.0	1.19	57-ket/van
351.15	944.5 ± 6.0	-12.35	1893-eyk-1 <sup>1)</sup>	293.15	991.4 ± 1.0	-1.41	62-mel
291.15	994.0 ± 2.0	-0.05	04-ham	299.15	989.0 ± 1.0	-0.09	62-mel
293.15	992.1 ± 1.0	-0.71	23-kau/ada	293.15	990.4 ± 2.0	-2.41	67-ano-5
293.15	993.8 ± 2.0	0.99	27-tri	293.15	990.4 ± 2.0	-2.41	68-ano
284.15	998.0 ± 1.0	-0.39	34-pau	293.15	994.3 ± 2.0	1.49	68-naz/tsy
299.15	989.0 ± 2.0	-0.09	45-sch/gel	278.15	1005.9 ± 3.0	3.79	75-nak/kom <sup>1)</sup>
293.15	991.4 ± 1.0	-1.41	50-cle/mac	298.15	997.3 ± 3.0	7.59	75-nak/kom <sup>1)</sup>
293.15	992.3 ± 1.0	-0.51	52-cur/joh	318.15	986.0 ± 3.0	8.69	75-nak/kom <sup>1)</sup>
293.15	990.4 ± 2.0	-2.41	54-ano-12	293.15	992.8 ± 0.4	-0.02	88-cze/zyw
293.15	989.0 ± 2.0	-3.81	55-mos	303.15	986.7 ± 0.4	0.12	88-cze/zyw
293.15	994.0 ± 2.0	1.19	57-ket/van	313.15	981.2 ± 0.4	0.84	88-cze/zyw
343.15	962.8 ± 2.0	0.99	57-ket/van				

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	1001.0 ± 1.7	298.15	989.7 ± 1.3	330.00	970.0 ± 2.0
290.00	994.8 ± 1.4	310.00	982.4 ± 1.4	340.00	963.8 ± 2.4
293.15	992.8 ± 1.4	320.00	976.2 ± 1.7	350.00	957.6 ± 2.8

**2,3-Pentanediol** [42027-23-6] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 671

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	994.4 ± 4.0	1875-wag/say-1 <sup>1)</sup>
287.15	979.9 ± 4.0	1875-wag/say-1 <sup>1)</sup>
273.15	1005.0 ± 1.0	37-mil/sus
273.15	1005.0 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2,4-Pentanediol** [625-69-4] C<sub>5</sub>H<sub>12</sub>O<sub>2</sub> MW = 104.15 672

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.900$ .

Coefficient	$\rho = A + BT$
$A$	1201.54
$B$	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	963.5 ± 2.0	2.34	11-zel/arj <sup>1)</sup>
287.15	966.0 ± 1.0	-0.08	14-vav
293.15	962.3 ± 1.0	1.14	52-cur/joh
298.15	956.0 ± 1.0	-1.06	72-caz/mar

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
280.00	971.9 ± 1.7
290.00	963.7 ± 1.2
293.15	961.2 ± 1.1
298.15	957.1 ± 1.2

**2,2-Dimethyl-1,3-butanediol** [76-35-7] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 673

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	768.4 ± 1.0	61-ano-11



**2,2-Dimethyl-1,4-butanediol** [32812-23-0] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 674

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
277.15	996.0 ± 2.0	04-bou/bla

**2,3-Dimethyl-1,3-butanediol** [24893-35-4] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 675

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.082$ .

Coefficient	$\rho = A + BT$
$A$	1179.17
$B$	-0.720

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	968.0 ± 0.6	-0.10	53-hat/jou
298.15	964.5 ± 0.6	-0.00	53-hat/jou
303.15	961.0 ± 0.6	0.10	53-hat/jou
293.15	998.0 ± 10.0	29.90	57-sar/vor <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	970.4 ± 0.6
293.15	968.1 ± 0.5
298.15	964.5 ± 0.4
310.00	956.0 ± 0.7

**2,3-Dimethyl-1,4-butanediol** [57716-80-0] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 676

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	977.1 ± 2.0	62-raz/bog

**dl-2,3-Dimethyl-1,4-butanediol** [66553-14-8] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 677

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	974.0 ± 2.0	54-mcc/pro

**meso-2,3-Dimethyl-1,4-butanediol** [500009-29-0] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 678

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	970.0 ± 2.0	54-mcc/pro

**2,3-Dimethyl-2,3-butanediol** [76-09-5] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 679

**Table 1.** Fit with estimated  $B$  coefficient for 5 accepted points. Deviation  $\sigma_w = 0.524$ .

Coefficient	$\rho = A + BT$
$A$	1196.92
$B$	-0.800

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
288.15	966.3 ± 2.0	-0.11	1884-per	290.15	964.1 ± 2.0	-0.70	46-lau/wie
298.15	958.0 ± 2.0	-0.39	1884-per	288.15	967.0 ± 2.0	0.60	52-cur/joh
288.15	967.0 ± 2.0	0.60	25-vor/wal	293.15	933.0 ± 3.0	-29.40	52-pet/she <sup>1)</sup>

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	972.9 ± 1.7
290.00	964.9 ± 1.6
293.15	962.4 ± 1.6
298.15	958.4 ± 1.6

**3,3-Dimethyl-1,2-butanediol** [59562-82-2] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 680

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
323.15	940.0 ± 2.0	09-cla

**2-Ethyl-1,3-butanediol** [66553-17-1] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 681

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
298.15	967.7 ± 0.8	48-adk/bil

**2-Ethyl-1,4-butanediol** [57716-79-7] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 682

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	982.5 ± 2.0	14-Ion

**2-Ethyl-2-methyl-1,3-propanediol** [77-84-9] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 683

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
323.15	958.0 ± 1.0	58-ano-13
323.15	958.0 ± 1.0	67-ano-5
323.15	958.0 ± 1.0	68-ano
323.15	958.2 ± 1.0	Recommended

**1,2-Hexanediol** [6920-22-5] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 684

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	950.7 ± 2.0	51-cop/fie

**1,3-Hexanediol** [21531-91-9] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 685

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.15	958.0 ± 2.0	44-gla

**1,4-Hexanediol** [16432-53-4] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 686

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
289.45	982.0 ± 2.0	44-gla

**1,5-Hexanediol** [928-40-5] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 687

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 1.120$ .

Coefficient	$\rho = A + BT$
$A$	1215.01
$B$	-0.840

cont.

**1,5-Hexanediol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	971.0 ± 2.0	2.24	56-cri
298.15	964.0 ± 1.0	-0.56	64-ber/lon

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
290.00	971.4 ± 1.9
293.15	968.8 ± 1.8
298.15	964.6 ± 1.8

**1,6-Hexanediol**

[629-11-8]

C<sub>6</sub>H<sub>14</sub>O<sub>2</sub>

MW = 118.18

688

**Table 1.** Fit with estimated *B* coefficient for 3 accepted points. Deviation  $\sigma_w = 1.678$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1183.31
<i>B</i>	-0.680

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
318.55	957.1 ± 4.0	-9.59	52-cur/joh <sup>1)</sup>
293.15	989.7 ± 2.0	5.73	63-tsy/sol <sup>1)</sup>
278.15	991.8 ± 1.0	-2.37	75-nak/kom
298.15	981.6 ± 1.0	1.03	75-nak/kom
318.15	968.3 ± 1.0	1.33	75-nak/kom

<sup>1)</sup> Not included in calculation of linear coefficients.**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	999.7 ± 2.3	293.15	984.0 ± 1.8	320.00	965.7 ± 2.1
280.00	992.9 ± 2.0	298.15	980.6 ± 1.8		
290.00	986.1 ± 1.8	310.00	972.5 ± 1.9		

**2,3-Hexanediol**

[617-30-1]

C<sub>6</sub>H<sub>14</sub>O<sub>2</sub>

MW = 118.18

689

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
288.15	989.0 ± 2.0	37-tya

**2,4-Hexanediol** [19780-90-6] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 690

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
294.15	951.6 ± 1.0	32-les/wak

**2,5-Hexanediol** [2935-44-6] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 691

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{\text{c,w}} = 1.4746$  (combined temperature ranges, weighted),

$\sigma_{\text{c,uw}} = 5.9932 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.00$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.00102 \cdot 10^3$
B	$3.21158 \cdot 10^{-1}$
C	$-1.57871 \cdot 10^{-3}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
273.00	966.89 ± 4.00	-4.14	1859-wur(×)	293.15	959.95 ± 0.40	0.46	96-gri/zhu(×)
273.00	966.90 ± 4.00	-4.13	1864-wur(×)	303.15	953.30 ± 0.40	0.01	96-gri/zhu(×)
293.15	961.00 ± 1.00	1.51	02-dud/lem(□)	313.15	946.60 ± 0.40	-0.17	96-gri/zhu(×)
293.15	960.10 ± 1.00	0.61	52-cur/joh(O)	323.15	939.80 ± 0.40	-0.14	96-gri/zhu(×)
293.15	960.00 ± 1.00	0.51	53-ano-5(Δ)	333.15	932.80 ± 0.40	0.01	96-gri/zhu(×)
293.15	961.70 ± 2.00	2.21	62-raz/bog(V)	343.15	925.60 ± 0.40	0.28	96-gri/zhu(×)
293.15	962.50 ± 2.00	3.01	63-shu/bar(◆)				

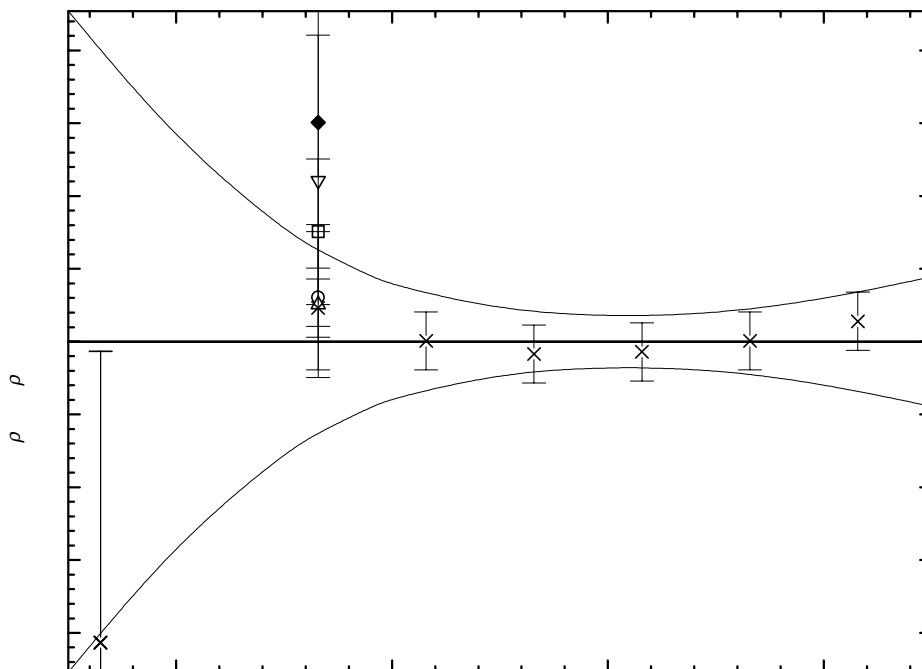
**Further references:** [56-lev/sch, 62-mel].

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
270.00	972.64 ± 4.54	298.15	956.43 ± 0.89	330.00	935.08 ± 0.38
280.00	967.17 ± 2.76	300.00	955.28 ± 0.78	340.00	927.71 ± 0.58
290.00	961.38 ± 1.53	310.00	948.86 ± 0.43	350.00	920.03 ± 0.89
293.15	959.49 ± 1.25	320.00	942.13 ± 0.34		

cont.

**2,5-Hexanediol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**3,4-Hexanediol** [922-17-8] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 692

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	799.3 ± 20.0	1859-wur

**2-Methyl-1,3-pentanediol** [149-31-5] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 693

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
295.15	973.7 ± 2.0	43-kul/nor <sup>1)</sup>
293.15	971.8 ± 1.0	52-cur/joh
293.15	972.9 ± 1.0	60-ano-13
293.15	972.3 ± 1.1	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Methyl-1,5-pentanediol** [42856-62-2] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 694**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	971.9 ± 1.0	51-mca/cul
293.15	971.9 ± 1.0	51-whi/dea
293.15	975.0 ± 2.0	62-yur/rev <sup>1)</sup>
293.15	971.9 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**2-Methyl-2,3-pentanediol** [7795-80-4] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 695**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.200$ .

Coefficient	$\rho = A + BT$
$A$	1167.70
$B$	-0.700

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
293.15	962.7 ± 1.0	0.20	28-ven-1
273.15	976.3 ± 1.0	-0.20	28-ven-1

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
270.00	978.7 ± 1.1
280.00	971.7 ± 0.9
290.00	964.7 ± 1.0
293.15	962.5 ± 1.0
298.15	959.0 ± 1.2

**2-Methyl-2,4-pentanediol** [107-41-5] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 696**Table 1.** Coefficients of the polynomial expansion equation. Standard deviations (see introduction): $\sigma_{\text{c,w}} = 4.4579 \cdot 10^{-1}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 1.7903 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 273.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
$A$	$1.09017 \cdot 10^3$
$B$	$-4.33615 \cdot 10^{-1}$
$C$	$-4.76496 \cdot 10^{-4}$

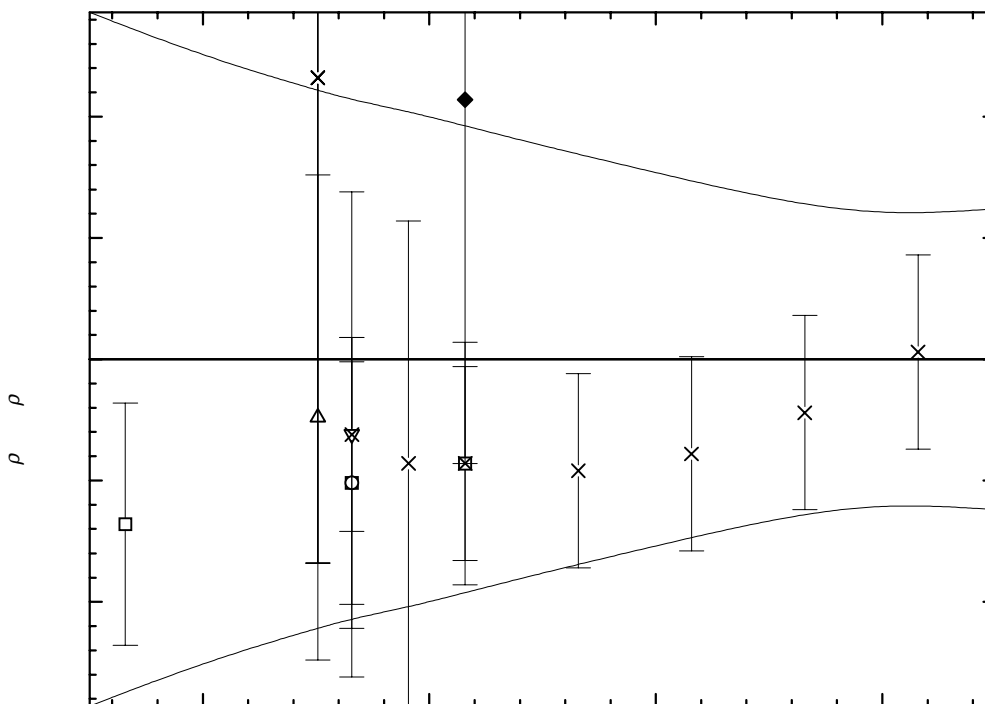
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**2-Methyl-2,4-pentanediol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
290.15	925.40 ± 2.00	1.16	01-zel/zel(✕)	298.15	920.00 ± 1.50	1.47	62-ste/van(◆)
290.15	924.00 ± 1.00	-0.24	12-ost(Δ)	303.15	916.00 ± 1.50	1.07	62-ste/van(◆)
290.15	925.40 ± 2.00	1.16	39-dup/dar(✕)	293.15	921.60 ± 0.60	-0.51	68-ano(○)
293.15	921.80 ± 1.00	-0.31	53-ano-5(∇)	293.15	921.80 ± 0.40	-0.31	96-gri/zhu(✕)
293.15	924.00 ± 2.00	1.89	57-chi/tho <sup>1)</sup>	303.15	914.50 ± 0.40	-0.43	96-gri/zhu(✕)
298.15	918.10 ± 1.00	-0.43	57-chi/tho(✕)	313.15	907.20 ± 0.40	-0.46	96-gri/zhu(✕)
273.15	935.50 ± 0.50	-0.68	62-mel(□)	323.15	899.90 ± 0.40	-0.39	96-gri/zhu(✕)
293.15	921.60 ± 0.50	-0.51	62-mel(□)	333.15	892.60 ± 0.40	-0.22	96-gri/zhu(✕)
303.15	914.50 ± 0.50	-0.43	62-mel(□)	343.15	885.30 ± 0.40	0.03	96-gri/zhu(✕)

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [52-cur/joh, 56-far/she].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

cont.



**Table 3.** Recommended values (fit to the reliable experimental values according to the equations  $\rho = A + BT + CT^2 + DT^3 + \dots$  or  $\rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4]$ ).

$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{K}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
270.00	938.36 ± 1.43	298.15	918.53 ± 1.02	330.00	895.19 ± 0.66
280.00	931.40 ± 1.25	300.00	917.20 ± 1.00	340.00	887.66 ± 0.59
290.00	924.35 ± 1.11	310.00	909.96 ± 0.88	350.00	880.03 ± 0.62
293.15	922.11 ± 1.07	320.00	902.62 ± 0.77		

**3-Methyl-1,3-pentandiol** [33879-72-0] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 697

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	972.6 ± 3.0	32-pfa/pla <sup>1)</sup>
273.15	975.5 ± 2.0	48-zal <sup>1)</sup>
290.75	965.5 ± 2.0	48-zal <sup>1)</sup>
293.15	969.0 ± 1.0	62-esa/shi
293.15	969.0 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Methyl-1,5-pentandiol** [4457-71-0] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 698

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	973.8 ± 1.0	51-mca/cul
293.15	973.8 ± 1.0	51-whi/dea
293.15	972.6 ± 1.0	55-blo/ver-1
293.15	973.8 ± 1.0	56-ano-3
293.15	973.5 ± 1.0	Recommended

**3-Methyl-2,3-pentandiol** [63521-37-9] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 699

**Table 1.** Experimental and recommended values with uncertainties.

$\frac{T}{K}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
293.15	970.1 ± 2.0	52-van <sup>1)</sup>
288.15	975.0 ± 2.0	52-van <sup>1)</sup>
298.15	963.8 ± 1.0	58-hen/wat
298.15	963.8 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Methyl-2,4-pentanediol** [5683-44-3] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 700

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
287.15	990.6 ± 2.0	01-zel/zel

**4-Methyl-1,4-pentanediol** [1462-10-8] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 701

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.15	965.1 ± 2.0	52-wil/sch <sup>1)</sup>
293.15	964.5 ± 1.0	55-sar/mor
293.15	970.0 ± 2.0	58-col/fal <sup>1)</sup>
293.15	964.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-(1-Methylethyl)-1,3-propanediol** [2612-27-3] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 702

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	976.2 ± 1.0	53-pin/hun
293.15	977.0 ± 0.5	62-bog/osi
293.15	976.8 ± 0.5	Recommended

**2-Propyl-1,3-propanediol** [2612-28-4] C<sub>6</sub>H<sub>14</sub>O<sub>2</sub> MW = 118.18 703

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	963.6 ± 2.0	48-adk/bil <sup>1)</sup>
293.15	965.9 ± 0.5	62-bog/osi
293.15	965.9 ± 0.5	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

3.1.2 Alkanediols, C<sub>7</sub> - C<sub>14</sub>

**2-Butyl-1,3-propanediol** [2612-26-2] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 704

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	946.1 ± 1.0	48-ack/bil

**2,2-Diethyl-1,3-propanediol** [115-76-4] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 705

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
<i>crystal</i>		
293.15	1052.0 ± 5.0	54-ano-12
293.15	1052.0 ± 5.0	60-ano-13
293.15	1052.0 ± 5.0	62-mel
<i>liquid</i>		
334.45	949.0 ± 2.0	54-ano-12
334.45	949.0 ± 2.0	60-ano-13

**2,3-Dimethyl-1,3-pentanediol** [66225-52-3] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 706

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
296.15	957.0 ± 1.0	53-col/dre

**2,3-Dimethyl-2,3-pentanediol** [6931-70-0] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 707

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	961.3 ± 2.0	41-fav/oni

**(R\*,S\*)-2,4-Dimethyl-1,5-Pentanediol** [3817-48-9] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 708

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	945.0 ± 2.0	55-nol/pan

**2,4-Dimethyl-2,4-pentanediol** [24892-49-7] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 709

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	920.6 ± 2.0	09-lem-1

**3,4-Dimethyl-1,4-pentanediol** [63521-36-8] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 710

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	952.8 ± 1.0	57-sar/vor

**2-Ethyl-1,5-pentanediol** [14189-13-0] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 711

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	967.9 ± 1.0	62-yur/rev

**2-Ethyl-2,4-pentanediol** [38836-25-8] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 712

**Table 1.** Experimental and recommended values with uncertainties.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	920.6 ± 4.0	09-lem <sup>1)</sup>
293.15	929.6 ± 2.0	63-esa
293.15	929.6 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**3-Ethylpentane-2,3-diol** [66225-32-9] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 713

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	961.2 ± 2.0	58-hen/wat

**1,4-Heptanediol** [40646-07-9] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 714

**Table 1.** Fit with estimated  $B$  coefficient for 4 accepted points. Deviation  $\sigma_w = 0.173$ .

Coefficient	$\rho = A + BT$
$A$	1158.80
$B$	-0.700

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	954.3 ± 2.0	0.70	27-bra/ada <sup>1)</sup>
298.15	950.4 ± 1.0	0.30	34-bur/adk
288.15	957.0 ± 1.0	-0.10	51-gor
288.15	957.0 ± 1.0	-0.10	51-gor
288.15	957.0 ± 1.0	-0.10	52-roe/stu

<sup>1)</sup> Not included in calculation of linear coefficients.

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
280.00	962.8 ± 1.3	293.15	953.6 ± 0.8
290.00	955.8 ± 0.7	298.15	950.1 ± 1.1

**1,5-Heptanediol****[60096-09-5]****C<sub>7</sub>H<sub>16</sub>O<sub>2</sub>****MW = 132.2****715****Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	970.5 ± 2.0	25-pie/ada
288.15	962.0 ± 6.0	35-pau-2 <sup>1)</sup>
293.15	970.5 ± 2.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**1,6-Heptanediol****[13175-27-4]****C<sub>7</sub>H<sub>16</sub>O<sub>2</sub>****MW = 132.2****716****Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	962.0 ± 2.0	66-bue

**1,7-Heptanediol****[629-30-1]****C<sub>7</sub>H<sub>16</sub>O<sub>2</sub>****MW = 132.2****717****Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

 $\sigma_{\text{c,w}} = 1.9518 \cdot 10^{-2}$  (combined temperature ranges, weighted), $\sigma_{\text{c,uw}} = 9.7590 \cdot 10^{-3}$  (combined temperature ranges, unweighted).

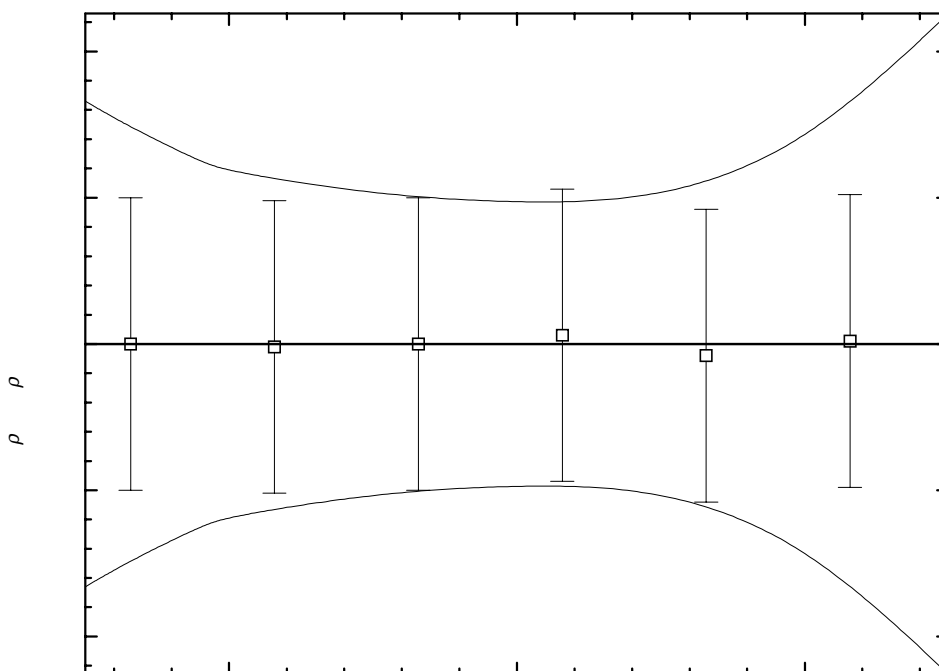
Coefficient	$T = 293.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.12164 \cdot 10^3$
B	$-5.46836 \cdot 10^{-1}$
C	$-7.14286 \cdot 10^{-5}$

cont.

**1,7-Heptanediol** (cont.)**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref. (Symbol in Fig. 1)
293.15	955.20 ± 0.50	0.00	96-gri/zhu(□)	323.15	937.50 ± 0.50	0.03	96-gri/zhu(□)
303.15	949.30 ± 0.50	-0.01	96-gri/zhu(□)	333.15	931.50 ± 0.50	-0.04	96-gri/zhu(□)
313.15	943.40 ± 0.50	0.00	96-gri/zhu(□)	343.15	925.60 ± 0.50	0.01	96-gri/zhu(□)

**Further references:** [34-bur/adk, 51-hub, 64-pol/bel].



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>	$T$ K	$\rho \pm \sigma_{\text{fit}}$ kg·m <sup>-3</sup>
290.00	957.05 ± 0.83	300.00	951.16 ± 0.59	330.00	933.41 ± 0.49
293.15	955.20 ± 0.74	310.00	945.26 ± 0.51	340.00	927.46 ± 0.67
298.15	952.25 ± 0.62	320.00	939.34 ± 0.48	350.00	921.50 ± 1.13

**2,4-Heptanediol** [20748-86-1] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 718**Table 1.** Fit with estimated *B* coefficient for 2 accepted points. Deviation  $\sigma_w = 0.100$ .

Coefficient	$\rho = A + BT$
A	1134.61
B	-0.700

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg·m <sup>-3</sup>	Ref.
298.15	926.0 ± 1.0	0.10	39-stu/adk
288.15	932.8 ± 1.0	-0.10	47-dev

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>
280.00	938.6 ± 1.1	293.15	929.4 ± 0.9
290.00	931.6 ± 0.9	298.15	925.9 ± 0.9

**3,4-Heptanediol** [62593-33-3] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 719**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	945.7 ± 2.0	25-pie/ada <sup>1)</sup>
295.15	943.0 ± 1.0	36-wie
295.15	943.0 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.**2-Methyl-2,4-hexanediol** [66225-35-2] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 720**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
291.15	932.1 ± 1.0	26-pas/zam

**2-Methyl-2,6-hexanediol** [1462-11-9] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 721**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
295.15	967.0 ± 2.0	56-cri

**4-Methyl-1,5-hexanediol** [66225-37-4] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 722**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	966.3 ± 2.0	62-yur/pen

**2-Methyl-2-propyl-1,3-propanediol** [78-26-2] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 723

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	857.0 ± 1.0	54-ano-12
293.15	857.1 ± 1.0	59-ano-7
293.15	858.5 ± 1.0	60-ano-13
293.15	857.5 ± 1.1	Recommended

**2-(1-Methylethyl)-1,4-butanediol** [39497-66-0] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 724

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	967.2 ± 0.8	54-fre/lwo

**2-Propyl-1,4-butanediol** [62946-68-3] C<sub>7</sub>H<sub>16</sub>O<sub>2</sub> MW = 132.2 725

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	962.5 ± 2.0	14-lon

**2,4-Dimethyl-2,4-hexanediol** [29649-22-7] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 726

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.35	922.9 ± 2.0	34-jac-5

**2,5-Dimethyl-2,4-hexanediol** [3899-89-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 727

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	917.2 ± 2.0	64-esa/das

**3,4-Dimethyl-2,4-hexanediol** [90002-90-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 728

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	938.2 ± 2.0	62-fav/por



**3,5-Dimethyl-2,3-hexanediol** [99799-29-8] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 729

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	915.7 ± 2.0	51-ber-2 <sup>1)</sup>
298.15	928.5 ± 1.0	58-hen/wat
298.15	928.5 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Ethyl-1,3-hexanediol** [94-96-2] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 730

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.176$ .

Coefficient	$\rho = A + BT$
$A$	1180.92
$B$	-0.820

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
295.15	938.4 ± 2.0	-0.50	64-bla/per-1
293.15	940.6 ± 1.0	0.06	53-ano-15
293.15	940.6 ± 1.0	0.06	62-mel

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
290.00	943.1 ± 1.3
293.15	940.5 ± 1.2
298.15	936.4 ± 1.3

**2-Ethyl-1-methyl-1,5-pentanediol** [900002-72-4] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 731

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	960.0 ± 2.0	62-yur/rev

**4-Ethyl-1,4-hexanediol** [1113-00-4] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 732

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
292.15	970.4 ± 1.0	51-gor

**4-Ethyl-1,5-hexanediol** [90951-82-9] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 733

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	960.0 ± 2.0	62-yur/pen

**2-Methyl-2,3-heptanediol** [1068-81-1] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 734

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	929.0 ± 2.0	64-col/var

**3-Methyl-3,5-heptanediol** [99799-27-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 735

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
291.15	929.9 ± 2.0	26-pas/zam
294.15	928.0 ± 2.0	51-dub

**5-Methyl-1,5-heptanediol** [99799-26-5] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 736

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
292.15	961.0 ± 2.0	56-cri

**5-Methyl-2,4-heptanediol** [500014-48-2] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 737

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	928.0 ± 2.0	39-stu/adk

**6-Methyl-1,6-heptanediol** [5392-57-4] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 738

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	959.0 ± 2.0	66-bue

**2-(1-Methylethyl)-1,5-pentanediol** [90951-89-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 739

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	956.1 ± 2.0	62-yur/rev

**1,5-Octanediol** [2736-67-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 740

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.15	949.0 ± 2.0	35-pau-2 <sup>1)</sup>	298.15	949.0 ± 1.0	66-bue-1
289.15	946.0 ± 2.0	56-cri <sup>1)</sup>	298.15	949.0 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**1,6-Octanediol** [4066-76-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 741

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	943.0 ± 3.0	65-mor/lam
298.15	954.0 ± 3.0	66-bue

**1,7-Octanediol** [13175-32-1] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 742

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	942.0 ± 1.0	62-col/gir
298.15	944.0 ± 1.0	66-bue
298.15	943.0 ± 1.2	Recommended

**2,4-Octanediol** [90162-24-6] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 743

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	918.0 ± 2.0	39-stu/adk

**2-Propyl-1,5-pentanediol** [90951-90-9] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 744

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	953.0 ± 2.0	62-yur/rev

**2,2,4-Trimethyl-1,3-pentanediol** [144-19-4] C<sub>8</sub>H<sub>18</sub>O<sub>2</sub> MW = 146.23 745

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
296.15	961.0 ± 10.0	43-kul/nor <sup>1)</sup>
293.15	922.9 ± 1.0	59-ano-7
293.15	922.9 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Butyl-2-ethyl-1,3-propanediol** [115-84-4] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 746

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
323.15	929.0 ± 1.0	53-ano-15	323.15	931.0 ± 2.0	62-mel <sup>1)</sup>
323.15	929.0 ± 1.0	60-ano-13	323.15	929.0 ± 1.0	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**2-Butyl-1,5-pentanediol** [90724-91-7] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 747

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	941.4 ± 2.0	62-yur/rev

**2,4-Dimethyl-2,4-heptanediol** [59194-83-1] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 748

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
290.35	913.8 ± 2.0	34-jac-5

**2,4-Dimethyl-2,6-heptanediol** [73264-94-5] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 749

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	920.0 ± 1.5	64-hin/dre

**2,5-Dimethyl-3,5-heptanediol** [3955-69-9] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 750

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	915.6 ± 2.0	64-esa/das

**2,6-Dimethyl-2,4-heptanediol** [73264-93-4] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 751

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.15	902.0 ± 2.0	26-pas/zam

**4,4-Dimethyl-1,7-heptanediol** [900002-74-6] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 752

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	939.0 ± 1.0	55-blo/whe

**4-Ethyl-1,4-heptanediol** [900002-73-5] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 753

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	970.0 ± 2.0	64-des/sou

**5-Ethyl-1,5-heptanediol** [57740-06-4] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 754

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
291.15	958.0 ± 2.0	56-cri

**3-Methyl-3,5-octanediol** [38836-28-1] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 755

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	916.0 ± 1.0	62-esa/zhu

**4-Methyl-2,4-octanediol** [38836-27-0] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 756

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	911.7 ± 1.0	63-esa

**6-Methyl-1,6-octanediol** [13175-25-2] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 757

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	952.0 ± 2.0	66-bue

**6-Methyl-1,7-octanediol** [91391-44-5] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 758

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	953.0 ± 2.0	62-col/gir

**7-Methyl-1,7-octanediol** [13175-30-9] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 759

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	938.0 ± 2.0	66-bue

**1-Methyl-2-propyl-1,5-pentanediol** [900002-75-7] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 760

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	954.3 ± 2.0	62-yur/pen

**2-(2-Methylpropyl)-1,5-pentanediol** [57740-10-0] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 761

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	941.6 ± 2.0	62-yur/rev

**1,4-Nonanediol** [2430-73-1] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 762

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	929.5 ± 1.0	62-nik/vor

**1,5-Nonanediol** [13686-96-9] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 763

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	937.0 ± 1.0	25-pie/ada

**1,6-Nonanediol** [4066-78-8] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 764

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
294.15	935.0 ± 3.0	65-mor/lam
298.15	941.0 ± 3.0	66-bue

**1,7-Nonanediol** [4469-84-5] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 765

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	944.0 ± 2.0	66-bue

**4-Propyl-1,5-hexanediol** [13687-05-3] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 766

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	954.3 ± 2.0	62-yur/pen

**2,4,5-Trimethyl-2,4-hexanediol** [36587-81-2] C<sub>9</sub>H<sub>20</sub>O<sub>2</sub> MW = 160.26 767

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
301.35	920.7 ± 2.0	34-jac-5

**1,4-Decanediol** [37810-94-9] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 768

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	922.0 ± 2.0	62-nik/vor
293.15	917.6 ± 1.0	51-gor
293.15	917.6 ± 1.0	52-roe/stu

**1,7-Decanediol** [13175-33-2] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 769

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	929.0 ± 2.0	66-bue

**1,10-Decanediol** [112-47-0] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 770**Table 1.** Fit with estimated *B* coefficient for 4 accepted points. Deviation  $\sigma_w = 2.320$ .

Coefficient	$\rho = A + BT$
<i>A</i>	1151.52
<i>B</i>	-0.755

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{\rho_{\text{exp}} - \rho_{\text{calc}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
<i>crystal</i>			
298.15	1100.0 ± 5.0		62-par/mos
<i>liquid</i>			
353.15	883.0 ± 1.5	-1.89	50-boe/ned
403.15	850.0 ± 2.0	2.86	50-boe/ned
453.15	812.0 ± 2.0	2.61	50-boe/ned
513.15	762.0 ± 2.0	-2.09	50-boe/ned

**Table 3.** Recommended values.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$
350.00	887.3 ± 4.4	410.00	842.0 ± 2.9	470.00	796.7 ± 3.9
360.00	879.7 ± 4.1	420.00	834.4 ± 2.9	480.00	789.1 ± 4.2
370.00	872.2 ± 3.7	430.00	826.9 ± 2.9	490.00	781.6 ± 4.6
380.00	864.6 ± 3.4	440.00	819.3 ± 3.1	500.00	774.0 ± 5.0
390.00	857.1 ± 3.2	450.00	811.8 ± 3.3	510.00	766.5 ± 5.4
400.00	849.5 ± 3.0	460.00	804.2 ± 3.5	520.00	758.9 ± 5.8

**2,5-Diethyl-1,6-hexanediol** [91241-30-4] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 771**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	930.7 ± 1.0	38-hil/adk

**3,4-Diethyl-3,4-hexanediol** [6931-71-1] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 772**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
298.15	943.5 ± 0.2	79-bal/fri

**2,4-Dimethyl-2,4-octanediol** [7177-01-7] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 773**Table 1.** Experimental value with uncertainty.

$\frac{T}{\text{K}}$	$\frac{\rho_{\text{exp}} \pm 2\sigma_{\text{est}}}{\text{kg} \cdot \text{m}^{-3}}$	Ref.
294.65	902.0 ± 1.0	34-jac-5



**2,5-Dimethyl-3,5-octanediol** [3899-88-5] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 774

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	909.7 ± 2.0	64-esa/das

**3,7-Dimethyl-1,6-octanediol** [53067-10-0] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 775

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	948.1 ± 2.0	32-lon/kha

**3,7-Dimethyl-1,7-octanediol** [107-74-4] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 776

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	926.0 ± 2.0	42-mul

**3,7-Dimethyl-3,5-octanediol** [56548-45-9] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 777

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
285.15	911.8 ± 2.0	26-pas/zam

**3,4-Dimethyl-3,4-octanediol** [91179-88-3] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 778

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	932.6 ± 1.0	64-nog/rtv

**3,7-Dimethyl-1,3-octanediol** [102880-60-4] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 779

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	916.5 ± 2.0	32-pfa/pla

**2,3-Dipropyl-1,4-butanediol** [74854-17-4] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 780

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg·m <sup>-3</sup>	Ref.
293.15	936.2 ± 2.0	39-mar/wil

**4-Ethyl-3,5-octanediol** [900002-77-9] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 781

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	926.3 ± 1.0	51-dra-1

**6-Methyl-2-(1-methylethyl)-1,3-hexanediol** [900002-78-0] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 782

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
296.15	916.1 ± 2.0	43-kul/nor

**2-Methyl-2,3-nonanediol** [900002-76-8] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 783

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
273.15	937.5 ± 2.0	26-nic

**6-Methyl-1,6-nonanediol** [13175-26-3] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 784

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	942.0 ± 2.0	66-bue

**7-Methyl-1,7-nonanediol** [13379-31-2] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 785

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	934.0 ± 2.0	66-bue

**2-Propyl-1,3-heptanediol** [6628-65-5] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 786

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
301.15	915.5 ± 2.0	43-kul/nor

**2,4,6-Trimethyl-2,4-heptanediol** [33070-42-7] C<sub>10</sub>H<sub>22</sub>O<sub>2</sub> MW = 174.28 787

**Table 1.** Fit with estimated  $B$  coefficient for 3 accepted points. Deviation  $\sigma_w = 0.696$ .

Coefficient	$\rho = A + BT$
$A$	1117.71
$B$	-0.720

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$\rho_{\text{exp}} - \rho_{\text{calc}}$ kg · m <sup>-3</sup>	Ref.
293.15	906.1 ± 2.0	-0.54	31-deg
288.15	909.8 ± 2.0	-0.44	31-deg
292.35	908.2 ± 2.0	0.98	34-jac-5

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>
280.00	916.1 ± 2.0	293.15	906.6 ± 1.9
290.00	908.9 ± 1.9	298.15	903.0 ± 2.0

**4,4-Diethyl-1,7-heptanediol** [72936-15-3] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 788

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	953.0 ± 2.0	79-zel/hub

**2,4-Dimethyl-2,4-nonanediol** [69201-96-3] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 789

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
299.75	896.3 ± 2.0	34-jac-5

**3-Methyl-3,4-decanediol** [90002-79-1] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 790

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
273.15	940.0 ± 2.0	26-nic

**7-Methyl-1,7-decanediol** [13175-31-0] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 791

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
298.15	929.0 ± 2.0	66-bue

**2,4,7-Trimethyl-2,4-octanediol** [90002-80-4] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 792

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
295.35	896.1 ± 2.0	34-jac-5

**1,4-Undecanediol** [4272-02-0] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 793

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	915.7 ± 1.0	65-das/mae

**1,5-Undecanediol** [13686-98-1] C<sub>11</sub>H<sub>24</sub>O<sub>2</sub> MW = 188.31 794

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
294.15	914.0 ± 2.0	56-cri

**2-Butyl-1,3-octanediol** [55109-62-1] C<sub>12</sub>H<sub>26</sub>O<sub>2</sub> MW = 202.34 795

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
298.15	918.4 ± 2.0	43-kul/nor

**4-Methyl-4,5-undecanediol** [90002-81-5] C<sub>12</sub>H<sub>26</sub>O<sub>2</sub> MW = 202.34 796

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
273.15	935.5 ± 2.0	26-nic

**2-Methyl-1,4-dodecanediol** [92153-96-3] C<sub>13</sub>H<sub>28</sub>O<sub>2</sub> MW = 216.36 797

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	897.2 ± 2.0	62-nik/vor

**3-Methyl-1,3-dodecanediol** [90002-82-6] C<sub>13</sub>H<sub>28</sub>O<sub>2</sub> MW = 216.36 798

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	902.0 ± 2.0	32-pfa/pla

**2-Pentyl-1,3-nonanediol** [55109-63-2] C<sub>14</sub>H<sub>30</sub>O<sub>2</sub> MW = 230.39 799

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
296.15	898.4 ± 2.0	43-kul/nor

## 3.2 Unsaturated Diols

### 3.2.1 Unsaturated Diols of General Formula C<sub>n</sub>H<sub>2n</sub>O<sub>2</sub>

**2-Butene-1,4-diol** [110-64-5] C<sub>4</sub>H<sub>8</sub>O<sub>2</sub> MW = 88.11 800

**Table 1.** Experimental values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
288.15	1082.0 ± 3.0	46-pre/val
293.15	1080.0 ± 3.0	48-pud
293.15	1080.0 ± 3.0	48-val
298.15	1080.0 ± 3.0	78-ovc/kry

**(E)-2-Butene-1,4-diol** [821-11-4] C<sub>4</sub>H<sub>8</sub>O<sub>2</sub> MW = 88.11 801

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	1068.7 ± 1.0	52-cur/joh
293.15	1068.5 ± 0.8	56-smi/ebe
293.15	1068.6 ± 0.8	Recommended

**(Z)-2-Butene-1,4-diol** [6117-80-2] C<sub>4</sub>H<sub>8</sub>O<sub>2</sub> MW = 88.11 802

**Table 1.** Experimental and recommended values with uncertainties.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
293.15	1069.8 ± 2.0	28-pre-4 <sup>1)</sup>
294.15	1069.9 ± 2.0	44-pre <sup>1)</sup>
293.15	1074.0 ± 0.8	56-smi/ebe
293.15	1074.0 ± 0.8	Recommended

<sup>1)</sup> Not included in calculation of recommended value.

**(Z)-2-Pentene-1,4-diol** [500036-05-5] C<sub>5</sub>H<sub>10</sub>O<sub>2</sub> MW = 102.13 803

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ kg · m <sup>-3</sup>	Ref.
291.15	1017.0 ± 2.0	51-gor

**(Z)-4-Methyl-2-pentene-1,4-diol** [500036-09-9]  $C_6H_{12}O_2$  MW = 116.16 804

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
290.15	$990.0 \pm 2.0$	51-gor

**(Z)-2-Heptene-1,4-diol** [83726-19-6]  $C_7H_{14}O_2$  MW = 130.19 805

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
299.65	$970.0 \pm 2.0$	51-gor

**5-Methyl-3-hexene-1,5-diol** [19764-75-1]  $C_7H_{14}O_2$  MW = 130.19 806

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$980.2 \pm 1.0$	67-min/che

**(Z)-4-Ethyl-2-hexene-1,4-diol** [500036-10-2]  $C_8H_{16}O_2$  MW = 144.21 807

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
288.15	$974.0 \pm 0.0$	51-gor

**5-Methyl-3-heptene-1,5-diol** [19764-76-2]  $C_8H_{16}O_2$  MW = 144.21 808

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$972.5 \pm 1.0$	67-min/che

**5-Methyl-3-octene-1,5-diol** [19764-77-3]  $C_9H_{18}O_2$  MW = 158.24 809

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	$\text{kg} \cdot \text{m}^{-3}$	
293.15	$955.5 \pm 1.0$	67-min/che

**(Z)-2-Decene-1,4-diol** [500036-07-7] C<sub>10</sub>H<sub>20</sub>O<sub>2</sub> MW = 172.27 810

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	930.0 ± 2.0	51-gor

**3,4-Dimethyl-5-octene-3,4-diol** [91008-98-9] C<sub>10</sub>H<sub>20</sub>O<sub>2</sub> MW = 172.27 811

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	970.4 ± 2.0	64-nog/rtv

**2-Dodecene-1,4-diol** [97029-80-6] C<sub>12</sub>H<sub>24</sub>O<sub>2</sub> MW = 200.32 812

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	934.3 ± 2.0	62-nik/vor

**6,7-Diethyl-3-methyl-6-nonene-3,4-diol** [20368-03-0] C<sub>14</sub>H<sub>28</sub>O<sub>2</sub> MW = 228.38 813

**Table 1.** Experimental value with uncertainty.

$T$	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$	Ref.
K	kg · m <sup>-3</sup>	
293.15	921.2 ± 1.0	67-zal/aru





3.2.2 Unsaturated Diols of General Formula  $C_nH_{2n-2}O_2$ 

**2-Butyne-1,4-diol** [110-65-6]  $C_4H_6O_2$  MW = 86.09 814

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$1100.1 \pm 0.0$	66 -koz/rab

**2-Pentyne-1,4-diol** [927-57-1]  $C_5H_8O_2$  MW = 100.12 815

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
290.15	$1072.0 \pm 1.5$	51-gor

**2-Methyl-3-pentyne-2,5-diol** [90002-87-1]  $C_6H_{10}O_2$  MW = 114.14 816

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$1029.1 \pm 1.0$	66-vla/vas

**4-Methyl-2-pentyne-1,4-diol** [10605-66-0]  $C_6H_{10}O_2$  MW = 114.14 817

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
290.15	$1029.0 \pm 2.5$	51-gor

**2-Heptyne-1,4-diol** [18864-39-6]  $C_7H_{12}O_2$  MW = 128.17 818

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
288.15	$1012.4 \pm 1.5$	51-gor

**4-Methyl-2-hexyne-1,4-diol** [920-09-2]  $C_7H_{12}O_2$  MW = 128.17 819

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$1022.40 \pm 1.0$	66-vla/vas

**4-Ethyl-2-hexyne-1,4-diol** [163005-62-7]  $C_8H_{14}O_2$  MW = 142.2 820

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
291.15	$1000.5 \pm 2.0$	51-gor

**4-Methyl-2-heptyne-1,4-diol** [10605-67-1]  $C_8H_{14}O_2$  MW = 142.2 821

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$996.5 \pm 1.0$	66-vla/vas

**2-Decyne-1,4-diol** [71393-78-7]  $C_{10}H_{18}O_2$  MW = 170.25 822

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 0.200$ .

Coefficient	$\rho = A + BT$
$A$	1148.34
$B$	-0.680

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
273.15	$962.4 \pm 1.0$	-0.20	51-gor
293.15	$949.2 \pm 1.0$	0.20	51-gor

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$
270.00	$964.7 \pm 1.1$
280.00	$957.9 \pm 0.9$
290.00	$951.1 \pm 1.0$
293.15	$949.0 \pm 1.0$
298.15	$945.6 \pm 1.2$

**3,4-Dimethyl-5-octyne-3,4-diol** [92490-84-1]  $C_{10}H_{18}O_2$  MW = 170.25 823

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$964.2 \pm 2.0$	64-nog/rtv

## 4 Tabulated Data on Density - Triols

**1,2,3-Propanetriol**

[56-81-5]

$C_3H_8O_3$

MW = 92.09

824

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 5.4871 \cdot 10^{-1}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.5204 \cdot 10^{-1}$  (combined temperature ranges, unweighted).

Coefficient	$T = 288.15 \text{ to } 533.15 \text{ K}$ $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.43632 \cdot 10^3$
B	$-5.28889 \cdot 10^{-1}$
C	$-2.29556 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

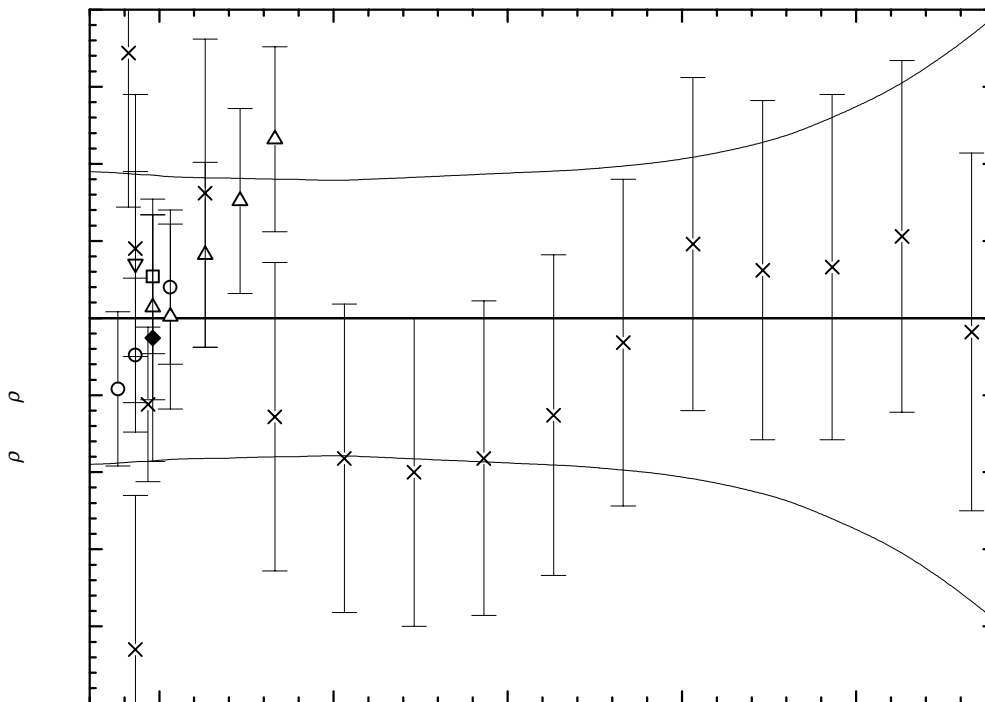
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)
293.15	$1259.40 \pm 1.00$	-2.15	1864-lan(✕)	333.15	$1234.00 \pm 1.00$	-0.64	58-cos/bow(✕)
291.15	$1264.60 \pm 1.00$	1.72	07-che-1(✕)	353.15	$1220.00 \pm 1.00$	-0.91	58-cos/bow(✕)
295.65	$1257.20 \pm 1.00$	-2.69	07-che-1 <sup>1)</sup>	373.15	$1206.00 \pm 1.00$	-1.00	58-cos/bow(✕)
288.15	$1264.40 \pm 0.50$	-0.46	35-tim/hen(○)	393.15	$1192.00 \pm 1.02$	-0.91	58-cos/bow(✕)
293.15	$1261.31 \pm 0.50$	-0.24	35-tim/hen(○)	413.15	$1178.00 \pm 1.04$	-0.63	58-cos/bow(✕)
303.15	$1255.09 \pm 0.50$	0.20	35-tim/hen(○)	433.15	$1164.00 \pm 1.06$	-0.16	58-cos/bow(✕)
298.15	$1258.50 \pm 0.50$	0.27	37-alb(□)	453.15	$1150.00 \pm 1.08$	0.48	58-cos/bow(✕)
298.15	$1258.30 \pm 0.60$	0.07	42-bri/rin(Δ)	473.15	$1135.00 \pm 1.10$	0.31	58-cos/bow(✕)
303.15	$1254.90 \pm 0.60$	0.01	42-bri/rin(Δ)	493.15	$1120.00 \pm 1.12$	0.33	58-cos/bow(✕)
313.15	$1248.60 \pm 0.60$	0.41	42-bri/rin(Δ)	513.15	$1105.00 \pm 1.14$	0.53	58-cos/bow(✕)
323.15	$1242.20 \pm 0.60$	0.76	42-bri/rin(Δ)	533.15	$1089.00 \pm 1.16$	-0.09	58-cos/bow(✕)
333.15	$1235.80 \pm 0.60$	1.16	42-bri/rin(Δ)	553.15	$1068.00 \pm 1.18$	-5.53	58-cos/bow <sup>1)</sup>
296.75	$1258.60 \pm 0.50$	-0.56	46-par/wes(✕)	293.15	$1261.90 \pm 0.60$	0.35	68-ano(∇)
293.15	$1262.00 \pm 1.00$	0.45	58-cos/bow(✕)	298.15	$1258.10 \pm 0.80$	-0.13	69-ver/lau(◆)
313.15	$1249.00 \pm 1.00$	0.81	58-cos/bow(✕)				

<sup>1)</sup> Not included in Fig. 1.

**Further references:** [1885-sto, 1891-gla, 17-jae-1, 32-bri-2, 35-but/ram-1, 36-ern/wat, 70-che/tho, 77-cam/sch].

cont.

## 1,2,3-Propanetriol (cont.)



**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$	$\frac{T}{\text{K}}$	$\frac{\rho \pm \sigma_{\text{fit}}}{\text{kg} \cdot \text{m}^{-3}}$
280.00	1270.23 ± 0.95	360.00	1216.17 ± 0.90	460.00	1144.46 ± 1.07
290.00	1263.64 ± 0.94	370.00	1209.21 ± 0.91	470.00	1137.03 ± 1.12
293.15	1261.55 ± 0.93	380.00	1202.19 ± 0.92	480.00	1129.56 ± 1.18
298.15	1258.23 ± 0.93	390.00	1195.14 ± 0.93	490.00	1122.05 ± 1.27
300.00	1256.99 ± 0.92	400.00	1188.04 ± 0.94	500.00	1114.49 ± 1.37
310.00	1250.30 ± 0.91	410.00	1180.89 ± 0.95	510.00	1106.88 ± 1.48
320.00	1243.57 ± 0.91	420.00	1173.69 ± 0.96	520.00	1099.23 ± 1.62
330.00	1236.79 ± 0.90	430.00	1166.45 ± 0.98	530.00	1091.53 ± 1.78
340.00	1229.96 ± 0.90	440.00	1159.17 ± 1.00	540.00	1083.78 ± 1.96
350.00	1223.09 ± 0.89	450.00	1151.84 ± 1.03		

**1,2,4-Butanetriol** [3068-00-6]  $C_4H_{10}O_3$  MW = 106.12 825

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
298.15	$1184.0 \pm 2.0$	62-mel

**1,3,5-Pentanetriol** [4328-94-3]  $C_5H_{12}O_3$  MW = 120.15 826

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
298.15	$1103.6 \pm 1.0$	48-ack/bil

**1,2,6-Hexanetriol** [106-69-4]  $C_6H_{14}O_3$  MW = 134.18 827

**Table 1.** Coefficients of the polynomial expansion equation.

Standard deviations (see introduction):

$\sigma_{c,w} = 5.4613 \cdot 10^{-2}$  (combined temperature ranges, weighted),

$\sigma_{c,uw} = 1.4472 \cdot 10^{-2}$  (combined temperature ranges, unweighted).

Coefficient	$T = 293.15$ to $343.15$ K $\rho = A + BT + CT^2 + DT^3 + \dots$
A	$1.26157 \cdot 10^3$
B	$-4.84437 \cdot 10^{-1}$
C	$-1.92931 \cdot 10^{-4}$

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

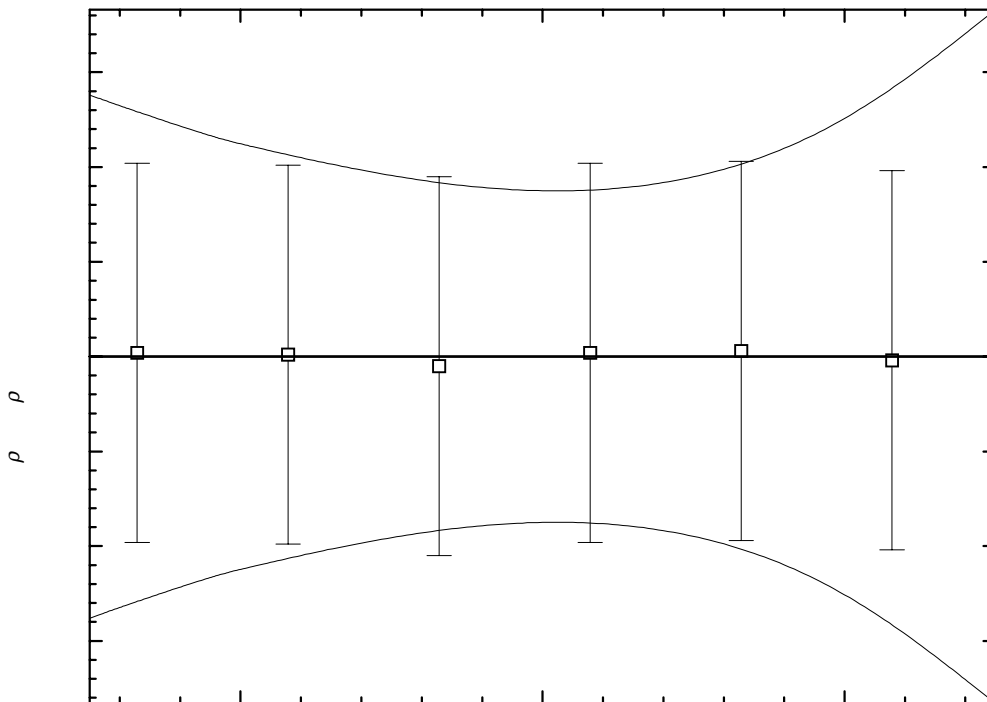
$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)	$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref. (Symbol in Fig. 1)
293.15	$1103.00 \pm 1.00$	0.02	96-gri/zhu(□)	323.15	$1084.90 \pm 1.00$	0.02	96-gri/zhu(□)
303.15	$1097.00 \pm 1.00$	0.01	96-gri/zhu(□)	333.15	$1078.80 \pm 1.00$	0.03	96-gri/zhu(□)
313.15	$1090.90 \pm 1.00$	-0.05	96-gri/zhu(□)	343.15	$1072.60 \pm 1.00$	-0.02	96-gri/zhu(□)

**Table 3.** Recommended values (fit to the reliable experimental values according to the equations

$$\rho = A + BT + CT^2 + DT^3 + \dots \text{ or } \rho = [1 + 1.75(1 - T/T_c)^{1/3} + 0.75(1 - T/T_c)][\rho_c + A(T_c - T) + B(T_c - T)^2 + C(T_c - T)^3 + D(T_c - T)^4].$$

$T$ K	$\rho \pm \sigma_{\text{fit}}$ $\text{kg} \cdot \text{m}^{-3}$	$T$ K	$\rho \pm \sigma_{\text{fit}}$ $\text{kg} \cdot \text{m}^{-3}$	$T$ K	$\rho \pm \sigma_{\text{fit}}$ $\text{kg} \cdot \text{m}^{-3}$
290.00	$1104.86 \pm 1.38$	300.00	$1098.88 \pm 1.12$	330.00	$1080.70 \pm 0.91$
293.15	$1102.98 \pm 1.29$	310.00	$1092.86 \pm 0.94$	340.00	$1074.56 \pm 1.20$
298.15	$1099.99 \pm 1.16$	320.00	$1086.80 \pm 0.85$	350.00	$1068.39 \pm 1.83$

cont.

**1,2,6-Hexanetriol** (cont.)

**Fig. 1.** The symbols show the deviation of the calculated from the experimental values from Table 2. The curves above and below the zero line indicate the calculated error region of the recommended values given in Table 3. The error bars represent the experimental errors. (Error bars smaller than the symbols are omitted for clarity of the figure.)

**1,3,6-Hexanetriol** [18990-98-2]  $C_6H_{14}O_3$  MW = 134.18 828

**Table 1.** Experimental value with uncertainty.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
293.15	$1104.1 \pm 10.0$	62-nik/vor

**1,4,7-Heptanetriol** [3920-53-4]  $C_7H_{16}O_3$  MW = 148.2 829

**Table 1.** Fit with estimated  $B$  coefficient for 2 accepted points. Deviation  $\sigma_w = 1.260$ .

Coefficient	$\rho = A + BT$
$A$	1259.98
$B$	-0.640

cont.

**Table 2.** Experimental values with uncertainties and deviation from calculated values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$	$\rho_{\text{exp}} - \rho_{\text{calc}}$ $\text{kg} \cdot \text{m}^{-3}$	Ref.
291.00	$1075.0 \pm 3.0$	1.26	18-ham
273.00	$1084.0 \pm 3.0$	-1.26	18-ham

**Table 3.** Recommended values.

$T$ K	$\rho_{\text{exp}} \pm 2\sigma_{\text{est}}$ $\text{kg} \cdot \text{m}^{-3}$
270.00	$1087.2 \pm 3.2$
280.00	$1080.8 \pm 3.0$
290.00	$1074.4 \pm 3.1$
293.15	$1072.4 \pm 3.2$
298.15	$1069.2 \pm 3.4$

## References

Reference codes are those used in the TRC SOURCE database. A reference code consists of the year prior to 1900, or the last two digits of the year after 1899, the first three letters of the first author, the first three letters of the second author. An additional sequence number is used when more than one reference in the database has an identical code.

- 1811-bra Brande, W. T.; *Philos. Trans. R. Soc. London* **101** (1811) 337.  
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1869-lie Lieben, A.; *Justus Liebigs Ann. Chem.* **150** (1869) 87.  
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