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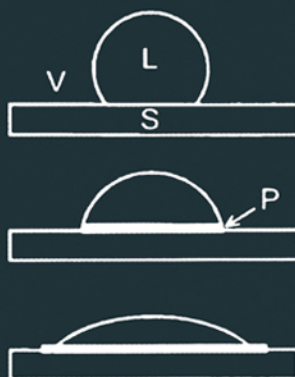
# WETTABILITY AT HIGH TEMPERATURES

by

N. EUSTATHOPOULOS

M.G. NICHOLAS

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Pergamon

**PERGAMON MATERIALS SERIES  
VOLUME 3**

## **Wettability at High Temperatures**

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**PERGAMON MATERIALS SERIES**

# **Wettability at High Temperatures**

by

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## Series Preface

My editorial objective in this new series is to present to the scientific public a collection of texts that satisfies one of two criteria: the systematic presentation of a specialised but important topic within materials science or engineering that has not previously (or recently) been the subject of full-length treatment and is in rapid development; or the systematic account of a broad theme in materials science or engineering.

The books are not, in general, designed as undergraduate texts, but rather are intended for use at graduate level and by established research workers. However, teaching methods are in such rapid evolution that some of the books may well find use at an earlier stage in university education.

I have long editorial experience both in covering the whole of a huge field – physical metallurgy or materials science and technology – and in arranging for specialised subsidiary topics to be presented in monographs. My intention is to apply the lessons learned in 40 years of editing to the objectives stated above. Authors have been invited for their up-to-date expertise and also for their ability to see their subjects in a wider perspective.

I am grateful to Elsevier Science Ltd., who own the Pergamon Press imprint, and equally to my authors, for their confidence.

The third book in the Series, on a topic not previously treated in full-length book form, is presented herewith to our readership.

ROBERT W. CAHN, FRS  
(Cambridge University, UK)



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# Preface

The purpose of this book is to bring together current scientific understanding of wetting behaviour that has been gained from theoretical models and quantitative experimental observations. The materials considered are liquid metals or inorganic glasses in contact with solid metals or ceramics at temperatures of 200-2000°C.

Wetting has been a significant scientific concern for the last two centuries and reference will be made to classical work by nineteenth century scientists such as Dupré, Laplace and Young that was validated by observations of the behaviour of chemically inert ambient-temperature systems. This classical work still provides the basic language for discussions of wetting behaviour and similar studies have continued in recent decades to provide understanding of the effects of factors such as the roughness or chemical heterogeneity of the solid surface. Due and proper notice is given both to such work and to studies dedicated to high-temperature systems. Although a limited number of wetting studies at high temperature were published before World War II, the first systematic studies, motivated mainly by the importance of wetting properties in powder metallurgy and steel-making, were performed in the fifties by Kingery and co-workers in the USA, Bailey and Watkins in the UK, Kozakevitch in France and Eremenko and Naidich in the Ukraine. A new impetus to wetting studies was given in the eighties by increased interest in the fabrication of metal-matrix composites by liquid routes and the joining of metals and particularly of ceramics by brazing and glazing. This intensification was accompanied by a marked increase in the number of research teams specializing in this field and it is significant that original papers have been published by teams from more than twenty different countries during the last five years.

Although many basic concepts established for chemically inert ambient temperature systems are also valid for high-temperature systems, these latter systems possess specific characteristics that exert a major influence on their wetting properties. First, the surface properties of nearly all metals and many ceramics at high temperatures are extremely sensitive to impurities, mainly oxygen, that are invariably contained in furnace atmospheres. For this reason, particular attention is paid throughout this book to interactions between oxygen and metallic or ceramic surfaces and to their effects on surface chemistry and wetting behaviour. Because only those wetting studies which were carried out during the last decade have benefited from high-resolution techniques for characterization of surfaces, recent experimental results are generally, but not exclusively, preferred to older

ones. Secondly, contrary to “low-temperature” materials, the cohesion of which is due to weak physical interactions, the liquids and solids of concern in wetting at high temperatures are bonded by strong chemical forces (metallic, ionic or covalent) and quite often the liquid/solid interface required is between materials with different bonding characteristics, as when brazing ceramics or glazing metals. Understanding of interactions *at non-reactive interfaces* between dissimilar materials of high cohesion is a formidable challenge and wetting studies, allowing measurement of the key parameter of *work of adhesion*, have contributed greatly to this understanding. Finally, many liquid/solid couples are far from chemical equilibrium and the resultant interfacial reactions can strongly modify the chemistry, structure and topography of interfaces. These changes affect both spreading kinetics and the ultimate degree of wetting and those aspects of *reactive wetting* that can be exploited in practice to control wetting and adhesion are extensively developed in this book.

In attempting to achieve the aims of the book, the text has been divided into ten Chapters that can be grouped into four stages of presentation. The first stage comprises two Chapters that review established and newly developed models for their relevance to wetting behaviour at high temperatures, including recent models that encompass the role of chemical reactions at the solid/liquid interfaces. Attention is paid both to equilibrium wetting behaviour (Chapter 1) and to the factors that control the approach to equilibrium (Chapter 2). Then follow Chapters concerned with experimental techniques for scientific measurement of the extent of wetting (Chapter 3) and with the surface energy data for both metals and non-metals that are essential for quantitative interpretation of wetting behaviour (Chapter 4). Descriptions of experimentally determined and quantified wetting behaviour are presented and interpreted in the third part comprising five Chapters dealing with the characteristics of metal/metal, metal/oxide, metal/non-oxide, metal/carbon and molten glass/solid systems. The book concludes with a Chapter commenting on the role of wetting behaviour in joining similar and dissimilar materials by liquid route techniques.

This preface cannot be ended before a grateful acknowledgement is made of the assistance generously given by many professional colleagues during the writing of the book. Those who have influenced our technical growth and have promoted our general understanding of wetting behaviour are too numerous to mention but particular thanks are due to a number who have made specific contributions that have assisted the formulation of this book. Jean-Paul Garandet of the CEA (Grenoble, France), Andréas Mortensen of the EPFL (Lausanne, Switzerland), Alberto Passerone of the ICFAM-CNR (Genova, Italy), Stathis Peteves of the JRC (Petten, The Netherlands), Christian Chatillon, Lucien Coudurier, Jean-Charles Joud, Alain Pasturel and Cyril Rado of the LTPCM (Grenoble,

France) kindly read and commented on individual Chapters. Nick Ebrill of the University of Newcastle (Australia) allowed us to read his as yet unpublished thesis. Robert Cahn of Cambridge University, the series editor, is particularly deserving of our thanks for initiating the writing of this book and for exercising a remarkable tolerance of its prolonged gestation. We are also of course grateful to our families for cheerfully enduring the domestic and social disruptions caused by the writing process. Finally, it should be noted that while many people have helped with this book we are solely responsible for any errors of omission or commission.

BÉATRICE DREVET, NICOLAS EUSTATHOPOULOS  
and MICHAEL NICHOLAS  
*January 1999*

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*“Now, supposing the angle of the fluid to be obtuse, the whole superficial cohesion of the fluid being represented by the radius, the part which acts in the direction of the surface of the solid will be proportional to the cosine of the inclination ; and this force, added to the force of the solid, will be equal to the force of the common surface of the solid and fluid, or to the differences of their forces (...). And the same result follows when the angle of the fluid is acute.”*

The famous Young’s equation, as described by Thomas Young himself in his original paper “An Essay on the Cohesion of Fluids” published in 1805 in Philosophical Transactions of the Royal Society of London (vol. 94, p. 65).

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## Chapter 1

# Fundamental equations of wetting

This first Chapter provides a context and language for subsequent analysis of the many and varied important scientific and technical aspects of high temperature capillarity. It does so by first defining the thermodynamic and atomistic characteristics of the interfaces between different phases and then by developing the fundamental equations describing the wetting behaviour of *ideal* surfaces of chemically inert systems. Since a controversy regarding the validity of Young's equation periodically appears in the literature, particular attention is drawn to the effects of factors such as gravity, scale of observation, system size and time scale. Then, the wetting behaviour of *real* surfaces is presented taking into account the effects of roughness and chemical heterogeneity of the solid surface. The energetical quantities used to describe the various types of wetting occurring in practice (immersion, spreading, infiltration) are defined and discussed at the end of this Chapter.

### 1.1. SURFACE AND INTERFACIAL ENERGIES IN SOLID/LIQUID/VAPOUR SYSTEMS

The work needed for reversible creation of additional surface of a liquid L in contact with a vapour V, identified by the term  $\sigma_{LV}$ , was defined by Gibbs (1961) as :

$$\sigma_{LV} = \left( \frac{\partial F}{\partial \Omega} \right)_{T, v, n_i} \quad (1.1)$$

where F is the total free energy of the system,  $\Omega$  the surface area, T temperature, v volume and  $n_i$  the number of moles of component i. The dimensions of  $\sigma_{LV}$  are energy per unit area. However this definition is not sufficient to describe the work needed for creation of a solid S surface because this can occur by two different processes.

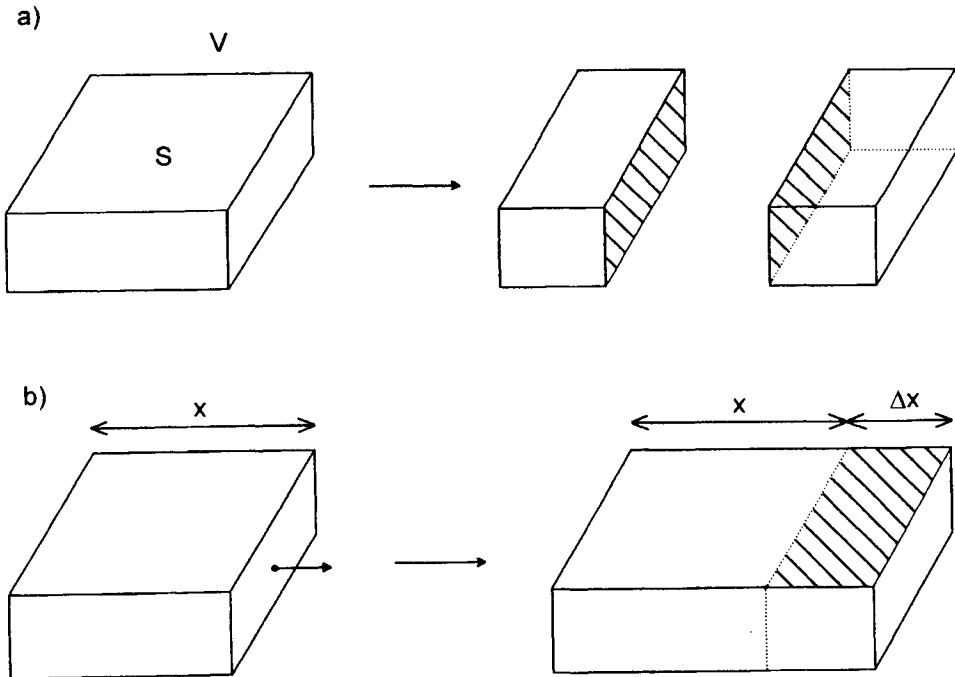
First, the new surface can be created *at constant strain* by breaking bonds to increase the number of solid atoms (or molecules) which belong to the surface. A typical example of such a process is cleavage achieved without any elastic or plastic deformation of the solid (Figure 1.1.a). The reversible work done to create a surface of unit area by this process is simply  $\sigma_{SV}$  :



$$\sigma_{SV} = \left( \frac{\partial F}{\partial \Omega} \right)_{T, V, n_i} \quad (1.2)$$

Although  $\sigma_{SV}$  is a specific surface *free* energy quantity (it includes both energy and entropy), it is often called “surface energy” because of the greater simplicity of this term, and to avoid any confusion with the “specific surface free energy” defined by Gibbs which, in multicomponents systems, is different from  $\sigma_{SV}$  (Defay et al. 1966). In the following,  $\sigma_{SV}$ , as defined by equation (1.2), will be called the solid surface energy.

Second, the new surface can be created *without increasing the number of surface atoms* by purely elastic strain of the solid (Figure 1.1.b). The extra stress due to the surface, called by Gibbs “surface tension” or by other authors “surface stress” (Mullins 1963, Cahn 1989), is denoted as  $\gamma_{SV}$  and expressed as a force per unit length.



**Figure 1.1.** Creation of solid surfaces (shaded) by cleavage (a) and elastic deformation (b).

For liquids,  $\sigma_{LV}$  and  $\gamma_{LV}$  are equal because a reversible stretching of a liquid surface is identical to a reversible creation of new surface. In both cases, the liquid can increase its surface area only by the addition of new atoms to the surface. Note that, from a dimension point of view, an energy per unit area is equivalent to a force per unit length and the values are numerically equal when  $\sigma_{LV}$  is measured in  $\text{J.m}^{-2}$  (or  $\text{mJ.m}^{-2}$ ) and  $\gamma_{LV}$  is measured in  $\text{N.m}^{-1}$  (or  $\text{mN.m}^{-1}$ ).

For solids,  $\sigma_{SV}$  and  $\gamma_{SV}$  are different quantities. For instance, for each crystal face, there is a unique value of  $\sigma_{SV}$  (which is a scalar) while  $\gamma_{SV}$  depends also on the orientation along the face. Moreover,  $\sigma_{SV}$  is always a positive quantity (breaking bonds needs work to be done) while  $\gamma_{SV}$  can be either positive or negative (Nolfi and Johnson 1972). For high symmetry surfaces, the surface tension is related to the surface energy by the equation (Shuttleworth 1950) :

$$\gamma_{SV} = \sigma_{SV} + \frac{d\sigma_{SV}}{d\varepsilon} \quad (1.3)$$

where  $\varepsilon$  is a macroscopic elastic strain. The physical origin of the difference between  $\gamma_{SV}$  and  $\sigma_{SV}$  i.e., of the term  $d\sigma_{SV} / d\varepsilon$  in equation (1.3), can be explained taking into account the atomistic origin of  $\sigma_{SV}$ . As it will be seen below for monoatomic solids,  $\sigma_{SV}$  is proportional to the difference in potential energy between an atom of the surface and an atom of the bulk solid (equation (1.13)). When a new surface is created by stretching the solid (Figure 1.1.b), this difference does not remain constant. Indeed, because surface atoms are bonded weakly compared to those in the bulk, the work needed to stretch the surface is less than for the bulk material.

From now on, for S/V and S/L boundaries, only the surface and interfacial energies,  $\sigma_{SV}$  and  $\sigma_{SL}$ , will be considered. For L/V surfaces, both the surface tension  $\gamma_{LV}$  and surface energy  $\sigma_{LV}$  will be used interchangeably depending on the context.

Let us consider two bodies A and B which can be either two solids, or two liquids or a solid and a liquid, that have a unit cross-sectional area. A and B are surrounded by a vapour phase V at constant temperature. The free energy change corresponding to the reversible creation of two new surfaces of A and of B of unit area, by the process schematized on Figure 1.2, is :

$$\Delta F_{1-2} = 2(\sigma_{AV} + \sigma_{BV}) \quad (1.4)$$

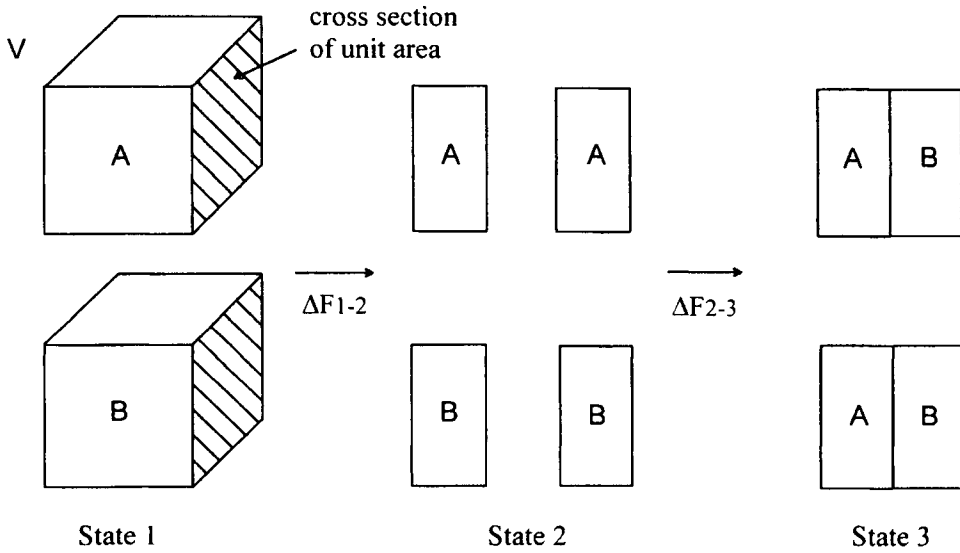
Similarly, the free energy change corresponding to creation of two A/B interfaces by joining two surfaces of A and of B is equal to :

$$\Delta F_{2-3} = 2(\sigma_{AB} - \sigma_{AV} - \sigma_{BV}) \quad (1.5)$$

Finally, the transformation 1-3 corresponds to :

$$\Delta F_{1-3} = \Delta F_{1-2} + \Delta F_{2-3} = 2\sigma_{AB} \quad (1.6)$$

where  $\sigma_{AB}$  is the A/B interface energy.



**Figure 1.2.** Formation of two A/B interfaces of unit area from pure A and B bodies.

For pure A or B, the quantity  $2\sigma_{AV}$  or  $2\sigma_{BV}$  defines the *work of cohesion*  $W_c$  of A or B :

$$W_c^A = 2\sigma_{AV} \quad (1.7.a)$$

$$W_c^B = 2\sigma_{BV} \quad (1.7.b)$$

In equation (1.5), the quantity  $(\sigma_{AB} - \sigma_{AV} - \sigma_{BV})$  is equal but with an opposite sign to the *work of adhesion* defined by Dupré (1869) :

$$W_a = \sigma_{AV} + \sigma_{BV} - \sigma_{AB} \quad (1.8)$$

These macroscopic quantities can be related to the bond energies  $\varepsilon_{AA}$  and  $\varepsilon_{BB}$  in the bulk phases and  $\varepsilon_{AB}$  at the interface by a simple “nearest neighbour” interaction model. Assuming that :

- A and B are monoatomic solids that are chemically inert towards each other,
- A and B have the same crystal lattice and the same atomic volume and are perfectly matched at the interface,
- both cohesion and adhesion result from atomic interactions between nearest neighbours,
- entropy contributions to surface energies are negligible,

the three interfacial energies contained in equation (1.8) can be calculated simply from transformation 1-2 of Figure 1.2 :

$$\sigma_{AV} = -\frac{Zm_l}{\omega} \frac{\varepsilon_{AA}}{2} \quad (1.9)$$

$$\sigma_{BV} = -\frac{Zm_l}{\omega} \frac{\varepsilon_{BB}}{2} \quad (1.10)$$

and from transformation 1-3 :

$$\sigma_{AB} = \frac{Zm_l}{\omega} \left[ \varepsilon_{AB} - \frac{\varepsilon_{AA} + \varepsilon_{BB}}{2} \right] \quad (1.11)$$

Using equation (1.8), one obtains :

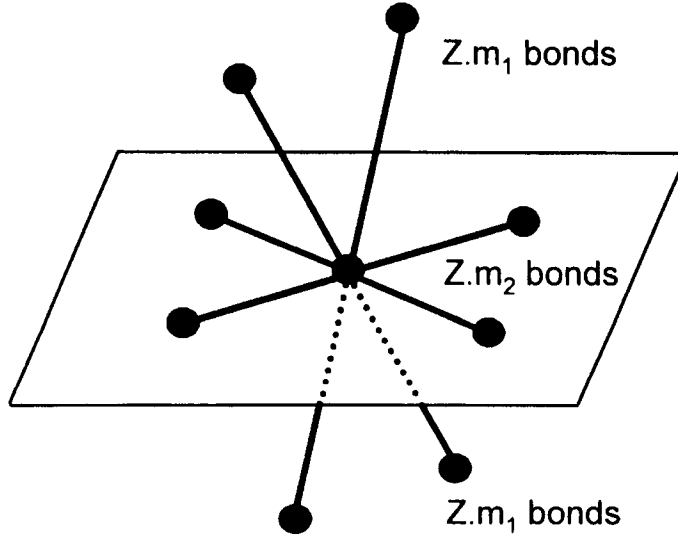
$$W_a = -\frac{Zm_l}{\omega} \varepsilon_{AB} \quad (1.12)$$

In equations (1.9) to (1.12),  $\omega$  is the surface area per atom,  $Z$  the number of nearest neighbours in the bulk crystal,  $m_l$  the fraction of broken bonds at the surface of A or B per atom and  $\varepsilon_{AA}$ ,  $\varepsilon_{BB}$  and  $\varepsilon_{AB}$  the bond pair energies, defined as negative quantities.

It is also interesting to derive the expression of the surface energy of a crystal, by equating this quantity to the difference in potential energy of an atom at the surface ( $E'$ ) and a bulk atom ( $E$ ) divided by the surface area per atom  $\omega$  :

$$\sigma_{AV} = \frac{E' - E}{\omega} \quad (1.13)$$

In the framework of the nearest neighbour model,  $E'$  and  $E$  equal the product of the number of atoms in nearest neighbour position and the pair energy per atom i.e.,  $E' = Z(m_1 + m_2)\epsilon_{AA} / 2$  and  $E = Z(2m_1 + m_2)\epsilon_{AA} / 2$ , where  $m_2$  is the fraction of nearest neighbours located in the surface plane ( $2m_1 + m_2 = 1$ ) (Figure 1.3). Introducing the expressions for  $E'$  and  $E$  into equation (1.13) leads to expression (1.9).



**Figure 1.3.** Definition of the fractions  $m_2$  and  $2m_1$  of nearest neighbours lying respectively in the same plane and in adjacent planes for a bulk atom lying in a symmetry plane of a crystal and having  $Z$  nearest neighbours.

The bond energies  $\epsilon_{AA}$  and  $\epsilon_{BB}$  are related to the energy of sublimation per atom  $L_s$  of the crystals A and B as follows :

$$L_s^A = -Z \frac{\epsilon_{AA}}{2} \quad (1.14)$$

Combining equations (1.9) and (1.14) yields :

$$\sigma_{AV}\omega = m_1 L_s^A \quad (1.15)$$

This equation shows that the surface energy *per atom*  $\sigma_{AV}\omega$  of a monoatomic solid A is proportional to  $L_s^A$ . For a given family of compounds, a correlation between the surface energy per atom and the energy of sublimation (or evaporation) is expected provided  $m_1$  is constant. Such correlations hold well for the solid and liquid surfaces of metallic bodies and also for the liquid surfaces of oxides and halides (see Figures 4.1, 4.9 and 4.10).

Equation (1.12) indicates that the magnitude of  $W_a$  directly reflects the intensity of interactions between A and B atoms across the common interface. Obviously, in real systems, the relation between  $W_a$  and bond energies is more complicated than equation (1.12) suggests. However, the physical meaning of  $W_a$  remains the same.

## 1.2. IDEAL SOLID SURFACES

Consider a flat, undeformable, perfectly smooth and chemically homogeneous solid surface in contact with a non-reactive liquid in the presence of a vapour phase. If the liquid does not completely cover the solid, the liquid surface will intersect the solid surface at a “contact angle”  $\theta$ . The equilibrium value of  $\theta$ , used to define the wetting behaviour of the liquid, obeys the classical equation of Young (1805):

$$\cos \theta_Y = \frac{\sigma_{SV} - \sigma_{SL}}{\sigma_{LV}} \quad (1.16)$$

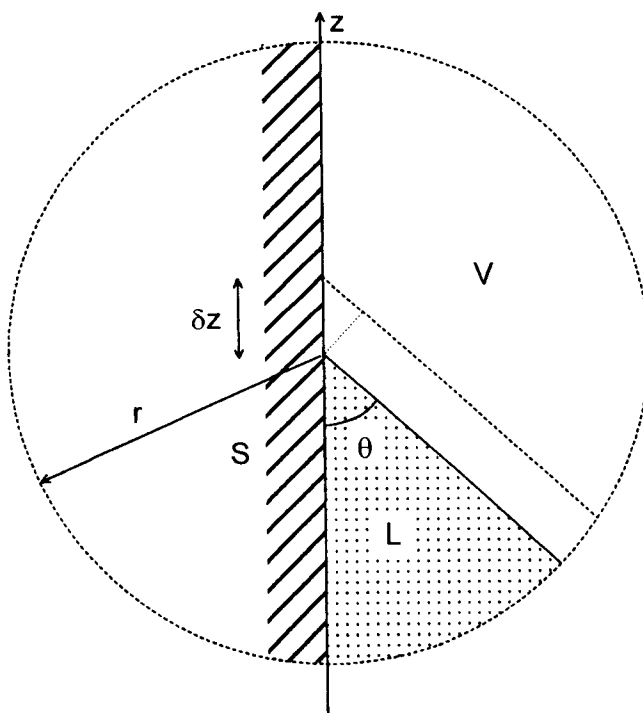
In this book, a contact angle of less than  $90^\circ$  will identify a wetting liquid, while a greater value will identify a non-wetting liquid. If the contact angle is zero, the liquid will be considered to be perfectly wetting (see also Table 1.1 in Section 1.4.1).

Equation (1.16) can be easily derived by calculating the variation of the *surface* free energy  $F_s$  of the system caused by a small displacement  $\delta z$  of the S/L/V *triple line*, usually hereafter referred to as TL. In Figure 1.4 the solid surface is vertical and TL is perpendicular to the plane of the figure and assumed to be a straight line, rendering the problem two-dimensional. Thus, the total length of TL is constant during its displacement, as in the case of a meniscus formed on a vertical plate. Moreover, the radius  $r$  of the TL region considered in this calculation (Figure 1.4) is much larger than the range of atomic (or molecular) interactions in the system.

For metallic and ionocovalent ceramics, this range is roughly 1–2 nm, while for bodies with long range van der Waals interactions it can attain 10 nm (de Gennes 1985). However, the radius  $r$  must be small compared to a characteristic dimension of the liquid, for instance the average drop base radius  $R$  in the sessile drop configuration (see Figure 1.6) or the maximum height of a meniscus formed on a vertical solid wall (see Figure 1.9) which are both typically in the millimetre range. Further, inside the region of radius  $r$ , the intersection of the L/V surface with the plane of Figure 1.4 is assumed to be essentially a straight line. With these assumptions, the variation of interfacial free energy per unit length of TL, resulting from a small linear displacement  $\delta z$  of TL, is:

$$F_s(z + \delta z) - F_s(z) = \delta F_s = (\sigma_{SL} - \sigma_{SV})\delta z + \cos(\theta)\sigma_{LV}\delta z \quad (1.17)$$

and the equilibrium condition  $d(\delta F_s)/d(\delta z) = 0$  leads to equation (1.16).

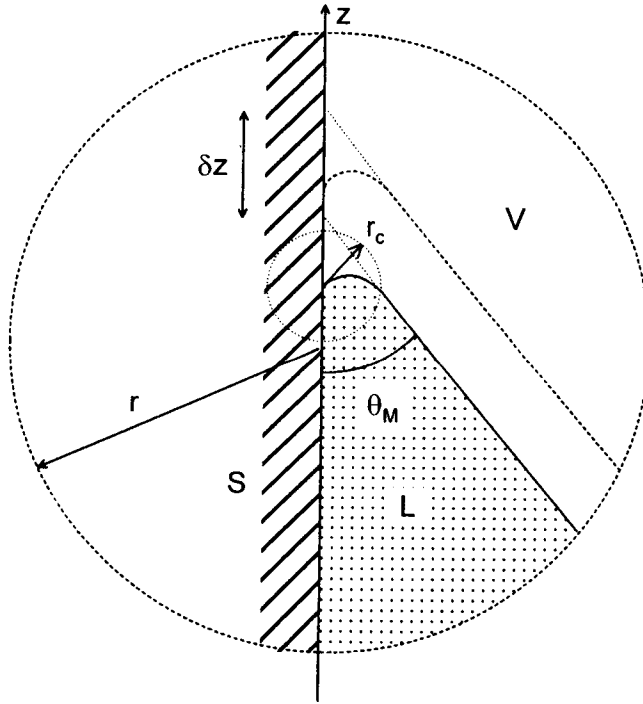


**Figure 1.4.** Displacement of a triple line around its equilibrium position that allows derivation of the Young equation. Only a small region close to the triple line is taken into account to neglect the curvature of the L/V surface.

### 1.2.1 Microscopic and macroscopic contact angles

In practice, the geometry in a *core* region around TL, i.e. inside a sphere of radius  $r_c$  which is of the order of the range of atomic interactions in the system, can be different from that shown in Figure 1.4. Due to long range interactions, the energy of an atom lying on a given interface inside this core region is different to the energy of an atom at the same interface far from TL. Thus, the three relevant interfacial energies close to and far from TL are different and this difference increases with the range of atomic interactions. Consequently, the local contact angle, as far as it can be defined at this nanometric scale, may be different to the macroscopic contact angle  $\theta_M$ . An example is given schematically on Figure 1.5.

As pointed out by de Gennes (1985), the deviation of TL from its nominal position does not modify equation (1.17) provided this deviation does not change during the displacement  $\delta z$ . This is a reasonable assumption for small displacements around the equilibrium position.



**Figure 1.5.** As Figure 1.4 but showing a microscopic contact angle different from the macroscopic  $\theta_M$ .



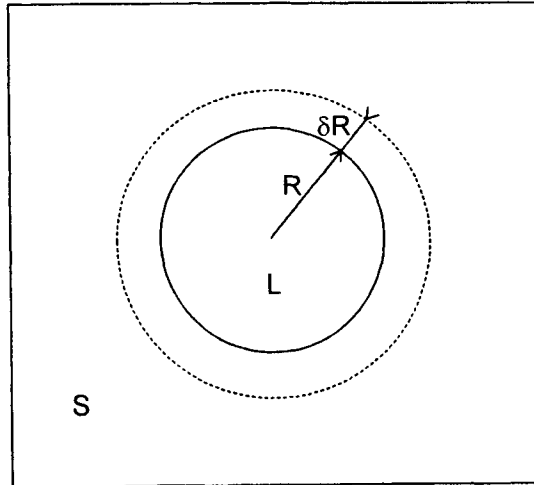
### 1.2.2 Effect of system size

In the sessile drop configuration (Figure 1.6), when the drop size becomes of the order of magnitude of the radius  $r_c$  of the core region defined in Figure 1.5, the relevant contact angle is no longer the Young contact angle but the microscopic contact angle. The relation between these two angles has been discussed using the concept of line energy (or line tension). During wetting, the increase  $\delta R$  of the drop base radius leads to an increase of the TL length (Figure 1.6) and the free energy associated with the increase of the TL length must be taken into account in the interfacial energy calculation. The triple line can be treated phenomenologically as an equilibrium line defect with a specific *excess* free energy  $\tau$  (per unit length). To some extent, it can be compared to the step energy on faceted crystals used to describe crystal growth or changes of crystal surface energy with crystallographic orientation in the case of vicinal surfaces. Then, the variation of interfacial free energy during wetting in the sessile drop configuration (Figure 1.6) is:

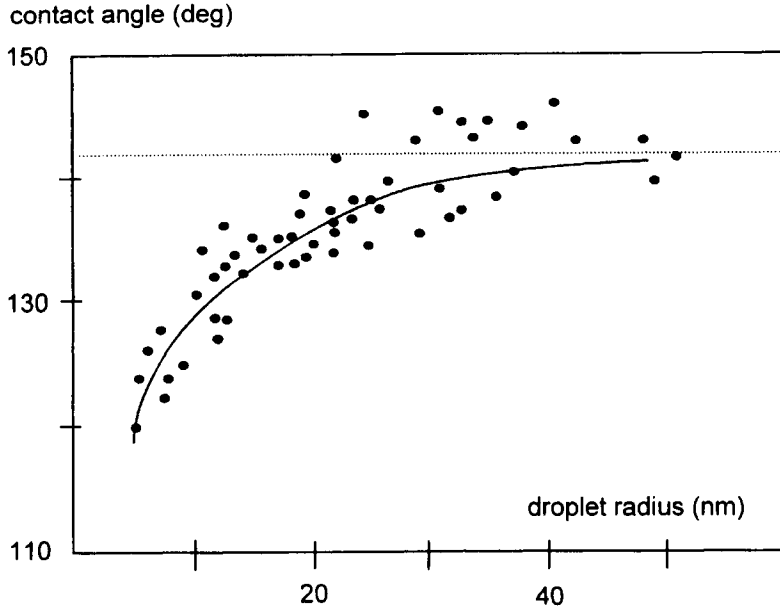
$$\delta F_s = 2\pi R(\sigma_{SL} - \sigma_{SV})\delta R + 2\pi R \cos(\theta)\sigma_{LV}\delta R + 2\pi\tau\delta R \quad (1.18)$$

Therefore, the equilibrium condition  $d(\delta F_s)/d(\delta R) = 0$  leads to:

$$\cos \theta_{eq} = \cos \theta_Y - \frac{\tau}{R\sigma_{LV}} \quad (1.19)$$



**Figure 1.6.** Top view of a sessile drop during spreading.



**Figure 1.7.** Dependence of contact angle on the metal droplet radius for Pb on vitreous carbon at a temperature close to the melting point of Pb. The horizontal line identifies the macroscopic contact angle. Data from work reported in (Chizhik et al. 1985).

The importance of the corrective term  $\tau(R\sigma_{LV})^{-1}$  decreases when the drop size increases and it appears to be negligible for  $R > 100$  nm (Shcherbakov et al. 1995). For instance, no significant differences in contact angle of pure Cu on monocrystalline  $\text{Al}_2\text{O}_3$  were found between millimetre and micron size Cu droplets (Soper et al. 1996). However, the correction can be important for very small drops, for instance for those nucleated by condensation on to solid substrates, which can be as small as a few nanometers. For such small droplets, differences in contact angle of tens of degrees can exist, corresponding to differences in work of adhesion of 100%, as shown by the results in Figure 1.7 for pure Pb on vitreous carbon. Thus, care has to be taken in the use of contact angle data obtained with macroscopic droplets in small size systems because no information, either theoretical or experimental, about  $\tau$  is available for high temperature materials.

Note that equation (1.19) has been established assuming the line energy  $\tau$  to be a constant. However it was argued (Marmur 1997) that since this quantity results from the atomic or molecular interactions between the three phases in the vicinity of the triple line, it cannot be independent of the contact angle since the relative inclination of the phases affects the extent of these interactions. Calculations of  $\tau$

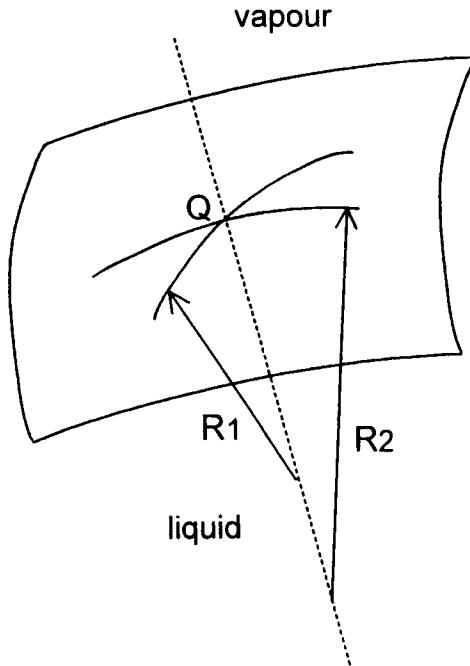
for liquid/solid systems bonded by van der Waals interactions confirmed this point and showed that, for this type of system, the sign of  $\tau$  is positive for acute contact angles and negative for obtuse contact angles.

### 1.2.3 Effect of the curvature of the liquid/vapour surface

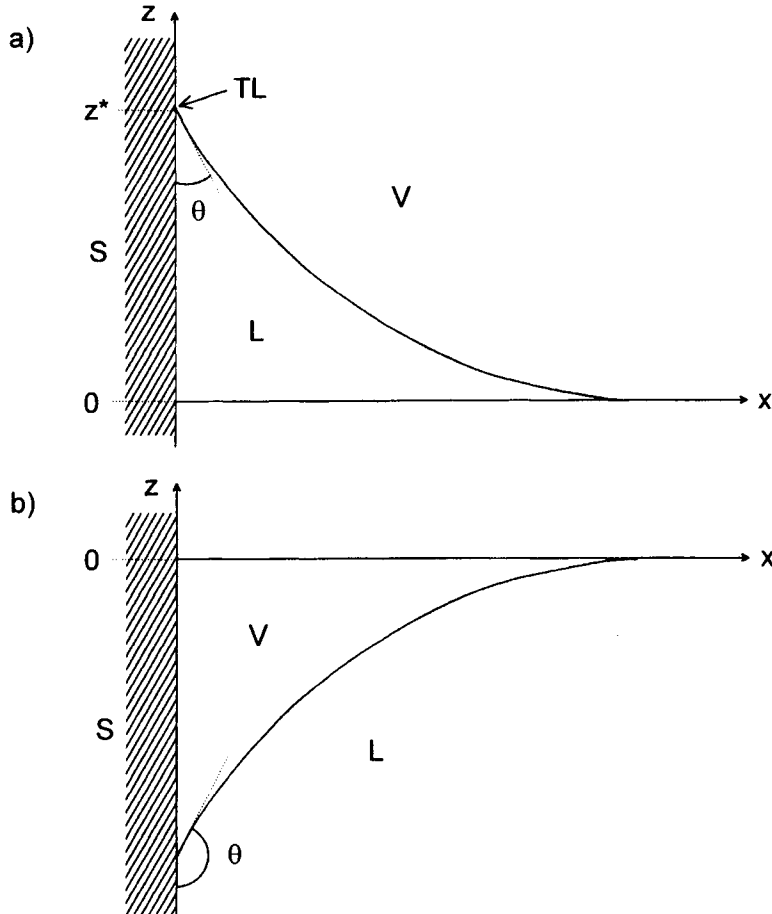
Until now the L/V surface in the vicinity of TL assumed to have a negligible curvature. Hereafter, this assumption will be removed by minimizing the free energy of the whole S/L/V system in the gravitational field, rather than the free energy of the region of radius  $r$  around TL. In this case, the curvature at each point Q of the L/V surface has to satisfy the equation of Laplace (1805) (see Appendix A):

$$P_L^Q - P_V^Q = \sigma_{LV} \left( \frac{1}{R_1} + \frac{1}{R_2} \right) \quad (1.20)$$

where  $P_L^Q$  and  $P_V^Q$  are the pressures on the liquid and vapour sides of the surface and  $R_1$  and  $R_2$  are the principal radii at point Q (Figure 1.8).



**Figure 1.8.** The principal radii of curvature  $R_1$  and  $R_2$  at a point Q on a curved liquid surface.



**Figure 1.9.** Meniscus rise on a vertical wall when  $\theta < 90^\circ$  (a) and depression when  $\theta > 90^\circ$  (b).

Because no analytical solution of the shape of the surface in the gravitational field is available in the sessile drop configuration (see Section 3.1.3.2), we prefer to consider a meniscus formed on a vertical plate (Figure 1.9) as in the papers of McNutt and Andes (1959) and Neumann and Good (1972). The calculations given below come from Neumann and Good (1972) but the conclusions are also valid for a tilted plate, as shown by Eick et al. (1975). The geometry used is given in Figure 1.9 with the vertical plate and TL perpendicular to the plane of the figure. The total free energy change  $\Delta F$  can be calculated when a liquid surface initially in a horizontal position ( $z^* = 0$ ,  $\theta = 90^\circ$ ) is raised (or depressed) to form a meniscus of height  $z^*$ , corresponding to a contact angle  $\theta$ . Thus, the equilibrium contact angle

can be determined by minimizing  $\Delta F$  as a function of  $z^*$ , or equivalently of the contact angle  $\theta$ .  $\Delta F$  is composed of two terms:  $\Delta F_b$  arising from changes in the potential energy of the bulk phase of the system, and  $\Delta F_s$  resulting from changes in the surface and interfacial energies of the system. The last term takes into account both the difference between a S/V surface and a S/L interface ( $\Delta F_{s,1}$ ) and the increase of the L/V area ( $\Delta F_{s,2}$ ) during the meniscus formation. Calculations of these terms are given in Appendix B. For a triple line of unit length, the total free energy change  $\Delta F$  is (Neumann and Good 1972):

$$\frac{\Delta F}{\sigma_{LV}l_c} = \mp A(1 - \sin \theta)^{1/2} + [2^{1/2} - (1 + \sin \theta)^{1/2}] + \frac{1}{3}[(2 - \sin \theta)(1 + \sin \theta)^{1/2} - 2^{1/2}] \quad (1.21)$$

where the minus sign before  $A$  corresponds to  $0 \leq \theta \leq 90^\circ$  and the plus sign to  $90 \leq \theta \leq 180^\circ$ . In equation (1.21),  $A$  is a parameter that depends on the three interfacial energies of the system:

$$A = \frac{\sigma_{SV} - \sigma_{SL}}{\sigma_{LV}} \quad (1.22)$$

For any rise  $z^*$  of the meniscus,  $z^*$  and  $\theta$  are related by:

$$z^* = \pm \left( \frac{2\sigma_{LV}}{\rho g} \right)^{1/2} (1 - \sin \theta)^{1/2} = \pm l_c (1 - \sin \theta)^{1/2} \quad (1.23)$$

where a positive value of  $z^*$  corresponds to  $0 \leq \theta \leq 90^\circ$  and a negative value to  $90 \leq \theta \leq 180^\circ$ . The quantity  $l_c = (2\sigma_{LV}/(\rho g))^{1/2}$ , in which  $\rho$  is the liquid density and  $g$  the acceleration due to gravity, is often called “capillary length” and is simply the maximum rise of a liquid on a perfectly wetted vertical plate. (Note that in some papers the capillary length is defined without the factor  $2^{1/2}$ ). The equilibrium contact angle of the system is obtained by setting  $d\Delta F/d\theta = 0$ , so that:

$$\pm A(1 - \sin \theta)^{-1/2} - (1 + \sin \theta)^{1/2} = 0 \quad (1.24)$$

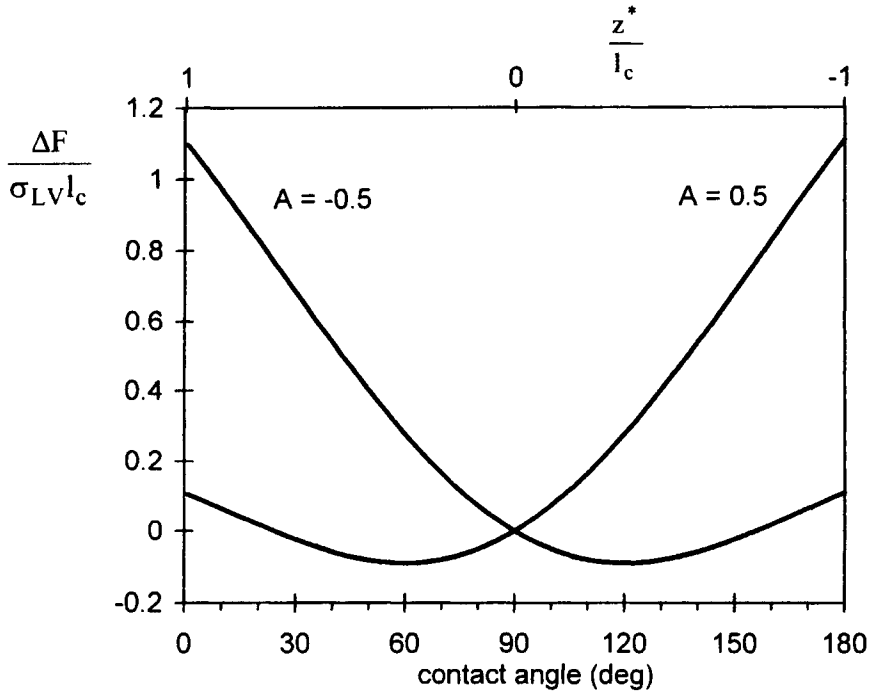
For  $0 \leq \theta \leq 90^\circ$ , equation (1.24) yields only the solution:

$$\cos \theta_{\text{eq}} = A = \frac{\sigma_{\text{SV}} - \sigma_{\text{SL}}}{\sigma_{\text{LV}}} > 0 \quad (1.25)$$

which is identical to the Young equation (1.16), i.e.  $\theta_{\text{eq}} = \theta_Y$ . For  $90^\circ \leq \theta \leq 180^\circ$ , equation (1.24) again yields one solution:

$$\cos \theta_{\text{eq}} = A = \frac{\sigma_{\text{SV}} - \sigma_{\text{SL}}}{\sigma_{\text{LV}}} < 0 \quad (1.26)$$

The contact angle satisfying equation (1.25) or (1.26) corresponds to a minimum of the total free energy of the system  $\Delta F(\theta)$ . Examples are given on Figure 1.10 for  $A = 0.5$  and  $A = -0.5$  using equation (1.21) written with the minus sign for  $0^\circ \leq \theta \leq 90^\circ$  and with the plus sign for  $90^\circ \leq \theta \leq 180^\circ$ . The minima of the curves are located at  $\theta = 60^\circ$  and  $\theta = 120^\circ$ , values which correspond to  $\arccos A$ .



**Figure 1.10.** Reduced total free energy of a meniscus per unit length of triple line as a function of its height  $z^*$  or the corresponding contact angle for two values of the parameter  $A = (\sigma_{\text{SV}} - \sigma_{\text{SL}})/\sigma_{\text{LV}}$ . The minima of these curves correspond to the equilibrium contact angle of the system.

Figure 1.10 demonstrates that the equilibrium contact angle depends only on the value of  $A$ . Variations in the values of  $\sigma_{LV}$ ,  $\rho$  or  $g$  (such as might be encountered in spacelab experiments) for a constant value of  $A$  will merely displace the  $\Delta F(\theta)$  curve perpendicularly to the  $\theta$ -axis, without changing the position of the minimum value of  $\theta$ .

The above calculations show that the Young equation is valid in the presence of a gravitational field for the configuration of a vertical plate. This is also true for other configurations in which one curvature of the L/V surface is zero, as for a cylindrical “drop” on a horizontal plane (Marmur 1996). The validity of the Young equation in the classical configuration of an axisymmetric sessile drop has been discussed by various authors, for instance Johnson (1959), Collins and Cooke (1959) and more recently Garandet et al. (1998). In the last paper, a clear proof of the validity of the Young equation was achieved by minimizing the free energy of the system, including a gravitational term. Moreover, it was shown that the Young equation holds also when the fluid is subject to other kinds of body forces, e.g. dielectric or magnetic forces. Only localised “surface” forces such as those induced by Foucault’s currents in high frequency heating can, in principle, modify the contact angle.

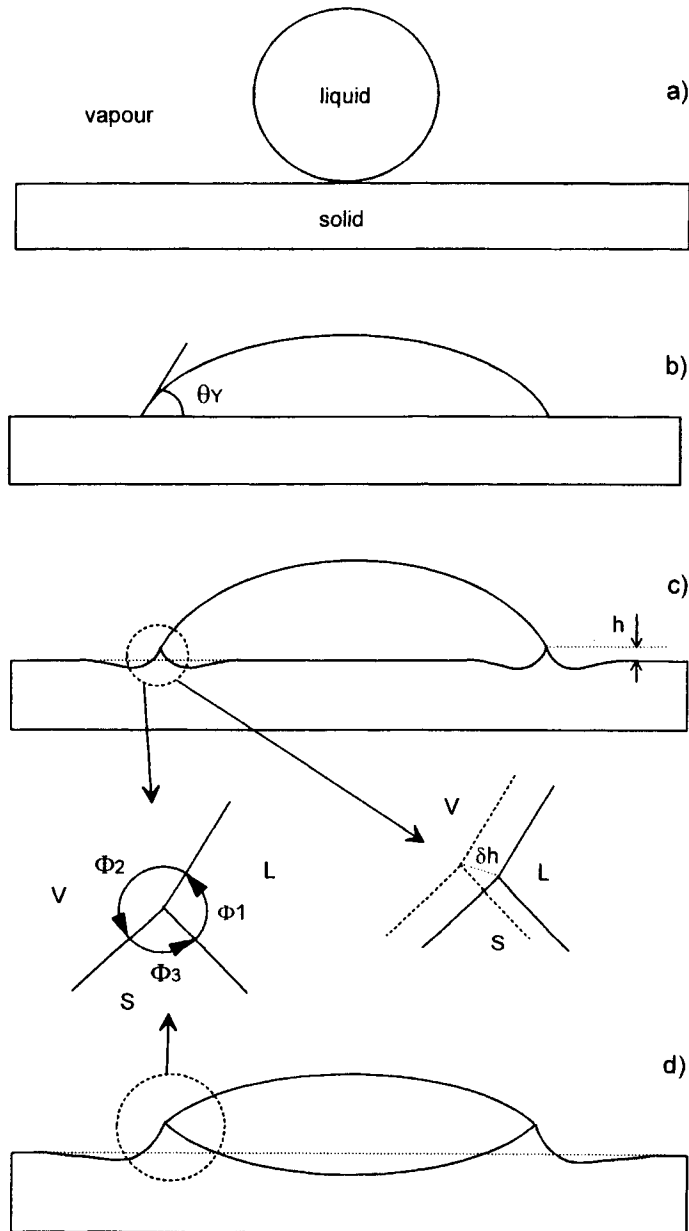
#### 1.2.4 Metastable and stable equilibrium contact angles

The Young equation can be derived from minimization of the free energy of the system carried out by considering only displacements of the triple line parallel to an S/V surface assumed to be undeformable (Figure 1.11.b). Therefore,  $\theta_Y$  corresponds to a metastable equilibrium configuration. Hereafter, deformation of the solid close to TL will be considered and the local stable equilibrium shown in Figure 1.11.c will be analysed. Equations describing the stable equilibrium in terms of three dihedral angles  $\Phi_1$ ,  $\Phi_2$  and  $\Phi_3$  can be obtained by regarding the displacement  $\delta h$  of TL (Figure 1.11.c) as two elementary displacements, one perpendicular to the intersection of the L/V surface in the figure plane ( $\delta h_1$ ) and one perpendicular to the intersection of the S/L interface in the figure plane ( $\delta h_2$ ). Assuming isotropic S/V and S/L surface and interfacial energies, the interfacial free energy change for the first displacement is (Figure 1.12):

$$\delta F_s = \sigma_{SV} \sin(\Phi_2) \delta h_1 - \sigma_{SL} \sin(\Phi_1) \delta h_1 \quad (1.27)$$

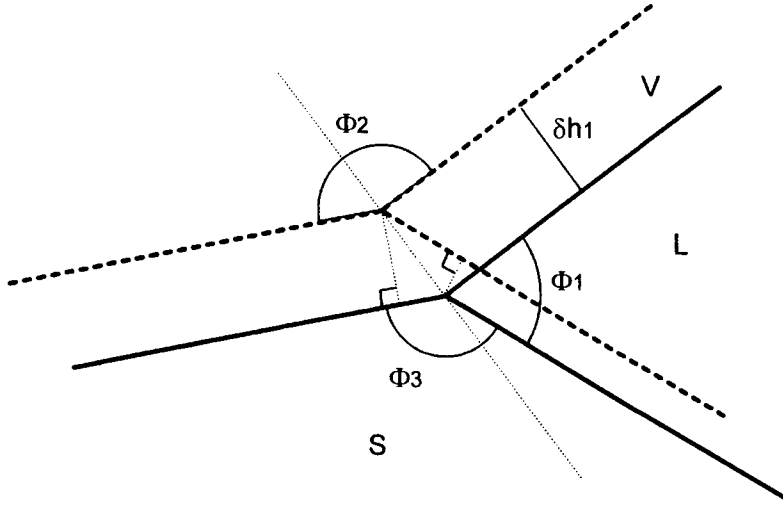
The equilibrium condition  $d(\delta F_s)/d(\delta h_1) = 0$  leads to:

$$\sigma_{SV} \sin \Phi_2 = \sigma_{SL} \sin \Phi_1 \quad (1.28)$$



**Figure 1.11.** Metastable (b) and stable (c) equilibrium angles at a solid/liquid/vapour junction obtained after spreading of a liquid droplet (a). In configuration (d), both local equilibrium at the triple line and total equilibrium along the whole solid/liquid interface are attained.





**Figure 1.12.** Displacement of the triple line around its equilibrium position when the solid is deformable. The displacement  $\delta h_1$  is perpendicular to the intersection of the L/V surface in the figure plane and allows derivation of equation (1.28).

Similarly,  $d(\delta F_s)/d(\delta h_2) = 0$  yields:

$$\sigma_{SV} \sin \Phi_3 = \sigma_{LV} \sin \Phi_1 \quad (1.29)$$

By combining equations (1.28) and (1.29), the relationship first given by Smith (1948) is obtained:

$$\frac{\sigma_{SV}}{\sin \Phi_1} = \frac{\sigma_{SL}}{\sin \Phi_2} = \frac{\sigma_{LV}}{\sin \Phi_3} \quad (1.30)$$

in which  $\Phi_1 + \Phi_2 + \Phi_3 = 360^\circ$ . The configuration described by the Smith equation corresponds to local equilibrium. Total equilibrium requires an unchanging curvature at any point of the S/L interface (Figure 1.11.d), as in the case of a small liquid droplet on the surface of another immiscible liquid.

The actual TL configuration observed after a certain time of contact between the solid and liquid phases depends on the scale of observation and on the relative rates of two processes: (i) the movement of TL over large distances to satisfy the Young equation and (ii) the distortion of TL to satisfy locally the more general Smith equation. The kinetics of the two movements may be very different.

In non-reactive S/L couples and for liquids with a low viscosity, such as molten metals or certain oxide melts at high temperature, the lateral movement of TL is very fast, with spreading times for millimetre size droplets of  $10^{-1}$  second or less (see Section 2.1.1). The movement of TL perpendicular to the initial S/V surface can occur first by elastic deformation of the solid. Remembering that the surface energy  $\sigma_{LV}$  of a liquid is equivalent to the surface tension  $\gamma_{LV}$ , the solid is strained at the triple line, the initial stress being  $\gamma_{LV}\sin\theta$ . The height  $h$  of the deformed region (Figure 1.13.a) is of the order of  $\gamma_{LV}/E$ , where  $E$  is the modulus of elasticity. Taking typical values for high temperature materials  $\gamma_{LV} = 1$  N/m and  $E = 10^{11}$  Pa,  $h$  is a negligible  $10^{-2}$  nm (however, for “soft” or viscoelastic solids,  $h$  can attain several tens of nm (Carré and Shanahan 1995)).

The growth of the “wetting ridge”, to easily measurable dimensions, can take place by mechanisms similar to those occurring during grain-boundary grooving, as described by Mullins (1957, 1960). When a grain boundary of energy  $\sigma_{gb}$  meets a S/L interface (or a S/V surface), a groove is formed with a dihedral angle  $\Phi$  (Figure 1.13.b) which, at equilibrium, is given by:

$$\cos\left(\frac{\Phi}{2}\right) = \frac{\sigma_{gb}}{2\sigma_{SL}} \quad (1.31)$$

Once formed, the groove continues to grow, driven by differences in curvature  $\kappa$  at the S/L interface. These differences result in variations of the chemical potential of the solid,  $\mu$ , according to the Gibbs–Thomson equation:

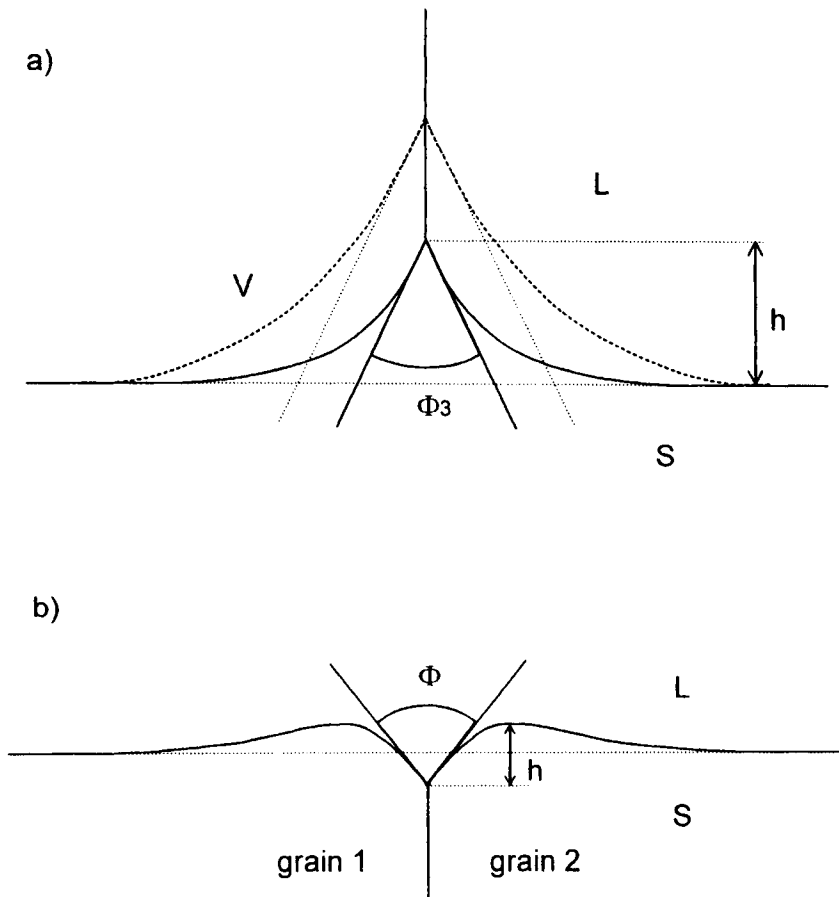
$$d\mu = v_m \sigma_{SL} d\kappa \quad (1.32)$$

where  $v_m$  is the molar volume of the solid. Thus, the S/L interfacial energy  $\sigma_{SL}$  provides a driving force for the transfer of solid atoms from regions of high curvature at the root of the groove to regions of small curvature far from the groove. As a result, although the shape of the groove and the angle  $\Phi$  are constant with time, its linear dimensions, such as its depth  $h$ , increase continuously with time according to a power law:

$$h^n = K t \quad (1.33)$$

where  $n = 3$  when the limiting process is diffusion in bulk solid or liquid (Mullins 1960),  $n = 4$  for interface diffusion and  $n = 2$  for dissolution-precipitation mechanism (or evaporation/condensation in the case of S/V surface) (Mullins 1957). For couples with low or negligible miscibility (for instance with an

equilibrium molar fraction of solid component in the liquid of the order of  $10^{-4}$  or less), the power law (equation (1.33)) leads to very small grooving rates and several hours or tens of hours are needed for groove depths to reach the micron scale (Eustathopoulos 1983).



**Figure 1.13.** Formation of a wetting ridge at the triple line (a) by a mechanism similar to grain-boundary grooving (b).

In the vicinity of a triple line, a deformation of the solid surface can also occur by a mechanism in which the role of the grain boundary is played by the L/V surface (Figure 1.13.a). In this case, the mass transfer will occur from the S/L interface

and S/V surface far from TL to regions close to TL where the curvature is relatively high but negative. Experimental evidence of the formation of wetting ridges, attributed to a mechanism similar to that occurring in grain-boundary grooving, was given by Saiz et al. (1998) for Cu and Ni droplets on  $\text{Al}_2\text{O}_3$  surfaces in Ar. At the end of the spreading process, the droplets were maintained in contact with the substrate for several tens of minutes, allowing the ridge to grow to a size that permitted easy observation. For Cu, a wetting ridge with  $h = 10$  nm was formed after 2 hours at  $1150^\circ\text{C}$  and for Ni  $h = 0.2\ \mu\text{m}$  after 1 hour at  $1500^\circ\text{C}$ .

It is interesting to note that in the past, some authors used the stable TL configuration (Figure 1.11.c) to derive S/L and S/V interfacial and surface energies in nearly immiscible molten metal/solid metal systems by measuring the relevant dihedral angles,  $\sigma_{\text{LV}}$  values being measured independently by other techniques. To obtain deformed regions large enough to permit measurement of the angles, long duration experiments were needed. However, significant evaporation of the drop can occur during such experiments and cause some decrease in the drop volume resulting in instabilities in the position of the triple line and inaccurate measurements.

In liquid/solid systems with a high mutual solubility (as for many metallic systems), calculations show that the size of the deformed area close to the triple line can attain dimensions of about a micron in a minute or so. However, in this case, the equilibrium configuration at the triple line can be masked by the dissolution of the solid in the liquid (Warren et al. 1998) as discussed in Section 2.2.1.

From the above discussion, it appears that wetting of low viscosity liquid drops on solid substrates can occur in two stages. In the first rapid stage, the macroscopic contact angle approaches  $\theta_Y$  (Figure 1.11.b), largely determining the area of the S/L interface and the L/V surface, followed by a much slower process occurring at the vicinity of TL to satisfy the requirements of a stable local equilibrium in accord with the Smith equation (Figure 1.11.c). Much longer times are needed to obtain a total equilibrium i.e., a constant curvature on the whole S/L interface (Figure 1.11.d). This description is also valid for the infiltration of liquids into porous media, as when sintering of metallic or ceramic powders in the presence of molten metals. On melting, infiltration of the liquid will occur rapidly by wetting non-deformed solid particle surfaces and the complete three-phase equilibrium will be developed at the solid particle/liquid/void contact line at a slower rate.

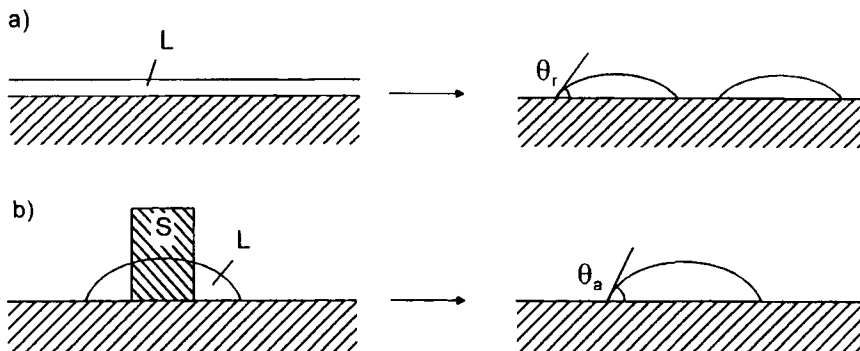
For vitreous solids, such as  $\text{SiO}_2$ , viscosity decreases strongly before reaching the melting point. In this case, the solid meniscus can be formed by viscous flow and the height  $h$  can reach easily measurable sizes in quite short times. For example, wetting of a Ni alloy droplet on a  $\text{SiO}_2$  substrate at  $1743\ \text{K}$  is associated with the

formation in about 20 minutes of an easily observable  $\text{SiO}_2$  meniscus on the drop ( $h = 5$  to  $10\ \mu\text{m}$ ) (Merlin 1992).

### 1.3. NON-IDEAL SOLID SURFACES

Real solid surfaces never satisfy completely the conditions for the Young equation to be valid, namely chemical homogeneity and perfect smoothness. Several phenomena result from this deviation, most importantly:

- *advancing* contact angles  $\theta_a$  measured after spreading of the liquid on the solid are different from *receding* contact angles  $\theta_r$  reached when the liquid retreats, with  $\theta_a > \theta_r$  (Figure 1.14). An hysteresis domain of contact angle is thus defined by the difference  $(\theta_a - \theta_r)$ ;
- even when contact angle measurements are limited to advancing contact angles, the observed  $\theta$  values are very sensitive to the deviation from ideality. This sensitiveness, which is at the origin of the large dispersion of experimental contact angle values of literature for a given liquid/solid system (see Section 3.3), is due to roughness and/or chemical homogeneity defects.



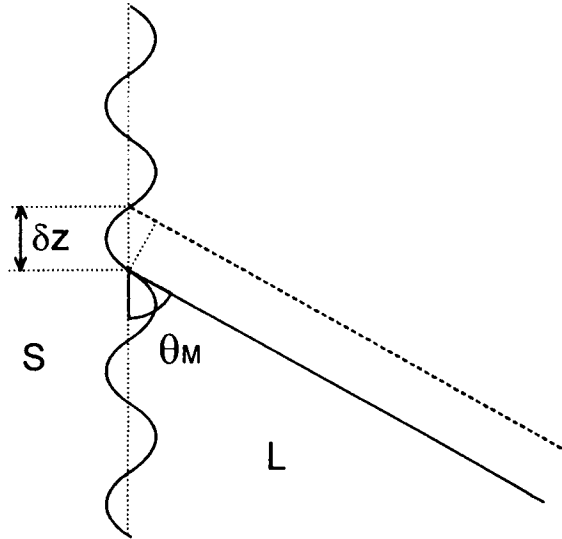
**Figure 1.14.** Contact angle characteristics of rough solid surfaces. (a) Destabilization of a liquid film L on a solid substrate leads to formation of droplets with a receding contact angle  $\theta_r$ . (b) Melting of a small solid sample S produces an advancing contact angle  $\theta_a$ .

Following Neumann and Good (1972) and Eick et al. (1975), the thermodynamic equations of wetting for rough surfaces and for inhomogeneous surfaces can be developed more conveniently by considering a vertical plate

partially immersed in a liquid rather than a sessile drop because of the availability in the former case of analytical expressions for the interfacial and potential energies.

### 1.3.1 Rough surfaces

The roughness of solid surfaces affects wetting owing to two different effects: the first is the fact that the actual surface area is increased and the second is pinning of the triple line by sharp edges.



**Figure 1.15.** Small displacement of a triple line on a rough substrate that allows derivation of the Wenzel equation.

**1.3.1.1 Effect of an increased surface area.** If  $s_r$  denotes the ratio of the actual to the planar area ( $s_r > 1$ ) and  $\theta_M$  is the apparent macroscopic contact angle, for a surface with a small asperity wave-length compared with the maximum meniscus height  $z_{\max}^*$  (equation (1.23)), the variation of interfacial free energy  $F_s$  per unit length of TL, resulting from a small displacement  $\delta z$  of TL (Figure 1.15), is:

$$\delta F_s = (\sigma_{SL} - \sigma_{SV})s_r\delta z + \sigma_{LV} \cos(\theta_M)\delta z \quad (1.34)$$

The equilibrium condition  $d(\delta F_s)/d(\delta z) = 0$  leads to the equation of Wenzel (1936):

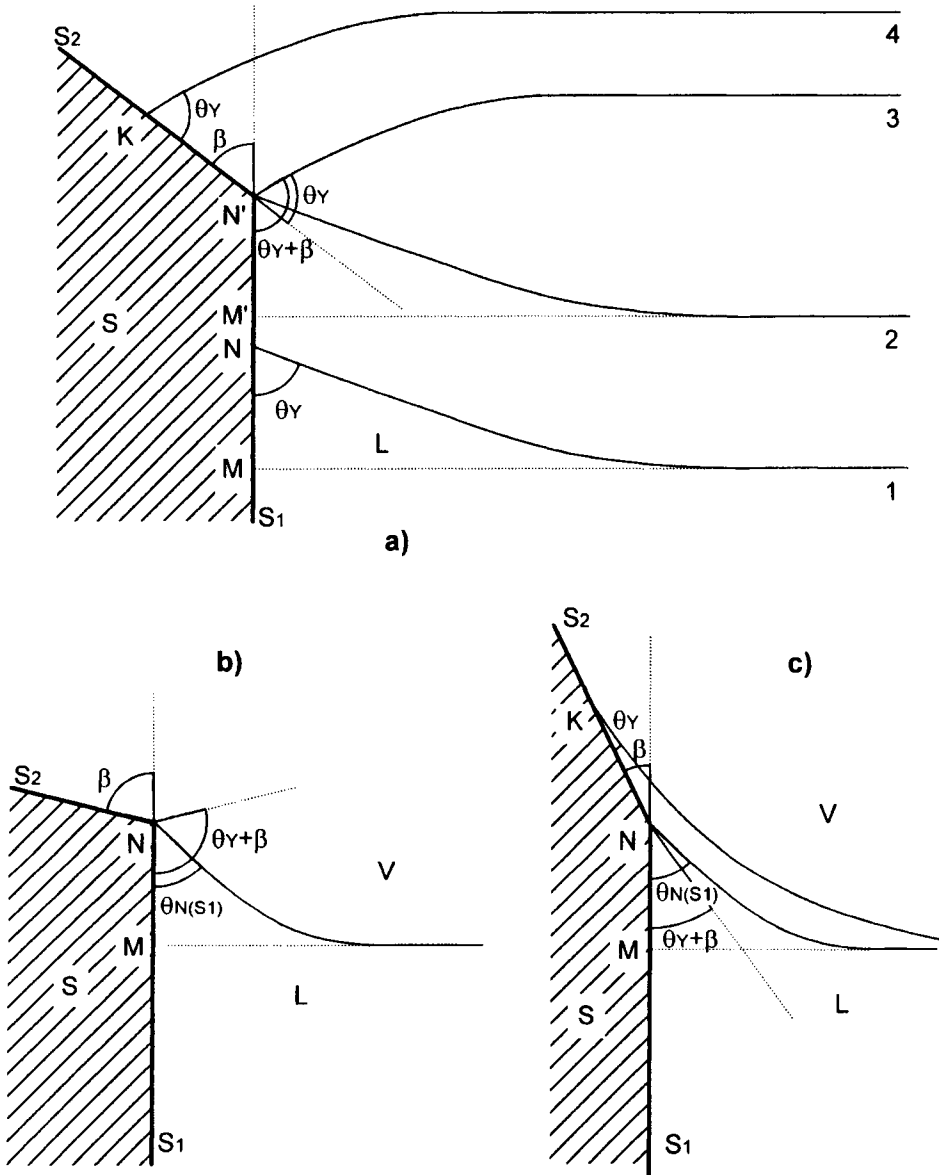
$$\cos \theta_W = s_r \cos \theta_Y \quad (1.35)$$

**1.3.1.2 Effect of sharp edges.** A sharp edge can pin the triple line at positions far from stable equilibrium, i.e., at contact angles markedly different from  $\theta_Y$ . This effect is illustrated schematically in Figure 1.16.a where we consider a solid wall of a crucible consisting of a vertical surface  $S_1$  and another surface  $S_2$  inclined at an angle  $\beta$ . The initial equilibrium configuration of the liquid surface is identified 1 in Figure 1.16.a, corresponding to  $MN = z_{\max}^*$  and to a contact angle at point N on the  $S_1$  surface  $\theta_N(S_1) = \theta_Y$ . Then, if the liquid volume is increased slowly enough for the liquid to retain capillary equilibrium, TL will advance on the  $S_1$  surface and assume configuration 2 where  $M'N' = z_{\max}^*$  and  $\theta_{N'}(S_1) = \theta_Y$ . Thereafter, TL will be pinned at point N' and the macroscopic contact angle on  $S_1$ ,  $\theta_{N'}(S_1)$ , will increase until the liquid surface assumes configuration 3 where  $\theta_{N'}(S_1) = \theta_Y + \beta$  which corresponds to the establishment of the Young contact angle on the  $S_2$  surface i.e.,  $\theta_{N'}(S_2) = \theta_Y$ . Any further increase in the liquid volume will produce a rise of the liquid on the  $S_2$  surface, for example to configuration 4 with  $\theta_K(S_2) = \theta_Y$ . Thus, the liquid can form an infinite number of *advancing* contact angles at point N' on the  $S_1$  surface lying between  $\theta_Y$  and  $\theta_Y + \beta$ . This last value defines the maximum advancing contact angle on  $S_1$ :

$$\theta_a(\max) = \theta_Y + \beta \quad (1.36.a)$$

Consider now that configuration 4 in Figure 1.16.a represents the initial liquid surface and that the liquid volume is slowly decreased. Using similar arguments for the retreat of a liquid on a solid wall, it can be shown that the liquid can form an infinite number of *receding* contact angles at point N' on the  $S_2$  surface lying between  $\theta_Y$  and  $\theta_Y - \beta$ . This last value defines the minimum receding contact angle on  $S_2$ :

$$\theta_r(\min) = \theta_Y - \beta \quad (1.36.b)$$



**Figure 1.16.** Effects of a sharp edge on the contact angle formed by a meniscus advancing on a solid surface. In (a) 1, 2, 3 and 4 denote the successive configurations of the liquid surface when the liquid volume is increased. With a constant volume of liquid, an advancing triple line is either pinned (b) or not (c) by the sharp edge.



Now consider the meniscus formation, on the same solid wall, of a liquid of *constant* volume initially in an horizontal position such that  $MN \ll z_{\max}^*$  i.e., the contact angle at point N on  $S_1$ ,  $\theta_N(S_1)$ , is greater than  $\theta_Y$  (Figures 1.16.b and c). Two cases can be distinguished depending on the value of  $\beta$ . If  $\theta_N(S_1) < \theta_Y + \beta$  (Figure 1.16.b), TL will be blocked at point N. If  $\theta_N(S_1) > \theta_Y + \beta$  (Figure 1.16.c), TL will be able to advance on the  $S_2$  surface until capillary equilibrium is reached ( $\theta_K(S_2) = \theta_Y$ ).

Finally consider a vertical solid wall with one small groove (Figure 1.17) and a constant liquid volume. When TL reaches position 2, in principle it will be blocked by the groove if the inequality  $\theta < \theta_Y + \beta$  is satisfied. In practice, whether TL will be pinned or pass over the groove when it reaches position 2 depends also on the other energies of the system, particularly the vibrational energy of the experimental device, as well as on the size of the groove.

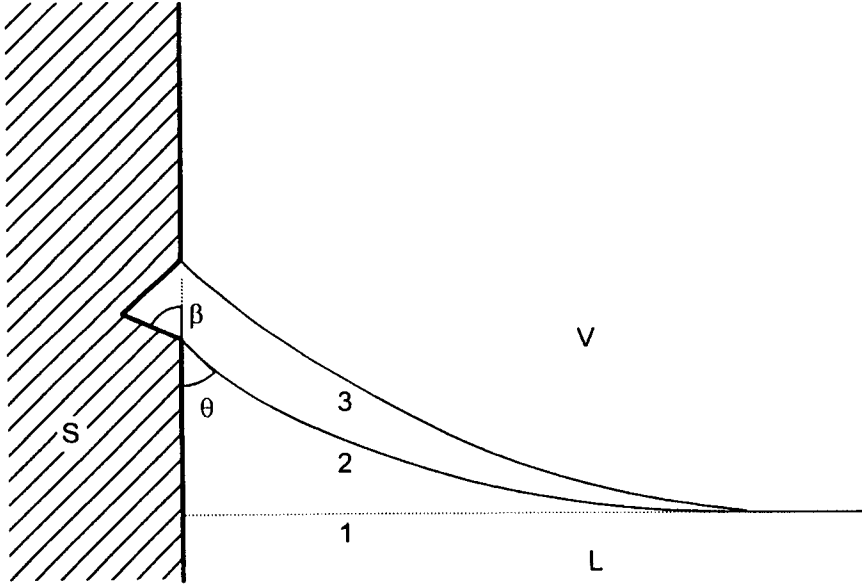
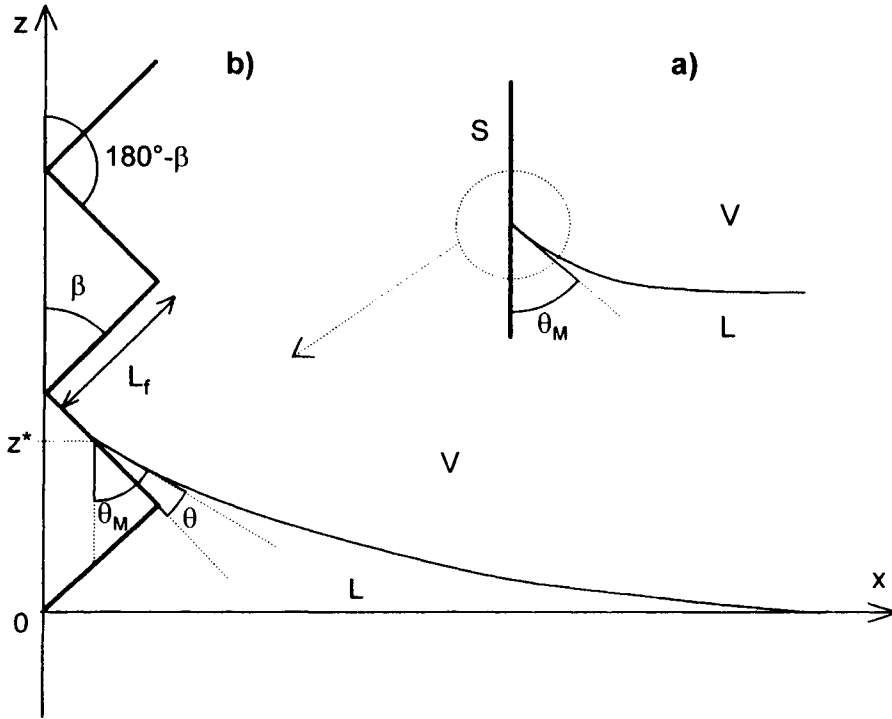


Figure 1.17. Meniscus rise on a vertical wall with a small groove.

**1.3.1.3 Wetting on sawtooth surface.** Now consider the system sketched on Figure 1.18. The solid surface is a series of facets of length  $L_f$  forming alternate angles  $\beta$  and  $(180^\circ - \beta)$  with the  $z$ -axis. In this geometry, the triple line is parallel to the grooves (Figure 1.19). The asperity wave-length ( $2L_f \cos \beta$ ) is assumed to be small

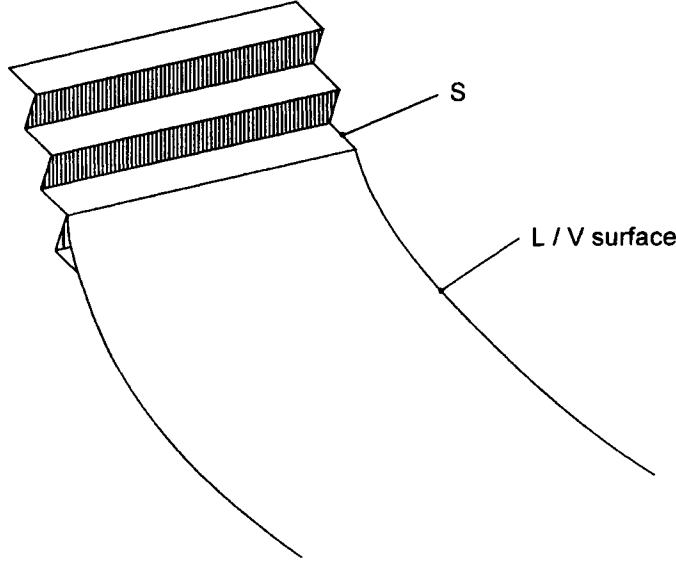
compared to the maximum height of the meniscus  $z_{\max}^*$ . This assumption allows the definition, for each position  $z^*$  of the triple line, of a macroscopic contact angle  $\theta_M$  between the vertical and the tangent to the L/V surface (Figure 1.18.a) and a microscopic contact angle  $\theta$  (Figure 1.18.b). It should be noted that generally only  $\theta_M$  can be measured experimentally. For the geometry of Figure 1.18, ratio  $s_r$  of the real surface to its projection on the  $z$ - $y$  plane is  $(\cos\beta)^{-1}$ .



**Figure 1.18.** Model sawtooth surface used in calculations of the free energy of a meniscus.  $\theta_M$  represents the macroscopic contact angle at each height  $z^*$  of the triple line.

As for the ideal smooth surface (Section 1.2.3 and Appendix B), the free energy change  $\Delta F$  can be calculated as a function of  $\theta_M$ , when a liquid surface initially in a horizontal position ( $z^* = 0$ ,  $\theta_M = 90^\circ$ ) rises to form a meniscus of height  $z^*$  and a contact angle  $\theta_M$ . The interfacial ( $\Delta F_{s,1}$  and  $\Delta F_{s,2}$ ) and potential ( $\Delta F_b$ ) energy contributions need to be modified to take into account the particular geometry of

the rough surface. For instance the  $\Delta F_{s,l}$  term, representing the change from a S/V surface to a S/L interface (equation (B.1) in Appendix B), is now equal to  $s_r z^*(\sigma_{SL} - \sigma_{SV})$ . Results of calculations are given in Figure 1.20 for  $\beta = 10^\circ$  and  $L_f = 100 \mu\text{m}$  (corresponding to a roughness parameter  $s_r = 1.015$ ) and  $\theta_Y = 40^\circ$ .



**Figure 1.19.** Sawtooth surface with grooves parallel to the triple line.

The modelling of Figure 1.20 leads to a number of conclusions:

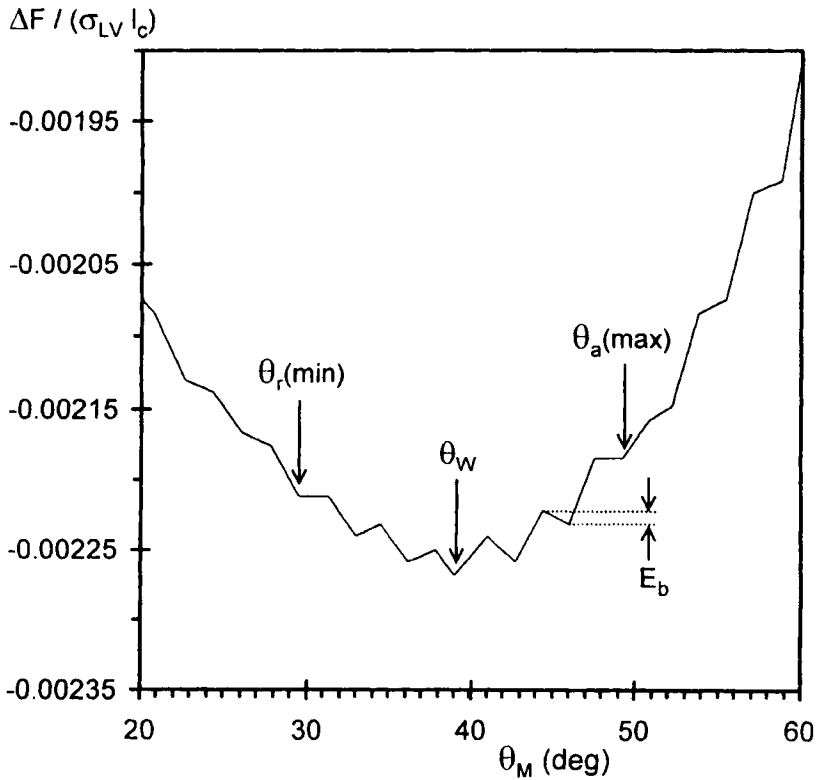
(i) The contact angle at the minimum of the  $\Delta F(\theta_M)$  curve, representing the equilibrium contact angle of a liquid on a rough and undeformable solid surface, is not equal to the Young contact angle  $\theta_Y$  but to  $\theta_W$  (equal to  $39^\circ$  in the calculations for Figure 1.20) as defined by the Wenzel equation (1.35). This equation was the first to take into account roughness effect on contact angles. However, it does not predict the existence of contact angle hysteresis and predicts that roughening the substrate improves wetting for wetting liquids ( $\theta_W < \theta_Y < 90^\circ$ ) but degrades wetting for non-wetting liquids ( $\theta_W > \theta_Y > 90^\circ$ ). In fact, experimental results show that the advancing contact angle increases with roughening not only for non-wetting liquids but also, in some cases, for wetting liquids (Figure 1.21).

(ii) Between the maximum value of the advancing contact angle and the minimum value of the receding contact angle, the  $\Delta F(\theta_M)$  curve exhibits a

succession of free energy minima, which correspond to metastable equilibria (Figure 1.20). The values of these extreme contact angles are given by equations (1.36.a) and (1.36.b), so that for  $\beta = 10^\circ$  and  $\theta_Y = 40^\circ$ , the contact angle hysteresis domain lies between  $30^\circ$  and  $50^\circ$ . In the case of a rough surface with a more realistic geometry and a variable  $\beta$ , for example sinusoidal surface shown in Figure 1.22, equations (1.36) become:

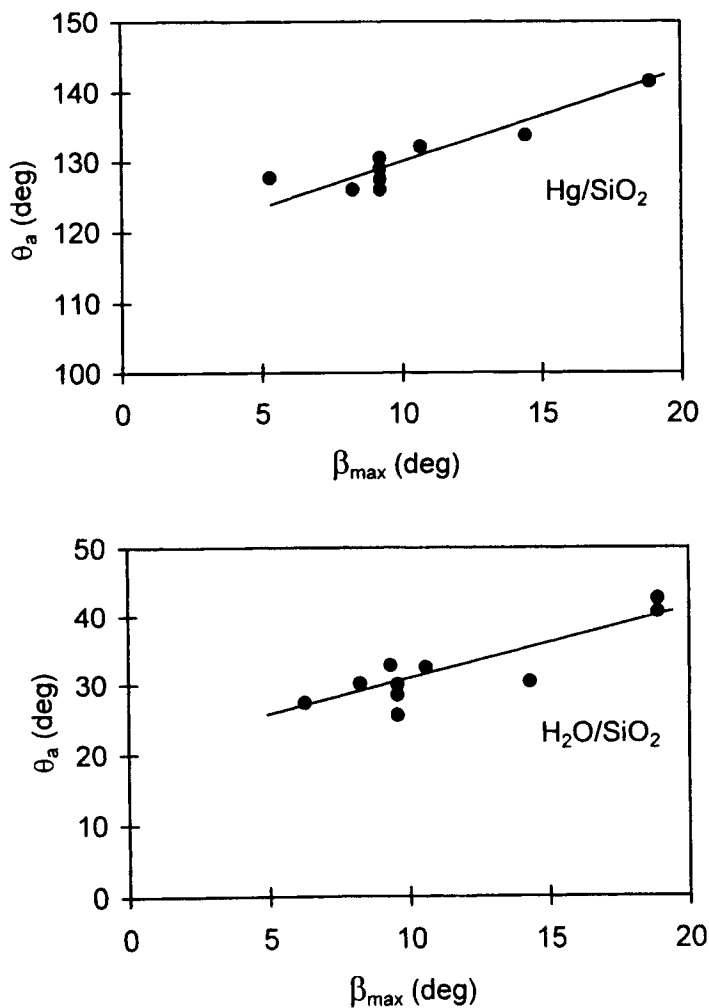
$$\theta_a(\max) = \theta_Y + \beta_{\max} \quad (1.37.a)$$

$$\theta_r(\min) = \theta_Y - \beta_{\max} \quad (1.37.b)$$

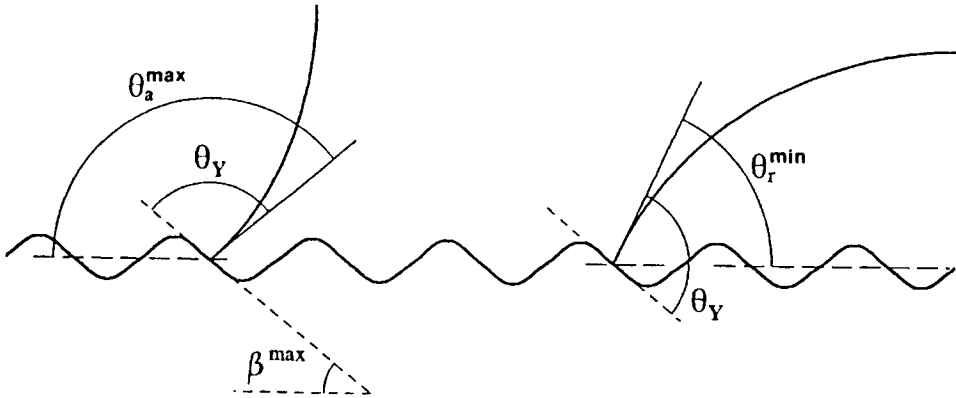


**Figure 1.20.** Reduced free energy per unit length of triple line of a meniscus on the solid surface shown in Figures 1.18 and 1.19 plotted as a function of the macroscopic contact angle. The physical parameters used in the calculation are  $\rho = 7 \times 10^3 \text{ kg.m}^{-3}$ ,  $\sigma_{LV} = 1 \text{ J.m}^{-2}$ ,  $\theta_Y = 40^\circ$ ,  $g = 9.81 \text{ m.s}^{-2}$ ,  $\beta = 10^\circ$  and  $L_f = 100 \text{ }\mu\text{m}$ . Results from (Eustathopoulos and Chatain 1990) [1].

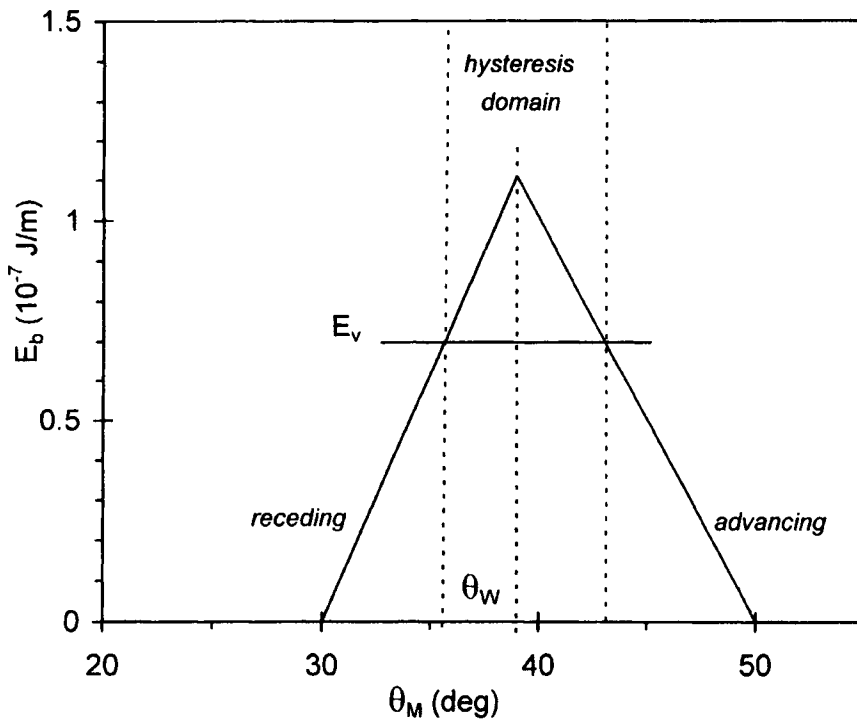
where  $\beta_{\max}$  is the maximum slope of the real surface. Equations (1.37) have been used already by Shuttleworth and Bailey (1948) to interpret wetting hysteresis. These authors considered that surface asperities could pin the triple line in positions not predicted by the Wenzel equation as soon as the *microscopic* contact angle is equal to the Young contact angle, as expressed by equations (1.37) (Figure 1.22).



**Figure 1.21.** Advancing contact angles plotted as a function of the maximum slope of surface asperities for non-wetting (top) and wetting (bottom) systems (Hitchcock et al. 1981) [2].

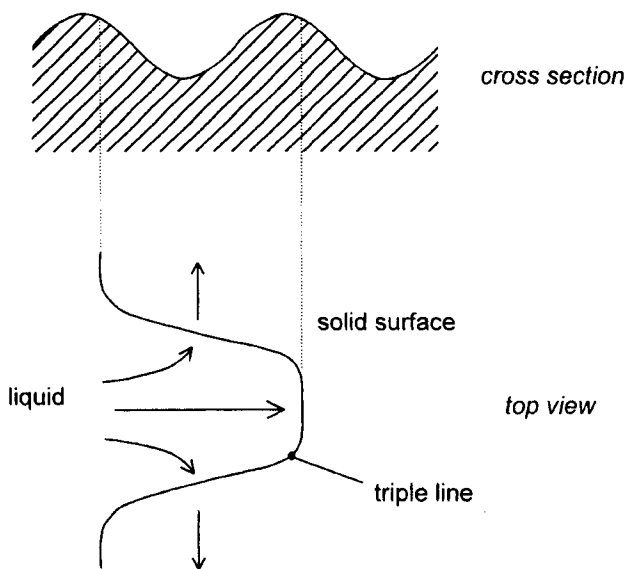


**Figure 1.22.** Identification of the maximum advancing contact angle and minimum receding contact angle on a rough surface.

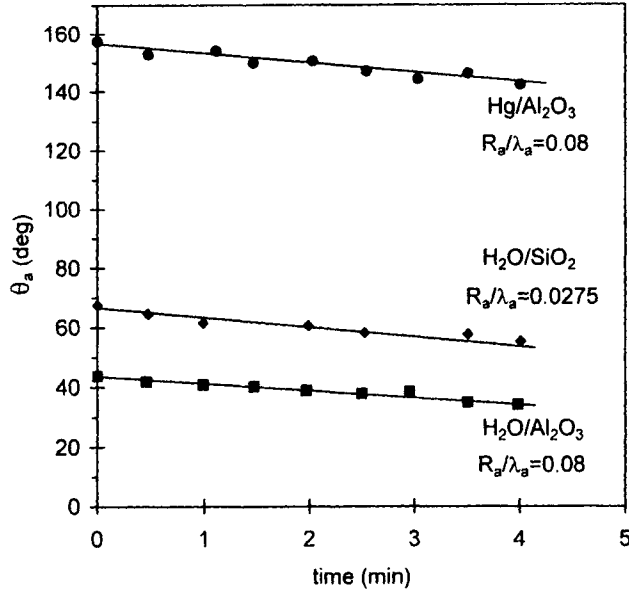


**Figure 1.23.** The energy barrier per unit length of triple line corresponding to the curve of Figure 1.20. From Eustathopoulos and Chatain (1990) [1].

(iii) As several states of metastable equilibrium exist, each of them being separated from neighbouring states by energy barriers  $E_b$  (Figure 1.20), it may be asked what is the metastable position chosen by the triple line in the course of an experiment. The variation of  $E_b$  in the metastable domain (Figure 1.23) shows that  $E_b$  is maximum when  $\theta_M$  tends towards  $\theta_W$ . According to Johnson and Dettre (1964), the triple line will be pinned in a position depending on the relative values of  $E_b$  and the “vibrational energy of the liquid”  $E_v$  (i.e., an energy due to vibrations which occur unavoidably in any experimental device). Thus, the values of advancing and receding contact angles would be determined by the condition  $E_b = E_v$  (Figure 1.23). In the model of Johnson and Dettre, the whole triple line passes a defect in one move, and  $E_b$  is proportional to the length of TL and the physical size of the barrier. As pointed out by de Gennes (1985), the necessary energy would be very high and such a mechanism is thus not realistic. In fact, only a small part of the triple line needs to cross the defect : once this nucleation stage is realized, the remaining part of the triple line can advance by a lateral movement of the liquid along the valleys (Figure 1.24). In spite of this criticism, the vibrational energy concept of Johnson and Dettre was qualitatively confirmed by sessile drop experiments performed on substrates submitted to vibrations : the contact angle decreases irreversibly as a function of time (Figure 1.25).



**Figure 1.24.** Movement of a triple line over a surface defect by a two step mechanism. According to de Gennes (1985).

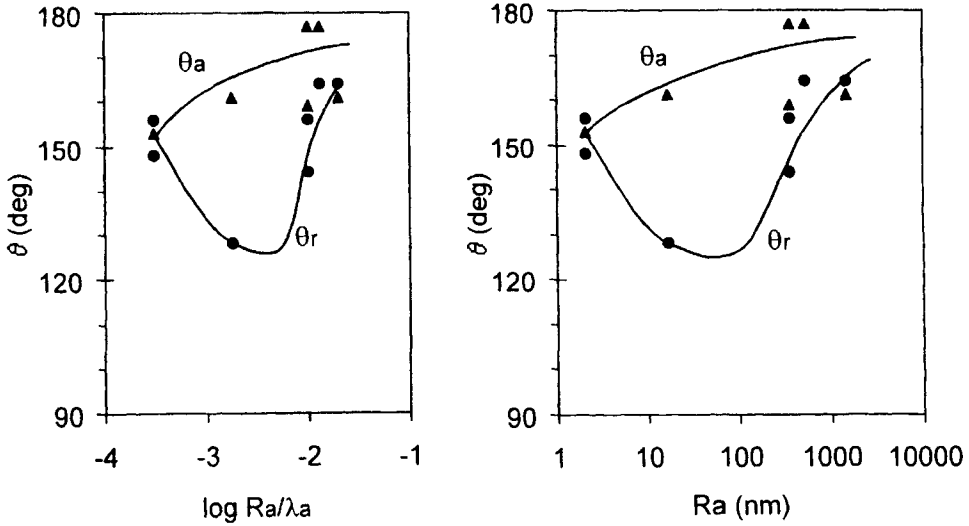


**Figure 1.25.** Effect of 50 kHz vibrations on the advancing contact angles of Hg and  $\text{H}_2\text{O}$  on rough substrates with different values of the ratio  $R_a/\lambda_a$  where  $R_a$  is the average roughness of the surface and  $\lambda_a$  is the average wavelength of the surface features. In practice  $10R_a/\lambda_a \sim \tan\beta$ . From (Hitchcock et al. 1981) [2].

An example of advancing and receding contact angles formed by liquid mercury on sapphire cylinders of variable roughness is given in Figure 1.26. Their roughness was characterized by the average displacement from the mean height of asperities  $R_a$  and the ratio of  $R_a$  to the average wavelength  $\lambda_a$  of asperities, as proposed by Hitchcock et al. (1981).  $R_a$  and  $\lambda_a$  are easily obtained by mechanical or optical surface profilometry techniques and ratio  $R_a/\lambda_a$  relates to the average slope of surface asperities. For very small roughness (a few nanometers), the hysteresis domain ( $\theta_a - \theta_r$ ) is only a few degrees, allowing the Young contact angle to be defined with reasonable precision as  $150^\circ$  for Hg/sapphire. With increasing roughness, the difference ( $\theta_a - \theta_r$ ) at first increases and then decreases, tending towards zero for very rough surfaces. This inversion produced at high roughnesses is due to the fact that a non-wetting liquid cannot infiltrate surface cavities, resulting in the formation of a *composite* interface, i.e. a mixed solid/liquid interface and solid/vapour surface (Figure 1.27.a). A characteristic of such an interface is the disappearance of the energy barriers  $E_b$  (Johnson and Dettre 1964). Indeed, the liquid surface contacts the solid only at a limited number



of points so that no pinning of TL can occur, explaining why the difference ( $\theta_a - \theta_r$ ) tends towards zero. Thus, mercury droplets on ceramic surfaces are very mobile. Indeed, owing to the poor wetting by mercury and the formation of a composite interface, droplets are never pinned and move easily.



**Figure 1.26.** Advancing and receding contact angles in the Hg/Al<sub>2</sub>O<sub>3</sub> system measured by the immersion-emersion technique as a function of substrate roughness. Data from work reported in (De Jonghe et al. 1990) [3].

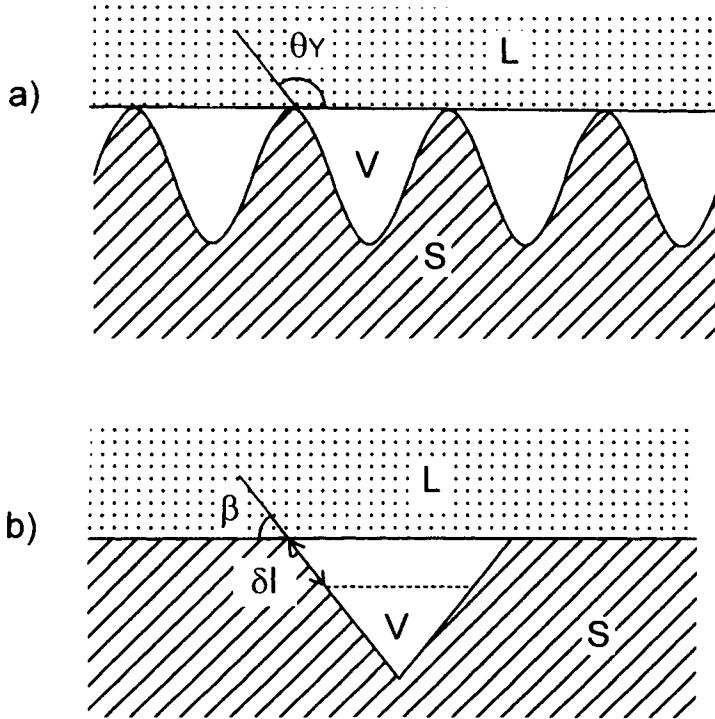
To establish the condition for the transition from an S/L to composite interfaces, consider a liquid surface infiltrating a model triangular groove (Figure 1.27.b). The interfacial free energy change relative to a displacement  $\delta l$  along the groove wall is:

$$\delta F_s = -2\sigma_{LV} \cos(\beta)\delta l + 2(\sigma_{SL} - \sigma_{SV})\delta l \quad (1.38)$$

Setting  $d(\delta F_s)/d(\delta l) = 0$  and recalling that  $(\sigma_{SV} - \sigma_{SL})/\sigma_{LV} = \cos \theta_Y$ , one gets  $\cos \beta = -\cos \theta_Y$ , that is:

$$\beta^* = 180^\circ - \theta_Y \quad (1.39)$$

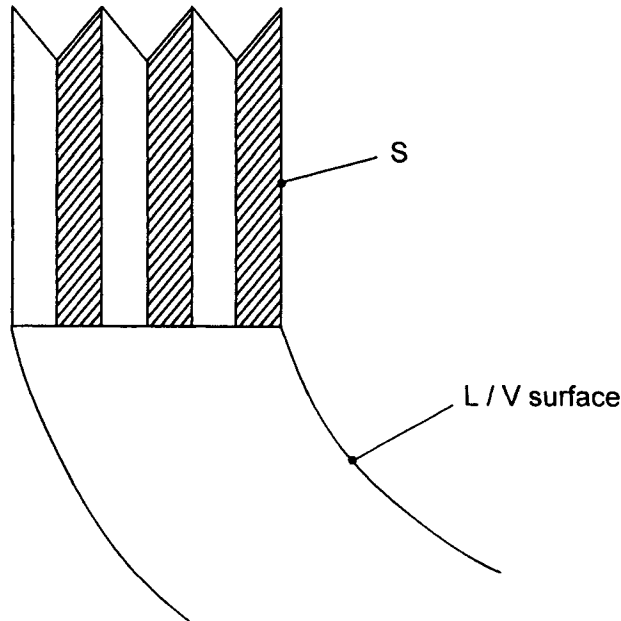
For any cavity with a  $\beta$  value higher than  $\beta^*$ ,  $d(\delta F_s)/d(\delta l)$  will be positive whatever the value of  $l$ , so the cavity will not be infiltrated by the liquid. Equation (1.39) shows that composite interfaces can be produced only for non-wetting liquids and very rough surfaces.



**Figure 1.27.** (a) Formation of a composite interface in the case of a non-wetting system. (b) Model triangular groove used in the calculation of the critical angle  $\beta^*$ .

Energy barriers to the movement of TL and contact angle hysteresis are predicted to exist only for grooves parallel to TL. When grooves are perpendicular to TL (Figure 1.28), no such barriers exist and the macroscopic contact angle is equal to the Wenzel contact angle given by equation (1.35) (Johnson and Dettre 1964). For wetting liquids, this equation predicts that roughness always promotes wetting and it is possible to obtain apparently perfect wetting ( $\theta_w = 0^\circ$ ) when the roughness parameter  $s_r$  is higher than  $(\cos\theta_Y)^{-1}$ . In this case, grooves act as open capillaries to reinforce wetting. This effect of surface texture is used for practical

purposes, for instance for the recycling of liquids in heat exchangers using liquid metals.



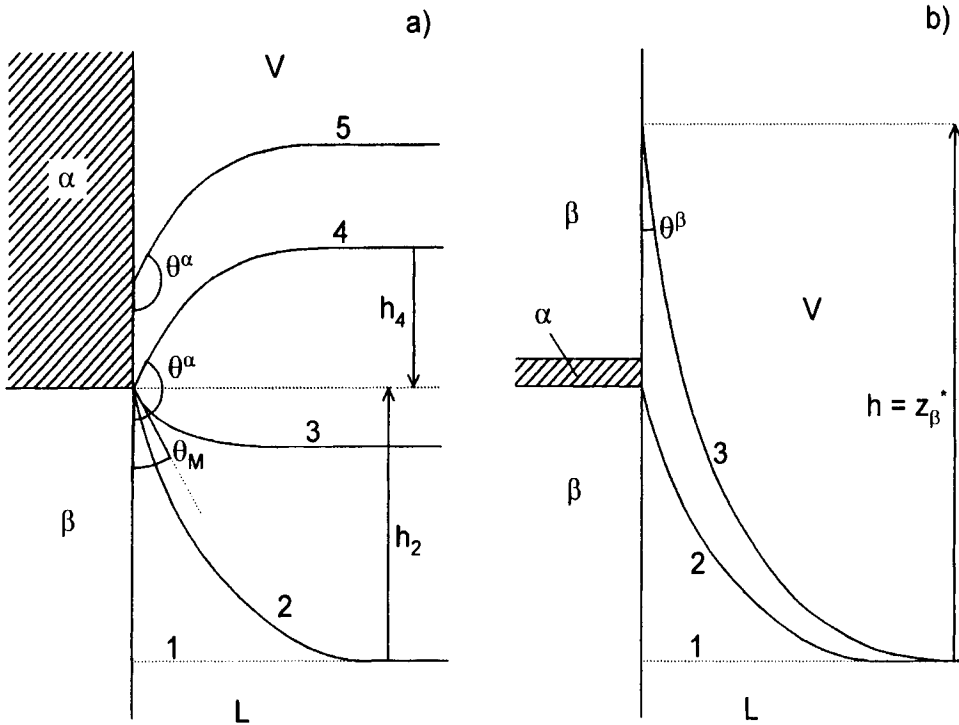
**Figure 1.28.** Sawtooth surface with grooves perpendicular to the triple line.

### 1.3.2 Heterogeneous surfaces

Many materials of practical interest are multi-phase solids with heterogeneous surfaces that can be either regular (orientated eutectics, unidirectional composites, etc) or random (“hard” alloys processed by liquid phase sintering, or alloys strengthened by precipitation, etc).

Consider a vertical solid wall of a crucible consisted of two macroscopic phases  $\alpha$  and  $\beta$  separated by a plane intersecting the solid wall by an horizontal straight line (Figure 1.29.a). The intrinsic contact angles on the two phases are such that  $\theta^\alpha > \theta^\beta$ , and for the sake of simplicity  $\theta^\alpha > 90^\circ$  and  $\theta^\beta < 90^\circ$ . Moreover, we assume that the level of liquid in the crucible far from the wall is such that  $h_2 \ll z_\beta^*$ , where  $z_\beta^*$  is the maximum meniscus height on the  $\beta$  phase i.e.,  $z_\beta^*$  would be the meniscus rise on a homogeneous vertical plate of  $\beta$  (equation (1.23)). During

meniscus rise, when TL reaches the line of separation from  $\beta$  to  $\alpha$ , it will be pinned at this position by the non-wetted  $\alpha$  phase (configuration 2 in Figure 1.29.a). When the volume of the liquid in the crucible is increased and configuration 3 is assumed, TL does not move and the macroscopic contact angle  $\theta_M$  takes a value such that  $\theta^\beta < \theta_M < \theta^\alpha$ . This value of  $\theta_M$  does not satisfy the condition of capillary equilibrium but can be deduced from the geometry of the system and the quantity of liquid. A further increase in the liquid volume, to produce a surface contour shown as configuration 4 such that  $h_4 = z_\alpha^*$  (where  $z_\alpha^*$  is the capillary depression on the  $\alpha$  phase), causes  $\theta_M$  to equal the equilibrium contact angle  $\theta^\alpha$ , so that capillary equilibrium is established at TL on the  $\alpha$  surface. If the liquid volume is increased again, TL will move up (configuration 5 in Figure 1.29.a) while  $\theta_M$  will remain equal to  $\theta^\alpha$ .



**Figure 1.29.** (a) Successive configurations of a meniscus on a vertical solid surface consisting of two macroscopic phases when the liquid volume is increased. (b) Effect of a small chemical heterogeneity on the advance of such a meniscus.

Now consider the same system where the vertical solid wall is a  $\beta$  phase with one narrow  $\alpha$  strip (Figure 1.29.b). When TL assumes its position in configuration 2, it may be blocked by the  $\alpha$  strip, depending on the strip width and the vibrational energy of the system. If this energy is high enough, TL will overcome the barrier and for this particular geometry, the final contact angle will be equal to  $\theta^\beta$ .

Consider now the case of a composite solid consisting of alternate strips of  $\alpha$  and  $\beta$  phases, with contact angles  $\theta^\alpha$  and  $\theta^\beta$ , such that the surface area fractions are  $f^\alpha$  and  $f^\beta$ . The width of the strips is assumed small compared to the capillary length, so that the macroscopic TL is a straight line which is either perpendicular (Figure 1.30.a) or parallel (Figure 1.30.b) to the strips. For the first situation, as for a rough surface with grooves perpendicular to TL (Figure 1.28), it has been shown that there are no metastable states and, as a consequence, no hysteresis of contact angle (Johnson and Dettre 1969, Neumann and Good 1972). The macroscopic contact angle that would be observed at equilibrium can be derived by calculating the variation of interfacial free energy  $F_s$  of the system per unit length of TL caused by a small displacement  $\delta z$  of TL (Figure 1.30.a):

$$\delta F_s = (\sigma_{\alpha L} - \sigma_{\alpha V})f^\alpha \delta z + (\sigma_{\beta L} - \sigma_{\beta V})f^\beta \delta z + \sigma_{LV} \cos(\theta_M) \delta z \quad (1.40)$$

When  $d(\delta F_s)/d(\delta z) = 0$ ,  $\theta_M$  equals the equilibrium contact angle  $\theta_C$  given by:

$$\cos \theta_C = f^\alpha \cos \theta^\alpha + (1 - f^\alpha) \cos \theta^\beta \quad (1.41)$$

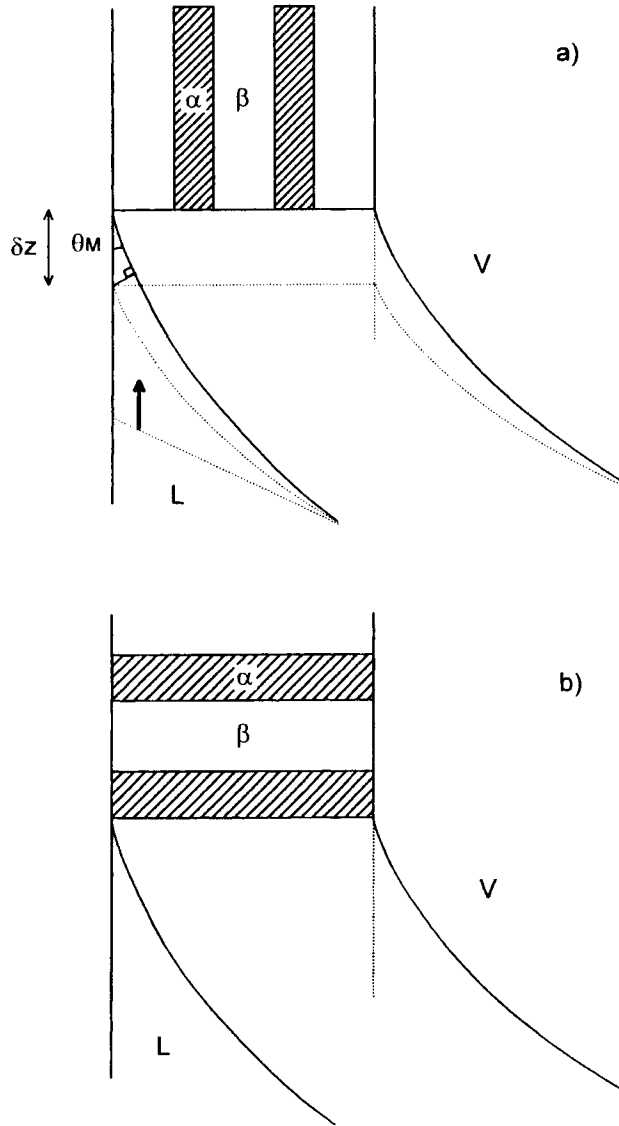
where the subscript C refers to Cassie (1948) who first proposed this equation. This equation, which is an analogue of the Wenzel equation for rough surfaces, gives the stable equilibrium contact angle for any heterogeneous surface.

When TL is parallel to the strips, situation analogous to a rough surface with grooves parallel to TL (Figure 1.19), free energy change calculations (Johnson and Dettre 1969, Neumann and Good 1972) indicate the existence of metastable states separated by energy barriers for any position of TL corresponding to a macroscopic contact angle  $\theta_M$  between  $\theta^\alpha$  and  $\theta^\beta$ . Consequently, the maximum advancing and minimum receding contact angles are given by the equations:

$$\theta_a(\max) = \theta^\alpha \quad (1.42.a)$$

$$\theta_r(\min) = \theta^\beta \quad (1.42.b)$$

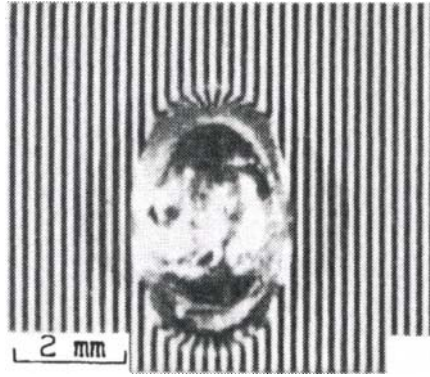
which are analogous to those of Shuttleworth and Bailey for rough surfaces (see Appendix C).



**Figure 1.30.** Composite solid consisting of alternate strips perpendicular (a) and parallel (b) to the triple line.

Wetting experiments with liquid tin on heterogeneous surfaces composed of oxide glass ceramic ( $\alpha$ ) and molybdenum ( $\beta$ ) with  $\theta^\alpha = 125^\circ$  and  $\theta^\beta = 18^\circ$  were performed using the sessile drop technique (Voitovich 1992, Naidich et al. 1995).

The photograph in Figure 1.31 of a tin drop on a striped surface shows that anisotropic wetting occurs preferentially parallel to the strips. For a strip width of 100  $\mu\text{m}$ , the experimental contact angle measured in the direction where TL is perpendicular to the strips was  $80^\circ$ , in good agreement with the  $79^\circ$  predicted by the Cassie equation (1.41). For the direction where TL is parallel to the strips, the experimental advancing contact angle is  $120^\circ$ , close to the maximum value of  $125^\circ$  given by equation (1.42.a). This result can be explained by the large strip width but testifies also to a low vibration level in the experimental device.



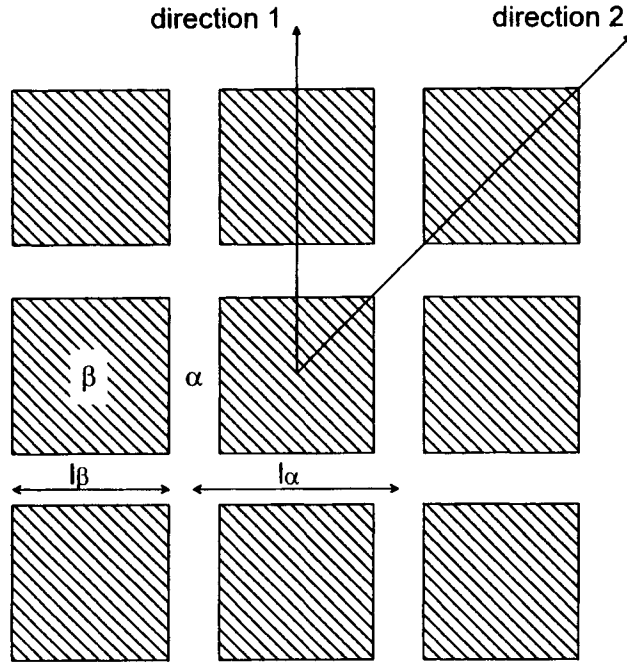
**Figure 1.31.** Tin drop on a striped surface consisted of non-wetted (oxide glass) and wetted (molybdenum) strips. Reprinted from (Voitovich 1992) with kind permission of the author.

As a general rule, metastable states are predicted for patched surfaces. For such surfaces, Horsthemke and Schröder (1981) proposed the following expressions for advancing and receding contact angles:

$$\cos \theta_a = f_{\max}^x \cos \theta^x + (1 - f_{\max}^x) \cos \theta^\beta \quad (1.43.a)$$

$$\cos \theta_r = f_{\min}^x \cos \theta^x + (1 - f_{\min}^x) \cos \theta^\beta \quad (1.43.b)$$

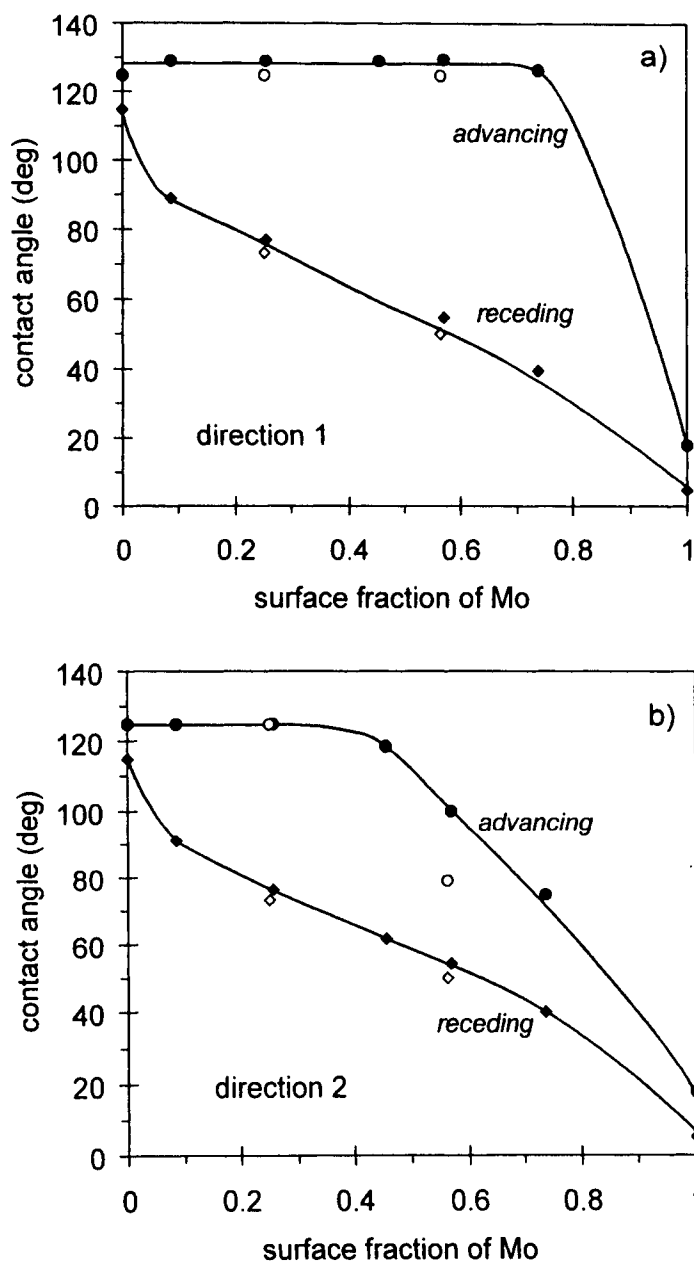
where  $f_{\max}^x$  and  $f_{\min}^x$  are the maximum and minimum surface fractions of the least wetted  $\alpha$  component in regions adjacent to TL, which is assumed to be a straight line. In the extreme case of a strip surface, equations (1.43) reduce to the Cassie equation (1.41) for TL perpendicular to the strips (Figure 1.30.a), and to equations (1.42) for TL parallel to the strips (Figure 1.30.b).



**Figure 1.32.** Patched surface with  $\beta$  surface fraction  $f^\beta = 0.5625$  ( $l_\beta/l_\alpha = 0.75$ ). In the experiments of Naidich et al. (1995) (see results on Figure 1.33), the continuous  $\alpha$  matrix was an oxide glass ceramic ( $\theta^\alpha = 125^\circ$ ) and the  $\beta$  squares were Molybdenum ( $\theta^\beta = 18^\circ$ ).

Experimental determinations of wetting hysteresis on patched surfaces have been made by De Jonghe and Chatain (1995) and Naidich et al. (1995). These last authors performed wetting experiments with liquid tin on surfaces composed of wettable  $\beta$  square patches (molybdenum) dispersed in a continuous  $\alpha$  matrix (oxide glass ceramic). Such a surface is shown in Figure 1.32 with a  $\beta$  surface fraction,  $f^\beta$ , of 0.562. The experimental contact angle hysteresis is determined as a function of  $f^\beta$  for direction 1 (Figure 1.33.a) parallel to the sides of the patches, and direction 2 (Figure 1.33.b) diagonally across the patches. Theoretical values of advancing and receding contact angles for  $f^\beta = 0.25$  and  $f^\beta = 0.562$ , as calculated by equations (1.43), are also presented on Figure 1.33 that are in good agreement with the experimental data. It can be seen that for  $f^\beta = 0.25$ , the contact angle hysteresis is identical in directions 1 and 2, as these two directions have identical values of  $f_{\max}^\alpha$  and  $f_{\min}^\alpha$  (equations (1.43)). For  $f^\beta = 0.562$ , the hysteresis domains are different, so one gets  $f_{\max}^\alpha = 1$ ,  $f_{\min}^\alpha = 0.25$  in direction 1 and  $f_{\max}^\alpha = 0.5$ ,  $f_{\min}^\alpha = 0.25$  in direction 2 (see Figure 1.32).





**Figure 1.33.** Advancing and receding contact angles vs surface fraction of Mo,  $f^{\beta}$ , for a triple line moving along the two directions of the composite surface shown on Figure 1.32. Open symbols : calculated data, full symbols: experimental data from work reported in (Naidich et al. 1995).

To sum up, the effects on static contact angles of the departures from ideality of solid surfaces are qualitatively well understood and some of these effects are used in practice to improve or reduce wettability. Moreover, for simple geometries, a semi-quantitative agreement is obtained between experimental results and theoretical predictions. For surfaces with random roughness, predictions of wetting hysteresis present a great difficulty because the relevant size of defects is not yet well-established.

#### 1.4. DIFFERENT TYPES OF WETTING

In the past, various thermodynamic quantities, resulting usually from linear combinations of interfacial energies, were introduced to characterize the different types of wetting.

##### 1.4.1 Adhesive wetting – The Young-Dupré equation

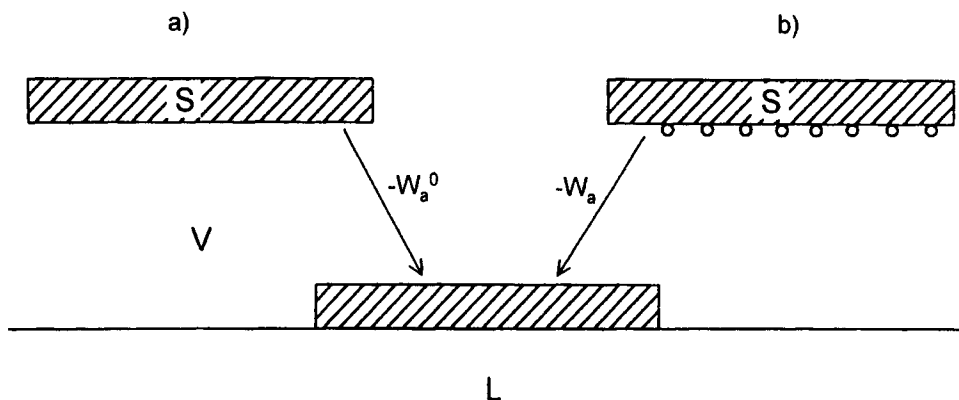
Consider a system consisting of a solid with a cross-section of unit area and a liquid of a different species, immiscible with the solid, held at constant temperature. Both the solid and liquid surfaces are assumed free of any adsorbed species. When the solid surface is lowered towards the liquid until contact is established (Figure 1.34.a), the change of interfacial free energy of the system, or the work gained, is given by:

$$-W_a^0 = \sigma_{SL} - (\sigma_{SV} + \sigma_{LV}) \quad (1.44)$$

where  $W_a^0$  is the work of adhesion of the liquid on the solid. Combining equations (1.44) and (1.16), the following fundamental equation of wetting, known as the Young-Dupré equation (Dupré 1869), is obtained:

$$\cos \theta = \frac{W_a^0}{\sigma_{LV}} - 1 \quad (1.45)$$

Introducing into equation (1.45) the expressions (1.9) and (1.12) for  $\sigma_{LV}$  and  $W_a^0$  derived from the simple nearest-neighbour model described in Section 1.1, this equation can be re-written as a function of S/L and L/L pair energies:



**Figure 1.34.** Work of adhesion in absence (a) and in the presence (b) of adsorbed vapour.

$$\cos \theta = \frac{\varepsilon_{SL}}{\varepsilon_{LL}/2} - 1 \quad (1.46)$$

Equation (1.46) shows that the contact angle results from the competition of two types of forces: cohesion forces responsible for  $\sigma_{LV}$  ( $= W_c/2$ ) and adhesion forces responsible for  $W_a^0$ . Depending on the strength of S/L and L/L interactions, different contact angles can be obtained (Table 1.1).

**Table 1.1.** Degrees of wetting according to the strength of S/L and L/L interactions.

S/L interactions →	weak	strong
↓ L/L interactions		
weak	wetting ( $0 < \theta < 90^\circ$ )	perfect wetting ( $\theta = 0$ )
strong	no wetting ( $90 \leq \theta \leq 180^\circ$ )	wetting ( $0 < \theta < 90^\circ$ )

As shown in the Table, wetting can be obtained not only in systems featuring strong L/S interactions (ionic, covalent, metallic or some mixture of them), but also in systems featuring weak L/S interactions (for instance van der Waals interactions) provided that L/L interactions are weak too. The nearly immiscible molten Cu/W system ( $\theta = 10^\circ$ , Table 5.2) is a typical example of strong L/L and

S/L interactions, which are both metallic. No wetting is observed in the Cu/Al<sub>2</sub>O<sub>3</sub> system ( $\theta = 128^\circ$ , Table 6.1) which features strong L/L but weak S/L interactions. However, many organic liquids, whose cohesion is due to weak, physical, interactions, wet silica well despite the fact that their S/L interactions are rather weak (Johnson and Dettre 1993).

From the above, it is obvious that good wetting does not necessarily mean a thermodynamically strong interface: good wetting means that the interfacial bond is energetically nearly as strong as the cohesion bond of the liquid itself.

#### 1.4.2 Equilibrium and non-equilibrium work of adhesion – Work of spreading

Adsorption of vapour of a pure liquid on the solid surface was neglected in the previous Section. Although it does not change the general tendencies revealed by Table 1.1, adsorption must be taken into account when considering experimental results of wetting for a particular system, especially when these results are compared with theoretical predictions.

Consider now that some adsorption of liquid vapours on the solid surface occurs (Figure 1.34.b), leading to a reduction of its surface energy by a quantity  $\Delta\sigma_{SV}$  (we will continue to neglect any adsorption of vapours of the solid on the liquid surface). For the sake of clarity, we denote by  $\sigma_{SV}^0$  and  $W_a^0$  the solid surface energy and the work of adhesion *in the absence of adsorption*, while  $\sigma_{SV}$  and  $W_a$  refer to these quantities when adsorption has occurred. Because in a pure solid/pure liquid/vapour system held at constant temperature, the solid surface is in equilibrium with a saturated vapour of the liquid at a partial pressure of  $P_{sat}$ , the equilibrium values of  $\sigma_{SV}$  and  $W_a$  are denoted  $\sigma_{SV}(P_{sat})$  and  $W_a(P_{sat})$ . According to these definitions:

$$\sigma_{SV}^0 = \sigma_{SV}(P_{sat}) + \Delta\sigma_{SV}(P_{sat}) \quad (1.47)$$

$$W_a^0 = W_a(P_{sat}) + \Delta\sigma_{SV}(P_{sat}) = \sigma_{LV}(1 + \cos\theta) + \Delta\sigma_{SV}(P_{sat}) \quad (1.48)$$

with  $\sigma_{SV}(P_{sat}) > 0$ . A typical wetting experiment usually allows measurement of  $\sigma_{LV}$  and  $\theta$ , so that it provides only the value of the *equilibrium* work of adhesion  $W_a(P_{sat}) = \sigma_{LV}(1 + \cos\theta)$ . Note that only the non-equilibrium work of adhesion  $W_a^0$  reflects the interaction energy between the solid and the liquid phases and this can be calculated from theoretical models. For instance, in the nearest-neighbour model, the quantity  $-Zm_1\varepsilon_{SL}/\omega$  in equation (1.12) equals  $W_a^0$  and not  $W_a$ .

At this point, it is useful to introduce the *work of spreading*  $W_s$ , sometimes called the spreading coefficient, which is defined by:

$$W_s(P_{\text{sat}}) = \sigma_{\text{LV}} + \sigma_{\text{SL}} - \sigma_{\text{SV}}(P_{\text{sat}}) = 2\sigma_{\text{LV}} - W_a(P_{\text{sat}}) \quad (1.49)$$

Thus,  $W_s(P_{\text{sat}})$  represents the change in the interfacial energy of the system resulting from the formation on a solid surface of a continuous liquid film with a macroscopic thickness. Taking into account the expressions (1.9) and (1.12) for  $\sigma_{\text{LV}}$  and  $W_a$ , it appears that the conditions for stability of such a film can be discussed using parameters representative of the cohesion energy of the liquid ( $\epsilon_{\text{LL}}$ ) and the adhesion energy of the liquid on the solid ( $\epsilon_{\text{SL}}$ ). Depending on their values, two very different situations can arise (Table 1.2):

(1) If the adhesion energy is higher (in absolute value) than the cohesion energy of the liquid ( $|\epsilon_{\text{SL}}| > |\epsilon_{\text{LL}}|$ ), significant adsorption of liquid atoms on to the solid can occur as a monolayer or multilayer depending on the ratio  $P/P_{\text{sat}}$  and the type of S-L interactions even for  $P \ll P_{\text{sat}}$  (Figure 1.35). Increasing  $P$  causes the growth of a macroscopic film at a negligible supersaturation i.e., without any significant nucleation barrier. This corresponds to the 2D or Frank-van der Merwe growth of thin films (Chernov 1984). In a wetting experiment, the partial pressure of a pure liquid close to the triple line is fixed at  $P_{\text{sat}}$ , implying perfect wetting as expressed by the conditions  $\theta = 0$  and  $\Delta\sigma_{\text{SV}}(P_{\text{sat}}) > 0$ . Although there exists some experimental evidence that these conditions hold for certain metal/metal couples (Chernov 1984), quantitative measurements of  $\Delta\sigma_{\text{SV}}(P_{\text{sat}})$  have been made only for low cohesion energy liquids on various solid substrates. These experiments consisted of determining the adsorption isotherms of a species on a solid substrate for  $0 \leq P \leq P_{\text{sat}}$ , and the energy gained by adsorption (i.e. the quantity  $\Delta\sigma_{\text{SV}}(P_{\text{sat}})$ ) was then deduced by integrating the Gibbs adsorption equation (Defay et al. 1966):

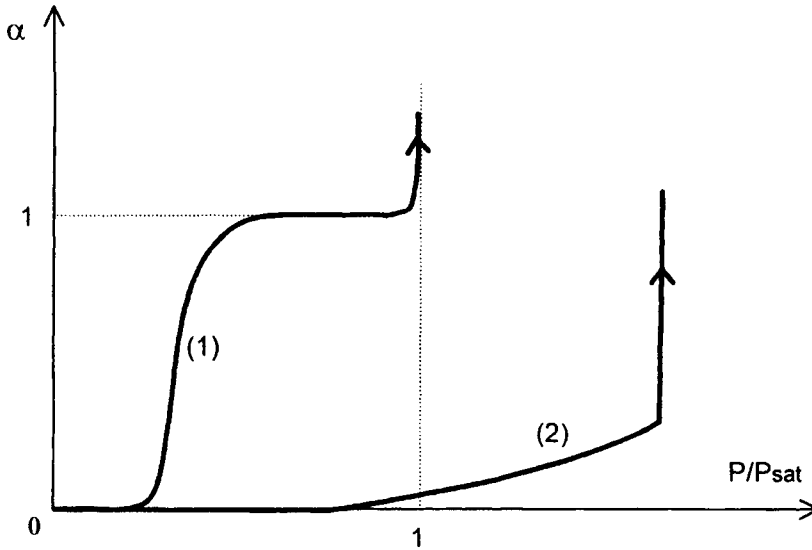
$$\Delta\sigma_{\text{SV}}(P_{\text{sat}}) = RT \int_0^{P_{\text{sat}}} \Gamma d(\ln P) \quad (1.50)$$

between  $P = 0$  and  $P = P_{\text{sat}}$ . In equation (1.50),  $\Gamma$  is the surface excess of the condensate on the solid which, neglecting the density of liquid atoms in the vapour, reduces to the number of moles of adsorbed species per unit surface area (see also Section 6.4.1). Results show that the term  $\Delta\sigma_{\text{SV}}(P_{\text{sat}})$ , also called the *spreading pressure*, can be high and in some cases even higher than the cohesion energy of the liquid,  $2\sigma_{\text{LV}}$ . For instance for water on clean silica,  $\theta = 0$ ,  $W_a = 2\sigma_{\text{LV}} = 145.6 \text{ mJ/m}^2$  and  $\Delta\sigma_{\text{SV}}(P_{\text{sat}}) = 316.4 \text{ mJ/m}^2$  corresponding to  $W_a^0 = 462 \text{ mJ/m}^2$ . Thus, the non-equilibrium adhesion energy for this couple is three times higher than the cohesion energy of water (Johnson and Dettre 1993).

**Table 1.2.** Different types of solid surface in equilibrium with a saturated vapour of a liquid.

Energy conditions	Wetting	Adsorption on the solid	Examples of adsorption isotherms of Figure 1.35	Example
$ \epsilon_{SL}  >  \epsilon_{LL} $	$\theta = 0^\circ$	$\Delta\sigma_{SV}(P_{\text{sat}}) > 0$	1	H <sub>2</sub> O/SiO <sub>2</sub> ( $\theta = 0^\circ$ ) <sup>(a)</sup>
$ \epsilon_{SL}  \ll  \epsilon_{LL} $	$\theta \gg 0^\circ$	$\Delta\sigma_{SV}(P_{\text{sat}}) = 0$	2	Pb/graphite ( $\theta = 117^\circ$ ) <sup>(b)</sup>

<sup>(a)</sup>(Johnson and Dettre 1993), <sup>(b)</sup>(Gangopadhyay and Wynblatt 1994)



**Figure 1.35.** Schematic monolayer adsorption isotherms (surface coverage  $\alpha$  versus  $P/P_{\text{sat}}$ ) for the two cases in Table 1.2. At  $P/P_{\text{sat}} = 1$ , the solid surface is “wet” in case (1) and nearly “dry” in case (2).

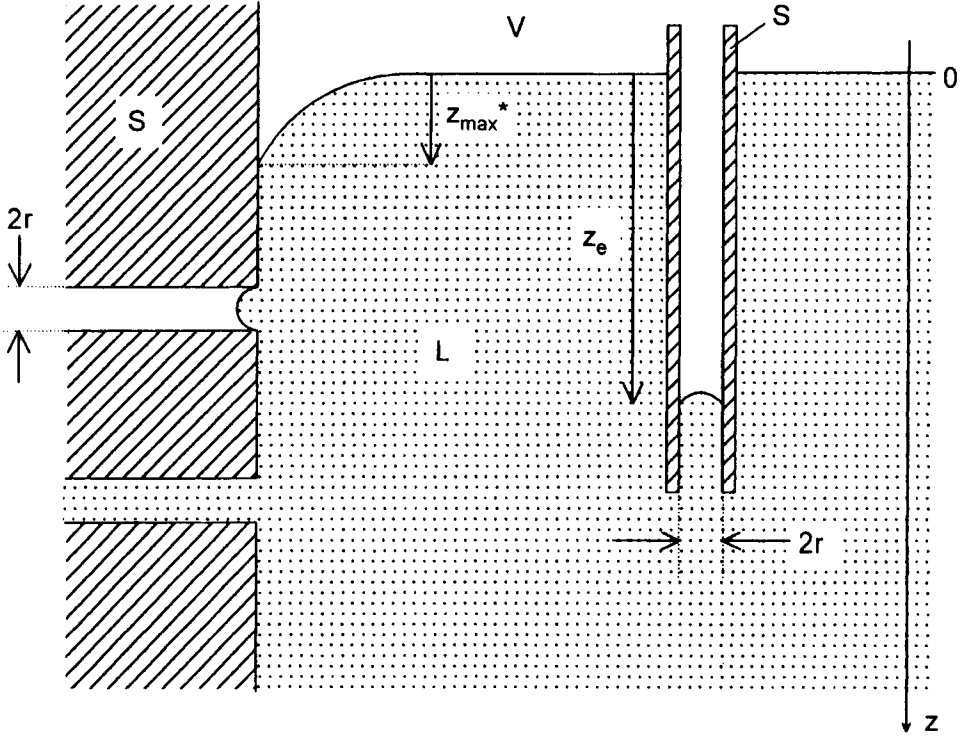
(2) When the adhesion energy is much lower than the cohesion energy of the liquid ( $|\epsilon_{SL}| \ll |\epsilon_{LL}|$ ), adsorption is negligible or weak, even at  $P = P_{\text{sat}}$  (Figure 1.35). Growth of a macroscopic film on the substrate from the vapour is possible only if the supersaturation is sufficient to overcome nucleation barriers. This corresponds to 3D nucleation or Volmer-Weber mode of growth of thin films. In wetting experiments,  $P = P_{\text{sat}}$  and the spreading coefficient  $W_s$  is positive so that a

macroscopic film is not stable and will collapse to form droplets (i.e.  $\theta > 0^\circ$ ). Typical examples are non-reactive metal/ionocovalent oxide and metal/graphite couples, in which adhesion is due to physical interactions that are weak compared to the cohesion energy of the metal. Experimental  $\Delta\sigma_{SV}(P_{\text{sat}})$  data exist only for three metal/oxide couples (Section 4.2.2) : Sn/Al<sub>2</sub>O<sub>3</sub> ( $T = 1200^\circ\text{C}$ ,  $\theta = 121^\circ$ ), Co/Al<sub>2</sub>O<sub>3</sub> ( $T = 1505^\circ\text{C}$ ,  $\theta = 113^\circ$ ) and Cu/UO<sub>2</sub> ( $T = 1400\text{--}1600^\circ\text{C}$ ,  $\theta = 90\text{--}100^\circ$  (Hodkin and Nicholas 1973)). They were obtained using the multiphase equilibria technique (see Section 4.1.3) by measuring the surface energy of the oxide in vacuum or in a neutral atmosphere and in a saturated vapour of the metal. No significant difference between  $\sigma_{SV}^0$  and  $\sigma_{SV}$  was found in any case. A negligible adsorption of metal atoms on the substrate surface was also revealed by direct Auger electron spectroscopy analysis of the Pb-Ni/graphite samples that had been heated at temperatures close to but slightly lower than the melting point of Pb (Gangopadhyay and Wynblatt 1994). In that system, the contact angles were in the range  $100\text{--}120^\circ$ , depending on the molar fraction of Ni in Pb.

To sum up, fragmentary results show that solid surfaces in equilibrium with a saturated vapour of a species exhibit a transition from a “wet” surface ( $\Delta\sigma_{SV}(P_{\text{sat}}) \gg 0$ ) to a “dry” surface ( $\Delta\sigma_{SV}(P_{\text{sat}}) \cong 0$ ) when the contact angle increases from zero to about  $90^\circ$ . According to Johnson and Dettre (1993), for organic liquids on low cohesion energy solids, if  $\theta > 0$  then  $\Delta\sigma_{SV}(P_{\text{sat}}) \ll W_a(P_{\text{sat}})$  and  $W_a(P_{\text{sat}}) \cong W_a^0$ . However, there is experimental evidence that in some nearly immiscible couples consisting of a low-melting-point metal on a high-melting-point metallic substrate, for which very low but finite contact angles are observed ( $0 < \theta \leq 20^\circ$ ), adsorption is significant (see Table 4.4 and Section 5.2). On the other hand, a negligible effect of saturated vapour of U on the surface energy of uranium carbide was found in the range  $1300\text{--}1600^\circ\text{C}$ , the contact angles being close to  $60^\circ$  (Hodkin et al. 1971). While interesting, these results are not sufficient to define accurately the range of  $\theta$  corresponding to a transition between a “wet” and a “dry” solid surface.

### 1.4.3 Immersion

Consider now a liquid in a crucible that is unwetted by the liquid and surrounded by a vapour phase (Figure 1.36). The triple line between the liquid surface, the crucible wall and the vapour, is at a depth  $z_{\text{max}}^*$  below the general level of the liquid. For a crucible radius much larger than the capillary length  $l_c$ ,  $z_{\text{max}}^*$  is given by (see equation (1.23)):



**Figure 1.36.** Formation of menisci of height  $z_{\max}^*$  on a crucible wall and of height  $z_e$  in a capillary of the same material.

$$z_{\max}^* = l_c(1 - \sin \theta)^{1/2} \quad (1.51)$$

where  $\theta$  is the equilibrium contact angle. Note that  $z$  is defined here as being positive when directed downwards. We introduce into the liquid a capillary of internal radius  $r$  made of the same material as the crucible (Figure 1.36). The depression  $z_e$  of the liquid in the capillary can be calculated by minimizing the total free energy change of the system as a function of depth  $z$ . This free energy change is:

$$\Delta F = F(z) - F(z = 0) = (\sigma_{SV} - \sigma_{SL})2\pi rz + (\pi r^2 z) \frac{z}{2} \rho g \quad (1.52)$$

Setting  $d(\Delta F)/dz = 0$ , the equilibrium depression  $z_e$  is:

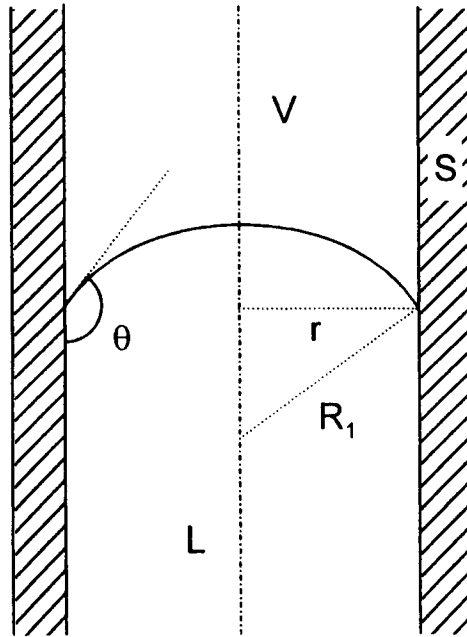


$$z_e = \frac{2(\sigma_{SL} - \sigma_{SV})}{r\rho g} \quad (1.53)$$

The quantity  $(\sigma_{SL} - \sigma_{SV})$  is called the *work of immersion*  $W_i$  because it defines the surface energy change when a S/V surface of unit area is replaced by a S/L interface of equal area by immersion of a solid in a liquid. In both the immersion and capillary rise processes, S/V and S/L areas change but the total L/V surface remains constant. Using the Young equation (1.16),  $W_i$  and  $z_e$  can be written:

$$W_i = \sigma_{SL} - \sigma_{SV} = -\sigma_{LV} \cos \theta \quad (1.54)$$

$$z_e = -\frac{2\sigma_{LV} \cos \theta}{r\rho g} \quad (1.55)$$



**Figure 1.37.** Configuration of the surface of a meniscus in a capillary.

Note that for  $\theta > 90^\circ$ ,  $z_e$  is positive i.e., it corresponds to a depression; for  $\theta < 90^\circ$ ,  $z_e$  is negative and corresponds to a capillary rise. Equation (1.55) can also be derived by a mechanical approach, considering the hydrostatic pressure  $\Delta P_h = \rho g z$  and the capillary pressure  $\Delta P_c$ . Applying the Laplace equation (1.20) to the capillary configuration with  $R_1 = R_2 = -r/\cos\theta$  (see Figure 1.37),  $\Delta P_c$  is:

$$\Delta P_c = -\frac{2\sigma_{LV} \cos \theta}{r} \quad (1.56)$$

By equating  $\Delta P_h$  and  $\Delta P_c$ , one finds again equation (1.55).

The work of immersion  $W_i$  is a thermodynamic quantity that describes any process of infiltration of liquids into porous media, for instance fabrication of composites by liquid routes, liquid state sintering or infiltration of refractories by molten metals or salts. In the example of Figure 1.36, at a depth  $z$ , any porosity (assumed cylindrical and open) of radius  $r$  larger than  $(-2\sigma_{LV} \cos \theta)/(\rho g z)$  will be infiltrated by the non-wetting liquid, while for smaller porosities no infiltration will occur.

All the energetic quantities used to describe the different types of wetting ( $W_a$ ,  $W_s$ ,  $W_i$ ) can be determined experimentally by measuring the contact angle and the  $L/V$  surface energy. When the measurement of  $\theta$  is performed to quantify atomic or molecular  $S/L$  interactions, great care must be taken to ensure that the measurement is of the Young contact angle and that adsorption of vapours of the liquid on the solid surface can be safely neglected.

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## Chapter 2

# Dynamics of wetting by metals and glasses

In Section 2.1 spreading kinetics will be presented for non-reactive liquid/solid systems i.e., for systems in which the mass transfer through the interfaces is very limited and has a negligible effect on the interfacial energies. Thus these quantities can be taken constant with time. The discussion of the results for molten metals and glasses will be based on models developed mainly for low cohesion energy viscous liquids at room temperature. The dynamics of wetting in reactive systems are developed in Section 2.2 taking into account the substantial progress made in the 90's in understanding the driving force and spreading kinetics for this important type of wetting.

### 2.1. NON-REACTIVE WETTING

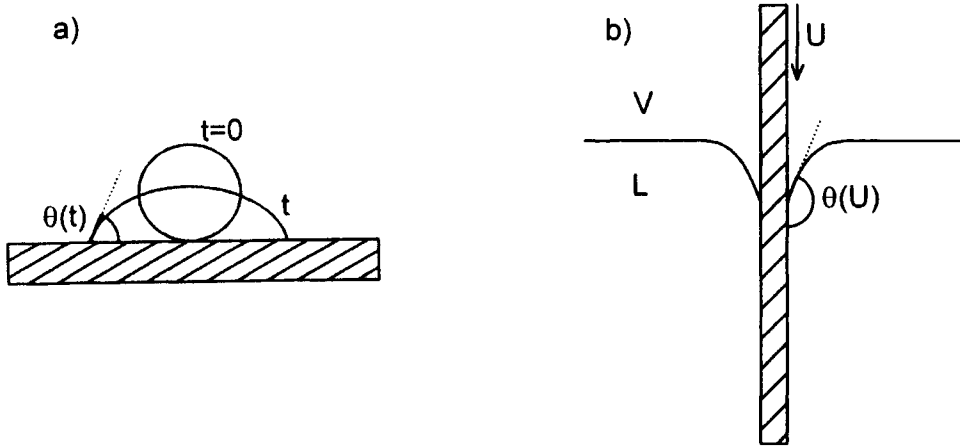
#### 2.1.1 *Experimental facts*

In general, two types of dynamic wetting can be distinguished. In *spontaneous wetting*, a drop is placed on a solid substrate and the rate at which it tends towards its equilibrium shape is measured (Figure 2.1.a). In *forced wetting*, a relative velocity of one phase (liquid or solid) with respect to the other one is imposed and the contact angle is measured as a function of the velocity. An example of forced wetting is the steady immersion (or withdrawal) of a plate in a liquid bath (Figures 2.1.b and 3.16). In the following, we will focus on spontaneous wetting which is the most studied of the high temperature systems.

A typical spreading experiment performed using the sessile drop configuration consists of measuring the rate of advance of the triple line over the solid surface when the contact angle decreases towards its final i.e., equilibrium, value  $\theta_F$ . Achieving reproducible results that can be interpreted in terms of scientific fundamentals needs (i) isothermal conditions, (ii) clean liquid and solid surfaces (otherwise spreading may be controlled for instance by deoxidation kinetics), (iii) negligible or at least controlled roughness of solid substrate, and (iv) negligible external forces (although the study of the effect of a well-quantified external force on spreading can also be of great interest).

There is only a limited number of studies which satisfy all these criteria and many of them were devoted to complex metal/metal, metal/ceramic or slag/oxide systems of interest for applications in steel-making or in composite processing (this

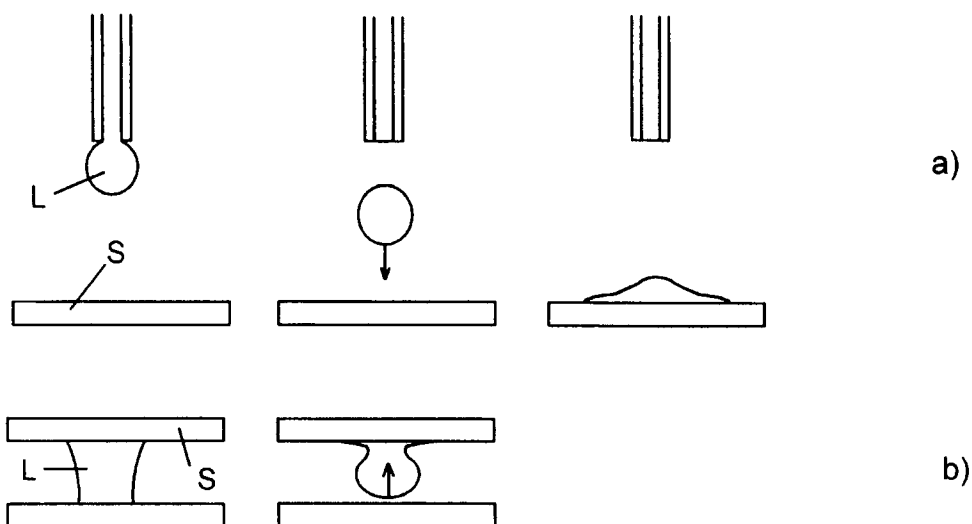
is true also for reactive systems). The major part of these studies have been performed by Russian and Ukrainian teams, whose results were reviewed by Popel (1994).



**Figure 2.1.** Examples of spontaneous (a) and forced (b) wetting.

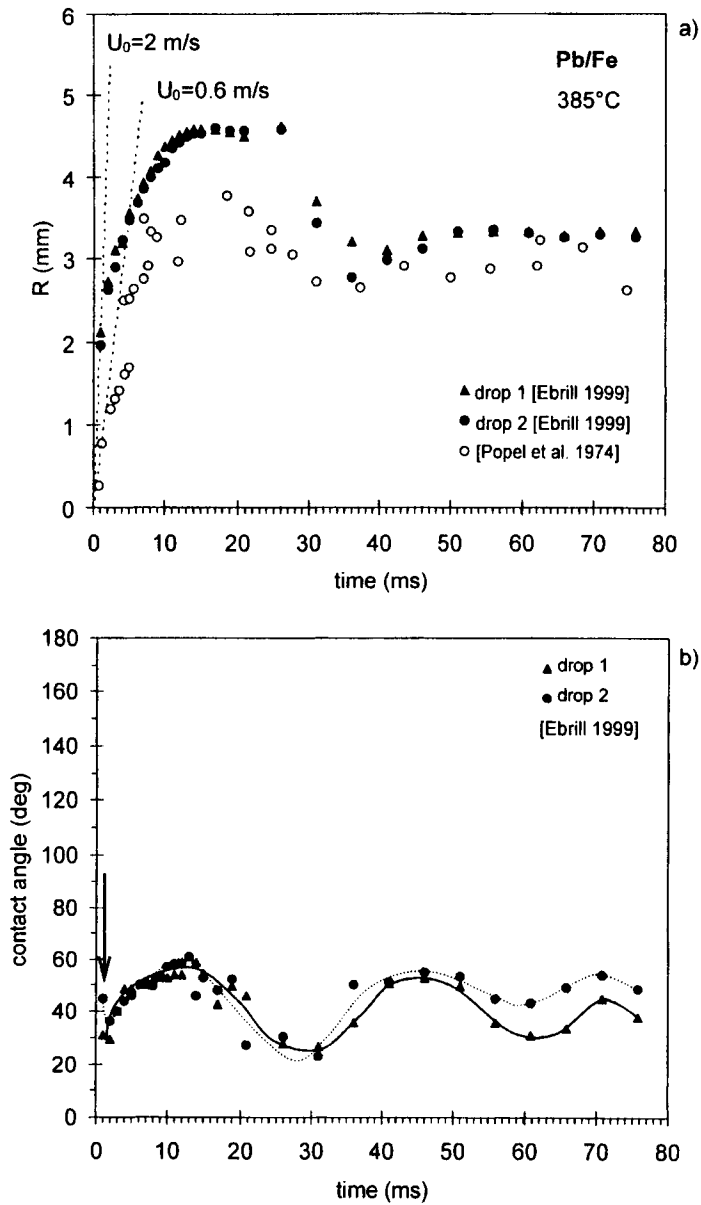
For low-viscosity liquids like metals or certain oxide melts at high temperature, the spreading time for millimetre size droplets is as brief as a few tens of milliseconds. In these systems, it is impossible to carry out truly isothermal spreading experiments by the conventional sessile drop technique (configurations a and b of Figure 3.7) in which the droplet is formed by the melting of a small solid piece. Indeed, in this case, spreading is strongly influenced by kinetics of the melting process. This drawback is avoided using arrangements c and d of Figure 3.7, in which the drop and the substrate are heated separately before they are brought in contact at a fixed temperature. These techniques allow clean liquid and solid surfaces to be prepared before contact, for instance by an appropriate heat treatment. However, for both of these arrangements, the spreading process may be perturbed by external forces. Thus, in the dispensed drop method (Figure 2.2.a), the kinetic energy of a falling drop transiently can increase the driving force for wetting and lead to oscillations of the triple line around the final drop base radius  $R_F$ . Indeed, the mechanical energy ( $m_d g z$ ) of a drop of mass  $m_d$  and radius  $r_d$  falling from a height  $z$  of a few millimeters is of the same order of magnitude as its surface energy  $4\pi r_d^2 \sigma_{LV}$ . As for the transferred drop variant (Figure 2.2.b), when the liquid bridge is detached from the lower substrate, it moves towards the upper substrate with an acceleration which can again lead to oscillations of the triple line. Both in the dispensed and transferred drop techniques, using a small drop mass

diminishes these perturbations. Finally, the effect of substrate roughness on spreading kinetics of high temperature melts has been little studied and most experiments were carried out on what were described as “well polished” substrates. In the following, spreading kinetics will be reviewed for selected systems. Particular attention will be paid to the distinction between features due to the experimental technique and features characteristic of the intrinsic behaviour of the system.



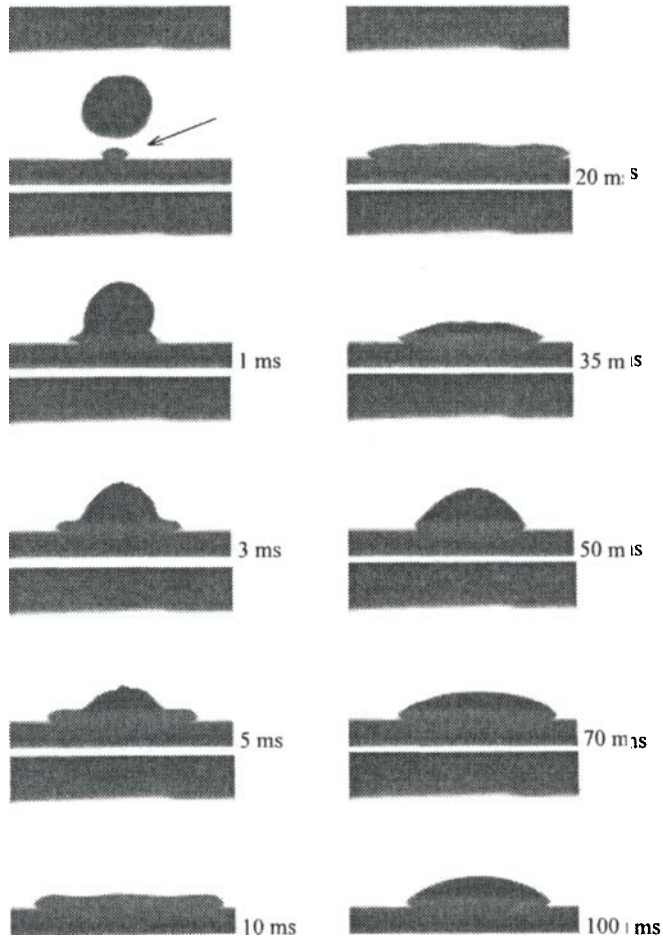
**Figure 2.2.** Shape of a drop when it contacts the substrate in the dispensed drop method (a) or when the liquid bridge is detached from the lower substrate in the transferred drop method (b).

**Molten Pb on solid  $\alpha$ -Fe.** The maximum solubility of  $\alpha$ -Fe in molten Pb at a temperature close to 400°C is less than 1 ppm. Spreading kinetics in this inert system have been studied by two different teams (Popel et al. 1974, Ebrill 1999) who used dry  $H_2$  atmospheres to reduce Fe before contact with Pb. Droplets of about 200 mg were dropped on high purity Fe substrates from 5 to 10 mm height. Smooth surface substrates were used ( $R_a = 5$  nm in the experiments of Ebrill). Good wetting is expected in this system and, indeed, the final contact angle  $\theta_F$  was found to be close to 40–45° by both teams. Figure 2.3 shows the changes with time of the drop base radius  $R$  and of the instantaneous contact angle measured by the tangent method.



**Figure 2.3.** Variation of drop base radius (a) and contact angle (b) with time for the Pb/Fe system at 385°C using the dispensed drop method. The framerate of the video technique used in the experiments did not allow following of the initial decrease of contact angle from 180° to about 40°. Data from works reported in (Popel et al. 1974, Ebrill 1999).





**Figure 2.4.** Successive images taken with a high speed camera of a Pb drop spreading on a Fe substrate at 370°C. The first image represents the falling drop before contact. The arrow shows the shadow of the drop on the solid substrate. Reprinted from (Ebrill 1999) with kind permission of the author.

In all the experiments, oscillations of the triple line around the final position (corresponding to  $\theta_F \cong 40\text{--}45^\circ$  and  $R_F \cong 3\text{--}3.5$  mm) are observed. Curves in Figure 2.3 show that the first contact angle, measured after about 1 ms, is close to the final value  $\theta_F$ , but at this moment the drop is clearly non-spherical (Figure 2.4). Thereafter, oscillations around  $R_F$  and  $\theta_F$  are observed which decay in about  $10^2$  ms. At this time, the droplet becomes a nearly spherical cap (Figure 2.4). Because external forces act at the moment of impact of the drop on the solid, it is

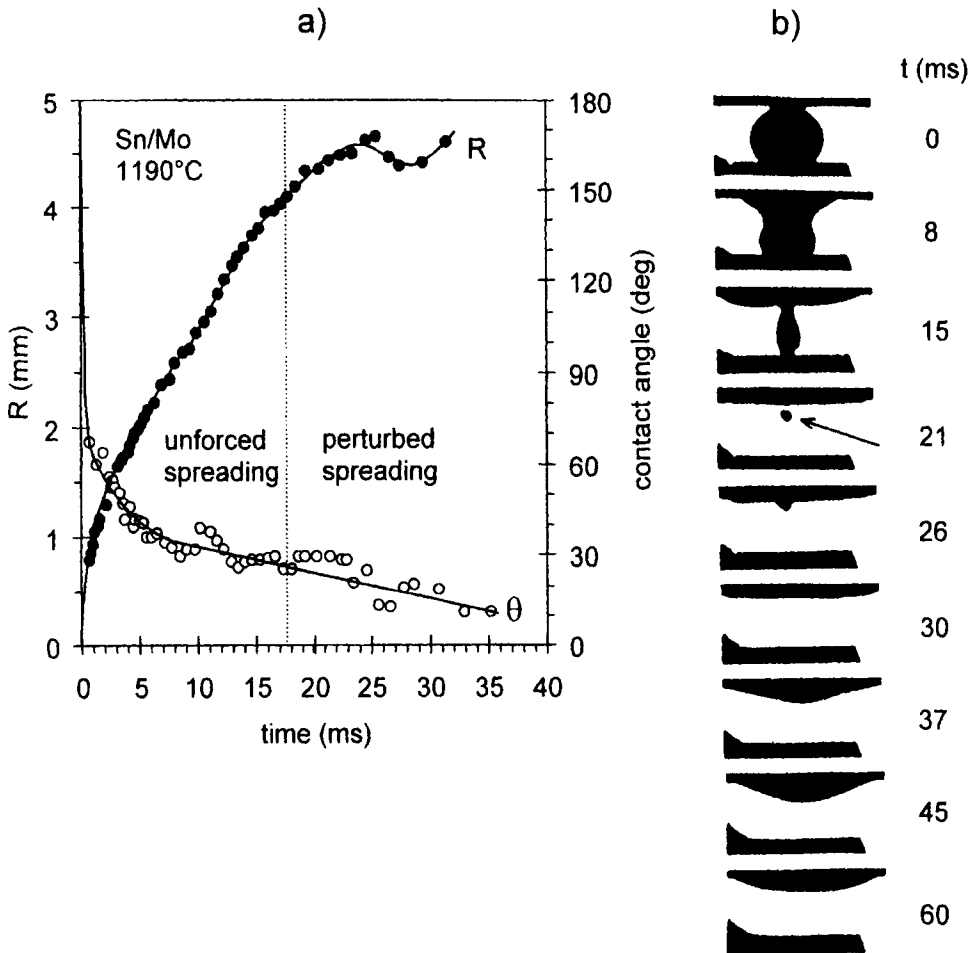
not clear if this behaviour is an intrinsic feature of the system or if it is only due to external forces. For the same reason, the initial spreading rate  $U_0 = dR/dt$  which is of the order of 1 m/s (Figure 2.3.a) may be overestimated. However, the order of magnitude of  $U_0$  in these experiments seems to be right. Indeed, the same order of magnitude has been found for other metal/metal couples using the transferred drop configuration (see below).

**Molten Sn on solid Mo.** This system, in which the mutual solubility is negligible, was studied by Sabuga (1990) and Naidich et al. (1992) using the transferred drop technique in high vacuum. Before contact, both the liquid and the solid were cleaned *in situ* by heating at a temperature higher than that used in the subsequent experiment. The volume of the drop placed on a lower graphite substrate was 0.025 ml. Changes of  $R$  and  $\theta$  with time, illustrated by photographs, are given in Figure 2.5 for an experiment performed at 1190°C. Similar results were obtained at lower temperatures (down to 760°C) but at such temperatures, the phase diagram indicated the presence of intermetallics.

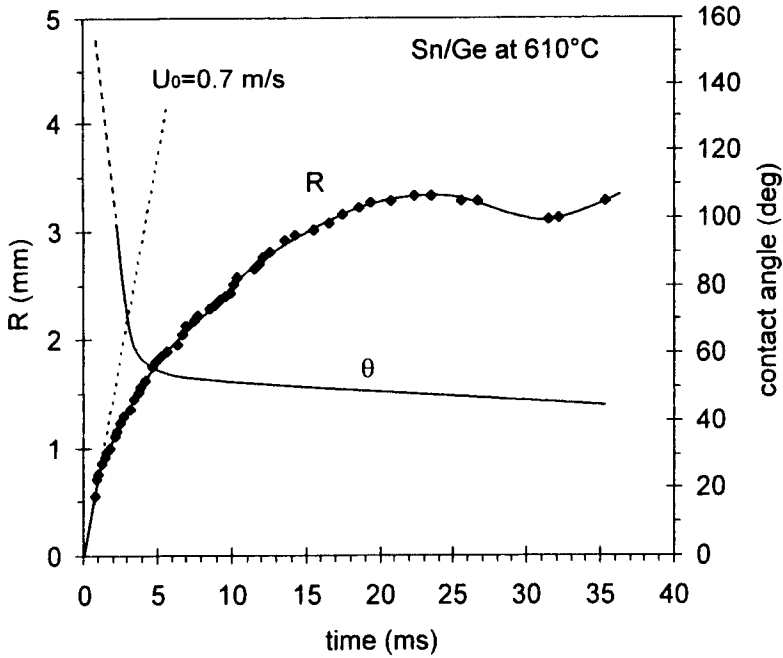
The complete transfer of the drop on to the Mo substrate occurs after 15 to 21 ms (Figure 2.5.b). Then, the acceleration of the drop is so high that a satellite drop is formed which also moves towards the upper substrate and coalesces with the main drop. As a result of the transfer process, the triple line oscillates around its equilibrium position. Thus, an unforced spreading takes place for 15 ms, with an initial rate  $U_0$  close to 0.75 m/s (because there are no experimental points for  $t < 1$  ms, this value may be too low). The contact angle decreases towards 40° in about 5 ms and thereafter changes comparatively slowly with time. At  $t \geq 5$  ms, the contact radius  $R$  increases significantly at a nearly constant rate. During this stage, spreading is due to fresh liquid coming from the lower part of the bridge, while the configuration of the triple line i.e., the  $\theta$  value, changes by comparison, only slightly.

**Molten Sn on solid Ge.** In this system, the phase diagram does not exhibit intermetallics and there is no solubility of Sn in solid Ge. The solubility of Ge in Sn is small at temperatures much lower than the melting point of Ge. Moreover, the changes in the configuration of the triple line due to dissolution occurs at comparatively longer times (see Section 2.2.1.1) and, as a result, there is no significant difference in spreading kinetics between pure Sn and Sn saturated in Ge on solid Ge for  $t < 50$  ms (Naidich et al. 1972). Figure 2.6 shows results obtained using the transferred drop technique in high vacuum. As in the Sn/Mo system, the initial spreading rate is about 0.5–1 m/s and the contact angle reaches a nearly constant value in only 5 ms while the drop base radius changes significantly for about 20 ms.

Changes in experimental temperature between 510°C and 920°C have only a small effect on  $U_0$  and spreading time (a few tens of %). The relatively weak effect of temperature on spreading kinetics appears to be a common feature in spreading of non-reactive liquid metals on metallic solids.



**Figure 2.5.** a) Changes of contact angle and drop base radius with time for Sn on Mo (upper surface) studied at 1190°C using the transferred drop technique (Naidich et al. 1992). b) Corresponding images of the drop. At  $t = 21$  ms, the arrow shows a satellite drop separated from the main liquid. Images reprinted from (Sabuga 1990) with kind permission of the author.



**Figure 2.6.** Changes of contact angle and drop base radius with time for Sn on Ge studied at 610°C using the transferred drop technique. Data from work reported in (Naidich et al. 1992).

**Molten metals on ceramics.** Using a high-speed camera, Grigorenko et al. (1998) used the transferred drop technique to study the spreading of a Ni-45 at.% Pd alloy on a vitreous carbon substrate with a surface roughness  $R_a$  of 30–40 nm. The low melting temperature of this alloy allowed a spreading experiment to be performed at a temperature of 1250°C at which reactivity between the alloy and C is negligible. The equilibrium contact angle (about 140°) was reached in less than 10 ms. However, the spreading rate could not be measured due to the poor stability of the liquid bridge.

Popel (1994) reported results obtained by Ishimov et al. (1971) showing that the initial spreading rate of Cu on  $\text{Al}_2\text{O}_3$  at 1350°C, i.e. for a system for which  $\theta_F \gg 90^\circ$  (see Table 6.1), is close to 1 m/s which is similar to that observed in metal/metal systems where  $\theta_F \ll 90^\circ$ .

**Oxide melts on solid substrates.** Contrary to metals for which the viscosity  $\eta$  changes little with temperature or from one metal to the other, the viscosity of

oxides and other ionocovalent liquid compounds can vary by several orders of magnitude.

Molten mixtures of  $\text{CaF}_2\text{-Al}_2\text{O}_3$  rich in  $\text{CaF}_2$  have a viscosity of the order of a few mPa.s, comparable to that of liquid metals. Results of Sorokin et al. (1968), reported by Popel (1994), showed that the initial spreading rate of these mixtures on  $\text{Al}_2\text{O}_3$  substrate is close to 1 m/s, as for liquid metals on solids, and decreases strongly with time, particularly when the instantaneous contact angle becomes very low.

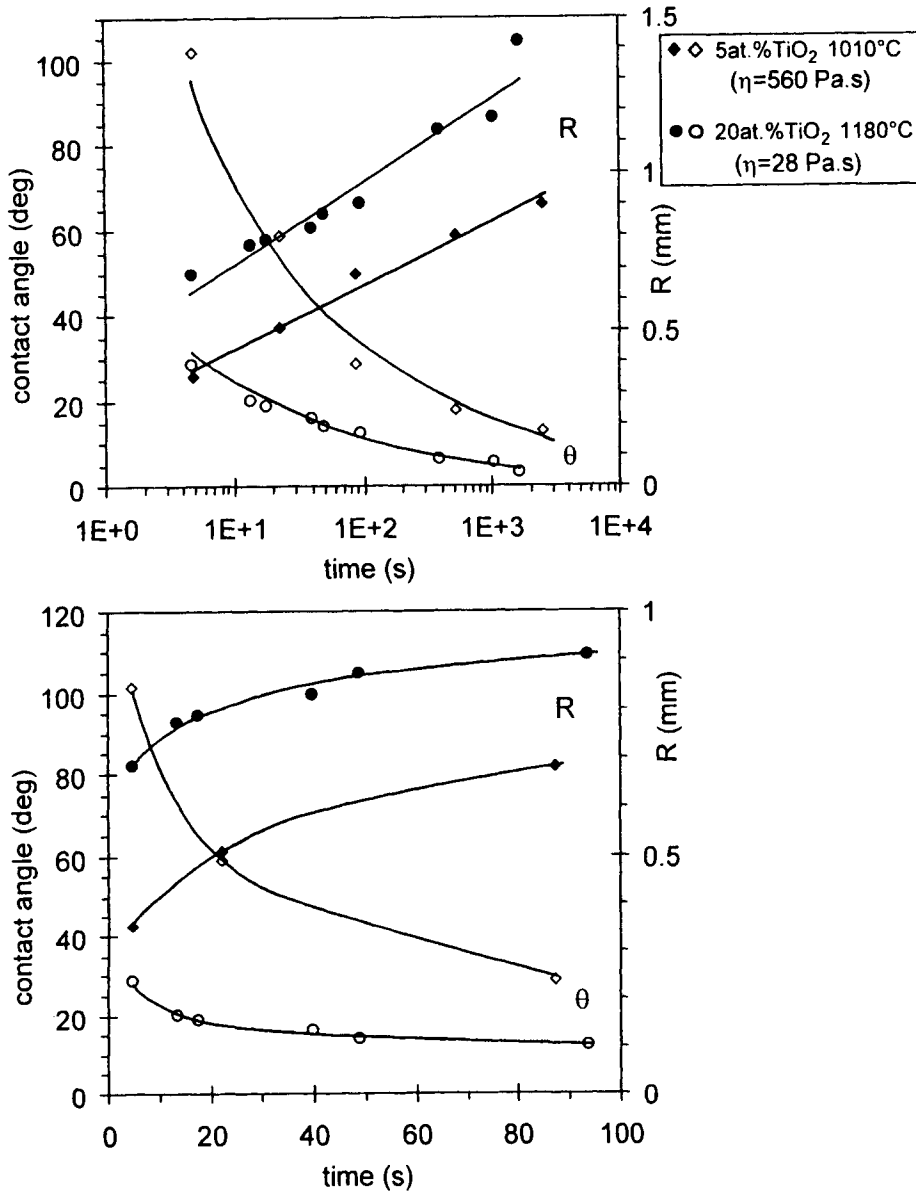
The viscosity of the ternary silicate glass  $\text{SiO}_2\text{-Na}_2\text{O-TiO}_2$  is in the range  $10^2\text{--}10^3$  Pa.s i.e., five orders of magnitude higher than that of  $\text{CaF}_2\text{-Al}_2\text{O}_3$  molten mixtures. Results obtained by the conventional sessile drop technique for millimetre size droplets on polished Pt are given in Figure 2.7 for two different compositions of glasses (Hocking and Rivers 1982). In these experiments, the drop surfaces maintained a nearly spherical shape during the whole spreading process. Both  $R$  and  $\theta$  vary significantly up to about 500 seconds. Thereafter, spreading continues very slowly, specially when  $\theta$  tends towards the equilibrium value ( $\theta_F = 5^\circ\text{--}15^\circ$ ). Dramatically slow spreading has been observed also for viscous  $\text{SiO}_2\text{-Al}_2\text{O}_3\text{-CaO-MgO}$  glass on  $\text{Al}_2\text{O}_3$  when the contact angle tends towards the equilibrium value close to  $10^\circ$  (Ownby et al. 1995).

To sum up, in spontaneous spreading, i.e., in the absence of any external force, the spreading time for millimetre-size droplets of high viscosity ( $\eta > 10$  Pa.s) is greater than  $10^2$  seconds and drops maintain a spherical shape during the whole process, indicating equilibrium of pressures inside the droplet at any instant. For the low viscosity liquid metals ( $\eta \approx 1$  mPa.s), the spreading time is  $10^{-2}\text{--}10^{-1}$  second and a lower limit of the initial spreading rate is 1 m/s. However, owing to experimental difficulties relating to such high spreading rates, no reliable information exist on the drop shape during spreading.

### **2.1.2 Modelling**

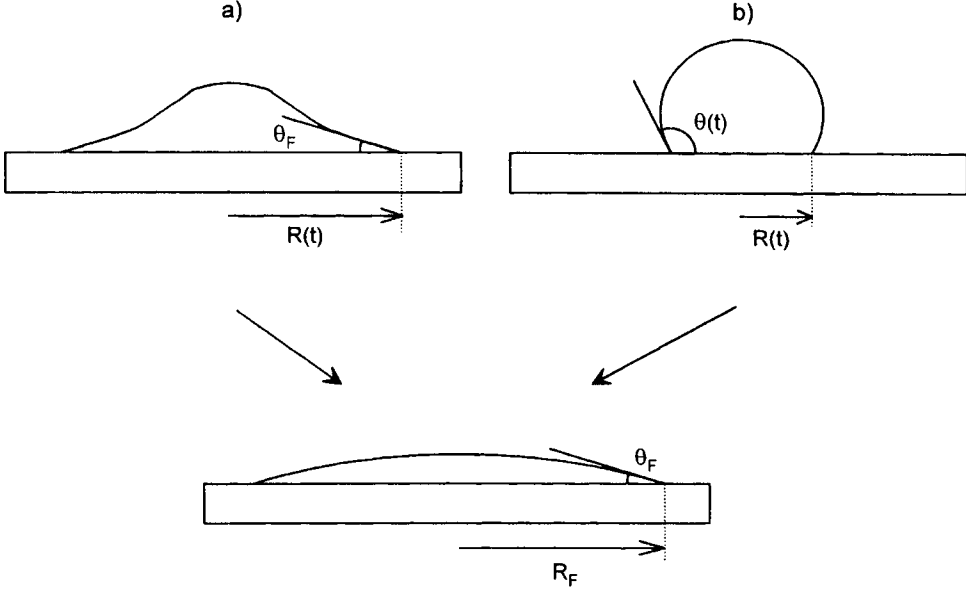
Modelling of non-reactive spreading has been performed mainly for the configuration of a small droplet spreading on a horizontal and perfectly smooth solid substrate so that gravitational forces are negligible. The effect of gravity will be briefly described at the end of this Section.

In the absence of any external forces, including gravity, two shapes may be observed during spreading depending on the relative importance of viscous and inertial forces. In the configuration of Figure 2.8.a, the shape of the drop is not spherical. The instantaneous macroscopic contact angle rapidly approaches the final equilibrium value  $\theta_F$  and spreading consists of an increase of  $R$  while the configuration of the triple line remains nearly unchanged. The spreading rate will



**Figure 2.7.** Variations of contact angle with time for ternary silicate glasses containing SiO<sub>2</sub> and Na<sub>2</sub>O in a 4:1 mole ratio with additions of TiO<sub>2</sub> on Pt substrates (Hocking and Rivers 1982). The  $R(t)$  curves are calculated from contact angles values assuming a spherical shape for the drop and taking a drop volume of  $0.52 \text{ mm}^3$ .

depend on the rate at which the matter moves from the bulk drop to the triple line, driven by the differences in capillary pressure given by the Laplace equation (1.20). In the configuration b of Figure 2.8, both  $\theta$  and  $R$  change with time while the shape of the drop is a nearly spherical cap.



**Figure 2.8.** Inertial (a) and viscous (b) spreading of a sessile drop in a non-reactive liquid/solid system.

The first case is expected to apply for liquids with a very low viscosity which permit high triple-line velocities and in which, once the contact angle approaches its equilibrium value, spreading is controlled by inertial forces responsible for the non-spherical shape of the drop at  $t \ll t_F$ , where  $t_F$  is the time needed to reach a constant drop base radius. The second case corresponds to a spreading controlled by viscous resistance. Because, as we will see below, in viscous spreading the dissipation of energy occurs mainly in the liquid close to the triple line, the remaining liquid can move more easily, maintaining a macroscopic spherical shape i.e., a constant capillary pressure. In this case, the driving force for wetting per unit length of triple line,  $f_d$ , is given by the change in the surface and interfacial energy  $F_s$  of the system resulting from a lateral displacement of the triple line:

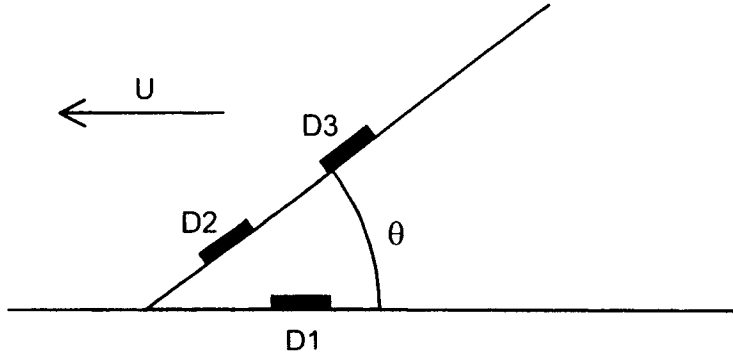
$$f_d = -\frac{dF_s}{dx} = \sigma_{SV} - \sigma_{SL} - \sigma_{LV} \cos \theta = \sigma_{LV} [\cos \theta_F - \cos \theta] \quad (2.1)$$

where  $x$  is the abscissa of the triple line and  $\theta$  is the instantaneous contact angle. When the triple line advances, the work done by surface forces, *per unit length of triple line and unit time*, is equal to:

$$W_d = U.f_d \quad (2.2)$$

where  $U$  is the triple line velocity ( $= dR/dt$ ).

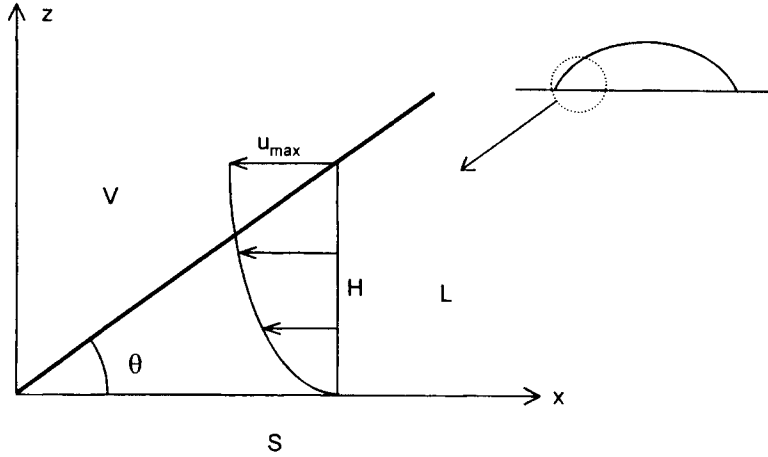
The viscous spreading of a sessile drop has been modelled by several authors (Tanner 1979, Hocking and Rivers 1982, de Gennes 1985, Summ et al. 1987). Although several differences exist between these treatments, they all regarded the drop as divided into two regions : (i) the bulk in which the motion of the fluid is easy and energy dissipation by viscous flow negligible and (ii) a macroscopic wedge near the triple line of typical width 0.1 mm. The motion of the fluid in this region has been observed by Dussan and Davis (1974) who marked the upper surface of a viscous liquid with small spots of dye and watched their motion. They found a characteristic rolling motion (Figure 2.9), similar to that of a caterpillar-tracked vehicle, which gives rise to viscous friction. Therefore, the work  $W_d$  is mainly dissipated by viscous friction in the wedge.



**Figure 2.9.** Motion of the liquid in the vicinity of the triple line in viscous spreading. In the Dussan and Davies experiment, spots of a dye D1, D2, D3 are laid on the free surface of an advancing edge. The spots slide down and then get stuck to the solid. From (de Gennes 1985) [4].

De Gennes (1985) considered also a precursor film ahead of the triple line, formed when the ratio  $(\sigma_{SV} - \sigma_{SL})/\sigma_{LV}$  is greater than unity, which corresponds to the case of more than perfect wetting. Because more than perfect wetting is not





**Figure 2.10.** Viscous spreading : fluid velocity profile in the liquid wedge close to the triple line. According to (de Gennes 1985) [4].

very common in high temperature systems, we consider (below) the case where  $\theta_F > 0^\circ$ . Viscous spreading will be discussed in the framework of the de Gennes model because it has the advantage of being analytical.

The fluid velocity in the wedge region is calculated by a “lubrication” approximation in which the fluid velocity  $u$  parallel to the interface varies parabolically between  $u = 0$  at  $z = 0$  and  $u = u_{\max}$  at the drop surface, as shown in Figure 2.10. (Note that this description is not valid near the drop center where the velocity field is much more complex (Denesuk et al. 1993); however, viscous dissipation in this region is deliberately neglected in the de Gennes model). The average value of  $u$  at a fixed distance  $x$  from the triple line is approximately equal to the triple line velocity  $U$ . At a fixed  $x$ , the viscous dissipation integrated over the liquid column of height  $H$  is  $3\eta U^2/H$  and the total dissipation in the wedge calculated between  $x = x_{\min}$  and  $x = x_{\max}$  is

$$E_{\text{diss}} = \frac{3\eta U^2}{\tan \theta} \ln \left| \frac{x_{\max}}{x_{\min}} \right| \quad (2.3)$$

$x_{\max}$  is a distance related to the macroscopic size of the droplet ( $x_{\max} \approx R$ ) while  $x_{\min}$  must be different from zero otherwise dissipation would diverge. Although all authors (Hocking and Rivers 1982, Marmur 1983, de Gennes 1985) agree on the necessity to remove this divergence by allowing slippage of the liquid layer in contact with the solid over a distance  $x_{\min}$ , neither the value of  $x_{\min}$  nor the

physical phenomena which permit such a slippage are well-defined in the general case. For instance, values of  $x_{\min}$  from 1 to  $10^2$  nm have been estimated, but it is possible that this distance depends on the strength of interfacial forces and on the structure of liquid molecules i.e., it is system dependent. Fortunately, the poor knowledge of the parameter  $x_{\min}$  has little effect on the final result because the dissipation energy depends logarithmically on  $x_{\min}$ . For instance, taking  $x_{\max} = 10^{-3}$  m, a change of  $x_{\min}$  from  $10^{-9}$  to  $10^{-7}$  m leads to a variation of the logarithmic term of about 30%, which is small compared to the possible errors due to several other approximations. Assuming that at each instant the work done by capillary forces  $W_d$  is equal to the energy dissipated by friction  $E_{\text{diss}}$ , one gets from equations (2.1) to (2.3):

$$\frac{3\eta K_1}{\sigma_{LV}} U = \tan \theta (\cos \theta_F - \cos \theta) \quad (2.4)$$

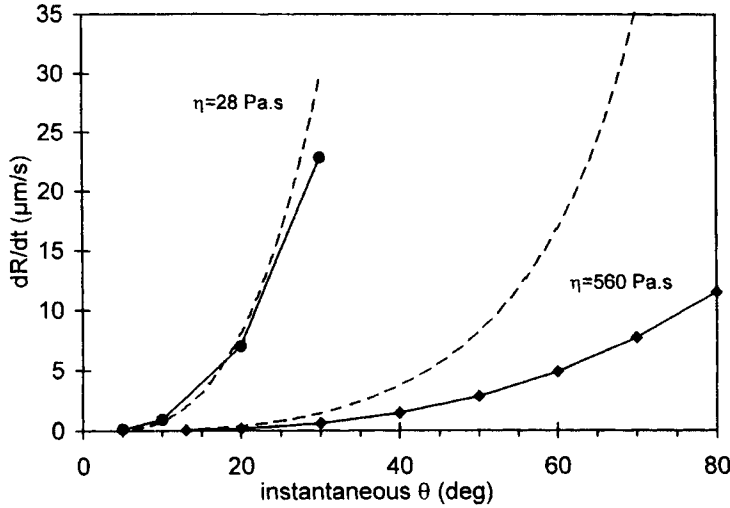
where  $K_1 = \ln|x_{\max}/x_{\min}| \cong 10$ . Note that this equation, valid for  $\theta < 90^\circ$ , is not specific to the sessile drop configuration but holds for all cases of spontaneous wetting, for instance in the case of the liquid bridge (Figure 2.2.b). According to this equation, the instantaneous spreading rate  $U$  depends for a given system only on the configuration of the triple line, or in other words, only on the instantaneous contact angle.

Figure 2.11 presents values of spreading rates calculated from equation (2.4) for two glasses studied in (Hocking and Rivers 1982). In agreement with experimental results computed from data of Figure 2.7, equation (2.4) predicts a strong dependence of  $U$  on  $\theta$  resulting from the conjunction of two facts : (i) the driving force decreases strongly when  $\theta$  decreases and (ii) the viscous losses in the liquid wedge increases when  $\theta$  decreases.

Replacing  $\tan \theta$  by  $\theta$  (this approximation introduces an error less than 10% for  $\theta < 45^\circ$ ) and  $\cos \theta$  by  $(1 - \theta^2/2)$  (the error is less than 2% for  $\theta \leq 45^\circ$ ), equation (2.4) becomes:

$$\frac{6\eta K_1}{\sigma_{LV}} U = \theta(\theta^2 - \theta_F^2) \quad (2.5)$$

where  $\theta$  and  $\theta_F$  are in radians. For the particular case  $\theta_F = 0^\circ$ ,  $U$  is proportional to  $\theta^3$ . This dependence, predicted for the spontaneous wetting, was also observed in the low  $U$ -low  $\theta$  range of experiments of *forced wetting* performed by Hoffman (1975), in which a liquid was forced to penetrate into a capillary at a fixed velocity,  $\theta$  being the corresponding contact angle measured at the penetration front (Figure



**Figure 2.11.** Variation of spreading rate with instantaneous contact angle for two silicate glasses on Pt. Full lines: experimental points from data of Figure 2.7 from (Hocking and Rivers 1982). Dashed lines: calculated curves from equation (2.4) with  $K_1 = 10$ ,  $\sigma_{LV} = 0.33 \text{ J.m}^{-2}$ ,  $\theta_F = 5^\circ$ .

2.12). At high  $U$ , the apparent contact angle first increases strongly with  $U$  and then tends towards  $180^\circ$ . In this high  $U$ -high  $\theta$  range, the penetration of the liquid into the capillary (or of the plate into the liquid bath, Figure 2.1.b) can be accompanied by gas entrainment between the liquid and the solid occurring above a certain velocity (Blake 1993, Kistler 1993).

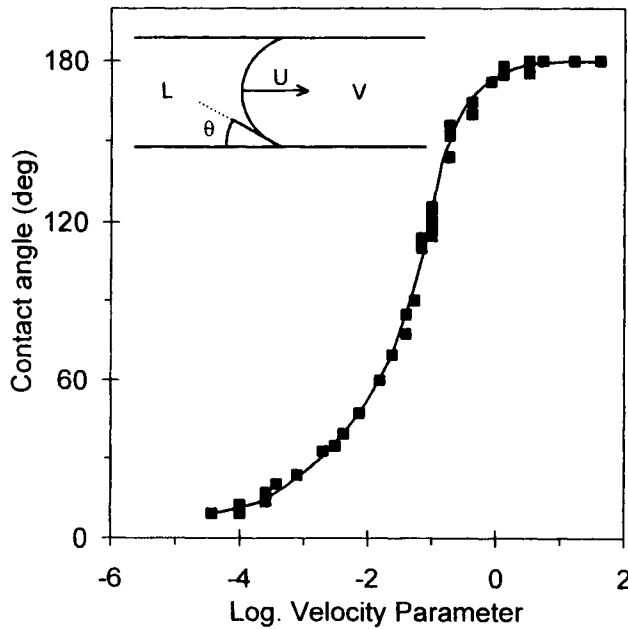
Let us come back to the case of spontaneous wetting in the sessile drop configuration. The variation of the drop base radius  $R$  with time can be easily calculated from equation (2.5) replacing  $\theta$  by  $4v/\pi R^3$ , where  $v$  is the drop volume, which is accurate to within 10% for  $\theta < 45^\circ$ . Thus integration of equation (2.5) with  $\theta_F = 0^\circ$  between  $R_0$  at  $t = 0$  and  $R$  leads to:

$$R^{10} - R_0^{10} = A_1 t \quad (2.6)$$

with  $A_1 \cong 3\sigma_{LV}v^3/(\eta K_1) \cong 0.3\sigma_{LV}v^3/\eta$ . This law, due to Tanner (1979) and de Gennes (1985), has been verified experimentally by Tanner using silicone oils. Results for spreading of high viscosity glasses on sapphire were also interpreted successfully using equation (2.6) (Ownby et al. 1995).

Taking into account the very limited number of experimental results for unforced wetting of liquid metals, no detailed comparison with model prediction is

possible. For Sn/Mo at  $\theta = 30^\circ$ , the value of  $U$  calculated from equation (2.4) (0.8 m/s) is higher than the experimental value (close to 0.2 m/s, see Figure 2.5). At higher contact angles, the calculated value of  $U$  increases much faster with  $\theta$  than the experimental one. For instance, for  $\theta = 65^\circ$ ,  $U_{\text{calc}} = 12$  m/s against  $U_{\text{exp}} = 0.3$  m/s which would mean that the spreading rate is not limited by viscous friction but by another process. In the following, three processes will be considered, namely (i) movement of atoms at the liquid/solid interface close to the triple line, (ii) inertia and (iii) movement of the ridge formed at the triple line.



**Figure 2.12.** Effect of velocity parameter  $U\eta/\sigma_{LV}$  on the contact angle of silicone oils flowing in glass tubes in forced wetting experiments, after (Hoffman 1975) [5].

**Kinetic regime.** The first mechanism corresponds to the so-called “kinetic” regime (Popel 1994, Grigorenko et al. 1998) which is similar to the adsorption/desorption model (Blake 1993). Contrary to macroscopic hydrodynamic models, the adsorption/desorption model is based on the hypothesis that the motion of the triple line is ultimately determined by the statistical kinetics of atomic or molecular events occurring within the three-phase zone (Samsonov and Muravyev 1998). Such processes may be limiting at the very early stages of spreading of low

viscosity liquids i.e., in the high  $U$ -high  $\theta$  range (Popel 1994, Grigorenko et al. 1998). However, there are not enough reliable experimental data of spreading kinetics in high temperature systems to confirm the effectiveness of the “kinetic” regime.

**Inertial regime.** For low-viscosity liquids like molten metals, the use of the viscous friction model is questionable because inertial forces can become very important. For a sessile drop of mass  $m_d$ , the inertial force is given by:

$$f_{in} = m_d \frac{dU}{dt} \quad (2.7)$$

For  $\theta \ll 90^\circ$ , the drop mass *per unit length of triple line* is  $2\rho R^2\theta/3$  ( $\rho$  denoting the liquid density), and the acceleration  $dU/dt$  can be easily calculated from equation (2.6) for the de Gennes model. The viscous force per unit length of triple line is:

$$f_v = \frac{3\eta UK_l}{\tan \theta} \cong \frac{3\eta UK_l}{\theta} \quad (2.8)$$

Then, the ratio of the inertial force to the viscous force is given by:

$$\frac{f_{in}}{f_v} = \frac{0.24}{K_l^2} \frac{\rho \sigma_{LV}}{\eta^2} \theta^5 R = c \theta^5 R \quad (2.9)$$

For a glass (with typical values  $\sigma_{LV} = 0.5 \text{ J/m}^2$ ,  $\rho = 0.5 \times 10^4 \text{ kg/m}^3$ ,  $\eta = 10 \text{ Pa.s}$ ), the constant  $c$  is  $0.06 \text{ m}^{-1}$ . Taking  $\theta = 1 \text{ rad}$  and  $R = 10^{-3} \text{ m}$ ,  $f_{in}/f_v = 6 \times 10^{-5}$ , which shows that inertial forces are negligible.

For a metal (with  $\sigma_{LV} = 1 \text{ J/m}^2$ ,  $\rho = 10^4 \text{ kg/m}^3$ ,  $\eta = 10^{-3} \text{ Pa.s}$ ), the constant  $c$  is  $2 \times 10^7 \text{ m}^{-1}$ . Then, for  $\theta = 1 \text{ rad}$  and  $R = 10^{-3} \text{ m}$ , the ratio  $f_{in}/f_v$  is  $2 \times 10^4$  (for this value the instantaneous velocity of the triple line calculated from equation (2.5) with  $\theta_F = 0^\circ$  would be  $16 \text{ m/s}$ ), which clearly indicates the predominance of inertial forces. The viscous friction becomes important only for very small  $\theta$  values. Indeed, for  $\theta = 0.1 \text{ rad}$  and  $R = 10^{-3} \text{ m}$ , the ratio  $f_{in}/f_v$  is  $0.2$ .

From this order of magnitude analysis, it seems that for liquid metals the viscous friction can be important only in the very late stages of spreading for nearly perfect wetting systems. In the early stages, viscous friction is negligible compared to the inertial force, the configuration being that of Figure 2.8.a in which local equilibrium is rapidly established at the triple line and fluid motion is driven by differences in capillary pressure between the drop bulk (where the capillary pressure is inversely proportional to the drop radius) and the triple line (where the

capillary pressure is nearly zero). By considering that the capillary energy of a droplet of initial radius  $r_d$  is transformed into kinetic energy, Joanny (1985), cited by de Gennes (1985), found a typical value of the spreading velocity given by:

$$U \cong \left( \frac{\sigma_{LV}}{\rho r_d} \right)^{1/2} \quad (2.10)$$

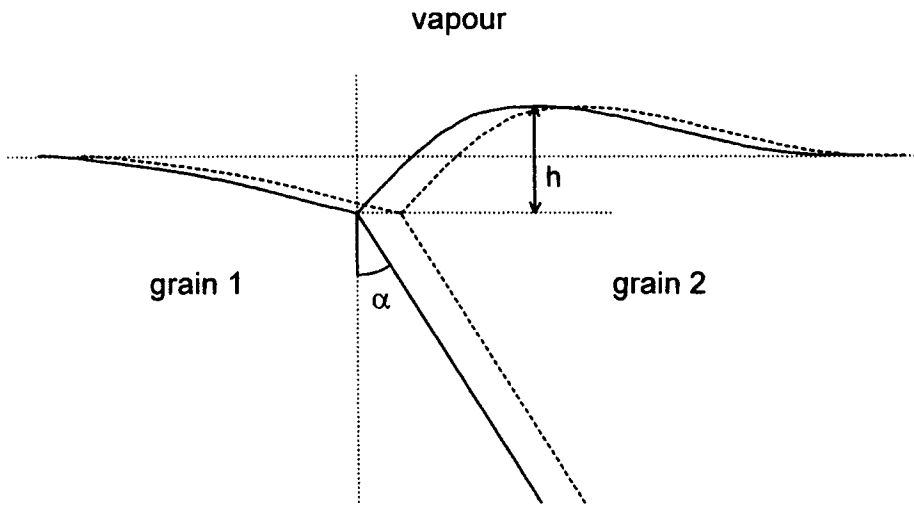
For a typical metal and taking  $r_d = 10^{-3}$  m, this expression leads to  $U \cong 0.3$  m/s, much closer to the experimental data than values calculated from the viscous model.

**Wetting ridge regime.** As shown in Section 1.2.4, complete equilibrium at the triple line is obtained only with a displacement of the triple line in the direction perpendicular to the solid surface. For “soft”, viscoelastic, substrates, this local deformation, or “wetting ridge”, is measurable (several tens of nm) and the lateral displacement of the ridge may control spreading (Carré and Shanahan 1995). For “hard”, high cohesion-energy, solids, the elastic deformation at the triple line is negligible (of the order of  $10^{-2}$  nm, see Section 1.2.4) and cannot affect the spreading process. However, at high temperature, atomic mobility can contribute to the growth of the ridge, as discussed in Section 1.2.4. The possibility that this ridge plays an important role in the spreading of metallic liquids on “hard” solids was discussed in (Saiz et al. 1998). The starting point of this work is the study of Mullins (1958), who calculated the effect of thermal grooving on grain-boundary motion.

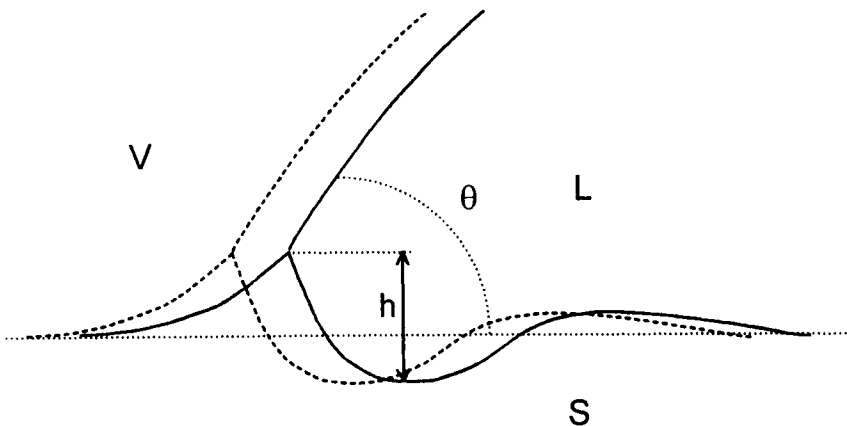
When a grain boundary forms an angle  $\alpha$  with the direction perpendicular to the interface, there is a critical value  $\alpha_c$  above which the grain boundary can move, driven by the difference in interface curvature across the groove root (Figure 2.13). When atomic movement in the groove is assumed to occur by surface diffusion, Mullins (1958) found a stationary solution for  $\alpha \geq \alpha_c$  corresponding to a constant grain boundary velocity and a constant groove depth  $h$ . For  $\alpha < \alpha_c$ , the grain boundary is pinned by the groove (i.e., the groove acts as an asperity pinning the triple line in wetting) and the groove grows according to the power law  $h^n = Kt$  (equation (1.33) with  $n = 4$ ).

Saiz et al. (1998) considered that in the case of a triple line, the L/V surface can play the role of a grain boundary and the “wetting ridge” can move either by bulk or surface (or interface) diffusion of solid atoms (Figure 2.14). They treated the case of surface diffusion with  $n = 4$ , taking into account the difference of diffusivities at the S/V surfaces and S/L interfaces. In their experiments with Cu and Ni droplets on  $Al_2O_3$  surfaces (see Section 1.2.4), Saiz et al. maintained the

droplets in contact with the substrate for several tens of minutes at the end of the spreading process, allowing the ridge to grow to a size that permitted easy observation. For Cu, a wetting ridge with  $h = 10$  nm was formed after 2 hours at  $1150^\circ\text{C}$  and for Ni  $h = 0.2\ \mu\text{m}$  after 1 hour at  $1500^\circ\text{C}$ . Much greater ridge heights (several tens of  $\mu\text{m}$ ) were observed for silicate glass droplets on Co at  $1440^\circ\text{C}$ , i.e., at a temperature very close to the melting point of the substrate.



**Figure 2.13.** Traveling grain-boundary groove according to Mullins (1958).



**Figure 2.14.** Wetting ridge at the triple line formed during spreading according to (Saiz et al. 1998).

A wetting ridge can affect spreading kinetics only if its size *during spreading* is significant with respect to the size of surface roughness of the substrate. Spreading kinetics studies are usually performed on polished surfaces with a typical average roughness of 10 nm. Accordingly, wetting ridges must have  $h > 10$  nm in order to affect spreading rates. For Ni, the time  $t_r$  needed for the ridge to attain  $h = 10$  nm can be extrapolated from data obtained for  $t = 1$  h using equation (1.33) with  $n = 3$ , which leads to  $t_r \cong 0.5$  s. Although the conclusions of this calculation would be the same with  $n = 4$ , it appears more plausible, at least on the liquid side of the ridge, for the ridge growth to be governed by diffusion through the liquid for which  $n = 3$  rather than by interface diffusion for which  $n = 4$ . If we consider a triple line with a lateral velocity  $U$  not yet affected by the ridge, the dwell time of the triple line on the area of a growing ridge of width  $w$  ( $w$  being of the order of  $h$  (Mullins 1960)) is  $t_w \cong h/U$ . For the two processes of ridge growth and drop spreading to interfere, the time  $t_r$  for ridge formation must be close to or lower than  $t_w$ , which will occur only for  $U < U^* = h/t_r$ . In the example of Ni,  $U^*$  is 20 nm/s. Therefore non-reactive spreading of Ni, for which  $U$  is expected to be of the order of  $10^2$ – $10^3$  mm/s, cannot be affected by wetting ridges, except at times  $t$  approaching  $t_F$  i.e., when  $U$  tends *asymptotically* towards zero. The same conclusion is *a fortiori* valid for Cu on  $Al_2O_3$ .

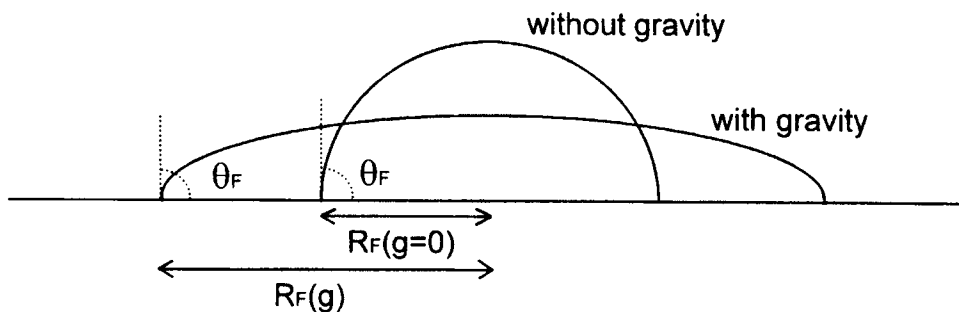
Another example is the molten Pb/solid Fe system for which the depth of a groove formed at the L/S interface is 10  $\mu$ m after 150 h at 1100°C (at this temperature the molar fraction of Fe dissolved in Pb in equilibrium with  $\gamma$ -Fe is  $8 \times 10^{-4}$ ) (Eustathopoulos 1983). The value of  $U^*$  calculated from these data is 20  $\mu$ m/s, which is again negligible compared with the expected spreading rate of non-reactive metals, except at  $t$  very close to  $t_F$ . Note that values of the spreading rate of the order of  $1$ – $10^2$   $\mu$ m/s are observed for several cases of reactive wetting and thus wetting ridges can, in principle, influence spreading kinetics in these cases.

**Effects of gravity.** Until now, spreading kinetics have been discussed for small droplets for which gravity can be neglected. For large droplets, gravity can modify spreading by two different effects : (i) by increasing the value of the final drop base radius  $R_F$  compared to the zero gravity situation (Figure 2.15) and (ii) by increasing the driving force of wetting  $f_d$  (equation (2.1)) which now will be given by:

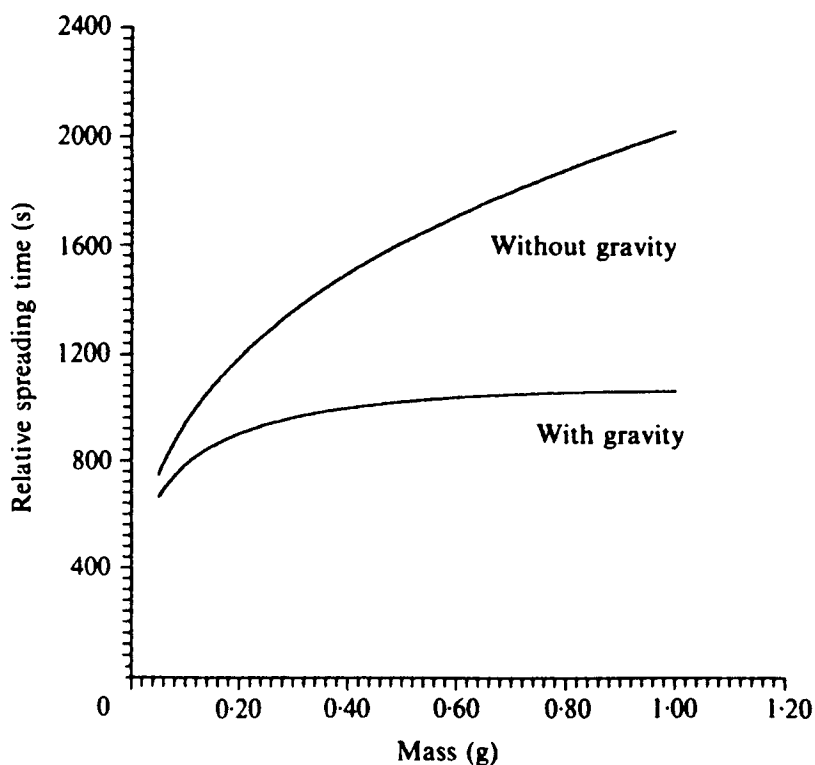
$$f_d = -\frac{dF_s}{dx} - \frac{dE_p}{dx} \quad (2.11)$$

where the second term of the right hand side takes into account the decrease in potential energy  $E_p$  of the spreading drop. The first effect tends to increase the spreading time for a fixed value of the drop mass while the second effect acts in an





**Figure 2.15.** Equilibrium shape of a sessile drop with and without gravity.



**Figure 2.16.** The predicted time, with and without gravity, required for a droplet to change from a contact angle of  $100^\circ$  to  $10^\circ$  as a function of the total droplet mass ( $\theta_F = 5^\circ$ ,  $\sigma_{LV} = 0.2 \text{ J.m}^{-2}$ ,  $\eta = 5 \times 10^3 \text{ Pa.s}$ ,  $\rho = 5 \times 10^3 \text{ kg.m}^{-3}$ ). Reprinted from (Denesuk et al. 1993) [6] with kind permission of the authors.

opposite manner. Figure 2.16 shows values of spreading times calculated for a viscous liquid as a function of drop mass  $m_d$  with and without gravity (Denesuk et al. 1993). With gravity, the curve shows that the spreading time first increases with  $m_d$  and then varies only weakly indicating that the two effects are partially compensated. At any  $m_d$ , the action of gravity leads to a decrease in spreading time but this effect is significant only for  $m_d > 0.1$  g.

### 2.1.3 Concluding remarks

For viscous liquids such as most glasses ( $\eta > 10$  Pa.s), the spreading time for millimetre size droplets is longer than  $10^2$  seconds. For these liquids, spreading rates at  $\theta < 90^\circ$  are described satisfactorily by models in which capillary energy is dissipated only by viscous friction, which occurs mainly in a wedge close to the triple line. For low viscosity liquid metals ( $\eta \sim 10^{-3}$  Pa.s), much shorter spreading times are observed ( $10^{-1}$ – $10^{-2}$  second) and the lower limit of the initial spreading rate is 1 m/s. For these liquids, models of viscous spreading cannot explain existing data, except probably in the region of very small contact angles. For higher  $\theta$  values, other processes may be limiting, specially inertia.

## 2.2. REACTIVE WETTING

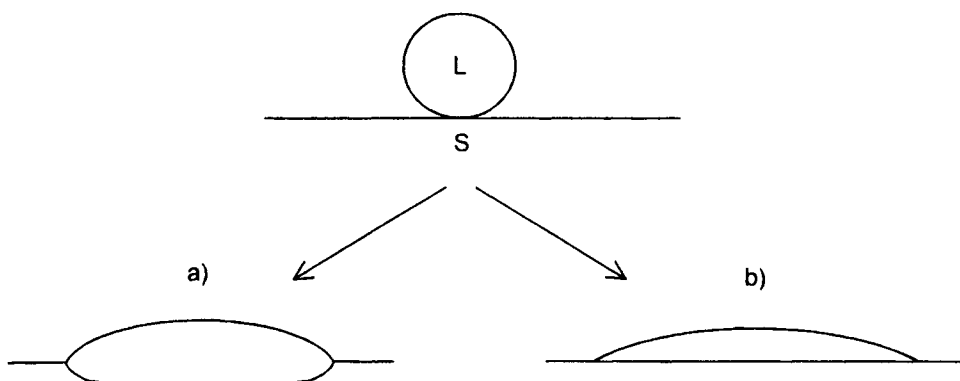
We will first discuss the case of simple dissolution of the solid in the liquid (Section 2.2.1) and then the case of formation at the interface of a 3D compound by reaction between the solid and the liquid (Section 2.2.2).

### 2.2.1 Dissolutive wetting

Two extreme cases will be considered. In the first one, dissolution of the solid into the liquid is assumed not to change significantly the surface and interfacial energies  $\sigma_{LV}$  and  $\sigma_{SL}$ . Therefore, dissolution modifies only the geometry at the triple line (Figure 2.17.a). In the second case, the interfacial energies are modified due to dissolution of small quantities of tensio-active species of the solid but the solid/liquid interface is assumed to remain nearly flat i.e., the equilibrium contact angle is still given by the Young equation (Figure 2.17.b).

**2.2.1.1 Dissolution-insensitive  $\sigma_{LV}$  and  $\sigma_{SL}$  values.** This case was studied by Warren et al. (1998) and Yost and O'Toole (1998) and modelled by the first authors for a liquid metal B/solid metal A system in which, at the experimental

temperature, there is no formation of intermetallics and the solubility of B in A is negligible.

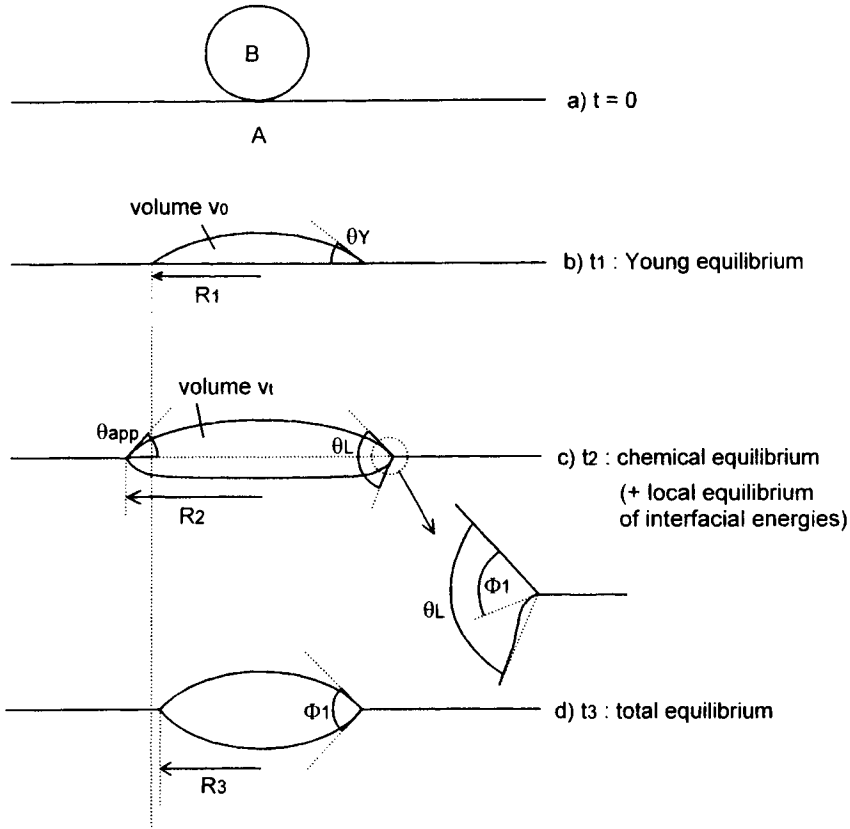


**Figure 2.17.** Two extreme cases of dissolutive wetting. (a) Dissolution of the solid modifies the geometry at the triple line. (b) A slight dissolution is enough to modify the surface energies of the system while the S/L interface remains macroscopically planar.

The treatment of Warren et al. provides an insight into the parameters of importance for this type of wetting. According to these authors, when a droplet of pure B, or B undersaturated in A, is placed on pure solid A, the approach to equilibrium occurs in three stages having different time scales (see Figure 2.18 for meaning of symbols used in the following):

(i) Non-reactive spreading takes place in a short time  $t_1$ . During this stage, the effect of dissolution on the macroscopic morphology is negligible and the contact angle at  $t = t_1$  is nearly equal to the Young contact angle of the system (Figure 2.18.b). We saw in Section 2.1.1 that  $t_1 \approx 10^{-2}$  s.

(ii) Then, dissolution of the solid in the liquid occurs (Figure 2.18.c) and affects the macroscopic contact angle after a certain time (in the experiments of Warren et al. on molten Sn/solid Bi couple, the S/L interface remained macroscopically flat even at  $t = 5$  s and was curved close to the triple line at  $t = 90$  s, see Figure 2.20). This is followed by diffusion, driven by differences of concentration,  $C$ , between the S/L interface, where  $C \cong C_i$ , and the drop bulk, where  $C = C_\infty$  (with  $C_\infty(t = 0) = C_0$ ). This process increases the total volume of the liquid phase and the final volume  $v_f$  depends on the initial volume  $v_0$ , the initial concentration of A in B and the phase diagram. The changes of morphology with time were calculated by Warren et al. (1998) by considering that the *microscopic* dihedral angle at the triple



**Figure 2.18.** Dissolutive wetting: the approach of local (c) and total (d) equilibrium in the sessile drop configuration. In liquid metal/solid metal systems, the characteristic times of the different stages are  $t_1 \sim 10^{-2}$  s,  $t_2 \sim 10^2$  s and  $t_3 \sim 10^8$  s. According to the calculations of Warren et al. (1998).

line is given by the Smith equation (1.30) and assuming that the triple line remains on the plane of the substrate. Moreover, assuming that the transfer of atoms through the interface is rapid compared to diffusion in the liquid alloy, it follows that the solid and liquid phases are in thermodynamic equilibrium at the interface. This equilibrium is described by the Gibbs-Thomson equation (1.32) which, expressing the chemical potential  $\mu$  as a function of the concentration in the liquid  $C$ , allows, after integration, the equilibrium concentration  $C_i$  in the liquid at an interface of curvature  $\kappa$  to be related to the equilibrium concentration  $C_{eq}$  for a flat interface:

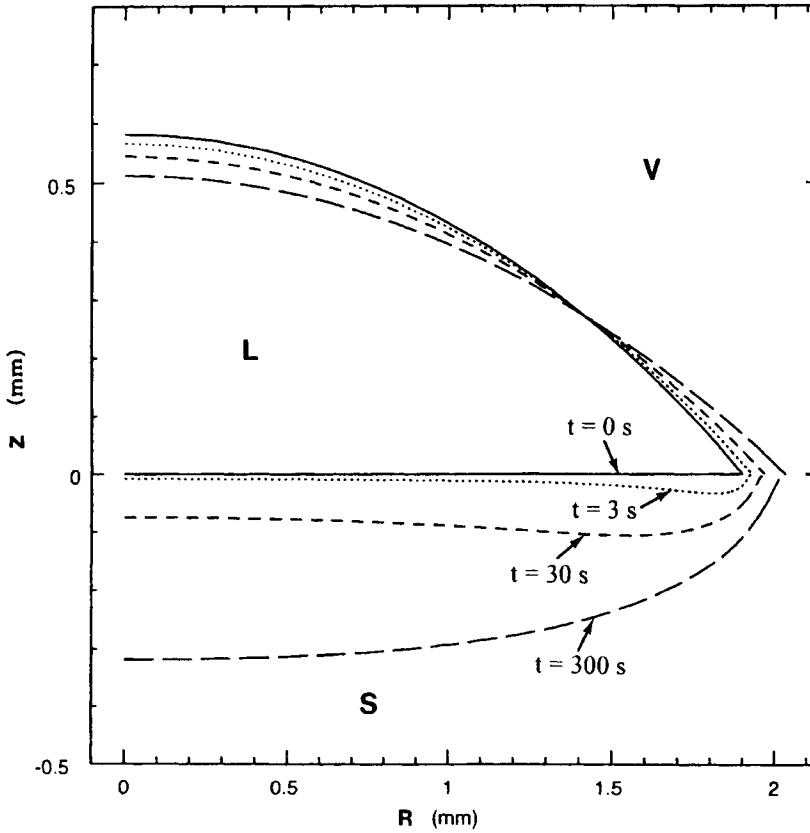
$$C_i = C_{eq}(T)[1 + \Lambda\kappa] \quad (2.12)$$

In this equation,  $\Lambda$  is the Gibbs-Thomson parameter defined by  $\sigma_{SL}v_m/(RT)$  ( $v_m$  being the molar volume of the solid). Then, the dissolution rate is derived by calculating the diffusion flux from the moving interface to the drop bulk. Such calculations were performed by Warren et al. (1998) for a Bi-Sn drop, of radius  $R_1 = 1.9$  mm at  $t_1$  and initial composition  $C_0 = 30.5$  at.% Sn, on a Bi substrate at  $245^\circ\text{C}$ . At this temperature, the equilibrium concentration  $C_{eq}$  is 16.4 at.% Sn, so that equilibration doubles the liquid volume. During this process, the drop base radius  $R$  increases moderately, the maximum value of  $(R_2 - R_1)/R_1$  being 7%. Most of this increase occurs during the first  $10^2$  seconds, which, for millimetre size droplets, can be regarded as the order of magnitude of the time  $t_2$  needed to approach chemical equilibrium in the liquid drop/solid system. During this time, the depth of the crater in the solid is greatest close to the triple line where the comparatively fresh liquid in contact with the solid causes a more rapid dissolution (Figure 2.19). At any instant, the apparent contact angle,  $\theta_{app}$ , is lower than the Young contact angle  $\theta_Y \cong \theta(t_1)$ . Finally, it should be noted that the macroscopic dihedral angle  $\theta_L$  is different from the true contact angle  $\Phi_1$  defined by the Smith equation (Figure 2.18.c). This is because at these relatively short times, the geometry of the system close to the triple line i.e., the value of  $\theta_L$ , is controlled by the diffusion process and not by interfacial energies. Indeed, as argued by Warren et al., based solely on diffusion and fluid flow, the liquid angle  $\theta_L$  “wants” to be near  $90^\circ$  since the liquid surface admits no-flux of solute and the liquid/solid interface is essentially an isoconcentrate. This is verified experimentally as shown by micrographs of the triple region for Bi-Sn/Bi (Figure 2.20), Al/Si (Nakae and Goto 1998) and Fe/C (Hara et al. 1995).

(iii) At much longer times, the shape of the solid/liquid interface will change to assume a uniform curvature. During this stage,  $\theta_L$  tends asymptotically towards  $\Phi_1$  while the contact radius  $R$  decreases towards a value  $R_3$  of less than  $R_1$  (Figure 2.18.d). However, this decrease in  $R$  starts only at  $t = 60$  h and  $R_3$  is approached at a time  $t_3$  estimated to be a few years!! This is because the shape change is driven by concentration differences along the S/L interface induced by curvature variations (equation (2.12)). For liquid metals, the Gibbs-Thomson parameter  $\Lambda$  is small (typically  $2 \times 10^{-10}$  m) which, combined with a small curvature ( $\kappa \approx (r_{drop})^{-1} \approx 10^3 \text{ m}^{-1}$ ), leads to extremely small concentration gradients along the interface ( $C_i - C_{eq} \approx 2 \times 10^{-7} C_{eq}$ ).

Calculations by Warren et al. for the second stage are in semi-quantitative agreement with experimental results. For instance, the calculated value of  $R_2/R_1$  at  $t = 300$  s is 1.07, lower but of the same order of magnitude as the experimental value of 1.26. To sum up, dissolution in metal/metal systems increases the contact

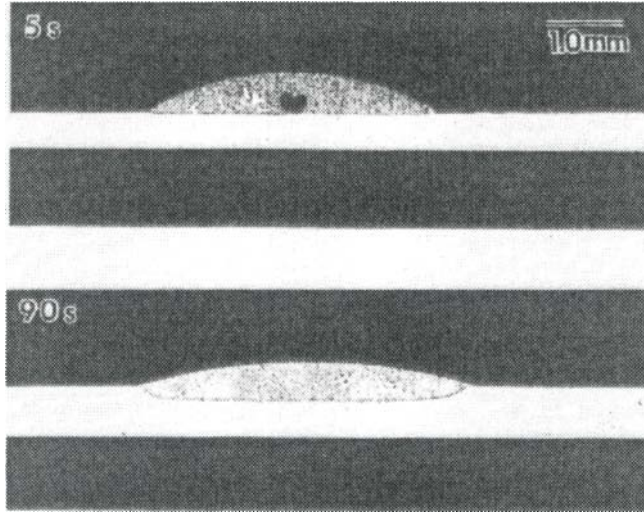
area between the liquid and the solid, mainly by increasing the available liquid (Yost and O'Toole 1998). In the absence of tensio-active effects, this increase of contact area is rather limited.



**Figure 2.19.** Calculated shape of the liquid region as a function of time for a Bi-30.5 at.% Sn drop on a Bi substrate at 245°C. Reprinted from (Warren et al. 1998) [7] with kind permission of the authors.

**2.2.1.2 Dissolution sensitive  $\sigma_{LV}$  and  $\sigma_{SL}$  values.** Much stronger increases in  $R$  are expected from dissolution of a tensio-active species able to decrease significantly  $\sigma_{SL}$  and/or  $\sigma_{LV}$ , even if the corresponding increase of the liquid volume is negligible. For example, for a droplet with  $\theta_Y = 40^\circ$ , a decrease of  $\sigma_{LV}$  of 30% is enough to increase the contact radius by a factor 2.

Laurent (1988) studied the particular case where dissolution is high enough to modify  $\sigma_{SL}$  (or  $\sigma_{LV}$ ) but small enough to allow neglect of any deviation of the S/L



**Figure 2.20.** Cross sections of Bi-30.5 at.% Sn drops on pure Bi substrates quenched at different times (5s and 90s). Reprinted from (Warren et al. 1998) [7] with kind permission of the authors.

interface from being planar. A typical example is a metal/oxide system, like Cu/NiO, see Section 6.4.1 and Table 6.8, in which slight dissolution of the oxide produces strong changes in  $\sigma_{SL}$  and  $\sigma_{LV}$ . Laurent examined how the driving force, given by equation (2.1) for the non-reactive case, is modified by dissolution. Using a free energy variation treatment, Laurent found that when dissolution does not affect  $\sigma_{SV}^0$  and  $\sigma_{LV}^0$  (the superscript 0 denotes the values of these quantities before reaction), the driving force of wetting can be described formally:

$$f_d(t) = \sigma_{SV}^0 - (\sigma_{SL}^0 + \Delta\sigma(t) + \Delta G(t)) - \sigma_{LV}^0 \cos \theta(t) \quad (2.13)$$

where  $\Delta\sigma(t)$  takes into account the change in  $\sigma_{SL}$  brought about by the reaction ( $\Delta\sigma(t) = \sigma_{SL}(t) - \sigma_{SL}^0$ ) and  $\Delta G(t)$  is the change of Gibbs energy per unit area released by the dissolution reaction at the interface.

Assuming that the mobility of the triple line (expressed by the velocity of the line in the corresponding non-reactive system for the same instantaneous contact angle) is high compared to the rate of interfacial transfer and to the diffusion rate in the bulk liquid, capillary equilibrium at the triple line is readily maintained, so that  $f_d(t) = 0$  and the instantaneous contact angle is given by:

$$\cos \theta(t) = \cos \theta^0 - \frac{\Delta\sigma(t)}{\sigma_{LV}^0} - \frac{\Delta G(t)}{\sigma_{LV}^0} \quad (2.14)$$

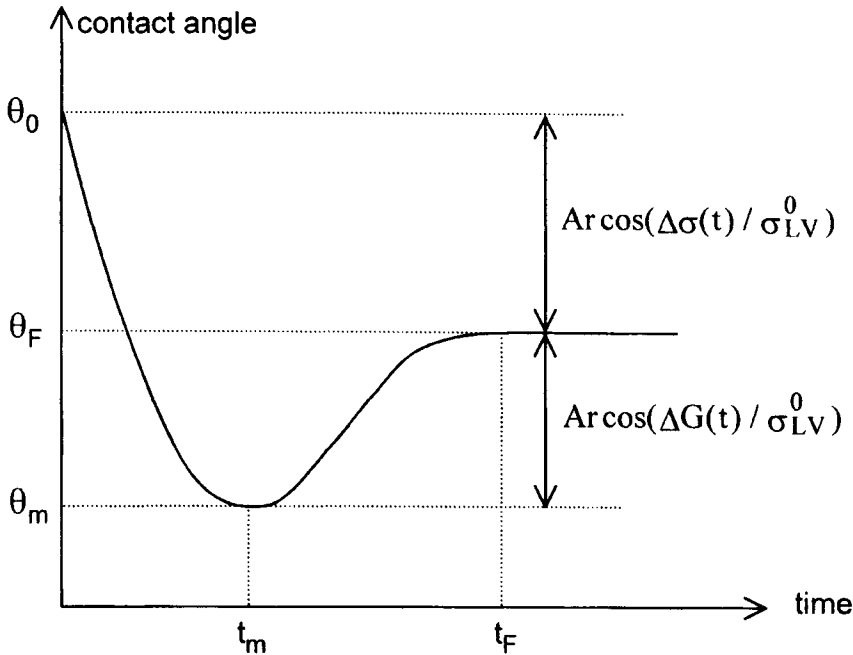
where  $\theta^0$  is the equilibrium contact angle in the absence of reaction.

The reaction energy term  $\Delta G(t)$  was first proposed by Aksay et al. (1974), both for dissolution reactions and for reactions with formation of a new phase at the interface. Aksay et al. considered that the energy produced by the reaction between the liquid and the solid at the periphery of the drop improves wettability. They argued that the effect of the  $\Delta G(t)$  term is strongest during the early stages of contact because the interfacial reaction rate is at its maximum when the liquid contacts a fresh solid surface, but thereafter the reaction kinetics decrease. Thus, the effect of the reaction is to cause an initial decrease in the contact angle, which then increases and gradually approaches the equilibrium value (Figure 2.21). Major difficulties lie in the calculation of the  $\Delta G(t)$  term because the coupling conditions of the time-dependent interfacial reaction with the kinetics of wetting are unknown. As a consequence, a calculation of the thickness of the reaction zone in “the immediate vicinity of the interface” is not yet possible.

The model of Aksay et al. predicts that the  $\theta$ - $t$  curve passes through a minimum. However, as a general rule, existing data for  $\theta(t)$  in reactive couples show that  $\theta$  decreases monotonically with time to a steady value. An exception is the Ag/SiC system in which transient decreases of  $\theta$  were observed and explained by means of the model of Aksay et al. (Li 1994). However it will be seen in Section 2.2.2.1 (see Figure 2.28) that the transient decreases of  $\theta$  in that system is not due to a  $\Delta G(t)$  term (reactivity in Ag/SiC is indeed very weak) but can be explained easily on the basis of changes in interfacial energies of the system.

Experiments carried out in a model system (Cu-Ag binary alloy) (Sharps et al. 1981) show no contact angle minimum but the results have been interpreted using Aksay's model because wetting for reactive combinations (for instance the Ag-Cu eutectic alloy on pure solid Cu) was better than for non-reactive couples (Ag-Cu eutectic alloy on Cu presaturated in Ag). Similar results were obtained by Naidich et al. (1965, 1971) who found that pure molten Ni (and other Fe group metals) wets graphite better than molten Ni presaturated with C. The above experiments were recently reassessed (Eustathopoulos 1996) using additional information now available for the same system (Ni/C (Hara et al. 1995)) and for similar systems (Cu/Fe (Eremenko et al. 1995)). From this new analysis, it appears that the different wetting behaviour observed in these equilibrium and non-equilibrium systems can be explained by surface energy effects taking into account the actual configuration at the triple line, without any contribution of a  $\Delta G$  term to the wetting driving force (Eustathopoulos 1996).



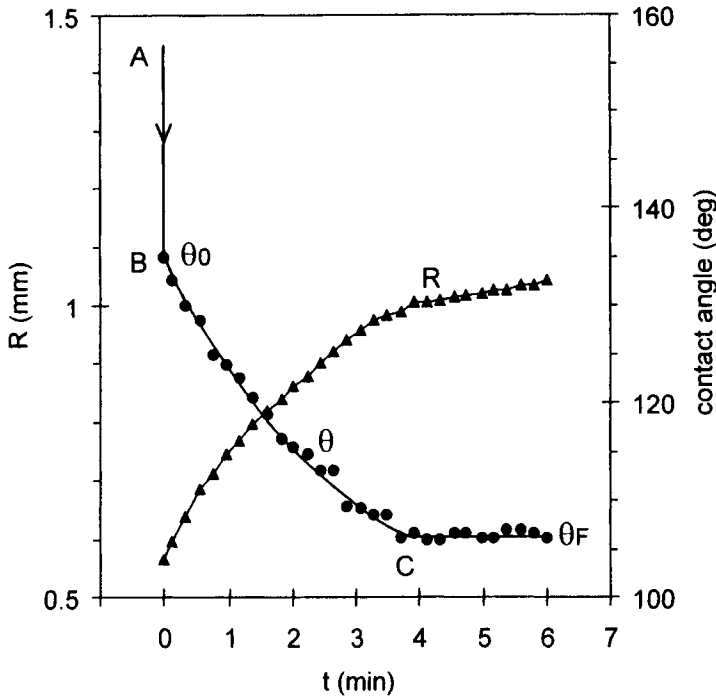


**Figure 2.21.** Contact angle versus time curve in a reactive system according to the model of Aksay et al. (1974).

Finally, the Aksay's model was used to explain the empirical correlation between reactivity and wettability observed in several metal/ceramic systems. It will be shown, for instance for metal/oxide couples (see Sections 6.4.1 and 6.5.2), that such a correlation can be explained by taking into account only the effect of reactions between liquid metals and oxides on interfacial energies.

According to the above discussion, the last term of the right hand side of equation (2.14) may be neglected, at least for systems with a weak or moderate reactivity. Therefore, any changes of contact angle for times much greater than  $10^{-2}$  second reflect changes with time of at least one of the three characteristic interfacial energies of the system. An example is a Cu-Si alloy on a  $\text{SiO}_2$  substrate studied by Rado (1997) using the dispensed drop technique (Figure 2.22). The first contact angle,  $\theta_0 = 135^\circ$ , is obtained in less than 0.04 second (the framerate of the video technique used in this experiment). Thereafter, the modification of  $\sigma_{\text{SL}}$  due to the interaction between Si and the surface of  $\text{SiO}_2$  (occurring as for the  $\text{Si}/\text{Al}_2\text{O}_3$  couple, see Section 6.3) leads to a significant decrease of the contact angle in about

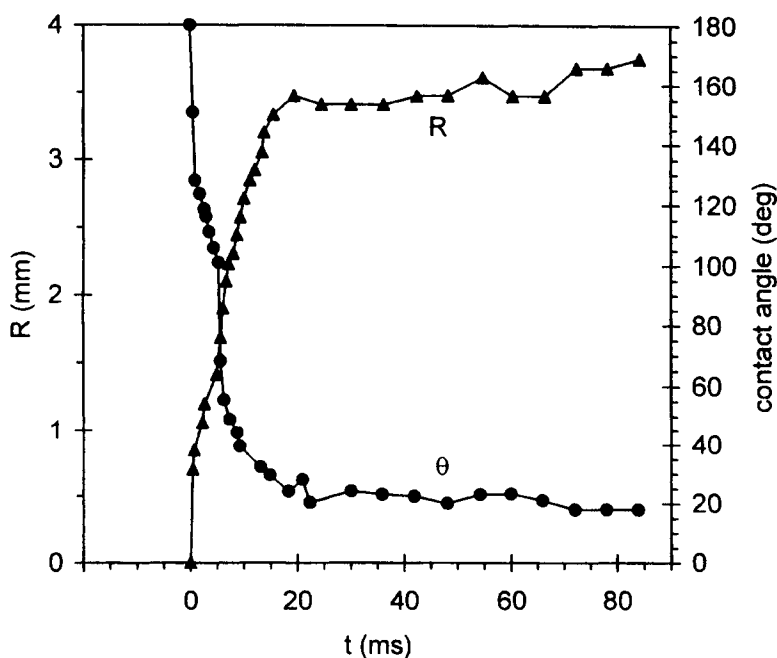
200 seconds. In this experiment, no significant dissolution of the substrate occurs, so that the S/L interface remains nearly planar.



**Figure 2.22.** Variation of contact angle and drop base radius with time for a Cu-25 at.% Si alloy on  $\text{SiO}_2$  at  $1150^\circ\text{C}$ . The duration of the A-B stage is shorter than 0.04 s. From (Rado 1997).

In many metal/ceramic systems with weak or moderate reactivity, interfacial reactions may be slow at relatively low temperatures, thus allowing the non-reactive stage (step A-B on Figure 2.22) and reactive stage (step B-C) to be separated. However, interfacial reactions at high temperature can be so fast for systems with a high reactivity, that the A-B and B-C stages cannot be separated (similarly, in some reactive glass/ceramic systems, these two stages can overlap because of a slow non-reactive stage due to the high viscosity of the glass). An example is Ni/SiC, a system in which Ni can dissolve up to 40 at.% Si at  $1500^\circ\text{C}$ . In Figure 2.23, one can see that the spreading rate for this system, measured by the transferred drop technique, is as high as that for non-reactive systems, with an initial spreading rate close to 1 m/s (Grigorenko et al. 1998). The contact angle

observed after 20 ms ( $\theta \cong 20^\circ$ ) is nearly equal to that measured for a Ni-40 at.% Si alloy on monocrystalline SiC (Rado et al. 1999). This good agreement can be explained for the Ni/SiC system by a rapid saturation of the interface in Si, and by the fact that the spreading time (20 ms) was too short to cause a heavy corrosion at the interface and creation of a significantly non-planar interface. Note that for the Ni/SiC system, high contact angles (in the range  $50\text{--}70^\circ$ ) were observed by several investigators in experiments in which the first observation was possible only at  $t > 1\text{ s}$ . At these times, interfacial reaction leading to graphite precipitation strongly perturbs the configuration of the triple line and therefore only apparent contact angles were observed.



**Figure 2.23.** Variation of contact angle and drop base radius with time for Ni on SiC at  $1500^\circ\text{C}$ . Data from work reported in (Grigorenko et al. 1998).

### 2.2.2 Formation of 3D compounds

This Section focusses on interfacial reactions that cause the formation of *dense* 3D layers of solid reaction product. It will be assumed that the thickness of the layer is

negligible compared to the drop size so that the layer does not disturb the measurement of the macroscopic contact angle. Moreover, although interfacial reactions occurring during spreading can be highly exothermic, the temperature is assumed to remain constant. This assumption seems reasonable in the sessile drop configuration, at least for spreading rates lower than  $100 \mu\text{m/s}$ , but it is much more questionable for infiltration of a porous medium (Mortensen et al. 1998).

**2.2.2.1 Driving force for reactive wetting.** As with dissolutive wetting, the general expression for the driving force at any time  $t$  is given by expression (2.13) in which  $\Delta\sigma(t)$  now represents the change in the S/V and S/L surface and interfacial energies brought about by the reaction. For the sake of simplicity, the L/V surface energy is taken to be unchanged. The  $\Delta G(t)$  term is the change in Gibbs energy of the system due to the formation of a new compound.

During the last few decades, reactive wetting has been explained usually by reference to the  $\Delta G(t)$  term. Accordingly, it has been concluded that the higher the reactivity in a system, the better the wettability. This conclusion has been tested recently by experiments in which the  $\Delta G(t)$  term was varied but the surface energy term was kept constant (Espie et al. 1994, Landry et al. 1997). An example is the wetting behaviour of a CuPd-Ti alloy of fixed composition on two oxide substrates of different thermodynamic stability ( $\text{Al}_2\text{O}_3$  and  $\text{SiO}_2$ ). In these systems, Ti reacts with both oxides leading to the same interfacial product ( $\text{Ti}_2\text{O}_3$ ) but reactivity, as measured by the thickness  $e$  of the  $\text{Ti}_2\text{O}_3$  layer, differed by an order of magnitude. Despite this difference, the wetting of the two substrates was nearly the same (Table 2.1).

**Table 2.1.** Interfacial chemistry and final contact angle for CuPd-15 at.% Ti on  $\text{Al}_2\text{O}_3$  and  $\text{SiO}_2$  substrates at 1473K (Espie et al. 1994).

Substrate	Interfacial product	Thickness $e$ ( $\mu\text{m}$ )	$\theta_F$ (deg)
$\text{Al}_2\text{O}_3$	$\text{Ti}_2\text{O}_3$	0.5	$34 \pm 2$
$\text{SiO}_2$	$\text{Ti}_2\text{O}_3$	10	$36 \pm 2$

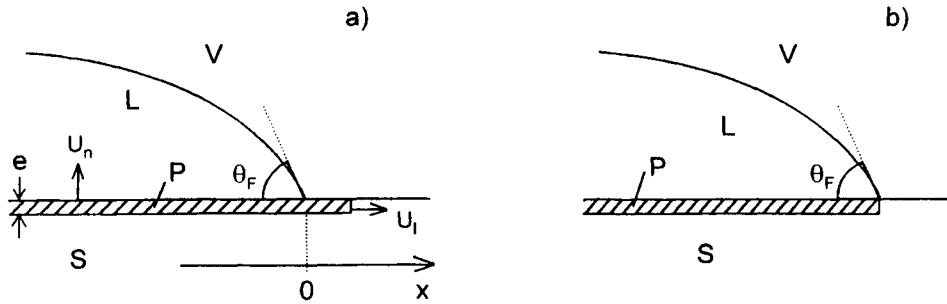
From these results and other experiments (Kritsalis et al. 1994, Landry et al. 1996, Landry et al. 1997), it has been concluded that wetting in reactive systems is governed by the final interfacial chemistry at the triple line rather than by the intensity of interfacial reactions. The key question is to determine the interfacial

configuration that defines the final contact angle  $\theta_F$  of the system. Two cases will be considered depending on the difference in wetting between the reaction product and the substrate.

**Reaction product more wettable than the substrate.** Two configurations, one stable and the other metastable, can be produced at the triple line when the final contact angle  $\theta_F$  is attained. The *stable* configuration depends on a layer of reaction product P extending on the free surface of the substrate S (Figure 2.24.a). Neglecting any effect of roughness of the reaction layer,  $\theta_F$  is simply given by the Young equation (1.16) applied to the P/L/V system:

$$\cos \theta_F = \cos \theta_P \cong \frac{\sigma_{PV} - \sigma_{PL}}{\sigma_{LV}} \quad (2.15)$$

in which  $\theta_P$  represents the equilibrium contact angle on the reaction product P.



**Figure 2.24.** Possible configurations of a reacting system at the solid/liquid/vapour triple line when the steady-state contact angle is reached.

In the *metastable* configuration, the reaction product layer does not extend beyond the edge of the drop (Figure 2.24.b). As a consequence, the final contact angle  $\theta_F$ , calculated by considering the effect of a small displacement of the triple line around the equilibrium position, is:

$$\cos \theta_F \cong \frac{\sigma_{SV} - (\sigma_{SP} + \sigma_{PL})}{\sigma_{LV}} \quad (2.16)$$

The configuration of Figure 2.24.b is possible if the extension of the reaction layer outside the P/L interface is blocked by thermodynamic barriers. The size of the barriers can be calculated by considering the change of the Gibbs energy  $G$  per unit length of triple line produced by a lateral extension  $\delta x$  of the reaction product layer outside the drop (Figure 2.24.a). Thus

$$\delta G = \Delta G_v e \delta x + (\sigma_{PV} + \sigma_{PS} - \sigma_{SV}) \delta x = \Delta G_v e \delta x + \Delta \sigma \delta x \quad (2.17)$$

where  $\Delta G_v$  is the Gibbs energy of the reaction per unit volume of P. Setting  $d(\delta G)/d(\delta x) = 0$ , a critical layer thickness  $e^*$  is obtained such that:

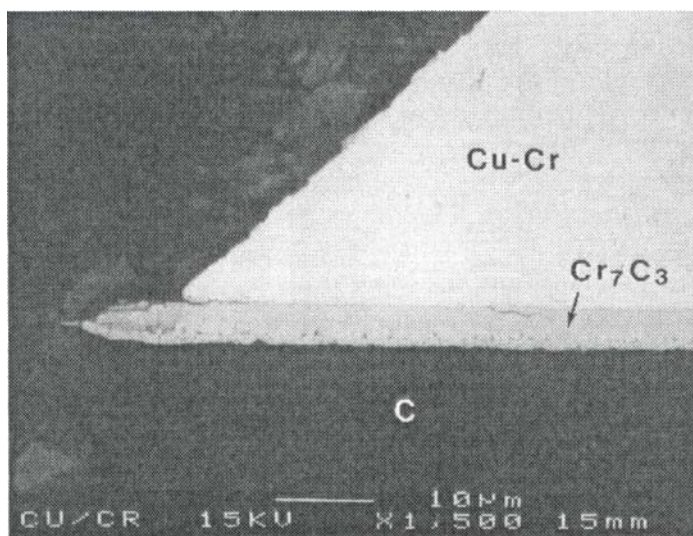
$$e^* = - \frac{\Delta \sigma}{\Delta G_v} \quad (2.18)$$

For  $e > e^*$ , no thermodynamic barrier to the extension of reaction product outside the drop exists, while for  $e < e^*$ , the configuration of Figure 2.24.b, corresponding to a metastable equilibrium, is possible. Taking typical values  $\Delta \sigma = 1 \text{ J.m}^{-2}$  and  $|\Delta G_v| = 10^9 \text{ to } 10^{10} \text{ J.m}^{-3}$ , we find that  $e^*$  is of the order of 1 nm. Such values of  $e^*$  are too low to create a true barrier to the formation of product P outside the drop. Indeed, the slightest growth of P in a direction perpendicular to the interface i.e., towards the interior of the liquid, would be sufficient to destroy such barriers. Note that in the few cases where the thickness of the reaction layer in the vicinity of a triple line was measured, it was found to vary from several tens of nm to a few microns (Eustathopoulos 1998). In conclusion, except for very large and unrealistic  $\Delta \sigma$  values, or extremely low values of  $|\Delta G_v|$  (in this case even the condition of a continuous layer of P becomes questionable), thermodynamic barriers to the lateral growth of P on the substrate free surface are unlikely. Therefore, the final configuration expected in reactive wetting is that of Figure 2.24.a. Note that once this configuration is attained, the growth of P layer continues both inside the liquid (by diffusion through the P layer) and over the substrate free surface (for instance by evaporation/condensation or by surface diffusion). So far as this growth does not produce any significant change of liquid composition,  $\theta_F$  (equation (2.15)) remains nearly constant with time.

An example which confirms the validity of equation (2.15) is Au-Ti alloy on  $\text{Al}_2\text{O}_3$ . Pure Au does not wet  $\text{Al}_2\text{O}_3$  (at  $1150^\circ\text{C}$ ,  $\theta_0 = 135^\circ$ ) but a Au-6 at.% Ti alloy wets this substrate ( $\theta = 69^\circ$ ) due to the formation of  $\text{Ti}_2\text{O}_3$  at the interface (Zhuravlev and Turchanin 1997). Effectively, the same angle is displayed ( $\theta = 67^\circ$ )

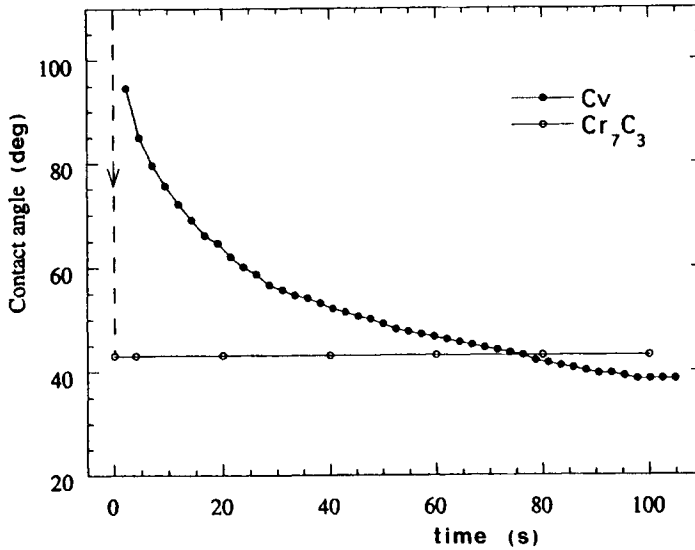
when Au-6 at.% Ti is used to wet a  $\text{Ti}_2\text{O}_3$  substrate (Naidich 1981), in agreement with equation (2.15).

A slightly different procedure was used in another experiment performed with a Cu-1 at.% Cr alloy on a vitreous carbon substrate (Landry et al. 1997). Cr promotes wetting, forming at the interface a continuous layer a few micron thick of the wettable, metal-like,  $\text{Cr}_7\text{C}_3$  carbide (Figure 2.25). After cooling, the solidified Cu-Cr drop was dissolved, a small quantity of a Cu-1 at.% Cr alloy was placed in the center of the Cr carbide layer and a second wetting experiment was performed at the same temperature. The plots in Figure 2.26 clearly show that the steady contact angle in the reactive Cu-Cr/C system is nearly equal to that in the non-reactive Cu-Cr/ $\text{Cr}_7\text{C}_3$  system, but the wetting kinetics are very different. Those for the non-reactive couple are fast but those for the reactive couple are slow because the wettable  $\text{Cr}_7\text{C}_3$  “substrate” is fabricated *in situ* and this takes a significant time.



**Figure 2.25.** SEM micrograph of a cross-section perpendicular to the interface of a Cu-Cr alloy on vitreous carbon cooled from 1373K at steady state contact angle. From (Landry et al. 1997) [8].

Thus, the final contact angle in a reactive system leading to the formation at the interface of a dense 3D compound is given with good accuracy by the Young contact angle of the liquid on the reaction product,  $\theta_P$ . Replacing  $\theta_F$  by  $\theta_P$  in equation (2.1), the reactive wetting driving force for  $\theta < \theta_0$  is written:



**Figure 2.26.** Contact angle versus time curves for a Cu-1 at.% Cr alloy on vitreous carbon and Cr<sub>7</sub>C<sub>3</sub> at 1373K. From (Landry et al. 1997) [8].

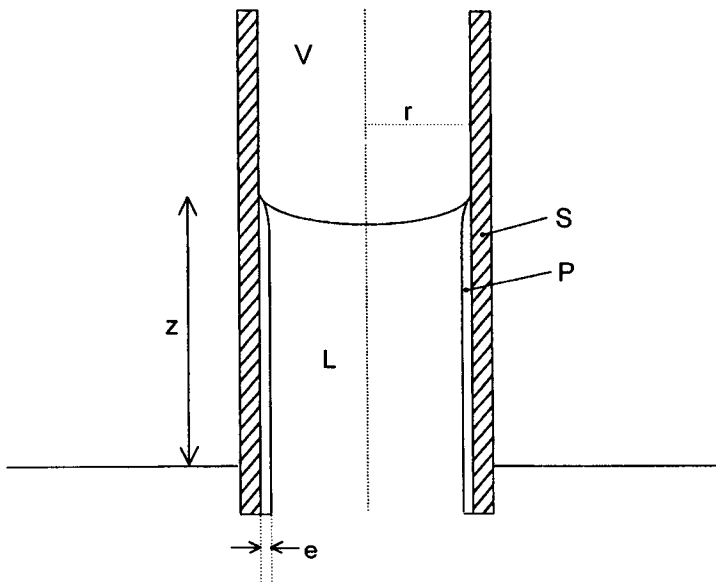
$$f_d(t) = \sigma_{LV}^0 [\cos \theta_P - \cos \theta(t)] \quad (2.19)$$

Several complications can produce differences between the value of the observed contact angle and the value  $\theta_P$  given by equation (2.15). First, differences can result from roughness of the reaction product surface. In the case of the Cu-Cr/C system, the roughness of the Cr carbide layer formed at the interface is only a few tens of nanometers (Landry et al. 1997). As a result, the reproducibility of  $\theta_F$  values ( $41 \pm 4^\circ$ ) was found to be comparable with that for non-reactive systems (see Section 3.3). However, the roughness of Al<sub>4</sub>C<sub>3</sub> formed by the Al/C system seems to be much higher (Landry and Eustathopoulos 1996b) and this can be one of the reasons for the comparatively high dispersion of experimental results obtained for this couple.

Another complication arises from the continuous change in the concentration of reactive solute resulting in changes of the L/V and L/S energies of the system. The concentration change depends on the value of the ratio  $HX/e$ , where  $H$  is the height of the drop,  $X$  the molar fraction of reactive element in the liquid and  $e$  the thickness of the reaction product  $P$ . The higher the value of this ratio, the smaller the change in  $X$  due to the growth of the compound  $P$ . Usually, when  $e$  becomes thicker than a few microns, the growth rate  $U_n$  normal to the S/L interface (see



Figure 2.24.a) is greatly decreased in accord with a parabolic law. Similarly, the lateral growth rate  $U_l$  decreases also with  $x$  because the source of reactive atoms for the spreading of P gets farther and farther away. For millimetre size droplets and not too low  $X$  values, it can be seen that in many cases changes in concentration in the liquid becomes negligible. For instance, wetting of a Cu-40 at.% Si droplet on vitreous carbon is due to the formation at the interface of a SiC layer of 0.1 to 0.5  $\mu\text{m}$  in thickness (Landry et al. 1997). This requires a consumption of only about  $10^{-3}$  of the Si molar fraction, a negligible change compared to the initial value of 0.4. For this reason, a nearly constant contact angle is observed at the end of spreading.



**Figure 2.27.** Capillary rise in a reactive solid/liquid system due to the formation of a wettable reaction product P.

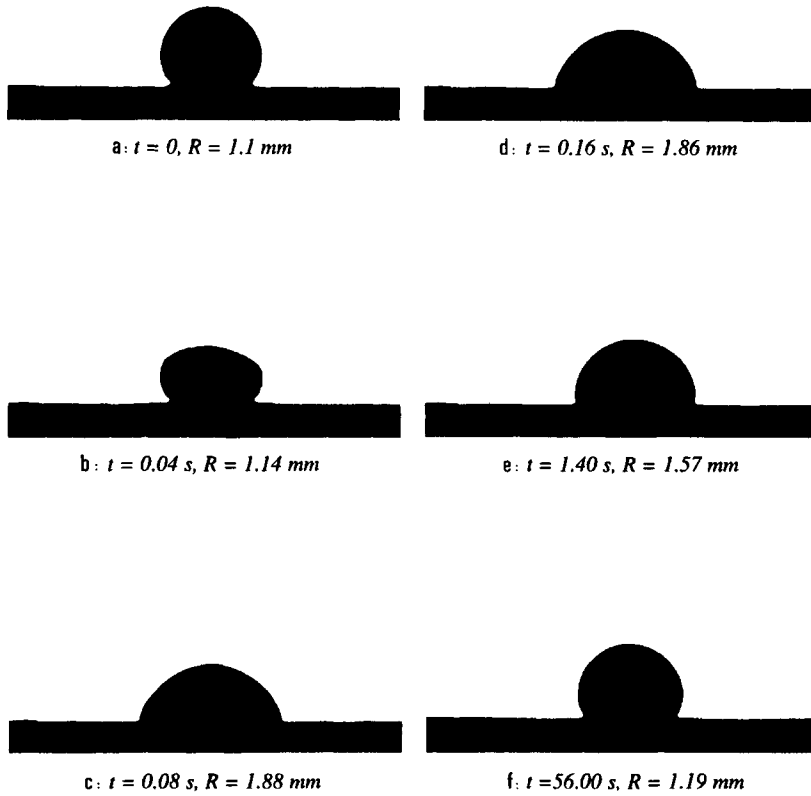
However, concentration changes will be much higher in other configurations, for instance when the liquid wets a capillary tube of small radius  $r$  (Figure 2.27). In this case, a gradient of  $X$  will be established along the liquid column such that the final capillary height  $z$  would be lower than the nominal value  $z^0 = 2\sigma_{LV} \cos \theta_F(X^0)/(r\rho g)$  given by equation (1.55), where  $\theta_F(X^0)$  is the steady contact angle as measured in a classical sessile drop experiment with a millimetre

size droplet and the nominal molar fraction of reactive solute  $X^0$ . When the capillary stands in a large volume of liquid, diffusion of reactive solute from the liquid to the infiltration front occurs, and at longer times  $z$  will tend towards the nominal value  $z^0$ . Otherwise, the capillary rise will be much lower than predicted by sessile drop experiments. Clearly, in reactive systems, one must pay attention when  $\theta_F$  values measured for a sessile drop configuration have to be transferred to other configurations with different volume/interface ratios.

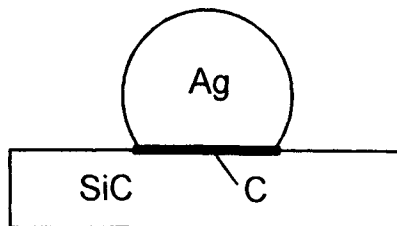
**Reaction product less wettable than the substrate.** The above discussion concerns systems in which the new compound formed at the interface is more wettable than the initial substrate. We will now consider the opposite case and take as an example the Ag/SiC couple (Figure 2.28). In this system, molten Ag reacts slightly with SiC forming Si dissolved in Ag and graphite (at 1100°C the molar fraction of Si in Ag in equilibrium with  $\alpha$ -SiC is about  $4 \times 10^{-3}$ ). Ag wets SiC before reaction ( $\theta \ll 90^\circ$ ) but not graphite ( $\theta \gg 90^\circ$ ) (see Table 7.2 and Section 8.1).

When a piece of Ag is placed on SiC and the temperature is raised and stabilized at a value higher than the metal melting point, the contact angle is close to  $120^\circ$ . Chemical analysis by Auger electron spectroscopy of the interface after cooling and elimination of the metallic phase indicates the formation of graphitic carbon, whose thickness is in the nanometre range, while the adjacent surface is found to be SiC. However, the configuration of Figure 2.29 is not stable. A slight perturbation can allow the liquid to contact fresh SiC substrate. This perturbation was produced by increasing the temperature, which led to a small decrease of  $\theta$  of Ag on C but sufficient for the Ag to expand on to the SiC. This produced a substantial lateral displacement of the drop on the substrate (Figure 2.28.b), driven by the decrease of the surface energy of the system when the Ag/C interface is replaced by an Ag/SiC interface, followed by a fast spreading up to  $\theta = 65^\circ$  (Figure 2.28.c). Thereafter, a graphite layer was formed again at the interface and caused a dewetting process up to a contact angle close to  $120^\circ$  (Figure 2.28.d to f).

This example shows that, when the contact angle on the reaction product,  $\theta_P$ , is higher than the contact angle on the substrate,  $\theta_S$ , and in the absence of perturbation, the final contact angles  $\theta_F$  are characteristic of the reaction product and not of the initial substrate ( $\theta_F \approx \theta_P$ ). This is the same conclusion as that drawn in the previous Section for the case when  $\theta_P$  is lower than  $\theta_S$  (equation (2.15)).

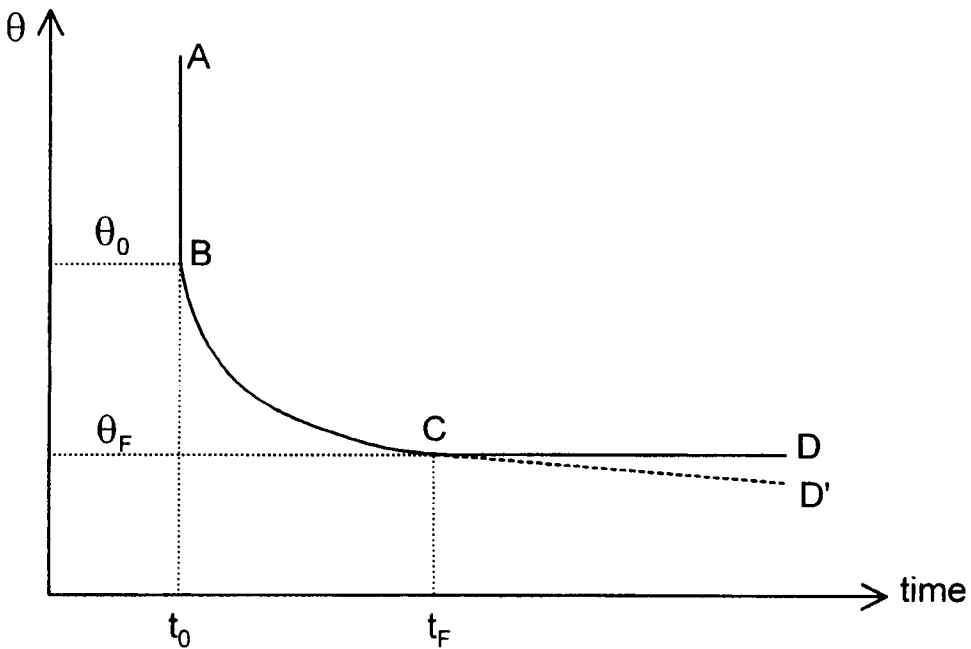


**Figure 2.28.** Successive images of a Ag drop on SiC ( $R$  : drop base radius). (a): initial steady configuration corresponding to a time taken arbitrarily equal to zero. (b): the droplet moves rapidly (with a velocity higher than 20 mm/s) towards a fresh SiC surface until it is stopped by the edge of the substrate. (c): spreading of the drop on SiC. (d to f): dewetting of the drop up to a final contact angle characteristic of a graphite substrate. From (Rado et al., in press).



**Figure 2.29.** Schematic representation of a Ag sessile drop on a SiC substrate. Wetting is blocked by the non-wettable reaction product (graphite) formed at the interface.

**2.2.2.2 Spreading kinetics.** The general  $\theta$ - $t$  curve observed at constant temperature is given schematically on Figure 2.30. The A-B step corresponds to the non-reactive wetting. The B-C step is due to the formation of the new compound. In some cases, a drift (C-D' step) is observed at long times resulting either from modification of the composition of the liquid (for instance by evaporation or interdiffusion with the solid) or from the modification of the solid surface (for instance by grain-boundary grooving, see Appendix H). For liquid metals on solid metals,  $\theta_0$  and  $\theta_F$  are not very different (it can be seen in Chapter 5 that the contact angles of a liquid metal on another metal and on an intermetallic compound are relatively close). In contrast, in several metal/oxide or metal/C systems,  $\theta_0$  is much higher than  $\theta_F$ . Moreover, in these systems, the two stages A-B and B-C usually have clearly different time scales and can be easily identified (for instance  $t_0 \approx 10^{-2}$  s and  $t_F \approx 10^2$ – $10^4$  s). For this reason, the mechanisms of spreading kinetics have been mainly studied in metal/ceramic systems.



**Figure 2.30.** Schematic contact angle versus time curve during reactive wetting with formation of a new compound at the interface.

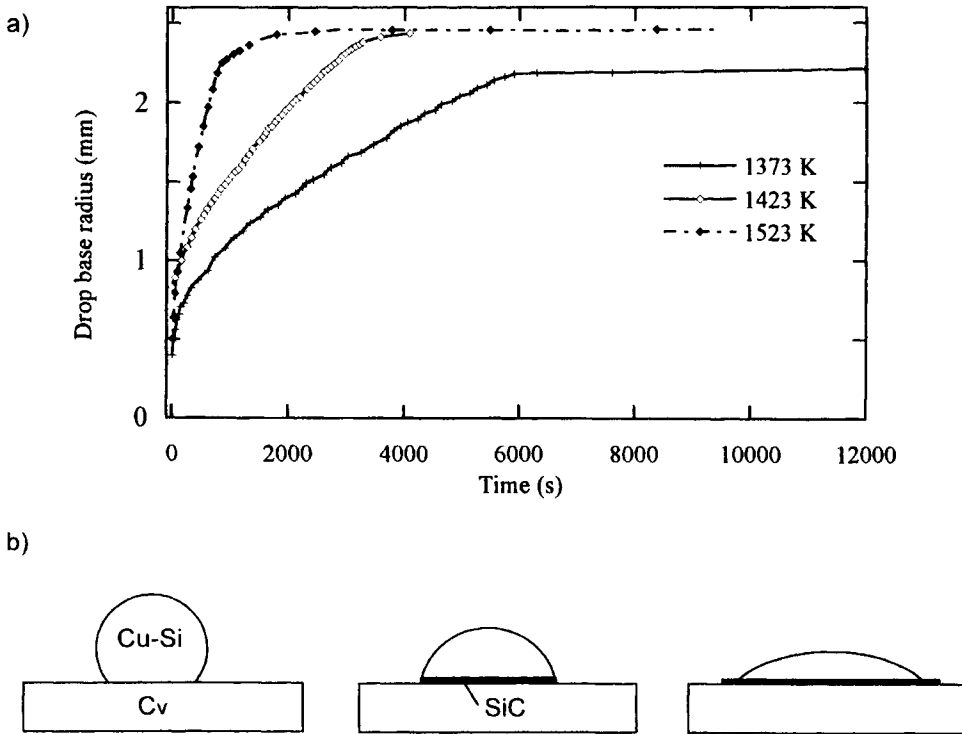
In the following, we consider a non-reactive liquid metal solvent A containing a reactive solute B that is in contact with a solid substrate. It is assumed that the reaction product P is better wetted by the A-B alloy than the initial substrate. Spreading kinetics will be discussed by means of the classical two-step scheme used in treating kinetic phenomena in materials science, consisting of a local process at the interface and transport phenomena in bulk materials. The only difference when considering reactive wetting, but an important one, is that the significant localised effects occur not at a 2D interface but at a 1D defect, the contact line between three phases S, L and V. At the line, *coupling between reaction and wetting processes* is established. Indeed, because the liquid wets the reaction product, the liquid is continuously in contact with (or close to) unreacted solid at the triple line. As a result, the reaction rate at this particular point is two to three orders of magnitude higher than that at the interface far from the triple line where the reaction occurs by slow diffusion through a solid layer (Landry and Eustathopoulos 1996b). On the other hand, reactivity is essential for wetting because it provides the wettable compound. Note that when  $\theta = \theta_F$ , spreading stops but the lateral extension of the reaction product continues. However, because the liquid source and the reaction front get farther and farther apart, the reaction slows down strongly (see Figure 2.31.b).

Within the framework of this general description, two limiting cases can be defined depending on the rate of the chemical reaction at the triple line compared to the rate of diffusion of reactive solute from the drop bulk to the triple line (or of a soluble reaction product from the triple line to the drop bulk). Note that this description does not need the knowledge of the detailed (and complicated) configuration close to the triple line, i.e., inside a small volume a few nm (or tens of nm) in diameter.

**Reaction-limited spreading.** In this first limiting case, chemical kinetics at the triple line are rate-limiting because diffusion within the droplet is comparatively rapid (or not needed when the drop is made of a pure reactive metal). In this case, (i) if the reaction does not change the global drop composition significantly so that the chemical environment of the triple line is constant with time and (ii) if a stationary configuration is established at the triple line during wetting, then the rate of reaction  $U_r$  (expressed in  $\text{mole.m}^{-2}.\text{s}^{-1}$ ) and hence the triple line velocity are constant with time (Landry and Eustathopoulos 1996b, Dezellus et al. 1998). Then, writing a mass balance at the triple line and denoting by  $v_m^P$  the molar volume of P, the velocity of the triple line for a reaction of the type  $M + S \rightarrow MS$  (where S is the solid substrate) is:

$$\frac{dR}{dt} = U_r \cdot v_m^P = K_2 v_m^P \exp\left(\frac{-\Delta G^*}{RT}\right)(a_B - a_B^{eq}) \quad (2.20)$$

where  $a_B^{eq}$  is the value of the activity of reactive solute B in the liquid which is in equilibrium with the substrate and the reaction product P.  $\Delta G^*$  is the activation Gibbs energy of the reaction and  $K_2$  is a constant.



**Figure 2.31.** (a) Spreading kinetics of Cu-40 at.% Si alloy on vitreous carbon. (b) Schematic representation of interfaces at the beginning of spreading (left), during the linear stage (middle) and in the plateau (right). From (Dezellus et al. 1998).

An example is the behaviour of Cu-Si alloys on vitreous carbon (Dezellus et al. 1998). In this system, wetting is promoted by the formation of a continuous layer, a

few tens of nm thick, of SiC, produced by Si concentrations higher than 15 at.%. Variations of drop base radius as a function of time at various temperatures are shown in Figure 2.31.a. The initial contact angle measured within 0.04 s is about  $160^\circ$  and thereafter, two main stages are observed for the  $R(t)$  curve. In the first stage,  $R$  increases parabolically with time. It is assumed that during this stage a steady-state growth is not still established due to incomplete covering of the S/L interface by the reaction product (Landry and Eustathopoulos 1996b). During the second stage, a steady configuration is established at the triple line and, as a result, the reaction rate and the triple line velocity are nearly constant with time. During this stage, the macroscopically observed contact angle is not related to capillary force equilibrium but is dictated by the drop volume and the radius of the reaction product layer (Figure 2.31.b middle). Indeed, the advance of the liquid is hindered by the presence of a non-wettable vitreous carbon surface in front of the triple line. Thus, the only way to move ahead is by lateral growth of the wettable SiC layer until the macroscopic angle equals the equilibrium contact angle of the liquid on SiC ( $\cong 40^\circ$ ). Then, the drop radius remains nearly constant while beyond the drop the reaction layer continues to extend but very slowly.

The Arrhenius activation energy  $\Delta G^*$  in equation (2.20) obtained for Cu-Si alloys of constant composition is close to  $250 \text{ kJ.mol}^{-1}$  which is of the order of magnitude expected for a chemical reaction.

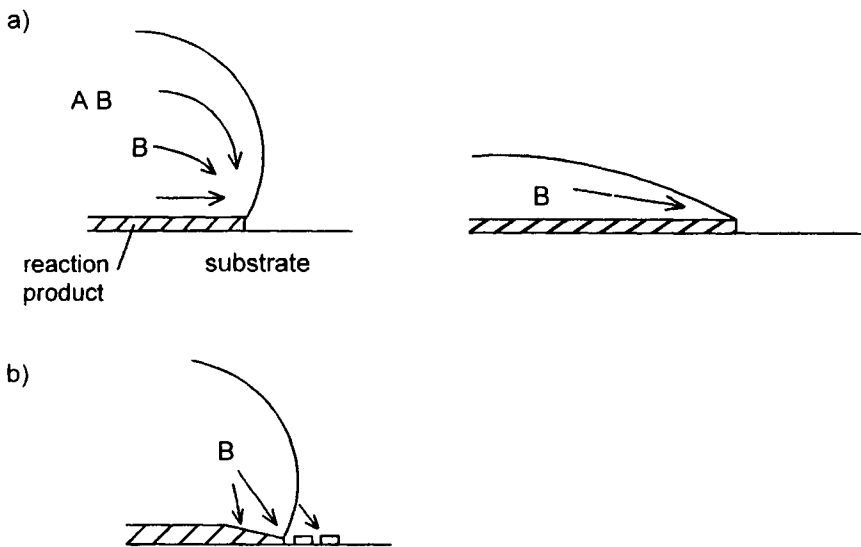
In this description, it is assumed that the formation of the reaction layer occurs only in the vicinity of the triple line. This does not take into account the possible effect of a reaction occurring ahead of the triple line to where the reactive species can be transferred by evaporation/condensation or by diffusion in the gas or by both processes. When the free surface of the droplet forms an acute angle through the vapour phase with the substrate, evaporation/condensation can provide a parallel transport path for Si from the drop to the triple line (see Figure 2.32.b). This should accelerate  $dR/dt$  to an extent that increases as  $\theta$  exceeds  $90^\circ$  and may be partially responsible of the parabolic branch of  $R(t)$  observed at the beginning of spreading (Figure 2.31.a) (Dezellus et al. 1998).

“Linear wetting” can occur in different systems and for different types of reaction. Examples are Cu-Si alloys on oxidized SiC (Rado 1997), the reactive CuAg-Ti/ $\text{Al}_2\text{O}_3$  system (Nicholas and Peteves 1995) or the Al/vitreous carbon system (Landry and Eustathopoulos 1996b). For the last system, small but significant deviations from linearity were observed when  $\theta$  tends towards  $\theta_F$  and attributed to roughness of the reaction product layer delaying the movement of the triple line by pinning.

For systems exhibiting linear wetting, it is expected that the spreading rate will be sensitive to the structure of the solid. Indeed, in the Al/C system, the spreading

rate in the linear stage was found to vary by a factor 4 between vitreous carbon and pseudo-monocrystalline graphite (Drevet et al. 1996) (see also Figure 8.7).

**Diffusion-limited spreading.** When local reaction rates are comparatively high, the rate of lateral growth of the reaction product at the triple line is limited by the diffusive supply of reactant from the drop bulk to the triple line. Because the contact angle decreases continuously during wetting, the reduction in diffusion field will lead to a continuous decrease in the reaction rate and, as a result, of the rate of movement of the triple line itself (Figure 2.32.a). Therefore time-dependent spreading rates are expected in this case (Landry and Eustathopoulos 1996b).



**Figure 2.32.** Diffusion limited spreading. (a) In the model configuration used in the analysis of Mortensen et al. (1997), the decrease of the triple line velocity with time is due to the reduction in diffusion field close to the triple line. (b) More realistic description of the reaction around the triple line.

In general, solutes are transported in the liquid by convection and diffusion and the governing equation is Fick's second law written in the referential of the triple line moving with a velocity  $U$  ( $U = dR/dt$ ):



$$\frac{\partial C}{\partial t} + \mathbf{u} \cdot \nabla C = D \nabla^2 C + \mathbf{U} \cdot \nabla C \quad (2.21)$$

In this equation, the concentration  $C$  of reactive species is expressed as a mass fraction.  $\mathbf{u}$  denotes the local velocity of the fluid and results both from the movement of the triple line and from convection caused by temperature and concentration gradients in the liquid.

Given the complexity of the real situation in the sessile drop configuration, a simplified analysis has been proposed by Mortensen et al. (1997). This neglects reactions at the interface far from the triple line and assumes that diffusion is the dominating mechanism for solute transport in a small volume near the triple line. Inside this volume, modelled as a straight wedge of angle  $\theta$ , the velocity  $\mathbf{u}$  is taken equal to  $\mathbf{U}$  so that equation (2.21) reduces to

$$\frac{\partial C}{\partial t} = D \nabla^2 C \quad (2.22)$$

Solving this equation, the triple line velocity of a drop of base radius  $R$ , containing a reactive solute at a concentration  $C_0$  (expressed in mole per unit volume), is found to depend on the instantaneous contact angle as follows:

$$\frac{dR}{dt} = \frac{2DK_3}{en_v} (C_0 - C_e) \theta \quad (2.23)$$

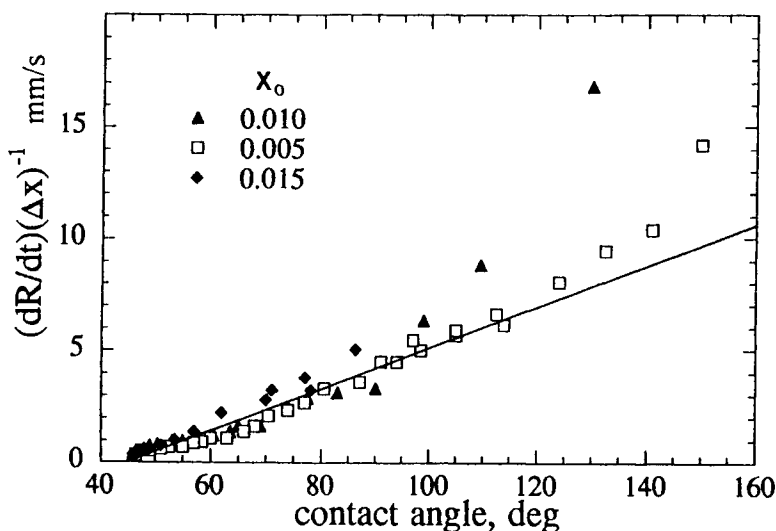
where  $D$  is the diffusion coefficient in the liquid phase,  $n_v$  is the number of moles of reactive solute per unit volume of the reaction product,  $e$  is the reaction product thickness at the triple line,  $C_e$  is the concentration of reactive solute in equilibrium with the reaction product and  $K_3$  is a constant close to 0.04. For modest contact angles,  $\theta < 60^\circ$ , the contact angle of a spherical cap can be approximated by  $\theta = 4v/(\pi R^3)$ . Introducing this into equation (2.23) yields:

$$R^4 - R_0^4 = \text{const. } vt \quad (2.24)$$

where  $v$  is the drop volume and  $R_0$  is the initial drop radius.

The most complete study so far used the Cu-Cr/vitreous carbon system and the transferred drop technique (Voitovich et al. 1998, 1999). In this system, the transition from large, non-wetting, contact angles to low wetting contact angles (Figure 2.26) is due to the formation of a continuous layer of a wettable  $\text{Cr}_7\text{C}_3$  compound along the S/L interface. For all experiments, the final contact angle was

nearly the same ( $\theta_F \cong 40^\circ$ ) and close to that of Cu-Cr alloy on a substrate of  $\text{Cr}_7\text{C}_3$  (see Figure 2.26).



**Figure 2.33.** Composition normalised triple line velocity as a function of the instantaneous contact angle in the Cu-Cr/vitreous carbon system at 1373K with drop mass of about 100 mg.  $\Delta X$  is equal to  $(X_0 - X_e)$  where  $X_0$  and  $X_e$  are the initial and equilibrium molar fractions of Cr respectively. From data of (Voitovich et al. 1998) [9].

In agreement with the analysis of Mortensen et al. (1997) (equations (2.23) and (2.24)), the experimental data in the Cu-Cr/vitreous carbon system show that the spreading rate normalised by reference to the molar fraction of solute depends only on the contact angle (i.e. on the instantaneous geometry of the drop) in an approximately linear way (Figure 2.33). Discrepancies with the predictions of the analysis are observed, however, in that (i) at angles higher than  $90^\circ$ , there is an upward deviation in the spreading rate from the linear relation with  $\theta$  observed at lower angles, and (ii) the intercept of the line of  $dR/dt$  versus  $\theta$  with the  $\theta$  axis is not at the origin ( $\theta = 0$ ), but near  $\theta = 45^\circ$ . The deviation from linearity observed at  $\theta > 90^\circ$  can be explained by a reaction occurring ahead of the triple line caused by evaporation of solute from the drop surface during the spreading process (Figure 2.32.b), as discussed above for the Cu-Si/vitreous carbon system. The second discrepancy at low contact angles is attributed to continued drop/substrate chemical reaction behind the triple line. Such a reaction can influence spreading

kinetics first by causing a gradual lowering of the bulk drop concentration with time, and second by diverting solute flux lines away from the triple line, towards the solid/liquid interface (Figure 2.32.b) (Voitovich et al. 1999). Numerical calculations taking into account this phenomenon seem to confirm this interpretation (Hodaj et al., to be published).

Note that equations (2.23) and (2.24) neglect convection. In the sessile drop configuration, Marangoni convection is predominant with regard to bulk convection and can affect spreading kinetics (Eustathopoulos et al. 1998b). In practice, significant Marangoni convection can be generated in sessile droplets by relatively weak thermal gradients which are often present in nominally isothermal furnaces.

In diffusion-controlled wetting, substrate orientation is not expected to influence spreading parameters. An example is the behaviour of Cu-Ti alloy on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> (Kritsalis et al. 1991, Drevet et al. 1996). The addition of about 10 at.% Ti in Cu decreases the contact angle from the 130° measured for pure Cu to about 30°. However, the  $\theta(t)$  curve exhibits two stages. The first one is completed in less than 1 second and can be attributed to adsorption of Ti at the interface (see Figure 6.37). The second stage is much slower (200 seconds) and corresponds to the formation of a wettable TiO layer, 1  $\mu$ m thick, at the interface. Non-linear spreading has been observed for the reactive stage, indicating that it is controlled by diffusion of Ti from the drop bulk to the triple line. Experiments with Cu-Ti droplets with a fixed composition and mass on four differently orientated substrates of Al<sub>2</sub>O<sub>3</sub> led to nearly equal spreading times. This behaviour is very different from that of Al/C system with linear spreading kinetics (see Figure 8.7).

Returning to the first stage of rapid spreading observed in the Cu-Ti/Al<sub>2</sub>O<sub>3</sub> system in which adsorption of Ti decreases significantly the contact angle. The observed fall is from an initial value of 130° to close to or lower than 90° depending on the Ti concentration in the melt. It is reasonable to think that for certain systems, especially for metal/oxide systems, the formation of a 3D layer at the interface is preceded by formation of an adsorption layer (i.e. of a 2D layer rich in reactive solute with a composition different from that of the adjacent bulk phases) leading to a first fall of the contact angle (Eustathopoulos and Drevet 1994, Tomsia et al. 1998).

Unfortunately, there are no specific experimental studies of spreading kinetics of alloy/oxide systems in which only adsorption occurs without formation of a 3D compound. However, when analysing  $R(t)$  curves in reactive systems, it may be useful to calculate the spreading rate in the case where the decrease of the contact angle is due to the lateral extension of an adsorption layer. This needs diffusion of interface-active solute from the drop bulk to the liquid adjacent to the adsorption layer at the triple line, followed by a transfer from the liquid to the adsorption

layer. Assuming that the overall process is limited by the diffusion stage, the spreading rate can be estimated from equation (2.23) taking  $e = 0.5$  nm, a typical value for an adsorption layer,  $D = 10^{-9}$  m<sup>2</sup>.s<sup>-1</sup>,  $n_v = 10^{-7}$  mole.m<sup>-3</sup> (assuming that the adsorption layer is constituted by pure interface-active solute),  $C_0 = 10^{-8}$  mole.m<sup>-3</sup> and  $C_e = 0$  (because transfer at the interface is assumed to be much faster than diffusion, the equilibrium concentration in the liquid adjacent to the adsorption layer is reasonably taken equal to 0). Then, for an instantaneous contact angle of  $\pi/2$  rad, the calculated spreading rate is 30 mm/s which corresponds to a spreading time of the order of  $10^{-1}$  second. This explains the fast initial spreading observed in the Cu-Ti/Al<sub>2</sub>O<sub>3</sub> system (Figure 6.37). Note that such spreading times are two to three orders of magnitude shorter than those observed in diffusion-limited reactive wetting during the formation of 3D compound. This is due to the value of  $e$  in equation (2.23) being typically  $10^2$ – $10^3$  nm as compared to only 1 nm for 2D adsorption.

A different interpretation of reactive wetting for alloy/oxide systems was proposed recently by Tomsia et al. (1998). According to these authors, reactive wetting is due to adsorption of an interface-active solute at the liquid/solid interface rather than to formation of a new 3D compound. As adsorption is a fast process, the comparatively slow spreading kinetics observed experimentally have been considered to be controlled by the propagation of “wetting ridges” pinning the triple line (see Section 2.1.2 and Figure 2.14).

### 2.2.3 Concluding remarks

Dissolution of the solid in the liquid leads to an increase of the contact radius  $R$  and to a decrease of the *apparent*, or visible, contact angle. However, the increase of  $R$  is rather limited in the absence of tensio-active effects of dissolved elements. For metal/metal systems, because dissolution is generally controlled by diffusion in the liquid alloy, a nearly stable configuration for millimetre size droplets can be reached only after times of the order of  $10^2$  seconds, i.e., several orders of magnitude higher than for wetting of non-reactive metals. Much stronger changes in the contact radius are expected when dissolved species modify either the S/L interface or L/V surface energies, as for some metal/oxide couples.

Wetting is promoted by the formation of a 3D compound that is more wettable than the initial substrate. In this case, two main regimes have been identified. In the first, spreading kinetics are controlled by the *chemical reaction* at the triple line and this results in a constant spreading rate. This regime has been observed in metal/ceramic couples and for millimetre size droplets it has characteristic times of the order of  $10^3$ – $10^4$  seconds. In the second regime occurring in systems exhibiting comparatively fast reactions (spreading times of  $10^1$ – $10^2$  seconds), spreading is limited by *diffusion* of a reactive species from the drop bulk to the

triple line, resulting in a spreading rate which scales with the instantaneous contact angle. More work is needed to specify the effect on reactive spreading kinetics of reactions ahead and behind the triple line as well as of “wetting ridges”.

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## Chapter 3

# Methods of measuring wettability parameters

The main part of this Chapter is dedicated to the different variants of the sessile drop method used in more than 90% of wetting studies at high temperatures. A detailed description is also given of the *wetting balance* technique, a simplified version of which is being widely used to control soldering processes in electronic industries. Another aspect of the wetting balance is that it allows study wetting on non-planar solids.

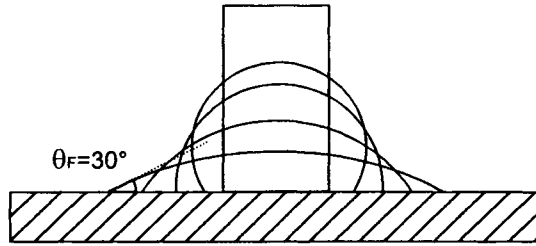
An attempt is made to evaluate the accuracy of data obtained by these techniques, to determine the main causes of scattering and the optimal conditions for contact angle and work of adhesion measurements.

A Section is devoted to “wetting” of a substrate by *solid* particles. This is particularly important in processing of nanomaterials for which capillary equilibrium is expected in short times because of the reduced size of the particles.

### 3.1. SESSILE DROP EXPERIMENTS

Sessile drop experiments are simple in principle and are the most commonly used means of quantitatively measuring wetting behaviour for both chemically inert and reactive systems. Attention will be paid first to the conduct and use of sessile drop experiments using inert systems, but for both inert and reactive systems the experiment consists essentially of permitting a drop of liquid, usually ranging in volume from 0.005 to 5 ml, to spread over a horizontal solid substrate until an equilibrium configuration is achieved. Thus the area of the liquid surface is increased and that of the substrate is decreased by conversion to liquid/solid interface. This change is sketched schematically in Figure 3.1 and continues until further advance of the liquid front is energetically unfavourable as discussed in Section 1.2 (see Figure 1.4). The rate at which the liquid front advances over the substrate surface to assume the equilibrium configuration is discussed in Chapter 2.

The contact angle is by far the most often quoted characteristic to be derived from sessile drop experiments, but reference will be made later in this Section to other liquid parameters and particularly to the liquid surface energies,  $\sigma_{LV}$ . While values for both  $\theta$  and  $\sigma_{LV}$  can be determined from measurements made during a single sessile drop experiment it is often convenient to use differently sized drops. Small drops will assume the profiles of nearly spherical caps and this regularity assists the estimation of  $\theta$  values from their dimensions, while the gravitational



**Figure 3.1.** Schematic illustration of the profiles assumed as a solid cylinder melts to form a sessile drop, with an initial contact angle of  $120^\circ$ , which then spreads over the substrate, displaying transient contact angles to achieve a final equilibrium contact angle  $\theta_F$  of  $30^\circ$ .

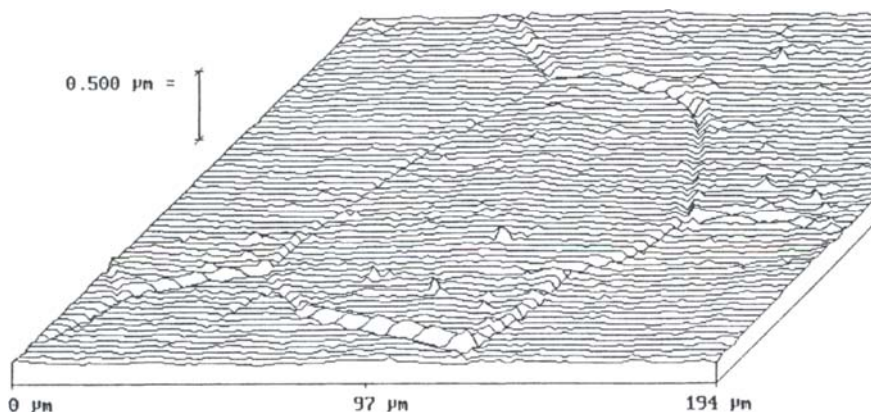
flattening of large drops assists calculation of  $\sigma_{LV}$  values. When selecting a suitable small or large size for a particular liquid, guidance can be provided by reference to the “capillary length” which defines the boundary between size regimes in which gravity is and is not of major importance. This critical size, equal to  $(2\sigma_{LV}/(\rho g))^{1/2}$  in which  $\rho$  is the liquid density and  $g$  is the acceleration due to gravity (see equation (1.23)), is a few millimetres for most metals and glasses. Thus a drop of volume 0.005 ml with a spherical diameter of 2 mm will be suitable for  $\theta$  measurements but one with a volume of several ml would be more convenient for the derivation of  $\sigma_{LV}$  values.

### 3.1.1 Materials and equipment requirements

The five main requirements for conduct of a sessile drop experiment relevant to high temperature capillary phenomena are: characterisation of the materials, a flat horizontal substrate, a test chamber to provide a controlled and generally inert gaseous environment, a facility that heats the sample to a predetermined temperature and a means of measuring the geometry and size of the sessile drop. Satisfying these requirements demands careful and precise experimental procedures.

Thorough characterisation of the materials used is essential if the experimental results are to be reproducible and usable by other workers. The prime requirement is a clear specification of their compositions, with particular attention being paid to surface and interface active components that will change the energies and hence the contact angle of the system as defined by the Young equation.

It is also important to have an understanding of the microstructure of the substrate, and of its surface texture. Thus preferential wetting of thermal grain-boundary grooves (Figure 3.2) can distort the triple line (see Appendix H) and the



**Figure 3.2.** Grain-boundary grooves formed on polycrystalline Ni surface (grain diameter of the order of  $100\ \mu\text{m}$ ) in two hours at  $900^\circ\text{C}$ . For wetting liquids, these grooves can act as capillaries. The profile was obtained by high-resolution optical profilometry.

presence of a second phase at the surface of the substrate will complicate the energy balance achieved by the equilibrated sessile drop and may give rise to pinning of the triple line as explained in Section 1.3.2. Using rough substrates increases the contact angle values for non-wetting systems, those for wetting systems also sometimes increase but generally decrease as discussed in detail in Section 1.3.1. What is meant by a “smooth” substrate depends on the wetting characteristics of the system, but in the past this has usually meant a roughness amplitude,  $R_a$ , of no more than  $1\ \mu\text{m}$  and an average asperity slope of no more than  $5^\circ$ . More demanding standards of smoothness, an  $R_a$  of no more than  $0.1\ \mu\text{m}$  and a slope of less than  $2^\circ$ , are used frequently at present in laboratory work. In the case of non-wetting systems, even very small defects in the substrate surfaces can pin the triple line. Thus surfaces with  $R_a$  values of less than  $0.01\ \mu\text{m}$  have to be used if an accuracy of  $\pm 2\text{--}3^\circ$  is needed for  $\theta$  values, (Hitchcock et al. 1981, De Jonghe et al. 1990). Further, it is almost certain that even higher standards will be needed in future for the reproducible characterisation of wetting behaviour and striving for these standards will enhance the attractiveness of using single crystals as substrates because they permit the easier preparation of smooth surfaces and also because they are of higher and more reproducible purity than most polycrystalline materials. In all cases, not only is statistical characterisation of the roughness necessary but also optical microscopy of the substrate surface for evidence of scratches which may not significantly affect  $R_a$  values but could cause profile distortions where they intersect the drop peripheries.

Unless the substrate is horizontal, the drop will not be circularly symmetrical and the contact angles assumed at diametrically opposed locations will not be equal as illustrated in Figure 3.7.f. Liquid will flow to the lower location and this excess will cause the drop to be distorted to two values of contact angle,  $\theta_a$  and  $\theta_r$ , respectively greater and smaller than that required by the equilibrium condition defined by the Young equation (1.16) or, in the case of a very smooth surface, to run down the slope. However, using a tilting substrate can be a means of determining the hysteresis domain of contact angle of a sessile drop, as explained in Section 3.1.2. Similar effects on a smaller scale can be caused if the substrate is convex or concave rather than flat. Distortions in the symmetry of the drops can also have major effects in degrading the reliability of derived values of liquid surface energies, and can have some effect on the measurement of density values.

No real substrate will be perfectly flat or horizontal, but experience suggests some practical standards of acceptance that are required for experiments to yield reliable sessile drop data. The substrate surfaces must be at least sufficiently horizontal for no movement to occur when a solid cylinder melts to form a sessile drop. A tilt of less than  $1-2^\circ$  is necessary if the drop profiles are to be acceptably symmetrical. An adequate horizontal standard can be assured at the start of the experiment by using a spirit level placed on top of the substrate, but there is no simple method of being certain that the standard is maintained during the course of the experiment when the test chamber furniture as well as the sample are heated. In practice it has to be accepted that the substrate is sufficiently horizontal if the sessile drop melts without moving over the substrate and produces an apparently symmetrical profile. This can be verified *in situ* by means of a rotating stage on which the substrate is placed (see Figure 3.6).

Achieving a controlled gaseous environment within the test chamber requires it to be leak-tight and to be purged with an inert gas or evacuated and, sometimes, to be back filled with an inert gas. The purity of the inert gas and the quality of the vacuum required for true, materials determined, characterisation of wettability depends on the chemical reactivity of the sessile drop and its substrate but it is common to employ inert gases containing only a few ppm of oxidising gases such as  $O_2$ ,  $H_2O$  and  $CO_2$ . This level of impurity, however, corresponds to a partial pressure of  $10^{-5}$ – $10^{-6}$  atm of oxidising agents in 1 atm of gas and is enough to cause oxidation of most common pure metals at their melting temperatures (Table 3.1). It is good practice, therefore, to purify the inert gases by passing them slowly over heated powder or shavings of a reactive metal such as Ti or Zr. If concern is felt about the use of such metals, an alternative is to mix a small amount of a reducing gas, normally  $H_2$ , in with the inert gas. Such mixtures also enable environments to be used with previously selected  $O_2$  partial pressures by controlling the  $H_2/H_2O$  or  $CO/CO_2$  ratios, and the value of  $P_{O_2}$  for such

environments can be verified by using electrochemical sensors, (Taimatsu and Sangiorgi 1992). Additionally, for inert gas or evacuated environments, verification of  $P_{O_2}$  values can be obtained by measuring the  $\sigma_{LV}$  of a well characterised metal such as Cu and interpolating these values with established  $\sigma_{LV} = f(P_{O_2})$  relationships (Gallois and Lupis 1981) (see Figure 4.3).

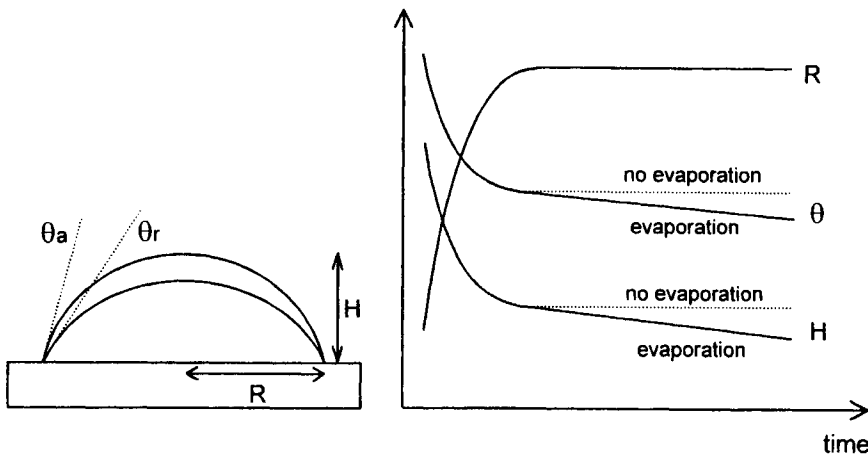
**Table 3.1.** Partial pressure of oxygen in equilibrium with the oxide of the metal at 1000°C and at the melting point of the metal  $T_F$ .

Metal	$P_{O_2}$ (atm) at 1000°C	$P_{O_2}$ (atm) at $T_F$
Al	$10^{-35}$	$3 \times 10^{-52}$
Cu	$10^{-7}$	$2 \times 10^{-6}$
Fe	$10^{-15}$	$2 \times 10^{-9}$
Mg	$10^{-38}$	$10^{-57}$
Ni	$10^{-10}$	$8 \times 10^{-6}$
Pb	$8 \times 10^{-9}$	$2 \times 10^{-28}$
Si	$10^{-28}$	$10^{-19}$
Sn	$6 \times 10^{-14}$	$10^{-50}$
Ti	$2 \times 10^{-30}$	$8 \times 10^{-17}$

Particularly in the past, many measurements of wettability have been made using evacuated chambers, although this can sometimes cause problems due to evaporation from the liquid or its substrate. Typically, vacua lying in the range  $5 \times 10^{-7}$ – $5 \times 10^{-5}$  mbar have been used in which the partial pressures of the oxidising gases in oil diffusion pumped systems are one to three orders of magnitude smaller because of the reducing atmosphere generated by cracked oil molecules. However this cracking can also result in C contamination of the sessile drop and the substrate surface, so in general it is better to strive for a clean system with a low partial pressure of oxidising gases by using liquid  $N_2$  traps to minimise back diffusion of pump oils or better still to employ oil free equipment such as turbo-molecular pumps.

At an equal  $P_{O_2}$  value, a high vacuum environment is preferable to inert gas because it promotes evaporation and dissociation of oxide films on the liquid or substrate surfaces by forming volatile sub-oxides, as elaborated in Section 6.4.2. However, the use of high vacuum environments also promotes evaporation of the liquid and this can lead to anomalously low measured contact angles since the drop peripheries tend to be fixed, and hence the measured contact angle changes from that of an advancing liquid front to that of one which is receding, from  $\theta_a$  to  $\theta_r$  as

illustrated in Figure 3.3. This effect occurs quite frequently but the change in the contact angle values usually lies within the range of measurement precision unless the loss exceeds several percent and the observation of major effects usually requires a loss of about 10%. Such losses can occur, however, when conducting sessile drop experiments using volatile metals such as Mg or Zn or materials containing volatile components, such as the alkali metals present in some glasses, rendering the measurements obtained of doubtful validity.



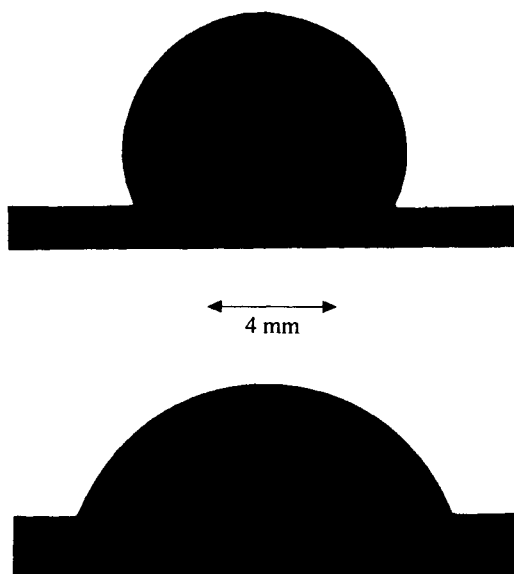
**Figure 3.3.** Schematic illustration of the effects of evaporation on the profile and parameters of a sessile drop.

Some form of mechanical pumping will be required to purge or evacuate and back fill the test chamber and care must be taken to minimise transmission of vibration to the sample. Vibration that causes movement of the sessile drop over its substrate is unacceptable and generally any vibration that can be felt by placing a hand on the test chamber should be avoided.

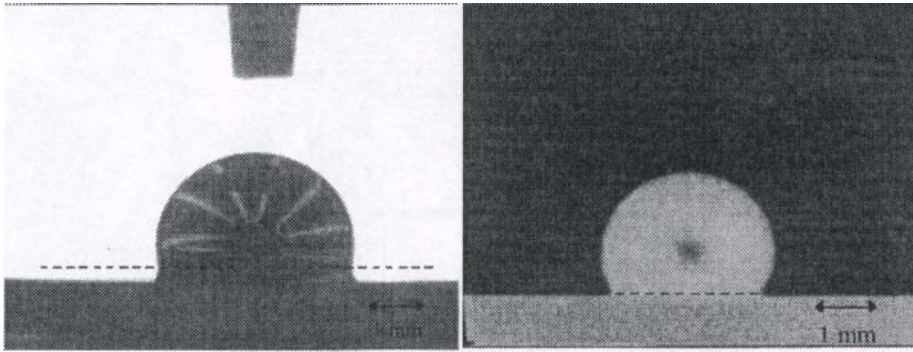
The methods of heating the samples and of controlling their temperatures are not specific to sessile drop tests and many methods have been employed in practice but most experiments are conducted using electrical resistance heating elements which, ideally, should be outside the test chamber to eliminate the possibility of contamination caused by evaporation or desorption from their hot surfaces. This possibility is particularly real when graphite heating elements are used which are often porous. Additionally, care must be taken to achieve melting of the liquid in times that are short compared to those allowed for subsequent spreading. In particular, when using alloys with wide melting ranges, the heating rates should be

fast through that temperature range to minimize premature wetting of a substrate by migration of a liquid phase from a partially molten drop.

As already said, the commonest measurement made on sessile drops is the value of their contact angles. The experiments, therefore usually require the use of some form of goniometer to measure the angle directly when viewing the drop profile, or a means of recording the drop size and geometry with still, cine-, video or X-ray cameras (Figure 3.4). It is essential, therefore, that the chamber be fitted with observation ports, some of which should be in the same plane as the sample, and that the axes of the cameras should be on the plane of the substrate surface. Failure to satisfy this last requirement will cause distortions in the drop image. For many experiments, it is also essential to use background illumination of the drop profile, and to ensure that the beam is collimated and in the same plane as the substrate. At temperatures of about 700°C or above, the sessile drops will be sufficiently luminous to be photographed optically, but it is still desirable to use background illumination if sharp images are to be obtained (Figure 3.5). This technique can to some extent mitigate the clouding of the cool observation ports by condensation of volatile species from the liquid drops, and it can also be helpful to back-fill the test chamber with an inert gas rather than leave it evacuated.



**Figure 3.4.** Photographs taken with background illumination of sessile drops of pure Al on polycrystalline alumina in high vacuum at 850°C (top) and 1200°C (bottom). From (Coudurier et al. 1984).



**Figure 3.5.** Video images of sessile drops of two Ni alloys on  $\text{Al}_2\text{O}_3$  at  $1500^\circ\text{C}$  with (left) and without (right) background illumination (Labrousse 1998). On the left image, one can distinguish the reflection of the resistance heater on the droplet as well as the capillary used to dispense the droplet. By tilting slightly the substrate, it is possible to determine accurately the position of the triple line (dashed line) by the intersection of the drop profile and the drop shadow (or reflection) on the substrate surface.

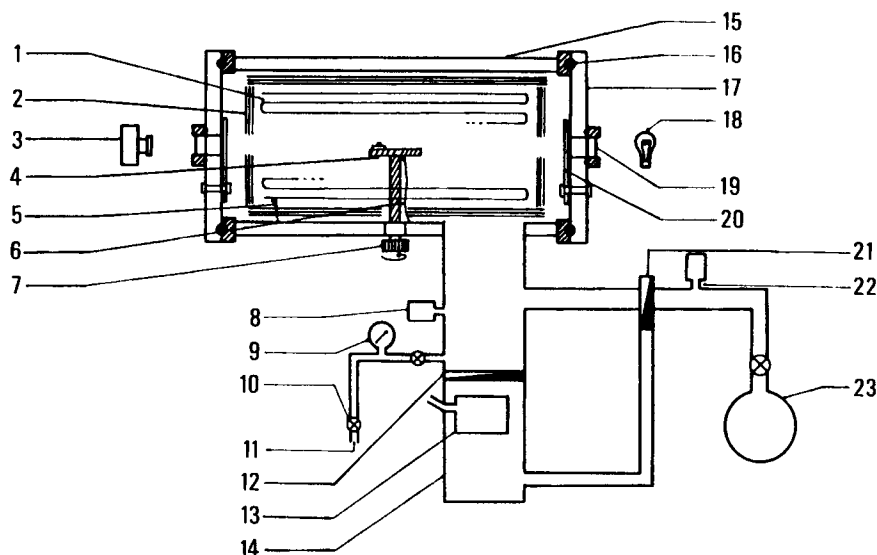
Thus conduct of even a simple sessile drop experiment can be difficult and require a complex array of sophisticated equipment, such as that shown in Figure 3.6.

### 3.1.2 Types of experiment

A sessile drop experiment can take one of several forms, as shown schematically in Figure 3.7. The classic form shown in Figure 3.7.a calls for a small piece of solid sessile drop material, typically 0.01 ml in volume, to be placed on a substrate and then heated above its melting temperature. The sessile drop can be composed of a pure material or it can be an alloy or a chemical compound. It is not always convenient to prepare alloys or compounds prior to conducting the sessile drop experiment, and a variant of the classic technique, shown in Figure 3.7.b, is to form the alloy or compound *in situ* from a mechanical mixture of the components, (Mortimer and Nicholas 1973). In some work done in the former Soviet Union, metal alloys were formed *in situ* by plunging a piece of solid solute into a molten sessile drop of solvent (Naidich and Zhuravlev 1971).

Another variant calls for a metal or alloy to be melted in an unwetted and chemically inert closed ceramic tube positioned and to be dispensed on to the substrate surface through a small hole in the tube end by applying a back pressure of inert gas, Figure 3.7.c, (Nicholas et al. 1984), or using a piston (Naidich et al. 1983, Rado et al. 1998). One advantage of this technique is that oxide films on



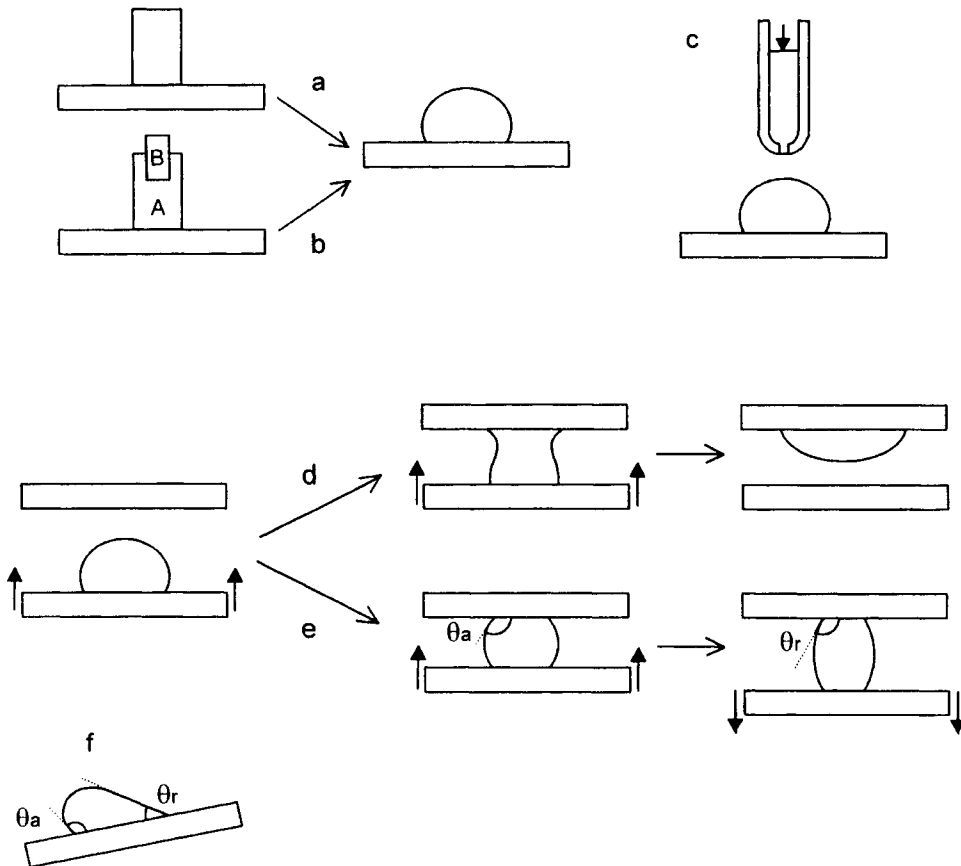


**Figure 3.6.** Laboratory equipment used to conduct sessile drop experiments at high temperatures (Rivollet et al. 1987) [10]. 1:molybdenum resistance heater, 2:molybdenum radiation shields.

3:camera, 4:alumina rotating stage, 5:PID regulation thermocouple, 6:thermocouple, 7:rotating vacuum seal, 8:ion-gauge, 9:manometer, 10:micrometer-valve, 11:gas inlet, 12:pneumatic gate valve, 13:N<sub>2</sub>-cooled trap, 14:diffusion pump, 15:water-cooled stainless steel enclosure, 16:copper gasket, 17:removable disk, 18:incandescent lamp, 19:view-port, 20:view-port mask, 21:3-way automatic gate valve, 22:Pirani gauge, 23:zeolite pump.

liquid metals are disrupted during dispensing. However, care must be taken to ensure that the distance between the tube and the substrate is sufficient to avoid bridging by the dispensed drop but not so great as to result in the drop bouncing off the substrate or splattering. Again, a sessile drop can be melted on an inert substrate which is then raised so that the top surface of the drop contacts a fresh and possibly reactive solid surface and subsequently lowered, Figures 3.7.d and 3.7.e, (Naidich et al. 1995, Hara et al. 1995, Voitovich et al. 1998). Liquid can be transferred to the top substrate provided this is better wetted than the donor and this configuration is particularly useful for the study of wetting kinetics because it avoids interactions between the liquid and its receiving substrate that can occur during heating to the experimental temperature, Figure 3.7.d. The configuration shown in Figure 3.7.e can be used to study hysteresis effects because both advancing and receding angles are formed as the bottom substrate is raised and lowered. Contact angles assumed by both advancing and receding liquid fronts can be measured also by tilting a substrate until the sessile drop begins to run down

hill, Figure 3.7.f, a technique usually used only with low-melting temperature liquids.



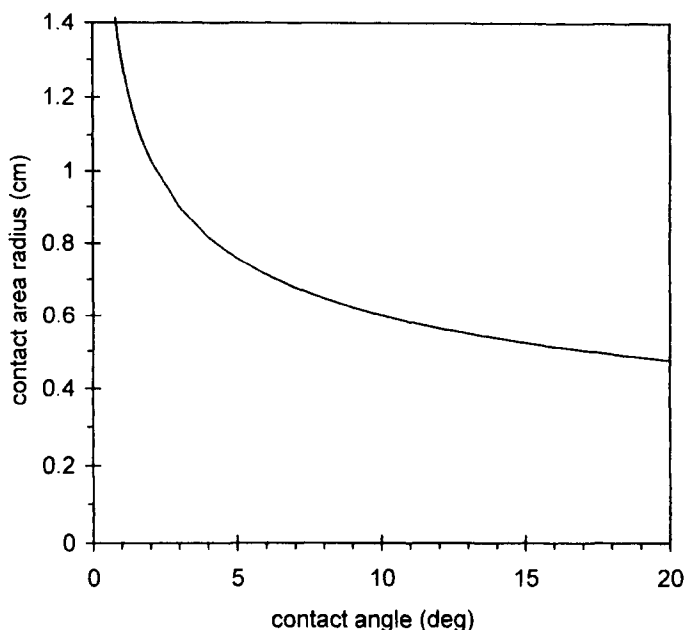
**Figure 3.7.** Methods of conducting sessile drop experiments : (a) classic technique, (b) *in situ* formation of an alloy, (c) dispensed drop, (d) transferred drop, (e) double substrate, (f) tilted plate.

### 3.1.3 Information that can be derived

**3.1.3.1 Contact angles.** According to the Young equation (1.16), the equilibrium contact angle,  $\theta_Y$ , is a unique characteristic for each particular materials combination, determined by the surface and interfacial energies of the system

components, and hence is independent of the liquid and solid configuration involved. This argument leads to the conclusion that a relatively simple sessile drop experiment can be used to provide information about the capillary behaviour of inert systems in situations in which direct measurements are not practical or easy, such as during the penetration of capillary gaps or the formation of braze fillets. For chemically reactive systems, care must be taken when contact angle values measured in the sessile drop configuration have to be transferred to other configurations, as discussed in Section 2.2.2.1 (see also Figure 2.27).

Sessile drop experiments permit the changes in wettability with temperature to be observed by ramping the temperature, or preferably by holding the sample at a series of increasing temperatures so that several measurements can be made during each constant temperature hold to test whether stable contact angle values have been achieved. Generally, increasing the temperature produces a small decline in contact angle values for inert systems, such as 10 degrees or so for a temperature rise of several hundred degrees Celsius. In principle, it should also be possible to check the effect of temperature on contact angle values by concluding the experiment with a series of holds at decreasing temperatures but this is seldom done in practice because receding liquid fronts often exhibit hysteresis effects.



**Figure 3.8.** Relationship between the contact radius,  $R$ , and the contact angle,  $\theta$ , of a sessile drop of volume 0.03 ml that has the form of a spherical cap.

If care is taken, angular measurements can be made from drop profiles with an accuracy of 1–2° for  $\theta$  values ranging from about 20 to 160°. Measurements of very small or high contact angles are difficult because precise alignment of the goniometer or camera with the plane of the substrate surface becomes critically important despite increasing uncertainty about the exact location of the contact line when viewing the drop profile. It is a common practice to view sessile drops from above during or after the experiment if they have very low contact angles and to use the radius of the contact area, identified as  $R$  in Figure 3.9, as a measure of wettability. This radius is sensitive to small changes in wettability as illustrated in Figure 3.8 and, if so wished, can be used to derive the contact angle by assuming the drop to be a spherical cap of volume  $v$  and substituting in the expression

$$v = \frac{\pi R^3}{3} \frac{(2 - 3 \cos \theta + \cos^3 \theta)}{\sin^3 \theta} \quad (3.1)$$

If the measurement of  $R$  is made after the experiment is completed, the volume used should still be that of the liquid because it is unusual for there to be significant contraction in the contact area when the drop solidifies.

To have unreserved confidence in such  $\theta$  data it is advisable to measure several geometric and dimensional characteristics of the sessile drop and to test for their internal consistency. Thus the  $\theta$  values assumed by the left hand and right hand sides of the drop profile should be measured and compared for consistency. Additionally, it is prudent to measure the height of the drop apex,  $H$ , and the radius  $R$  of the substrate contact area. If the drop has the profile of a spherical cap then a value can be calculated for the contact angle,  $\theta_{\text{calc}}$ , by substitution in

$$\tan\left(\frac{\theta_{\text{calc}}}{2}\right) = \frac{H}{R} \quad (3.2)$$

and comparison with  $\theta$  again provides a test of the assumed symmetry of the drop. On some occasions,  $\theta_{\text{calc}}$  may be preferred to that of  $\theta$  since a small and inconsequential perturbation at the drop periphery could cause a large change in  $\theta$  without much affecting  $\theta_{\text{calc}}$ .

It is also important to verify the consistency of changes in the geometric and dimensional characteristics occurring during the course of an experiment (Table 3.2). Thus a decrease in the contact angle and drop height that is not mirrored by an increase in the radius of the contact area suggests that liquid has been lost, by infiltration of the substrate or evaporation for example, while an increase in the

contact angle that is not mirrored by a decrease in the radius of the contact area demonstrates pinning of the advancing liquid front, triple line, by some localised substrate heterogeneity, (Rivollet et al. 1987).

**Table 3.2.** The different possible cases of changes with time in the shape of the drop at constant temperature (Rivollet et al. 1987).

$\theta(t)$	$R(t)$	$H(t)$	Comments
↓ or =	↑	↓	at steady state $\theta = \theta_a$
↑ or =	↓	↑	at steady state $\theta = \theta_r$
↓	=	↓	$\theta$ tends towards $\theta_r$ (ex.: decrease of drop volume)
↑	=	↑	pinning of an advancing triple line (ex.: increase of drop volume)

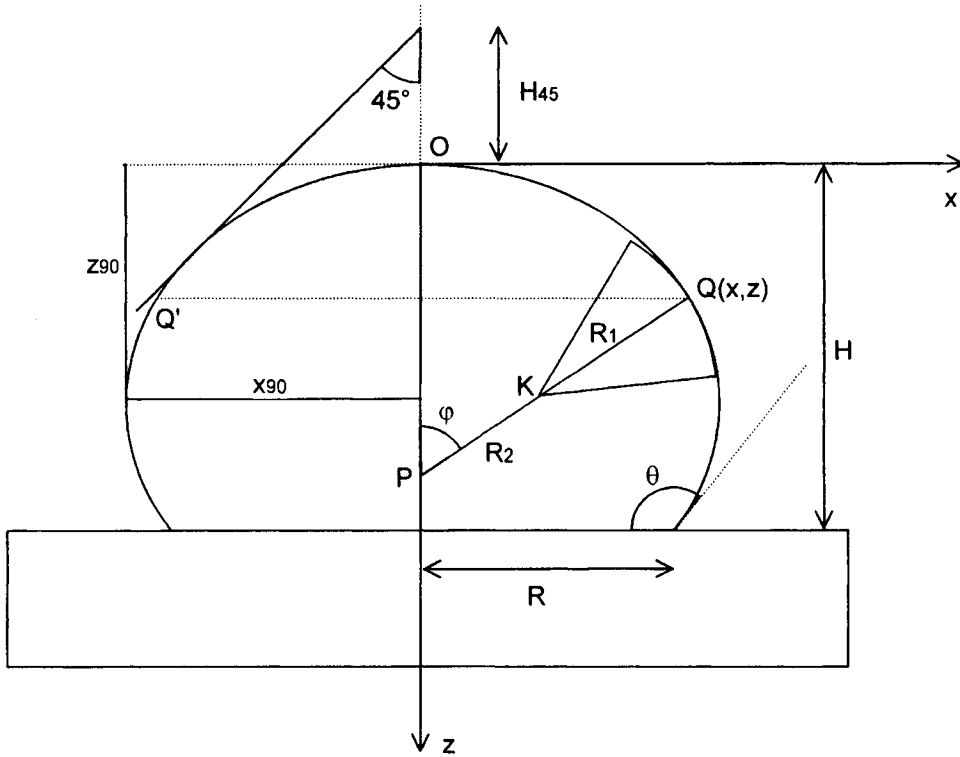
↑: increases, ↓: decreases, =: constant,  $\theta_a$ : advancing contact angle,  $\theta_r$ : receding contact angle

Workers concerned with liquid/solid systems with exceptionally good wettability, such as some braze/metal workpiece systems, find that the drops do not preserve a perfectly circular area of contact because of the sensitivity of the liquid to changes in capillary attraction caused by minor variations in the surface texture of the workpiece. Because of such irregularity, some workers have used the contact area of a small volume of braze as a measure of wettability. Thus Feduska used area measurements to differentiate between the wetting of different stainless steels by a wide range of metals and alloys (Feduska 1959).

Not all aspects of wetting behaviour are sensitive to the precise values of small contact angles. For example, the rise up a vertical capillary is a function of the *cosine* of the contact angle (equation (1.55)), and therefore a decrease in  $\theta$  from  $10^\circ$  to  $0^\circ$  causes an increase in penetration of only 1.5%.

**3.1.3.2 Liquid surface energies.** The surface energy of a liquid can be derived from very accurate measurements of the size and shape of a sessile drop (Passerone and Ricci 1998). This is not in fact the spherical cap which has been assumed or implied up to now but is somewhat flattened due to gravity. This is of particular importance for large drops with diameters substantially larger than the capillary length,  $(2\sigma_{LV} / (\rho g))^{1/2}$ . This flattening causes the principal radii  $R_1$  and  $R_2$  identified in Figure 3.9 to vary from point to point on the drop surface, reflecting the balance between the hydrostatic pressure and the capillary pressure due to the

liquid surface energy and it is this deviation from sphericity that is used to determine surface energy values.



**Figure 3.9.** Profile of a sessile drop showing the measurements used to derive liquid surface energy values. The principal radii of curvature at point Q are  $R_1 = QK$  and  $R_2 = QP$ .

For the sessile drop sketched in Figure 3.9, the principal radii of the surface at the opposed positions Q and Q' are  $R_1$  in the plane of the paper ( $R_1 = QK$ ) and  $R_2$  in a plane perpendicular to the paper ( $R_2 = QP = x/\sin\varphi$ ) so that

$$P_L^Q - P_V^Q = \sigma_{LV} \left( \frac{1}{R_1} + \frac{\sin\varphi}{x} \right) \quad (3.3)$$

Similarly, at the drop apex (point O)

$$P_L^O - P_V^O = \frac{2\sigma_{LV}}{b} \quad (3.4)$$

because at that point  $b = R_1 = R_2$ . Neglecting the difference in vapour pressure between points Q and O enables us to write

$$P_L^Q - P_L^O = \sigma_{LV} \left( \frac{1}{R_1} + \frac{\sin \varphi}{x} \right) - \frac{2\sigma_{LV}}{b} \quad (3.5)$$

But the difference between  $P_L^Q$  and  $P_L^O$  must be equal to the hydrostatic pressure of a column of height  $z$  so that

$$P_L^Q - P_L^O = \sigma_{LV} \left( \frac{1}{R_1} + \frac{\sin \varphi}{x} \right) - \frac{2\sigma_{LV}}{b} = \rho g z \quad (3.6)$$

In applying this equation it should be noted that the density of the liquid,  $\rho$ , is used instead of the more rigorously correct difference between it and the density of the vapour.

The radius of curvature  $R_1$  and  $\sin \varphi$  can be expressed in terms of the first and second derivatives of  $z$  with respect to  $x$ . Substituting this into equation (3.6) we obtain a differential equation for which numerical solutions are necessary. The best approach is by curve fitting using computerised iterative calculations such as those suggested by Maze and Burnet, (1969), until there is a convergence of  $\sigma_{LV}$  values. This approach can yield surface energy values with high estimated accuracies and a reproducibility of a few percent, but great care has to be taken to use contaminant free materials and environments and to ensure that the substrate is horizontal and not subject to vibration. Recording the sessile drop image is relatively simple, but its subsequent evaluation can be tedious, typically requiring measurement of  $x$  with a precision of about  $\pm 1 \mu\text{m}$  at perhaps 50 or more different locations with  $z$  values incrementally increasing by 10–20  $\mu\text{m}$ . These measurements have to be made on enlargements of the recorded images of the drop profiles and high-quality equipment must be used to retain sharpness. To test that the experimental procedures for recording and measuring images are of the desired standard, it is good practice to use them first to measure the surface energy of Hg at room temperature, established as  $0.487 \pm 0.005 \text{ J.m}^{-2}$ , and then of Au at its melting temperature, equal to  $1.138 \pm 0.015 \text{ J.m}^{-2}$  (see Table 4.1).

Today, the development of computerised numerical calculation and computer-aided imaging techniques (Rotenberg et al. 1983, Liggieri and Passerone 1989,

Naidich and Grigorenko 1992, Passerone and Ricci 1998) is making the sessile drop method more and more reliable and accurate. However, it should be noted that substantial effort has been required historically to derive a surface energy by curve fitting, and many authors have suggested simplifications which require far fewer measurements. Thus, Bashforth and Adams, (1883), rewrote equation (3.6) in the form:

$$\frac{b}{R_1} + \frac{b \sin \varphi}{x} = 2 + \beta \frac{z}{b} \quad (3.7)$$

with

$$\beta = \frac{b^2 \rho g}{\sigma_{LV}} \quad (3.8)$$

Bashforth and Adams generated tables of  $\beta$  and  $x/z$  for  $\varphi = 90^\circ$  as well as tables of the ratios  $x/b$  and  $z/b$  for differing values of  $b$  and  $\varphi$ . By measurement of  $x_{90}$  and  $z_{90}$  at  $\varphi = 90^\circ$ ,  $b$  and  $\beta$  can be determined from these tables and the liquid surface energy can then be derived from equation (3.8) with an accuracy of about  $\pm 2\%$  for  $\beta > 2$  if the droplet coordinates are measured with an accuracy better than 0.1% (Sangiorgi et al. 1982). A method is presented in Appendix D allowing calculation of the mass of a droplet for an optimised  $\sigma_{LV}$  measurement.

For drops with an  $x_{90}$  three or four times greater than the capillary constant, Worthington, (1885), derived the approximate expression

$$\sigma_{LV} = 0.5 \rho g z_{90}^2 \left( \frac{1.641 x_{90}}{1.641 x_{90} + z_{90}} \right) \quad (3.9)$$

which for big droplets i.e., pancakes ( $x_{90} > 10l_c$  where  $l_c$  is the capillary length), reduces to  $\sigma_{LV} = 0.5 \rho g z_{90}^2$ . Finally, many workers have made use of the empirical relationship:

$$\sigma_{LV} = \rho g x_{90}^2 \left( \frac{0.052}{f_1} - 0.1227 + 0.0481 f_1 \right) \quad (3.10)$$



suggested by Dorsey, (1928), which is the most accurate of these simplified expressions, making use of a factor  $f_1$  equal to  $(H_{45}/x_{90}) - 0.4142$  (see Figure 3.9 for the definition of  $H_{45}$ ).

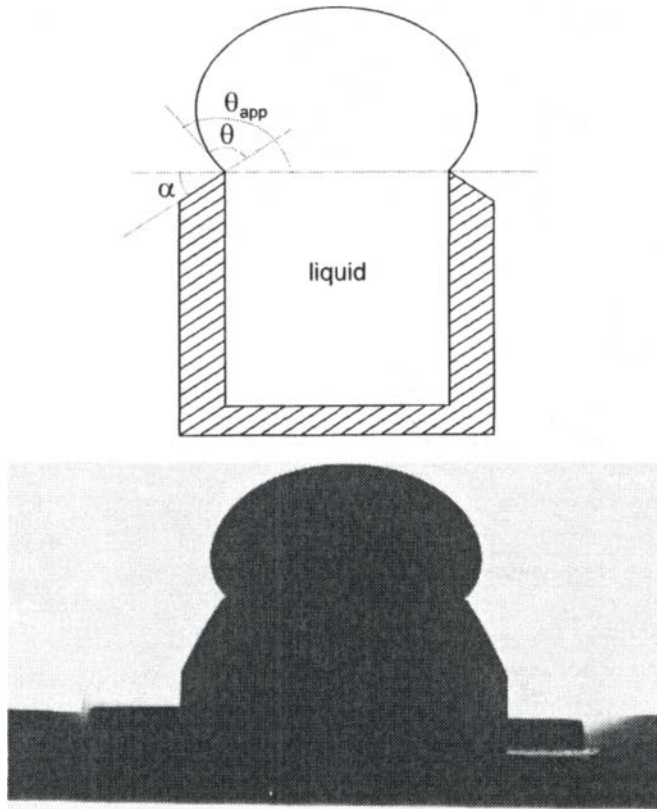
While convenient, it should be noted that most of these approximations require the same precision of measurement as do curve fitting techniques and obviously lead to less accurate results. They have been particularly used to derive values for high melting temperature metals and alloys, yielding values that have an author to author reproducibility of typically 10%, as demonstrated by examination of collected data for Cu and Fe, (Iida and Guthrie 1988). It is, however, often difficult when making such comparisons to decide whether the differences reflect varying precisions of measurement, differences in experimental procedure or qualities of materials.

Most of the approximation methods require the sessile drop to be non-wetting if they are to yield values with errors of less than about 10%. Curve fitting techniques can be applied to wetting drops, but these become increasingly imprecise as the contact angles decrease below 90°. For such wetting systems, the “large drop” approach of Naidich et al. (1963) shown in Figure 3.10 can be of value in that it produces a large and readily measurable apparent contact angle,  $\theta_{app} = \theta + \alpha$ , and hence facilitates the derivation of accurate  $\sigma_{LV}$  values.

Another approach to increasing the contact angle and hence improving the accuracy of  $\sigma_{LV}$  measurements is to change the substrate to one that is less wettable, and indeed the use of several different substrate materials is desirable if there is to be confidence that there has been no chemical interaction that may have affected the liquid surface.

Sessile drop experiments are also used to measure the effects of temperature on liquid surface energies. Because the temperature coefficient  $d\sigma_{LV}/dT$  of liquid metals and oxides is usually a very small, negative, value ( $-0.05$  to  $-0.5$   $\text{mJ.m}^{-2}.\text{K}^{-1}$ ), a temperature rise of several hundred degrees is necessary to produce decreases in the surface energy that can be reliably detected by measurements of drop profiles. Even in this case, the error on the temperature coefficient lies between 30% and 100% (see Section 4.1.1).

**3.1.3.3 Liquid density and other characteristics.** Profile measurements for a symmetrical sessile drop can be used to calculate its volume and hence its density if the original mass is known and there has been no significant loss due to evaporation. As for the measurement of  $\sigma_{LV}$ , the volume can be estimated by measurements of the drop profile coordinates and numerical integration by using image analysis techniques (Naidich and Grigorenko 1992). Alternatively, the



**Figure 3.10.** Top: arrangement of a “large drop” experiment, after (Naidich et al. 1963). Bottom: photograph of a large drop of gold alloy formed on a sapphire cup at 900°C in Ar atmosphere (cup diameter: 12 mm). Printed from (Ricci and Passerone, private communication) with kind permission of the authors.

volume can be roughly estimated from a few measurements and use of the Bashforth and Adams tables, (1883), by substitution in the expression

$$v = \pi R^2 \left( \frac{2b}{\beta} - \frac{2b^2 \sin \theta}{x_{90} \beta} + H \right) \quad (3.11)$$

where  $H$  is the drop height. Both methods of calculating volumes call for great experimental care to form symmetrical drops and for considerable precision in the dimensional measurements. Nevertheless, densities can be derived from sessile drop

experiments with modest estimated errors, less than 1% (Naidich and Grigorenko 1992).

Sessile drop experiments have been used extensively to derive quantities characterising spreading and penetration phenomena, such as the work of adhesion and work of immersion, given by equations (1.45) and (1.54), using a single sessile drop experiment to measure both the contact angle and the liquid surface energy.

### ***3.1.4 Information derivable from reactive systems***

**3.1.4.1 Contact angles.** The conduct of sessile drop experiments using chemically reactive materials, and environments, is essentially the same as that for inert systems but the configurations shown in Figures 3.7.c and 3.7.d are the most suitable because the first contact of the liquid drop is with a fresh, unreacted, substrate at the experimental temperature. Once more, well characterised materials should be used with flat horizontal substrates, as should means for making very precise measurements of the geometry and size of the drops. However, there are some differences of emphasis when considering the significance of the various requirements. Thus, control of heating rates and temperature hold times is more important with reactive than inert systems because these parameters can affect the progress of chemical interactions. Similarly, for the interpretation of results in reactive systems, it is particularly important to record not only the changes with time of contact angle values but also of drop base radii.

Strictly speaking, equilibrium wetting parameters cannot be measured for reacting systems because there is a continuous change in the chemistry of solid and liquid phases caused by dissolution reaction or by formation of new phases at the interface. Nevertheless, as discussed in Section 2.2.2, a local equilibrium can be established at the liquid front for many systems of practical interest and this results in the observation and measurement of an unchanging contact angle,  $\theta_F$ , that is close to but slightly different from the equilibrium value. For instance, in systems in which a continuous layer of new phase is formed at the interface,  $\theta_F$  is close to the Young contact angle of the liquid on the reaction product. In systems in which the substrate A is slightly dissolved in the liquid B,  $\theta_F$  tends towards the Young contact angle of a BA alloy on solid A. Differences between  $\theta_F$  and  $\theta_Y$  can be caused by a variety of effects, such as the roughness of the reaction product layers formed at the liquid/solid interface or a dissolution of the substrate to create a pit (see Figure 2.18). In all cases, interpretation of  $\theta_F$  values requires interface characterisation close to and far from the drop periphery.

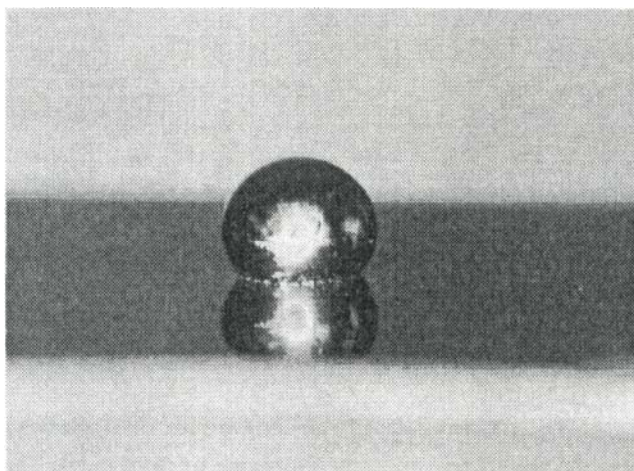
**3.1.4.2 Liquid surface energies.** The parameters needed to derive liquid surface energy values in reactive systems are almost always measured from photographic or video images, the changing size and shapes of drops rendering it impractical to employ the slow process of real time measurements using a goniometer telescope. The photographs provide a record of the conditions prevailing at a particular instant and hence can be used to monitor the effect of the change in composition induced by the reactions on the surface properties of the liquid drop.

Liquid surface energy values can be decreased by segregation of surface active components that enter the liquid from the substrate or from the gaseous environment. In the case of metal sessile drops, these components will be low melting temperature elements such as Pb or Sn or non-metals such as O, 1% of which halves the liquid surface energy of Fe (see Figure 4.4). In contrast, the surface energy values of molten metal alloys can be increased if the reaction depletes them of a low surface energy component that had segregated to the free surface. This could occur if the substrate has a stronger affinity with the surface active solute than does the liquid, as when Cu contaminated with O is brought into contact with Ti or W (Nicholas and Poole 1967).

These alterations in liquid surface energy values are genuine reflections of the reactions, but spurious changes can be caused if the reaction with the substrate or the gaseous environment results in the formation of a second, solid, phase in the drop or on its surface. The creation of an oxide skin on the surface of a metal drop can cause a dramatic increase in the apparent surface energy value, sometimes as much as ten to one hundred times, but this is without any physical or chemical meaning because the surface is no longer that of a liquid drop. Similar distortions, and even in the authors experience decreases to apparently meaningless negative  $\sigma_{LV}$  values, can be caused if a second solid phase is dispersed within the liquid due to supersaturation of some component released by reaction with the substrate or physical detachment of grains of the solid substrate.

### **3.1.5 Solidified sessile drop**

It is not always convenient or practical to measure contact angles while the sessile drops are liquid : this requires special equipment and is imprecise for very small contact angles. Many workers, therefore, have chosen to derive contact angle data from measurements of the size and geometry of solidified small sessile drops (Figure 3.11). The most common measurements made are of the base drop radii of well-wetting drops of a known volume, from which contact angles are derived by substitution into equation (3.1). The validity of this method depends not only on the reasonableness of assuming that the drop profile can be approximated by a spherical cap, but also that the volume of the sessile drop was not altered during



**Figure 3.11.** Solidified Cu drop (mass 107 mg) on an oxidised W substrate.  $\theta = 120 \pm 4^\circ$ . From (Lorrain 1996).

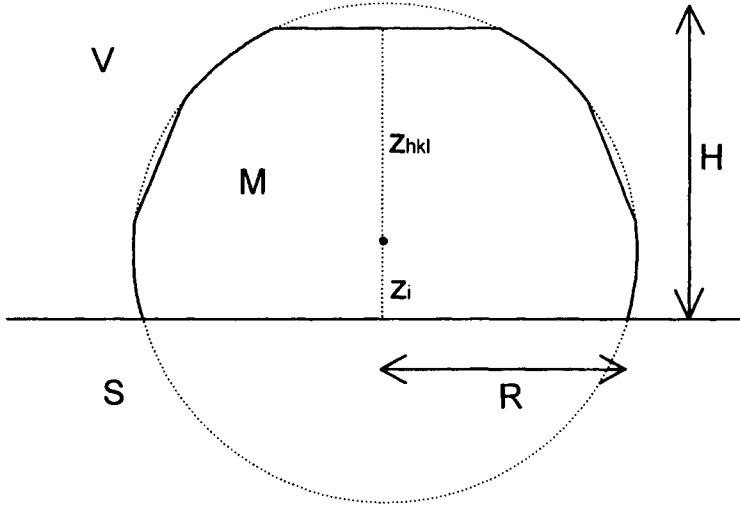
the experiment by evaporation or reaction with the substrate. Alternatively, if the solidified sessile drop is only moderately wetting, an approximate contact angle can be derived also by substitution into equation (3.2).

In principle, estimates of the contact angles of non-wetting sessile drops can be made similarly, but shape and size distortions caused by solidification make it increasingly difficult to derive precise estimates or even, for example, to rank the behaviour of families of alloys in a semi-quantitative manner.

Thus, measurements of solidified sessile drops can be and are used to derive estimated values of contact angles, but these estimates are less precise than those derived from direct observation of liquid drop profiles except for very well wetting systems. The estimates for solidified drops tend to be smaller, typically by up to  $5^\circ$ , and more variable than those derived from observation of liquid profiles. Larger differences can be observed when, during cooling, dewetting of the liquid drop occurs before the resolidification temperature is reached. In this case, traces of the location of the triple line before dewetting are easily seen on the substrate surface.

### ***3.1.6 Contact angles of solid particles on a substrate***

The shape of *solidified*, millimetre size, droplets reflect wetting of the liquid on the solid substrate. The equilibrium shape of a solid particle M on a solid S in a vapour



**Figure 3.12.** A liquid drop is spherical in shape (dashed line) while the equilibrium shape of a solid monocrystalline particle of cubic structure metal is a truncated sphere (full line).

V provides information on the wetting of the *solid* M on S. Micron size particles are needed to attain the equilibrium shape by surface self-diffusion in reasonable times (several hours or tens of hours depending on the value  $T/T_F^M$  where  $T_F^M$  is the melting temperature of M). For small isotropic solid particles, the equilibrium shape dictated only by surface forces is a spherical cap with a contact angle given by the Young-Dupré equation (1.45). Solids are usually anisotropic so that the surfaces of small particles at high temperatures display facets or both facets and curved regions (Figure 3.12). The equilibrium shape of such a particle lying on a substrate S, obtained by minimizing the total surface energy of the M/S system at constant temperature and M volume and assuming that the S/V surface and S/M interface are co-planar, is given by the generalised Wulff equation (Winterbottom 1967):

$$\frac{\sigma_{MV}^{hkl}}{z_{hkl}} = \frac{\sigma_{SM} - \sigma_{SV}}{z_i} \quad (3.12)$$

where  $\sigma_{MV}^{hkl}$  is the solid M/vapour surface energy for the (hkl) plane and  $z_{hkl}$  and  $z_i$  are respectively the distances from the (hkl) surface plane and the M/S interface to the centre of the crystallite. By introducing into equation (3.12) the expression (1.8) of work of adhesion  $W_a$ , we obtain

$$\frac{W_a}{\sigma_{MV}^{hkl}} = 1 - \frac{z_i}{z_{hkl}} \quad (3.13)$$

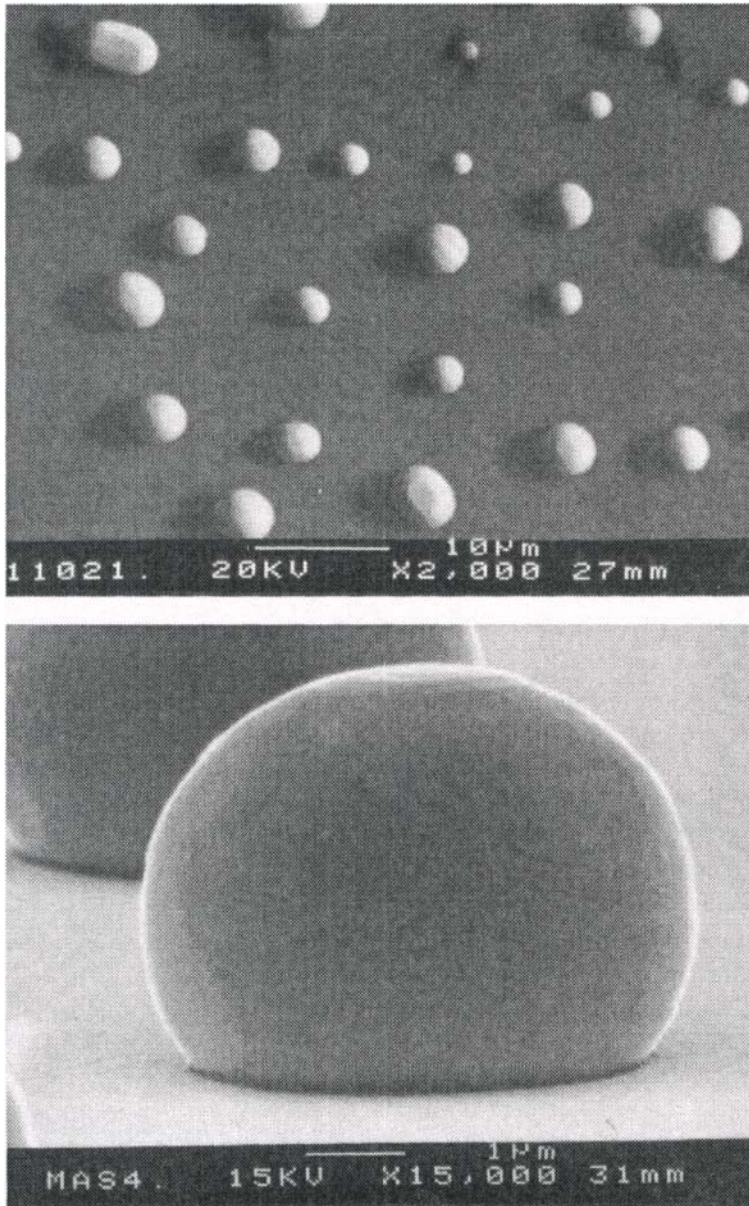
It is possible to write this expression in terms of an equivalent contact angle,  $\theta_{equiv}$ , by comparing with the classical Young-Dupré equation (1.45). Then one gets

$$\cos \theta_{equiv} = - \frac{z_i}{z_{hkl}} \quad (3.14)$$

The equilibrium shape of a metallic particle is a sphere with small facets. Thus, the value of  $\theta_{equiv}$  can also be estimated from the expression  $\tan(\theta_{equiv}/2) = H/R$ .

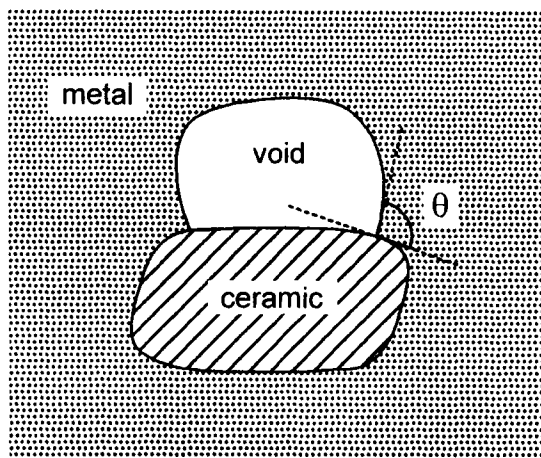
In practice, a metallic film, 100–300 nm thick, is deposited on the substrate S. The coated substrate is then annealed in high vacuum or a neutral atmosphere at high temperature, usually between 0.7 and 0.95  $T_F^M$ , for several tens of hours to break up the film into individual particles (Figure 3.13.a) and for these particles to attain their equilibrium morphology (Figure 3.13.b) (Soper et al. 1996). Another practice is to heat the coated substrate at a temperature slightly higher than  $T_F^M$  to obtain rapid breaking of the film into small droplets and then to decrease the temperature below  $T_F^M$  and anneal the solidified micro-droplets. Measurement of the linear dimensions of the particles by scanning electron microscopy leads to  $\theta_{equiv}$  values reproducible within a few degrees. This method has been applied with success to different non-reactive metal/oxide (Pilliar and Nutting 1967, Murr 1973, Soper et al. 1996) and metal/graphite (Heyraud and Metois 1980, Gangopadhyay and Wynblatt 1994) systems. The effect of alloying on  $\theta_{equiv}$  has also been studied by Gangopadhyay and Wynblatt (1994).

A variant of the equilibrium solid “drop” configuration is presented in Figure 3.14. This shows a ceramic particle embedded in a solid metallic matrix which had previously been subjected to deformation so that the particle decoheres from the matrix. Following a high-temperature treatment, the void in contact with the particle assumes an equilibrium form from which the contact angle  $\theta$  can be measured by transmission electron microscopy. This approach is interesting, principally because the surfaces should be less contaminated than in the sessile drop configuration. Examples of this technique for metal/oxide systems are given in (Hondros 1978).



**Figure 3.13.** Top: when annealed at high temperature, a thin film of Cu on monocrystalline alumina breaks and forms micron-size particles. Bottom: SEM micrograph of a Cu monocrystalline particle on (0001) face of alumina formed after annealing at 1040°C. The facet on the top of the particle is a (111) plane. From (Soper et al. 1996) [11].





**Figure 3.14.** Equilibrium configuration of a void at a ceramic particle contained in a metal matrix. According to Hondros (1978).

### 3.2. THE WETTING BALANCE TECHNIQUE

The wetting balance technique is a variant of the maximum pull (or detachment) method used to measure liquid-vapour surface tensions (Keene 1993). It is nowadays widely employed in the electronics industry to quantify wetting of solders, but has also been used for wetting studies in metal/ceramic systems (Naidich and Chuvashov 1983b, Nakae et al. 1989, Rivollet et al. 1990). As compared to the sessile drop method which needs planar substrates, solids of various geometry can be studied by this technique.

The method described in detail in (Chappuis 1982) consists of continuously monitoring the force acting on a solid, cylinder or blade, moving into and out of a liquid bath during an immersion-emersion cycle. The apparatus developed by Rivollet et al. (1986, 1990) for high temperature studies (Figure 3.15) consists mainly of a furnace and a pumping group, a translation system allowing the displacement of the crucible containing the liquid bath at a constant rate and an electronic microbalance connected to the solid. For wetting liquids, additional information on wetting parameters can be obtained by measuring optically the height of the meniscus formed by the liquid on the solid surface (Figure 3.16.a). The changes in weight, equal to the sum of capillary and buoyancy forces, versus the depth of immersion are analysed by means of the Laplace equation giving the shape of the meniscus formed around a vertical solid. This method allows a simultaneous measurement of the surface tension of the liquid and the contact

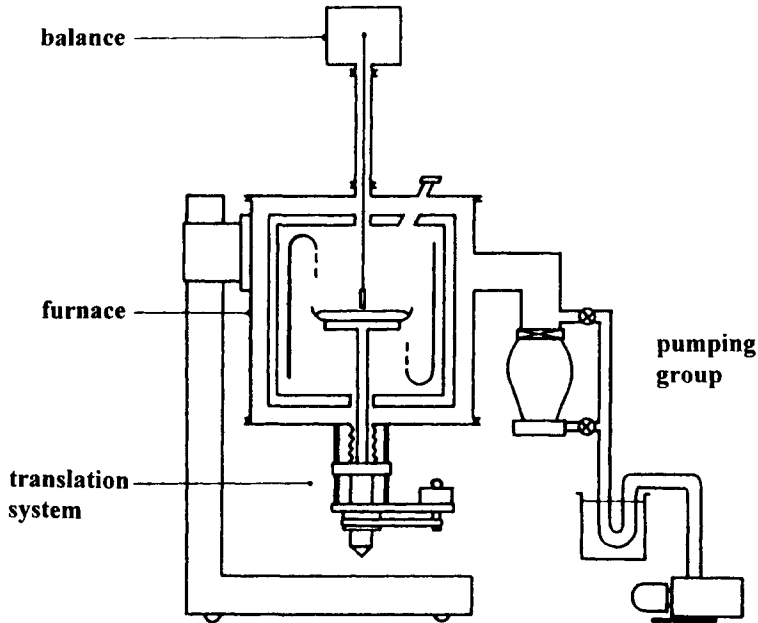


Figure 3.15. Sketch of the wetting balance (Rivollet et al. 1990) [2].

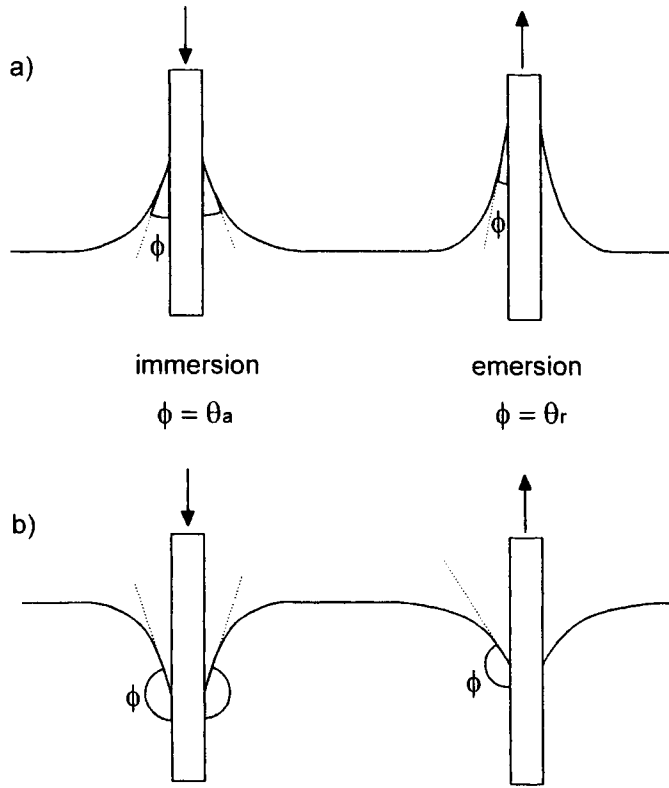
angles. Both advancing and receding contact angles can be deduced from the weight changes during immersion and emersion respectively (Figure 3.16).

In the following, and for the sake of simplicity, the vertical translation rate of the solid in the liquid is supposed to be infinitely slow. Then, if the origin of the weight measurements is taken as the weight of the solid in the gas, the force  $f$  exerted on a solid partially immersed in a liquid, whose base is located at a level  $z_b$  with respect to the flat horizontal surface of the liquid, is equal to the sum of the weight of the meniscus  $w_m$  and the buoyancy force:

$$f = w_m + \Omega \rho g z_b \quad (3.15)$$

where  $\Omega$  is the solid base area,  $\rho$  the liquid density and  $g$  the acceleration due to gravity. Orr et al. (1977) demonstrated that for a prism of any right section of perimeter  $p$ , the weight of the meniscus is:

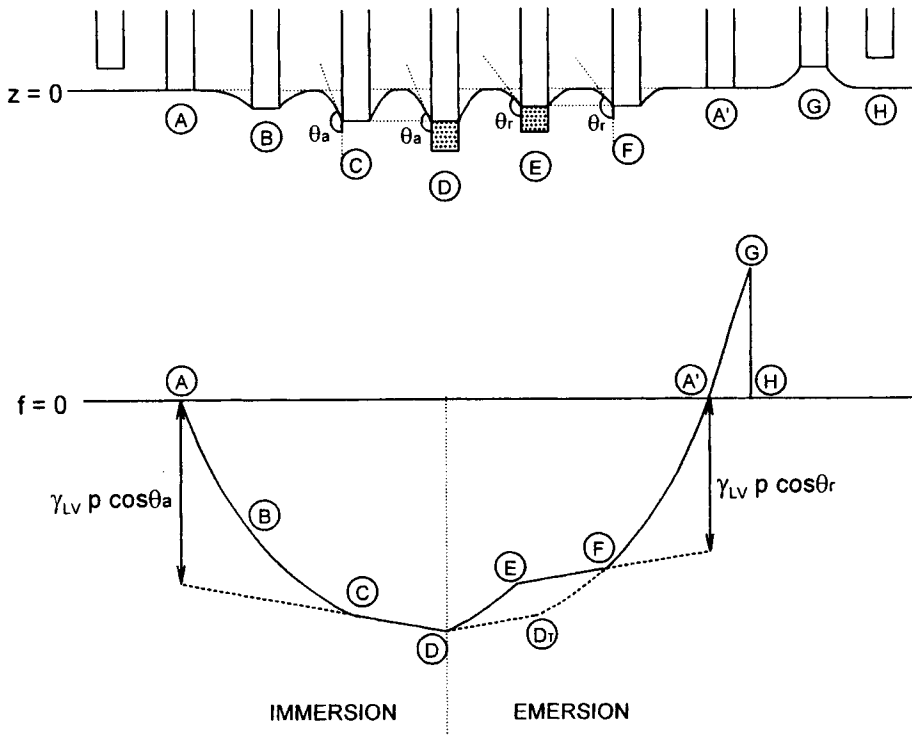
$$w_m = p \gamma_{LV} \cos \phi \quad (3.16)$$



**Figure 3.16.** Meniscus formed with a partially immersed vertical plate and a (a) wetting and (b) non-wetting liquid.

$\phi$  being the *joining angle* of the liquid meniscus on the solid surface, defined by the tangent to the liquid surface at the triple line and the vertical (see Figure 3.16), and  $\gamma_{LV}$  the surface tension of the liquid (as  $w_m$  is a force, surface tension instead of surface energy is used in equation (3.16)). As will be seen below,  $\phi$  corresponds to well-defined contact angles only at some particular points of the  $f(z_b)$  immersion-emersion curve.

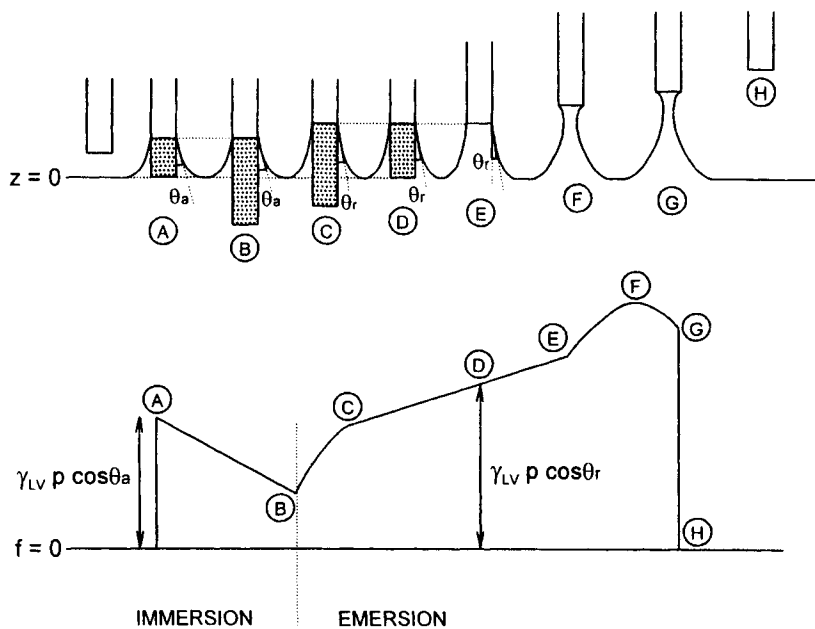
The curve of the variation in the force exerted on the solid during its immersion-emersion in a *non-wetting liquid* ( $\theta_Y > 90^\circ$ ) as a function of the depth of immersion is shown schematically on Figure 3.17 for successive positions of the solid in the liquid. As the solid is lowered, it contacts the liquid (A) and thereafter depresses its surface to form a downward curving meniscus (B). Then, the joining angle  $\phi$  becomes larger and larger until it equals the advancing contact angle  $\theta_a$  and



**Figure 3.17.** Common shape of an experimental curve of variations in the force exerted on a cylindrical solid during its immersion-emersion in a *non-wetting* liquid plotted as a function of the depth of immersion of the solid. The translation rate of the solid is supposed to be infinitely slow. From (Rivollet et al. 1990) [2].

the solid enters the liquid (C). After C, a deeper immersion of the solid does not give rise to any further change in the shape of the meniscus and the change in force is only due to the variation in the buoyancy force, which is linear with  $z_b$  according to equation (3.15) (C-D). The emersion of the solid begins in D. The joining angle changes continuously from  $\theta_a$  to the receding contact angle  $\theta_r$  (D-E). The meniscus has an equilibrium shape from E to F and the change in force is only due to buoyancy. From F to G, the joining angle changes from  $\theta_r$  to  $(\theta_r - 90^\circ)$  where the meniscus falls off the solid. If the solid motion is reversed between points F and A', the curve does not retrace the same path as during the emersion but goes through points F-D<sub>r</sub>-D, equivalent to B-C-D of the first immersion. This is a direct consequence of wetting hysteresis.

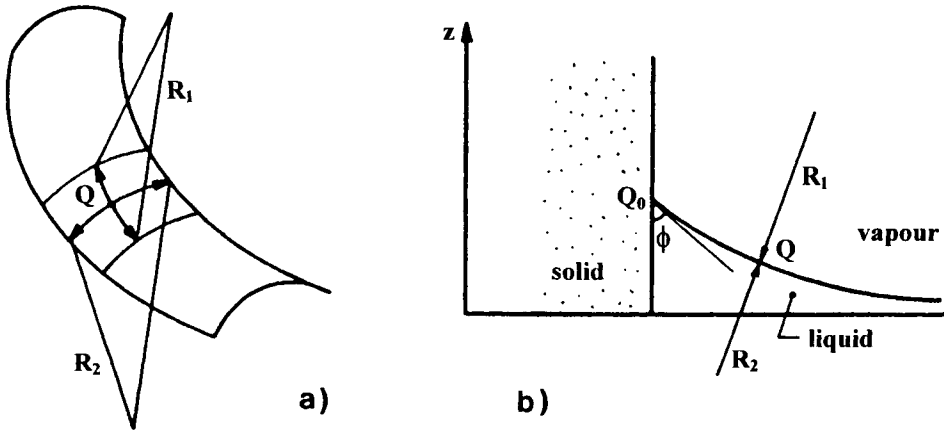
A slightly different series of events occurs when the liquid is *wetting* ( $\theta_v < 90^\circ$ ), as indicated in Figure 3.18. First, the advancing contact angle  $\theta_a$  is



**Figure 3.18.** Common shape of an experimental curve of variations in the force exerted on a cylindrical solid during its immersion-emersion in a *wetting* liquid plotted as a function of the depth of immersion of the solid. The translation rate of the solid is supposed to be infinitely slow. From (Rivollet et al. 1990) [2].

spontaneously reached as soon as the solid touches the liquid. This contact angle is similar to the advancing contact angle measured in a typical sessile drop experiment i.e., an irreversible contact angle. Hence, for smooth ( $R_a < 10$  nm) and chemically homogeneous solid surfaces, this angle is a good estimate (within a few degrees) of the thermodynamic contact angle of the system. Moreover, this step can be used not only to determine  $\theta_a$  values but also to study the spreading kinetics. The variation of the force is linear during the immersion (A-B), as it is only due to the buoyancy contribution. Secondly, from point E, the meniscus is connected to the base of the solid rather than its sides and the joining angle  $\phi$  becomes negative relative to the sides ( $\theta_r - 90^\circ < \phi < \theta_r$ ). When  $\phi$  becomes less than  $(\theta_r - 90^\circ)$  i.e., less than the receding contact angle on the base of the solid, a rupture of the meniscus occurs (G). Note that the curve goes through a maximum at point F when the increase of the buoyancy force is exactly balanced by the decrease of the weight of the meniscus. Although no solid is immersed in the liquid at point F, it can be verified that the hydrostatic pressure is not null in the liquid at  $z_b$  at point F because this pressure is zero for  $z_b = 0$ .

Using equations (3.15) and (3.16), the product  $\gamma_{LV}\cos\phi$  can be determined for each point of the curve A-C of Figure 3.17, as  $f$  and  $z_b$  are measured. Furthermore, the products  $\gamma_{LV}\cos\theta_a$  and  $\gamma_{LV}\cos\theta_r$  can be determined at some specific points of the curves. In the wetting case (Figure 3.18), they can be measured directly at A ( $f = p\gamma_{LV}\cos\theta_a$ ) and D ( $f = p\gamma_{LV}\cos\theta_r$ ) as there is no buoyancy force ( $z_b = 0$ ). In the non-wetting case (Figure 3.17), these values can be deduced by extrapolation of the linear parts C-D and E-F to the vertical of points A and A' respectively where  $z_b = 0$ .



**Figure 3.19.** Geometrical quantities used to describe the shape of a liquid surface. (a) principal curvature radii; (b) vertical position  $z$  of the point  $Q$  of the surface and joining angle  $\phi$  of the liquid profile with the solid. From (Rivollet et al. 1990) [2].

As shown previously, the product  $\gamma_{LV}\cos\phi$  can be measured from experimental values of the force  $f$  (equation (3.15)). To determine  $\theta_a$  and  $\theta_r$ , one must at first calculate  $\gamma_{LV}$ . To this end, the Laplace equation is introduced, which applies at each point  $Q$  of the liquid meniscus surface with a vertical coordinate  $z$  relative to the flat horizontal surface of the bulk liquid (Figure 3.19.b):

$$\Delta P = \gamma_{LV} \left( \frac{1}{R_1} + \frac{1}{R_2} \right) = \rho g z \quad (3.17)$$

Here,  $\Delta P$  is the pressure difference between the sides of the liquid surface and in the case of a meniscus,  $\Delta P$  is equal to the hydrostatic pressure.  $R_1$  and  $R_2$  are the

principal radii of the surface (Figure 3.19.a). Then,  $\gamma_{LV}$  depends on the three unknown quantities  $z$ ,  $R_1$  and  $R_2$ . However, the Laplace equation can be applied at point  $Q_0$  of the triple line (see Figure 3.19.b). Thus, one of the three unknown quantities can be suppressed if the height (or the depth) of the meniscus  $z^*$ , a function of  $\gamma_{LV}$  and  $\phi$ , is measured. This can be done either by a direct optical measurement (Mozzo 1970) or by examining the  $f(z_b)$  curve (Rivollet 1986).

The value of  $z^*$  being known,  $R_1$  and  $R_2$  have now to be determined. This is possible only in a few simple cases featuring a geometry of the solid with a high degree of symmetry.

For a vertical blade of infinite width, the Laplace equation becomes:

$$\frac{\gamma_{LV}}{R_1} = \rho g z \quad (3.18)$$

as  $R_2 \rightarrow \infty$ . According to equation (1.23), the height of the meniscus is given by:

$$z^* = \left( \frac{2\gamma_{LV}}{\rho g} \right)^{1/2} (1 - \sin \phi)^{1/2} \quad (3.19)$$

Here, we recall that the force is written:

$$f = p\gamma_{LV} \cos \phi + \Omega \rho g z_b \quad (3.20)$$

Thus, if  $f$  and  $z_b$  are given by the experimental  $f(z_b)$  curve and  $z^*$  measured by the means of an optical method, the two unknown quantities  $\gamma_{LV}$  and  $\phi$  can be obtained by solving equations (3.19) and (3.20). Note that this procedure can be applied for different  $z_b$  values to increase the accuracy.

For non-wetting liquids, the measurement of the height of the meniscus  $z^*$  is difficult to perform by an optical technique. In this case, one can use the method developed by Rivollet (1986) based on the non-linear parts of the  $f(z_b)$  curve corresponding to the situation where the meniscus is connected to the solid base (part A-C of Figure 3.17). The  $f(z_b)$  curve is obtained by solving equations (3.19) and (3.20) with  $z_b = z^*$ . The value of  $\gamma_{LV}$  is then determined by fitting the calculated curve to the experimental one.

However, although the mathematical problem is solved, interpretation of experiments with non-wetted blade-shaped solids can be problematical. This is because the corners of the blade induce variations in the triple line level and an erratic experimental curve  $f(z_b)$  in comparison to that calculated using equation

(3.18). For that reason, the use of solids of cylindrical shape is preferable in the non-wetting case (Appendix E).

Once  $\gamma_{LV}$  is known,  $\theta_a$  and  $\theta_r$  can be determined from the forces measured at points A and D (see Figure 3.18). For non-wetting liquids,  $\theta_a$  and  $\theta_r$  are quasi-reversible contact angles and are close to the maximum advancing and minimum receding contact angles for the solid substrate. Consequently, these values can differ greatly from the Young contact angle even for rather smooth solid surfaces (Table 3.3). Recalling that the stable equilibrium contact angle on a rough surface is the Wenzel contact angle  $\theta_W$  (equation (1.35)), this angle can be calculated from  $\theta_a$  and  $\theta_r$  values using (Rivollet 1986):

$$\theta_W = \text{Arc cos} \left( \frac{\cos \theta_a + \cos \theta_r}{2} \right) \quad (3.21)$$

Then, the Young contact angle is calculated combining equation (3.21) and the equation of Wenzel, yielding:

$$\theta_Y = \text{Arc cos} \left( \frac{\cos \theta_a + \cos \theta_r}{2s_r} \right) \quad (3.22)$$

where  $s_r$  is the Wenzel parameter equal to the ratio of the actual to the planar area. For well-polished surfaces ( $R_a < 100$  nm),  $s_r$  is very close to unity and equation (3.22) can be applied with a good accuracy taking  $s_r = 1$ . For substrates with a high roughness and for which the value of  $s_r$  is not known accurately, neither are values of  $\theta_Y$  calculated by equation (3.22) accurate (De Jonghe et al. 1990).

**Table 3.3.** Capillary properties of molten Sn/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub> system measured by the wetting balance technique at 1370K using Al<sub>2</sub>O<sub>3</sub> cylinders (De Jonghe et al. 1990).  $\theta_Y$  is calculated by equation (3.22).

$R_a$ (nm)	$s_r$	$\sigma_{LV}$ (mJ/m <sup>2</sup> )	$\theta_a$ (deg)	$\theta_r$ (deg)	$\theta_Y$ (deg)
5	1.0000	485	131	126	128
8.5	1.0001	465	137	116	126

Until now, the translation rate of the solid has been considered to be infinitely slow. In practice, the contact angle measured during an immersion-emersion cycle



performed with a constant translation rate  $U$ , is a function of  $U$  (see Figures 2.1 and 2.12). For instance, during the *immersion* of a solid in a non-wetting liquid performed with  $U \neq 0$ , a contact angle  $\theta_i$  greater than  $\theta_a$  was observed (Rivollet et al. 1990). If the motion of the solid is stopped between points C and D of Figure 3.17, then  $\theta_i$  reaches the static contact angle  $\theta_a$ . Similarly, the contact angle  $\theta_e$  measured during the *emersion* of the solid is less than  $\theta_r$ . It has been shown that for non-wetting systems, the difference between  $\theta_i$  and  $\theta_a$ , and  $\theta_e$  and  $\theta_r$ , is less than  $5^\circ$  for  $U \leq 1$  mm/min and smooth solids (Rivollet 1986, Rivollet et al. 1990). In practice, it is preferable to work with finite but low translation rates to determine wetting parameters because dynamic contact angles are more reproducible than static contact angles measured with  $U = 0$ .

Examples of measurements of wetting parameters carried out by the wetting balance technique are given in Table 3.4 for three non-reactive liquid/solid couples. Liquid metals were either non-wetting or wetting and the solids were cylinders. For non-wetting liquids (Sn and Al on  $\text{Al}_2\text{O}_3$ ),  $\theta_Y$  was calculated from  $\theta_a$  and  $\theta_r$  by means of equation (3.22). For molten Pb on solid Fe,  $\theta_Y$  was estimated by the irreversible advancing contact angle measured at point A (Figure 3.18). In all cases, contact angle values are in good agreement with those obtained by the sessile drop technique on solid plates.  $\sigma_{LV}$  values (equal to  $\gamma_{LV}$  values) measured by the wetting balance technique differ somewhat from values measured by other methods (see Table 4.1) but the differences remain reasonable.

**Table 3.4.** Comparison of  $\theta_Y$  and  $\sigma_{LV}$  values measured by the wetting balance technique and other methods.

Liquid	Solid	T (K)	Wetting balance		Sessile drop	$\sigma_{LV}$ (mJ/m <sup>2</sup> ) (from Table 4.1)
			$\sigma_{LV}$ (mJ/m <sup>2</sup> )	$\theta_Y$ (deg)	$\theta_Y$ (deg)	
Sn	$\alpha\text{-Al}_2\text{O}_3$	1373	487 <sup>(a)</sup>	128 <sup>(a)</sup>	126 $\pm$ 4 <sup>(c) (d)</sup>	474
Al	$\alpha\text{-Al}_2\text{O}_3$	1073	890 <sup>(a)</sup>	92 <sup>(a)</sup>	90 <sup>(e) (f)</sup>	846
Pb	Fe	1073	440 <sup>(b)</sup>	44 <sup>(b)</sup>	48 <sup>(g)</sup>	410

<sup>(a)</sup> (De Jonghe et al. 1990), <sup>(b)</sup> (Rivollet 1986), <sup>(c)</sup> (Rivollet et al. 1987), <sup>(d)</sup> (Naidich 1981), <sup>(e)</sup> (Landry and Eustathopoulos 1996), <sup>(f)</sup> (Naidich et al. 1983), <sup>(g)</sup> (Gomez-Moreno et al. 1982)

A standard electronic-zero microbalance can measure variations of masses of hundreds of milligrammes with an accuracy of 0.01%. Consequently, solid plates or cylinders of a few millimeters in perimeter are large enough to yield an excellent

accuracy. However, large quantities of liquid (several tens of grammes) are needed to ensure a nearly flat liquid-vapour surface. Hence, this method is not appropriate for study of expensive liquid materials. Nevertheless, the wetting balance technique offers several experimental advantages. It allows the study of solids with non-planar surfaces, and particularly those with cylindrical shapes, such as the fibres or monofilaments used in composites. Additionally, fundamental studies on contact angle hysteresis can be performed and the effect on the contact angle of the relative velocity of the solid and the liquid can be examined. This method can also be used to follow spreading kinetics, albeit only for wetting liquids. Wetting in reactive liquid/solid systems can be studied, providing that the variation of the solid perimeter owing to interfacial reaction remains negligible in the course of an immersion-emersion cycle.

### 3.3. ACCURACY OF CONTACT ANGLE DATA

Almost all the data on contact angles relevant to high temperature materials have been obtained since 1950. The subsequent decades have seen great progress in the chemical and morphological characterization of surfaces and gaseous atmospheres as well as the greater availability of pure materials, and these changes have allowed contact angle measurements to be made for increasingly well defined solid/liquid/vapour systems. However, if all contact angle data in the literature measured by the sessile drop method for a given liquid/solid system at the same temperature are considered, the experimental values of  $\theta$  can vary by several tens of degrees. In the Sn/Al<sub>2</sub>O<sub>3</sub> system for instance, values of  $\theta$  lie between 108° and 174°, and this leads to a variation of the work of adhesion of two orders of magnitude! This example is not exceptional as shown by similar dispersion observed for Ni, Fe or Cu on Al<sub>2</sub>O<sub>3</sub> (Table 3.5). This scatter is due principally to the uncontrolled effects of substrate roughness and of oxygen partial pressure in the furnace rather than errors in the measurement of the contact angle, which are only a few degrees (typically  $\pm 3^\circ$ ).

We saw in Section 3.1.1 that an average roughness much less than 100 nm is needed if the value of  $\theta_Y$  is to be measured accurately to within a few degrees. However, many of the published data have been obtained for “polished” surfaces, i.e., without any quantification of surface roughness. In practice, many of polished surfaces have roughness in the micron scale and this can lead to values of the advancing contact angle  $\theta_a$  being higher than  $\theta_Y$  by tens of degrees.

Generally, smooth surfaces are more easily obtained with monocrystals. The same average roughness  $R_a$  can be obtained by mechanical polishing of polycrystals but this operation often leads to an “accidental” roughness on this type

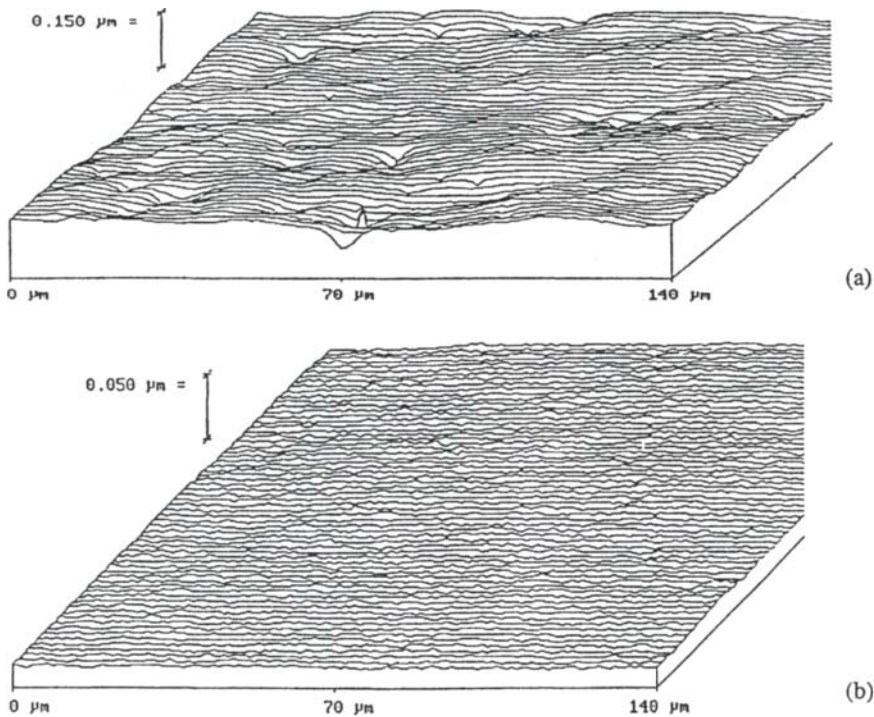
**Table 3.5.** Minimum and maximum values of contact angle measured for some pure metals on alumina. Results come from data compilations given in references.

Metal	Temperature (K)	$\theta_{\min} - \theta_{\max}$ (deg)	Reference
Ni	1823	100 – 141	(Eustathopoulos and Passerone 1978, Beruto et al. 1981)
Fe	1823	109 – 141	(Eustathopoulos and Passerone 1978, Beruto et al. 1981)
Cu	1423	114 – 170	(Li 1988, Tomsia et al. 1998)
Sn	1373	108 – 174	(Rivollet et al. 1987)

of substrate. For example, holes caused by the decohesion of grains can have a negligible influence on the average roughness but can pin the triple line and prevent spreading of the drop on the substrate. Moreover, use of polycrystals can lead to roughening at high temperature by grain boundary grooving, a process which occurs easily with metallic substrates (Figure 3.2). Solids obtained by sintering, as are most ceramics, have some porosities in the micrometre scale which also can pin the triple line, especially of non-wetting liquids (Figure 3.20). An additional advantage of monocrystals is that they minimize and even prevent the segregation of impurities to ceramic surfaces in short-time experiments which can occur through a rapid diffusion in the grain boundaries of polycrystalline materials. For all these reasons, contact angle values measured on monocrystals have to be preferred when the other experimental conditions (purity of materials, atmosphere, etc) are similar.

The second important cause of scattering of contact angle data is pollution from the atmosphere, mainly oxygen. For instance, a liquid metal on a ceramic surface in the low temperature range and/or in an atmosphere with a high  $P_{O_2}$  (a “bad” vacuum or impure neutral gas) can yield very high apparent contact angles due to an oxide film covering the liquid metal. In these conditions, no real interface between the metal and the substrate exists. Typical examples are Al on  $Al_2O_3$  or C substrates (Landry et al. 1996b). Similar effects can be produced by uncontrolled oxidation of the solid surface, for instance of metallic solids or non-oxide ceramics like SiC or  $Si_3N_4$  (see Sections 7.1.1.1 and 7.1.2.2).

At high temperatures or in an atmosphere with a low  $P_{O_2}$ , oxide films are often eliminated by dissolution in the metal, by thermodynamic decomposition or by formation of volatile sub-oxides. Even in these conditions, oxygen can still affect wettability, for instance by adsorption at metal/oxide interfaces. This effect leads to contact angles lower than the nominal contact angle of the inert system. Some examples of these oxygen effects are given in Section 6.4. Therefore, when contact



**Figure 3.20.** (a) Surface profile of sintered TiC after polishing. Pores opening on the surface can be seen and are responsible for the relatively high roughness of this substrate (average roughness  $R_a = 10$  nm, maximum roughness  $R_t = 200$  nm). For comparison, the surface profile of monocrystalline SiC after polishing is shown in (b) ( $R_a = 2$  nm,  $R_t = 10$  nm). From (Landry 1995).

angle values of the literature are used in a particular application, one has to verify that the working atmosphere is similar to that used for the determination of the contact angle.

To estimate the best accuracy that can be expected for contact angle values, results obtained for the non-reactive Au/monocrystalline  $\text{Al}_2\text{O}_3$  system either by the same team for different runs or by different laboratories are assembled, as shown in Table 3.6. This system is particularly simple as the surface properties of neither gold nor alumina seem to depend on values of oxygen partial pressure (Gallois 1980, Chatain et al. 1993). Moreover, the use of monocrystalline substrates allows reduction of surface roughness to the nanometre scale. The data in Table 3.6 show that, even for this very simple system, the accuracy of contact angle values is hardly better than  $\pm 5^\circ$ , leading to an uncertainty in work of adhesion

values of  $\pm 17\%$ . As substrates with different orientations were used, part of this scatter may be due to crystallographic effects.

**Table 3.6.** Contact angle values in the Au/monocrystalline  $\text{Al}_2\text{O}_3$  system at 1373K.

Atmosphere	Substrate orientation	$\theta$ (deg)	Reference
high vacuum, He, He- $\text{O}_2$	random	$131 \pm 2$	(Chatain et al. 1993)
high vacuum	(11 $\bar{2}$ 3)	141	(Brennan and Pask 1968)
high vacuum, Ar, Ar- $\text{H}_2$	(11 $\bar{2}$ 3)	$140 \pm 3$	(Gallois 1980)
high vacuum	(0001), (11 $\bar{2}$ 3)	138	(Naidich 1981)
He	random	$139 \pm 2$	(Rivollet et al. 1987)
air	not specified	$136 \pm 6^*$	(Grigorenko et al. 1995)

\* at 1473K

If gold is replaced by another metal with a greater affinity for oxygen and if rougher substrates are used, the scatter of contact angle values in non-wetting systems can be higher, as observed in Sn/ $\text{Al}_2\text{O}_3$  and Cu/ $\text{Al}_2\text{O}_3$  couples (Table 3.5). For wetting systems, the effect of roughness on the apparent contact angle is weaker as shown by the data given in Table 3.7 for a Si-rich Co-Si alloy on different types of SiC (Gasse 1996). Varying the average roughness by more than two orders of magnitude caused the contact angle to vary by less than 10 degrees, corresponding to a scattering of work of adhesion values of only  $\pm 4\%$ . This lower roughness sensitivity for a low contact angle system explains the good agreement observed for values of  $\theta$  for pure molten Si on the basal plane of  $\alpha$ -SiC (Table 3.8). This agreement is obtained despite the use of different polarity faces of SiC and different furnace atmospheres for a system in which both the liquid (Si) and the solid (SiC) have a high affinity for oxygen. In fact, owing to the high melting temperature of Si, both the Si and SiC surfaces are easily deoxidised by formation of volatile  $\text{SiO}$ , even in commercially pure argon containing several ppm of oxygen and water. At the molten Si/vapour surface as well as at the solid/liquid/vapour triple line,  $\text{P}_{\text{O}_2}$  is fixed locally at very low values by the Si itself rather than by the impinging oxygen molecules desorbed by the furnace walls (Drevet et al. 1993).

**Table 3.7.** Contact angle values in the non-reactive Co-66.6 at.% Si/SiC system at 1623K in a high vacuum (Gasse 1996).

SiC	$R_a$ (nm)	$\theta$ (deg)
sintered	50	30
sintered	900	20
monocrystal	2	29
monocrystal	60	22

**Table 3.8.** Contact angle values in the Si/monocrystalline  $\alpha$ -SiC system.

Atmosphere	Temperature (K)	$\theta$ (deg)	Reference
vacuum	1753	36	(Naidich and Nevodnik 1969)
vacuum	1713	30 – 45	(Yupko and Gnesin 1973)
Ar	1703	38	(Li and Hausner 1991)
Ar	1770	38	(Nikolopoulos et al. 1992)
He	1690	$34 \pm 2$	(Drevet et al. 1993)
vacuum	1697	39 (Si face of SiC) 47 (C face of SiC)	(Rado 1997)

Contact angles measured by different teams for the reactive Cu-1 at.% Cr/carbon system are given in Table 3.9. In this system, Cr reacts with carbon to form a layer of wettable chromium carbide. In sessile drop experiments at about 1400 K, a quasi-stationary contact angle  $\theta_F$  is reached after about 100 seconds (see Figure 2.26). It is noteworthy that the reproducibility of  $\theta_F$  values measured by the same team for eight different runs ( $41 \pm 4^\circ$  (Landry et al. 1997)) is comparable to that found for  $\theta$  values of non-reactive systems. Moreover, the agreement between results obtained at 1400 K by different teams is satisfactory. The lower contact angles obtained by Nogi et al. (1990) can be explained by the much higher temperature used by these authors.

At present, when working with high-purity materials, smooth solid surfaces and low  $P_{O_2}$  atmospheres, the thermodynamic contact angle in a particular system can be determined at best within about five degrees. Roughness must be very low, particularly in non-wetting systems in order to obtain such an accuracy. The control of  $P_{O_2}$  is critical for oxidisable liquids and solids, specially at relatively low temperatures, and dynamic vacuum is often preferable to a static neutral gas atmosphere.

**Table 3.9.** Stationary contact angle values in the reactive Cu-1 at.% Cr/carbon system.

Substrate	Atmosphere	Temperature (K)	$\theta_F$ (deg)	Reference
vitreous carbon	high vacuum	1423	40	(Mortimer and Nicholas 1973)
graphite	Ar	1403	45	(Devincent and Michal 1993)
vitreous carbon	high vacuum	1373	$41 \pm 4$	(Landry et al. 1997)
graphite	Ar-5% H <sub>2</sub>	1773	20–30	(Nogi et al. 1990)

### 3.4. CONCLUDING REMARKS

The variants of the sessile drop method remain the simplest and most employed techniques for wetting studies despite the great amount of information that can be derived from the wetting balance technique. When only contact angle data are needed, small droplets weighing typically  $10^{-2}$ – $10^{-1}$  g are preferable because they allow deformation of the drop by gravity to be neglected. For the measurement of the liquid/vapour surface energy, larger droplets usually weighing 1g or more are necessary to achieve a good accuracy. In all cases, an automatic system for data acquisition and image analysis is desirable.

When the optimal conditions are satisfied, i.e., a well-controlled atmosphere, a pure, homogeneous and smooth solid surface and an accurate measurement system, the Young contact angle and the liquid surface energy can be derived with an accuracy of  $\pm 3$  deg and  $\pm 2\%$  respectively allowing the work of adhesion ( $W_a = \sigma_{LV}(1 + \cos\theta)$ ) to be determined with an accuracy of about 10%.

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## Chapter 4

# Surface energies

As shown by the Young-Dupre equation (1.45), the equilibrium contact angle value results from the competition between adhesion forces between the liquid and the solid, as measured by the work of adhesion  $W_a$ , and cohesion forces in the liquid, expressed by its surface energy,  $\sigma_{LV}$ . Thus knowledge of this last quantity and of its variation with temperature, composition of the liquid and environmental parameters (mainly  $P_{O_2}$ ), is necessary to explain wetting behaviour. For this reason, the bulk of data given below are for  $\sigma_{LV}$  values. However, a limited amount of data will be presented also for two other quantities included implicitly in the Young-Dupré equation, i.e.,  $\sigma_{SV}$  and  $\sigma_{SL}$ .

### 4.1. DATA FOR METALS AND ALLOYS

Reliable values of  $\sigma_{LV}$  of pure metals for most commonly used metals have been obtained during the last forty years, using mainly:

- 1) the “maximum bubble pressure” technique in which the pressure necessary to push a gas bubble through a capillary into the liquid under investigation is measured,
- 2) the sessile drop technique described in Section 3.1 and
- 3) the “drop weight” technique in which a drop is formed at the end of a rod of the metal heated to its melting point. The  $\sigma_{LV}$  value is deduced from the weight of the drop after its detachment.

Only the two first methods allow measurement of the temperature coefficient of the surface energy. The maximum bubble pressure technique is well-adapted for metals with low and intermediate melting points and specially for oxidizable metals, while the sessile drop technique has been applied with success to measure  $\sigma_{LV}$  values up to 1500°C. The drop weight method is particularly useful for very high melting-point metals because it avoids liquid contact with container materials. This is also true for the recently developed “levitation drop” technique that analyses the oscillation spectrum of a magnetically levitated droplet.

#### 4.1.1 Pure liquid metals

Selected values of  $\sigma_{LV}$  and the temperature coefficient  $\sigma'_{LV} (= d\sigma_{LV}/dT)$  are given in Table 4.1, taken from the reference compilation (Eustathopoulos et al. 1999) in

which the selection criteria are described in detail. The metals have been divided into two classes A and B. For a metal of *class A*, the accuracy of  $\sigma_{LV}$  at the melting temperature  $T_F$ , estimated from the experimental measurements of the literature reviewed by Keene (1993), is better than  $\pm 5\%$  and the accuracy of  $\sigma'_{LV}$  is better than  $\pm 50\%$ . For a metal of *class B*, the accuracies are worse than  $\pm 5\%$  and  $\pm 50\%$ .

In the case of Fe and Si, although  $\sigma_{LV}$  values at the melting point measured by several authors are not very different, a high difference in  $\sigma'_{LV}$  values is observed. For this reason two values of  $\sigma'_{LV}$  are given in Table 4.1 characteristic of “low” and “high” values quoted in the literature.

**Table 4.1.** Experimental values of  $\sigma_{LV}$  vs temperature,  $T$ , taken from the compilation of Eustathopoulos et al. (1999) and values of  $\sigma'_{LV}$  calculated according to (Eustathopoulos et al. 1998) for Fe and Si, for class B metals except Te and for class A metals for which experimental values have not been measured ( $\sigma_{LV}(T) = \sigma_{LV}(T_F) + \sigma'_{LV}[T - T_F]$  where  $T_F$  is the melting temperature).

Element	$T_F$ (K)	Class	Experimental data $\sigma_{LV}(T)$ (mJ.m <sup>-2</sup> )	Calculated data $\sigma'_{LV}$ (mJ.m <sup>-2</sup> .K <sup>-1</sup> )
Ag	1234	A	910 - 0.17 (T - $T_F$ )	
Al	933	A	867 - 0.15 (T - $T_F$ )	
Au	1336	A	1138 - 0.19 (T - $T_F$ )	
Ba	1002	B	267 - 0.07 (T - $T_F$ )	-0.06
Be	1560	B	1320	-0.25
Bi	544	A	374 - 0.08 (T - $T_F$ )	
Ca	1112	A	366 - 0.11 (T - $T_F$ )	
Cd	594	B	642 - 0.20 (T - $T_F$ )	-0.16
Ce	1071	B	794 - 0.07 (T - $T_F$ )	-0.09
Co	1768	A	1884 - 0.37 (T - $T_F$ )	
Cr	2130	B	1628 - 0.20 (T - $T_F$ )	-0.33
Cs	302	A	69 - 0.06 (T - $T_F$ )	
Cu	1357	A	1355 - 0.19 (T - $T_F$ )	
Dy	1682	B	648 - 0.13 (T - $T_F$ )	-0.15
Er	1795	B	637 - 0.12 (T - $T_F$ )	-0.16
Eu	1090	B	264 - 0.05 (T - $T_F$ )	-0.16
Fe	1809	A	1855 - 0.23 (T - $T_F$ ) 1844 - 0.5 (T - $T_F$ )	-0.29
Ga	303	A	708 - 0.07 (T - $T_F$ )	
Gd	1585	B	664 - 0.06 (T - $T_F$ )	-0.13
Ge	1210	A	587 - 0.105 (T - $T_F$ )	
Hf	2500	A	1490	-0.19
Hg	234	A	500 - 0.215 (T - $T_F$ )	

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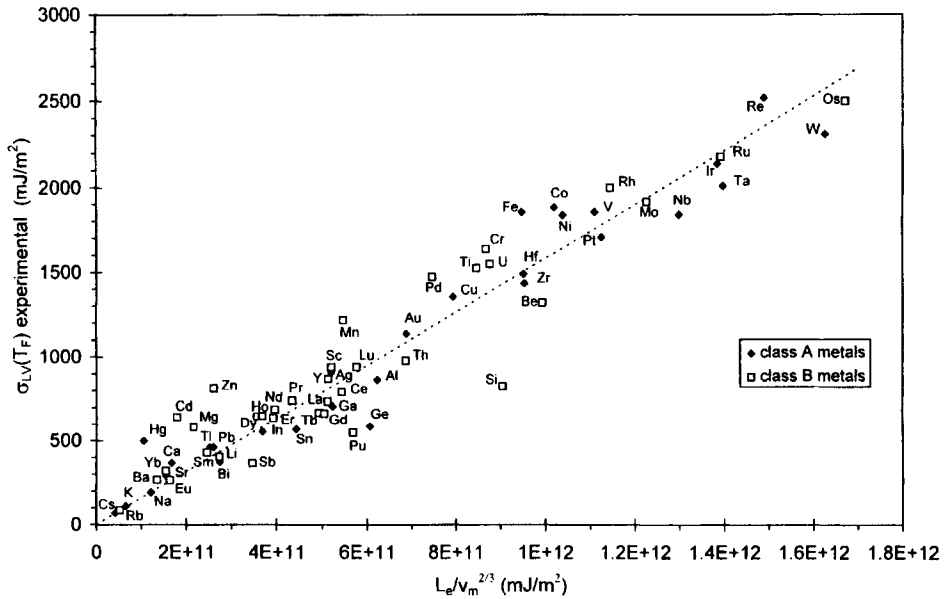
<b>Ho</b>	1743	B	650 - 0.12 (T - T <sub>F</sub> )	-0.15
<b>In</b>	430	A	555 - 0.12 (T - T <sub>F</sub> )	
<b>Ir</b>	2716	A	2140	-0.18
<b>K</b>	336	A	112 - 0.08 (T - T <sub>F</sub> )	
<b>La</b>	1193	B	737 - 0.11 (T - T <sub>F</sub> )	-0.09
<b>Li</b>	454	B	404 - 0.16 (T - T <sub>F</sub> )	-0.14
<b>Lu</b>	1936	B	940 - 0.07 (T - T <sub>F</sub> )	-0.21
<b>Mg</b>	922	B	583 - 0.15 (T - T <sub>F</sub> )	-0.16
<b>Mn</b>	1517	B	1219 - 0.35 (T - T <sub>F</sub> )	-0.23
<b>Mo</b>	2890	B	1915	-0.23
<b>Na</b>	371	A	192 - 0.095 (T - T <sub>F</sub> )	
<b>Nb</b>	2740	A	1840	-0.19
<b>Nd</b>	1289	B	689 - 0.09 (T - T <sub>F</sub> )	-0.11
<b>Ni</b>	1726	A	1838 - 0.42 (T - T <sub>F</sub> )	
<b>Os</b>	3300	B	2500	-0.29
<b>Pb</b>	601	A	462 - 0.11 (T - T <sub>F</sub> )	
<b>Pd</b>	1825	B	1475 - 0.28 (T - T <sub>F</sub> )	-0.24
<b>Pr</b>	1204	B	743 - 0.09 (T - T <sub>F</sub> )	-0.14
<b>Pt</b>	2042	A	1707	-0.29
<b>Pu</b>	913	B	550	-0.13
<b>Rb</b>	313	B	85 - 0.07 (T - T <sub>F</sub> )	-0.05
<b>Re</b>	3453	A	2520	-0.21
<b>Rh</b>	2233	B	2000	-0.24
<b>Ru</b>	2523	B	2180	-0.28
<b>Sb</b>	904	B	366 - 0.04 (T - T <sub>F</sub> )	-0.10
<b>Sc</b>	1812	B	939 - 0.12 (T - T <sub>F</sub> )	-0.21
<b>Se</b>	494	B	103 - 0.09 (T - T <sub>F</sub> )	
<b>Si</b>	1685	B	827 - 0.48 (T - T <sub>F</sub> )	-0.19
			749 - 0.15 (T - T <sub>F</sub> )	
<b>Sm</b>	1345	B	430 - 0.07 (T - T <sub>F</sub> )	-0.10
<b>Sn</b>	505	A	570 - 0.11 (T - T <sub>F</sub> )	
<b>Sr</b>	1041	A	289 - 0.075 (T - T <sub>F</sub> )	
<b>Ta</b>	3287	A	2010	-0.24
<b>Tb</b>	1630	B	669 - 0.06 (T - T <sub>F</sub> )	-0.16
<b>Te</b>	723	B	178	
<b>Th</b>	2028	B	978	-0.14
<b>Ti</b>	1943	B	1525	-0.28
<b>Tl</b>	577	A	461 - 0.09 (T - T <sub>F</sub> )	
<b>U</b>	1405	B	1550 - 0.14 (T - T <sub>F</sub> )	-0.16
<b>V</b>	2175	A	1855	-0.26
<b>W</b>	3653	A	2310	-0.20
<b>Y</b>	1799	B	872 - 0.09 (T - T <sub>F</sub> )	-0.11
<b>Yb</b>	1097	B	320 - 0.10 (T - T <sub>F</sub> )	-0.17
<b>Zn</b>	693	B	815 - 0.25 (T - T <sub>F</sub> )	-0.22
<b>Zr</b>	2125	A	1435	-0.19

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Equation (1.15), when applied to monoatomic liquids, predicts that the molar surface energy  $\sigma_{LV} \cdot \Omega_m$  (with  $\Omega_m = N_a \cdot \omega$ ) is proportional to the heat of evaporation of the liquid,  $L_e$ , and to a structural parameter  $m_1$ . If  $m_1$  is the same for all metals,  $\sigma_{LV}$  is expected to scale with the quantity  $L_e / \Omega_m$ . It was shown in (Eustathopoulos et al. 1998) that equation (1.15), valid in principle only at 0K, holds also at  $T_F$ . As  $\Omega_m$  is proportional to  $v_m^{2/3}$  ( $v_m$  denoting the molar volume), one obtains:

$$\sigma_{LV}(T_F) = C_1 \frac{L_e}{v_m^{2/3}} \quad (4.1)$$

where  $C_1$  is a dimensionless constant equal to  $0.25 \times 10^{-8}$ .



**Figure 4.1.** Experimental values of surface energy of pure liquid metals at their melting temperature plotted as a function of  $L_e/v_m^{2/3}$ . From (Eustathopoulos et al. 1998) [12].

Figure 4.1 shows that the correlation predicted by equation (4.1) is satisfied rather well. The slope of the straight line is  $0.16 \times 10^{-8}$  in good agreement with the value of  $C_1$ , considering the crudeness of the structural and energetical model of

Skapski (1948, 1956) used as a basis in (Eustathopoulos et al. 1998) to derive equation (4.1). Note that because the ratio  $L_e/T_F$  for pure metals is approximately constant, correlations between  $\sigma_{LV}(T_F)$  and  $T_F/v_m^{2/3}$  are also to be expected and have been found to hold (Keene 1993).

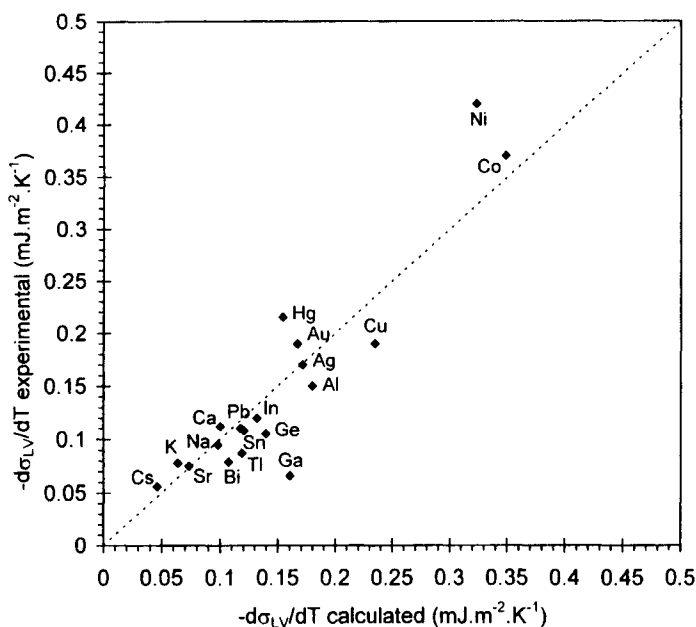
The temperature coefficient of surface energy,  $\sigma'_{LV}$ , is given by (Eustathopoulos et al. 1998):

$$\sigma'_{LV}(T) = -\frac{C_2 S_S}{v_m^{2/3}} + \frac{2}{3} \frac{\sigma_{LV}(T_F)}{\rho} \frac{d\rho}{dT} \quad (4.2)$$

where  $C_2$  is a constant and  $\rho$  is the liquid density.  $S_S$ , a quantity found to be nearly constant for all metals, is the molar surface excess entropy and results from an atomic disorder at the surface higher than in the bulk liquid ( $S_S > 0$ ). Thus, the first term of equation (4.2) is the entropy contribution of  $\sigma'_{LV}$  while the second term reflects the fact that the number of atoms per unit area contributing to the surface energy decreases with temperature. The contribution of the second term varies from 30% of the total for low  $\sigma_{LV}$  metals to 55% for high  $\sigma_{LV}$  metals. A comparison of experimental  $\sigma'_{LV}$  data for class A metals and calculated values from equation (4.2) with  $C_2 S_S = 5.7 \times 10^{-5} \text{ mJ.mole}^{-1}.\text{K}^{-1}$  is shown on Figure 4.2. In view of the good agreement, equation (4.2) was used to calculate  $\sigma'_{LV}$  values for class B metals and for metals for which  $\sigma'_{LV}$  has not been measured up to now (Table 4.1).

The surface energies of pure metals can be decreased by segregation of oxygen. This impurity can come from within the bulk of the liquid, from the gaseous environment or from the solid substrate used in wetting experiments. As will be discussed in more detail in Section 6.4.1, oxygen dissolved in bulk metal develops strong interactions accompanied by charge transfers from the metal to oxygen. Because these interactions create strong perturbations of the metallic bond adjacent to an oxygen atom, there is a marked tendency for oxygen to segregate at the free surface where the perturbation is partially relaxed.

Figure 4.3 shows the change of  $\sigma_{LV}$  of Cu as a function of the partial pressure of oxygen,  $P_{O_2}$ , set by using gas mixtures of Ar/H<sub>2</sub> or CO/CO<sub>2</sub>. The  $\sigma_{LV}$  values remain constant for a range of  $P_{O_2}$  from  $10^{-20}$  to  $10^{-12}$  atm at a value of  $1320 \text{ mJ.m}^{-2}$ , the surface energy of pure Cu. Above  $P_{O_2} \approx 10^{-12}$  atm,  $\sigma_{LV}$  decreases smoothly and at  $P_{O_2} \approx 10^{-9}$  atm the slope reaches a near constant value corresponding to a surface saturated with oxygen. It is worthwhile noting that the saturation level is attained for a bulk molar fraction of oxygen as low as  $1.5 \times 10^{-4}$  i.e., about 40 ppm. At higher  $P_{O_2}$  values,  $\sigma_{LV}$  continues to decrease, even though



**Figure 4.2.** Comparison between experimental and calculated values of the temperature coefficient of surface energy using equation (4.2) for class A liquid metals. From (Eustathopoulos et al. 1998) [12].

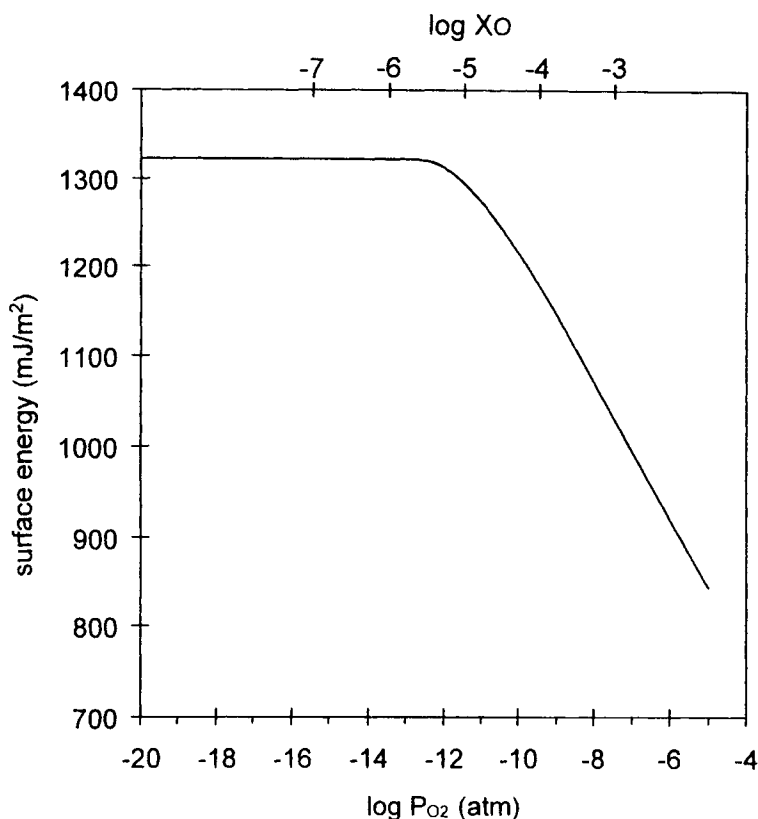
the surface composition remains nearly constant, because of the increase of the chemical potential of oxygen. No measurements were performed at  $P_{O_2}$  higher than  $10^{-5}$  atm to avoid precipitation of Cu oxide.

An analysis of this type of  $\sigma_{LV}$ - $P_{O_2}$  curve using the Gibbs adsorption equation is given in Section 6.4.1 for Ag which exhibits a similar behaviour and further discussion of the surface energy variations of metal-oxygen systems is given in (Joud and Passerone 1995). Experimental data for the effect of oxygen on  $\sigma_{LV}$  exist for Ag (Sangiorgi et al. 1982), Al (Goumiri and Joud 1982), Bi (Hasouna et al. 1991), Co (Ogino et al. 1982), Cr (Chung et al. 1992), Fe (Nakashima et al. 1992), Hg (Nicholas et al. 1961), Ni (Sharan and Cramb 1997), Pb (Passerone et al. 1983), Si (Niu et al. 1998) and Sn (Taimatsu and Sangiorgi 1992).

Figure 4.4 shows that O and other elements developing strong interactions with Fe such as S, Se and Te decrease its surface energy markedly (Kozakevitch 1968, Ogino et al. 1983). The effect of N is much smaller while that of dissolved C and P is very weak or even negligible (Kozakevitch 1968).

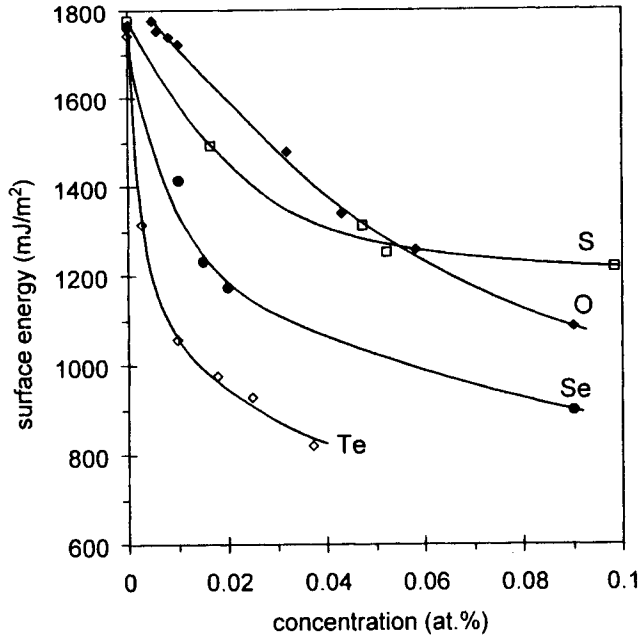
Kozakevitch and Urbain (1961) discussed the nature of the surface layer saturated with adsorbed oxygen (or another non-metallic element) by comparing





**Figure 4.3.** Experimental values of surface energy of liquid Cu-O mixtures as a function of partial pressure of oxygen  $P_{O_2}$  or molar fraction of dissolved oxygen  $X_O$  at 1108°C. Data from work reported in (Gallois and Lupis 1981) [13].

the area of the adsorbed species, as calculated from the adsorption isotherm (equation (6.16)), with that of neutral atoms or with the area of oxygen ions at an appropriate ionic compound surface. For instance, in the case of oxygen adsorbed at the liquid Fe surface, the area of  $\approx 9 \text{ \AA}^2$  is much closer to that occupied by oxygen ions in the plane (111) of FeO ( $8.2 \text{ \AA}^2$ ) than to the  $1.2 \text{ \AA}^2$  of neutral oxygen atoms in a close-packed structure. Kozakevitch and Urbain concluded that the adsorption layer was an ionic double-layer, the vapour side of the surface being occupied by anions and the liquid side by positively charged metal atoms. The formation of such a layer was assumed to produce a substantial decrease of the surface energy.



**Figure 4.4.** Surface energies of solutions of O, S, Se and Te in liquid Fe at 1600C (Ogino et al. 1983) [14].

#### 4.1.2 Liquid alloys

The surface energy of a metal can be affected also by the adsorption of a metallic solute. The surface energy of a binary A-B alloy has been calculated by Guggenheim (1945) from a regular solution model using mean-field approximation statistics (in which the atoms A and B are supposed to be randomly distributed on the sites of the “quasi-crystalline liquid” lattice) and a single parameter  $\lambda$  (*the exchange energy*) which accounts for the change of energy of the system when heteroatomic A-B pairs are formed from homoatomic A-A and B-B pairs:

$$\lambda = ZN_a \left[ \varepsilon_{AB} - \frac{\varepsilon_{AA} + \varepsilon_{BB}}{2} \right] \quad (4.3)$$

In (4.3),  $Z$  is the mean coordination number in the liquid,  $N_a$  is the Avogadro's number and  $\varepsilon_{ij}$  is the interaction energy of an i-j pair. Recalling that bond energies  $\varepsilon_{ij}$  have negative values, a high positive value of  $\lambda$  is due to A-B interactions being less strong than the average value of homoatomic A-A and B-B interactions. In the

regular solution model, the enthalpy of mixing of A-B alloy,  $\Delta H_m$ , is simply given by

$$\Delta H_m = \lambda X_B(1 - X_B) \quad (4.4)$$

where  $X_B$  is the molar fraction of B in the A-B alloy.

The interface between the liquid and the vapour phase is assumed to be a liquid monolayer in which the molar fraction of B is  $Y_B$  (see also Figure 6.27). The use of the monolayer approximation in describing equilibrium adsorption in binary liquids is satisfactory only when the temperature is not close to the critical temperature of the liquid mixture i.e., the temperature below which the A-B solution consists of a mixture of two solutions (Defay et al. 1966, Eustathopoulos and Joud 1980).

Using the symbols introduced in Section 1.1, an expression for  $\sigma_{LV}$  can be derived from the regular solution model (Guggenheim 1945):

$$\begin{aligned} \sigma_{LV} &= \sigma_{LV}^A + \frac{RT}{\Omega_m} \ln \frac{1 - Y_B}{1 - X_B} + \frac{m_2 \lambda}{\Omega_m} (Y_B^2 - X_B^2) - \frac{m_1 \lambda}{\Omega_m} X_B^2 \\ &= \sigma_{LV}^B + \frac{RT}{\Omega_m} \ln \frac{Y_B}{X_B} + \frac{m_2 \lambda}{\Omega_m} [(1 - Y_B)^2 - (1 - X_B)^2] - \frac{m_1 \lambda}{\Omega_m} (1 - X_B)^2 \end{aligned} \quad (4.5)$$

where  $m_1$  and  $m_2$  are structural parameters defined in Fig. 1.3 and the molar area  $\Omega_m$  is assumed to be the same for A and B. Solving this equation allows calculation of  $Y_B$  and  $\sigma_{LV}$  as a function of  $X_B$ :

$$\frac{Y_B}{1 - Y_B} = \frac{X_B}{1 - X_B} \exp \left[ -\frac{1}{RT} \{ (\sigma_{LV}^B - \sigma_{LV}^A) \Omega_m - m_1 \lambda + 2\lambda((m_1 + m_2)X_B - m_2 Y_B) \} \right] \quad (4.6)$$

For a dilute solution, when  $X_B \rightarrow 0$  then  $Y_B \rightarrow 0$ , and equation (4.6) reduces to:

$$\left( \frac{Y_B}{X_B} \right)_{X_B \rightarrow 0} = \exp \left( -\frac{E_{B(A)}^{\infty, LV}}{RT} \right) \quad (4.7)$$

where the adsorption energy of B at infinite dilution,  $E_{B(A)}^{\infty, LV}$ , is given by:

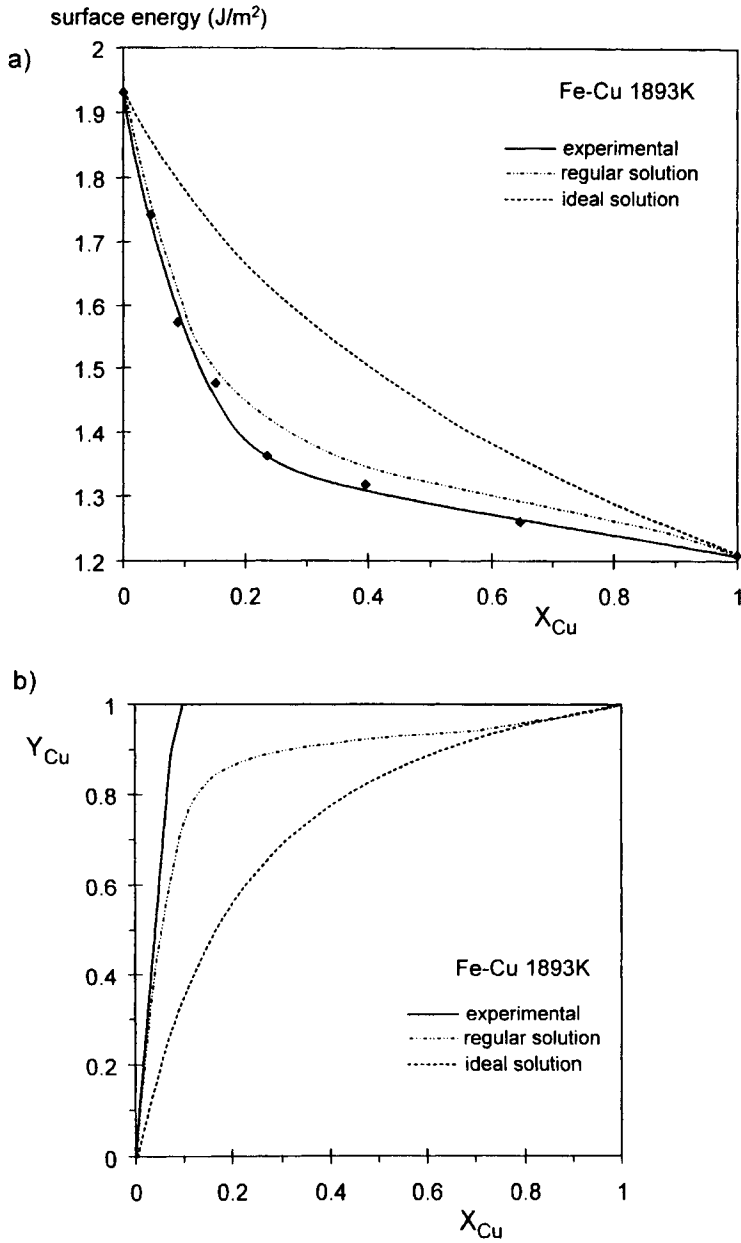
$$E_{B(A)}^{\infty, LV} = (\sigma_{LV}^B - \sigma_{LV}^A) \Omega_m - m_1 \lambda \quad (4.8)$$

A negative value of adsorption energy leads to a high value of the “enrichment factor”  $Y_B/X_B$  and to a sharp decrease of  $\sigma_{LV}$  with the first additions of B in A. Equation (4.8) shows that factors favoring adsorption of B are (i) a low value of  $\sigma_{LV}^B$  compared to  $\sigma_{LV}^A$  and (ii) weak A-B interactions i.e., a tendency of A-B alloy to form a miscibility gap ( $\lambda \gg 0$ ).

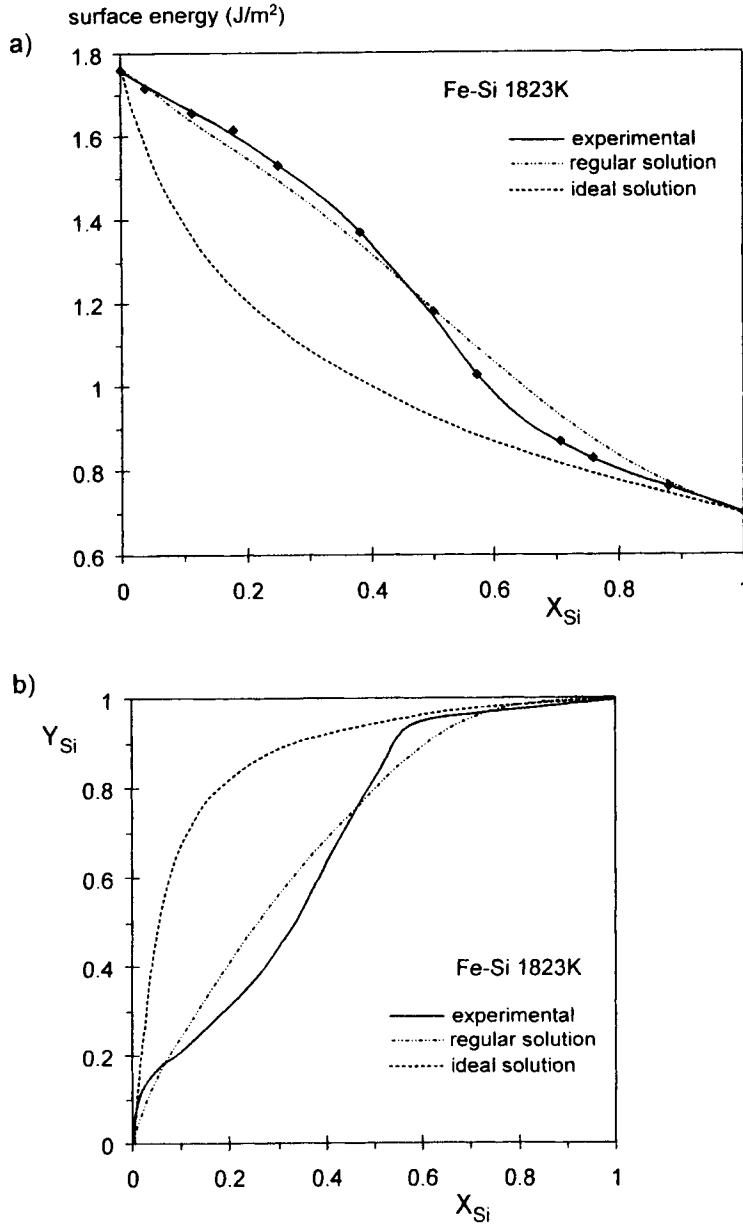
Figure 4.5 shows experimental and calculated curves of  $\sigma_{LV}$  and  $Y_{Cu}$  vs  $X_{Cu}$  for Fe-Cu alloys. The “experimental”  $Y_{Cu}$  vs  $X_{Cu}$  curve was deduced from the experimental  $\sigma_{LV}$ - $X_{Cu}$  curve applying the Gibbs adsorption equation (6.16) (Nogi et al. 1991). The thermodynamic properties of mixing of Fe-Cu alloys can be described satisfactorily by the regular solution model. Moreover, the molar volumes of Fe and Cu, from which the molar area is calculated, are close, as assumed when deriving equation (4.5). The experimental curve of Figure 4.5.a shows a marked decrease of  $\sigma_{LV}$  with the first additions of low-surface-energy Cu, but the additions of Fe in Cu have a comparatively little effect on  $\sigma_{LV}^{Cu}$ . This behaviour, which is a common feature, is discussed in Section 6.5.1 (see also Figure 6.28). The  $\sigma_{LV}$  curve calculated supposing the Fe-Cu alloys to be ideal solutions i.e., taking  $\lambda = 0$ , reproduces this behaviour very imperfectly, but taking into account enthalpy of mixing effects (the parameter  $\lambda$  for this system is positive) leads to a better agreement with experimental results. Both calculated and experimental values of surface composition (Figure 4.5.b) indicate marked enrichment of the surface in Cu, with small Cu additions to Fe.

It should be noted that the regular solution model has been extended to ternary alloys and applied successfully for systems for which interactions cause positive deviations from ideality (Joud et al. 1974).

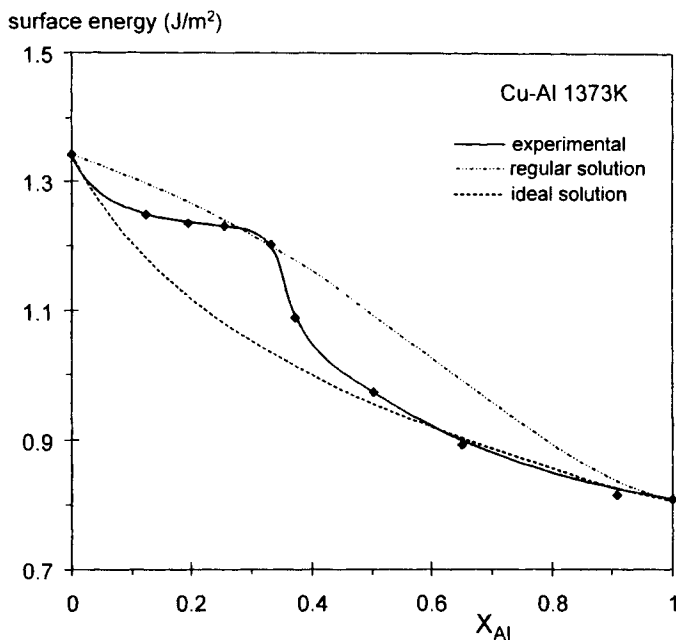
These treatments suppose the surface molar areas of A and B atoms to be equal. However, for alloys with  $\lambda \gg 0$ , the low  $\sigma_{LV}$  component, B, can have a molar volume much greater than that of A (up to 100%). Typical examples are the Cu-Pb, Cu-Bi and Al-Pb systems, for which the experimental decreases in  $\sigma_{LV}$  caused by adding small quantities of B are significantly more than those predicted by the regular solution model. These differences have been attributed to the fact that not all the sites of the “quasicrystalline lattice” on which A and B atoms are distributed are equivalent (Goumiri et al. 1979).



**Figure 4.5.** (a) Experimental (Nogi et al. 1991) and calculated surface energy and (b) surface composition curves for liquid Fe-Cu alloys at 1893K. The calculated curves were obtained taking  $\sigma_{\text{LV}}^{\text{Fe}} = 1.93 \text{ J/m}^2$ ,  $\sigma_{\text{LV}}^{\text{Cu}} = 1.21 \text{ J/m}^2$ ,  $\Omega_{\text{m}} = 3.6 \times 10^4 \text{ m}^2/\text{mole}$  and  $\lambda = 30700 \text{ J/mole}$ .



**Figure 4.6.** (a) Experimental (Popel et al. 1970) and calculated surface energy and (b) surface composition curves for liquid Fe-Si alloys at 1823K. The calculated curves were obtained taking  $\sigma_{LV}^{Fe} = 1.76 \text{ J/m}^2$ ,  $\sigma_{LV}^{Si} = 0.70 \text{ J/m}^2$ ,  $\Omega_m = 4.2 \times 10^4 \text{ m}^2/\text{mole}$  and  $\lambda = -79000 \text{ J/mole}$ .



**Figure 4.7.** Experimental (Eremenko et al. 1961) and calculated surface energy curves for liquid Cu-Al alloys at 1373K. The calculated curves were obtained taking  $\sigma_{LV}^{Cu} = 1.343 \text{ J/m}^2$ ,  $\sigma_{LV}^{Al} = 0.810 \text{ J/m}^2$ ,  $\Omega_m = 4.3 \times 10^4 \text{ m}^2/\text{mole}$  and  $\lambda = -55000 \text{ J/mole}$ .

Figure 4.6.a shows both experimental (Popel et al. 1970) and calculated  $\sigma_{LV}$  curves for Fe-Si alloys. This system exhibits strong heteroatomic interactions, ( $\lambda \ll 0$ ), as shown by the negative deviation of activities from ideality in the liquid alloys and by the formation of high-melting-point intermetallics. The shape of the experimental  $\sigma_{LV}$ - $X_{Si}$  curve is typical of systems with  $\lambda \ll 0$  and is significantly different from that observed for the Fe-Cu system, especially in the sign of its curvature at low B solute concentrations. This is in agreement with the simple regular solution model which predicts that strong bulk interactions (i.e.  $\lambda \ll 0$ ) decrease the tendency for adsorption (Figure 4.6.b). However, in some alloys with  $\lambda \ll 0$ , the experimental  $\sigma_{LV}$  curve exhibits a plateau at low B solute concentrations. This feature is not reproduced satisfactorily by the regular solution model (Figure 4.7) and is due to the fact that for alloys with  $\lambda \ll 0$ , short-range chemical ordering (i.e., clustering) effects cannot be ignored. Such effects are taken into account by more sophisticated statistical models allowing a better representation of experimental data (Laty et al. 1976).

To sum up, the factors favouring adsorption of a solute B in A, leading to a strong decrease of  $\sigma_{LV}^A$ , are  $\sigma_{LV}^B \ll \sigma_{LV}^A$ ,  $\lambda \gg 0$  and  $v_m^B \gg v_m^A$ .

#### 4.1.3 Solid metals

Our experimental knowledge of the surface energies of metallic solids is limited compared to that of liquid metals and consists of values of  $\sigma_{SV}$  for the most common pure metals determined mainly by the “zero-creep” method (Hondros 1970). This technique is based on the observation that thin wires or foils, when heated to a temperature close to the melting point (usually  $T > 0.9T_F$ ), contract to minimise the total surface energy of the system. Thus,  $\sigma_{SV}$  can be derived by measuring the applied load needed to suppress contraction, i.e., to produce a zero-creep. At these high temperatures, when small loads are applied the surface area changes occur by diffusion without any elastic deformation. Therefore, this kind of measurements leads to the determination of the surface energy rather than the surface tension of the solid (see Section 1.1). Compilations of  $\sigma_{SV}$  data are given in (Eustathopoulos and Joud 1980, Kumikov and Khokonov 1983) (Table 4.2).

**Table 4.2.** Solid/vapour surface energies of pure metals measured by the zero-creep technique (Eustathopoulos and Joud 1980).

Metal	$T_{\text{exp}}$ (K)	$T_{\text{exp}}/T_F$	$\sigma_{SV}$ (mJ/m <sup>2</sup> )
Ag	1183	0.86	1140 ± 90
Au	1273	0.95	1400 ± 50
Co	1678	0.95	2282 ± 300
Cu	1243	0.92	1650 ± 100
$\gamma$ -Fe	1648	0.91	2150 ± 325
$\delta$ -Fe	1723	0.95	2220 ± 250
In	420	0.98	674 ± 74
Nb	2523	0.92	2100 ± 100
Ni	1488	0.86	2385 ± 100
Pb	590	0.98	620 ± 20
Sn	488	0.97	685
Ti	1873	0.96	1700
Zn	653	0.94	830

For cubic metals, the value of  $\sigma_{SV}$  generally exceeds that of  $\sigma_{LV}$  at  $T_F$  by 10 to 20% as shown by the data presented in Table 4.3. There is some anisotropy of  $\sigma_{SV}$  values



but for metals with cubic structures (fcc or bcc) it is only a few percent when  $T$  is close to  $T_F$  (Eustathopoulos and Joud 1980). However, anisotropy is much higher (several tens of percent) for hexagonal structure metals like Zn and Cd whose axial ratio deviates strongly from ideality.

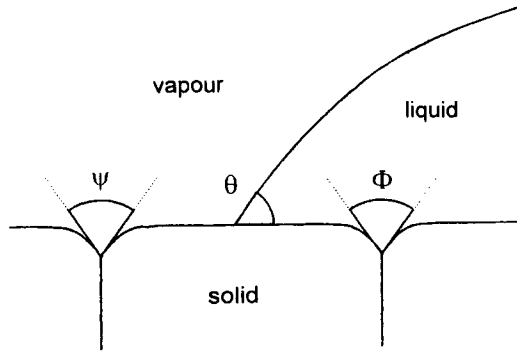
As for liquid metals, oxygen adsorbs strongly on solid surfaces, markedly decreasing  $\sigma_{SV}$  values, but this effect is very anisotropic (Hondros and McLean 1970b). Substantial reductions in  $\sigma_{SV}$  have also been observed with very small additions (less than  $10^{-1}$  at.%) of low-surface-energy metals like Sb or Bi in Cu, and Sn in  $\delta$ -Fe (Hondros 1978). Adsorption at solid surfaces (as well as at grain boundaries) is strongly reinforced by the relaxation of the lattice strain energy caused by solutes with atomic sizes much larger than that of the solvent. This contribution to the adsorption energy is always important and may even be predominant compared to other contributions to the adsorption energy, i.e., the cohesion energy of pure metals ( $(\sigma_{SV}^B - \sigma_{SV}^A)\Omega_m$ ) and chemical A-B interactions ( $m_1\lambda$ ) cited in equation (4.8) (Joud and Passerone 1995).

**Table 4.3.** Surface and interface energies of pure Cu at temperatures close to the melting point.

$\sigma_{LV}$	$1355 \pm 60 \text{ mJ/m}^2$	From Table 4.1
$\sigma_{SV}$	$1650 \pm 100 \text{ mJ/m}^2$	(Eustathopoulos and Joud 1980)
$\sigma_{SL}$	$235 \pm 35 \text{ mJ/m}^2$	(Eustathopoulos 1983)

Absolute values of surface energies of high-melting-point metals A in equilibrium with saturated vapours of a metal B have been determined at  $T \ll T_F^A$  by the “multiphase equilibrium technique” (MPE). This consists of placing a liquid drop of a metal B on a coarse-grained solid substrate of metal A and measuring both the contact angle  $\theta$  and the dihedral angles  $\Phi$  and  $\psi$  formed at the grain-boundary grooves in contact respectively with the liquid and the vapour (Figure 4.8). Then, combining the Young equation (1.16) with the Smith equation (1.30) applied to grain boundary grooves ( $\sigma_{gb} = 2\sigma_{SV} \cos(\psi/2) = 2\sigma_{SL} \cos(\Phi/2)$  where  $\sigma_{gb}$  is the grain boundary energy), the surface energy of the solid in equilibrium with a saturated vapour of metal B can be expressed in terms of measurable quantities:

$$\sigma_{SV} = \frac{\sigma_{LV} \cos(\theta) \cos(\Phi/2)}{\cos(\Phi/2) - \cos(\psi/2)} \quad (4.9)$$



**Figure 4.8.** Definition of the dihedral angles  $\psi$  and  $\Phi$  formed at grain-boundary grooves in the multiphase equilibrium technique.

To determine the surface energy of the solid A in equilibrium with its own vapour,  $\sigma_{SV}^0$ , a further experiment is needed to measure the dihedral angle  $\psi^0$  of grain boundary grooves in vacuum or a neutral gas. Then, assuming that the grain boundary energy of solid A in contact with liquid B is not affected by adsorption of B,  $\sigma_{SV}^0$  is obtained from the equation:

$$\sigma_{SV}^0 = \sigma_{SV} \frac{\cos(\psi/2)}{\cos(\psi^0/2)} \quad (4.10)$$

In practice,  $\theta$  is measured in short-time sessile drop experiments to avoid distortion of the triple line (see Section 1.2.4). The dihedral angles  $\Phi$ ,  $\psi$  and  $\psi^0$  are obtained after prolonged experiments, that allow the grooves to grow deep enough for measurements by metallographic or interferometric techniques (Eustathopoulos 1983). To obtain an acceptable accuracy for dihedral angles, several tens or even hundreds of grooves must be measured. If the value of  $\sigma_{LV}$  is known,  $\sigma_{SV}^0$  (and  $\sigma_{SV}$ ,  $\sigma_{SL}$  and  $\sigma_{gb}$ ) can be calculated as indicated for W in Table 4.4.

In the example of Table 4.4, the surface energy of solid W in equilibrium with a saturated vapour of Cu is lower than  $\sigma_{SV}^0$  due to adsorption of Cu atoms on the W surface. This is generally characteristic of metallic A-B pairs having a low mutual miscibility (Eustathopoulos and Joud 1980). For this reason, results of sessile drop experiments for such systems cannot be interpreted by taking for the surface energy of the solid metal the value of  $\sigma_{SV}$  of pure A in equilibrium with its own vapour (see Sections 1.4.2 and 5.2).

**Table 4.4.** Interfacial energies at 1500°C in Ar/liquid Cu/solid W system, calculated using data on dihedral angles and contact angle of Hodkin et al. (1970) and taking  $\sigma_{LV}^{Cu} = 1276 \text{ mJ/m}^2$  (see Table 4.1). Note that the contact angle is close to but higher than zero.

Angles (deg)	Interfacial energies (mJ/m <sup>2</sup> )
$\theta \cong 0$	$\sigma_{SV}^0 = 3200$
$\Phi = 113.1$	$\sigma_{SV} = 2400$
$\psi = 150.1$	$\sigma_{SL} = 1120$
$\psi^0 = 157.7$	$\sigma_{gb} = 1240$

#### 4.1.4 Solid/liquid interfaces

At S/V and L/V surfaces, the atomic density decreases sharply within a few layers from its value in the bulk phase to zero. This leads to a high excess energy of solid atoms at the surface and hence to a high surface energy. At S/L interfaces of pure metals, the change of atomic density is comparatively small, a few percent, so the value of  $\sigma_{SL}$  for a given metal is generally much lower than those of  $\sigma_{SV}$  and  $\sigma_{LV}$  (Table 4.3).

For pure bcc or fcc metals, experimental values of  $\sigma_{SV}$  and  $\sigma_{SL}$  reveal a relation  $\sigma_{SL}/\sigma_{SV} \cong 0.15 \pm 0.05$  (Eustathopoulos 1983). The constancy of this ratio is compatible with the simple nearest-neighbour interaction model of Skapski (1956) (see Section 5.1). Usually,  $\sigma_{SL}$  for pure metals and A-B alloys is of the order of  $10^2 \text{ mJ/m}^2$ . However, for some highly immiscible solid A/liquid B systems, values of  $\sigma_{SL}$  up to about  $10^3 \text{ mJ/m}^2$  can be observed (Table 4.4) (Eustathopoulos 1983), due at least partially to the contribution of heteroatomic interactions. This effect is discussed in more detail in Section 5.2.

## 4.2. DATA FOR NON-METALLIC COMPOUNDS

### 4.2.1 Liquid oxides and halides

The surface energy of molten oxides has been studied less extensively than that of pure liquid metals. For instance, the surface energy of molten  $\text{Al}_2\text{O}_3$ , which is the most widely studied oxide, has been measured by 12 teams (Ikemiya et al. 1993) while that of Fe has been measured by 28 (Keene 1993). One reason for this difference is the experimental difficulties arising from the high melting point of many oxides but

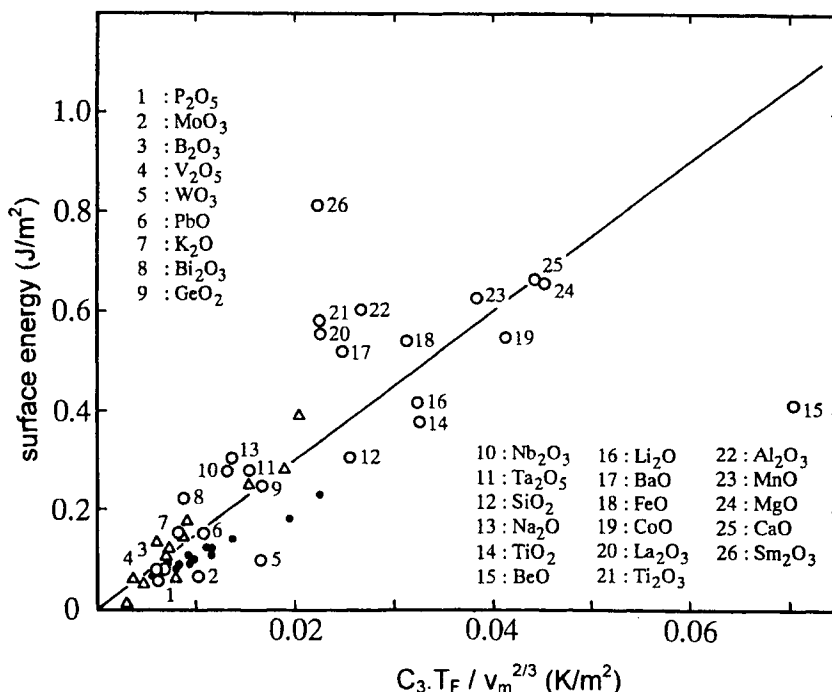
nevertheless experimental data for surface energies exist for about 30 oxides (Table 4.5) (Ikemiya et al. 1993).

**Table 4.5.** Surface energy of molten pure oxides at their melting point. From the compilation of (Ikemiya et al. 1993) except for  $\text{Al}_2\text{O}_3$  (see the text) and  $\text{Cr}_2\text{O}_3$  (Rasmussen 1972).

Oxide	$T_F$ (K)	$\sigma_{LV}$ (mJ/m <sup>2</sup> )	Oxide	$T_F$ (K)	$\sigma_{LV}$ (mJ/m <sup>2</sup> )
$\text{Al}_2\text{O}_3$	2320	630	$\text{MnO}$	2058	630
$\text{B}_2\text{O}_3$	723	80 (1173K)	$\text{MoO}_3$	1068	70
$\text{BaO}$	2196	520	$\text{Na}_2\text{O}$	1193	308 (1673K)
$\text{BeO}$	2843	415	$\text{Nb}_2\text{O}_5$	1773	279
$\text{Bi}_2\text{O}_3$	1098	213	$\text{P}_2\text{O}_5$	836	60
$\text{CaO}$	2860	670	$\text{PbO}$	834	132 (1173K)
$\text{CoO}$	2078	550	$\text{SiO}_2$	1993	307
$\text{Cr}_2\text{O}_3$	2573	812	$\text{Sm}_2\text{O}_3$	2593	815
$\text{FeO}$	1641	545	$\text{Ta}_2\text{O}_5$	2150	280
$\text{GeO}_2$	1389	250	$\text{TiO}_2$	2143	380
$\text{K}_2\text{O}$	980	156 (1673K)	$\text{Ti}_2\text{O}_3$	2090	584
$\text{La}_2\text{O}_3$	2573	560	$\text{V}_2\text{O}_5$	943	80
$\text{MgO}$	3073	660	$\text{WO}_3$	1743	100

There is insufficient information to allow classification of liquid oxide data into two types according to their accuracy, as was done for liquid metals. In the case of  $\text{Al}_2\text{O}_3$ , the determinations of  $\sigma_{LV}$  values by mainly the drop weight, sessile drop and maximum bubble pressure techniques converge to a value of  $630 \pm 70 \text{ mJ/m}^2$  near the melting temperature (Ikemiya et al. 1993). Moreover, the possible effect of  $\text{P}_{\text{O}_2}$  on the  $\sigma_{LV}$  value of  $\text{Al}_2\text{O}_3$  appears to be weak since similar values have been obtained when working in vacuum, in neutral or reducing atmosphere or air. Like liquid metals, the dispersion of values of temperature coefficient,  $d\sigma_{LV}/dT$ , is high and values lying between  $-0.15$  and  $-0.5 \text{ mJ.m}^{-2}.\text{K}^{-1}$  have been reported for  $\text{Al}_2\text{O}_3$  (Ikemiya et al. 1993).

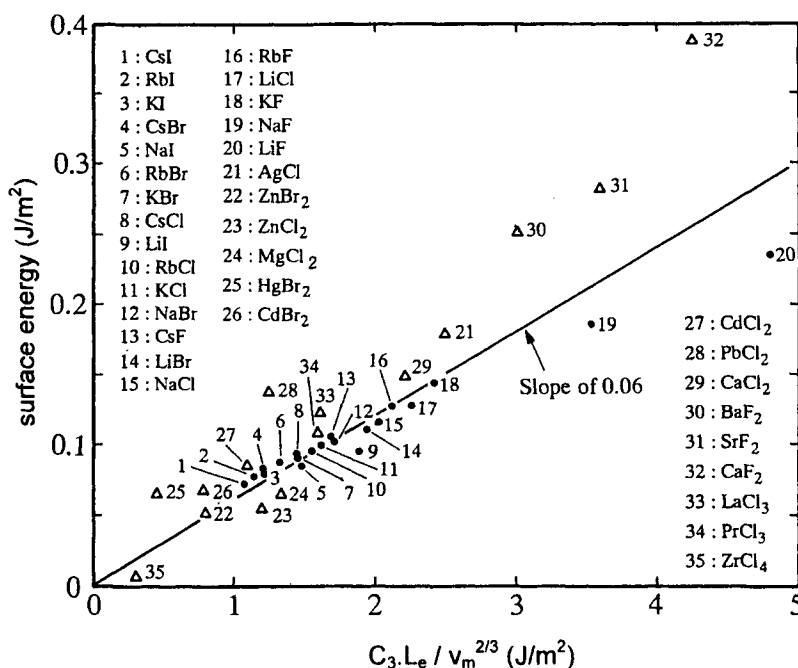
Because of the success of correlations between the molar surface energy of pure metals ( $\cong \sigma_{LV} \cdot v_m^{2/3}$ ) and various quantities reflecting the cohesion energy of the metal (heat of evaporation  $L_e$ , melting point  $T_F$ , etc), similar correlations have been assessed for molten oxides. An example is shown in Figure 4.9 in which the experimental values of  $\sigma_{LV}$  are plotted versus  $C_3 \cdot T_F \cdot v_m^{-2/3}$  where  $C_3$  is a constant equal to  $1.18 \times 10^{-8}$  (Tanaka et al. 1996) (in this correlation, the melting temperature was preferred to the heat of evaporation because this last quantity is not available for many oxides). Except for  $\text{BeO}$  and  $\text{Sm}_2\text{O}_3$ , the quality of the



**Figure 4.9.** Correlation between surface energy of molten oxides and  $C_3 \cdot T_F \cdot v_m^{-2/3}$  (with  $C_3 = 1.18 \times 10^{-8}$ ). Non-numbered symbols (full circles and hollow triangles) relate to the ionic melts of Figure 4.10. Reprinted from (Tanaka et al. 1996) with kind permission of the authors.

correlation is similar to that observed for liquid metals (Figure 4.1), indicating that the molar surface energy of oxides is also nearly proportional to their cohesion energy. However, the proportionality coefficient is found to be significantly lower than for pure metals. This suggests that the atomic and electronic rearrangements accompanying the creation of a surface is particularly important in oxides and hence results in a marked surface energy decrease (Kruse et al. 1996).

In Figure 4.10, values of  $\sigma_{LV}$  for molten halides at  $T_F$  are plotted versus the quantity  $C_3 \cdot L_e \cdot v_m^{-2/3}$  (Tanaka et al. 1996) (it should be noted that the constant  $C_3 = 1.18 \times 10^{-8}$  is similar but not equal to the constant  $C_1$  of equation (4.1)). Fused halides have comparatively low surface energies (lying between 0.05 and 0.4 J/m<sup>2</sup>) for two main reasons: (i) their heat of evaporation is low compared to that of metals (typical values being 30 as compared to 300 kJ/mole) and (ii) the coefficient of proportionality between  $\sigma_{LV}$  and  $L_e \cdot v_m^{-2/3}$  for halides is (as for oxides) only half of that for metals.

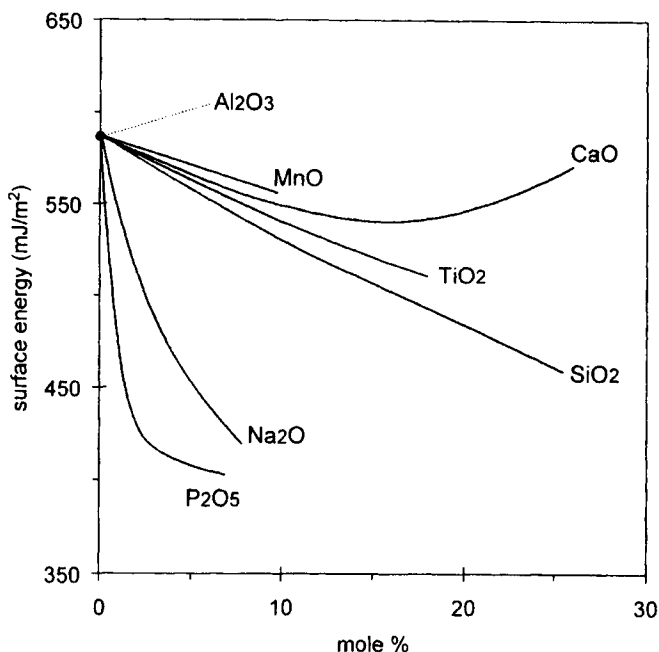


**Figure 4.10.** Correlation between surface energy of molten halides and  $C_3 \cdot L_e \cdot v_m^{-2/3}$  (with  $C_3 = 1.18 \times 10^{-8}$ ). Reprinted from (Tanaka et al. 1996) with kind permission of the authors.

As the surface energy varies by a factor 10 from one oxide or halide to another, tensio-active effects, such as those observed in liquid alloys, are to be expected also for mixtures of fused oxides or fused halides. One example is shown in Figure 4.11 which shows the effect of additions of various oxides on the surface energy of molten FeO. A sharp decrease of  $\sigma_{LV}$  is observed in the case of additions of low-surface-energy  $P_2O_5$  or  $Na_2O$  while additions of high surface energy  $Al_2O_3$ ,  $MnO$  or  $CaO$  have only weak effects on  $\sigma_{LV}$ . Because of the complexity of the structure of molten oxides, there is no statistical thermodynamic model that allows calculation of  $\sigma_{LV}$  values for binary oxide mixtures. However, useful semi-empirical techniques for estimating these quantities were proposed in (Tanaka et al. 1996).

#### 4.2.2 Solid oxides

In the literature, there is a very limited number of measurements of the surface energy of non-metallic solids. Most of them are for  $Al_2O_3$  and were derived using



**Figure 4.11.** Surface energies of binary mixtures based on FeO at 1400–1420°C. Data from work reported in (Kozakevitch 1949) [15].

the MPE technique (see Figure 4.8) with a non-reactive molten metal as the auxiliary liquid. Deriving meaningful data from these measurements requires care. As when applied to metals, the method needs the measurement of a great number of parameters and a small error on dihedral angles often produces a large uncertainty in the value of  $\sigma_{SV}$ . Additionally, by definition polycrystalline ceramics must be used but for these materials the impurity content is usually high. Because the growth of measurable dihedral angle grooves needs high temperatures and long equilibration times, impurities may easily migrate to surfaces and interfaces and affect results.

An example of the application of the MPE technique is given in Table 4.6 for  $\text{Al}_2\text{O}_3$ , which was studied using Sn and Co as the auxiliary liquids. The dihedral angles  $\psi$ ,  $\psi^0$  and  $\Phi$  in these systems were measured by Nikolopoulos (1985). For both systems, at each temperature, it was found that the difference between  $\psi$  and  $\psi^0$  is of the order of the experimental error, meaning that  $\sigma_{SV} \cong \sigma_{SV}^0$  (equation (4.10)). In other words, adsorption of metallic vapours on  $\text{Al}_2\text{O}_3$  surfaces was negligible. This result is to be expected for a non-reactive metal/oxide system in

which metal/oxide interactions are weak, as will be discussed in Section 6.2.2. Combining values of dihedral angles with  $\theta$  values derived from short time sessile drop experiments on monocrystalline  $\text{Al}_2\text{O}_3$  (as discussed in Section 3.3, the use of monocrystalline substrates leads to more reliable values of contact angles than polycrystalline ones),  $\sigma_{\text{SV}}$  can be calculated by substitution in equation (4.9) as was done for the data presented in Table 4.6. The uncertainty of the values for  $\sigma_{\text{SV}}$  is as high as 30–40% and is typical of this kind of measurements. Note that if the ratio of  $\sigma_{\text{SV}}/\sigma_{\text{LV}}$  for an oxide is as close to unity as for pure metals, the value of  $\sigma_{\text{SV}}$  of  $750 \text{ mJ/m}^2$  obtained at the highest temperature is compatible with the value of  $\sigma_{\text{LV}}$  of  $630 \pm 70 \text{ mJ/m}^2$  for molten  $\text{Al}_2\text{O}_3$ . Therefore, when a rough estimate of the surface energy of a solid oxide is needed at a temperature not too far from its melting point, the value of  $\sigma_{\text{LV}}$  of this oxide can be used. Finally it should be noted that values of  $\sigma_{\text{SL}}$  calculated from data of Table 4.6 lie in the range 1200–1500  $\text{mJ/m}^2$ .

**Table 4.6.** Experimental determination of  $\sigma_{\text{SV}}$  of  $\text{Al}_2\text{O}_3$  by the MPE technique.

T (K)	auxiliary liquid	$\sigma_{\text{LV}}^{(a)}$ ( $\text{mJ/m}^2$ )	$\tilde{\psi}^{(b)}$ (deg)	$\tilde{\Phi}^{(b)}$ (deg)	$\theta$ (deg)	$\sigma_{\text{SV}}$ ( $\text{mJ/m}^2$ )
1473	Sn	463	139	146.9	121 <sup>(c)</sup>	$1040 \pm 375$
1623	Sn	447	137	145.5	120 <sup>(c)</sup>	$947 \pm 330$
1783	Co	1878	139	159.6	113 <sup>(d)</sup>	$750 \pm 220$
1923	Co	1826	138	157.9	111 <sup>(d)</sup>	$752 \pm 210$

<sup>(a)</sup> from Table 4.1, <sup>(b)</sup> from (Nikolopoulos 1985), <sup>(c)</sup> from (Rivollet et al. 1987), <sup>(d)</sup> from (Chatain et al. 1986)

A similar study was done for  $\text{UO}_2$  using Cu (Hodkin and Nicholas 1973) and Ni (Nikolopoulos et al. 1977) as auxiliary liquids. As in  $\text{Sn/Al}_2\text{O}_3$  and  $\text{Co/Al}_2\text{O}_3$  couples, the effect of adsorption of metal atoms on  $\text{UO}_2$  surface at  $1500^\circ\text{C}$  was found to be negligible, i.e.  $\sigma_{\text{SV}} \cong \sigma_{\text{SV}}^0$ . The surface energy of  $\text{UO}_2$  was calculated using values of  $\sigma_{\text{LV}}$  of pure metals given in Table 4.1 and contact angle and dihedral angle data. The value of  $\sigma_{\text{SV}}^0$  when using liquid Cu was  $340 \text{ mJ/m}^2$  and  $850 \text{ mJ/m}^2$  when using liquid Ni. This difference in values for  $\text{UO}_2$  is much higher than the experimental error and underlines the difficulties in measuring surface energies of polycrystalline ceramics by the MPE technique. Complications may have been caused also by minor differences in the stoichiometry of the  $\text{UO}_2$  used by the two



teams, as shown by results obtained by Hodkin and Nicholas (1977) by varying the O/U ratio in  $\text{UO}_2$ .

#### 4.2.3 Carbon and solid carbides

Due to obvious technical difficulties, neither the zero-creep nor the multiphase equilibrium techniques have been used to measure the surface energy of *graphite*. However, a  $150 \text{ mJ/m}^2$  value (Donnet et al. 1982) for the basal plane of graphite was measured at room temperature by wetting experiments using the so-called “two liquids” method and alkane/water/graphite systems (Donnet et al. 1977). This technique does not allow measurement of the total surface energy but only the van der Waals component of  $\sigma_{\text{SV}}$ ,  $\sigma_{\text{SV}}^{\text{d}}$ . However, because the graphite basal planes are bonded by van der Waals dispersion force interactions,  $\sigma_{\text{SV}}(\text{basal}) \cong \sigma_{\text{SV}}^{\text{d}}(\text{basal}) = 150 \text{ mJ/m}^2$ .

In wetting experiments of a pure metal or alloy on graphite, adsorption of the liquid components on to the solid surface from the vapour phase can occur, to decrease  $\sigma_{\text{SV}}$ . However, for inert non-wetting metal/graphite systems, this effect is unlikely, as shown by results of Gangopadhyay and Wynblatt (1994). Indeed, at temperatures close to (but slightly lower than) the melting point of Pb, adsorption of Pb and Ni from Pb-Ni alloys on graphite surface, monitored by in-situ Auger analyses, was negligible. Negligible adsorption is expected *a fortiori* at higher temperatures.

The formation of a surface orientated perpendicularly to the basal plane needs the rupture of chemical carbon-carbon bonds. The surface energy for this prismatic orientation has not been determined experimentally, but is expected to be an order of magnitude higher than that of the basal plane ( $150 \text{ mJ/m}^2$ ).

In the case of *vitreous carbon*, the component  $\sigma_{\text{SV}}^{\text{d}}$  of  $\sigma_{\text{SV}}$  was measured by the technique used for graphite (Donnet et al. 1982) and found to be  $32 \text{ mJ/m}^2$ . This is five times lower than that of the graphite basal plane and may be explained by the low density of vitreous carbon ( $1.5 \times 10^3 \text{ kg/m}^3$ ) compared to that of graphite ( $2.26 \times 10^3 \text{ kg/m}^3$ ) (see also Section 8.1). Because the atomic structure of polished surfaces of vitreous carbon is not known, it is not possible to evaluate the percentage of  $\sigma_{\text{SV}}$  that is due to  $\sigma_{\text{SV}}^{\text{d}}$ .

The formation of the low-energy (111) surface planes of *diamond* requires breaking of chemical carbon-carbon bonds. Although surface reconstruction occurring at high temperatures can decrease the surface energy, this is still expected to be much higher than that of the basal plane of graphite. A rough estimation of the surface energy made by a simple nearest-neighbour model leads to a value close to  $4000 \text{ mJ/m}^2$  (Appendix F).

*Carbides* can be covalent or metal-like, the most important of the covalent carbides being SiC which like carbon crystallizes in both hexagonal and cubic structures. However, contrary to carbon, the basal planes in the hexagonal structure and the (111) faces of the cubic variant are linked by chemical bonds, so the corresponding surface energies should be about  $10^3$  rather than  $10^2$  mJ/m<sup>2</sup>. Estimated values for the surface energy of both faces are close to 1500 mJ/m<sup>2</sup> (Appendix F).

The only measurement of surface energy of a metal-like carbide was performed by the multiphase equilibrium technique for the molten U/UC system (Hodkin et al. 1971). In this system, because of the metallic character of UC, good wetting is observed, i.e.,  $\theta < 90^\circ$  (see also Section 7.2). The surface energy of UC at 1325°C was found to be 730 mJ/m<sup>2</sup> while the interfacial energy between U (saturated in C) and UC was about 140 mJ/m<sup>2</sup>. Thus the  $\sigma_{SL}/\sigma_{SV}$  ratio is closer to those for metal/metal rather than metal/oxide systems. It must be emphasized that at high temperature UC exhibits a range of non-stoichiometry which can affect its surface and interfacial energies. Therefore, the value  $\sigma_{SV} = 730$  mJ/m<sup>2</sup> corresponds to the particular stoichiometry of UC in equilibrium with molten U at 1325°C.

For other metal-like carbides (TiC, ZrC, VC, TaC), an estimation of the *minimum* value of  $\sigma_{SV}$  can be made using contact angle data of ferrous metals (see Table 7.12) and assuming that  $\sigma_{SL} = 0$ . This leads to values close to 1500 mJ/m<sup>2</sup>. However, the calculations of Warren (1980) suggest that  $\sigma_{SL}$  in ferrous metal/metallic carbide systems is close to 500 mJ/m<sup>2</sup>, so a more plausible value for  $\sigma_{SV}$  is 2000 mJ/m<sup>2</sup>.

Returning to the U/UC system in which contact angles close to 40°–60° were observed in the range 1300–1600°C, an interesting observation was that the dihedral angle  $\psi$  was nearly equal to  $\psi^0$  as for non-wetting metal/oxide systems. Thus adsorption of metal atoms on the ceramic surface was negligible. This behaviour differs from that observed for several low melting point metals B on high melting point metals A systems (see for instance Table 4.4), where adsorption of B atoms on solid A surfaces reduces  $\sigma_{SV}^A$  (see Figure 5.2). The condition for adsorption is  $\sigma_{LV}^B \ll \sigma_{SV}^A$  (Section 5.2) but this condition is not met by the pseudo-metallic U/UC system because  $\sigma_{LV}$  of liquid U is about 1500 mJ/m<sup>2</sup>, higher than the surface energy of UC by a factor two.

#### 4.3. CONCLUDING REMARKS

Measurements of the surface energy of pure liquid metals performed in the last decades by different investigators and different techniques have led to values of

$\sigma_{LV}$  differing by less than 5% for the most common metals. However, the dispersion is much more marked for the temperature coefficient of  $\sigma_{LV}$  (30–100%). The influence of dissolved oxygen on the surface energy of liquid metals can be large and has been studied formally for about ten elements. Surface energy variations with alloy composition have been determined for several binary systems and compilations of data are given in (Khilya 1980, Keene 1987). The experimental curves can be predicted satisfactorily using the monolayer-regular solution model or other more sophisticated approaches. For alloys containing more than two components, experimental measurements of  $\sigma_{LV}$  are essential, except for some simple ternary systems for which modelling is possible.

Although fused oxides and halides have been less extensively studied than liquid metals, surface energies have been determined for a number of such compounds. In the absence of models for estimating the surface energy of oxide or halide mixtures, this quantity must be determined experimentally.

Experimental data for the surface energy of solid compounds exist only for some pure metals and for a few non-metallic solids ( $Al_2O_3$ ,  $UO_2$ , UC, graphite). Even for these materials, the scatter of surface energy values is as high as 50%, owing to impurity effects and difficulties inherent in the experimental methods that have to be used. Thus it is not possible to analyse wetting data for high-temperature solids by an approach needing the accurate knowledge of surface energy of these solids.

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## Chapter 5

# Wetting properties of metal/metal systems

In the absence of barriers to wetting such as oxide films on the liquid or the solid, molten metals wet metallic substrates ( $\theta < 90^\circ$ ) whatever the intensity of interaction between the liquid and the solid. Wetting in this kind of systems can be discussed using the Young-Dupré equation and a simple nearest-neighbour interaction model described in Section 1.1. This model contains several approximations which make it only a rough description of the actual system. For instance, the solid and liquid metals are assumed to have the same structure and coordination,  $Z$ . However, for solid fcc metals  $Z = 12$ , while the average value of  $Z$  for liquid metals is in the range 9–11. Moreover, in this description, the interfacial energies are assumed to result only from bond energies and possible entropy contributions to these quantities are neglected. This approximation is particularly questionable for metal/metal interfaces because the excess entropy due to the interface can be substantial. This entropy results both from the variation of atomic order between the bulk liquid and liquid atoms at the interface (Ewing 1971, Spaepen and Meyer 1976) and from the atomic roughness of the solid in contact with the liquid (Eustathopoulos 1983). For metal/ceramic systems for which  $\sigma_{SL}$  is of the order of  $1\text{--}2\text{ J/m}^2$ , entropic effects are comparatively weak and may be neglected. However, in metal/metal systems for which  $\sigma_{SL}$  is usually in the range  $0.05$  to  $0.5\text{ J/m}^2$ , the contribution of interfacial entropy to  $\sigma_{SL}$  may become important. Despite drawbacks, the model is useful for qualitative and sometimes semi-quantitative discussion of the effects of variables such as the orientation of the solid surface and the intensity of solid-liquid interactions.

### 5.1. A PURE LIQUID METAL ON ITS OWN SOLID

As shown in Section 1.4.1, the Young-Dupré equation can be written:

$$\cos \theta = 2 \frac{\varepsilon_{SL}}{\varepsilon_{LL}} - 1 \quad (5.1)$$

Assuming that, for a pure metal on its own solid, the solid-liquid and liquid-liquid bond energies,  $\varepsilon_{SL}$  and  $\varepsilon_{LL}$ , are equal, which is the approximation used in the classical work of Skapski (1956), and knowing that the molar heat of melting of the pure metal  $L_m$  is related to pair energies by

$$L_m = ZN_a \frac{\varepsilon_{LL} - \varepsilon_{SS}}{2} \quad (5.2)$$

where  $Z$  is the coordination number and  $N_a$  is Avogadro's number, the expressions (1.11) for interfacial energy (written for a pure metal with  $A = S$  and  $B = L$ ) and (5.1) for contact angle become:

$$\sigma_{SL} = \frac{m_l L_m}{\Omega_m} \quad (5.3)$$

$$\cos \theta = 1 \quad (5.4)$$

where  $\Omega_m$  is the molar area and  $m_l$  denotes the fraction of bonds which are of S/L type for a solid atom at the interface (see Figure 1.3). Equation (5.4) is in good agreement with experimental results showing contact angles close to  $0^\circ$  for fcc metals with low-anisotropy surface energy. Thus, the contact angle for Au/Au is  $7^\circ$  (Naidich et al. 1975) and for Cu/Cu close to  $0^\circ$  (Wenzl et al. 1976). For the semi-metal Ga/Ga, the contact angle is  $6^\circ$  (Dokhov et al. 1971) and for the semi-conductors Si/Si the angle is  $12^\circ \pm 2^\circ$  (Naidich et al. 1975, Surek 1976) and for Ge/Ge is  $9^\circ$  to  $30^\circ$  depending on the orientation of the solid surface (Naidich et al. 1981). In view of the crude model, this quality of agreement between experiments and model predictions is almost certainly due to compensating errors made in the model.

The variation of contact angle with *orientation* of surface planes can be understood by considering the Young-Dupré equation and the definition of  $W_a$  based on the simple model of Section 1.1:

$$W_a = -\frac{Zm_l}{\omega} \varepsilon_{SL} \quad (5.5)$$

where  $\omega$  is the surface area per atom. When the atomic density of a surface plane increases, both  $m_l$  and  $\omega$  decrease but as the decrease of  $m_l$  is more pronounced, the work of adhesion of the liquid on this plane decreases. Therefore, in systems developing strong interactions at the interface, the wetting of the less close-packed (high-index) planes should be better than that of the closest-packed (low-index) planes. This prediction is confirmed by the results of Naidich et al. (1981) showing that contact angles of liquid Ge on (111), (110) and (100) faces were found to be  $30^\circ$ ,  $17^\circ$  and  $9^\circ$  respectively, i.e., they decreased in the same order as the atomic

density of these planes. Note that the opposite effect of atomic density is expected in liquid/solid systems with high cohesion energies but developing weak, van der Waals, interactions at the interface (see Section 8.1).

## 5.2. SYSTEMS WITH NEGLIGIBLE MUTUAL SOLUBILITY

Often the liquid and solid are not the same metal and sometimes they are mutually insoluble. When the equilibrium value of the molar fraction of solid component A in a liquid B  $X_A^L \ll 1$ , by equalling the chemical potentials of A in the solid and liquid phases,  $X_A^L$  is related to the regular solution parameter  $\lambda$  given by equation (4.3) by:

$$X_A^L \cong K_4 \exp \left[ \frac{-\lambda}{RT} \right] \quad \text{with} \quad K_4 = \exp \left[ -L_m^A \left( 1 - \frac{T}{T_F^A} \right) / (RT) \right] \quad (5.6)$$

where  $L_m^A$  and  $T_F^A$  are the heat of melting and the melting temperature of pure A, respectively. Thus, a very low solubility of A in liquid B is expected for temperatures  $T \ll T_F^A$  and high positive values of  $\lambda$ .

Typical examples are the Pb/Fe and Cu/W couples for which the solubility of Fe in molten Pb and W in molten Cu at temperatures close to the melting point of the liquid is as low as a few ppm. In this type of system for which spreading times are of the order of  $10^{-2}$  second for millimetre-size droplets (see Section 2.1.1), the final contact angles can be as low as  $10^\circ$  (Table 5.1). This indicates that strong A-B interactions can be established *at the interface*, even for nearly insoluble metallic couples, i.e., for systems having weak A-B interactions in the *bulk liquid* ( $\lambda \gg 0$ ).

To understand this apparent paradox, consider a Cu/W couple. For this system,  $\lambda = 90$  kJ/mole (Appendix G) and the heats of evaporation are 316 kJ/mole for Cu ( $= -ZN_a\epsilon_{CuCu}/2$ ) and 821 kJ/mole for W ( $= -ZN_a\epsilon_{WW}/2$ ) (Hultgren et al. 1973). Thus the value of  $ZN_a\epsilon_{CuW}$  can be calculated from equation (4.3) and the various interaction values are presented in the bond energy diagram of Figure 5.1 in terms of molar units ( $\epsilon^* = ZN_a\epsilon$ ). This diagram shows that even in the very insoluble Cu/W couple, the exchange energy  $\lambda$  is only a small quantity compared to the average cohesion energy of the two metals ( $\lambda$  is less than 10% of  $(\epsilon_{CuCu}^* + \epsilon_{WW}^*)/2$ ). As a consequence,  $\epsilon_{CuW}^*$  has a very negative value ( $|\epsilon_{CuW}^*|$  is



**Table 5.1.** Contact angles for nearly insoluble metal/metal systems.  $x_A^L$  is the molar fraction of A in liquid B at equilibrium. For all systems, the corresponding molar fraction of B in solid A is negligible ( $x_B^S \approx 0$ ).

Liquid B /solid A	T (°C)	$x_A^L$ <sup>(a)</sup>	Atmosphere	$\theta$ (deg)	Reference for $\theta$ values
Pb/Fe	350	$\sim 10^{-5}$	H <sub>2</sub>	57	(Popel et al. 1971)
	750	$3 \times 10^{-5}$	H <sub>2</sub>	53	
	750	$3 \times 10^{-5}$	Ar-5% H <sub>2</sub>	53	(Gomez-Moreno et al. 1982)
	1000	$4 \times 10^{-4}$	Ar-5% H <sub>2</sub>	32	
	1000	$4 \times 10^{-4}$	H <sub>2</sub>	27	(Eremenko and Lesnik 1963)
Ag/Fe	980	$6 \times 10^{-4}$	Ar+ H <sub>2</sub>	40	(Pique et al. 1981)
	1000	$6 \times 10^{-4}$	He ( $P_{O_2} = 5 \times 10^{-19}$ atm)	57-45-36 <sup>(b)</sup>	(Tomsia et al. 1982)
Ag/W	960	$6 \times 10^{-9}$	high vacuum	78	(Sugita et al. 1970)
	1000	$6 \times 10^{-9}$	high vacuum	50	(Naidich 1981b)
Ga/W	975	$2 \times 10^{-3}$	N <sub>2</sub> -10% H <sub>2</sub>	11	(Weirauch 1998)
Au/W	1063	$1.37 \times 10^{-3}$	high vacuum	66	(Sugita et al. 1970)
Cu/W	1100	$2 \times 10^{-5}$		10-55	see Table 5.2
Cu/Mo	1100	$6.7 \times 10^{-4}$	high vacuum	30	(Yupko et al. 1991)
	1100	$6.7 \times 10^{-4}$	He-18% H <sub>2</sub>	10	(Yupko et al. 1986)

<sup>(a)</sup> estimated values using data of enthalpy of mixing of Appendix G except values for Pb/Fe (Stevenson and Wulff 1961) and Ag/Fe, Au/W, Cu/Mo (Massalski 1990) which are experimental ones.

<sup>(b)</sup> these values correspond to three kinds of Fe substrate containing 1200, 60 and 5 ppm of oxygen respectively.

even higher than  $|\epsilon_{\text{CuCu}}^*|$ ), which indicates that strong interactions can be established at the Cu/W interface.

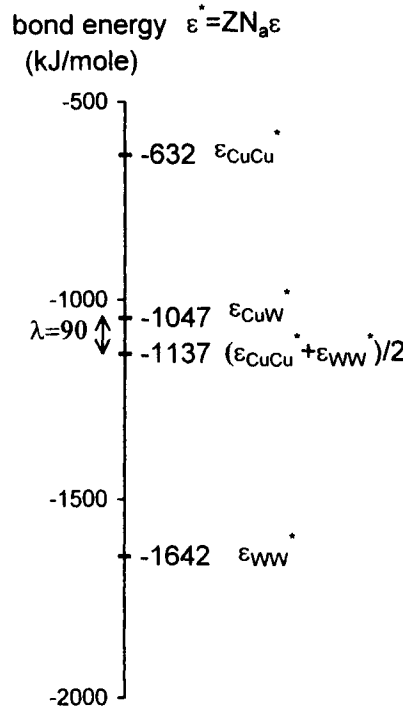
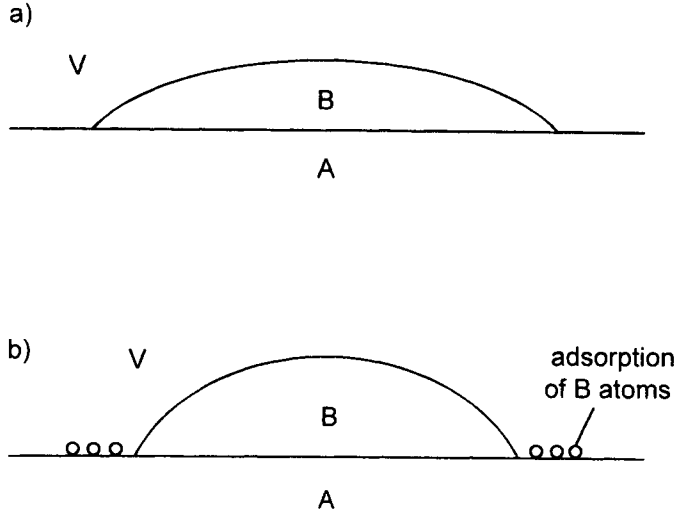


Figure 5.1. Bond energy diagram for the Cu-W system.

Writing equation (1.11) for a liquid B in contact with a solid A (Figure 5.2.a), and assuming that the bond energy between solid A and liquid B,  $\epsilon_{\text{AB}}^{\text{SL}}$ , is equal to the bond energy between liquid A and liquid B,  $\epsilon_{\text{AB}}^{\text{LL}}$ , as for an interface between a liquid and its own solid, we derive:

$$\sigma_{\text{SL}} = \frac{ZN_a m_l}{\Omega_m} \left( \epsilon_{\text{AB}}^{\text{LL}} - \frac{\epsilon_{\text{AA}}^{\text{SS}} + \epsilon_{\text{BB}}^{\text{LL}}}{2} \right) \quad (5.7)$$

Introducing equations (4.3), (5.2) and (5.3) into (5.7), one gets:



**Figure 5.2.** a) Wetting of liquid B on a “dry” A surface. b) The partial saturation of A broken bonds by adsorption of B decreases  $\sigma_{SV}^A$  and increases  $\theta$ .

$$\sigma_{SL} = \sigma_{SL}^A + \frac{m_l \lambda}{\Omega_m} \quad (5.8)$$

The first term of the right hand side of equation (5.8) is the interfacial energy of pure solid A in contact with pure liquid A, while the second term takes into account the fact that the liquid is not pure A but pure B.

Introducing equation (5.8) in the Young equation  $\cos \theta = (\sigma_{SV}^A - \sigma_{SL})/\sigma_{LV}^B$  and replacing  $\sigma_{LV}^B$  by  $m_l L_e^B/\Omega_m$  where  $L_e^B$  is the molar heat of evaporation of B (see the similar equation (1.15)), one obtains:

$$\cos \theta = \frac{\sigma_{SV}^A - \sigma_{SL}^A}{\sigma_{LV}^B} - \frac{\lambda}{L_e^B} \quad (5.9)$$

Assuming perfect wetting of pure molten A on pure solid A at  $T = T_F^A$  is also valid for supercooled liquid A, i.e., at  $T < T_F^A$ , then

$$\sigma_{SV}^A - \sigma_{SL}^A = \sigma_{LV}^A \quad (5.10)$$

and equation (5.9) becomes:

$$\cos \theta = \frac{\sigma_{LV}^A}{\sigma_{LV}^B} - \frac{\lambda}{L_e^B} \quad (5.11)$$

As a general rule,  $\sigma_{LV}^A/\sigma_{LV}^B$  in equation (5.11) is much higher than  $\lambda/L_e^B$ . For the Cu/W system, these terms are 1.9 and 0.3, and for the Pb/Fe system are 4 and 0.7. Therefore, the condition  $\sigma_{LV}^A \gg \sigma_{LV}^B$ , which is fulfilled for any combination of a low-melting point metal B and a high-melting point metal A, implies generally perfect wettability of A by B. Actually, wetting is good but not perfect (Table 5.1).

The main reasons for this lack of perfection are that (i) a drop of A supercooled at  $T \ll T_F^A$  does not probably wet perfectly its own solid so that  $\sigma_{SV}^A - \sigma_{SL}^A$  is lower than  $\sigma_{LV}^A$  (see (5.10)) and (ii) the solid surface is not pure A but is modified by adsorption of B atoms, Figure 5.2.b, which decreases the surface energy of the solid  $\sigma_{SV}^A$  and hence increases  $\theta$ . The larger the difference  $(\sigma_{LV}^A - \sigma_{LV}^B)$ , the greater the adsorption of B on A and the consequent decrease of the surface energy of the solid. This is confirmed by experimental results obtained by the multi-phase equilibria technique for this type of system showing that the ratio of the surface energy of solid A in equilibrium with a saturated vapour of B to the surface energy of pure solid A at the same temperature,  $\sigma_{SV}^A/\sigma_{SV}^{0,A}$ , lies in the range 0.6 to 0.8 (Eustathopoulos and Joud 1980).

In metal B/metal A systems, an increase in temperature is expected to favour desorption of B from the A surface, thus increasing  $\sigma_{SV}$ . Therefore, contact angles should decrease with increasing temperature as in Figure 5.3 not only because both  $\sigma_{LV}$  and  $\sigma_{SL}$  decrease with this parameter but also because  $\sigma_{SV}$  increases (Pique et al. 1981).

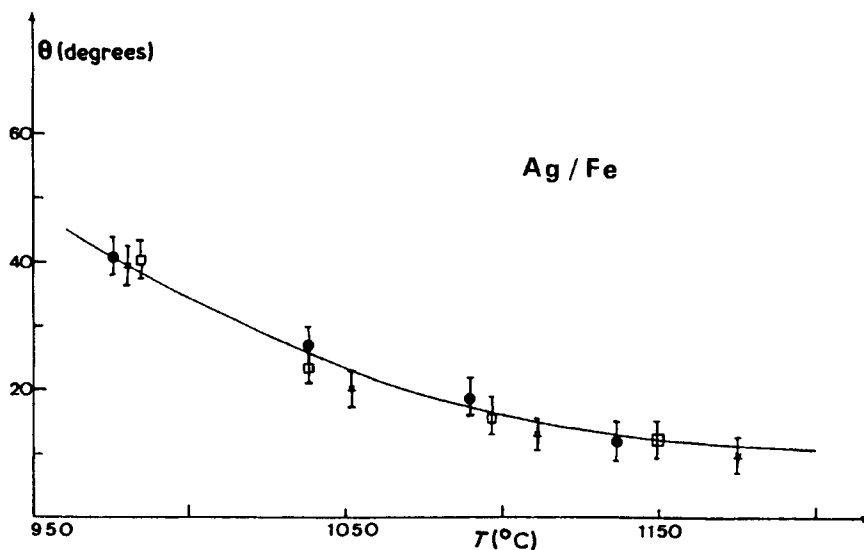
Contact angle values are sensitive to impurities, in particular to oxygen because this can modify not only the surface properties of liquid metals (as discussed in Section 4.1.1), but also the surface properties of solid metals and semi-conductors. Two different cases can occur, depending on the value of  $P_{O_2}$  in the furnace and on the oxygen content of the solid metal. In the first case, a three dimensional oxide layer covers the solid substrate and a non-wetting contact angle is observed. In the second case, the substrate surface has adsorbed oxygen but remains metallic in character so that good wetting ( $\theta \ll 90^\circ$ ) is observed but the contact angles are very sensitive to environmental conditions. This effect is illustrated by the differing contact angles of Cu on polycrystalline W, determined by several teams (Table

5.2). In all cases, good wetting is observed but  $\theta$  varies between  $10^\circ$  and  $55^\circ$ . Low contact angles were observed when using a reducing atmosphere or *in situ* cleaning of the substrate surface with an electron beam, while the higher contact angles were observed using high vacuum or a neutral gas atmosphere. Similar variations in  $\theta$  were observed for the Ag/Fe system using Fe substrates of different purity (Table 5.1). Pollution of W surface by oxygen is confirmed by the wetting kinetics. While spreading times as low as  $10^{-2}$  second are expected in non-reactive systems (Section 2.1.1), a stationary contact angle was obtained only after 20 minutes at  $1100^\circ\text{C}$  for Cu on W (Lorrain 1996). In this case, spreading kinetics are controlled by deoxidation of W, occurring by evaporation of W suboxides. At a lower temperature ( $900^\circ\text{C}$ ), deoxidation kinetics slow down and in some cases no deoxidation occurs, resulting in contact angles as high as  $130^\circ$ , typical of oxidized surfaces (Figure 5.4).

Taking into account the fact that deoxidation of solid metals is very difficult at low temperatures, it is usual to observe non-wetting contact angles for insoluble metal/metal systems.

**Table 5.2.** Contact angles measured by different authors for the Cu/W system at  $1100^\circ\text{C}$ .

Substrate characteristics	Atmosphere	$\theta$ (deg)	Reference
surface purified by electron beam	high vacuum ( $\approx 10^{-6}$ mbar)	10	(Doussin and Omnes 1967)
prior heat treatment for 1h at $1100^\circ\text{C}$ in $\text{H}_2$	$\text{H}_2$	30	(Ligachev et al. 1979)
	He	55	
	$\text{H}_2$	10	(Lesnik et al. 1984)
prior heat treatment for 30 min at $900^\circ\text{C}$ under vacuum	high vacuum ( $< 10^{-5}$ mbar)	50	(Nicholas and Poole 1967)
–	high vacuum ( $< 10^{-5}$ mbar)	40	(Gorskii et al. 1974)
prior heat treatment for 2h at $1100^\circ\text{C}$ under vacuum ( $R_a = 15$ nm)	high vacuum ( $< 5 \times 10^{-5}$ mbar)	$47 \pm 5$	(Lorrain 1996)

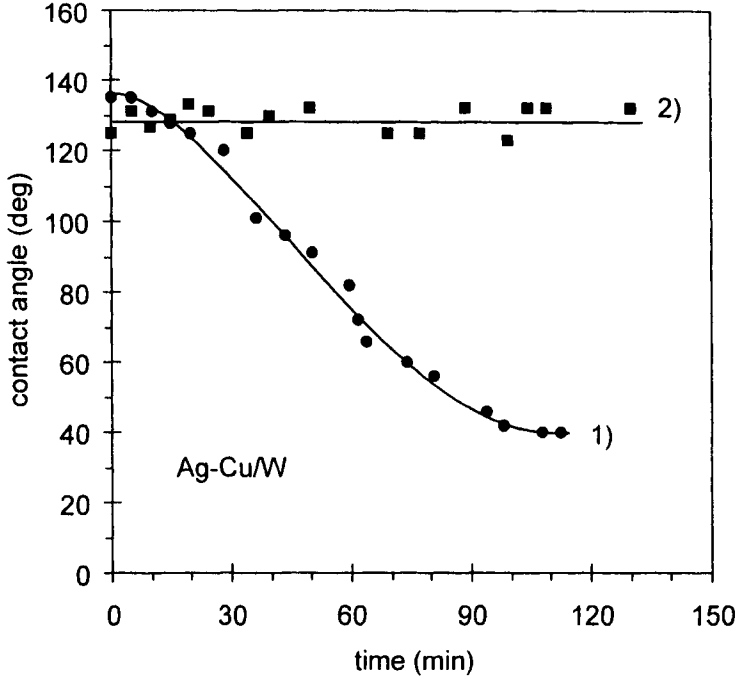


**Figure 5.3.** Stationary contact angle versus temperature data for the Ag/Fe system obtained from three experiments (Pique et al. 1981)[16].

### 5.3. SYSTEMS WITH SIGNIFICANT MUTUAL SOLUBILITY

When the solubility of A in B or B in A is not negligible, definition of a contact angle using the Young equation is problematic (see Figure 2.18) unless the two phases are presaturated. Dissolution of A in B, or B in A, or both, will produce a continuous change in drop volume and a non-planar solid/liquid interface. Therefore only data obtained with presaturated phases are given in Table 5.3. For all systems, except Si/Au, the regular solution parameter  $\lambda$  is positive.

When comparing results in Table 5.3 with those for insoluble systems presented in Table 5.1, the contact angles for systems with mutual solubility are usually lower. (Note, however, that the difference is small, even less than that caused by environment effects for the Cu/W system (Table 5.2)). For instance, the contact angle of Pb on Ni at 740°C is 25° i.e., significantly lower than the contact angle of the insoluble Pb/Fe couple ( $\theta = 53^{\circ}$ , Table 5.1). Because Ni is not tensio-active in molten Pb, the surface energy of Pb-4 at.% Ni is nearly equal to that of pure Pb. Moreover, the surface energies of solid Ni and Fe are very close (see Table 4.2). Therefore, the different contact angles in these systems must be due to significantly different solid-liquid interfacial energies. Similar reasoning accounts for the different contact angles observed at 350°C for Pb on Ag (19°) and on Fe (57°).



**Figure 5.4.** 1) Contact angle versus time for a eutectic (Ag-Cu) drop on polycrystalline W at 900°C in a high vacuum. Before the experiment, the W substrate was heat-treated in high vacuum at 1100°C for 2 h. Despite this treatment, the surface remained oxidised and a slow spreading, controlled by W deoxidation, was observed. 2) The same without prior heat treatment of W. In this case segregation of O at the W surface, by fast grain-boundary diffusion, prevents deoxidation of the substrate, resulting in non-wetting behaviour. From Lorrain (1996).

By neglecting segregation at the S/L interface, a simple expression can be obtained relating the solid-liquid interfacial energy  $\sigma_{SL}$  of a system displaying mutual solubility to the energies of the pure components,  $\sigma_{SL}^i$  ( $i = A, B$ ), the molar fractions of components  $i$  in phases  $j$ ,  $X_i^j$ , and the regular solution parameters in the solid and liquid phases,  $\lambda^S$  and  $\lambda^L$  (Gressin et al. 1982):

$$\sigma_{SL} = \sigma_{SL}^A X_A^S + \sigma_{SL}^B X_B^S + \frac{m_l \lambda^L}{\Omega_m} (X_A^L X_B^S + X_A^S X_B^L) - \frac{m_l \lambda^L}{\Omega_m} X_A^L X_B^L - \frac{m_l \lambda^S}{\Omega_m} X_A^S X_B^S \quad (5.12)$$

**Table 5.3.** Contact angles for systems with mutual solubility.

Liquid B /solid A	T (°C)	$X_A^L$ <sup>(b)</sup>	$X_B^S$ <sup>(b)</sup>	Atm.	$\theta$ (deg)	Reference for $\theta$ values
Pb <sup>(a)</sup> /Ag <sup>(a)</sup>	350	0.065	$\approx 10^{-2}$	Ar+H <sub>2</sub>	19	(Passerone et al. 1982)
Pb <sup>(a)</sup> /Cu	400	0.007	$\approx 0$	H <sub>2</sub>	43	(Bailey and Watkins 1951–52)
	700	0.06	$\approx 0$	H <sub>2</sub>	25	
	700	0.06	$\approx 0$	Ar+H <sub>2</sub>	21	(Coudurier et al. 1977)
Pb <sup>(a)</sup> /Ni	740	0.04	$5 \times 10^{-4}$	Ar+H <sub>2</sub>	25	(Foucher 1998)
Ag <sup>(a)</sup> /Cu <sup>(a)</sup>	782	0.40	0.05	He	19	(Sharps et al. 1981)
Si <sup>(a)</sup> /Au	370	0.81	$\approx 0$	high vacuum	34	(Naidich et al. 1975)

<sup>(a)</sup> presaturated in the other element<sup>(b)</sup> from (Massalski 1990) except for Pb/Ni (Foucher 1998)

When the solubility of B in the solid A is negligible, this equation reduces to:

$$\sigma_{SL} = \sigma_{SL}^A + \frac{m_l \lambda^L}{\Omega_m} (1 - X_A^L)^2 \quad (5.13)$$

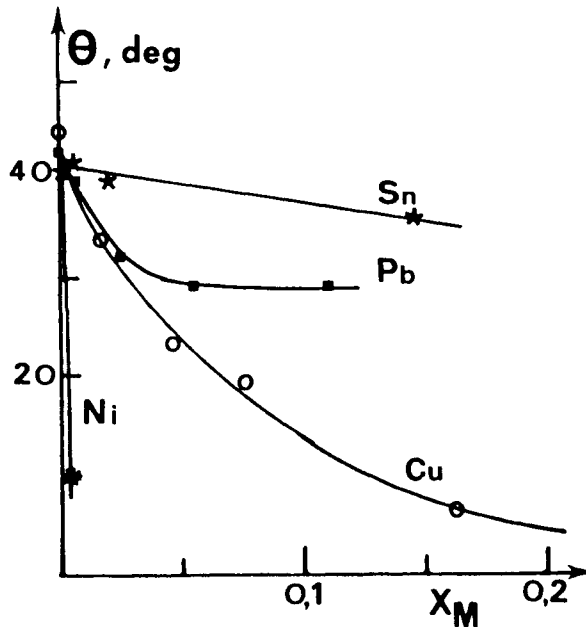
and for  $X_A^L \ll 1$ , equation (5.13) reduces to (5.8). For example,  $\lambda^L$  values are very different for the Pb/Fe and Pb/Ni systems (the enthalpy of mixing of Fe in molten Pb is 91 kJ/mole, but for Ni is 40 kJ/mole (Appendix G)), resulting in a substantial difference in  $\sigma_{SL}$ . For both Ni and Fe, the first term of equation (5.13) is about 0.3 J/m<sup>2</sup> (Eustathopoulos 1983), but the second term is equal to 0.28 J/m<sup>2</sup> for Pb/Ni and 0.65 J/m<sup>2</sup> for Pb/Fe.

Equations (5.6) and (5.13) clarify the relation between solubility and wetting. For a given solid metal A, at fixed temperature, a comparatively high value of  $X_A^L$  results from a low value of  $\lambda$ , which in turn leads to a low value of  $\sigma_{SL}$  (equation (5.13)). This relation between wettability and solubility in metallic systems, through their dependence upon the same energy parameter (i.e.,  $\lambda$ ), was identified long ago by Wassink (1967).



#### 5.4. EFFECTS OF ALLOYING ELEMENTS

The wetting of a liquid B on a solid A may be improved by additions to B of an element M. Thus, while Figure 5.5 shows that additions of Sn and Pb in Ag have little effect on wetting of Fe, that of Cu is moderate and of Ni is strong. Because the surface energies of Pb ( $390 \text{ mJ/m}^2$ ) and Sn ( $490 \text{ mJ/m}^2$ ) are much lower than that of Ag ( $910 \text{ mJ/m}^2$ ), additions of 10 at.% of Pb and Sn into Ag produce a decrease of the surface energy of as much as 30% (Eustathopoulos and Joud 1980). According to the Young equation, this decrease of  $\sigma_{LV}$  would lead to perfect wetting on Fe if  $\sigma_{SV}$  and  $\sigma_{SL}$  are constant. This is not observed experimentally, so  $\sigma_{SV}$  and  $\sigma_{SL}$  cannot be constant. Because the addition of these elements cannot increase  $\sigma_{SL}$  significantly (see Sections 6.5.1 and Figure 6.28) one must conclude that adsorption of these elements decreases not only  $\sigma_{LV}$  for molten Ag but also  $\sigma_{SV}$  for solid Fe. This suggests that an increase in wetting can seldom be produced by low-melting-point, low-surface-energy, additives because the resultant decrease of  $\sigma_{LV}$  may be compensated by that of  $\sigma_{SV}$  so that the net effect on the contact angle is weak.



**Figure 5.5.** Influence of Sn, Pb, Cu and Ni dissolved in Ag on the contact angles of the liquid Ag/solid Fe system at  $965^\circ\text{C}$  in an Ar-5%  $\text{H}_2$  atmosphere (Coudurier et al. 1987) [3].

Compared to Sn and Pb, molten Cu has a high liquid/vapour surface energy (1350 mJ/m<sup>2</sup>) that is higher than the surface energy of Ag and closer to the surface energy of Fe. For Ni, the value of  $\sigma_{LV}$  is even higher than that for Ag and does not differ significantly from that of Fe. Thus the beneficial influence of Cu and Ni on  $\theta$  must be due to a decrease in the solid Fe/liquid Ag interfacial energy. For an element M at infinite dilution in a liquid matrix B, the adsorption energy of an atom M at the liquid side of the interface of a liquid B/solid A system with a negligible mutual solubility is given by (Gomez-Moreno et al. 1982):

$$E_{M(B)}^{\infty,SL} = m_l(\lambda_{AM} - \lambda_{BM} - \lambda_{AB}) \quad (5.14)$$

The more negative the value of  $E_{M(B)}^{\infty,SL}$ , the stronger the decrease in  $\sigma_{SL}$  and  $\theta$  (see equation 6.28). For A = Fe, B = Ag and M = Cu,  $E_{Cu(Ag)}^{\infty,SL}/m_l$ , calculated using  $\lambda$  values of Appendix G, is -70 kJ/mole, indicating a strong adsorption of Cu. For M = Ni, this adsorption is even stronger, with  $E_{Ni(Ag)}^{\infty,SL}/m_l$  equal to -180 kJ/mole. Thus there is a much stronger effect on the contact angle of Ag by additions of Ni than of Cu (Figure 5.5). Note that a complete model, applicable also to concentrated B-M solutions and taking into account both adsorptions of M at the liquid side and the solid side of the interface, was proposed by Chatain et al. (1985). However, selection of alloying elements M for improved wetting based only on the value of  $E_{M(B)}^{\infty,SL}$  given by (5.14) and on the melting point of M achieved significant improvements with the Pb-M/Fe systems (Gomez-Moreno et al. 1982) and with the Ag-M/Fe systems (Coudurier et al. 1987).

## 5.5. SYSTEMS THAT FORM INTERMETALLIC COMPOUNDS

Comparison of the results for systems that form compounds (Table 5.4), for which the regular solution parameter  $\lambda$  is negative, with those for systems that do not form compounds (Tables 5.1 and 5.3) does not reveal strong differences in wetting. A more detailed examination of data obtained by individual teams for the same substrate, temperature and working conditions, but using two liquid metals, only one of which forms intermetallic compounds, shows some limited effects on contact angle values. Thus, the contact angle of Sn on Cu at 400°C (Table 5.4) is 20° lower than the contact angle of Pb on the same substrate (Table 5.3). A similar difference exists between contact angle values for Sn/Fe (Table 5.4) and Pb/Fe (Table 5.1). Moreover, the final wetting in systems in which intense reactions occur at the interface is usually less sensitive to environmental factors than in insoluble

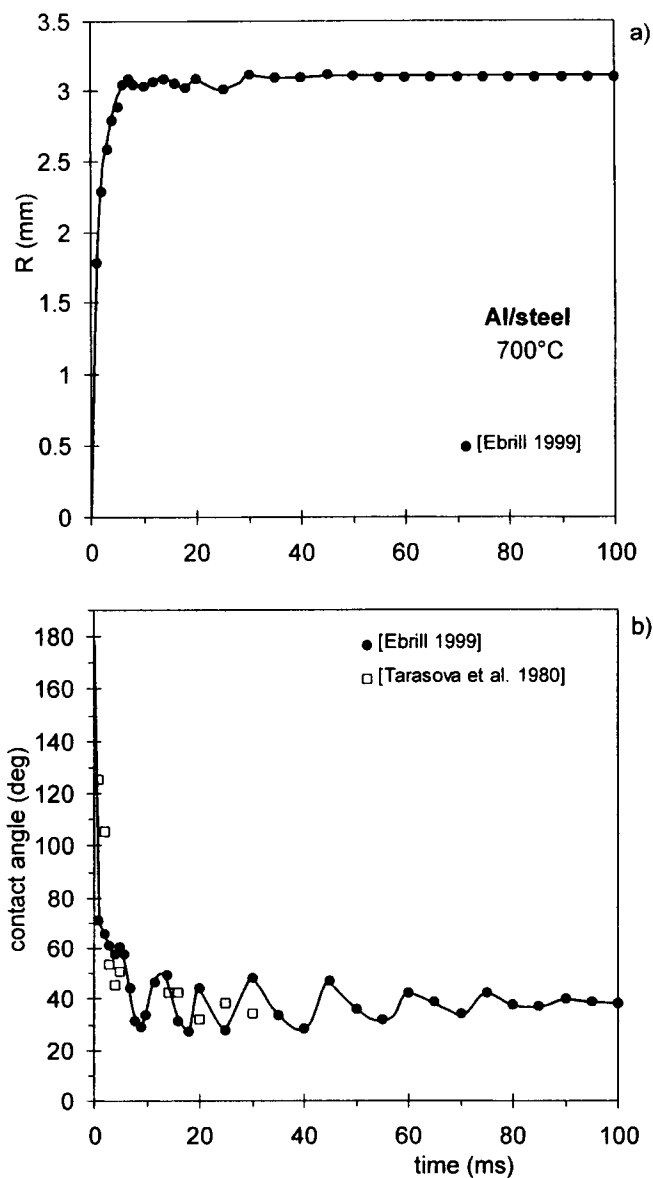
systems. This is because thin oxide layers on solid or liquid metals are disrupted locally by reaction product formation initiated either by diffusion of reacting components through the thin oxide layer or at oxide defects.

**Table 5.4.** Contact angles for systems that form intermetallic compounds.

Liquid B / solid A	T (°C)	$X_A^L$ <sup>(a)</sup>	Intermetallic compounds	Atm. <sup>(b)</sup>	$\theta$ (deg)	Ref. for $\theta$ values
Sn/Fe	350	$\approx 0$	FeSn <sub>2</sub> , FeSn	H <sub>2</sub>	43	(Popel et al. 1971)
	750	0.02	FeSn, Fe <sub>3</sub> Sn <sub>2</sub>	H <sub>2</sub>	38	
	420	$\approx 0$	FeSn <sub>2</sub> , FeSn	HV	42	(Harvey 1965)
Sn/Cu	400	0.12	Cu <sub>6</sub> Sn <sub>5</sub> , Cu <sub>3</sub> Sn, Cu <sub>4</sub> Sn	H <sub>2</sub>	23	(Bailey and Watkins 1951–52)
Al/Fe	750	0.022	FeAl <sub>3</sub> , Fe <sub>2</sub> Al <sub>5</sub> , FeAl <sub>2</sub> , FeAl	HV	33	(Eremenko et al. 1973)
Al/Fe <sup>(c)</sup>	700	0.012	FeAl <sub>3</sub> , Fe <sub>2</sub> Al <sub>5</sub> , FeAl <sub>2</sub> , FeAl	H <sub>2</sub>	35	(Ebrill 1999)
Al/Fe <sup>(d)</sup>	680	0.011	FeAl <sub>3</sub> , Fe <sub>2</sub> Al <sub>5</sub> , FeAl <sub>2</sub> , FeAl	H <sub>2</sub>	30	(Tarasova et al. 1980)
In/Co	300	$\approx 0$	CoIn <sub>3</sub> , CoIn <sub>2</sub>	HV	32	(Lesnik et al. 1970)
	500	0.003	CoIn <sub>2</sub>	HV	18	

<sup>(a)</sup> From (Massalski 1990), <sup>(b)</sup> HV = high vacuum, <sup>(c)</sup> Fe-0.055 wt.% C-0.24 wt.% Mn, <sup>(d)</sup> Fe-0.9 wt.% C-2 wt.% Mn

The effect of temperature on contact angle values is similar for systems that do or do not form intermetallic compounds, as can be seen by comparison of data for In/Co which does, Table 5.4, and Ag/Fe which does not, Figure 5.3. For the In/Co system, a final contact angle is observed in less than  $10^{-2}$  second whatever the temperature and thereafter remains constant for up to 1 h (Lesnik et al. 1970), as for non-reactive couples like Pb/Fe (Section 2.1.1). In the highly reactive Al/Fe system, spreading times close to  $10^{-2}$  second have been found, the final contact angle being close to  $35^\circ$ , Figure 5.6. Similar good wetting has been obtained for Al



**Figure 5.6.** Variation of drop base radius (a) and contact angle (b) with time for Al on steel at  $T \approx 700^\circ\text{C}$  in dry  $\text{H}_2$  using the dispensed drop technique (drop mass of about 50 mg). In the experiment of Ebrill, oscillations of the triple line are due to the kinetic energy of the drop falling from a height of 12–13 mm (see Section 2.1.1). Data from works reported in (Tarasova et al. 1980, Ebrill 1999).

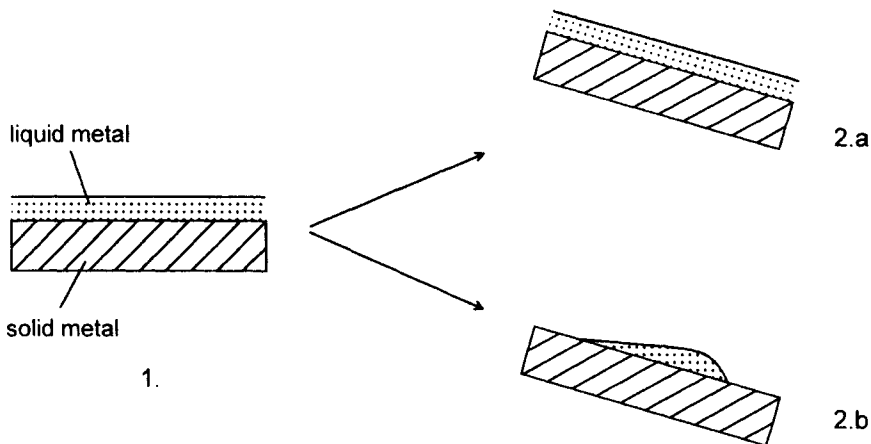
on Ni and Co after much longer spreading times (about 20 seconds) owing probably to oxidation of Al (Eremenko et al. 1980). Note that for Al and Al alloys on low-C steel, formation of intermetallics at the melt/solid interface was detected even for contact times as short as 20 milliseconds (Durandet et al. 1998).

## 5.6. WETTING UNDER TECHNICAL CONDITIONS

The behaviour described in the preceding Sections has been that observed during rigorously controlled laboratory studies using carefully cleaned materials in chemically inert environments. In practice, it may not be possible or economic to adopt such procedures, but nevertheless observations of the wetting behaviour in technical conditions can be interpreted provided it is realised that most solid surfaces of technical materials are covered by oxide films. Thus consideration must be given to how metal-metal contact can be achieved as well as to the implications of such contact for wetting behaviour.

The procedures that have been adopted to achieve adequate wetting behaviour of technically important materials are multitudinous and often very material- and application-specific. Nevertheless, Bailey and Watkins (1951–52) systematically studied the wetting behaviour of a considerable number of metal/metal combinations in an attempt to identify improved ways of soldering, brazing and liquid coating. They assessed wetting behaviour in flowing  $H_2$  by a variety of test methods: by flooding the solid surface with a liquid and observing the behaviour when the melt was decanted, by immersing a solid plate and observing draining during its withdrawal, and by spreading drop tests. In the flooding test, a solid foil, after heat treatment at 600°C in  $H_2$  for 15 minutes, came into contact with a liquid metal to form a continuous film on its surface (Figure 5.7.1). Thereafter, the foil was tilted for 15 seconds, leading either to configuration 2.a of Figure 5.7 in which the film is stable, or to configuration 2.b in which the film has collapsed into drops. A third case was observed and classified as “non-wetting”, in which no liquid adhered as a film or drops to the solid surface. Bailey and Watkins found that couples forming stable films had receding contact angles close to 0° and equilibrium contact angles of about 20°. Similarly, in systems forming drops, the equilibrium contact angle was more than about 20° and non-wetting couples had equilibrium contact angles of more than 90°.

Selected results of Bailey and Watkins (1951–52) are given in Table 5.5. These demonstrate that configuration 2.a of Figure 5.7 is achieved with a wide range of couples that form intermetallics compounds or in which the liquid member dissolves in the solid. For Ag/Fe, the drop-forming behaviour accords with the results of sessile drop experiments which identified contact angles of 36°–57° as



**Figure 5.7.** Flooding test used in experiments of Bailey and Watkins (1951–52) to determine if a L/S system forms stable films (2.a) or drops (2.b).

equilibrium values at about 1000°C (Table 5.1). Bailey and Watkins identified other couples that were drop-forming or non-wetting (Table 5.5): they all resemble Ag/Fe in being insoluble, the only exception being the Bi/Cu system in which Bi at 400°C dissolves a limited quantity of Cu. The Pb/Fe system was described in Section 5.2 as having a sessile drop contact angle of 57° at 350°C but was classified by Bailey and Watkins as non-wetting at 400°C. However, this possible contradiction can be resolved by reference to the results of their spreading drop tests which yielded contact angles of more than 90° up to 1000°C for both Pb and Bi on the same particularly impure Fe. These results strongly suggest that even in their highly reducing H<sub>2</sub> atmosphere, impure Fe substrates were oxidized.

The Bailey and Watkins study shows that continuous liquid film formation is favoured by interfacial reactivity due to mutual solubility or to formation of intermetallics. This correlation between film stability and reactivity is due to several reasons:

- 1) As shown in the previous Sections, the stable contact angles for systems displaying mutual solubility or forming intermetallics are somewhat lower than those for insoluble couples.
- 2) Systems in which there is some reactivity between liquid and solid phases are less sensitive to oxygen pollution than insoluble couples. This is shown by comparing results in Table 5.5 for different liquid metals on Fe. Couples forming intermetallics (Sn/Fe, Zn/Fe) readily established a metal-metal interface and stable liquid film. For the same Fe solid substrate in contact with insoluble metals

such as Pb and Bi, a metal-metal interface is not formed even at temperatures as high as 900°C.

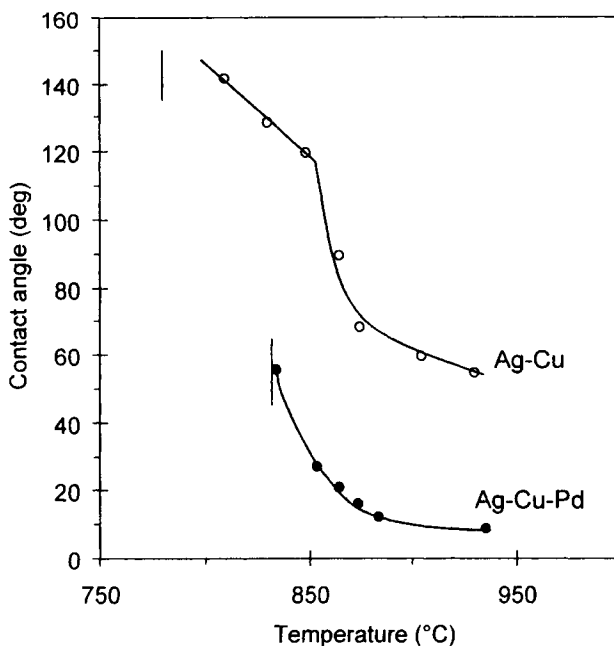
3) Collapse of a liquid film into drops depends on both equilibrium contact angle and the topography of the solid/liquid interface, so film stability is favoured by roughness of the surface. Dissolution of the solid in the liquid, grain-boundary grooving to produce the “secondary wetting” analysed in Appendix H or formation of intermetallics can increase the roughness of the solid surface and cause near-zero receding contact angles.

**Table 5.5.** Wetting data derived from flooding tests (Bailey and Watkins 1951–52).

System	Temperature (°C)	Phase diagram characteristics	Behaviour
Bi/Au	300	intermetallics	film
Cd/Cu	350	intermetallics	film
Bi/Ni	400	intermetallics	film
Pb/Au	400	intermetallics	film
Sn/Fe	400	intermetallics	film
Zn/Au	450	intermetallics	film
Zn/Cu	500	intermetallics	film
Zn/Fe	500	intermetallics	film
Sb/Ag	550 (*)	intermetallics	film
Sb/Cu	600 (*)	intermetallics	film
Al/Fe	700	intermetallics	film
Sb/Fe	700	intermetallics	film
Pb/Ag	400	soluble	film
Ag/Cu	850 (*)	soluble	film
Ag/Au	1000	soluble	film
Ag/Ni	1000	soluble	film
Bi/Cu	400	2 at.% Cu in liquid Bi	drops
Bi/Fe	400	insoluble	non-wetting
Pb/Cu	400	insoluble	drops
Pb/Fe	400	insoluble	non-wetting
Ag/Fe	1000	insoluble	drops

(\*) using eutectic liquid

Bailey and Watkins used solid metal substrates that were only moderately oxidizable and therefore their observations are not directly relevant to many current technical requirements. A similar systematic survey using metals and alloys with high oxygen affinities is not known but nevertheless some more



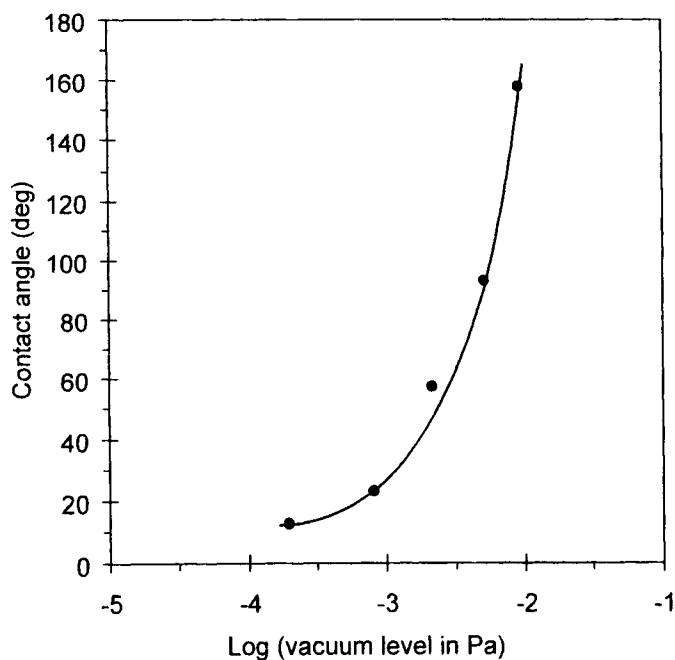
**Figure 5.8.** Contact angle data for Ag-28 wt.% Cu and Ag-16 wt.% Cu-14 wt.% Pd on AISI 321 steel in a vacuum of  $2 \times 10^{-4}$  Pa during a temperature rise with a heating rate of  $5^\circ\text{C}/\text{min}$ . The vertical bars identify melting temperatures. From (McGurran and Nicholas 1985).

restricted studies cast light on the influence of metal-metal interactions on wetting behaviour. Thus McGurran and Nicholas (1985) examined the ability of Ag-Cu alloys to wet AISI 321 steel, a Fe-18Cr-8Ni-1Ti (in wt.%) alloy that forms a chemically stable surface of  $\text{Cr}_2\text{O}_3$ . Abraded and degreased coupons of the steel were wetted by sessile drops of Ag-28 wt.% Cu at temperatures of  $850^\circ\text{C}$  in a good vacuum. However, sessile drops of an Ag-16 wt.% Cu-14 wt.% Pd alloy wetted much better as soon as they melted at  $835^\circ\text{C}$ , as shown in Figure 5.8. Pd had two effects on wetting. First, it improved the “intrinsic” wetting of Ag-Cu eutectic on steel, as seen by the contact angles obtained at the highest temperature in Figure 5.8. This can be easily explained using equation (5.14). Taking  $A = \text{Fe}$ ,  $B = \text{Ag}$  and  $M = \text{Pd}$ , we find  $E_{\text{Pd}(\text{Ag})}^{\infty, \text{SL}}/m_1 = -104 \text{ kJ/mole}$ , which indicates a stronger effect of Pd on  $\sigma_{\text{SL}}$  and  $\theta$  than Cu ( $E_{\text{Cu}(\text{Ag})}^{\infty, \text{SL}}/m_1 = -70 \text{ kJ/mole}$ ). Second, Pd favoured the disruption of the oxide film on the substrate, because its solubility in Fe is much greater than that of Ag or Cu. Oxide film disruption implies that the surface oxide



is flawed in at least some locations. Diffusion of Pd into the substrate in such regions to form a solid solution will cause a volume change and this then could produce decohesion of the oxide/substrate interface to increase the area of liquid metal/solid metal contact and hence decrease the contact angle. Other evidence consistent with such a picture is the detrimental effect of oxidising the steel surface to produce thick oxide films; oxidation for 1 hour at 750°C increased the Ag-Cu-Pd contact angle to 52° while oxidation for 16 hours increased it to 135°. Degrading the vacuum level, and hence presumably increasing the partial pressure of O<sub>2</sub> also caused contact angles to rise, as shown in Figure 5.9. Finally it should be noted that such effects are not specific to surface films of Cr<sub>2</sub>O<sub>3</sub>, qualitatively similar observations having been made by Wall and Milner (1961–62), for substrates of Al and alloys containing Al whose surfaces were coated by exceptionally tenacious films of Al<sub>2</sub>O<sub>3</sub>.

The need to deoxidise metallic solid surfaces to make them wettable by liquid metals has been recognized for a long time and various types of liquid fluxes are used to achieve this, as discussed in Section 10.2.



**Figure 5.9.** The wettability of AISI 321 steel by Ag-16 wt.% Cu-14 wt.% Pd at 880°C as function of vacuum quality (McGurran and Nicholas 1985).

**5.7. CONCLUDING REMARKS**

Liquid metals wet well metallic substrates ( $\theta \ll 90^\circ$ ) whatever the intensity of interfacial interactions unless the metallic surfaces are oxidized. Adsorption of oxygen on solid substrates can increase contact angles by tens of degrees. Intrinsic wetting seems to be slightly improved in systems with some solubility or which form intermetallics. The main effect of interfacial reactions is the disruption of oxide layers covering the metallic surfaces, allowing the formation of real metal-metal interfaces.

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## Chapter 6

# Wetting properties of metal/oxide systems

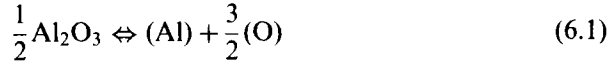
Knowledge of wetting and bonding in metal/oxide systems is important in many fields of materials engineering because oxides are the most widely used ceramics. Moreover, metal/oxide interfaces play also a key role in metal/metal and metal/non-oxide ceramic couples in which one of the partners is an oxidisable material, such as stainless steel or SiC. Finally, certain oxides lend themselves well to fundamental studies because they can be obtained easily as high-purity and monocrystalline ( $\text{Al}_2\text{O}_3$ ,  $\text{MgO}$ ) or amorphous ( $\text{SiO}_2$ ) solids.

In the first Section, attention is paid to distinguishing between reactive and non-reactive systems from the point of view of wettability. Then, after describing wetting and bonding of non-reactive couples, we discuss the effect on these characteristics of oxygen, which is the most common impurity in solid/liquid/vapour systems, as well as the effect of reactive and non-reactive alloying elements. Finally, in a short Section, we consider some results for the wetting of fluorides which like oxides are very ionic.

### 6.1. REACTIVE AND NON-REACTIVE SYSTEMS

At high temperatures, there is always some dissolution of the oxide in the liquid metal but to what extent can this reactivity affect wettability? Useful insight can be obtained by studying spreading kinetics: the time for millimetre size droplets to reach capillary equilibrium is less than  $10^{-1}$  second for non-reactive systems (see Section 2.1.1), so much slower spreading kinetics are a strong indication of control by interfacial reactions.

Another method of obtaining the needed insight is to plot equilibrium or stationary contact angles for a series of metal/oxide systems versus a parameter characterising the oxidation-reduction reaction between a liquid metal M and an oxide  $\text{A}_n\text{O}_m$ , leading to the formation of  $\text{M}_p\text{O}_q$  oxide (Naidich 1981, Eustathopoulos and Drevet 1994), or more simply oxide dissolution in the liquid. Consider at a given temperature a pure liquid metal M on an oxide substrate, for instance  $\text{Al}_2\text{O}_3$ . The dissolution reaction of  $\text{Al}_2\text{O}_3$  in M at the solid/liquid interface can be written as:



where the parentheses mean that the elements are dissolved in the matrix M. The equilibrium constant  $K_D$  for reaction (6.1) is:

$$K_D(T) = a_{\text{Al}}a_{\text{O}}^{3/2} = \exp\left(\frac{\Delta G_{f(\text{Al}_2\text{O}_3)}^0}{2RT}\right) \quad (6.2)$$

where  $a_{\text{Al}}$  is the thermodynamic activity of Al in the alloy (reference state: pure liquid Al),  $a_{\text{O}}$  is the activity of dissolved oxygen (reference state: one atmosphere of pure  $\text{O}_2$ ) and  $\Delta G_{f(\text{Al}_2\text{O}_3)}^0$  is the standard Gibbs energy of formation per mole of  $\text{Al}_2\text{O}_3$ . For mole fractions of Al and O in the liquid,  $X_{\text{Al}}$  and  $X_{\text{O}}$ , lower than  $10^{-3}$ , the activity coefficients  $\gamma$  of these elements are nearly constant (Henry's law) and equal to the activity coefficients at infinite dilution in M,  $\gamma_{\text{O}}^\infty$  and  $\gamma_{\text{Al}}^\infty$ . Then, equation (6.2) becomes:

$$K'_D(T) = X_{\text{Al}}X_{\text{O}}^{3/2} \quad \text{with} \quad K'_D(T) = K_D(T)(\gamma_{\text{Al}}^\infty)^{-1}(\gamma_{\text{O}}^\infty)^{-3/2} \quad (6.3)$$

If (i) the vapour phase does not influence reactions at the solid/liquid interface and (ii) the diffusion of components of the solid (Al and O) in bulk  $\text{Al}_2\text{O}_3$  is slow compared to the dissolution rate at the interface, the values of  $X_{\text{Al}}$  and  $X_{\text{O}}$  must satisfy the condition:

$$3X_{\text{Al}} = 2X_{\text{O}} \quad (6.4)$$

The progress of the dissolution reaction (6.1) reached at equilibrium can be characterised by the equilibrium mole fraction of O in the liquid M. Combining equations (6.3) and (6.4):

$$X_{\text{O}} = \left(\frac{3}{2}\right)^{2/5} (K'_D(T))^{2/5} \quad (6.5)$$

Activity coefficients can be related to the partial enthalpies and partial excess entropies of mixing of Al and O at infinite dilution in M as follows:

$$\gamma_{\text{Al}}^{\infty} = \exp\left(\frac{\overline{\Delta G}_{\text{Al(M)}}^{\text{xs},\infty}}{RT}\right) = \exp\left(\frac{\overline{\Delta H}_{\text{Al(M)}}^{\infty} - T\overline{\Delta S}_{\text{Al(M)}}^{\text{xs},\infty}}{RT}\right) \quad (6.6.a)$$

$$\gamma_{\text{O}}^{\infty} = \exp\left(\frac{\overline{\Delta G}_{\text{O(M)}}^{\text{xs},\infty}}{RT}\right) = \exp\left(\frac{\overline{\Delta H}_{\text{O(M)}}^{\infty} - T\overline{\Delta S}_{\text{O(M)}}^{\text{xs},\infty}}{RT}\right) \quad (6.6.b)$$

Substituting equations (6.6) in equation (6.5) yields:

$$X_{\text{O}} = \left(\frac{3}{2}\right)^{2/5} \exp\left[\frac{\Delta G_{\text{R}}^*}{5RT}\right] \quad (6.7.a)$$

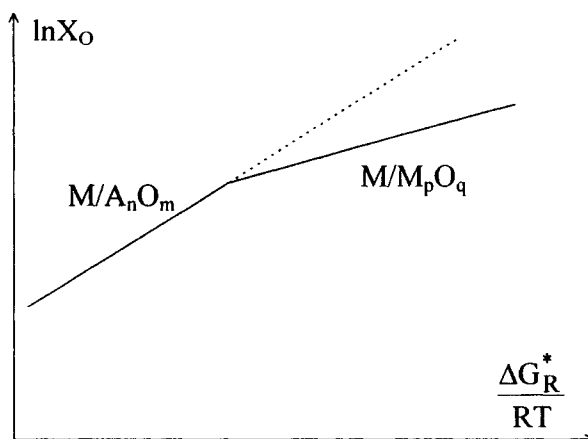
$$\text{with} \quad \Delta G_{\text{R}}^* = \Delta G_{\text{f(Al}_2\text{O}_3)}^0 - 2\overline{\Delta G}_{\text{Al(M)}}^{\text{xs},\infty} - 3\overline{\Delta G}_{\text{O(M)}}^{\text{xs},\infty} \quad (6.7.b)$$

In the general case of an  $\text{A}_n\text{O}_m$  oxide,  $X_{\text{O}}$  is given by:

$$X_{\text{O}} = \left(\frac{m}{n}\right)^{n/(n+m)} \exp\left[\frac{\Delta G_{\text{R}}^*}{(n+m)RT}\right] \quad (6.8.a)$$

$$\text{with} \quad \Delta G_{\text{R}}^* = \Delta G_{\text{f(A}_n\text{O}_m)}^0 - n\overline{\Delta G}_{\text{A(M)}}^{\text{xs},\infty} - m\overline{\Delta G}_{\text{O(M)}}^{\text{xs},\infty} \quad (6.8.b)$$

Note that when the mole fraction of dissolved oxygen is higher than the solubility limit of oxygen in M, precipitation of an  $\text{M}_p\text{O}_q$  oxide occurs. However, for the sake of homogeneity, only the dissolution reaction will be considered when establishing the reactivity scale. In other words, the value of  $X_{\text{O}}$  used in the reactivity scale is that for equilibrium, stable or metastable, between a M-A-O ternary alloy and the  $\text{A}_n\text{O}_m$  oxide (Figure 6.1).



**Figure 6.1.** Reactivity in liquid metal M/oxide  $A_nO_m$  systems: above a certain value of  $\Delta G_R^*/(RT)$ , where  $\Delta G_R^*$  given by equation (6.8.b) is a Gibbs energy for dissolution of  $A_nO_m$  oxide in liquid metal M, a new oxide ( $M_pO_q$ ) precipitates at the interface. (Note that the reactivity scale in Figure 6.2 is built using the extrapolated part of the curve (dotted line) corresponding to the equilibrium between the liquid metal and the initial oxide  $A_nO_m$ ).

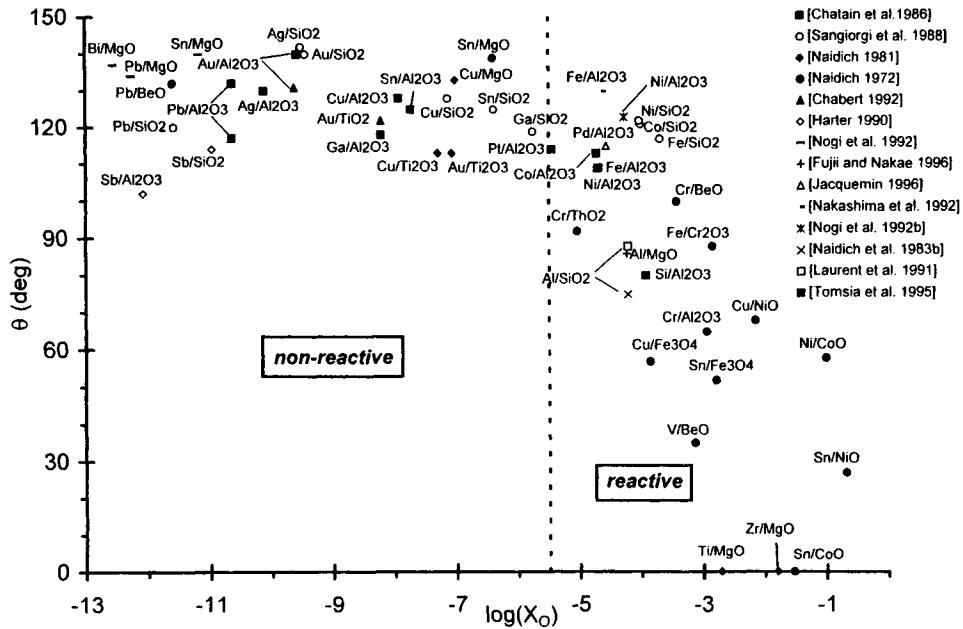
Experimental contact angles  $\theta$  are presented in Figure 6.2 as a function of calculated values of  $\log X_O$  for a number of pure metal M/ionocovalent oxide systems. The  $\theta$  values have been obtained by the sessile drop technique under high vacuum or in neutral or reducing gas atmosphere. Experimental data used in Figure 6.2 come mainly from compilations (Naidich 1981), (Chatain et al. 1986) and (Sangiorgi et al. 1988). Calculations of  $X_O$  from equation (6.8), with approximations allowing use of homogeneous thermodynamic data, are detailed by (Eustathopoulos and Drevet 1998).

The main comment that can be made concerning this figure is that for  $X_O < 10^{-6}$ , contact angles hardly vary with  $X_O$ . All  $\theta$  values (except that for  $Sb/Al_2O_3$ ) lie between  $110^\circ$  and  $140^\circ$  and systems with such  $\theta$  values henceforth will be considered as *non-reactive* regarding wettability.

For  $X_O > 10^{-5}$ ,  $\theta$  decreases steeply and tends towards zero as reactivity increases. This reactivity consists first of dissolution reactions (e.g.  $Cu/NiO$ ,  $Cu/Fe_3O_4$ ), then of reactions to form new phases at the interface (e.g., the  $Ti/MgO$  and  $Zr/MgO$  systems, which form  $Ti$  and  $Zr$  oxides). In the  $Sn/NiO$  and  $Sn/CoO$  systems studied in high vacuum, the reduction of  $NiO$  and  $CoO$  by liquid  $Sn$  is possible and as dissolved oxygen is eliminated continuously by pumping the amount of dissolved  $Ni$  or  $Co$  produced by this reaction can become greater than that



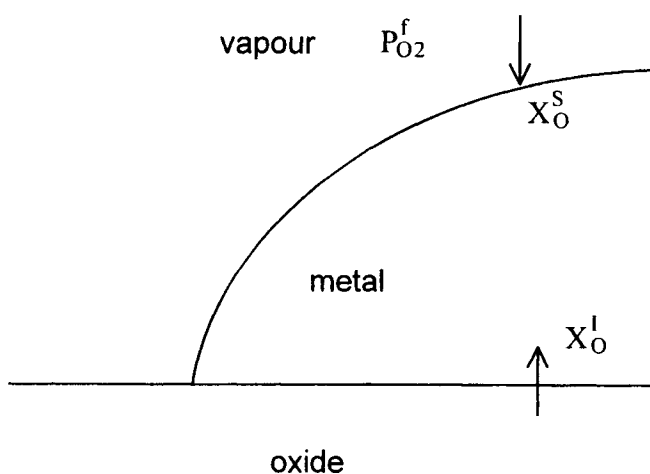
needed to precipitate the intermetallics  $\text{Ni}_3\text{Sn}$  or  $\text{Co}_3\text{Sn}_5$  that are wettable by liquid metals (see Section 5.5).



**Figure 6.2.** Experimental contact angles for pure liquid metal/oxide systems (taken from references given in the figure) versus calculated values of molar fraction of oxygen in the liquid metal caused by dissolution of the oxide. From (Eustathopoulos and Drevet 1998) [17].

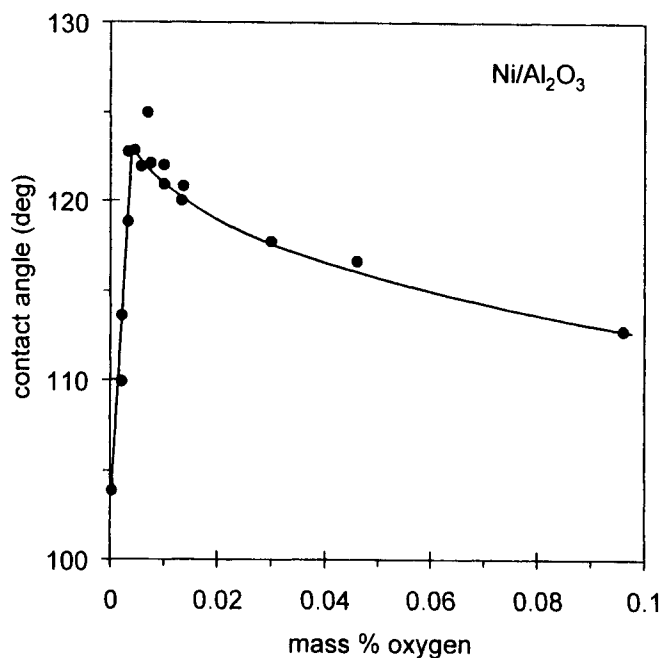
The above distinction between non-reactive and reactive systems does not take into account the possible effect on reactivity and wettability of the furnace atmosphere. The concentration of dissolved oxygen in the liquid close to the S/L/V triple line will lie between two limits. The first of these is that for congruent dissolution of the oxide. This can be calculated using equations (6.8) by assuming that local equilibrium is established between the liquid metal and the oxide at the interface. This limit will be identified as  $X_O^I$  where the superscript I denotes its relevance to the interface. The second limit,  $X_O^S(P_{O_2}^f)$  at the liquid surface, is determined by equilibration with the furnace atmosphere in which the oxygen partial pressure is  $P_{O_2}^f$  (see Figure 6.3). Note that even if  $X_O^I$  and  $X_O^S$  can be calculated, it is impossible in practice to calculate the actual value of  $X_O$  at the

triple line, which is the important parameter for the wetting process, because it depends also on the kinetics of the interfacial reaction and oxygen adsorption processes. Despite these difficulties, it is expected that for systems with very small  $X_O$  values, such as Ag/ $Al_2O_3$  (Figure 6.2), and for any reasonable value of  $P_{O_2}$  in the furnace (in high vacuum or in reducing atmosphere  $P_{O_2}$  is typically lower than  $10^{-10}$  atm), the value of  $X_O$  at the triple line will be different from  $X_O^I$  but stay still sufficiently small for the system to remain in the non-reactive range of Figure 6.2. For such systems, the influence of  $P_{O_2}^f$  on wettability is expected to be weak.



**Figure 6.3.** Dissolved oxygen in the liquid metal can come from dissolution of the oxide at the interface (molar fraction  $X_O^I$ ) or from the vapour phase through the drop surface (molar fraction  $X_O^S$ ).

The situation is different for systems such as Cu/NiO and Cu/ $Fe_3O_4$  that lie in the reactive range or close to the non-reactive/reactive transition as when the high melting point d-metals Ni, Co, Fe, Pd or Pt contact  $Al_2O_3$  or  $SiO_2$ . Suppose the dissolved oxygen and/or the dissolved oxide metal (Al in the case of  $Al_2O_3$  or Si in the case of  $SiO_2$ ) have a significant effect on  $\theta$ . Any variation in the concentration of these elements due to a shift of equilibrium (reaction (6.1)) caused by varying  $P_{O_2}$  in the vapour phase would modify  $\theta$ . An example is Ni/ $Al_2O_3$  (Nogi et al. 1992b) at 1873 K for which the experimental  $\theta$ -oxygen content curve passes through a maximum (Figure 6.4). The value of  $\theta$  for the non-reactive Ni/ $Al_2O_3$  system is equal to or higher than the maximum measured value of  $\theta$  ( $\theta_{\max} \cong 123^\circ$ ).



**Figure 6.4.** Contact angle of Ni on  $\text{Al}_2\text{O}_3$  versus oxygen content of Ni at 1873 K. 0.01 mass % of O in Ni corresponds to a molar fraction of  $3.7 \times 10^{-4}$ . Data from work reported in (Nogi et al. 1992b) [18].

Lower  $\theta$  values are due to adsorption of either O and/or Al at the interface (see also Section 6.4.1). Similar behaviour has been observed for the  $\text{Fe}/\text{Al}_2\text{O}_3$  system (Nakashima et al. 1992) at 1873 K with  $\theta_{\text{max}} \cong 130^\circ$ .

The  $\text{Al}/\text{Al}_2\text{O}_3$  system, in which the metal is the oxide cation, is not plotted in Figure 6.2. For this system, equation (6.4) is not valid and  $X_{\text{O}}$  calculated from equation (6.2) taking  $a_{\text{Al}} = 1$  is equal to  $3 \times 10^{-10}$  at 1150 K, at which temperature the contact angle is  $82^\circ$  (Chatain et al. 1986). Similarly, for  $\text{Si}/\text{SiO}_2$  at 1723 K, a value of  $X_{\text{O}} = 2 \times 10^{-5}$  is obtained ( $\theta = 87^\circ$  (Sangiorgi et al. 1988)). These results are discussed in Section 6.3.

A final remark can be made concerning the  $\text{In}/\text{Al}_2\text{O}_3$ ,  $\text{In}/\text{SiO}_2$  and  $\text{In}/\text{MgO}$  systems studied by Harding and Rossington (1970) at 429 K in ultrahigh vacuum. These systems are not plotted in Figure 6.2 because calculated values of  $X_{\text{O}}$  are off the scale: for  $\text{In}/\text{Al}_2\text{O}_3$ ,  $\theta$  is  $124^\circ$  and  $\log X_{\text{O}}$  is  $-29$ , for  $\text{In}/\text{SiO}_2$ ,  $\theta$  is  $128^\circ$  and  $\log X_{\text{O}}$  is  $-25$  and for  $\text{In}/\text{MgO}$ ,  $\theta$  is  $133^\circ$  and  $\log X_{\text{O}}$  is  $-25$ . Such low values of  $X_{\text{O}}$  are not realistic because the oxygen content, coming either from the vapour phase or present as an impurity in In will be much higher. However, these results confirm the

previously observed tendency of contact angle values to be nearly independent of  $X_O$  when  $X_O$  is lower than  $10^{-6}$ .

## 6.2. NON-REACTIVE PURE METAL/IONOCOVALENT OXIDE SYSTEMS

### 6.2.1 Main experimental features

Ionocovalent oxides are characterized by a high thermodynamic stability with negative values of the Gibbs formation energy of several hundreds of kJ/g · atom O, and gap energies of several eV that make them electrical insulators. Their bonding characteristics lie between that of predominantly ionic compounds like MgO (Pauling ionicity: 73%) and more covalent compounds like SiO<sub>2</sub> (Pauling ionicity: 51%).

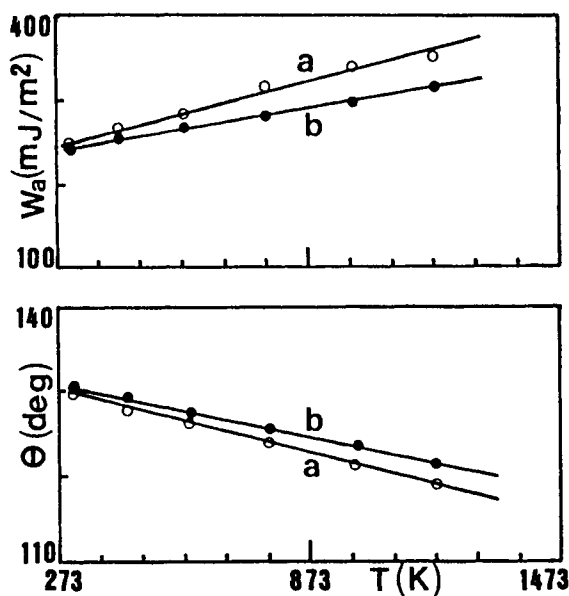
For non-reactive metal/ionocovalent oxide systems, contact angles lie between 110 and 140°, as shown by Figure 6.2. Experimental data for the wetting of smooth monocrystalline Al<sub>2</sub>O<sub>3</sub> substrates by non-reactive metals in high vacuum or low P<sub>O<sub>2</sub></sub> neutral gas atmosphere (P<sub>O<sub>2</sub></sub> between 10<sup>-14</sup> and 10<sup>-20</sup> atm typically) are given in Table 6.1. According to the Young-Dupré equation, the work of adhesion  $W_a$  is only about 20% of the work of cohesion  $W_c$  of the liquid metal (Table 6.1). Because the attraction of the liquid by the solid is very low in these systems, even small barriers to the movement of the triple line, such as surface asperities a few tens of nanometers high, can pin the triple line in a non-equilibrium position (see Figure 1.26). Although no systematic study on spreading kinetics exist for these systems, the stable equilibrium contact angles for millimetre size droplets are expected to be reached in less than 10<sup>-1</sup> second (Section 2.1.1). Thus significant variations of  $\theta$  observed in longer times indicate environment effects or interfacial reactions. The variation of  $\theta$  with temperature is very weak, typically of the order of a few multiples of -0.01 deg/K. For instance, an increase from room temperature to 1000°C produces a decrease of  $\theta$  for Ga on Al<sub>2</sub>O<sub>3</sub> or SiO<sub>2</sub> of only 10 degrees (Figure 6.5). As the liquid metal surface energy  $\sigma_{LV}$  decreases slightly with increasing temperature, the temperature coefficient of the work of adhesion is also weak but always positive (typically 0.1 mJ.m<sup>-2</sup>.K<sup>-1</sup>) (Figure 6.5). Significantly higher values of  $-d\theta/dT$  and  $dW_a/dT$  strongly suggest the occurrence of interfacial reactions or environment effects.

No systematic studies have been performed on the *anisotropy* of wetting. However contact angle measurements for pure Cu on very smooth ( $R_a = 1-2$  nm) surfaces of  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> single crystals revealed contact angle differences of less than 10° (Table 6.2) corresponding to changes in the work of adhesion of less than 150 mJ/m<sup>2</sup> (Vikner 1993). These rather weak effects on  $\theta$  and  $W_a$  do not mean that  $\sigma_{SV}$

**Table 6.1.** Contact angle data for some pure metals on monocrystalline  $\text{Al}_2\text{O}_3$  obtained under high vacuum or reducing gas environment. From (Chatain et al. 1986) except for Au at 1365K (Chabert 1992), Fe (Nakashima et al. 1992), Ni (Nogi et al. 1992b) and Sb (Harter 1990).

Metal	$T_{\text{exp}}$ (K)	$\theta$ (deg)	$W_a/W_c$
Ag	1373	130	0.18
Au	1373	140	0.12
Au	1365	131	0.17
Cu	1423	128	0.19
Fe	1873	130 <sup>(*)</sup>	0.18
Ga	1173	118	0.26
In	429	124	0.22
Ni	1873	123 <sup>(*)</sup>	0.23
Pb	1173	117	0.27
Pb	1173	132	0.16
Sb	998	102	0.40
Sn	1373	125	0.21

<sup>(\*)</sup> maximum experimental values (see Section 6.4.1 and Figure 6.4).



**Figure 6.5.** Work of adhesion and contact angle of Ga on monocrystalline  $\text{Al}_2\text{O}_3$  (a) and vitreous  $\text{SiO}_2$  (b) in high vacuum as a function of temperature. From data reported in (Naidich and Chuvashov 1983).

and  $\sigma_{SL}$  are nearly isotropic quantities. They may vary in the same sense with surface orientation and, as they appear in the Young and Young-Dupré equations with opposing signs, the effect of anisotropy on  $\sigma_{SV}$  and  $\sigma_{SL}$  will be partially compensated. Differences in contact angle of up to  $30^\circ$  were observed for different liquid metals (Pb, Bi, Sn) on three surfaces of highly ionic MgO single crystals as shown in Table 6.3 for Sn. However, it should be noticed that in some systems with very high contact angles and low-surface-energy metals like Pb, Bi or Sn, small changes in  $W_a$  produce relatively large changes in  $\theta$ .

**Table 6.2.** Contact angle of pure Cu on smooth as-received  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> surfaces at 1373K under high vacuum (Vikner 1993).

Surface	$\theta$ (deg)	$W_a$ (mJ/m <sup>2</sup> )
0001	120	650
1 $\bar{1}$ 02	123	592
random	128	500

**Table 6.3.** Contact angle of pure Sn on as-received MgO single crystals at 873K under purified H<sub>2</sub> (Nogi et al. 1992).

Surface	$\theta$ (deg)	$W_a$ (mJ/m <sup>2</sup> )
100	140	121
110	170	8
111	147	84

### 6.2.2 Nature of metal-oxide bond

To identify the nature of predominant interactions at interfaces between non-reactive metal M and ionocovalent oxide AO, different attempts have been made to correlate the energetic properties of interfaces (work of adhesion, work of immersion) to the energy of formation of M oxide or other quantities characteristic of the contacting phases, such as the surface energy of the metal or the gap energy of the ceramic. Any successful correlation between an energetic quantity of interfaces and the formation energy or enthalpy of MO oxide indicates the occurrence of a chemical *interaction* between M and AO at the interface, even

in the absence of a chemical *reaction*. For a series of different metals M on the same oxide AO, the enthalpy of formation of MO oxide,  $\Delta H_{f(MO)}$ , from pure liquid M and gaseous oxygen roughly quantifies the difference between the bond energy  $\epsilon_{M-O}$  in bulk MO and half the bond energy  $\epsilon_{M-M}$  in bulk M (the bond energy  $\epsilon_{O-O}$  in gaseous oxygen being a constant):

$$\Delta H_{f(MO)} \propto \epsilon_{M-O} - \frac{\epsilon_{M-M}}{2} \quad (6.9)$$

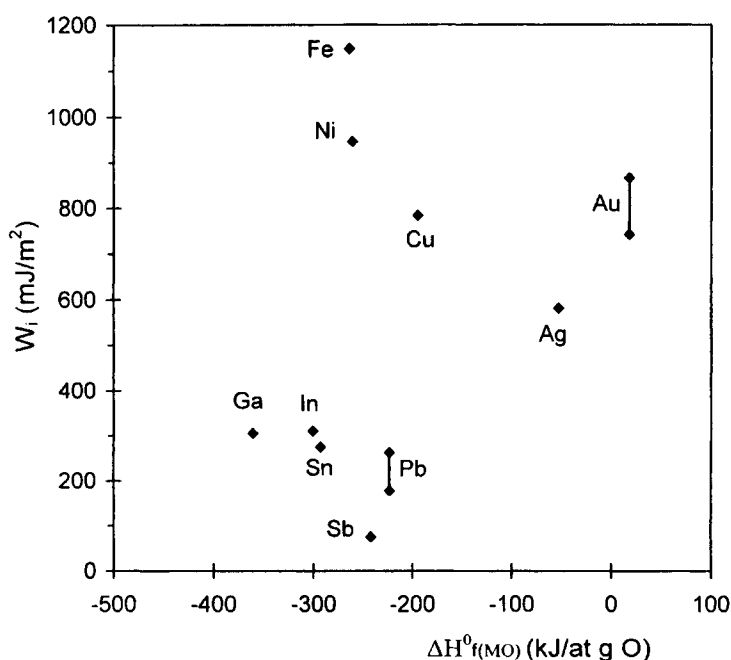
According to the definition of the work of adhesion  $W_a$  in terms of bond energies (equation (1.12) with A = M and B = AO),  $W_a$  is proportional to  $\epsilon_{M-AO}$  where  $\epsilon_{M-AO}$  is an average interaction energy between M atoms and oxide ions. Clearly,  $W_a$  is proportional to an absolute bond energy while  $\Delta H_{f(MO)}$  is proportional to a difference of bond energies. As a result, the interfacial quantity to be used in a correlation with  $\Delta H_{f(MO)}$  should not be  $W_a$  but the work of immersion  $W_i$  which, taking into account its definition (equation (1.54)) and expressions (1.9) to (1.11) of  $\sigma_{SV}$  and  $\sigma_{SL}$ , is indeed proportional to:

$$W_i \propto \epsilon_{M-AO} - \frac{\epsilon_{M-M}}{2} \quad (6.10)$$

Comparing the expressions (6.9) and (6.10) reveals that for a series of metals M on the same oxide AO, if a correlation is observed between  $W_i$  and  $\Delta H_{f(MO)}$  it can be concluded that the interfacial energy  $\epsilon_{M-AO}$  varies as the chemical bond energy  $\epsilon_{M-O}$  in the bulk M oxide (Eustathopoulos and Drevet 1998).

Values of the work of immersion  $W_i (= -\sigma_{LV}\cos\theta)$  of non-reactive metals M on  $Al_2O_3$ , plotted on Figure 6.6 as a function of the standard enthalpy of formation of M oxides  $\Delta H_{f(MO)}^0$ , show no correlation between these two quantities. No improvement in correlation is obtained when  $W_i$  is plotted versus a parameter taking into account both M-O and M-Al interactions (Eustathopoulos and Drevet 1998). Accordingly, it may be concluded that the contribution to adhesion of chemical interactions between M atoms and oxide ions is negligible or weak. Therefore, the interfacial metal/oxide bond is mainly due to *physical* interactions. This conclusion agrees, in the particular case of the Cu/ $Al_2O_3$  system, with results of a spectrometric study of the interfacial bond (Ohuchi and Kohyama 1991). The  $Al_2O_3$  surface was fabricated *in situ*, under ultrahigh vacuum, by thermal

oxidation of Al by microleaks of  $O_2$ . Photoemission spectroscopy was used to monitor the evolution of chemical bonding during Cu deposition but no significant reduction of either the Cu or the substrate energy levels was observed, indicating no chemical interaction between Cu and  $Al_2O_3$ . Note that in contrast the same technique identified strong chemical interaction in the Ti/ $Al_2O_3$  system, which indeed belongs to the reactive range of Figure 6.2.

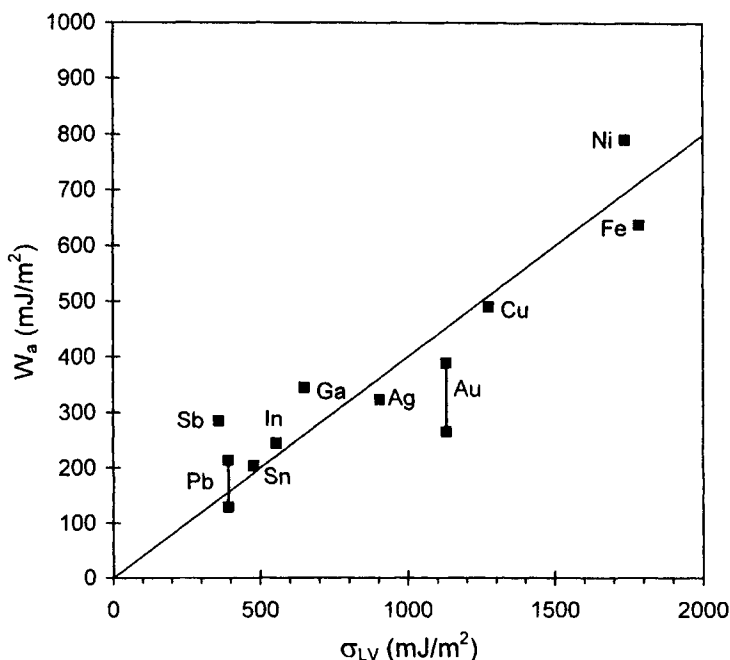


**Figure 6.6.** Experimental values of the work of immersion determined from the data in Table 6.1 for non-reactive pure metal M/monocrystalline  $Al_2O_3$  systems versus the standard enthalpy of formation of M oxide referred to pure liquid M. From (Eustathopoulos and Drevet 1998) [17].

More information about the physical interactions can be obtained noting that contact angles for non-reactive metals are about  $120^\circ$  whatever the metal (Figure 6.2), so this suggests that  $W_a$  varies roughly as the surface energy,  $\sigma_{LV}$ , of the metal in accord with the Young-Dupré equation (1.45). This is verified plotting  $W_a$  as a function of  $\sigma_{LV}$  (Figure 6.7) for a series of non-reactive metals on monocrystalline  $Al_2O_3$ , which leads to a ratio of the work of adhesion to the work of cohesion of the



metal ( $W_c = 2\sigma_{LV}$ ) equal to about 0.20. It may be expected that a similar correlation exists for other ionocovalent oxides.



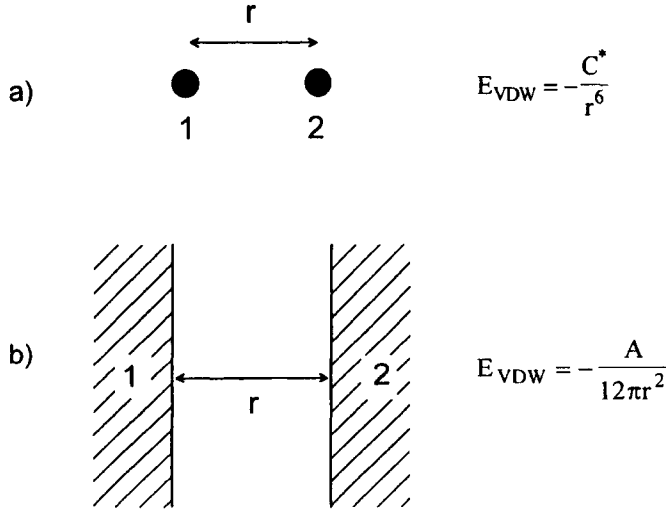
**Figure 6.7.** Experimental values of the work of adhesion for non-reactive pure metal/monocrystalline  $Al_2O_3$  systems versus the liquid surface energies of metals. From (Eustathopoulos and Drevet 1998) [17].

A possible explanation for this correlation is that  $\sigma_{LV}$  for pure metals increases with the plasmon energy of the metal (Stoneham et al. 1995). The plasmon energy is a parameter explicitly contained in the expression of the adhesion energy due to van der Waals *dispersion forces* (Didier and Jupille 1994). The main features of these forces are first that they can be developed between all species, even between neutral and non-polar molecules (cohesion in liquified or solidified rare gas or in liquid hydrocarbons is ensured by these forces), and, second, that they are long-range forces which can be effective up to a range of several tens of nanometers. To understand their origin, consider a non-polar atom such as argon. Although the time average of its electron dipole moment is zero, at any instant there exists a finite dipole moment determined by the instantaneous position of the

electrons around the nuclear protons. This instantaneous dipole generates an electric field that polarizes any nearby neutral atom, inducing a dipole moment in it. The resulted interaction between the two dipoles gives rise to an instantaneous attractive force *between the two atoms* and the time average of this force is finite (Israelachvili 1991). When the two atoms, denoted 1 and 2, at a distance  $r$  and separated by vacuum (Figure 6.8.a), are dissimilar, the resultant interaction energy is given by the London expression:

$$E_{VDW} = -\frac{3}{2} \frac{\alpha_1^0 \alpha_2^0}{(4\pi\epsilon_0)^2 r^6} \frac{I_1 I_2}{(I_1 + I_2)} = -\frac{C^*}{r^6} \quad (6.11)$$

where  $\alpha^0$  is the electronic polarizability,  $I$  is the first ionization potential and  $\epsilon_0$  is the dielectric constant of vacuum.



**Figure 6.8.** Variation with separation distance  $r$  of the interaction energy due to van der Waals forces as calculated by the pairwise interaction model, between two different atoms (a) and between two surfaces (b).  $A$ , the Hamaker constant, equals  $\pi^2 C^* \rho_1 \rho_2$  where  $C^*$  is the constant of the atom-atom pair potential in equation (6.11) (case a) and  $\rho_1$  and  $\rho_2$  are the number of atoms per unit volume in the two bodies (Israelachvili 1991).

Equation (6.11) has been used to calculate the contribution of van der Waals interactions to the metal/oxide adhesion energy (McDonald and Eberhart 1965,

Naidich 1981). To this end, only nearest-neighbour interactions between a metal atom  $M$  and an oxygen ion  $O^{2-}$  of the oxide have been considered, taking  $r$  as the sum of the atomic radius of  $M$  and the ionic radius of  $O^{2-}$ . Note that in equation (6.11) the equilibrium separation distance  $r$  is raised to the sixth power, so the calculated values of interaction energy are very sensitive to assumptions on the interfacial atomic structure. Moreover these calculations contain several approximations. First, although the nearest-neighbour interactions are predominant, longer-range interactions are not negligible. While long-range interactions are weak for each pair of atoms, the final contribution can be significant because many pairs can participate. Thus, although atom-atom van der Waals interactions vary as  $r^{-6}$ , in order to calculate the interaction energy between two flat surfaces (Figure 6.8.b) one must sum (integrate) the energies of all the atoms in one body with all the atoms in the other, which leads to an interaction potential *between the two surfaces* varying as  $r^{-2}$  (Israelachvili 1991). Second, in solids with delocalized electrons like metals, the modes of collective excitation, the *plasmons*, make a supplementary contribution to van der Waals interactions which is not taken into account by pairwise interaction models. Despite these imperfections, equation (6.11) predicts the right order of magnitude for the work of adhesion in metal/oxide systems, namely from 100 to 500 mJ/m<sup>2</sup> (McDonald and Eberhart 1965, Naidich 1981).

Difficulties arising from the use of the pair interaction model are avoided in the Lifshitz theory in which the forces between large bodies, treated as continua, are derived in terms of bulk properties such as dielectric constants and refractive indices. Calculations (Didier and Jupille 1994) of adhesion energy for metal/oxide systems based on the dielectric continuum model of Barrera and Duke (1976) predict that the values for different non-reactive metals on the same oxide ( $Al_2O_3$  or  $SiO_2$ ) increased with the plasmon energy of the metal, in good agreement with experimental findings. However, the calculated values of  $W_a$  exceed experimental measurements by a factor of two. Additionally, these calculations predict that for a given metal on different oxides, the work of adhesion increases as the band gap of the insulator narrows but more accurate wetting experimental results for the same metal on various oxides are needed to test this prediction. Similar calculations using the Lifshitz continuum theory of van der Waals forces were performed by Lipkin et al. (1997) for non-reactive metal/ $Al_2O_3$  systems. These predict the right order of magnitude of  $W_a$ , close to 600 mJ/m<sup>2</sup>, but did not suggest any significant variation of  $W_a$  between low melting point metals like Pb and high melting point metals like Ni.

In these models, the method consists of (i) assuming that a certain type of interaction such as van der Waals dispersion forces (Didier and Jupille 1994, Naidich 1981) or image forces (Stoneham et al. 1995) is predominant at metal/oxide interfaces, (ii) calculation of the adhesion energy resulted from these

forces and (iii) comparison with experimental data. However, because of numerous approximations, calculations based on different types of physical interactions all lead to a similar correct order of magnitude for the work of adhesion, so no firm conclusion can be drawn about the nature of interfacial bonding.

Since 1990, a different approach has been used in the so-called first principles or *ab initio* theories which allow calculation of the electronic charge density, the total energy and the relaxed interfacial atomic structure without any need for fit parameters. Because the computer time for these calculations is long, such methods are possible at present only for systems containing a small number of different atoms (typically one hundred) (Magaud and Pasturel 1998). An example is the solid Ag/MgO couple, assuming the (100) face of Ag being in contact with the (100) face of fcc MgO (Schönberger et al. 1992, Hong et al. 1995). In the work of Hong et al. (1995), the model cell contained three layers of MgO in contact with five layers of Ag. The oxide layers parallel to the interface are stoichiometric and therefore charge-neutral. Two translational configurations were studied, both of which led to the right order of magnitude for the work of adhesion (about  $1 \text{ J/m}^2$ ). The translational configuration in which Ag atoms sat on top of the O atoms across the interface was found to have an adhesion energy twice that of the configuration in which the Ag atoms are above the Mg atoms. When, instead of Ag with its filled d-band, a transition metal like Ti with a partially filled d-band is examined (Schönberger et al. 1992), calculations indicate hybridization of the d-band of Ti with the 2p-band of oxygen i.e., a significant covalent/metallic contribution to the adhesion energy. As a result, a higher adhesion energy is suggested for this system than for Ag/MgO (Schönberger et al. 1992). Actually Ti reacts with MgO as indicated by the location of the Ti/MgO couple in Figure 6.2, meaning that the calculations of Schönberger et al. were made for a Ti layer in a metastable equilibrium with MgO. More systematic studies of this kind are needed to draw definitive conclusions about the bonding mechanism in metal/oxide systems but the results obtained so far are encouraging.

To sum up, in non-reactive *liquid* metal/ionocovalent oxide systems, wetting seems to result from physical, van der Waals, interactions which lead to contact angles of typically  $120\text{--}130^\circ$  and to a  $W_a/(2\sigma_{LV})$  ratio of about 0.20. Any significant difference from the above values indicates the establishment of chemical interactions at the interface.

These conclusions appear to be valid also for non-reactive *solid* metal/oxide systems. Indeed, by studying the equilibrium shape of a solid metallic particle on  $\text{Al}_2\text{O}_3$  (see Section 3.1.6), non-wetting contact angles in the range  $120\text{--}130^\circ$  have been found for noble metals as Au, Ag and Cu at about  $900^\circ\text{C}$  (Pilliar and Nutting 1967, Soper et al. 1996). These values are very close to those obtained for the same metals in the liquid state near their melting point. This closeness can be explained

by taking into account that, on melting, the surface energy of the metal and its work of adhesion on the oxide both decrease and, as shown by the Young-Dupré equation, their effects on the contact angle are opposing and apparently nearly compensating. Indeed the metal/vapour surface energy decreases by about 15% on melting, Section 4.1.3, because the cohesion energy of the bulk metal decreases. Moreover, because the van der Waals interaction energy is simply proportional to the atomic density of contacting phases (see Figure 6.8), the work of adhesion would decrease at melting.

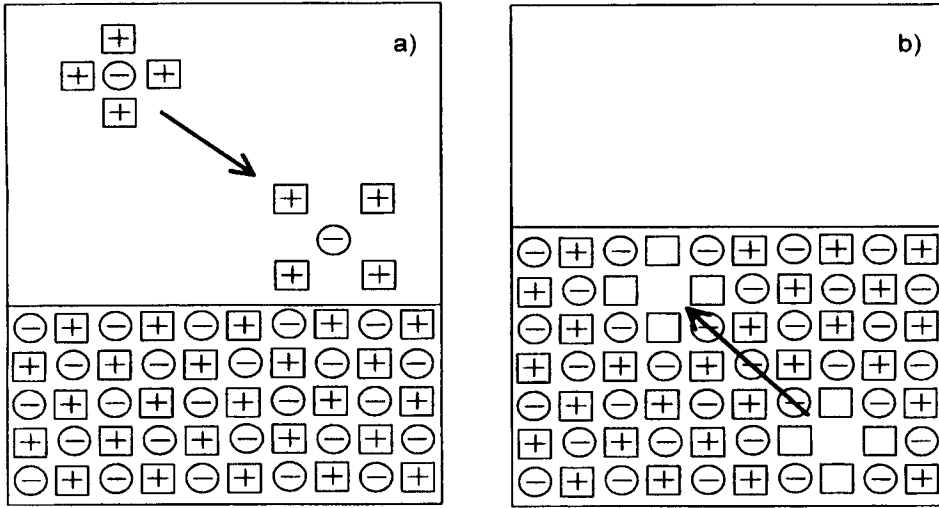
The predominance of van der Waals interactions at solid metal/ $\text{Al}_2\text{O}_3$  interfaces is also shown by the fact that whatever the orientation of monocrystalline  $\text{Al}_2\text{O}_3$  surface, Cu particles are orientated with (111) faces parallel to the  $\text{Al}_2\text{O}_3$  surface (Soper et al. 1996). This orientation maximises the number of metal atoms per unit area in nearest-neighbour interactions with  $\text{Al}_2\text{O}_3$ . A similar behaviour was found for non-reactive fcc metals on carbon substrates i.e., for systems with predominant van der Waals interfacial interactions (Section 8.1).

### 6.3. EFFECT OF ELECTRONIC STRUCTURE OF THE OXIDE

Many oxides of technological importance, such as  $\text{TiO}_2$ ,  $\text{ZrO}_2$ ,  $\text{UO}_2$  and  $\text{Y}_2\text{O}_3$ , possess a significant range of non-stoichiometry which introduces charged defects into the crystal. These defects can interact with the metal at the interface, thus affecting adhesion and wetting.

For the  $\text{Cu}/\text{UO}_{2+x}$  system, it was observed that on increasing the value of  $x$  from 0.001 to 0.084, the contact angle of Cu at 1446K was reduced from  $116^\circ$  to  $84^\circ$  (Hodkin and Nicholas 1977). According to thermodynamic data, the partial pressure of oxygen,  $P_{\text{O}_2}$ , in equilibrium with  $\text{UO}_{2+x}$  for  $x = 0$  at 1446K is  $10^{-16}$  Pa and for  $x = 0.084$  is  $10^{-2}$  Pa. At a  $P_{\text{O}_2}$  value as high as  $10^{-2}$  Pa, molten Cu dissolves a large quantity of oxygen ( $\approx 0.2$  at.% O at 1373K) and as will be seen in Section 6.4.1, oxygen dissolved in liquid metals improves wetting even in concentration as low as a few ppm or tens of ppm. To explain this effect, it was proposed (Naidich 1981) that dissolved oxygen and metal atoms form clusters having a partially ionic character due to charge transfer from the metal to oxygen (Figure 6.9.a). Such clusters can develop coulombic interactions with any ionic substrate and, for this reason, segregate to metal/oxide interfaces, thus improving wetting and thermodynamic adhesion. Accordingly, in the  $\text{Cu}/\text{UO}_{2+x}$  couple, the oxide substrate acts as an oxygen source.

A different mechanism was demonstrated for the  $\text{U}/\text{Y}_2\text{O}_{3-x}$  system studied at 1673K (Tournier et al. 1996). In this study, three different experimental configurations were produced leading to decreasing concentrations of dissolved



**Figure 6.9.** (a) Adsorption of oxygen clusters from the bulk metal at the metal/oxide interface can occur when  $P_{O_2}$  is *high* according to the considerations of Naidich. (b) Adsorption of a cluster centred on an oxygen vacancy from the bulk oxide at the interface can occur when  $P_{O_2}$  is *low*. For the sake of simplicity, total oxidation (case a) or total reduction (case b) of metal around oxygen atoms (case a) or vacancies (case b) has been assumed.

oxygen in U and to increasing degrees of hypostoichiometry. Table 6.4 shows that these decreases produce a strong improvement in wetting and adhesion. The final value of  $W_a$  is four times higher than that predicted to result from physical interactions. Thus, taking  $W_a/(2\sigma_{LV}) \approx 0.20$  as typical of van der Waals interactions (see Section 6.2.2) and the surface tension of liquid U  $\sigma_{LV} = 1600 \text{ mJ/m}^2$ , one obtains a  $W_a$  of about  $640 \text{ mJ/m}^2$ . Therefore, in very low  $P_{O_2}$  environment, the metal/oxide bond for hypostoichiometric oxide must be chemical in nature.

An explanation of the adsorption capability of oxygen vacancies was proposed (Tournier et al. 1996) by analogy with the mechanism of Naidich for the adsorption of dissolved oxygen from the bulk metal to the metal/oxide interface. What is interesting for our purposes in the diagram of Figure 6.9.a is that the strong metal-oxide interaction results from partial rupture of the metallic bond in the cluster and its replacement by an ionic-type bonding. Formation of oxygen vacancies also can lead to a partial rupture of the ionic bond and it may be expected that some reduction in metal ions around a vacancy would occur. Indeed it has been shown, both experimentally and theoretically, that the presence of oxygen vacancies in

**Table 6.4.** Experimental contact angles and corresponding  $W_a$  values for the U/Y<sub>2</sub>O<sub>3-x</sub> system at 1673K for different partial pressures of oxygen (Tournier et al. 1996).

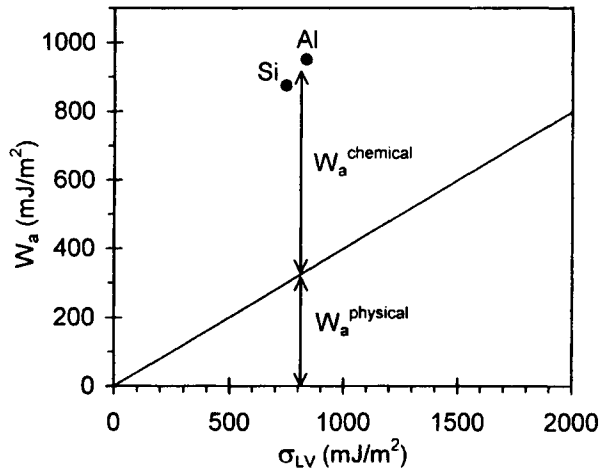
$P_{O_2}$ (Pa)	$\theta$ (deg)	$W_a$ (mJ/m <sup>2</sup> )
$10^{-7}$	106	1160
$10^{-20}$	68	2200
$10^{-23}$	52	2585

yttria locally leads to a more covalent bond (Jollet et al. 1991). In the diagram of Figure 6.9.b, the interface-active species is a cluster consisting of an oxygen vacancy surrounded by partially reduced metal ions. Segregation of such clusters to the oxide side of the interface would ensure a gradual transition from oxidised metal atoms (yttrium cations in the oxide) to metallic bonded atoms (uranium atoms in the liquid).

$\alpha$ -Al<sub>2</sub>O<sub>3</sub> is an oxide with a negligible non-stoichiometry range but (0001) faces of Al<sub>2</sub>O<sub>3</sub> are known to lose oxygen which leads to a two dimensional reconstruction of the surface in very high vacuum at high temperatures (about 1500K) (French and Somorjai 1970). Similar transformations seem to occur on other faces (French and Somorjai 1970, Gillet and Ealet 1992, Pham Van 1992). Furthermore, Al and Si vapours shift the temperature of this 2D reconstruction towards temperatures of 1200K or less (French and Somorjai 1970). Such a transformation may increase the surface energy of Al<sub>2</sub>O<sub>3</sub> (Brennan and Pask 1968) or the metal/Al<sub>2</sub>O<sub>3</sub> adhesion energy by a mechanism similar to that applicable to U/Y<sub>2</sub>O<sub>3-x</sub>. This could explain why contact angles for the Al/Al<sub>2</sub>O<sub>3</sub> and Si/Al<sub>2</sub>O<sub>3</sub> systems are close to 90° and 80° at the melting point of Al and Si respectively, significantly lower than the values 110–140° observed for non-reactive metal/ionocovalent oxide systems (see Figure 6.2). The *chemical interactions* developed between Al or Si and Al<sub>2</sub>O<sub>3</sub> at the interface explain why the experimental work of adhesion for these two metals ( $\approx 900$  mJ/m<sup>2</sup>) deviates strongly from the corresponding van der Waals value, 300 mJ/m<sup>2</sup>, taken from the straight line of Figure 6.10.

Some oxides are electric conductors like metals and can be regarded as metallic, for example TiO, VO and ReO<sub>3</sub>. Thus, TiO has a rocksalt structure (NaCl type) in which each Ti<sup>2+</sup> is surrounded by six O<sup>2-</sup> in an octahedral configuration TiO<sub>6</sub> and the cohesion energy of the crystal is due both to ionocovalent and metallic interactions. The ionocovalent interactions come from charge transfer (ionic) and orbital overlapping (covalent) between Ti and O ions while the metallic character of TiO is due to both overlapping of d orbitals of Ti<sup>2+</sup> ions to produce a partly-filled band (Duffy 1990) and to s electrons.

Note that other monoxides like NiO, MnO, FeO and CoO also have a rocksalt structure but they do not conduct. When the above description for TiO is used for NiO, one finds that the overlapping of orbitals leads to a completely-filled band which does not allow conduction. However, the cohesive properties for the NiO compound are known to display a specific behaviour, as discussed in (Anisimov et al. 1991).



**Figure 6.10.** Experimental values of the work of adhesion versus the liquid surface energies for molten Al and Si on monocrystalline  $\text{Al}_2\text{O}_3$ . These values exceed significantly the values of the straight line for van der Waals bonded systems shown in Fig. 6.7.

**Table 6.5.** Contact angle and work of adhesion of Cu on different oxides at 1423K (Naidich 1981). Values of the gap energy  $E_g$  of oxides come from Duffy (1990).

Oxide	$\theta$ (deg)	$W_a$ (mJ/m <sup>2</sup> )	$E_g$ (eV)
$\text{SiO}_2$	128	500	10
$\text{MgO}$	133	410	7.3
$\text{TiO}_{1.14}$	82	1480	0
$\text{TiO}_{0.86}$	72	1700	0

It may be expected that at the interface between a metal and a metal-like compound, bonding would be at least partially metallic, leading to a high adhesion energy and better wetting than in metal/ionocovalent compound systems. This is confirmed by results in Table 6.5 for the wetting by Cu of oxides with different

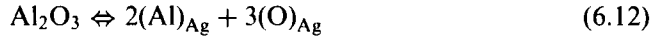


electrical conductivities, ranging from insulators (including predominantly ionic MgO and the more covalent SiO<sub>2</sub>) to metal-like TiO. Similar results have been obtained by Chabert (Chabert 1992) who found  $\theta = 122^\circ$  for Au on TiO<sub>2</sub> (which is of semi-conductor type with a gap energy  $E_g = 3$  eV (Duffy 1990)) and  $\theta = 88^\circ$  on TiO.

#### 6.4. EFFECTS OF OXYGEN

These effects will be described and discussed for non-reactive metal/oxide systems whose behaviour belongs to the plateau of the  $(\theta, X_O^I)$  curve of Figure 6.2. Conclusions will be drawn and then used to explain results for systems which belong to the reactive range, i.e., those for which the molar fraction of oxygen at the interface,  $X_O^I$ , is greater than  $10^{-5}$ .

Consider as an example the Ag/Al<sub>2</sub>O<sub>3</sub> couple. Dissolution of Al<sub>2</sub>O<sub>3</sub> into liquid Ag is described by the equation:



Ignoring any influence of the vapour phase (Figure 6.3), the equilibrium values of molar fractions of O and Al in Ag,  $X_O^I$  and  $X_{\text{Al}}^I$ , are easily calculated from equations (6.4) and (6.7). Taking  $\overline{\Delta G}_{\text{Al}(\text{Ag})}^{\text{xs},\infty}$  at 1273K to be  $-34$  kJ/mole (Hultgren et al. 1973),  $\Delta G_{\text{f}(\text{Al}_2\text{O}_3)}^0$  to be  $-1272$  kJ/mole (Chase et al. 1985) and  $\overline{\Delta G}_{\text{O}(\text{Ag})}^{\text{xs},\infty}$  to be  $41$  kJ/at.g O (Chang et al. 1988), values of  $X_O^I = 1.5 \times 10^{-11}$  and  $X_{\text{Al}}^I = 10^{-11}$  are obtained. These values are extremely low, justifying consideration of Ag/Al<sub>2</sub>O<sub>3</sub> as a non-reactive system (Figure 6.2). The corresponding value of  $P_{\text{O}_2}^I$  for the equilibrium

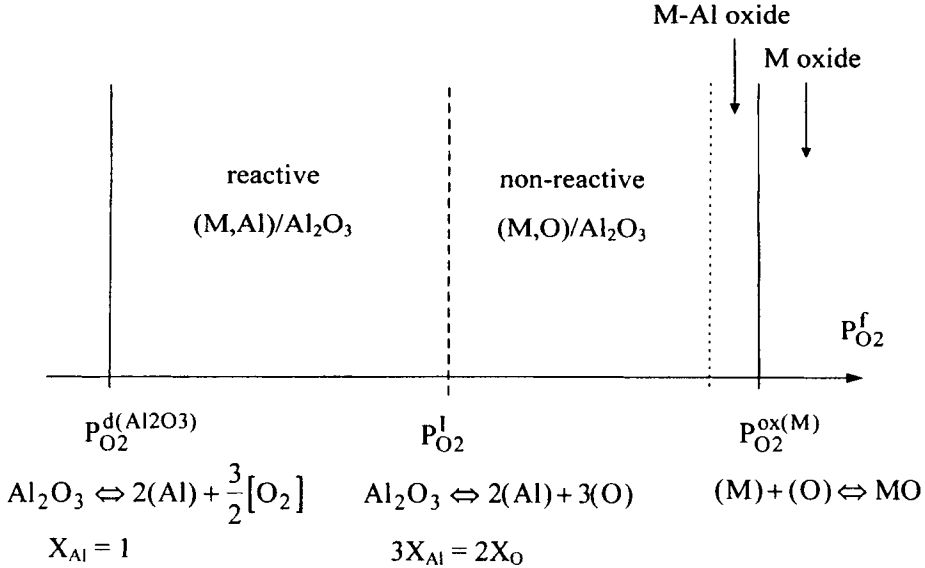


is given by:

$$(P_{O_2}^I)^{1/2} = a_O^I = \gamma_{O(Ag)}^\infty \cdot X_O^I \quad (6.14)$$

where  $a_O^I$  is the activity of oxygen, defined for a reference state of one atmosphere of pure  $O_2$ .

Now, let us take into account the influence of the vapour phase in the furnace, for which we assume the partial pressure of oxygen,  $P_{O_2}^f$ , to be fixed by an appropriate gas mixture ( $CO/CO_2$ ,  $H_2/H_2O$ ,  $He+O_2$ , etc). Equilibrium between a (Ag,O) solution and  $Al_2O_3$  exists for a range of  $P_{O_2}^f$  values, the highest value of which corresponds to the formation of the metal oxide,  $Ag_2O$ , at a partial pressure of oxygen  $P_{O_2}^{ox(Ag)}$ , (see Figure 6.11 taking  $M = Ag$ ), in accord with the reaction:



**Figure 6.11.** Range of partial pressure of oxygen in which a two-phase metal  $M/Al_2O_3$  equilibrium exists.  $P_{O_2}^I$  corresponds to the congruent dissolution of  $Al_2O_3$ .

Formation of oxide films on metal surfaces strongly affects wetting as will be seen in Section 6.4.2. The lowest  $P_{O_2}^f$  value at which there is equilibrium between (Ag,O) and  $Al_2O_3$  is  $P_{O_2}^{d(Al_2O_3)}$  below which there is decomposition of  $Al_2O_3$ , indicated by the superscript d (Figure 6.11).

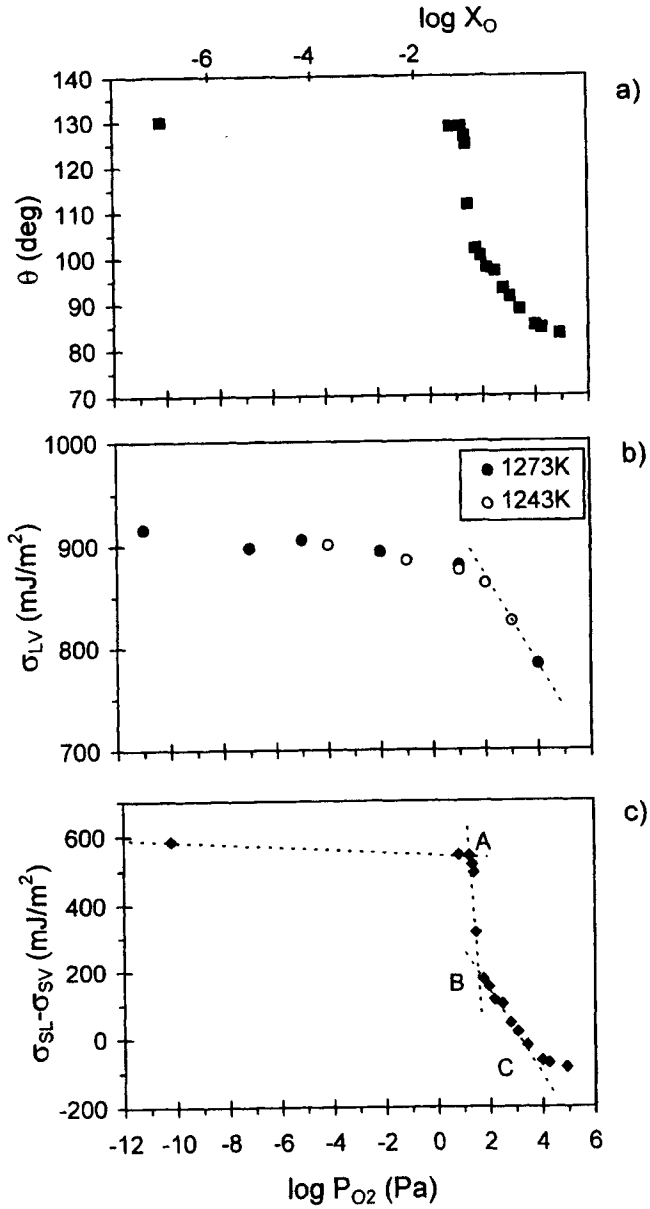
If  $P_{O_2}^f$  is higher than  $P_{O_2}^l$ , the concentration of dissolved oxygen in the bulk liquid will increase. According to equation (6.3), this will produce a decrease of the molar fraction of Al towards values even lower than  $X_{Al}^I = 10^{-11}$ . Clearly, for  $P_{O_2}^l < P_{O_2}^f < P_{O_2}^{ox(Ag)}$ , the only species dissolved in Ag is oxygen. In this range, the Ag/ $Al_2O_3$  system is still non-reactive and the only phenomenon which can modify wetting is adsorption of oxygen at the different surfaces of the system. For some metals, at  $P_{O_2}^f$  lower than but close to  $P_{O_2}^{ox(M)}$ , mixed oxides M-Al-O can form, modifying the nature of the interface (Figure 6.11). Typical examples are  $CuAlO_2$  (Gonzalez and Trumble 1996) and  $NiAl_2O_4$  (Mehrotra and Chaklader 1985).

If  $P_{O_2}^{d(Al_2O_3)} < P_{O_2}^f < P_{O_2}^l$ , dissolution of the substrate into the liquid metal will occur until  $X_{Al}$  satisfies equation (6.2) with  $a_O = (P_{O_2}^f)^{1/2}$ . The equilibrium contact angle will be that of a Ag-Al alloy on  $Al_2O_3$  (see Section 6.5 for the effect of alloying elements on wetting).

#### 6.4.1 Dissolved Oxygen

Now, we will describe in some detail experimental results and their interpretation for the Ag-O/ $Al_2O_3$  system in the range of  $P_{O_2}$  from  $10^{-12}$  to  $10^5$  Pa, in which no complications arise from interfacial reactions or from oxidation of Ag.

The contact angles of Ag on monocrystalline  $Al_2O_3$  are shown in Figure 6.12.a as a function of  $P_{O_2}^f$ . The change of  $\sigma_{LV}$  with  $P_{O_2}^f$  is presented in the same figure, as well as the change of work of immersion  $W_i$ , which is equal to  $(\sigma_{SL} - \sigma_{SV})$  and hence to  $-\sigma_{LV}\cos\theta$ . As  $P_{O_2}^f$  increases, the contact angle remains nearly constant in a wide range of  $P_{O_2}^f$ , then decreases sharply from  $130^\circ$  to about  $100^\circ$  and thereafter more slowly. A more regular decrease is observed for  $\sigma_{LV}$  values that can be analysed using the Gibbs adsorption equation (Defay et al. 1966):



**Figure 6.12.** The variation with partial pressure of oxygen or the corresponding molar fraction of oxygen in Ag of the a) contact angle at 1253K (Gallois 1980), b) surface energy of liquid Ag (Mehrotra and Chaklader 1985) and c) ( $\sigma_{SL} - \sigma_{SV}$ ) in the Ag/Al<sub>2</sub>O<sub>3</sub> system.

$$\frac{1}{RT} d(\sigma_{LV}) = -\Gamma_O^{Ag} d(\ln a_O) = -\frac{1}{2} \Gamma_O^{Ag} d(\ln P_{O_2}) \quad (6.16)$$

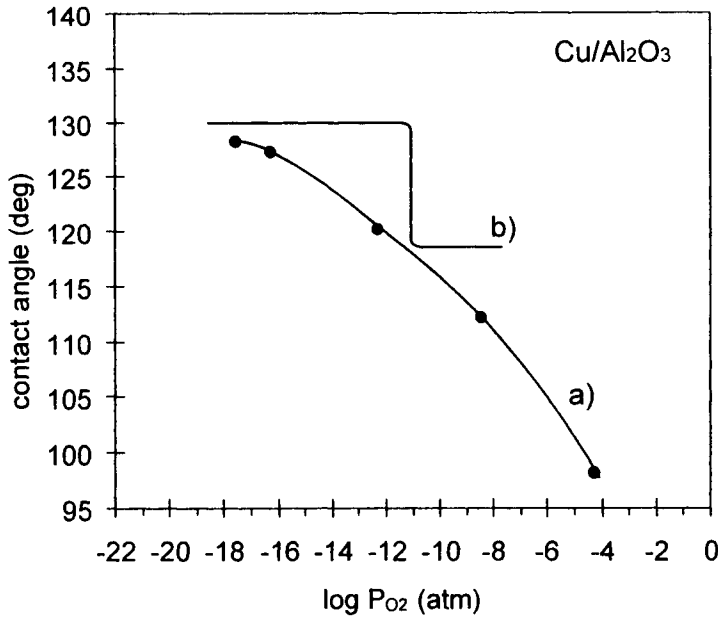
where  $\Gamma_O^{Ag}$  is the *relative adsorption* of oxygen with respect to Ag at the liquid surface. A positive value of  $\Gamma_O^{Ag}$  means that the surface is enriched in oxygen with respect to the bulk liquid, while a negative value of this quantity indicates the opposite situation.  $\Gamma_O^{Ag}$  is related to the *absolute adsorptions*  $\Gamma_O$  and  $\Gamma_{Ag}$  by the equation:

$$\Gamma_O^{Ag} = \Gamma_O - \Gamma_{Ag} \frac{X_O}{X_{Ag}} \quad (6.17)$$

For dilute solutions,  $X_O/X_{Ag}$  is much lower than unity, so that  $\Gamma_O^{Ag} \cong \Gamma_O$ . As it is usually assumed that only the first atomic layer of the liquid has a different composition from that of the bulk liquid,  $\Gamma_O$  is given by:

$$\Gamma_O^{Ag} \cong \Gamma_O = \frac{Y_O - X_O}{\Omega_m^O} \quad (6.18)$$

$Y_O$  is the mole fraction of oxygen within the surface monolayer and  $\Omega_m^O$  the area occupied by a mole of oxygen at the surface. Figure 6.12.b shows that the absolute value of the slope of  $\sigma_{LV}$ -log  $P_{O_2}^f$  curve is negligible for a large range of  $P_{O_2}$  values and then begins to increase and attains a nearly constant value. In this region, the surface is saturated in oxygen with a maximum value  $\Gamma_O$  of  $4 \times 10^{-6}$  mole/m<sup>2</sup> obtained from equations (6.16) and (6.18). Taking  $Y_O = 1$  at saturation and neglecting  $X_O$ , the atomic surface area of oxygen  $\omega_O$  ( $= \Omega_m^O/N_a$ ) is equal to about 40 Å<sup>2</sup>/atom. This is close to the area occupied by an oxygen ion on the (111) face of bulk Ag<sub>2</sub>O oxide (Gallois and Lupis 1981). In other words, although this oxide is not stable as a 3D compound at this temperature and value of  $P_{O_2}$  (much higher  $P_{O_2}$  values are needed for Ag<sub>2</sub>O to be stable at 1273K), a 2D “compound” would form *gradually* as a result of Gibbsian adsorption. Similar situations have been found for systems such as Cu-O and Fe-O (Gallois and Lupis 1981) (see also Section 4.1.1).

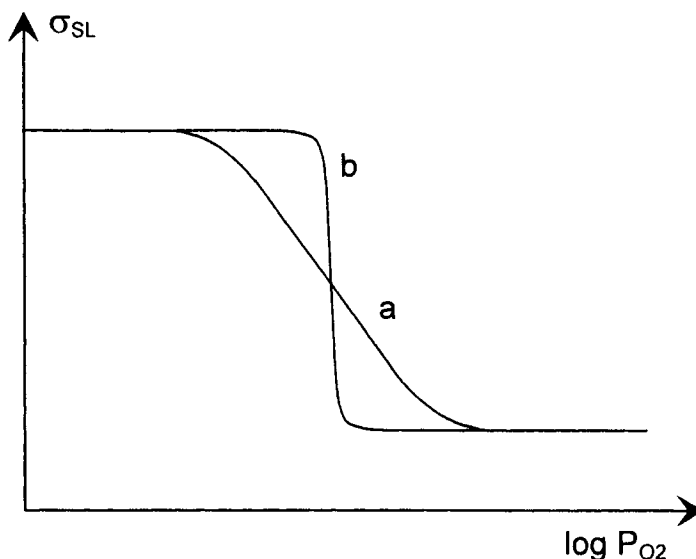


**Figure 6.13.** The variation of contact angle with oxygen partial pressure for Cu/Al<sub>2</sub>O<sub>3</sub> at 1100°C. a) (Owaby and Liu 1988), b) (Ghetta et al. 1996).

In Figure 6.12.c, the decrease of  $(\sigma_{SL} - \sigma_{SV})$  occurs in two stages, a first step A→B takes place at a nearly constant activity of oxygen, followed by a progressive decline B→C, similar to that for  $\sigma_{LV}$ . The B→C part of the curve may be explained by Gibbsian adsorption. Thus because it has been found that the surface energy of Al<sub>2</sub>O<sub>3</sub> does not depend on P<sub>O2</sub> in the range 10<sup>-15</sup>–10<sup>5</sup> Pa (Ghetta et al. 1996), the B→C decrease must result from a reduction of  $\sigma_{SL}$ . Gibbsian adsorption cannot explain the A→B part of the curve since such a rapid decrease causes equations (6.16) to (6.18) to predict an extremely low value of the atomic surface area of oxygen, that is without physical meaning. Because this decrease takes place at a nearly constant P<sub>O2</sub> value, it may be considered instead as equivalent to a *first-order* 2D phase transition. For instance, it has been suggested that the complex oxide AgAlO<sub>2</sub>, which is unstable as a bulk compound at low P<sub>O2</sub>, forms as a 2D structure at the Ag/Al<sub>2</sub>O<sub>3</sub> interface (Chaklader et al. 1981).

At present, available experimental results do not allow precise definitions of  $(\theta - \log P_{O_2}^f)$  isotherms. For instance, one study of the couple Cu/Al<sub>2</sub>O<sub>3</sub> (Figure 6.13) (Owaby and Liu 1988) found behaviour consistent with Gibbsian adsorption (curve a in Figure 6.14) and another one (Ghetta et al. 1996) behaviour indicative

of a 2D phase transition (curve b in Figure 6.14). These divergences underline the difficulties of performing wetting experiments, using stable and controlled  $P_{O_2}$  values in the gas mixture. Moreover, because this type of experiment usually lasts several hours or tens of hours, segregation at the interface of impurities from the substrate (Ca, Mg, Si, etc) can occur and affect results (Chabert 1992).



**Figure 6.14.** Possible isotherms of liquid metal/oxide interfacial energy in the non-reactive range when enrichment of the interface in oxygen occurs by a) Gibbsian adsorption or b) 2D phase transition.

Despite these difficulties, except for the noble metals Au, Pt and Ir on oxides, for which  $P_{O_2}$  has little or no effect on contact angles, published data (Tables 6.6 and 6.7) show that oxygen decreases both  $\sigma_{LV}$  and  $\sigma_{SL}$ . This effect is higher for  $\sigma_{SL}$  than for  $\sigma_{LV}$ , causing a decrease in the contact angle of several degrees or tens of degrees (Figure 6.15). An attempt to explain these effects was made by Naidich (1981) using the oxygen-metal cluster model already cited in Section 6.3. There is no direct evidence on the formation and lifetime of such clusters. However, analysis of thermodynamic data concerning interaction of dissolved oxygen with metallic atoms in bulk liquid provides strong arguments in favour of their existence. These interactions are usually quantified by the *activity coefficient of oxygen* at infinite dilution in the melt,  $\gamma_O^\infty$ . Because it is usually easier to calculate variations of a thermodynamic quantity than its absolute value models have been proposed to

predict the variation of  $\gamma_{\text{O}}^{\infty}$  in a A-B binary alloy when the alloy composition changes from pure A to pure B (Belton and Tankins 1965, Jacob and Alcock 1972, Chang et al. 1988). Although differences exist among these models, they all assume that strong metal-oxygen bonds distort the distribution of electrons around the metal atoms. In the framework of a simple nearest-neighbour interaction model (see Section 1.1), such a distortion modifies the metal-metal bonds around the oxygen, the energy of which is only a fraction  $(1 - \alpha)$  of that of normal metal-metal bonds. In other words, a partial rupture of the metallic bond occurs in the vicinity of oxygen.

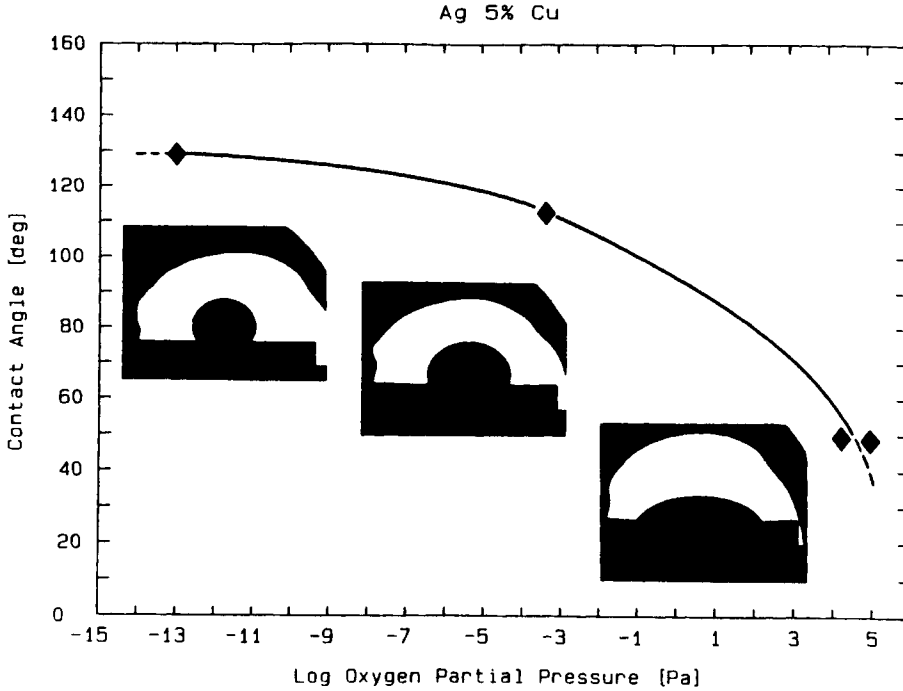
**Table 6.6.** Metal/oxide systems for which determinations of contact angle as a function of  $P_{\text{O}_2}$  exist.

System	Reference
Cu/ $\text{Al}_2\text{O}_3$	(Chaklader et al. 1981) (Ownby and Liu 1988)
Ag/ $\text{Al}_2\text{O}_3$	(Ghetta et al. 1996) (Gallois 1980) (Chatain et al. 1994) (Chaklader et al. 1981)
Au/ $\text{Al}_2\text{O}_3$	(Ghetta et al. 1996)
Ni/ $\text{Al}_2\text{O}_3$	(Nogi et al. 1992b)
Fe/ $\text{Al}_2\text{O}_3$	(Nakashima et al. 1992)
Pb/ $\text{SiO}_2$	(Sangiorgi et al. 1995)
Ag/ $\text{SiO}_2$	(Sangiorgi et al. 1982)

**Table 6.7.** Wetting of oxides by Pt-group metals in air showing that the contact angle values for Ag and Rh are much lower than the values of 120-130° observed in inert gas (Grigorenko et al. 1995).

Metal	T (°C)	$\theta$ (deg) on MgO	$\theta$ (deg) on $\text{ZrO}_2$	$\theta$ (deg) on $\text{Al}_2\text{O}_3$
Ag	1100	$83 \pm 4$	$73 \pm 8$	$84 \pm 3$
Rh	2100	$97 \pm 4$	$98 \pm 4$	—
Pt	1900	$103 \pm 5$	$118 \pm 5$	$139 \pm 6$
Au	1200	$119 \pm 2$	$125 \pm 4$	$136 \pm 6$
Ir	2500	$138 \pm 4$	—	—





**Figure 6.15.** Effect of the oxygen partial pressure on the wetting of a sapphire substrate by a Ag-5 at.% Cu alloy at 1373K. Results from (Chatain et al. 1993). Photographs kindly provided by Muolo of ICFAM-CNR (Genova).

Consider an A-B lattice with a coordination number  $Z$  and, inside this lattice, an oxygen atom forming a total of  $n$  bonds with metal atoms A or B. The atomic fraction of B atoms around O,  $Y_B$ , is given as a function of atomic fraction of B in the bulk alloy,  $X_B$ , by an equation obtained from the quasichemical treatment of solutions (Jacob and Alcock 1972):

$$\frac{Y_B}{1 - Y_B} = \frac{X_B}{1 - X_B} \exp\left(\frac{-\Delta G_{\text{ex}}^{\text{xs}}}{RT}\right) \quad (6.19)$$

where  $\Delta G_{\text{ex}}^{\text{xs}}$  is the excess Gibbs energy change that occurs when a A-O pair is changed to a B-O pair by *exchanging* a A atom in the coordination shell of the oxygen atom with a B atom in the melt bulk. Calculations lead to the equations:

$$\frac{Y_B}{1 - Y_B} = \frac{X_B}{1 - X_B} \left( \frac{\gamma_{O(A)}^\infty}{\gamma_{O(B)}^\infty} \right)^{1/n} \left( \frac{\gamma_B}{\gamma_A} \right)^\alpha \quad (6.20)$$

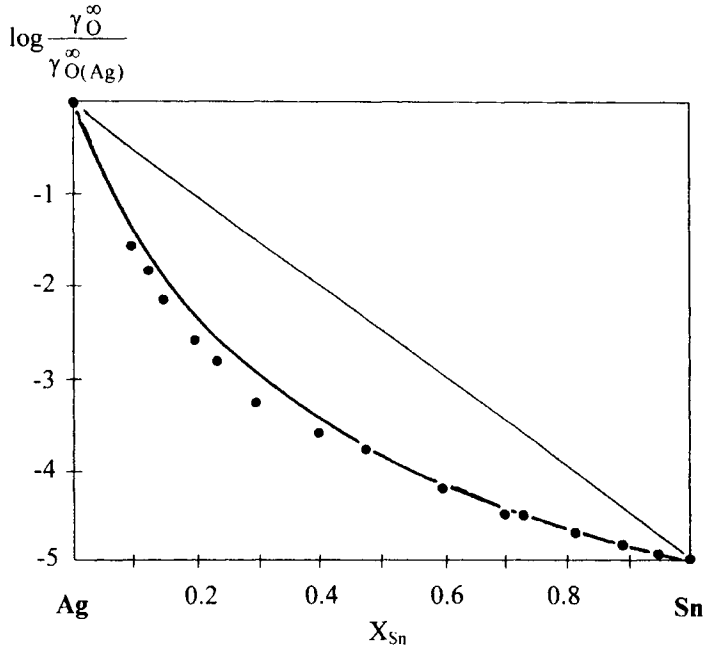
$$(\gamma_O^\infty)^{-1/n} = X_B(\gamma_B)^\alpha (\gamma_{O(B)}^\infty)^{-1/n} + (1 - X_B)(\gamma_A)^\alpha (\gamma_{O(A)}^\infty)^{-1/n} \quad (6.21)$$

This model allows calculation of the activity coefficient of oxygen at infinite dilution in a binary A-B alloy,  $\gamma_O^\infty$ , from known values of the activity coefficient of oxygen at infinite dilution in pure A,  $\gamma_{O(A)}^\infty$ , and pure B,  $\gamma_{O(B)}^\infty$ , and the activity coefficients of A and B,  $\gamma_A$  and  $\gamma_B$ , in the A-B alloy. This model provides a satisfactory prediction of  $\gamma_O^\infty$  in several binary A-B alloys taking  $n = 4$  and  $\alpha = 1/2$  (Jacob and Alcock 1972). An example is given in Figure 6.16 for the Ag-Sn couple in which  $\gamma_O^\infty$  differs by five orders of magnitude between pure Ag and pure Sn. It can be seen that the first additions of Sn to Ag produce a strong decrease of  $\gamma_O^\infty$ . This behaviour results from the fact that even for small  $X_{Sn}$  values,  $Y_{Sn}$  is high (the calculated value of  $(Y_{Sn}/X_{Sn})_{X_{Sn} \rightarrow 0}$  is 20), so oxygen clusters are enriched in Sn atoms. Conversely, the first additions of Ag to Sn have relatively weak effects, so that Ag atoms have a negligible tendency to segregate around O atoms.

Henry's law ( $\gamma_B$  nearly constant and equal to  $\gamma_B^\infty$ ) holds for A-B alloys dilute in B. For this range of composition, another quantity can be introduced which takes into account interactions between dissolved O and dissolved B in an A matrix. This is the Wagner's first-order interaction parameter,  $\epsilon_O^B$ , defined by an equation in which high-order terms are neglected:

$$\ln \gamma_O = \ln \gamma_{O(A)}^\infty + \epsilon_O^B X_B + \dots \quad (6.22)$$

In the quasichemical model of Jacob and Alcock,  $\epsilon_O^B$  is given by:



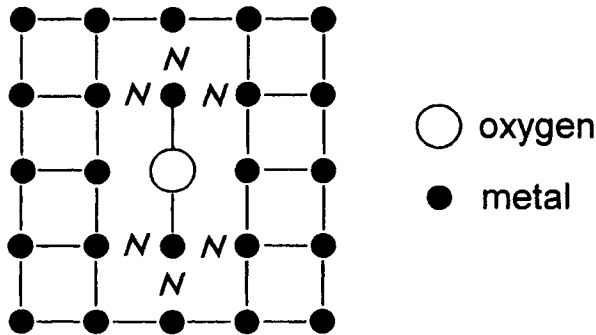
**Figure 6.16.** Effect of alloy composition on the activity coefficient of oxygen in Ag-Sn alloys at 1473K. Circles: experimental results, full line: values calculated according to the quasichemical model of Jacob and Alcock (1972) [19] (equation (6.21) with  $n = 4$  and  $\alpha = 1/2$ ).

$$\varepsilon_O^B = -n \left[ \left( \frac{\gamma_{O(A)}^\infty}{\gamma_{O(B)}^\infty} \right)^{1/n} (\gamma_B^\infty)^\alpha - 1 \right] \quad (6.23)$$

A strong solute-solute interaction between O and B atoms in an A matrix results in a very negative value of  $\varepsilon_O^B$  and in a strong decrease of the activity coefficient of oxygen in the alloy. For instance, for Ag-Sn alloys dilute in Sn (Figure 6.16),  $\varepsilon_O^{Sn} = -50$ . It must be emphasized, however, that values of  $\varepsilon_O^B$  calculated by equation (6.23) are very sensitive to values of the model parameters,  $\alpha$  and  $n$ . Errors in calculated values of  $\varepsilon_O^B$  can be such that they must be considered at best as semi-quantitative estimates. However, equation (6.23) is interesting because it identifies the parameters determining the sign and the absolute value of  $\varepsilon_O^B$ . Thus, the favourable conditions for  $\varepsilon_O^B \ll 0$  are (i) a strong O-B interaction in pure B that

yields a low value of  $\gamma_{O(B)}^\infty$ , (ii) a weak O-A interaction in pure A that results in a high value of  $\gamma_{O(A)}^\infty$  and (iii) a weak A-B interaction so the partial enthalpy of mixing of B in A,  $\Delta H_{B(A)}$ , is positive or close to zero and  $\gamma_B$  has a high value. All these conditions are satisfied for instance for binary Cu-B alloys with B = Fe, Cr, Ti resulting in very negative values of  $\epsilon_O^B$  ( $\epsilon_O^{Fe} = -540$  (Chang et al. 1988),  $\epsilon_O^{Cr} = -2800$  (Kritsalis et al. 1990),  $\epsilon_O^{Ti} = -10^4$  (Kritsalis et al. 1991)). For such values of  $\epsilon_O^B$ , the calculated values of  $(Y_B/X_B)_{X_B \rightarrow 0} (= 1 - \epsilon_O^B/n)$  can attain very high values, from several  $10^2$  to several  $10^3$ , meaning that for Cu alloys containing a few atomic percent of Fe, Cr or Ti, dissolved oxygen is in the form of O-B clusters rather than O-Cu clusters.

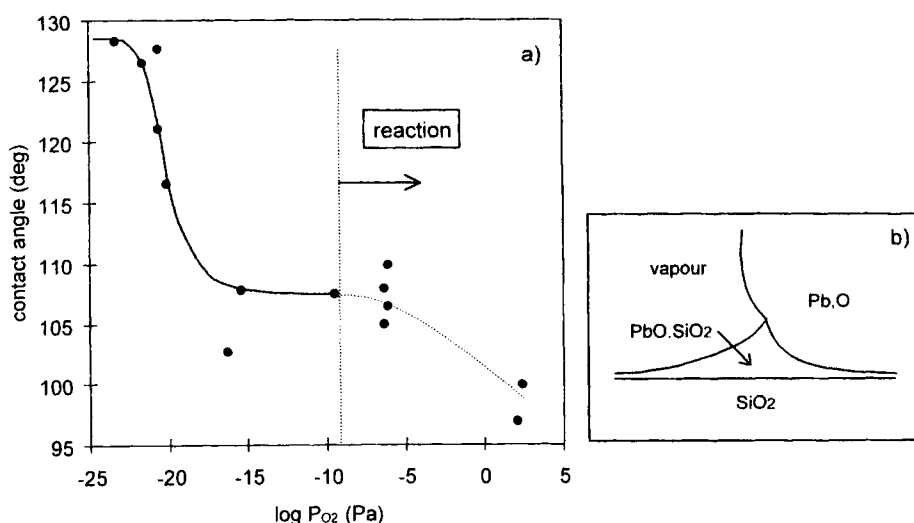
This quasichemical model is compatible with the Naidich hypothesis of oxygen clusters and allows a rough description of their structure and energy to be given: oxygen atom is surrounded by four metal atoms ( $n = 4$ ) and the charge transfer from these atoms to oxygen halves the strength of the metal-metal bonds around oxygen ( $\alpha = 1/2$ ), Figure 6.17.



**Figure 6.17.** Schematic illustration of an oxygen cluster according to Jacob and Alcock (1972). For 2D representation the number of metal atoms bonded to oxygen,  $n$ , is 2 and the coordination in bulk metal is 4. The symbol  $N$  means partial rupture of the metal-metal bond.

Consider now the influence of oxygen clusters on metal/vapour and metal/oxide interfacial energies. Because oxygen clusters cause a major perturbation of the structure and energy of the bulk metal, they are expected to segregate at 2D defects such as surfaces and interfaces, where the perturbation can be partially relaxed. This may explain the strong tendency for oxygen adsorption at both solid

metal/vapour and liquid metal/vapour surfaces, to decrease the corresponding surface energies. The adsorption energy at the metal/oxide interface i.e., the change in energy of the system when an oxygen atom segregates at the interface from the bulk, will be even higher in absolute value because of the ionic interactions between the clusters and the oxide surface (Figure 6.9.a). Thus, the reduction of  $\sigma_{LV}$  due to oxygen adsorption will be lower than the reduction of  $\sigma_{SL}$ , resulting in an increase of the work of adhesion,  $W_a = \sigma_{SV} + \sigma_{LV} - \sigma_{SL}$ , and a decrease of  $\theta$ , since  $\cos\theta = W_a/\sigma_{LV} - 1$ .

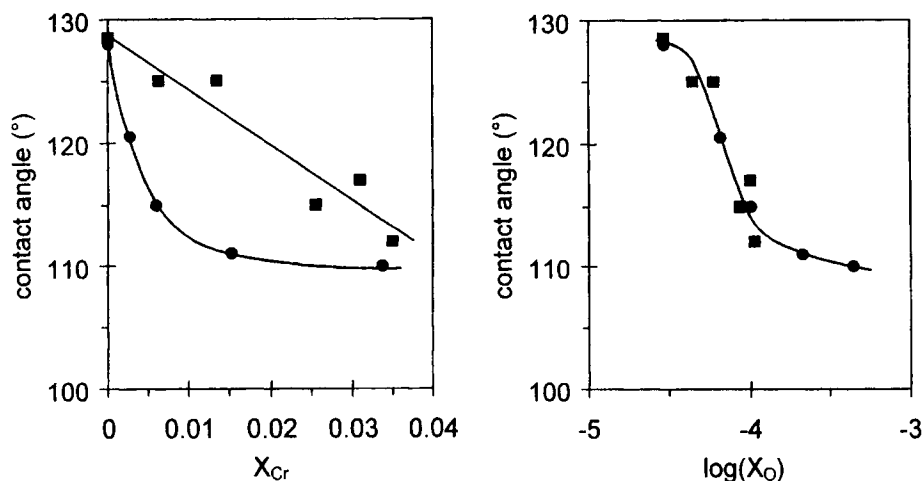


**Figure 6.18.** a) Contact angle of the Pb/SiO<sub>2</sub> system plotted as a function of  $\log P_{O_2}$  at 1050K. b) At high  $P_{O_2}$ , formation of a liquid interfacial reaction product (PbO·SiO<sub>2</sub>) occurs so the apparent contact angle is not a Young contact angle. From work reported in (Sangiorgi et al. 1995).

A complex oxide is formed at the interface in certain systems at high  $P_{O_2}$  values by reaction between the liquid metal and the oxide substrate (see Figure 6.11). An example is the Pb/SiO<sub>2</sub> system (Figure 6.18). With increasing  $P_{O_2}$ , the contact angle decreases owing to adsorption of oxygen at the Pb/SiO<sub>2</sub> interface. At  $P_{O_2} > 10^{-10}$  Pa, a reaction occurs to form *liquid* PbO-SiO<sub>2</sub> oxide at the interface that wets the SiO<sub>2</sub> surface such that the wetting of Pb occurs on a liquid PbO-SiO<sub>2</sub> layer rather than on SiO<sub>2</sub>. The configuration at the PbO-SiO<sub>2</sub>/Pb/vapour triple

line deviates strongly from that assumed by Young (Figure 6.18.b) and obeys Smith's equation (1.30). As a result, the macroscopic contact angles in this type of system are not Young contact angles.

In the studies cited in Table 6.6, the oxygen affecting surface and interface properties of metal/oxide systems comes from the vapour phase. "Pure" metals and alloys contain oxygen as an impurity, but its concentration in many cases is sufficient to affect wettability. An example is given in Figure 6.19.a, in which the contact angle of Cu-Cr alloys is represented as a function of the molar fraction of Cr for two series of experiments performed using Cr with different oxygen contents. Significant differences were observed in  $\theta$  that are mainly due to oxygen. Thus Figure 6.19.b shows that all  $\theta$  values belong to the same curve when plotted against  $\log X_O$  whatever the type of Cr used. In this example, the improved wettability of the Cu/ $\text{Al}_2\text{O}_3$  system by Cr additions in Cu is not an intrinsic effect of Cr, but is due to adsorption at the Cu-Cr/ $\text{Al}_2\text{O}_3$  interface of oxygen fixed by Cr in the melt. Similar effects may be observed in other alloys consisting of a noble metal matrix and an alloying element with a greater affinity for oxygen, for example the Au-Ni/ $\text{Al}_2\text{O}_3$  (Rivollet et al. 1987) and Au-Si/ $\text{Al}_2\text{O}_3$  (Drevet et al. 1990) systems.



**Figure 6.19.** Contact angles of Cu-Cr alloys on monocrystalline  $\text{Al}_2\text{O}_3$  at 1423K plotted as a function of molar fraction of Cr (left) and molar fraction of oxygen (right) in the alloy. Circles : Cr containing  $(3700 \pm 500)$  ppm of oxygen. Squares: Cr containing  $(700 \pm 150)$  ppm of oxygen. From (Kritsalis et al. 1990) [20].

Conclusions and concepts developed for non-reactive (M, O)/oxide systems can be used to explain wetting observed for reactive metal/oxide combinations, i.e., for systems with  $X_O^I > 10^{-5}$  (Figures 6.2 and 6.3). A typical example is Cu/NiO for which  $\theta$  is  $68^\circ$  at 1473K (Naidich 1972). Using the data in Table 6.8 relevant to this system and the value  $\epsilon_O^{Ni} \approx -7$  (Chang et al. 1988), equilibrium thermodynamic calculations lead to a molar fraction of oxygen coming from the dissolution of NiO ( $X_O^I = X_{Ni}^I$ ) of  $1.5 \times 10^{-2}$ . This value of  $X_O^I$  is not high enough to produce precipitation of the copper oxide  $Cu_2O$  which requires that  $X_O \approx 4 \times 10^{-2}$ . Thus, the only possible effect of interfacial reaction on wetting in the Cu/NiO system is the adsorption of dissolved oxygen at the metal/oxide interface. Wettability in systems like Sn/ $Fe_3O_4$  ( $\epsilon_O^{Fe} \approx -50$  (Chang et al. 1988)), Fe/ $Cr_2O_3$  ( $\epsilon_O^{Cr} \approx -10$  (Heinz et al. 1989)) or Cu/ $Fe_3O_4$  ( $\epsilon_O^{Fe} \approx -540$  (Chang et al. 1988)) can be interpreted in the same way. For the last system, since  $\epsilon_O^{Fe} \ll 0$ , adsorption of oxygen would occur as O-Fe clusters rather than O-Cu clusters.

**Table 6.8.** Thermochemical data at 1473K relative to the Cu/NiO system (Eustathopoulos and Drevet 1994).

Reaction	Gibbs energy (kJ)
$(Ni) + \frac{1}{2} [O_2] \rightleftharpoons (NiO)$	$\Delta G_f^0 = -111$
$2(Cu) + \frac{1}{2} [O_2] \rightleftharpoons (Cu_2O)$	$\Delta G_f^0 = -60$
$(Ni) \rightleftharpoons (Ni)_{Cu}$	$\overline{\Delta G}_{Ni(Cu)}^{xs, \infty} = +12.5$
$\frac{1}{2} [O_2] \rightleftharpoons (O)_{Cu}$	$\overline{\Delta G}_{O(Cu)}^{xs, \infty} = -19$

For the systems with  $X_O^I > 10^{-5}$ , variations in the concentration of dissolved oxygen and the dissolved metal of the oxide, that are caused by varying  $P_{O_2}$  in the vapour phase using a gas mixture with a controlled  $P_{O_2}$ , are expected to modify  $\theta$ . An example is Ni/ $Al_2O_3$  (Nogi et al. 1992b) at 1873K for which the experimental  $\theta$ -oxygen content curve passes through a maximum (Figure 6.4). The value of  $\theta$  at the maximum ( $\theta_{max} \cong 123^\circ$ ) is close to that predicted for a non-reactive Ni/ $Al_2O_3$

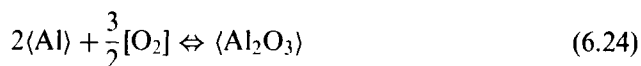
interface i.e., an interface with mainly van der Waals interactions. The decrease in  $\theta$  to the right of the maximum can be attributed to adsorption of oxygen as O-Ni clusters; the decrease to the left can be explained by the adsorption of Al (very small additions of Al in a non-reactive metal can significantly improve wetting on  $\text{Al}_2\text{O}_3$  as shown in Figure 6.25). Similar curves with a maximum  $\theta$  have been obtained by several workers for Fe/ $\text{Al}_2\text{O}_3$  couples (Nakashima et al. 1992).

We saw in Section 4.1.1 that elements other than O that develop strong interactions with a liquid metal (such as S, Se and Te in molten Fe) decrease the liquid surface energy of the metal quite markedly. The effect of these elements on the contact angle and the work of adhesion of Fe on  $\text{Al}_2\text{O}_3$  has been studied by Ogino et al. (1983) using well-polished sintered  $\text{Al}_2\text{O}_3$  substrates. They found that S, Se and Te adsorb at Fe/ $\text{Al}_2\text{O}_3$  interface but that the reduction in  $\sigma_{\text{SL}}$  is much lower than that in  $\sigma_{\text{LV}}$ . As a result, the contact angle increases with the additions of these elements and contact angles as large as  $160^\circ$  were observed for concentrations close to 0.05 at. %.

#### 6.4.2 Oxide films at a metal surface

For  $P_{\text{O}_2}^{\text{f}} > P_{\text{O}_2}^{\text{ox(M)}}$  (see Figure 6.11), an oxide skin is formed at the metal *surface*, inhibiting the movement of the triple line. Because this phenomenon is very important in the processing of interfaces in multimaterials or in brazed-joint fabrication, it will be discussed in detail in this sub-section.

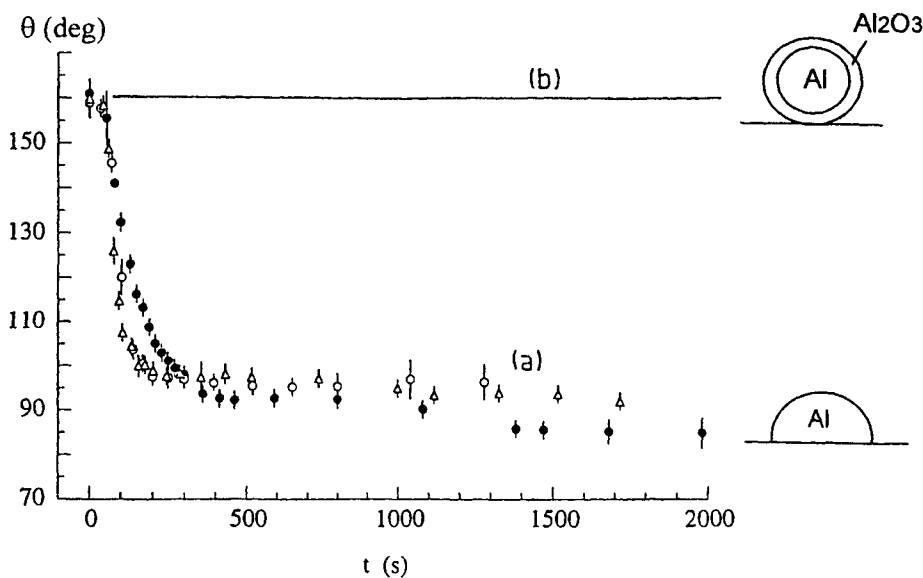
When thick oxide films are formed on a sessile drop, oxidation is evident because at melting, the surface of the liquid is not smooth. However, thin oxide skins of up to a few tens of nanometers are easily deformable, allowing a smooth surface to be formed. However, even when very thin, skins do not allow metal/substrate interface to be established and as a result the apparent contact angles are as high as  $160^\circ$ . A classical example is pure Al on  $\text{Al}_2\text{O}_3$  (Figure 6.20) (Brennan and Pask 1968, Eustathopoulos et al. 1974, Weirauch 1988). At room temperature, Al is instantaneously covered by an oxide layer about 2 nm thick formed by the reaction:



Thus, the surface of liquid Al is covered by a film of  $\text{Al}_2\text{O}_3$  on melting and this results in an apparent contact angle of about  $160^\circ$  (Figure 6.20). On heating to  $827^\circ\text{C}$ , two different effects can be observed that depend on the value of  $P_{\text{O}_2}$  in the furnace. In a metallic chamber furnace with a low  $P_{\text{O}_2}$ , a decrease of the

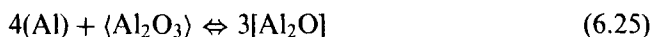


contact angle towards a value close to  $90^\circ$  occurs in a few hundreds of seconds. In an alumina chamber furnace with a relatively high  $P_{O_2}$ , no decrease of contact angle is observed even after several hours at temperature. To obtain a curve similar to that shown as (a) in Figure 6.20, a further increase of temperature is needed, for example up to  $1000^\circ\text{C}$ .



**Figure 6.20.** Experimental contact angles in high vacuum versus time of Al on  $\text{Al}_2\text{O}_3$  substrates at  $827^\circ\text{C}$  in (a) a metal chamber furnace (low  $P_{O_2}$ ) and in (b) an alumina chamber furnace (high  $P_{O_2}$ ). From (Landry et al. 1998) [17].

Deoxidation of Al by *dissociation* of  $\text{Al}_2\text{O}_3$  according to reaction (6.24) needs extremely low values of  $P_{O_2}$  in the furnace (for instance  $10^{-43}$  Pa at the melting temperature of Al and  $10^{-35}$  Pa at  $900^\circ\text{C}$ ). Such low  $P_{O_2}$  values are not easily achieved in a furnace in which  $P_{O_2}$  is usually in the range  $10^{-15}$ – $10^{-5}$  Pa. Therefore, deoxidation of Al observed under high vacuum does not occur by dissociation of  $\text{Al}_2\text{O}_3$  and has been attributed to the reduction of the oxide film by liquid Al to form volatile  $\text{Al}_2\text{O}$  by the reaction (Laurent et al. 1988, Castello et al. 1994):



The condition for such deoxidation is that the total flow of oxygen,  $\Phi_O$ , leaving the drop surface is higher than the flow of oxygen impinging on the drop. This egress of O is proportional to  $P_{Al_2O}$  but the ingress is proportional to the partial pressure of  $O_2$  in the furnace,  $P_{O_2}^f$ . The maximum  $P_{Al_2O}$  value is the value corresponding to the equilibrium of three phases: liquid (Al), solid ( $Al_2O_3$ ) and vapour (equation (6.25)). This equilibrium can be established if the oxide film on the Al drop surface is disrupted as shown in Figure 6.21.a. The value of  $P_{Al_2O}^{eq}$  can be easily calculated from thermodynamic data (Chase et al. 1985) and increases strongly with temperature (Figure 6.22). Accordingly, for a fixed value of  $P_{O_2}^f$ , there is a threshold value of temperature,  $T^*$ , below which the oxide film thickens and above which it is eroded to deoxidise the surface (Figure 6.22).

If the operating conditions ( $T$ ,  $P_{O_2}^f$ ) permit deoxidation, this will occur at a time that depends mainly on the temperature (because  $P_{Al_2O}^{eq} = f(T)$ ) and the thickness of the oxide skin. This thickness increases from its initial value  $e_0$  during heating between room temperature and  $T^*$  by an amount that is strongly dependent on  $P_{O_2}^f$  (Figure 6.23).

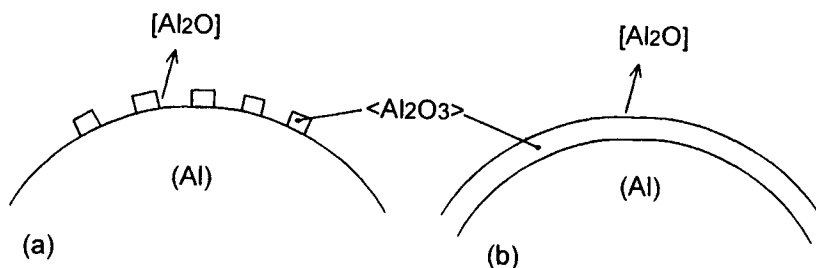
When, at a temperature  $T$ , the condition  $P_{Al_2O}^{eq} \gg P_{O_2}^f$  is fulfilled, the impinging flow of oxygen can be neglected. Then, the deoxidation time  $t_d$  for a *monolayer* of oxide is simply given by (Laurent et al. 1988) (Figure 6.24):

$$t_d = \frac{1}{\Omega_m \Phi_O} \quad (6.26)$$

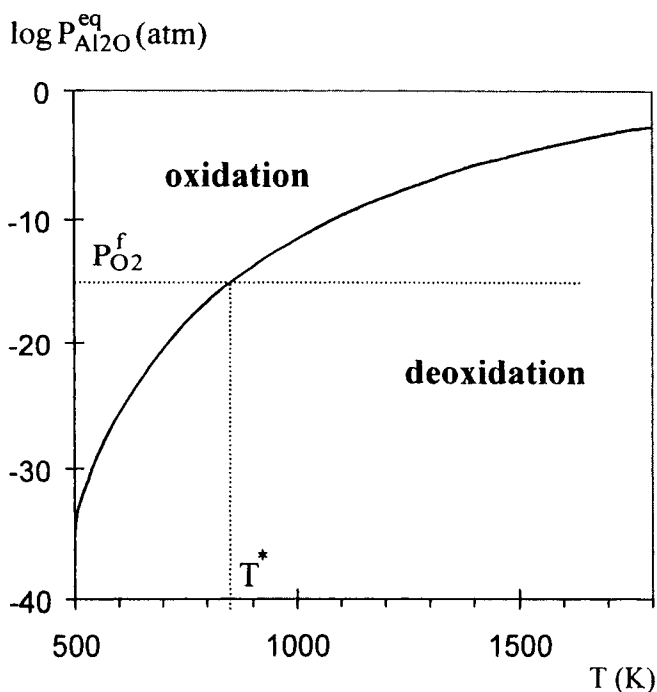
$\Omega_m$  is the molar surface area of the oxide and the flow of oxygen leaving the drop surface,  $\Phi_O$ , is given by:

$$\Phi_O = \frac{\alpha_{Al_2O} P_{Al_2O}^{eq}}{(2\pi m_{Al_2O} k T)^{1/2}} \quad (6.27)$$

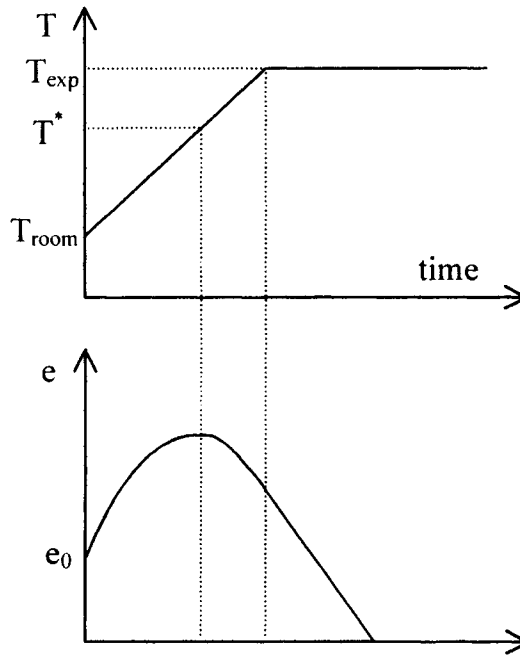
where  $k$  is the Boltzmann constant,  $m_{Al_2O}$  is the mass of a molecule of  $Al_2O$  and  $\alpha_{Al_2O}$  is the “evaporation coefficient” which takes into account a possible departure from equilibrium (6.25) at the surface of the oxide film on the drop ( $\alpha_{Al_2O} < 1$ ). This mechanism has also been used with success to explain deoxidation of other pure molten metals as Si (Drevet et al. 1990) and U (Tournier et al. 1996).



**Figure 6.21.** The model of Laurent et al. (1988) for deoxidation of an Al drop under high vacuum is based on the assumption that deoxidation is controlled by the rate of evaporation of a volatile oxide formed according to reaction (6.25). This is justified for disrupted oxide films (a) or for continuous but very thin films (b), through which diffusion is very fast, but not for thick oxide films.



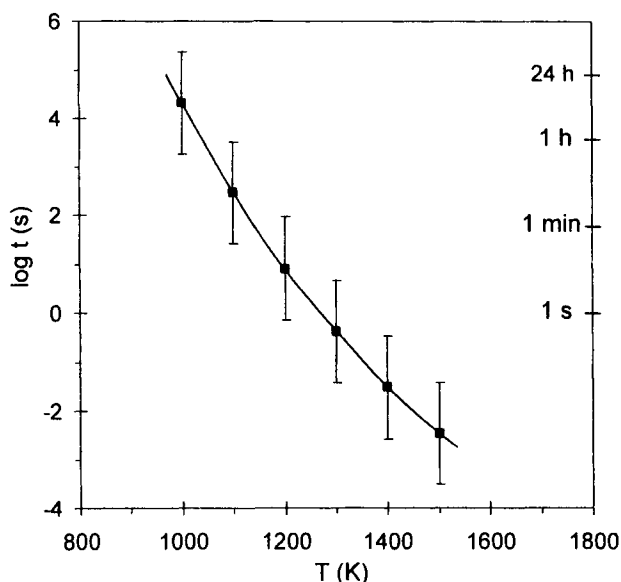
**Figure 6.22.** Equilibrium partial pressure of  $\text{Al}_2\text{O}$ , derived from equation (6.25), plotted as a function of temperature. For a given value of the partial pressure of oxygen in the furnace,  $P_{\text{O}_2}^f$ , there is a threshold temperature,  $T^*$ , below which the oxide film thickens and above which it is eroded.



**Figure 6.23.** Schematic variation of thickness,  $e$ , of an oxide film on a metallic drop during a thermal cycle from room temperature to the experimental temperature.

In such calculations, the diffusion through a continuous oxide layer (Figure 6.21.b) has been neglected. This may be a good approximation for films a few monolayers thick but for thicker films, diffusion may control the overall deoxidation rate such that the deoxidation time is much higher than the product of  $t_d$  by the number of monolayers of the film (Chatillon et al. 1996).

For a binary alloy containing an oxidable metal such as Al or Si, the partial pressure of volatile suboxide ( $\text{Al}_2\text{O}$  or  $\text{SiO}$ ) depends not only on temperature but also on the activity of the oxidable element in the alloy. Thus, for a Cu-Al alloy at constant temperature,  $P_{\text{Al}_2\text{O}}^{\text{eq}}$  (i.e. roughly  $1/t_d$ ) is proportional to  $a_{\text{Al}}^{4/3}$  according to reaction (6.25). As a result, under high vacuum, it is much easier to deoxidise Cu-Al (Li et al. 1987–88) or Au-Si (Drevet et al. 1990) alloys that are rich in Al or Si. This straightforwardly explains the apparent contact angle maxima observed by many authors for alloys diluted in the oxidable element (Figure 6.25): for these alloys, the oxidable element is present in a concentration sufficient to produce oxidation at  $T < T^*$ , but not enough to produce deoxidation in a reasonable time at  $T > T^*$ . When experiments are performed in a metallic furnace with a very low  $P_{\text{O}_2}$



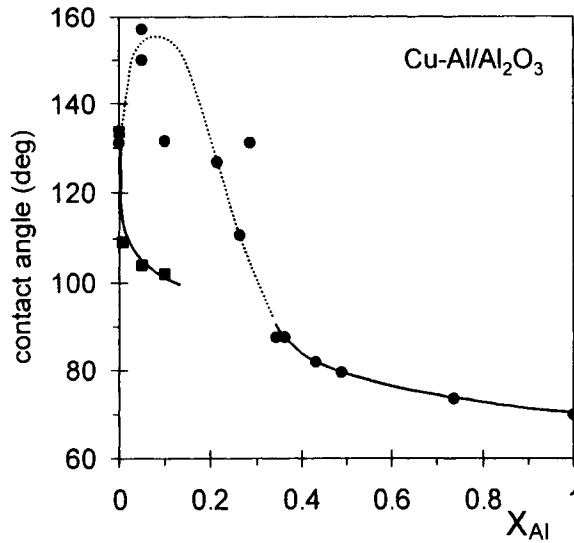
**Figure 6.24.** Times required for the disappearance of an oxide monolayer from the surface of liquid Al at different temperatures. The error bars are due to the uncertainty of the Gibbs energy of reaction (6.25). From (Laurent et al. 1988) [21].

using the dispensed drop technique (see Figure 3.7.c), no oxidation occurs and the maximum in the  $\theta$ -composition curve is suppressed as shown in Figure 6.25.

When experiments are performed in a static neutral gas atmosphere, deoxidation depends on diffusion of volatile species into the gas. For the same temperature and  $P_{O_2}$  values, deoxidation takes longer in such atmospheres than in a high vacuum but some acceleration can be achieved by using dynamic conditions i.e., gas flow (Ricci et al. 1994).

The disappearance of an oxide film may be achieved not only by reduction by the liquid metal but also by mechanical disruption or dissolution in the liquid. For instance, mechanical disruption can occur when the liquid drop is dispensed onto the substrate surface through a small hole in a tube end (Figure 3.7.c). When this technique is used for Al on  $Al_2O_3$ , the deoxidation stage is suppressed and a contact angle close to  $80^\circ$  is rapidly achieved (Landry et al. 1996).

In the case of liquid Al, the solubility of oxygen is too low for a dissolution process to be effective. However, for other metals like Sn, it may be the principal mechanism. The variation in contact angle of Sn on  $Al_2O_3$  shown in Figure 6.26 as a function of temperature displays three ranges. At low temperatures, high apparent



**Figure 6.25.** Variation of contact angle with the Al molar fraction for the Cu-Al/ $\text{Al}_2\text{O}_3$  system at 1423 K in high vacuum. Circles: in an alumina furnace using the sessile drop technique (Li et al. 1987–88).

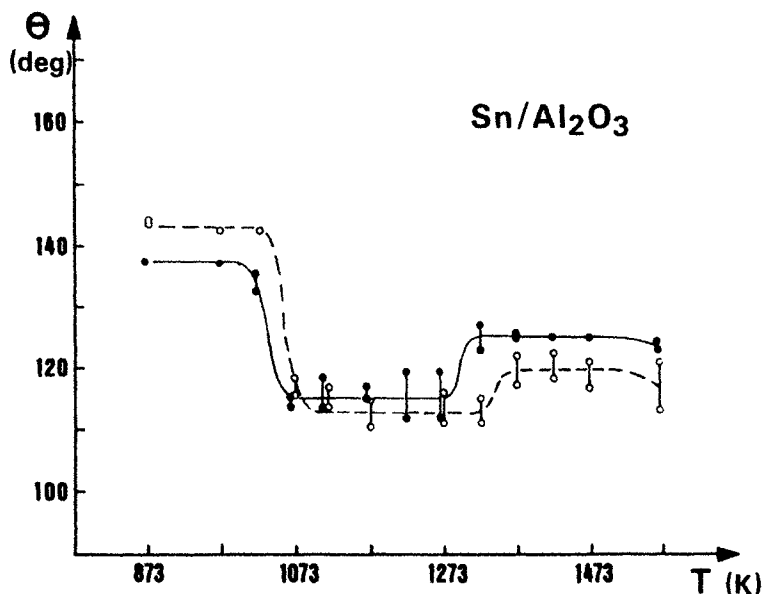
Squares: in a metal chamber furnace using the dispensed drop technique (Labrousse et al., to be published). All points represented by circles for  $0 < X_{Al} < 0.3$  are for oxidised drops.

$\theta$  values are caused by the  $\text{SnO}_2$  film around melted Sn; when the temperature increases, the oxide film is dissolved in Sn since the concentration of oxygen in Sn in *equilibrium with tin oxide* increases. When the oxide film disappears, enough oxygen is present in the melt to affect the metal/oxide interface and the contact angle decreases. When the temperature is further increased, the concentration of oxygen in Sn in *equilibrium with the vapour phase* decreases and oxygen desorbs from the interface leading to dewetting. At high temperatures, the normal wetting behaviour of non-reactive pure metal/oxide systems is observed.

## 6.5. ALLOYING ELEMENTS

### 6.5.1 Non-reactive solutes

Consider a non-reactive system consisting of a binary liquid alloy A-B and an oxide substrate such as  $\text{Al}_2\text{O}_3$  at constant temperature. A simple statistical thermodynamic model has been developed (Li et al. 1989) to predict the contact angle and the work of adhesion isotherms,  $\theta(X_B)$  and  $W_a(X_B)$ , from the known values of contact angles

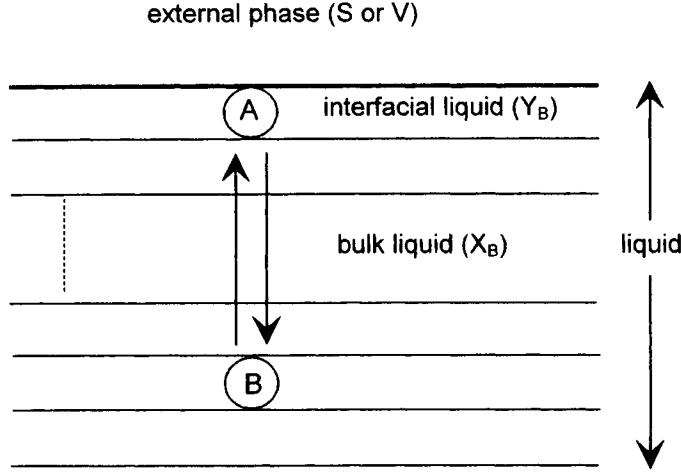


**Figure 6.26.** Contact angle variation with temperature for Sn on  $\text{Al}_2\text{O}_3$  under one atmosphere of He with  $P_{\text{O}_2} = 10^{-16}$  Pa (Rivollet et al. 1987) [10].

$\theta_A$  and  $\theta_B$ , works of adhesion  $W_a^A$  and  $W_a^B$ , and liquid surface energies  $\sigma_{LV}^A$  and  $\sigma_{LV}^B$  of the pure metals. Adsorption of metal atoms on free  $\text{Al}_2\text{O}_3$  surfaces is negligible for non-wetting metals (see Section 1.4.2), so  $\sigma_{SV}$  is constant and calculation of the contact angle and work of adhesion isotherms is reduced to calculating the  $\sigma_{LV}$  and  $\sigma_{SL}$  isotherms.

These calculations were performed by Li et al. (1989) using a regular solution model (Section 4.1.2) and assuming that the interface between the liquid and the external phase, solid or vapour, is a liquid monolayer (Figure 6.27). Moreover, when the external phase is a solid, interpenetration of the liquid and solid phases at the atomic level was neglected. Indeed, for metal-ceramic interfaces any roughening on an atomic level would be more expensive in energy than the gains due to configurational entropy.

Although the model was developed for a A-B alloy over the whole composition range (Li et al. 1989), application to the case of a solution that is infinitely dilute in B leads to simple expressions for the slope of  $\sigma$ - $X_B$  curve and for the “enrichment factor” at the interface  $Y_B/X_B$  where  $Y_B$  is the molar fraction of B in the interfacial monolayer:



**Figure 6.27.** Schematic representation of a monolayer interface in a binary liquid A-B/external phase system according to the model of Li et al. (1989).

$$\left( \frac{d\sigma}{dX_B} \right)_{X_B \rightarrow 0} = \frac{RT}{\Omega_m} \left[ 1 - \exp \left( -\frac{E_{B(A)}^\infty}{RT} \right) \right] \quad (6.28)$$

$$\left( \frac{Y_B}{X_B} \right)_{X_B \rightarrow 0} = \exp \left( -\frac{E_{B(A)}^\infty}{RT} \right) \quad (6.29)$$

$\Omega_m$  is equal to  $\omega N_a$ , where  $\omega$  is the surface area per atom and is readily derived from the molar volume of the alloy ( $\Omega_m \approx v_m^{2/3}$ ).

The pertinent parameter in equations (6.28) and (6.29) is the quantity  $E_{B(A)}^\infty$ , which is the adsorption energy of solute B from the bulk liquid A to the surface or interface (Figure 6.27): a negative value of  $E_{B(A)}^\infty$  indicates attraction of B by the interface, while a positive value indicates attraction by the bulk liquid. The adsorption energy is equal to the difference in energy of the system after and before segregation of B. If  $m_2$  and  $m_1$  are, for an atom, the fractions of nearest neighbours located respectively in the same layer and in an adjacent one ( $m_2 + 2m_1 = 1$ , see Figure 1.3) and  $\epsilon_{i-ex}$  is the energy of a bond formed between the atom  $i$  and the external



phase, by calculating the variation of the number of pairs A-A and A-B during segregation, it holds:

$$\begin{aligned}
 E_{B(A)}^{\infty} &= [Z(m_2 + 2m_1)\varepsilon_{AA} + Z(m_2 + m_1)\varepsilon_{AB} + Zm_1\varepsilon_{B-ex}] \\
 &\quad - [Z(m_2 + 2m_1)\varepsilon_{AB} + Z(m_2 + m_1)\varepsilon_{AA} + Zm_1\varepsilon_{A-ex}] \\
 &= -Zm_1\varepsilon_{AB} + Zm_1\varepsilon_{AA} + Zm_1\varepsilon_{B-ex} - Zm_1\varepsilon_{A-ex} \\
 &= -Zm_1\left[\varepsilon_{AB} - \frac{\varepsilon_{AA} + \varepsilon_{BB}}{2}\right] + Zm_1\left[\frac{\varepsilon_{AA}}{2} - \frac{\varepsilon_{BB}}{2}\right] + Zm_1[\varepsilon_{B-ex} - \varepsilon_{A-ex}]
 \end{aligned} \tag{6.30}$$

The first term results from the heat of mixing of A-B alloy (see equations (4.3) and (4.4)). The second term comes from the cohesion energies of pure A and pure B and is related to the liquid surface energies  $\sigma_{LV}^A$  and  $\sigma_{LV}^B$  (see equations (1.9) and (1.10)). The third term comes from the adhesion energy of pure A and B on the external phase. When the external phase is the vapour,  $\varepsilon_{B-ex} = \varepsilon_{A-ex} = 0$  and the molar adsorption energy is reduced to equation (4.8):

$$E_{B(A)}^{\infty, LV} = (\sigma_{LV}^B - \sigma_{LV}^A)\Omega_m - m_1\lambda \tag{6.31}$$

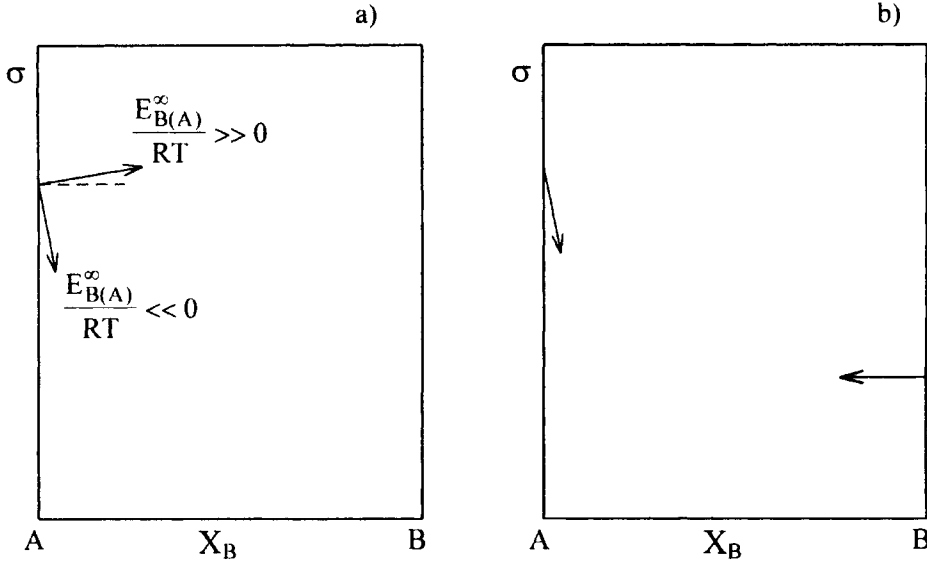
When the external phase is a solid substrate S,  $\varepsilon_{B-ex}$  and  $\varepsilon_{A-ex}$  are related to the work of adhesion of pure B and pure A on the solid (see equation (1.12)):

$$W_a^i = -\frac{Zm_1 N_a \varepsilon_{i-S}}{\Omega_m} \quad i = A, B \tag{6.32}$$

and the adsorption energy is given by:

$$E_{B(A)}^{\infty, SL} = (\sigma_{LV}^B - \sigma_{LV}^A)\Omega_m - (W_a^B - W_a^A)\Omega_m - m_1\lambda \tag{6.33}$$

Following equation (6.28), if  $E_{B(A)}^{\infty}/RT$  is very negative, the slope  $(d\sigma/dX_B)_{X_B \rightarrow 0}$  will also be very negative. Conversely, if  $E_{B(A)}^{\infty}/RT$  is very positive, the slope will be positive but small (Figure 6.28.a). Indeed, the maximum value of  $(d\sigma/dX_B)_{X_B \rightarrow 0}$  will be equal to  $RT/\Omega_m$  and substitution of typical values of temperature (1000K) and molar surface area ( $\Omega_m \approx 5 \times 10^4 \text{ m}^2 \cdot \text{mol}^{-1}$ ), gives the negligible value of  $2 \text{ mJ/m}^2$  per 1% of solute. This behaviour predicted by the



**Figure 6.28.** a) Effect of small additions of an alloying element on the interfacial or liquid surface energies of a non-reactive binary alloy/ceramic system for very positive and very negative values of adsorption energy. b) A very negative value of the slope of  $\sigma$  when  $X_B \rightarrow 0$  implies a negligible slope when  $X_B \rightarrow 1$ .

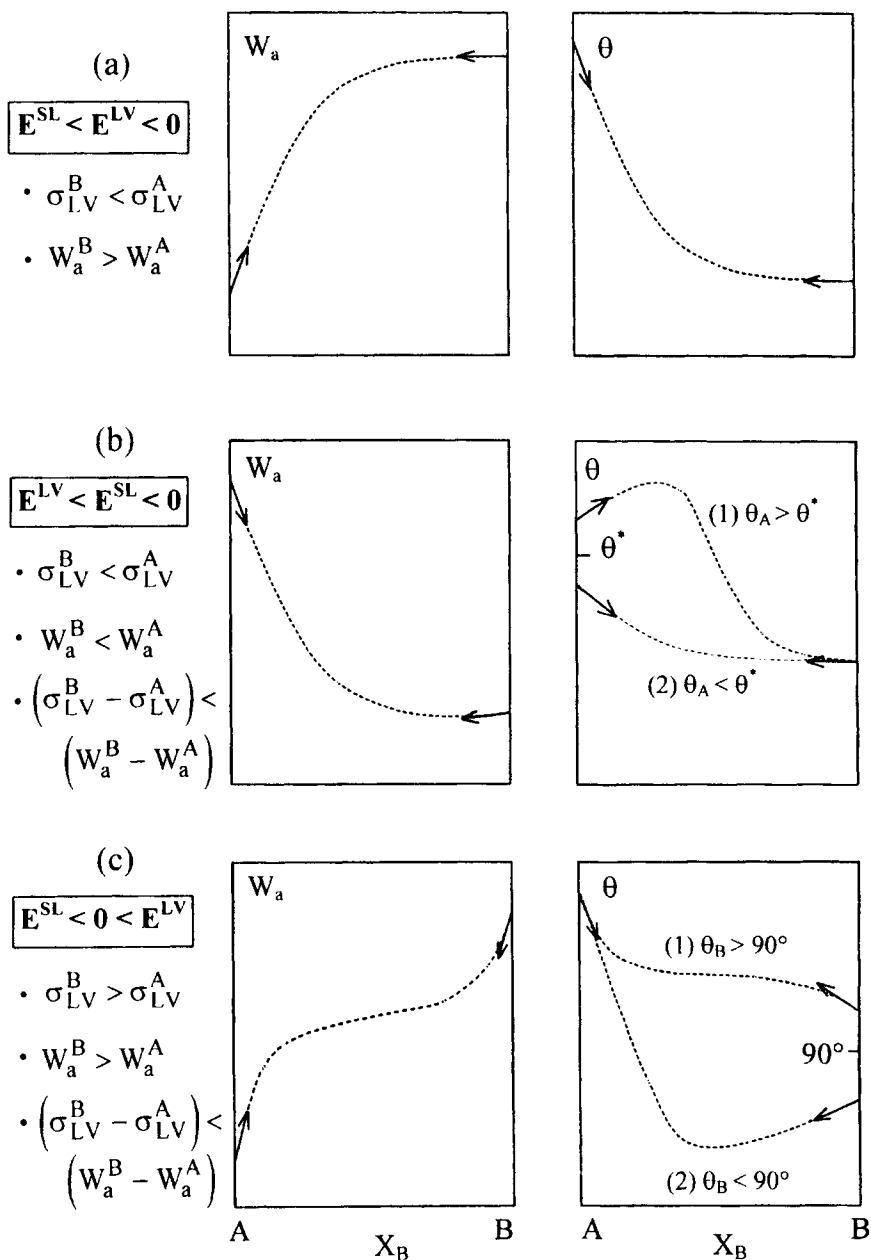
monolayer model is confirmed by the experimental surface energy values of binary alloys (Brunet et al. 1977).

Moreover, since the absolute value of the interaction term in equations (6.31) and (6.33),  $|m_1 \lambda|$ , is usually much less than that of the capillary terms,  $|\sigma_{LV}^B - \sigma_{LV}^A| \Omega_m$  and  $|W_a^B - W_a^A| \Omega_m$ , the following relation applies for both the  $E^{LV}$  and  $E^{SL}$  energies of adsorption for a binary alloy:

$$E_{B(A)}^\infty \ll 0 \Leftrightarrow E_{A(B)}^\infty \gg 0 \quad (6.34)$$

Thus, if the slope of the  $\sigma$ - $X_B$  curve at  $X_B \rightarrow 0$  is negative, that at  $X_B \rightarrow 1$  will nearly equal zero (see Figure 6.28.b and experimental results in Figure 4.5.a).

For A-B/oxide systems, and more generally non-reactive liquid A-B/solid systems, the model predicts three main types of  $W_a(X_B)$  and  $\theta(X_B)$  isotherms, depending on the absolute and relative values of the adsorption energies  $E_{B(A)}^{\infty, LV}$  and  $E_{B(A)}^{\infty, SL}$  (Figure 6.29). In the particular case of isotherms (b), two different

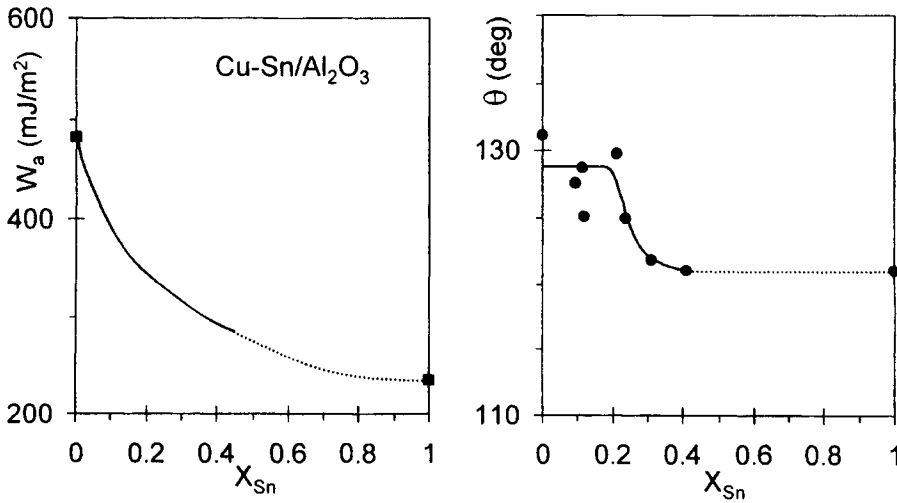


**Figure 6.29.** Main forms of work of adhesion and contact angle isotherms for non-reactive A-B liquid alloy/ceramic systems (Li et al. 1989) [2].

curves can be obtained for  $\theta(X_B)$  depending on whether  $\theta_A$  is greater or smaller than a value  $\theta^*$  given by (Li et al. 1989):

$$\cos \theta^* = - \frac{1 - \exp[-E_{B(A)}^{\infty,SL}/RT]}{1 - \exp[E_{B(A)}^{\infty,LV}/RT]} \quad (6.35)$$

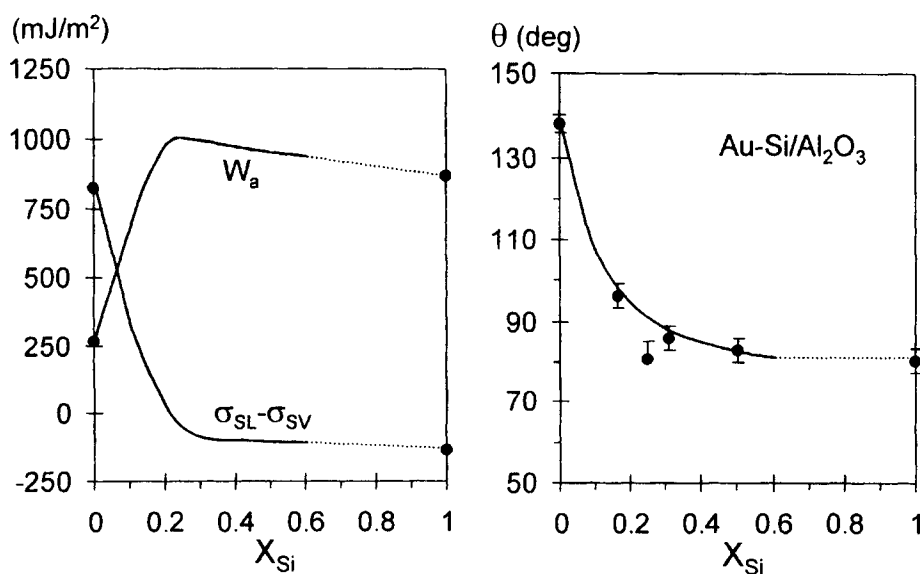
For alloys consisting of two non-wetting, non-reactive metals developing van der Waals interactions with the oxide, we have seen in Figure 6.7 that  $W_a$  is nearly proportional to  $\sigma_{LV}$  ( $W_a \cong 0.4\sigma_{LV}$ ). It can be readily shown that the behaviour of such binary alloys on  $Al_2O_3$  belongs to the type (b) isotherms of Figure 6.29. Thus, addition of B to A (with  $\sigma_{LV}^B \ll \sigma_{LV}^A$ ) hardly decreases  $\theta_A$  but in all cases decreases the work of adhesion of A on  $Al_2O_3$  and any other ceramic for which adhesion is mainly due to van der Waals interactions. Examples are Cu-Sn on  $Al_2O_3$  (Figure 6.30), Ga-Sb on  $Al_2O_3$  and  $SiO_2$  (Harter et al. 1993) and Cu-Au on  $Al_2O_3$  (Ghetta et al. 1996).



**Figure 6.30.** Experimental  $W_a(X_{Sn})$  and  $\theta(X_{Sn})$  isotherms for the Cu-Sn/ $Al_2O_3$  system at 1423K (Li et al. 1989) illustrating case (b) in Figure 6.29.

In order to obtain the maximum improvement in wetting and adhesion for a A/oxide system, the alloying element B must satisfy the conditions that generated

the (a) isotherms of Figure 6.29 i.e., it must have a low surface energy and a high work of adhesion compared to A. These conditions can be satisfied only using elements that develop chemical interactions at the liquid/oxide interface, such as Al and Si (as discussed in Section 6.3, the values of  $W_a$  for these elements are three times higher than those for metals with the same  $\sigma_{LV}$  but that develop only van der Waals interactions with  $\text{Al}_2\text{O}_3$ ). Thus the wetting of  $\text{Al}_2\text{O}_3$  is enhanced by the addition of Al to Cu (Figure 6.25) and of Si to Au (Figure 6.31). Note the presence in the  $W_a$ - $X_{\text{Si}}$  curve of Figure 6.31 of a slight maximum not predicted by the model. This maximum, which can be more pronounced for other systems such as Ni-Al/ $\text{Al}_2\text{O}_3$  (Merlin and Eustathopoulos 1995, Grigorenko et al. 1998), was attributed to dissolved oxygen. However, further work is needed to confirm this interpretation.



**Figure 6.31.** Work of adhesion, difference ( $\sigma_{\text{SL}} - \sigma_{\text{SV}}$ ) and contact angle for the Au-Si/ $\text{Al}_2\text{O}_3$  system at 1423K (Drevet et al. 1990) [3] illustrating case (a) in Figure 6.29.

The third kind of isotherms ((c) in Figure 6.29) is generated by a solute B which adsorbs strongly at the A/oxide interface but not at the A/vapour surface. An example of such a system is Al in Sn on  $\text{Al}_2\text{O}_3$  (Figure 6.32). When Al is added to Sn, the contact angle decreases because the solid/liquid interfacial energy decreases. When Sn is added to Al, the contact angle decreases again because the

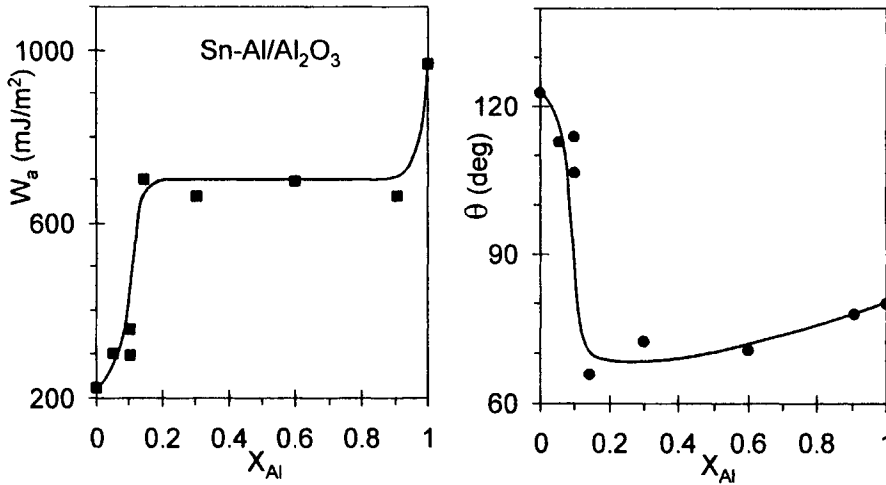


Figure 6.32. Experimental  $W_a(X_{Al})$  and  $\theta(X_{Al})$  isotherms for the Sn-Al/Al<sub>2</sub>O<sub>3</sub> system at 1273K (Li et al. 1989) [2] illustrating case (c) in Figure 6.29.

surface energy decreases. Thus, as predicted by the model, the contact angle isotherm passes through a minimum and such behaviour has been observed not only for oxide substrates but also other ceramics such as AlN (Naidich and Taranets 1998).

These examples show that it is possible to produce transitions from non-wetting ( $\theta > 90^\circ$ ) to wetting in metal/oxide systems using a non-reactive solute able to develop chemical interactions with the oxide. Such solutes cause  $E_{B(A)}^{\infty,SL}$  to be negative and hence are capable of modifying solid/liquid interfaces by adsorption. A further decrease in  $\theta$  can then be achieved by adding a second solute that decreases the surface energy of the liquid ( $E_{B(A)}^{\infty,LV} < 0$ ). An example is the Cu-Al-Sn/Al<sub>2</sub>O<sub>3</sub> system, in which Al is active at the Cu/Al<sub>2</sub>O<sub>3</sub> interface and Sn is active at the Cu/vapour surface (Li et al. 1988).

Despite their great technical importance, there are few reported studies of segregation at *solid* metal/oxide interfaces. Hondros (1978) used Auger spectroscopy to examine interfaces formed between sapphire and Fe containing Cr or Ni and found a high interfacial enrichment of Cr over a zone of a few nanometers. The results were used to explain the strong *mechanical* adhesion of Fe on Al<sub>2</sub>O<sub>3</sub> induced by Cr additions.

In another study, Shashkov and Seidman (1996) used atom-probe field-ion microscopy to examine the adsorption of Ag dissolved in solid Cu at semi-coherent interfaces between Cu-Ag and MgO precipitates obtained by internal oxidation of

a ternary Cu-Mg-Ag alloy. At 500°C and for a molar fraction of Ag in Cu of  $5 \times 10^{-3}$ , a strong adsorption of Ag was found that corresponded to a Ag monolayer at the Cu/MgO interface. Such an adsorption cannot be explained by the model used for liquid alloys, that is, taking into account only differences in cohesion energy and adhesion energy of pure components and the regular solution parameter. It is possible that a term of elastic energy due to atomic size differences becomes predominant in some cases, as for the segregation of alloying elements at grain boundaries or free surfaces of solid metals (see also Section 4.1.3).

### 6.5.2 Reactive solutes

As a general rule, the addition of non-reactive solutes to a liquid metal does not cause contact angle decreases below 60°. In principle, lower contact angles can be achieved using reactive solutes.

Consider a reactive solute B dissolved in a non-reactive matrix M in contact with an oxide substrate such as  $\text{Al}_2\text{O}_3$ . The chemical interaction in this system can be described by the dissolution of  $\text{Al}_2\text{O}_3$  in the alloy:



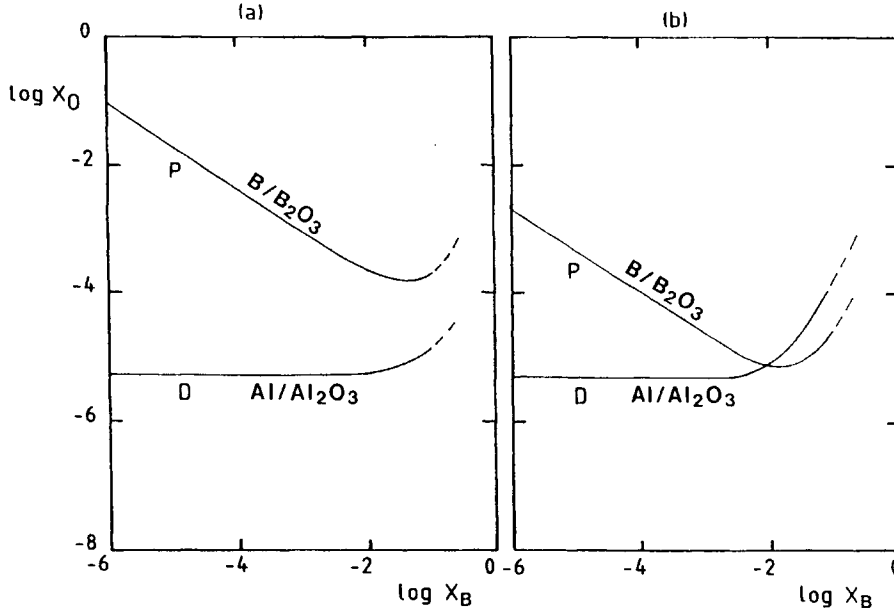
possibly followed by the precipitation of a B oxide at the interface, for example:



For small molar fractions of B and Al, and taking into account equation (6.4), the equilibrium mole fraction of dissolved oxygen  $X_{\text{O}}^{\text{D}}$  for reaction (6.36) (the superscript D stands for dissolution) will be given by the equation:

$$X_{\text{O}}^{\text{D}} = \left(\frac{3}{2}\right)^{2/5} (K'_{\text{D}}(T))^{2/5} \exp\left(-\frac{3}{5}\epsilon_{\text{O}}^{\text{B}}X_{\text{B}}\right) \quad (6.38)$$

where the constant  $K'_{\text{D}}(T)$  is given by equation (6.3).  $\epsilon_{\text{O}}^{\text{B}}$  is Wagner's first order interaction parameter between the O and B solutes defined by equation (6.22). If  $\epsilon_{\text{O}}^{\text{B}} < 0$ , then  $X_{\text{O}}^{\text{D}}$  increases rapidly at high values of  $X_{\text{B}}$ : strong O-B interactions will promote  $\text{Al}_2\text{O}_3$  dissolution in the melt (curves D in Figure 6.33).



**Figure 6.33.** Thermodynamics of (matrix M-solute B)/Al<sub>2</sub>O<sub>3</sub> systems with  $\epsilon_O^B < 0$ . Curve D presents the logarithm of the molar fraction of oxygen coming from stoichiometric dissolution of Al<sub>2</sub>O<sub>3</sub> in M-B alloys as a function of log  $X_B$ . Curve P illustrates the variation of  $X_O$  in equilibrium with B<sub>2</sub>O<sub>3</sub> as a function of  $X_B$ . In a) only dissolution of Al<sub>2</sub>O<sub>3</sub> in the melt occurs, as for Ni-Cr alloys at 1773K (Kritsalis et al. 1992). In b) the solute B reduces Al<sub>2</sub>O<sub>3</sub> to the right of the intersection point of the two curves, as for Ni-Ti at 1773K (Naidich et al. 1974, Merlin et al. 1992).

Moreover, a solute B satisfying the condition  $\epsilon_O^B \ll 0$  can cause precipitation of an oxide B<sub>2</sub>O<sub>3</sub> by reaction with the excess oxygen in the alloy. The mole fraction of dissolved oxygen in equilibrium with the B<sub>2</sub>O<sub>3</sub> precipitate (reaction (6.37)), denoted  $X_O^P$ , is given by:

$$X_O^P = K'_P(T) X_B^{-2/3} \exp(-\epsilon_O^B X_B) \quad (6.39)$$

In this equation,  $K'_P(T)$  is a constant given by (Kritsalis et al. 1992):

$$K'_P(T) = (K_P(T))^{-2/3} (\gamma_B)^{-2/3} (\gamma_{O(M)}^\infty)^{-1} \quad (6.40)$$



where  $K_p(T)$  is the equilibrium constant of reaction (6.37),  $\gamma_B$  is the activity coefficient of B in the alloy and  $\gamma_{O(M)}^\infty$  is the activity coefficient of oxygen at infinite dilution in pure M. When  $X_B \rightarrow 0$ ,  $X_O^P$  varies as  $X_B^{-2/3}$ , i.e. it is a decreasing function of  $X_B$ . However, for  $\epsilon_O^B \ll 0$ , the exponential term in equation (6.39) predominates at higher  $X_B$  values and  $X_O^P$  increases rapidly with  $X_B$  (curves P in Figure 6.33). Thus, the concentration of dissolved oxygen increases above a certain value of  $X_B$  for both dissolution and precipitation.

If for a particular value of  $X_B$  the inequality  $X_O^D > X_O^P$  is verified, the solute B will reduce  $Al_2O_3$  forming  $B_2O_3$ :

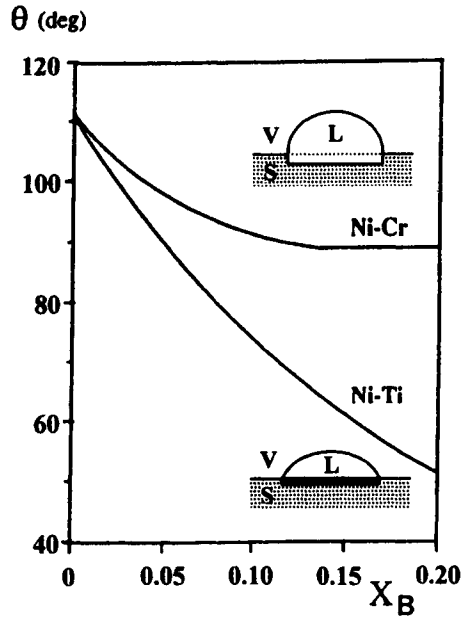


This condition is satisfied for the Ni-Ti alloy because interactions between O and Ti solutes are very strong ( $\epsilon_O^{Ti} = -100$ ), but not for Ni-Cr alloys ( $\epsilon_O^{Cr} = -25$ ). Thus, additions of Cr up to 20 at.% in Ni do not cause formation of a chromium oxide, the only effect is to increase the dissolution of  $Al_2O_3$  in the alloy. As shown in Figure 6.34, Cr additions in Ni significantly decrease the contact angle of Ni on  $Al_2O_3$  and this could result from two effects, both of which require that  $\epsilon_O^B < 0$ :

- i) an increased concentration of dissolved oxygen due to interfacial reactions i.e., an increased concentration of O-M clusters which can be adsorbed at the metal/oxide interface;
- ii) an increased adsorption capability of the O-Cr clusters as compared with the O-Ni clusters. Indeed, as Cr is more electropositive than Ni, the charge transfer from Cr to O (or, in other terms, the degree of ionicity of O-Cr clusters) would be greater than in the case of Ni.

Other examples of alloying elements leading to strong improvements in wetting without forming 3D reaction products at the interface are Ti in Cu in contact with  $Y_2O_3$  (Figure 6.36) and Ti in Sn in contact with  $Al_2O_3$  (Naidich 1981, Tomsia et al. 1998).

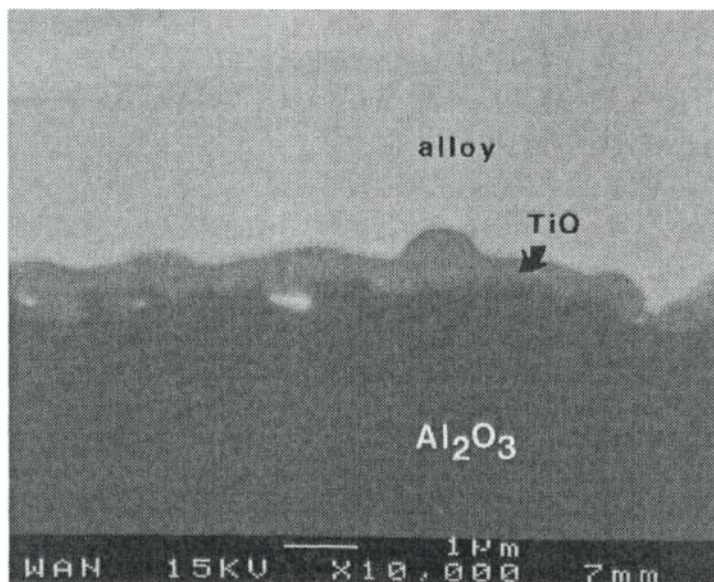
In the Ni-Ti/ $Al_2O_3$  system, as  $\epsilon_O^{Ti} \ll 0$ , O-Ti clusters in Ni are very active at metal/oxide interfaces but wettability is affected also by the formation of a continuous  $Ti_2O_3$  layer at the Ni/ $Al_2O_3$  interface. The replacement of ionocovalent  $Al_2O_3$  by the semi-metallic oxide  $Ti_2O_3$  increases  $W_a$  and decreases  $\theta$ , as explained in Section 6.3. The combination of these two effects, i.e., adsorption of O-Ti clusters at the *liquid-side* of the interface and formation of a semi-metallic oxide



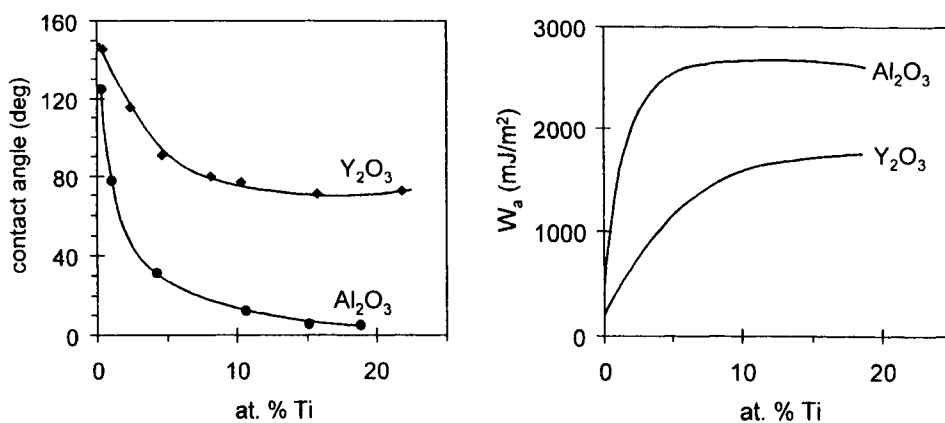
**Figure 6.34.** Contact angles at 1773 K of Ni-based alloys on  $\text{Al}_2\text{O}_3$  plotted as a function of the Cr(Ti) molar fraction for Ni-Cr (Kritsalis et al. 1992) and Ni-Ti (Naidich et al. 1974). The Ni-Cr alloys cause dissolution of  $\text{Al}_2\text{O}_3$  but the Ni-Ti alloys cause dissolution of  $\text{Al}_2\text{O}_3$  followed by precipitation of a Ti oxide.

such as  $\text{Ti}_2\text{O}_3$  at the *solid-side* of the interface, explains the strong decrease in contact angle caused by Ti additions in Ni (Figure 6.34).

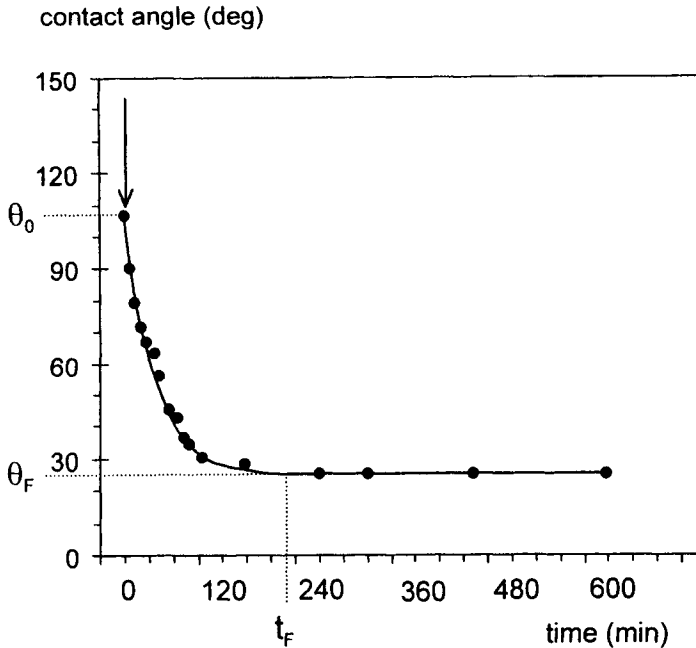
This influence of Ti is even greater in the case of Cu-Ti alloys on  $\text{Al}_2\text{O}_3$  (Naidich et al. 1990, Kritsalis et al. 1991) and NiFeCr-Ti alloys on  $\text{Al}_2\text{O}_3$  (Wan et al. 1996) where the metal-like oxide TiO is formed at the interface owing to the higher thermodynamic activity of Ti (Figure 6.35). Wetting is nearly perfect as opposed to the Cu-Ti/ $\text{Y}_2\text{O}_3$  system (Figure 6.36) where only dissolution of  $\text{Y}_2\text{O}_3$  into the alloys occurs, to produce a significant but limited decrease of  $\theta$  from  $140^\circ$  to  $80^\circ$ . However, adding Ca to Al on  $\text{Al}_2\text{O}_3$  or  $\text{SiO}_2$  substrates has no effect on wetting in spite of the formation of CaO at the interface (Mori et al. 1983) because the ionocovalent substrate is replaced by an oxide of the same type. A similar result was obtained by Kritsalis et al. (1992) for NiPd-Cr alloys on  $\text{Al}_2\text{O}_3$  at 1523K: Cr additions do not affect wetting in spite of the precipitation of Cr oxide at the interface.



**Figure 6.35.** SEM micrograph of the cross-section of a Ni alloy containing 16 at.% Ti with  $\text{Al}_2\text{O}_3$  showing the TiO reaction product at the interface (holding time of 30 min at 1463K). The final contact angle in this system is about  $20^\circ$ . From (Wan et al. 1996) [22].



**Figure 6.36.** Contact angle and work of adhesion values for Cu-Ti melts on  $\text{Y}_2\text{O}_3$  and  $\text{Al}_2\text{O}_3$  at 1423K. Reactions cause dissolution of the oxide substrate in the first case, and dissolution + precipitation of a Ti oxide at the interface in the second. Data from work reported in (Naidich et al. 1990) [2].



**Figure 6.37.** Contact angle of a Cu-9.5 at.% Ti alloy on  $\text{Al}_2\text{O}_3$  as a function of time at 1373K (Kritsalis et al. 1991) [2].

Figure 6.37 shows the change with time of the contact angle of a reactive Cu-Ti alloy on  $\text{Al}_2\text{O}_3$ . This result is also discussed in Section 2.2.2.2 (sub-section “diffusion-limited spreading”). The addition of 9.5 at.% Ti decreases the contact angle from the  $130^\circ$  of pure Cu to about  $30^\circ$ . However, the  $\theta$  versus time curve exhibits two stages. The first corresponds to a change of  $\theta$  from  $130^\circ$  to  $100^\circ$  that is achieved in less than 1 second and attributed to adsorption of Ti at the interface. The second is much slower and controlled by the lateral extension of the interfacial reaction product (TiO) at the triple line. Similar two stage kinetics have been observed in (Espie et al. 1994) for other Ti containing alloys on various oxide substrates.

These considerations can explain the results of Figure 6.2 for reactive pure metal/oxide couples in which a new phase is formed at the interface. Wettability then depends on the bonding character of this interfacial layer and two cases can be distinguished:

1) First, replacement at the interface of an ionocovalent oxide by another of the same type. No significant improvement of wetting is expected for this type of

system. Al on  $\text{SiO}_2$  provides an example of intense reactivity, causing reduction of  $\text{SiO}_2$  to form  $\text{Al}_2\text{O}_3$  and a slight liquid enrichment in Si. Because the ionocovalent oxide  $\text{SiO}_2$  is replaced by an oxide of the same type, the contact angle of Al on  $\text{SiO}_2$  ( $\theta \approx 80^\circ \pm 5^\circ$  at 1073K) is similar to that of Al on  $\text{Al}_2\text{O}_3$ . The same explanation is valid for the Al/MgO system in which the reaction leads to formation of  $\text{Al}_2\text{O}_3$  or  $\text{MgAl}_2\text{O}_4$  at the interface.

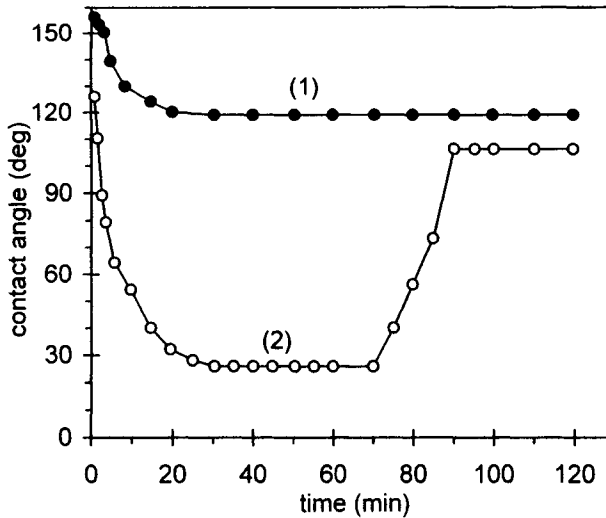
2) Second, replacement at the interface of an ionocovalent oxide by a metallic one. A typical example of this is provided by the Ti/MgO system. Liquid Ti can react to dissolve several at.% O and form metal-like oxides such as TiO or even solid solutions of Ti with high oxygen contents. The perfect wetting observed for this system (Figure 6.2) can be explained by the double *in-situ* modification of the interface: the adsorption of oxygen at the liquid-side and the formation of a metallic phase at the solid-side.

## 6.6. WETTING OF FLUORIDES

Like many oxides, alkaline-earth metal fluorides such as  $\text{CaF}_2$  and  $\text{BaF}_2$  are very stable thermodynamically and have a high degree of ionocity, for instance that of  $\text{CaF}_2$  on the Pauling's scale is 89%. Only van der Waals dispersion force interactions are expected to develop at interfaces with non-reactive metals, resulting in large, obtuse, contact angles. For instance, sessile drop experiments carried out for pure Cu and Sn on smooth, monocrystalline  $\text{CaF}_2$  surfaces in high vacuum at 1100°C yield contact angles of 140° and 118° (Naidich and Krasovsky 1998). For molten Al on  $\text{CaF}_2$ , a contact angle of 130° was found at 700°C, decreasing to 100° at 1000°C (Naidich et al. 1983b).

Using alloying elements with high affinities for F, such as Ti, Zr and Hf, improves wetting as shown by the examples in Figure 6.38. The addition of 1.3 at.% Ti to a Cu-Sn alloy at 900°C produces only a limited improvement in wetting, but addition of 35 at.% Ti causes the contact angle to decrease strongly to about 30° owing to the formation of  $\text{TiF}_3$  at the interface. However, as  $\text{TiF}_3$  is volatile with a boiling temperature of 1037°C, it is eliminated from the interface by evaporation in high vacuum and the contact angle increases with time to a value greater than 90°. When the wetting experiment is repeated at 1150°C, i.e., at a temperature higher than the boiling temperature of  $\text{TiF}_3$ , no minimum in the  $\theta$ -t curve appears and the final contact angle is close to 120°.

Alkaline-earth metal fluorides have been proposed for use as refractories when melting and casting Ti, Zr and Hf alloys which react with and wet most current materials (Naidich and Krasovsky 1998).



**Figure 6.38.** Contact angle vs time at 900°C in high vacuum for a Cu-11.9 at.% Sn alloy containing 1.3 at.% Ti (curve 1) and 35 at.% Ti (curve 2) on CaF<sub>2</sub>. Data from work reported in (Naidich and Krasovsky 1998) [9].

## 6.7. CONCLUDING REMARKS

Pure metal/oxide systems can be divided into three categories. Systems for which the molar fraction of oxygen dissolved in the liquid metal coming from the oxide,  $X_O$ , is lower than  $10^{-6}$  have contact angles of 110–140°. Weak physical metal/oxide interactions are localized at a sharp interface and result in work of adhesion values that are small compared to the work of cohesion of the metal. For systems with  $X_O > 10^{-5}$  that do not react to form a new phase, dissolved oxygen and metal atoms from the oxide can produce significant improvements in wetting by forming 2D adsorption layers (i.e., with a typical thickness of 1 nm) at the metal/oxide interface. These adsorptions can lead to contact angles lower than 90° but usually  $\theta$  remains above 60°. Even lower contact angles can be achieved by metals that react with the oxide forming 3D compounds at the interface which are, at least partially, metallic in their bonding characteristics.

For a non-reactive and non wetting pure metal on an oxide, improved wetting can be achieved either by adsorption at metal/oxide interface of oxygen supplied by a gas with a controlled  $P_{O_2}$  or by introducing certain specific alloying elements

modifying *in situ* the interface. In practice, it is difficult to operate in a gas atmosphere with a fixed  $P_{O_2}$  using a buffer gas and hence wetting behaviour is more often modified by introducing alloying elements capable of producing a favourable interfacial chemistry.

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## Chapter 7

# Wetting properties of metal/non-oxide ceramic systems

Oxides are not the only technically important ceramic materials. Carbides (SiC, B<sub>4</sub>C, TiC) and nitrides (BN, AlN, TiN, Si<sub>3</sub>N<sub>4</sub>) are of prime importance as bonded components in advanced developments for the machine tool, microelectronics, aircraft, automobile and heat exchanger industries.

Although some of the concepts established for metal/oxide systems are also valid for non-oxide ceramics, there are other concepts which are specific to these kinds of ceramics, owing to their predominantly covalent (SiC, BN, AlN) or metallic (TiC, TiN, WC) character. These materials seldom can be obtained as the high-purity monocrystalline specimens desirable for fundamental wetting studies. Usually, they are sintered materials with impurity contents higher than 0.1% and they often contain open porosity. Further difficulties arise from the high oxidation tendency of many of them, the presence of an oxide layer dramatically changing their wettability by liquid metals.

The first Section of this Chapter deals with predominantly covalent ceramics (Table 7.1), with a particular emphasis on SiC for which a recent detailed study of wetting by liquid metals combined with a study of surface chemistry has been reported. In the second Section, wetting by liquid metals of metal-like ceramics is presented.

## 7.1. METALS ON PREDOMINANTLY COVALENT CERAMICS

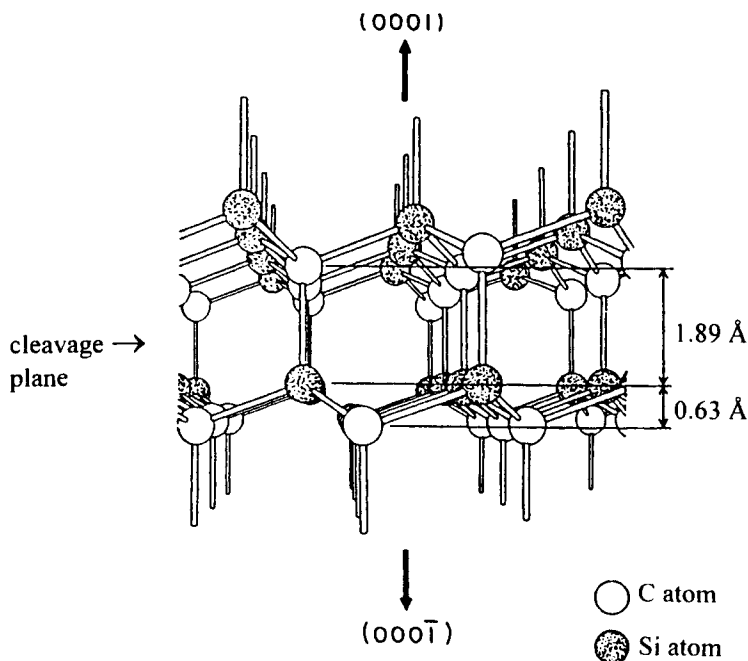
### 7.1.1 *Wetting of SiC*

SiC is a covalent ceramic of technological interest because of its semi-conductor character, good mechanical properties, high thermal conductivity and good thermal shock behaviour. SiC is easily oxidizable but the oxide layer is protective so the ceramic can be used as a structural material in high temperature applications or as reinforcement in metal matrix composites. Also, it is an interesting material for basic studies of wetting as it can be obtained in the form of high purity monocrystals.

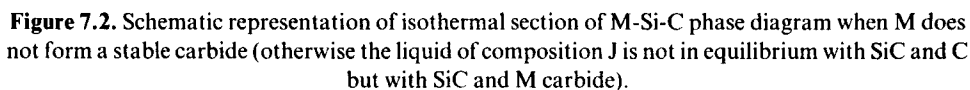
There are two main allotropic forms of SiC: hexagonal ( $\alpha$ -SiC) and cubic ( $\beta$ -SiC). The lattice planes of SiC consist of tetrahedrons of SiC<sub>4</sub> (four C atoms around a Si atom) or CSi<sub>4</sub> (Figure 7.1). If we consider a SiC<sub>4</sub> tetrahedron, the distance

**Table 7.1.** Degree of covalence of different ceramics according to the scale of electronegativity of Pauling (1960).

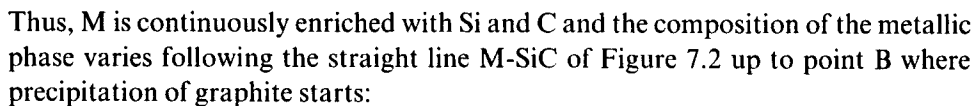
Compound	B <sub>4</sub> C	SiC	Al <sub>4</sub> C <sub>3</sub>	BN	Si <sub>3</sub> N <sub>4</sub>	AlN	SiO <sub>2</sub>	Al <sub>2</sub> O <sub>3</sub>	MgO
Degree of covalence (%)	94	89	78	78	70	57	49	37	27

**Figure 7.1.** Si face  $(0001)$  and C face  $(000\bar{1})$  of the hexagonal structure of  $\alpha$ -SiC.

between Si and the plane containing the three C atoms at the base of the tetrahedron ( $0.63 \text{ \AA}$  for  $\alpha$ -SiC) is much smaller than the distance between this Si atom and the fourth C atom located at the top of the tetrahedron ( $1.89 \text{ \AA}$  for  $\alpha$ -SiC). As a consequence, the cleavage of SiC occurs only between the more widely separated planes of Si and C. Thus, one gets two parallel faces with different surface chemistry, the Si face terminated by Si atoms  $(0001)$  for  $\alpha$ -SiC and  $(111)$  for  $\beta$ -SiC) and the C face terminated by C atoms  $(000\bar{1})$  for  $\alpha$ -SiC and  $(\bar{1}\bar{1}\bar{1})$  for  $\beta$ -



When a drop of metal M *which does not form a stable carbide* is placed on a SiC substrate, SiC dissolves in the liquid metal:



Dissolution of SiC continues, leading to an increase of the Si content in the liquid M while the excess C precipitates. The overall reaction is:

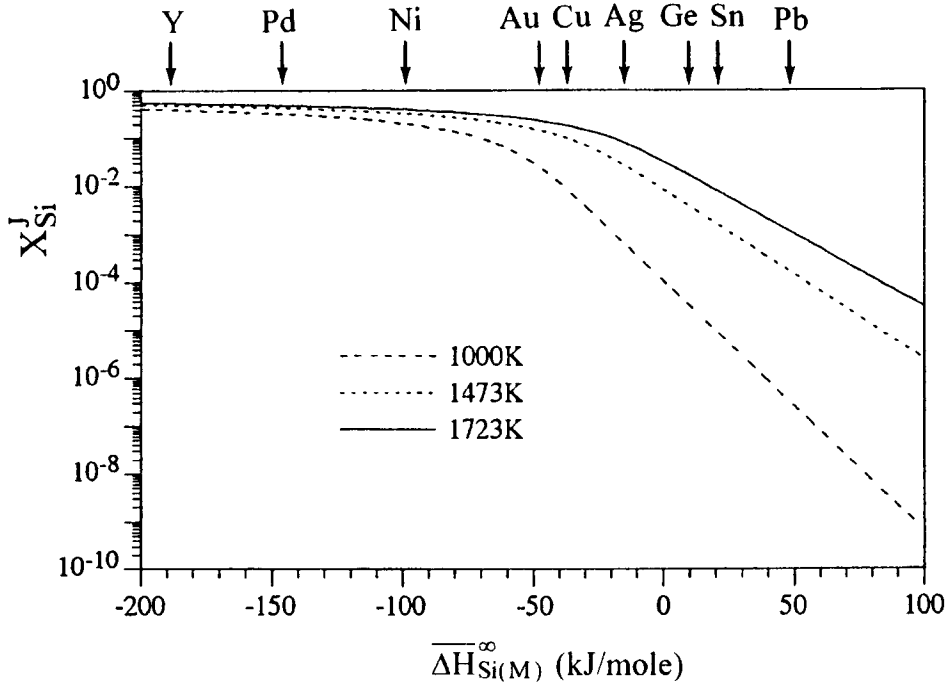


This reaction stops when the liquid composition reaches point J, where SiC becomes stable in contact with the liquid and precipitated C. At this point, the equilibrium molar fraction of Si dissolved in M,  $X_{\text{Si}}^{\text{J}}$  (Figure 7.2), is related to the partial enthalpy of mixing of Si in M,  $\overline{\Delta H}_{\text{Si(M)}}$  (neglecting the partial excess entropy of mixing), and to the molar Gibbs energy of formation of SiC,  $\Delta G_{\text{f(SiC)}}^0$ , by the equation:

$$X_{\text{Si}}^{\text{J}} = \exp\left(\frac{\Delta G_{\text{f(SiC)}}^0 - \overline{\Delta H}_{\text{Si(M)}}}{RT}\right) \quad (7.4)$$

Semi-quantitative calculations of  $X_{\text{Si}}^{\text{J}}$  can be made for all metals by equating  $\overline{\Delta H}_{\text{Si(M)}}$  to the value at infinite dilution,  $\overline{\Delta H}_{\text{Si(M)}}^{\infty}$  (data for this last quantity are given in Appendix G). Figure 7.3 suggests that, except for some low melting point elements like Pb and Sn (and also Bi, Sb), metals have a significant reactivity with SiC even at a temperature as low as 1000K. For high-melting-point transition metals like Ni and Pd, the reactivity is very high and results in substantial dissolution of SiC that occurs rapidly and is accompanied by the formation of large graphite precipitates (Figure 7.4).

In wetting experiments, such graphite precipitation makes the spreading process an extremely complex phenomenon owing to the fact that graphite is less wetted by M-Si alloys than SiC: graphite precipitates act as barriers to wetting (see Section 2.2.2.1, Figures 2.28 and 2.29). Because of these complications, results of wetting for non-reactive, Si saturated liquids i.e., M-Si alloys with  $X_{\text{Si}} > X_{\text{Si}}^{\text{J}}$ , will be presented first. However, even for such M-Si/SiC systems, spreading on SiC surfaces is a complex process because the chemistry of SiC surfaces is very different from that of the bulk.

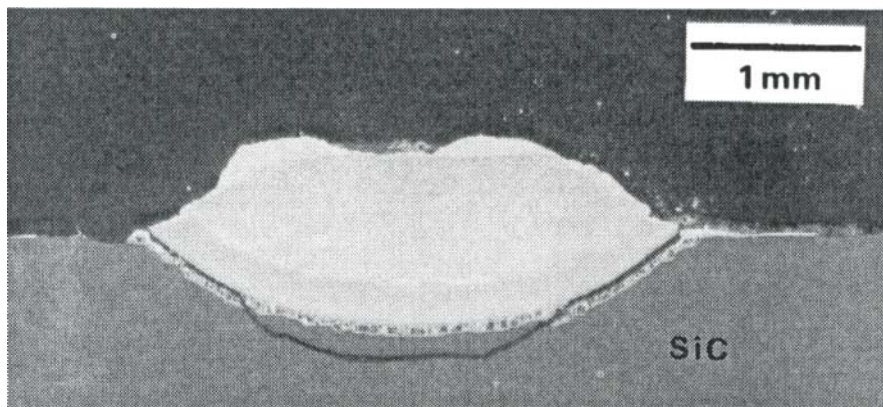


**Figure 7.3.** Calculated values of molar fraction of Si in liquid metal M at the three phase M/SiC/C<sub>g</sub> equilibrium (equation 7.4) as a function of the partial enthalpy of mixing of Si at infinite dilution in M. Arrows indicate values of  $\overline{\Delta H}_{\text{Si(M)}}^{\infty}$  for some metals M given in Appendix G.

#### 7.1.1.1 Non-reactive systems: silicon alloys on SiC

**Equilibrium contact angles.** At the Si melting point, the Si/SiC couple is a nearly non-reactive system, with only a slight dissolution of SiC into Si. Pure Si wets SiC well ( $\theta = 30\text{--}50^\circ$ ) regardless of whether the furnace atmosphere is a high vacuum or neutral gas and whether the ceramic is monocrystalline, polycrystalline, CVD or sintered  $\alpha$ -SiC or  $\beta$ -SiC (Naidich and Nevodnik 1969, Yupko and Gnesin 1973, Nikolopoulos et al. 1992, Drevet et al. 1993, Rado 1997). For monocrystalline SiC, the degree of wetting depends on the polarity of the (111) face for  $\beta$ -SiC and of the (0001) face for  $\alpha$ -SiC. However, the contact angle on Si-terminated faces is lower than on C-terminated faces by only  $5\text{--}10^\circ$  for both  $\alpha$ -SiC (Rado 1997) and  $\beta$ -SiC (Bakovets 1977). The good wetting observed for Si/SiC corresponds to a value of the work of adhesion of about 90% of the work of cohesion  $W_c$  of liquid Si ( $W_c = 2\sigma_{LV}$ ). Such a value is too high to be attributed to van der Waals interactions so chemical interactions must be responsible. In solid Si, bonds are covalent (with a



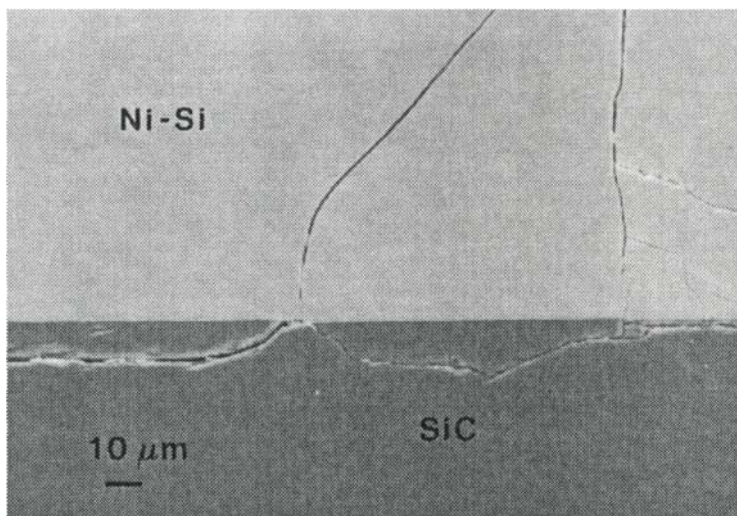


**Figure 7.4.** SEM micrograph of a cross section in a Ni/SiC specimen showing the strong reactivity between Ni and SiC. The holding time was 15 min at 1350°C (complete melting occurs at 1262°C). From (Rado et al. 1999) [23].

coordination number equal to 4) but at melting some delocalisation of bond electrons occurs accompanied by an increase of the number of nearest neighbours, and molten Si becomes a metallic conductor. However, this effect is limited as indicated by the fact that the average coordination number in molten Si ( $\approx 5$  to 6.5 (Kita et al. 1994)) is much lower than in a typical metal ( $\approx 9$  to 11). These considerations indicate that bonding in molten Si will be partially covalent and partially metallic, so Si can establish covalent interactions with atoms of the SiC surface.

For Ni-Si alloys at 1360°C (Rado et al. 1999), the experimental value of  $X_{Si}^I$  is 0.37 while the calculated molar fraction of C at point J,  $X_C^I$  (Figure 7.2), is  $10^{-3}$ . Therefore, no alloys with Si content greater than 0.37 will react with SiC (e.g., Figure 7.5). Equilibrium contact angles for different alloys are given in Figure 7.6. Additions of Ni in Si causes a limited but significant decrease in contact angle and a substantial increase, by a factor two or more, in the work of adhesion (Figure 7.6). To explain these effects, the Gibbsian adsorption (or the equivalent enrichment factor  $Y_{Ni}/X_{Ni}$ , see Figure 7.7) was calculated from the experimental  $(\sigma_{SL} - \sigma_{SV})$  versus  $\ln(a_{Ni})$  curve by a method similar to that described in Section 6.4.1, assuming that the surface energy of SiC does not change with  $X_{Ni}$ :

$$\frac{1}{RT} d(\sigma_{SL}) = -\Gamma_{Ni}^{Si} d(\ln a_{Ni}) \quad (7.5)$$

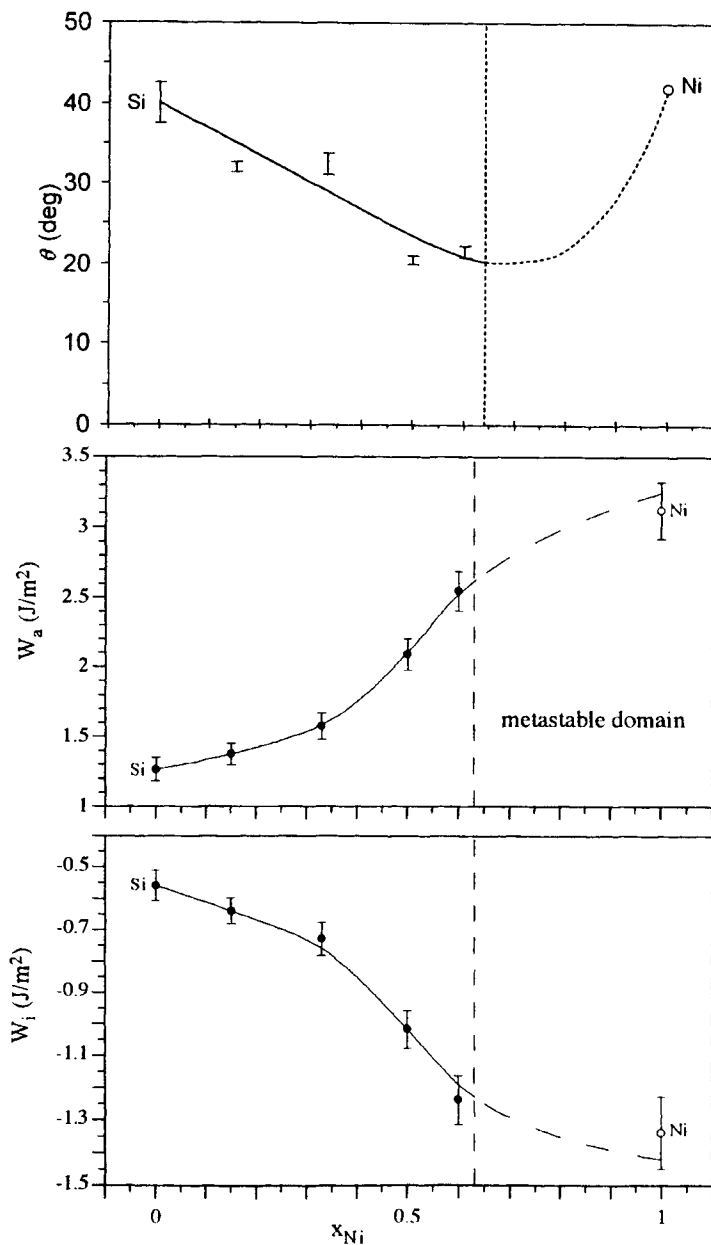


**Figure 7.5.** SEM micrograph of a cross section in a Ni-40 at.% Si/SiC specimen (20 min at 1350°C) showing a smooth interface without any graphite precipitate. Some cracks in bulk materials are seen but not at the interface which is comparatively strong. From (Rado et al. 1999) [23].

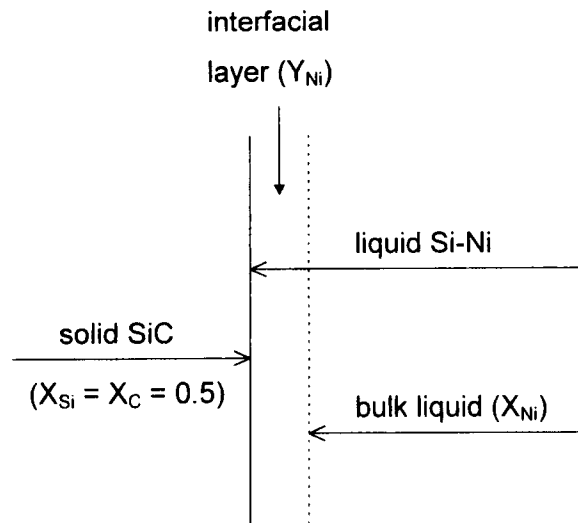
Whatever the composition of the Ni-Si alloy, the adsorption of Ni,  $\Gamma_{\text{Ni}}^{\text{Si}}$ , at the alloy/SiC interface is positive, corresponding to  $Y_{\text{Ni}}/X_{\text{Ni}}$  values of 1.5 to 2. Enrichment of the interface in Ni indicates that interactions between Ni and SiC at the interface are stronger than those between Si and SiC. The work of adhesion of pure Ni on SiC in *metastable equilibrium* (i.e., for a supposed non-reactive Ni/SiC system), evaluated in Appendix I, is  $W_a^{\text{Ni}} = 3.17 \text{ J/m}^2$ . This value is reported in Figure 7.6 along with the corresponding values of work of immersion and contact angle.

The work of adhesion of pure Ni on SiC of  $3.17 \text{ J/m}^2$  is about 90% of the work of cohesion  $W_c^{\text{Ni}}$  ( $\approx 2\sigma_{\text{LV}}^{\text{Ni}}$ ). Such a high adhesion energy indicates the establishment of chemical interactions between Ni and carbide atoms at the interface. Magaud and Pasturel (1998) carried out first principles calculations of electronic structure and adhesion energy for pure Ni on the Si-terminated surface of (111)  $\beta$ -SiC, equivalent to the (0001) plane of hexagonal  $\alpha$ -SiC. They found a strong hybridization between the s-p hybrid states of the SiC surface and the d-orbitals of Ni at the interface and an adhesion energy of  $3.10 \text{ J/m}^2$ , in good agreement with the  $3.17 \text{ J/m}^2$  found by Rado et al. (1999).

To sum up, the good wetting observed for pure Si on SiC ( $\theta = 40^\circ$ ) is due to strong interactions established at the interface between Si and SiC. The addition of



**Figure 7.6.** Isotherms of contact angle, work of adhesion and work of immersion ( $W_i = \sigma_{SL} - \sigma_{SV}$ ) for non-reactive Ni-Si alloys on  $\alpha$ -SiC at 1360°C in high vacuum. Points for pure Ni are extrapolated ones, as calculated in Appendix I. Data from work reported in (Rado et al. 1999) [23].



**Figure 7.7.** Schematic representation of the monolayer adsorption model in the Ni-Si/SiC system.  $Y_{Ni}$  and  $X_{Ni}$  are the molar fractions of Ni in the interfacial layer and bulk liquid respectively.

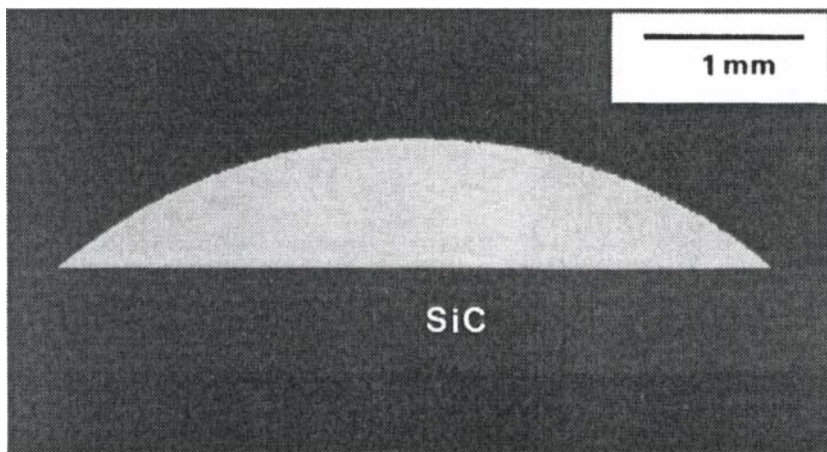
**Table 7.2.** Experimental contact angles of non-reactive M-Si alloys on SiC in high vacuum except for Ag (in purified He).

Metal matrix M	T (K)	$X_{Si}^I$	$X_{Si}$	$\theta$ (deg)	Reference
Ag	1473	0.004	0.05	38	(Rado 1997)
Cu	1423	0.14	0.20	32	(Rado 1997)
Ni	1633	0.37	0.40	21	(Rado et al. 1999)
Co	1773	0.41	0.50	17	(Gasse 1996)
Fe	1633	0.27 <sup>(*)</sup>	0.33	35	(Kalogeropoulou et al. 1995)

<sup>(\*)</sup> calculated

Ni to Si improves wetting and increases the work of adhesion because interfacial interactions between Ni and SiC are stronger than those between Si and SiC (it should be recalled that  $W_a$  is proportional to the solid-liquid interaction energy, equation (1.12)).

Rado (1997) observed similar changes of  $\theta$  and  $W_a$  with  $X_M$  for other binary M-Si alloys. Some of these results are reported in Table 7.2 for non-reactive alloys i.e., alloys for which  $X_{Si} > X_{Si}^I$  (see also Figures 7.8 and 7.9). In all cases, low

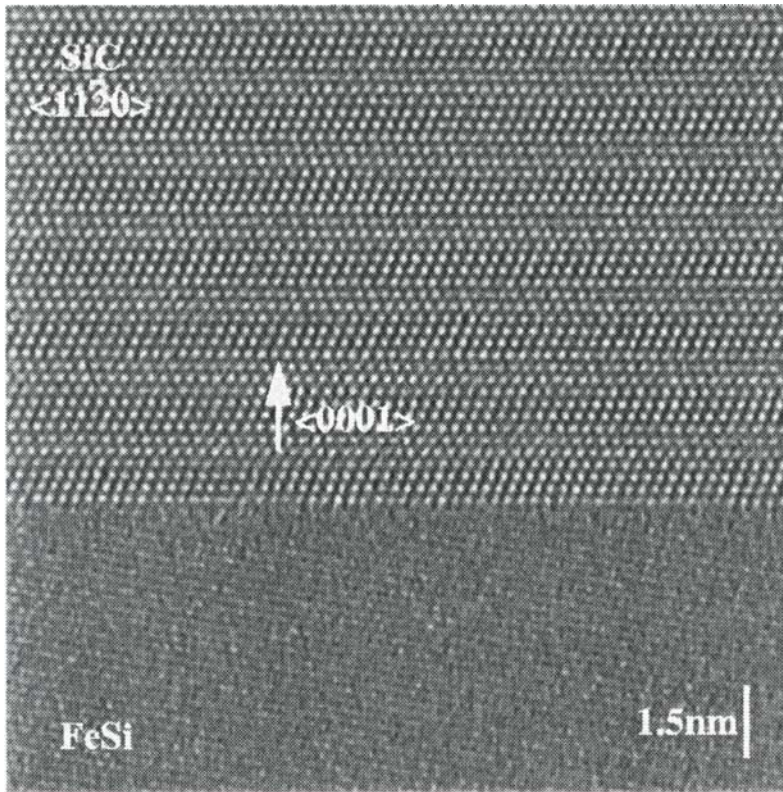


**Figure 7.8.** Solidified drop of eutectic Ag-Si alloy on  $\alpha$ -SiC after heating at 1200°C in a purified He atmosphere. In this non-reactive system, wetting is good and the interface is strong after cooling (Rado 1997).

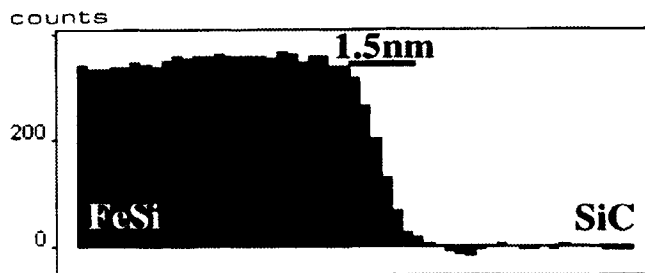
contact angles were observed that could be explained by strong chemical interactions at the interface between atoms of the transition metal M and those of SiC. High values of  $W_a^M$  and low contact angles were calculated by extrapolating data for binary M-Si alloys to pure M. These findings have been confirmed also by the experiment described in Section 2.2.2.1 showing that the contact angle of pure Ag on unreacted SiC is much lower than 90°.

To determine if these interactions are mainly between the M and Si or C atoms of SiC, Rado attempted to correlate the work of immersion of pure M,  $W_i^M$ , with different thermodynamic quantities characterising the energy of M-Si and M-C interactions. He found that  $W_i^M$  scaled rather well with the parameter  $\lambda_{M-Si} / \Omega_m$ ,  $\Omega_m$  being the molar surface area (Figure 7.10). The regular solution parameter  $\lambda_{M-Si}$  is proportional to  $\epsilon_{M-Si} - (\epsilon_{M-M} + \epsilon_{Si-Si})/2$  (equation (4.3)) while  $W_i^M \cdot \Omega_m$  varies as  $\epsilon_{M-S} - (\epsilon_{M-M}/2)$  where  $\epsilon_{M-S}$  is an average interaction energy between M and Si or C atoms at the interface (see the similar equation (6.10)). Therefore, in a series of different metals M on SiC, the correlation observed between  $W_i^M$  and  $\lambda_{M-Si} / \Omega_m$  shows that the bond energy  $\epsilon_{M-S}$  at the interface scales with  $\epsilon_{M-Si}$ , suggesting that the interactions predominant at the M/SiC interface are M-Si rather than M-C.

The extrapolation of the straight line of Figure 7.10 at  $W_i^M = 0$  defines a threshold value  $(\lambda_{M-Si} / \Omega_m)^* = 1.72 \text{ J/m}^2$  corresponding to a transition from non-

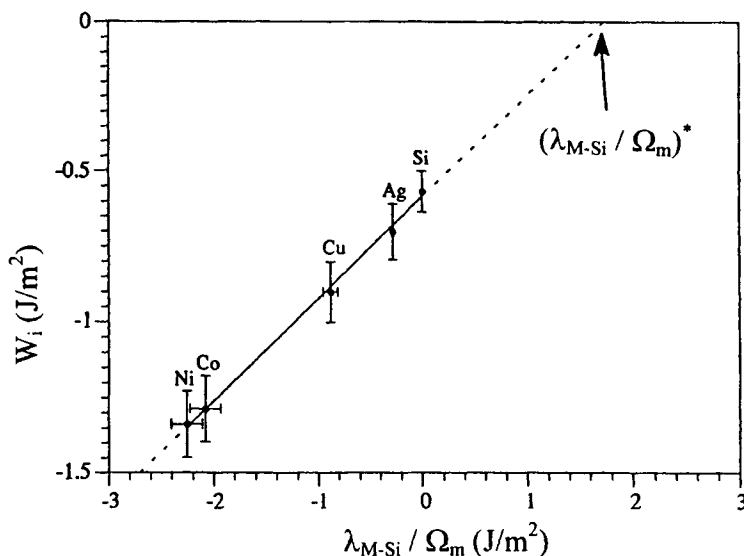


Courtesy CEA Grenoble /DRFMC/SP2M



**Figure 7.9.** Interface between a solidified non-reactive Fe-Si alloy and monocrystalline  $\alpha$ -SiC (for this alloy  $\theta \cong 40^\circ$  (Kalogeropoulou et al. 1995)). Top: high resolution transmission electron Micrograph showing that the interface is sharp at the atomic scale. Bottom : Fe concentration profile across the interface. The thickness of the “chemical” interface is the 1.5 nm resolution of the technique (electron energy-loss spectroscopy). Reprinted from (Lamy, private communication) with kind permission.





**Figure 7.10.** Work of immersion for pure metals M on SiC, evaluated from data for binary M-Si alloys, plotted as a function of  $(\lambda_{M-Si} / \Omega_m)$ . The value  $W_i = 0$  corresponds to  $\theta = 90^\circ$ . From (Rado 1997).

wetting ( $W_i > 0$ ) to wetting ( $W_i < 0$ ). Almost all pure metals, even those with high positive values of  $\lambda_{M-Si}$ , such as Pb, Sn and In, have  $\lambda_{M-Si} / \Omega_m$  values less than  $1.72 \text{ J/m}^2$  and *should* wet SiC surfaces. This prediction is not confirmed by experimental results obtained in the systematic studies performed by Naidich and Nevodnik (1969) and by Nogi and Ogino (1988), which show large non-wetting contact angles for all metals that have a negligible or a weak reactivity with SiC (Table 7.3). The reasons for this disagreement are discussed in the next Section.

**Spreading kinetics.** The wetting behaviour cited in Table 7.3 is that for metals experiencing weak van der Waals interactions with SiC, while the analysis of Rado predicts chemical interactions at their interfaces. To understand this discrepancy, Rado used Auger Electron Spectroscopy (AES) and X-ray Photoelectron Spectroscopy (XPS) in a study of the surface chemistry of the basal planes of  $\alpha$ -SiC as a function of temperature in a high vacuum environment typical of sessile drop experiments (Rado 1997, Rado et al. 1998). Figure 7.11 shows the evolution of the Auger peaks of Si, C and O for SiC substrates heated at various temperatures for 5 minutes. The AES spectra of substrates heated at  $900^\circ\text{C}$  and  $1000^\circ\text{C}$  are nearly identical to that of the reference substrate (i.e., non-heated) and indicate only some pollution by oxygen. XPS analysis of this substrate showed that the thickness of the

**Table 7.3.** Wettability of SiC by different liquid metals M with a negligible or weak reactivity with SiC.

Metal M	$\alpha$ -SiC (*)	T (°C)	Atmosphere	$\theta$ (deg)	$(\lambda_{\text{M-Si}} / \Omega_{\text{m}})$ (J/m <sup>2</sup> )
Ga	M	800	high vacuum	118 <sup>(1)</sup>	0.03
In	M	800	high vacuum	130 <sup>(1)</sup>	0.46
Sn	M	1024	Ar	137 <sup>(2)</sup>	0.46
	M	1050	high vacuum	135 <sup>(1)</sup>	
	S	1100	Ar	150 <sup>(2)</sup>	
Ge	M	1050	high vacuum	113 <sup>(1)</sup>	0.19
	M	1230	Ar	135 <sup>(2)</sup>	
Ag	S	1010	Ar	140 <sup>(2)</sup>	-0.28
	M	1100	high vacuum	128 <sup>(1)</sup>	
	M	1100	He	120 <sup>(3)</sup>	
Au	M	1100	Ar	118 <sup>(2)</sup>	-1.12
	M	1150	high vacuum	138 <sup>(1)</sup>	
	M	1100	high vacuum	138 <sup>(4)</sup>	

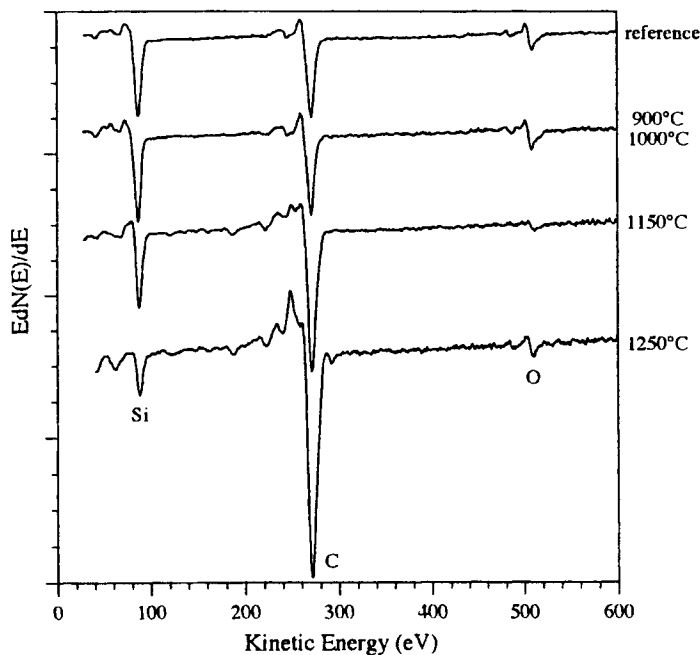
(\*) S = sintered, M = monocrystal

<sup>(1)</sup> (Naidich and Nevodnik 1969), <sup>(2)</sup> (Nogi and Ogino 1988), <sup>(3)</sup> (Rado 1997), <sup>(4)</sup> (Drevet et al. 1993)

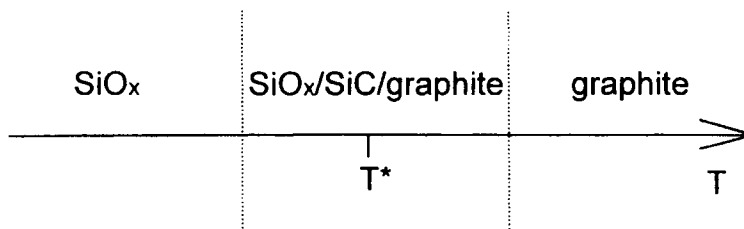
contamination layer was less than 1 nm and resembled a very thin SiO<sub>x</sub> (with  $x \leq 2$ ) or SiO<sub>x</sub>C<sub>y</sub> layer more than one of pure SiO<sub>2</sub>. However, heating to 1150°C produces two significant changes. First, the Auger O peak intensity decreases and second, the C peak increases while that of Si decreases. At the same time, a small shoulder appears at 250 eV, characteristic of C graphite. Clearly, some carbidic C at the SiC surface was transformed into graphite. These two phenomena i.e., enrichment of the surface in C and transformation of surface carbidic C to graphite, are enhanced when the heating temperature is raised to 1250°C. At this temperature and using ion beam erosion analysis, the thickness of the C rich layer was found to be about 3 nm.

From Rado's study, it can be concluded that the nature of SiC surface changes dramatically at a temperature  $T^*$  which depends on the oxygen partial pressure in the furnace (in Rado's experiments  $T^* \approx 1050^\circ\text{C}$ ). At lower temperatures, the SiC surface is *oxidised* while at higher temperatures it is *graphitized*. The transition is continuous around  $T^*$  i.e., without an intermediate state of a non-contaminated,



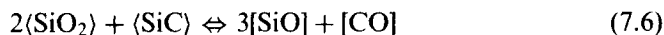


**Figure 7.11.** Auger spectra of the  $\alpha$ -SiC Si face after 5 min holding in a high vacuum metallic furnace at different temperatures (except for the reference specimen) (Rado et al. 1998) [9].



**Figure 7.12.** Surface chemistry of SiC in high vacuum as a function of temperature. Wettability of SiC by non-reactive metals is mainly dictated by the oxidation layer on SiC at  $T \ll T^*$  and by the graphite-rich layer formed by Si evaporation at  $T \gg T^*$ .

stoichiometric, SiC surface (Figure 7.12). Deoxidation of SiC can occur by reaction between  $\text{SiO}_2$  and SiC leading to formation of volatile SiO and CO (Rado et al. 1995):



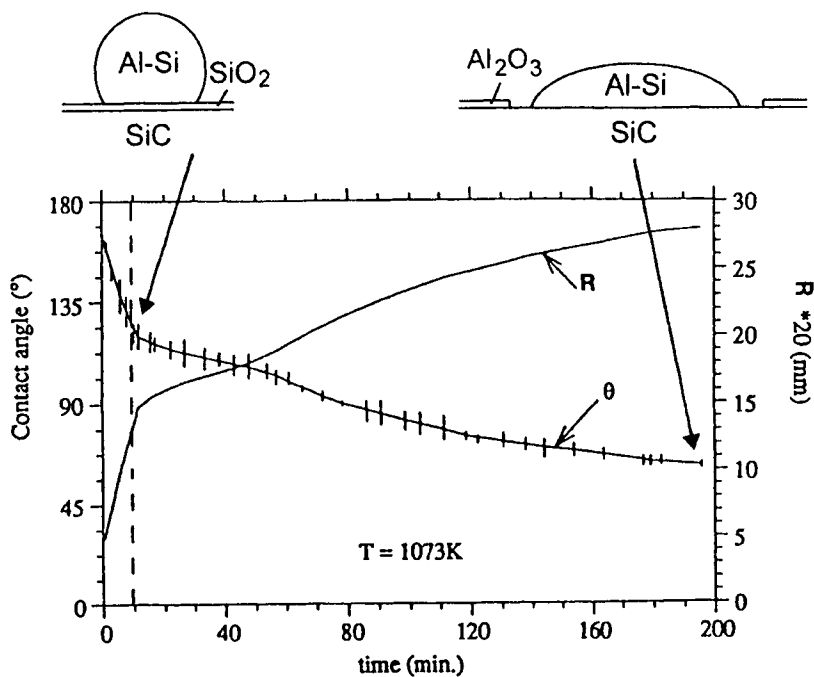
Graphitization of SiC in a high vacuum is known to occur above 1100°C by preferential evaporation of Si (Muehlhoff et al. 1986):



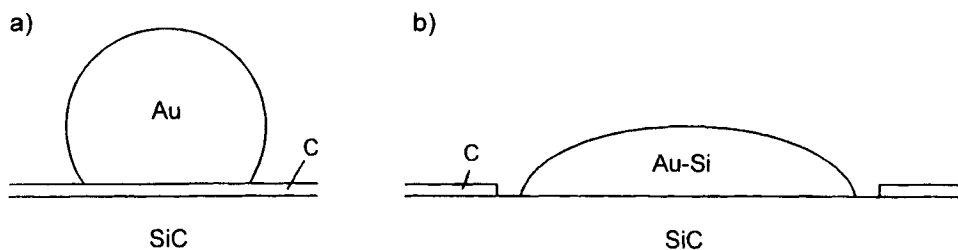
At temperatures much lower than  $T^*$ , deoxidation by the reaction (7.6) is too slow to be effective during wetting experiments typically lasting  $10^3$  seconds, so contact angles for low melting-point metals such as In and Ga in a high vacuum (and *a fortiori* in a commercially pure neutral gas) are expected to be close to those on  $\text{SiO}_2$  i.e., in the range 120°–130°. However, in high vacuum, some metals such as Al and Si can reduce  $\text{SiO}_2$  layers to form the volatile  $\text{Al}_2\text{O}$  and  $\text{SiO}$ . For alloys containing such elements, the contact angle is expected to change from an initial value typical of that on  $\text{SiO}_2$  to a final value characteristic of SiC. An example is the non-reactive Al-19.5 at.% Si/SiC system under high vacuum at 800°C, for which spreading times as long as 150 minutes were observed (Figure 7.13). In this case, the spreading kinetics are controlled by the kinetics of SiC deoxidation occurring at the triple line.

At temperatures higher than  $T^*$ , the SiC surface is covered by a thin graphite layer that should strongly affect wetting and reaction kinetics, graphite acting as a barrier in both cases. An example is Au on monocrystalline SiC. Several authors have found that at temperatures close to its melting point, the contact angle for pure Au is in the range 120–140° (Table 7.3). However, it is clear that these contact angles are for Au on graphite and not on SiC. Moreover, no significant reactivity was observed after 150 minutes of contact between Au and monocrystalline SiC at 1200°C (Rado et al. 1994) despite the fact that Au dissolves SiC up to 15 at.% of Si according to the experimental Au-Si-C phase diagram. Therefore, for metals with very weak affinity for C, the contact angles on SiC at  $T > 1100^\circ\text{C}$  are expected to be close to those on carbon i.e., close to or higher than 120° (Figure 7.14.a) (see Tables 8.3 and 8.4).

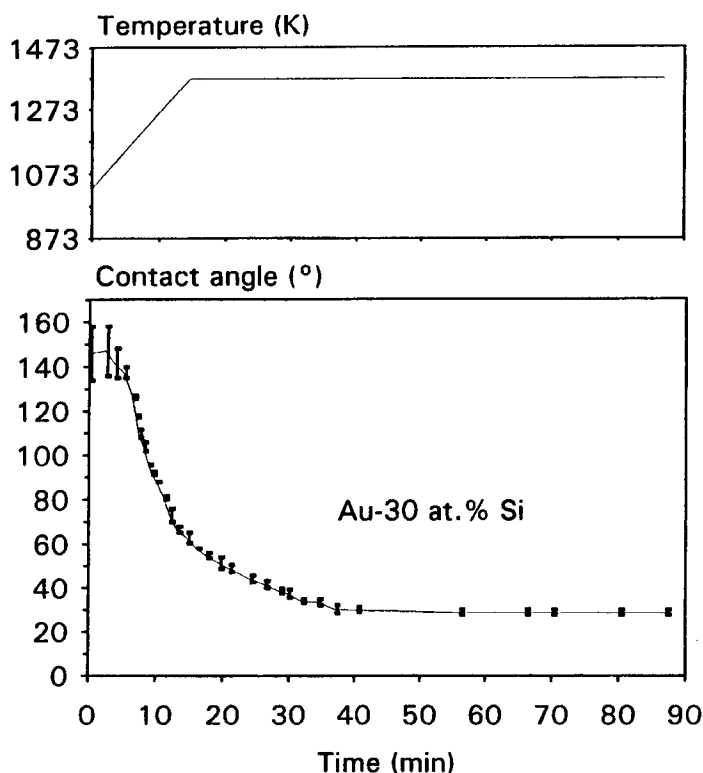
For Au-Si alloys with molar fractions of Si higher than  $X_{\text{Si}}^1 \approx 0.15$  (equation (7.4)), the graphite layer is not stable in contact with Au-Si (Figure 7.14.b). The spreading kinetics are thus controlled by the degraphitization process at the triple line, either simple dissolution of C (the solubility of C in Au is enhanced by Si) or dissolution of C followed by precipitation of SiC. In both cases the final contact angle is that on SiC and, as for other binary alloys of Si (Table 7.2), this angle is very low (Figure 7.15). Note that the “cleaning” of SiC surface can also be achieved by alloying Au (or another metal which does not react with C) with Ni



**Figure 7.13.** Contact angle and radius of the sessile drop base versus time for Al-19.5 at.% Si on monocrystalline  $\alpha$ -SiC at 800°C ( $P = 1$  to  $3 \times 10^{-7}$  mbar). After a comparatively rapid spreading due to deoxidation of the drop (between  $t = 0$  and  $t = 10$  min), spreading is controlled by deoxidation of SiC surface close to the triple line. In front of the triple line, the  $\text{SiO}_2$  layer was transformed into  $\text{Al}_2\text{O}_3$  by reaction with Al coming from the liquid drop. From (Laurent et al. 1996) [22].



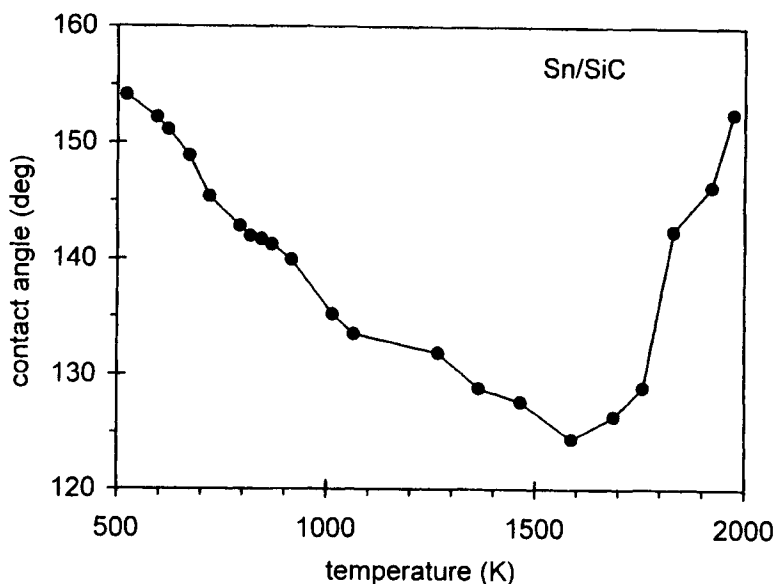
**Figure 7.14.** a) In contact with metals with a negligible affinity for C (such as Au, Ag, Sn), graphitization of SiC surface at high temperature inhibits both wetting and chemical reaction with the metal. b) Additions of Si to Au causes C dissolution followed eventually by SiC precipitation. This configuration corresponds to a true contact angle on SiC.



**Figure 7.15.** Contact angle changes with temperature and time during temperature rise for Au-30 at.% Si on monocrystalline  $\alpha$ -SiC. The experiment was performed in an alumina chamber furnace under high vacuum (Drevet et al. 1993) [24].

and other metals that dissolve large quantities of C. However, Ni aggressively attacks the SiC itself after dissolving the graphite layer (Drevet 1987).

The results shown in Figure 7.16 for Sn on  $\alpha$ -SiC under Ar were obtained for a wide range of temperatures. Large non-wetting contact angles were observed at both low and high temperatures, whereas a contact angle minimum was found at intermediate temperatures close to 1500K. These results can be explained easily by the oxidation of SiC at low temperatures and graphitization of SiC at high temperatures. Similarly Table 7.4 presents contact angles measured by Allen and Kingery (1959) for Sn on  $\text{Al}_2\text{O}_3$  and SiC in two different atmospheres. In the case of  $\text{Al}_2\text{O}_3$ , very large contact angles were observed at all temperatures. These values are much higher than those measured on smooth, monocrystalline  $\text{Al}_2\text{O}_3$  surfaces ( $120$ – $130^\circ$ , see Table 6.1) and could result from the roughness of the sintered



**Figure 7.16.** Contact angle versus temperature plot for Sn on sintered  $\alpha$ -SiC under one atmosphere of Ar. Data from work reported in (Tsoga et al. 1995).

**Table 7.4.** Contact angles of liquid Sn on  $\text{Al}_2\text{O}_3$  and SiC (Allen and Kingery 1959).

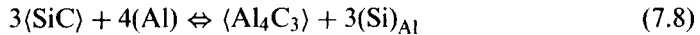
		1073K	1373K	1473K	1743K
$\text{Al}_2\text{O}_3$	$\text{H}_2$	161°	174°	165°	149°
	high vacuum	162°	167°	166°	-
SiC	$\text{H}_2$	166°	165°	160°	140°
	high vacuum	162°	165°	75°	-

ceramic surfaces. For the experiments performed on sintered SiC in a high vacuum, but not in  $\text{H}_2$ , the contact angle suddenly decreases at a temperature between 1373K and 1473K, to a value lower than  $90^\circ$ . This is in good agreement with the correlation of Figure 7.10 which predicts wetting of SiC by Sn ( $W_i < 0$  implying  $\theta < 90^\circ$ ). Results of Table 7.4 suggest that, in high vacuum, before the occurrence of the transition from a non-wettable oxidized SiC surface at low temperatures to a non-wettable graphitized SiC surface at high temperatures, molten Sn contacts a surface more representative of stoichiometric SiC.

### 7.1.1.2 Reactive systems

**Pure metals.** Ferrous metals (Fe, Ni, Co, etc) have a high affinity for Si, reflected by a very negative value of  $\lambda_{\text{M-Si}}$  (and  $\overline{\Delta H}_{\text{Si(M)}}^{\infty}$  in Figure 7.3), but they do not form stable carbides. When solid pure Ni is placed on a SiC substrate, melting starts at the interface at about 1000°C because of a deep eutectic in the Ni-Si phase diagram. Melting is complete at 1260°C, i.e., at a temperature much lower than that needed to melt Ni, owing to the Si and C dissolved in Ni. Observation of the interface after cooling confirms a deep corrosion of SiC and formation of large graphite precipitates (Figure 7.4). Therefore, the contact angles between 50° and 80° given in the literature are only apparent values devoid of thermodynamic meaning. These values are much greater than the 20° obtained for non-reactive Ni-Si alloys with compositions close to  $X_{\text{Si}}^1$  because of the presence of graphite precipitates close to the interface which are less wetted than SiC. In the case of Cu on monocrystalline SiC, the formation of a thin graphite layer at the interface leads to initial contact angles as large as 120-130°. Thereafter, the apparent contact angle decreases slowly with time as an intense dissolution of SiC occurs followed by the formation of large graphite plates detached from the interface (Rado 1997).

Pure Al reacts with SiC to form  $\text{Al}_4\text{C}_3$  at and close to the interface by a dissolution-precipitation mechanism according to the overall reaction:

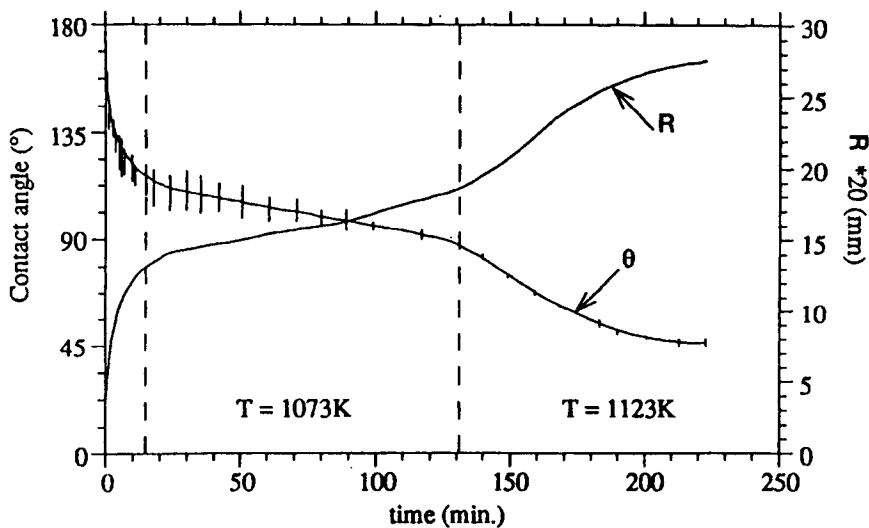


At temperatures lower than 900°C, the kinetics of this reaction are very slow and this leads to the limited formation of discrete particles of  $\text{Al}_4\text{C}_3$  at the interface. The wetting kinetics of pure Al on SiC (Figure 7.17) are very similar to those observed for the non-reactive Al-19.5 at.% Si alloy. Thus spreading of deoxidised Al is controlled by deoxidation of SiC (as for the non-reactive alloy, Figure 7.13) and not by the formation of  $\text{Al}_4\text{C}_3$ . The contact angle after 200 minutes shown in Figure 7.17 is that of Al on nearly unreacted SiC. This contact angle of between 50° and 60° depends on the temperature and, as for the Si/SiC couple, indicates the occurrence of strong chemical interactions localized at the interface.

The electronic structure and energy of an Al cluster in metastable equilibrium with a  $\beta$ -SiC (face (001)) have been modelled by Hoekstra and Kohyama (1998) using *ab initio* calculations. Both C- and Si-terminated faces were examined and strong bonds with Al were found in all cases, but with a higher adhesion energy for Al/C-SiC than Al/Si-SiC. Moreover, the Al/C-SiC bond was found to be predominantly covalent (albeit with some charge transfer from Al to C), as for the bond between Si and C in bulk SiC, while the Al/Si-SiC bond was rather metallic. These calculated results are compatible with the fact that the affinity of Al for C (as

quantified by the enthalpy of formation of  $\text{Al}_4\text{C}_3$ ,  $\Delta H_f = -72$  kJ per mole of C) is much higher than that for Si (the enthalpy of mixing of Si in Al being  $\overline{\Delta H}_{\text{Si(Al)}}^\infty = -9$  kJ/mole).

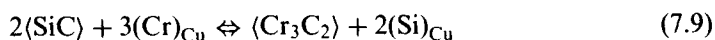
At temperatures higher than  $1000^\circ\text{C}$ , the formation of  $\text{Al}_4\text{C}_3$  at the interface is so greatly accelerated that the stationary contact angles observed during the first few minutes or tens of minutes (depending on the temperature, the furnace atmosphere and whether monocrystalline or sintered SiC is the substrate), lying between  $35^\circ$  and  $55^\circ$  (Naidich 1981, Nogi and Ogino 1988, Shimbo et al. 1989, Ferro and Derby 1995), correspond to those for Al on  $\text{Al}_4\text{C}_3$ . These values are close also to the contact angles observed at low temperatures for Al on an nearly unreacted SiC, indicating that the types of interactions developed at Al/ $\text{Al}_4\text{C}_3$  and Al/SiC interfaces are similar.



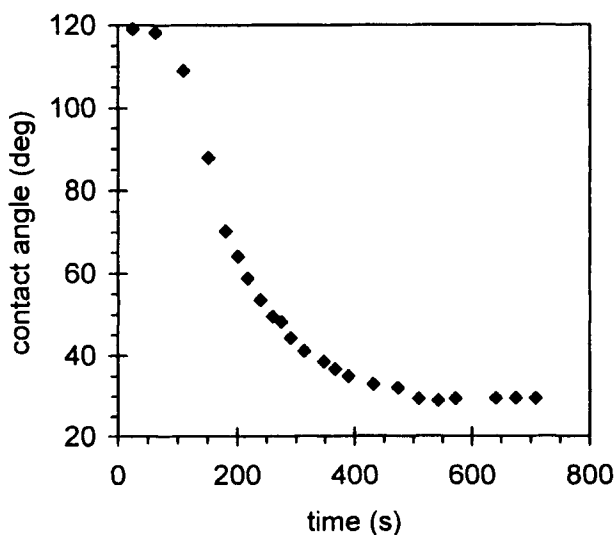
**Figure 7.17.** Contact angle and radius of a sessile drop base versus time for Al on monocrystalline  $\alpha$ -SiC. The increase in temperature by 50K leads to a significant acceleration of spreading rate (Laurent et al. 1996) [22].

**Alloying elements.** As mentioned above, Cu reacts strongly with SiC and the graphite formed during the reaction inhibits wetting. With polycrystalline SiC substrates, this phenomenon results in large non-wetting apparent contact angles, which do

not change with time. By alloying Cu with Cr, the C liberated by SiC decomposition is combined to form a continuous layer of  $\text{Cr}_3\text{C}_2$  a few microns thick according to the reaction:



The  $\text{Cr}_3\text{C}_2$  is wettable (see Table 7.10) and as a result, low wetting contact angles can be achieved by Cu-Cr alloys (Figure 7.18). However, this reaction layer is not protective and Cu penetrates the grain boundaries of the SiC substrate far from the interface to react and form graphite (Landry and Eustathopoulos unpublished, Xiao and Derby 1998).



**Figure 7.18.** Contact angle versus time for Cu-1 wt.% Cr on pressureless-sintered  $\alpha$ -SiC at 1100°C in a high vacuum (Landry and Eustathopoulos unpublished).

Additions of 3.1 at.% Ti to an Ag-Cu alloy with a composition close to the eutectic allow nearly perfect wetting of SiC to be achieved at 900°C in a few minutes. In this case, the interfacial reaction leads to the formation of two layers: a layer of TiC about 1  $\mu\text{m}$  thick on the SiC side and a layer a few microns thick on the metal side with a composition close to  $\text{Ti}_2\text{Si}$  (Ljungberg 1992). The reaction mechanisms at a (Ag-Cu-Ti/monocrystalline  $\alpha$ -SiC) interface were studied by *in*



*situ* high resolution transmission electron microscopy by Iwamoto and Tanaka (1998) who found the reaction started by dissolution of SiC basal planes and continued by epitaxial nucleation and growth of TiC particles on the SiC. No silicide was observed, suggesting that  $\text{Ti}_2\text{Si}$  found by Ljungberg (1992) probably formed during cooling.

Additions of Ti to Al suppress the formation of  $\text{Al}_4\text{C}_3$  at the Al/SiC interface and lead to contact angles close to  $20^\circ$  at  $1150^\circ\text{C}$ . *Post mortem* analysis reveals the formation of a reaction product layer consisting mainly of TiC and  $\text{TiSi}_2$  phases (Sobczak et al. 1998).

### 7.1.2 Wetting of nitrides

The nitrides of Al, Si and B are nearly stoichiometric compounds with a predominantly covalent character. Their ionicity, Table 7.5, and other characteristics are intermediate between those of oxides and carbides. However, individual members possess specific characteristics that have led to the emergence of several nitrides as important engineering materials during the last two decades. Thus AlN can be used as a heat-dissipating electronic substrate and cubic BN finds applications as an ultra-hard cutting material.  $\text{Si}_3\text{N}_4$  and sialon (a complex  $\text{Si}_3\text{N}_4\text{-Al}_2\text{O}_3$  ceramic) have found applications in the aerospace and automobile industries where lightness and high temperature strength are required.

At high temperature, nitrides can dissociate to form  $\text{N}_2$ . In the case of AlN, the dissociation reaction at a temperature higher than the melting point of Al is:



Taking  $a_{\text{Al}} = 1$ , the dissociation pressure of AlN,  $P_{\text{N}_2}^{\text{d}}$ , can be readily calculated from the Gibbs energy of formation of nitride (Kubaschewski and Alcock 1979, Chase et al. 1985). The values given in Table 7.5 indicate a rather weak thermal stability for the three nitrides. In the absence of kinetic barriers, nitrides would decompose rapidly at 1673K in a high vacuum and decomposition of  $\text{Si}_3\text{N}_4$  would occur at a significant rate even at 1273K. Actually, little or no dissociation is observed because of kinetic barriers resulted from a low atomic mobility, on surface and in the bulk, for these compounds (Chatillon and Massies 1990). These barriers lead to a “retarded vaporisation” in which the effective pressure in the vicinity of the nitride surface is  $\alpha \cdot P_{\text{N}_2}^{\text{d}}$ , where the *evaporation coefficient*  $\alpha$  ( $\alpha < 1$ ) can attain very low values (Table 7.5).

**Table 7.5.** Nature of bonding and thermochemical properties of nitrides.

Nitride MeN	Degree of ionicity (%) ( <sup>1</sup> )	$P_{N_2}^d$ (atm)		Evaporation coefficient $\alpha$	Bond energy ( <sup>2</sup> )	
		1273K	1673K		Me-N (kJ/at. g N)	Me-O (kJ/at. g O)
AlN	43	$2 \times 10^{-15}$	$5 \times 10^{-9}$	$< 2 \times 10^{-3}$ (1873K) ( <sup>3</sup> )	-322	-558
BN	22	$5 \times 10^{-12}$	$4 \times 10^{-7}$	$6 \times 10^{-3}$ (1200-1800K) ( <sup>4</sup> ) $< 6 \times 10^{-3}$ (2000K) ( <sup>3</sup> )	-252	-424
Si <sub>3</sub> N <sub>4</sub>	30	$3 \times 10^{-7}$	$10^{-3}$	$10^{-4}$ (1673K) ( <sup>5</sup> )	-185	-354

(<sup>1</sup>) Pauling's scale

(<sup>2</sup>) (Kubaschewski and Alcock 1979), (<sup>3</sup>) (Hildenbrand and Hall 1964), (<sup>4</sup>) (Chatillon and Massies 1990)

(<sup>5</sup>) (Rocabois et al. 1996)

The three Me nitrides (Me = Al, Si, B) are oxidizable materials, the Me-O bond being stronger than the Me-N bond (Table 7.5). As a result, the surface of these nitrides is complex and consists of oxides and oxynitrides even in a high vacuum.

**7.1.2.1 Wetting of AlN.** AlN crystallizes with a hexagonal structure of the wurtzite ZnS type. The Al-N bond is covalent of the  $sp^3$  type but with a substantial degree of ionicity (Table 7.5). Nearly all the wettability data for AlN by liquid metals have been obtained using polycrystalline substrates fabricated by sintering that often contain several % of additives, mainly  $Y_2O_3$ . Even when these substrates are prepared without additives, they can contain several thousands ppm of various impurities, mainly O and C, which can enter the AlN lattice substituting for N atoms. Because of the partially ionic character of AlN, N substitution by O is associated with Al vacancies to maintain electrical neutrality. Dissolved O can migrate to the surface and modify wetting and bonding at high temperatures.

In contact with a liquid metal M, AlN dissociates according to the reaction:



Therefore, the stability of AlN depends both on the strength of the Al-M interactions in the liquid and on the partial pressure of nitrogen in the furnace. For

values of the molar fraction of Al in M at equilibrium  $X_{\text{Al}}^{\text{eq}} \ll 1$ , this quantity is given by:

$$X_{\text{Al}}^{\text{eq}} = P_{\text{N}_2}^{-1/2} \exp \left[ \frac{\Delta G_{\text{f(AIN)}}^0 - \overline{\Delta H}_{\text{Al(M)}}^{\infty}}{RT} \right] \quad (7.12)$$

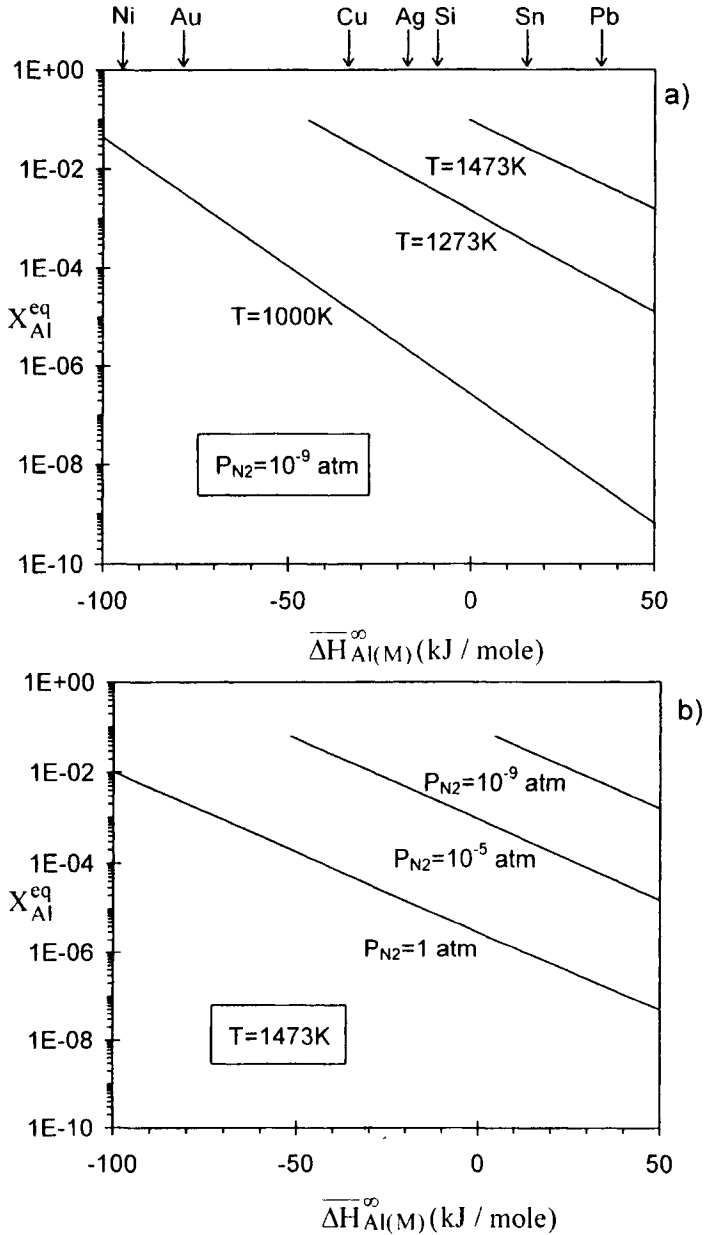
The results shown in Figure 7.19.a have been obtained taking  $P_{\text{N}_2}$  to be  $10^{-9}$  atm which is typical for furnaces evacuated using an oil diffusion pump (Nicholas et al. 1990). These results show high reactivity for all metals at temperatures above 1273K in vacuum. When using a neutral gas with a total pressure of one atmosphere,  $P_{\text{N}_2}$  is approximately  $10^{-5}$  atm. In this case, the reactivity, as expressed by  $X_{\text{Al}}^{\text{eq}}$ , is decreased by a factor  $10^2$  (Figure 7.19.b).

**Table 7.6.** Contact angle of Al on sintered AlN at 1000°C.

AlN characteristics	Atmosphere (*)	Final contact angle $\theta_{\text{F}}$ (deg)	Reference
not specified	HV ( $2 \times 10^{-4}$ Pa) $P_{\text{O}_2} = 10^{-11}$ Pa	53	(Tomsia et al. 1989)
2 wt.% O 0.2 wt.% C	HV ( $2 \times 10^{-3}$ Pa) $P_{\text{O}_2} = 3 \times 10^{-6}$ Pa	60	(Nicholas et al. 1990)
99% AlN porosity <5%	HV ( $2 \times 10^{-3}$ Pa)	53	(Naidich and Taranets 1995)

(\*) HV = high vacuum

At temperatures below 1500°C, the solubility of nitrogen in molten Al in equilibrium with AlN is negligible, so Al/AlN can be considered as a non-reactive couple. Table 7.6 summarises the experimental conditions and results obtained in a high vacuum by three different investigations using sintered AlN. In all cases, good wetting is ultimately observed, with small contact angles indicating a chemical bond across the interface. Taking into account the differences in AlN substrates and furnace atmospheres, the agreement between different investigations on the contact angle at 1000°C can be regarded as remarkable.



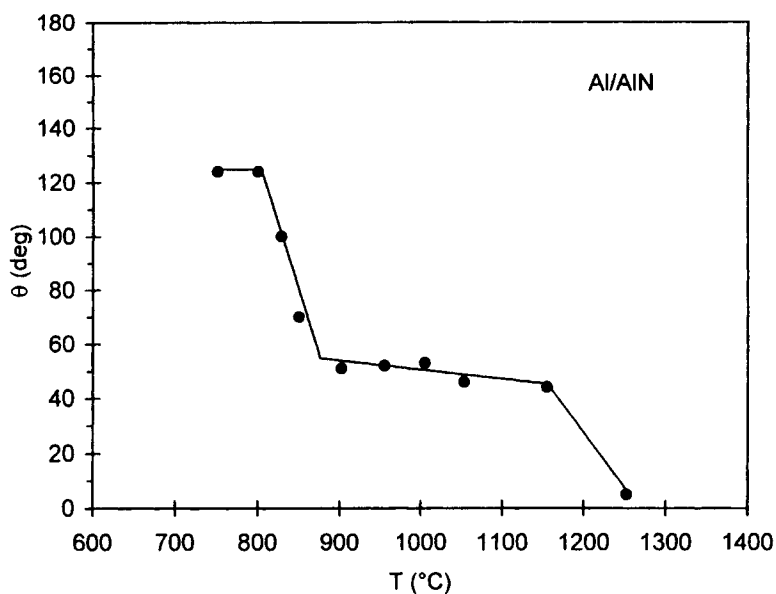
**Figure 7.19.** Calculated values of molar fraction of Al in liquid metal M in equilibrium with AlN at a fixed  $P_{N_2}$  and temperature plotted as a function of the partial enthalpy of mixing of Al at infinite dilution in M. Arrows indicate values of  $\overline{\Delta H_{Al(M)}^\infty}$  for some metals M that do not form stable nitride.

However, the spreading kinetics during the experiments listed in Table 7.6 were very different. They were relatively rapid for the experiments of Nicholas et al. (1990) and Naidich and Taranets (1995), in which the contact angles given in Table 7.6 were reached in a few minutes or tens of minutes. On the other hand, the initial contact angle at 1000°C measured by Tomsia et al. (1989) was 150° and it decreased very slowly through 90° after 7 hours to reach a stationary value of 53° after 30 hours. These slow kinetics cannot be controlled by deoxidization of Al drops because this occurs rapidly at 900°C and above in a high vacuum (see Section 6.4.2). They may, however, be controlled by segregation at the interface of an AlN impurity such as O and XPS analyses showed enrichment of AlN surfaces in O, in the form of Al<sub>2</sub>O<sub>3</sub> or AlON (Jones and Nicholas 1989). However, the contact angle of Al on Al<sub>2</sub>O<sub>3</sub> at 1000°C of 80° is significantly higher than the 50°–60° observed on sintered AlN, so the presence of Al<sub>2</sub>O<sub>3</sub> or an oxynitride would be a barrier to wetting. Therefore, spreading kinetics may be controlled by the elimination of these oxide films on AlN, as in the case of SiC at temperatures below 1000°C. Liquid Al can activate the *in situ* “cleaning” of AlN surface by forming volatile Al suboxide (for example  $4(\text{Al}) + (\text{Al}_2\text{O}_3) \rightleftharpoons 3[\text{Al}_2\text{O}]$ ). Thus, it can be concluded that the good wetting observed ultimately in the Al/AlN system is not due to an effect of impurities but rather to intrinsic interactions between Al and AlN. The interface between Al and AlN should be similar to that between Si and SiC from energetic point of view.

Figure 7.20 shows the change with temperature of the stationary contact angle for the Al/AlN system, measured by the sessile drop technique in high vacuum. Between 900 and 1150°C, the contact angle decreases slowly as for non-reactive couples. Two important changes occur in the low- and high-temperature ranges. A dramatic increase in contact angle is observed at low temperatures, indicating that the kinetics of Al drop and AlN surface deoxidization are too slow to be effective in times typical of sessile drop experiments. A contact angle close to zero is observed at high temperatures, but the fundamental significance of this observation is unclear because the intense evaporation of liquid Al associated with surface roughness of the substrate can produce an apparent decrease in  $\theta$  (see Figure 3.3).

This analysis of the literature on the Al/AlN system reveals the complexity of the surface chemistry of AlN that is influenced strongly, and probably dominated, by oxygen even though the results do not exclude possible effect of other impurities, for instance carbon. A detailed study by spectroscopic techniques, for instance XPS, of the surface chemistry of AlN after heat treatment at different temperatures is needed to clarify the wettability of this ceramic by liquid metals.

Literature data for the wetting behaviour of low or moderate melting point metals on AlN in a high vacuum are reported on Table 7.7. Large non-wetting contact angles are observed, usually in the range 130–150° (it is noteworthy that



**Figure 7.20.** Contact angle versus temperature plot of sessile drops of Al on AlN in a high vacuum. Data from work reported in (Naidich and Taranets 1995).

**Table 7.7.** Wetting by pure metals on sintered AlN under high vacuum.

Metal	$T_{\min} - T_{\max}$ (°C)	$\theta(T_{\min}) - \theta(T_{\max})$ (deg)
Sn	250-1150	130-125 <sup>(1)</sup>
	900	142 <sup>(2)</sup>
In	200-700	132-125 <sup>(1)</sup>
Ga	400-1000	120-110 <sup>(1)</sup>
Pb	350-750	148-137 <sup>(1)</sup>
	420-540	154-143 <sup>(3)</sup>
Ge	950-1200	122-114 <sup>(1)</sup>
Ag	1000	134 <sup>(1)</sup>
	1000	135 <sup>(4)</sup>
Au	1100-1250	138-134 <sup>(1)</sup>
Cu	1100-1200	123-118 <sup>(1)</sup>
	1150	135 <sup>(5)</sup>
	1150	134 <sup>(2)</sup>
	1150	135 <sup>(4)</sup>

<sup>(1)</sup> (Naidich and Taranets 1995), <sup>(2)</sup> (Tomsia et al. 1989), <sup>(3)</sup> (Rhee 1970b), <sup>(4)</sup> (Rhee 1970c)

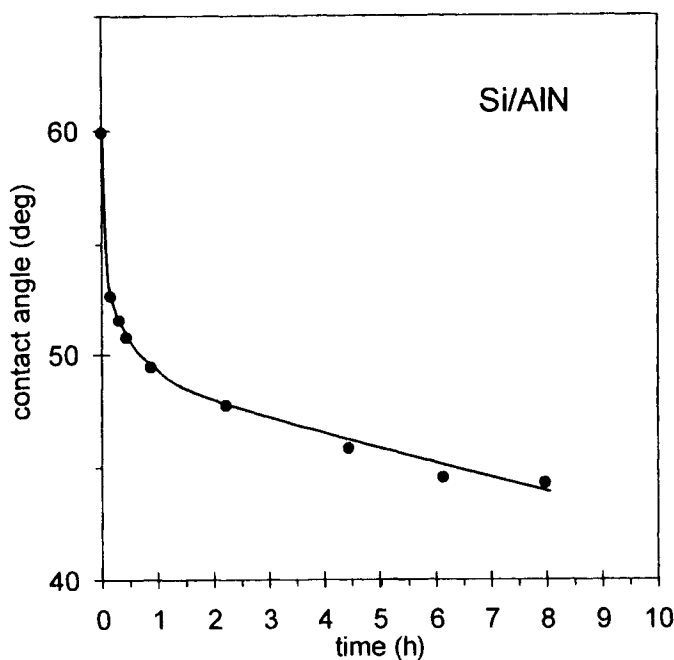
<sup>(5)</sup> (Nicholas et al. 1990)

these values are the same as those observed on polycrystalline oxides). These values suggest the occurrence of weak, van der Waals, interactions between AlN surfaces and the metals, including Cu. However, these results are in disagreement with those, both experimental and theoretical, of a comparative study of the bonding of Cu with  $\text{Al}_2\text{O}_3$  and AlN (Ohuchi and Kohyama 1991). Both ceramics were fabricated *in situ* in an ultrahigh vacuum. The  $\text{Al}_2\text{O}_3$  surface was obtained by thermal oxidation of Al using microleaks of  $\text{O}_2$  and the AlN surface was formed by direct nitridation of clean Al using a nitrogen ion beam. Monitoring of the photoemission spectra during Cu deposition was used to follow the evolution of chemical bonding. In the case of Cu deposition on  $\text{Al}_2\text{O}_3$ , no significant reduction of either Cu or substrate energy levels was observed, indicating that interaction between Cu and  $\text{Al}_2\text{O}_3$  is weak. On the contrary, very different photoemission features were observed during Cu deposition on AlN with a shift in the binding energy of Cu and an increased intensity of characteristic peaks. These results were interpreted by Ohuchi and Kohyama as signs of the formation of a chemical bond between Cu and AlN. This conclusion agrees with theoretical results of electronic structure and bonding of Cu on AlN obtained by first-principle calculations (Ohuchi and Kohyama 1991). Indeed, the total energy of the system decreased with the development between Cu and Al atoms of a metal-like interaction. The disagreement between the wetting behaviour and the electronic structure of the Cu/AlN interface can be explained by assuming that surfaces of sintered AlN used in the wetting experiments were oxidized.

Literature reports of the wetting behaviour of the Cu/AlN system (Table 7.7) do not mention any significant reactivity between Cu and AlN. For instance, Rhee (1970c) observed no severe chemical reaction and reported that a flat interface boundary was maintained throughout the experiment. In view of the data presented in Figure 7.19, this is rather surprising. A more precise calculation of  $X_{\text{Al}}^{\text{eq}}$  resulting from AlN dissociation into Cu (reaction 7.11), carried out using experimental values of activity of Al in Cu-Al alloys (Hultgren et al. 1973) and taking  $P_{\text{N}_2} = 10^{-9}$  atm, leads to  $X_{\text{Al}}^{\text{eq}} = 0.25$  at  $1100^\circ\text{C}$  (for  $P_{\text{N}_2} = 10^{-8}$  atm,  $X_{\text{Al}}^{\text{eq}} = 0.17$ ). These values indicate a considerable reactivity so there is again a disagreement between calculations and experimental findings, suggesting that the barriers of wetting which seem to exist on the AlN surface are also barriers of reactivity as for SiC.

Naidich and Taranets (1995) reported contact angles of ferrous metals on AlN for temperatures in the range  $1500$ – $1600^\circ\text{C}$ . The values were  $95^\circ$  and  $105^\circ$  for Ni and Pd much lower than those in Table 7.7 for low or moderate melting point metals. Since the reactivity barriers existing at low temperatures (i.e., oxide films on AlN) are unlikely to be present at temperatures as high as  $1500^\circ\text{C}$ , a strong reactivity

between Ni or Pd and AlN is expected (Figure 7.19). Interfacial reactions can affect contact angles both by changing the geometry at the triple line and by modifying the composition of the liquid.



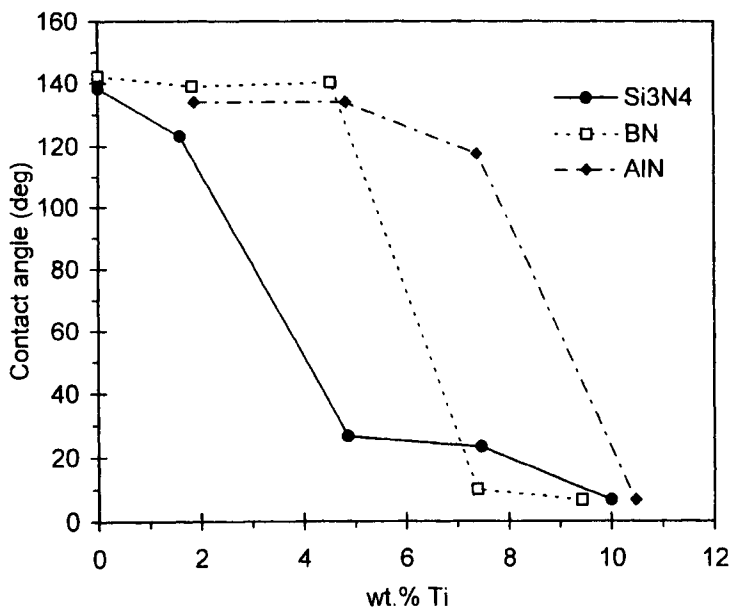
**Figure 7.21.** Contact angle versus time for Si on AlN at 1430°C in an  $\text{H}_2/\text{H}_2\text{O}$  flowing buffer gas under a total pressure of one atmosphere ( $P_{\text{O}_2} = 8.7 \times 10^{-21}$  atm). Data from work reported in (Barsoum and Ownby 1981).

The only other element that wets AlN for which data are available is Si (Barsoum and Ownby 1981, Naidich and Taranets 1995). In the investigation by Barsoum and Ownby (1981), AlN was in the form of layers produced by a variant of the CVD process and a  $\text{H}_2/\text{H}_2\text{O}$  flowing buffer gas at a pressure of 1 atm was employed to keep the  $\text{O}_2$  partial pressure at a level close to  $10^{-20}$  atm. No precision was given for  $P_{\text{N}_2}$  in the gas but  $\text{N}_2$  is generally present in gas mixtures as an impurity at the ppm level, which would lead to  $P_{\text{N}_2} = 10^{-5}$ – $10^{-6}$  atm. This value is much higher than  $P_{\text{N}_2}$  in high vacuum environments, thus increasing the stability of AlN. At the melting temperature of Si, the contact angles are close to 60°, and then decrease to about 45° in 5 hours (Figure 7.21). Such contact angle variations



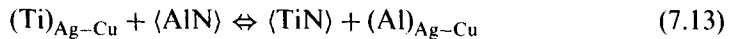
with time can be due either to an *in situ* modification of the surface chemistry of AlN, like for Al on AlN, but cleaning of AlN surfaces is expected to occur rapidly at 1430°C, or to reactions between molten Si and AlN (since the calculated equilibrium molar fraction of Al dissolved in Si at 1700K and for  $P_{N_2} = 10^{-5}$  atm is 0.04). Some of this decrease may result also from evaporation at high temperature in the flowing buffer gas, that produces receding contact angles. Whatever the reason for the slow kinetics, Figure 7.21 indicates the formation of a strong Si/AlN interface. This conclusion is similar to that drawn for molten Si on covalent SiC, for which the contact angle was also close to 40°.

Improved wetting by the metals of Table 7.7 on AlN can be obtained by Al additions, as suggested by the low contact angle and the high work of adhesion observed in the Al/AlN system. Naidich and Taranets (1998) found that the wetting of Sn on AlN at 1100°C in a high vacuum was greatly improved by Al additions. For instance, with 60 at.% Al in Sn, a contact angle of 20° was observed after 35 min and the  $\theta$ - $X_{Al}$  isotherm passes through a minimum as does that for Sn-Al/ $Al_2O_3$  (see Figure 6.32).



**Figure 7.22.** Contact angles of Cu-Ti alloys on Si<sub>3</sub>N<sub>4</sub>, BN and AlN at 1150°C in a vacuum (Nicholas et al. 1990) [2].

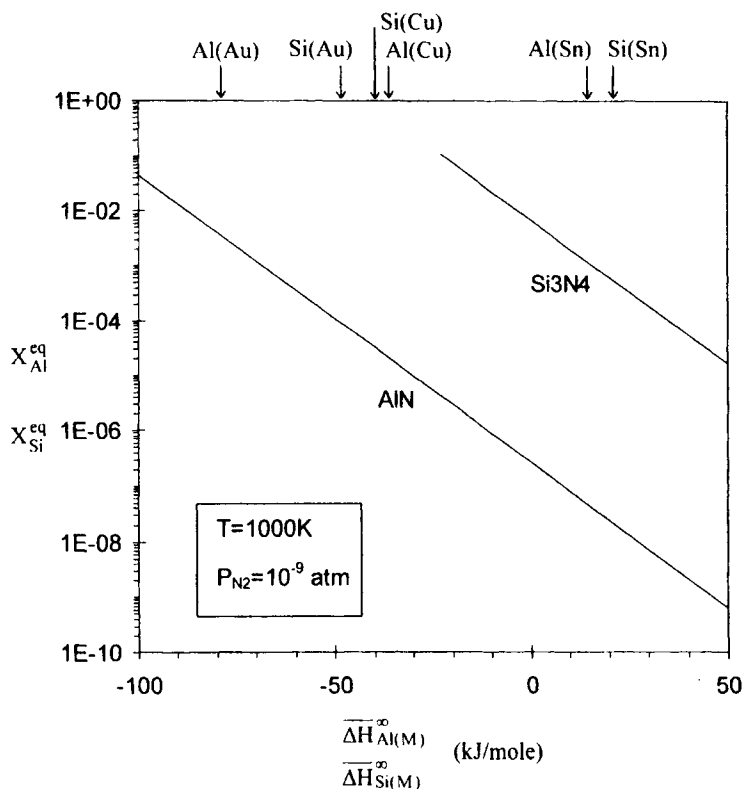
Naidich and Taranets (1995) attempted to improve wetting of Cu, Ge and Sn on AlN at 1150°C in a high vacuum by additions of up to 6 at.% of Cr, Ta, Nb, V and Ti which have a high affinity for N. Although some improvement in wetting was observed, contact angles lower than 90° were achieved only with Ti. The addition of 10 wt.% Ti in Cu at 1150°C produced a decrease of the contact angle from 135° to close to zero (Figure 7.22) with formation at the interface of a few microns thick continuous layer of wettable metal-like TiN (see Section 7.2). Similarly, very low contact angles have been achieved at temperatures close to 900°C in a high vacuum with Ag-Cu alloys containing 1 to 5 wt.% of Ti (Tomsia et al. 1989, Nicholas et al. 1990, Loehman and Tomsia 1992). It was found that a continuous layer of hypostoichiometric TiN ( $\text{TiN}_{0.7}$ ) formed at the interface in accord with the reaction:



Al liberated by this reaction can react with the excess Ti to form the  $\text{Al}_3\text{Ti}$  intermetallic (Tomsia et al. 1989).

Finally, contact angles less than 30° were measured for Ni alloyed with 2 wt.% of Ti, Zr or Hf on sintered AlN at 1500°C in gettered Ar (Trontelj and Kolar 1978). In all cases, dense reaction product layers of nitrides, up to several tens of microns in thickness, were formed at the interface.

**7.1.2.2 Wetting of  $\text{Si}_3\text{N}_4$ .**  $\text{Si}_3\text{N}_4$  is similar to AlN in its structure (hexagonal), type of bonding (predominantly covalent), complex chemistry (it usually contains several percent of sintering aids, mainly  $\text{Y}_2\text{O}_3$  and  $\text{Al}_2\text{O}_3$ ) and oxidizability. Even after a few minutes exposure in air at room temperature, it forms 0.5–3 nm thick layers which appear to be  $\text{Si}_2\text{N}_2\text{O}$  (Maguire and Augustus 1972, Raider et al. 1976, Ljungberg and Warren 1989). These layers are relatively stable in temperature and several hours at 1140°C in an ultrahigh vacuum are needed to remove oxygen (Maguire and Augustus 1972). Of the three nitrides in Table 7.5,  $\text{Si}_3\text{N}_4$  is the least stable and its stability is even lower when in contact with liquid metals with a high affinity for Si, such as Cu and Au (Figure 7.23). In sessile drop experiments carried out in a high vacuum at temperatures of 1100°C or below, no evidence of reactions was found (Ljungberg and Warren 1989, Tomsia et al. 1989). This confirms the presence of barriers to reactivity on the surface of  $\text{Si}_3\text{N}_4$  resulted from a reduced atomic mobility i.e., a low value of the evaporation coefficient  $\alpha$  (Table 7.5). These barriers can be enhanced by oxide or oxynitride layers, as for AlN. The presence of such layers can explain also the high contact angles measured for low or moderate melting point metals and alloys which do not form stable nitrides. As for AlN, these



**Figure 7.23.** Calculated values of molar fractions of Al and Si in liquid metal M in equilibrium with AlN and Si<sub>3</sub>N<sub>4</sub> respectively as a function of the partial enthalpy of mixing of the nitride metal at infinite dilution in M. Arrows indicate values of  $\Delta H_{Al(M)}^\infty$  and  $\Delta H_{Si(M)}^\infty$  for some metals M which do not form stable nitride.

values lie between 120° and 170° at temperatures of no more than 1100°C (Table 7.8) and are close to those obtained for non-reactive metals on polycrystalline oxides which can have very rough surfaces. However, in the case of the Cu/Si<sub>3</sub>N<sub>4</sub> system at 1150°C, some mobility of Cu drops on the substrate surface was detected (Tomsia et al. 1989) ; such drop mobility is often observed in systems in which interfacial reaction leads to formation of bubbles. Moreover, an exceptional decrease in contact angle was observed at a temperature between 1100°C and 1200°C by Allen and Kingery (1959) for Sn (Table 7.8). This result suggests that the barriers at low temperatures consist of oxide or oxynitride layers (contact angles of various metals on Si<sub>3</sub>N<sub>4</sub> and Si<sub>2</sub>N<sub>2</sub>O are very close at 900°C (Tomsia et al.

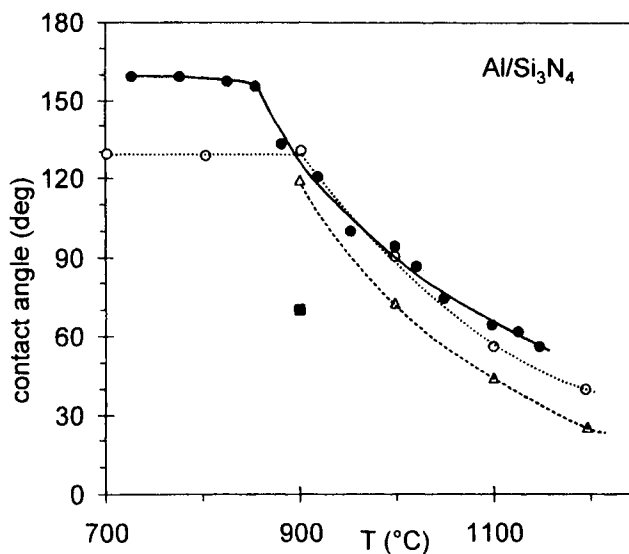
1989)), but these disappear at high temperature to permit a direct contact and reactions between Sn and  $\text{Si}_3\text{N}_4$ .

**Table 7.8.** Wetting of  $\text{Si}_3\text{N}_4$  in a high vacuum by pure metals and alloys which do not form stable nitrides.

Liquid	T (°C)	$\theta$ (deg)	$\text{Si}_3\text{N}_4$	Reference
Sn	1100	144	HIP	(Ljungberg and Warren 1989)
Cu	1100	131	1% $\text{Y}_2\text{O}_3$	
Au	1100	157		
Ag	1100	155		
Au-42.5 at.%Ni	1050	120	pressureless sintered with $\text{Y}_2\text{O}_3$ and $\text{Al}_2\text{O}_3$	(Paulasto et al. 1996)
Sn	900	153	no additives	(Tomsia et al. 1989)
Cu	1150	115-130 (*)		
Ag-28 wt.%Cu	900	142		
Cu	1150	135	6 wt.% $\text{La}_2\text{O}_3$ 4 wt.% $\text{Al}_2\text{O}_3$	(Nicholas et al. 1990)
Sn	800	168	sintered	(Allen and Kingery 1959)
	1100	154	95.1 % purity	
	1200	29		

(\*) mobile sessile drops

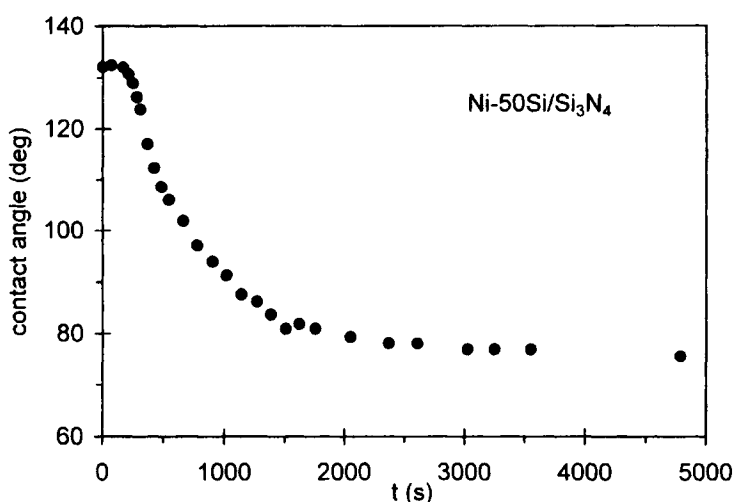
In a low  $\text{P}_{\text{O}_2}$  atmosphere generated by a flowing buffer gas, pure Si wets  $\text{Si}_3\text{N}_4$  produced by CVD (Barsoum and Ownby 1981). On melting, the initial contact angle is close to  $70^\circ$  and a decrease to  $60^\circ$  is observed after 1 hour. Although some dissociation of  $\text{Si}_3\text{N}_4$  occurs at the melting point of Si, this should not modify the nature of solid/vapour or solid/liquid interfaces, and thus the Si/ $\text{Si}_3\text{N}_4$  couple can be considered as non-reactive from the point of view of wettability. Slow wetting kinetics and stationary contact angles close to  $50^\circ$  have been observed in Ar (Li and Hausner 1992) and He (Duffy et al. 1980) atmospheres. The achievement of wetting in this system indicates the formation of a chemical bond localized between Si and  $\text{Si}_3\text{N}_4$ , as in the similar non-reactive couples Al/ $\text{AlN}$  ( $\theta \cong 55^\circ$ ) and Si/ $\text{SiC}$  ( $\theta \cong 40^\circ$ ).



**Figure 7.24.** Contact angle versus temperature for Al on  $\text{Si}_3\text{N}_4$ . Full circles: (Nicholas et al. 1990), open circles: (Ljungberg and Warren 1989), triangles: (Naka et al. 1987), square: (Tomsia et al. 1989).

Because AlN has a higher thermodynamic stability than  $\text{Si}_3\text{N}_4$  (Table 7.5), Al may react with  $\text{Si}_3\text{N}_4$  forming AlN. The contact angle versus temperature curves of Figure 7.24 for Al on  $\text{Si}_3\text{N}_4$  show a non-wetting to wetting transition, similar to transitions occurring for oxidizable metals, as discussed in Section 6.4.2 (see Figures 6.20 and 6.25). At low temperatures, large non-wetting contact angles are observed because both Al and  $\text{Si}_3\text{N}_4$  are oxidized. At about  $1100^\circ\text{C}$ , contact angles much lower than  $90^\circ$  are obtained that indicate the establishment of direct contact between Al and  $\text{Si}_3\text{N}_4$ . The transition from non-wetting to wetting appears to occur at  $950\text{--}1000^\circ\text{C}$  in the experiments of Figure 7.24, but the transition temperature depends strongly on the furnace atmosphere and the substrate purity. For instance, a stationary wetting contact angle ( $\theta = 71^\circ$ ) was reached in 40 minutes at  $900^\circ\text{C}$  in a high vacuum (Tomsia et al. 1989). It is possible, and even probable, that wetting in this system can be achieved at even lower temperatures provided the Al and  $\text{Si}_3\text{N}_4$  surfaces are cleaned. Characterization of Al/ $\text{Si}_3\text{N}_4$  interfaces of sessile drop specimens by SEM or microprobe analysis did not reveal any evidence of reaction between Al and  $\text{Si}_3\text{N}_4$  at the micrometer scale (Tomsia et al. 1989). However, higher spatial resolution techniques revealed the formation of submicronic layers with a complex chemistry, consisting of sialons (Ning et al. 1987) and/or a mixture of  $\text{SiO}_2$  and  $\text{Al}_2\text{O}_3$  (Tomsia et al. 1989).

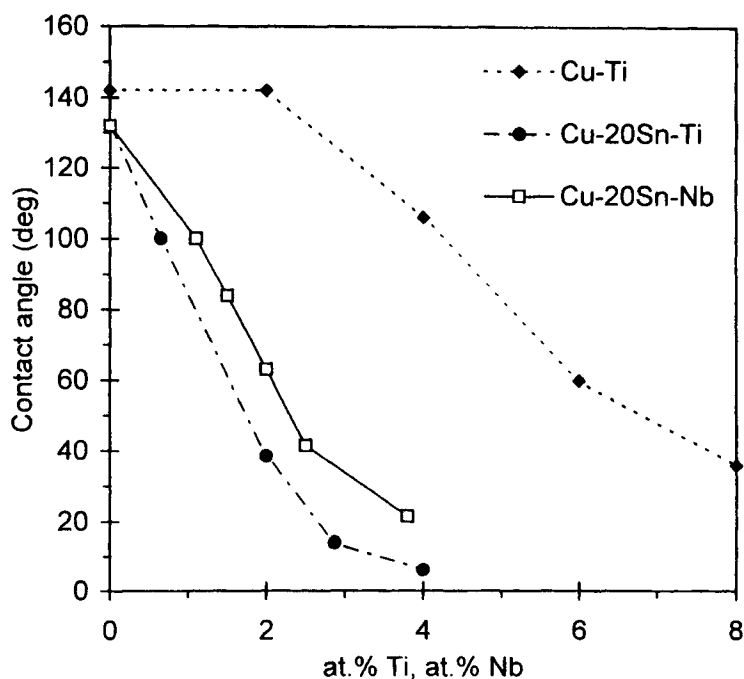
In view of the high work of adhesion of Si on  $\text{Si}_3\text{N}_4$  and the comparatively low surface energy of molten Si, an improvement in the wetting by inert pure metals can be expected by the addition of Si. Figure 7.25 shows the spreading kinetics at  $1200^\circ\text{C}$  in a high vacuum of a Ni-50 at.% Si alloy on  $\text{Si}_3\text{N}_4$  containing  $\text{Y}_2\text{O}_3$  and  $\text{Al}_2\text{O}_3$  as sintering aids. A wetting contact angle ( $\theta = 75^\circ$ ) is achieved after several thousands of seconds (van Dal 1997). Because no chemical reaction was detected by SEM and microprobe analysis, the slow spreading kinetics may result from an *in situ* cleaning of  $\text{Si}_3\text{N}_4$  surface by Si, acting as Al in the Al/AlN system (see Section 7.1.2.1).



**Figure 7.25.** Contact angle versus time for Ni-50 at.% Si on  $\text{Si}_3\text{N}_4$  at  $1200^\circ\text{C}$  in a high vacuum (van Dal 1997).

Even lower contact angles ( $\theta = 40^\circ$ ) have been obtained at a temperature close to  $1200^\circ\text{C}$  in a high vacuum using a Cu-10 wt.% Ni-7 wt.% Cr alloy. They were attributed to the formation of a continuous layer of the wettable  $\text{Cr}_2\text{N}$  compound that was several tens of microns thick (Xiao and Derby 1995). Similarly, while the Au-Ni alloy does not wet  $\text{Si}_3\text{N}_4$  (Table 7.8), additions of a few at.% of V to the alloy leads to contact angles of  $40\text{--}55^\circ$  with formation of  $\text{VN}_x$  at the interface (Paulasto et al. 1996). Additions of Ti and Nb to pure Cu or Cu-Sn alloys produce a strong improvement in wetting (Figures 7.22 and 7.26). In the Cu-Ti/ $\text{Si}_3\text{N}_4$  system, continuous layers of TiN up to 10 to 20 microns thick were found (Nicholas et al. 1990). A few at.% Ti in Ag-Cu alloys lead to very low contact

angles in the range 0–20° at 850°C and above, with formation at the interface of a bilayer consisting of TiN, formed by the reaction  $(\text{Ti}) + (\text{Si}_3\text{N}_4) \rightleftharpoons (\text{TiN}) + (\text{Si})$  and of Ti silicides formed by reaction between excess Ti in the alloy and Si liberated by the previous reaction (Tomsia et al. 1989, Nicholas et al. 1990, Ljungberg 1992, Nomura et al. 1998, 1999).



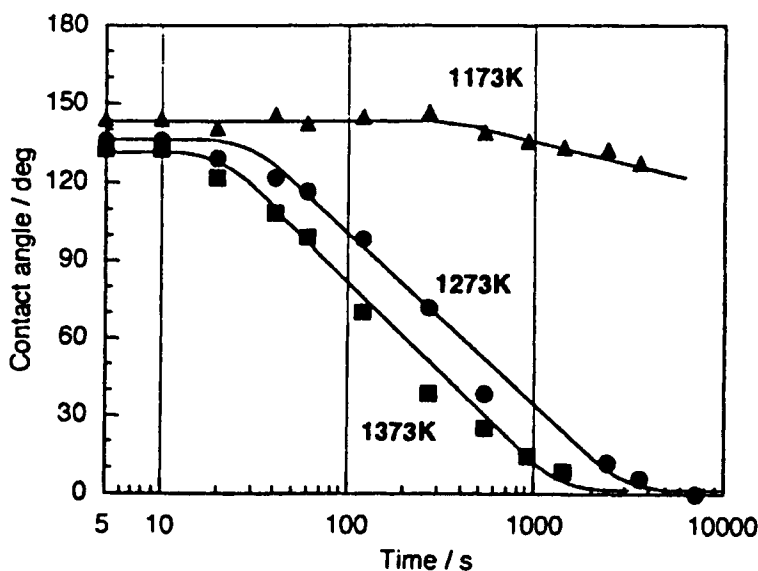
**Figure 7.26.** Contact angle on  $\text{Si}_3\text{N}_4$  at 1150°C (holding time 30 min) as a function of concentration of active element (Ti or Nb) in pure Cu and Cu-Sn alloy. Data from work reported in (Zhuravlev et al. 1998).

**7.1.2.3 Wetting of BN.** At equilibrium, the partial pressure of  $\text{N}_2$  for BN dissociation lies between the values for AlN and  $\text{Si}_3\text{N}_4$  (Table 7.5). In practice, even in a high vacuum the stability of BN is much higher than that predicted by equilibrium thermodynamics because the evaporation coefficient is as low as  $10^{-3}$  (Table 7.5). BN is also an oxidizable ceramic but boron oxide,  $\text{B}_2\text{O}_3$ , is volatile with a partial pressure at 1000°C  $P_{\text{B}_2\text{O}_3} = 10^{-7}$  atm (Chase et al. 1985). Moreover,

because  $B_2O_3$  is liquid at temperatures higher than  $450^\circ\text{C}$ , no retarded evaporation of this oxide is expected. Use of equations (6.26) and (6.27) predicts an evaporation rate of  $B_2O_3$  of several nm/s at  $1000^\circ\text{C}$ , indicating a rapid cleaning of BN (and also of  $B_4C$ ) surfaces at this temperature. In practice, the surface chemistry of BN and its evolution with temperature may be complex due to the presence of O and C impurities in nitride ceramics (Perevertailo et al. 1998). A detailed chemical characterization of BN surfaces in a high vacuum at different temperatures is needed to understand the interaction between BN and liquid metals.

Few studies of wetting of metals on BN exist, the only systematic investigation known to us being that of Naidich (1981) which was performed in the range  $1000\text{--}1500^\circ\text{C}$  using both cubic and hexagonal BN. No oxidation of BN surfaces is expected under these conditions. For metals with a negligible (Ag, Au, Sn) or weak (Ge, Ga, Cu) affinity for both N and B, contact angles lie in the range  $135\text{--}150^\circ$  at  $1000\text{--}1100^\circ\text{C}$  for both structures of BN.

Ferrous metals form contact angles lower than  $90^\circ$  (Naidich 1981). However, these metals have a high affinity for B at  $1500^\circ\text{C}$  (for instance liquid Ni dissolves up to 60 at.% B (Massalski 1990)), so a strong reactivity between these metals and BN is expected and the contact angles are only apparent (see Figure 2.18).



**Figure 7.27.** Contact angle versus time for Al on sintered hexagonal BN in an He-3%  $H_2$  gas. Data from work reported in (Fujii et al. 1993) [24].



Al reacts with BN forming a continuous layer of AlN at the interface and liberating B which reacts with Al to form borides precipitates (Fujii et al. 1993). Figure 7.27 shows results obtained for Al on sintered hexagonal BN (99.7 wt.% purity). In this experiment, the BN substrate was first cleaned in a high vacuum at 1423K for 1 hour before purified He-3% $H_2$  gas was introduced and the temperature was lowered to the experimental value. A pure Al drop was placed *in situ* on the substrate by a dispensed drop device (Figure 3.7.c) allowing the oxide layer on Al to be removed. The initial contact angle was close to  $140^\circ$  as for non-reactive metals on BN but decreased after a few minutes with a spreading rate that was strongly dependent on temperature. Very low contact angles were obtained at 1273K and 1373K in  $10^3$  seconds, and nearly perfect wetting was obtained in  $7 \times 10^3$  seconds at 1273K. Other investigators obtained higher stationary contact angles (in the range  $35$ – $60^\circ$  at 1373K (Naidich 1981, Nicholas et al. 1990)), that are consistent with those for Al on AlN (Figure 7.20) i.e., for Al on the reaction product at the Al/BN interface.

Silicon has an affinity both for B (at  $1500^\circ\text{C}$  Si dissolves up to 17 at.% B (Massalski 1990)) and N (although  $Si_3N_4$  is less stable than BN). Naidich (1981) achieved stationary contact angles of  $95^\circ$  and  $110^\circ$  for Si on cubic and hexagonal BN at  $1500^\circ\text{C}$  in a high vacuum in a few minutes. These values are much higher than those observed for Al, but significantly lower than the  $140^\circ$  or so observed for non-reactive metals. A detailed interpretation of these values is not possible in the absence of information on interfacial reactions which could occur in the Si/BN system.

Additions of Ti to Cu and Ag-Cu allowed very low contact angles to be achieved on BN at  $1150^\circ\text{C}$  (Figure 7.22) and  $950^\circ\text{C}$  (Nicholas et al. 1990). Electron probe micro-analysis revealed the formation of a Ti-rich layer several microns thick at the interface but the nature of Ti compounds (TiN or  $TiB_2$  or both) was not identified.

The wetting behaviour of metals on  $B_4C$  is very similar to that on BN (Naidich 1981). For metals with a negligible or weak affinity for both B and C (Cu, Ag, Ge, Sn), contact angles in the range  $130^\circ$ – $140^\circ$  were observed in a high vacuum at temperatures close to  $1100^\circ\text{C}$ . The addition of metals such as Cr and Ti that form metal-like carbides strongly improved wetting. Again, Al and Si, which form carbides more stable than  $B_4C$ , wet well  $B_4C$  at  $1150^\circ\text{C}$  and  $1430^\circ\text{C}$  respectively. As on BN, ferrous metals that can dissolve large quantities of B and C wet  $B_4C$  well and form an interface that is expected to be non-planar.

### 7.1.3 Concluding remarks

This review of the experimental results for metal/covalent ceramic systems shows that the intrinsic wetting properties in these systems are not well established at

present. Further work is needed using combined studies of the wetting and surface chemistry of ceramics, similar to those carried out by Rado (1997) for SiC. In future studies, to use monocrystalline ceramics is obviously desirable, and when they are not available, CVD layers are preferable to sintered materials.

For metals on “real” materials in neutral gas or high vacuum environments, good wetting is seldom observed at temperatures of 1000°C or less owing to pollution of the ceramic surfaces (SiC, Si<sub>3</sub>N<sub>4</sub>, AlN) by oxygen. At higher temperatures, cleaning of surfaces can occur but the wetting observed in many cases is accompanied by reactivity. Although BN and B<sub>4</sub>C surfaces seem not to be oxidized at temperatures close to 1000°C, non-wetting is still observed for metals such as Pb, Sn and Ag that have a negligible affinity for B, N and C.

At temperatures of 1000°C and above, Al and Si wet covalent ceramics rather well with contact angles close to 50° for both non-reactive (Al/AlN and Si/SiC) and reactive systems (Al/SiC and Al/BN). This behaviour relates well to theoretical studies indicating the formation of metallic or covalent chemical bonds at the interfaces between Al or Si and covalent ceramics. The ability of Al and Si to bond strongly with ceramic surfaces appears to correlate with the degree of covalence (or, equivalently, with the degree of ionicity) of the ceramic, as shown by the data in Table 7.9 for Si on non-reactive solids. A similar tendency is observed for Al on various solids, including solid Al considering the metallic bond in solid Al as a homopolar Al-Al bond (Table 7.9).

**Table 7.9.** Contact angles of Si and Al on solids of variable degree of ionicity.

Liquid/solid	Degree of ionicity (%)	T (°C)	$\theta$ (deg)	$W_a/W_c = (1+\cos\theta)/2$
Si/SiO <sub>2</sub>	51	~ 1410	87 <sup>(1)</sup>	0.53
Si/Si <sub>3</sub> N <sub>4</sub>	30	~ 1410	55 ± 5	0.79 ± 0.04
Si/SiC	11	~ 1410	40 ± 10	0.87 ± 0.05
Si/Si	0	~ 1410	14 <sup>(2)</sup>	0.98
Al/CaF <sub>2</sub>	89	700-1000	130-100 <sup>(3)</sup>	0.18-0.41
Al/Al <sub>2</sub> O <sub>3</sub>	63	700-1000	90-80 <sup>(3)</sup>	0.50-0.59
Al/AlN	43	1000	53	0.80
Al/Al	0	660	~ 0 <sup>(4)</sup>	~ 1

<sup>(1)</sup> (Sangiorgi et al. 1988), <sup>(2)</sup> (Naidich et al. 1975), <sup>(3)</sup> (Naidich et al. 1983), <sup>(4)</sup> (see Section 5.1)

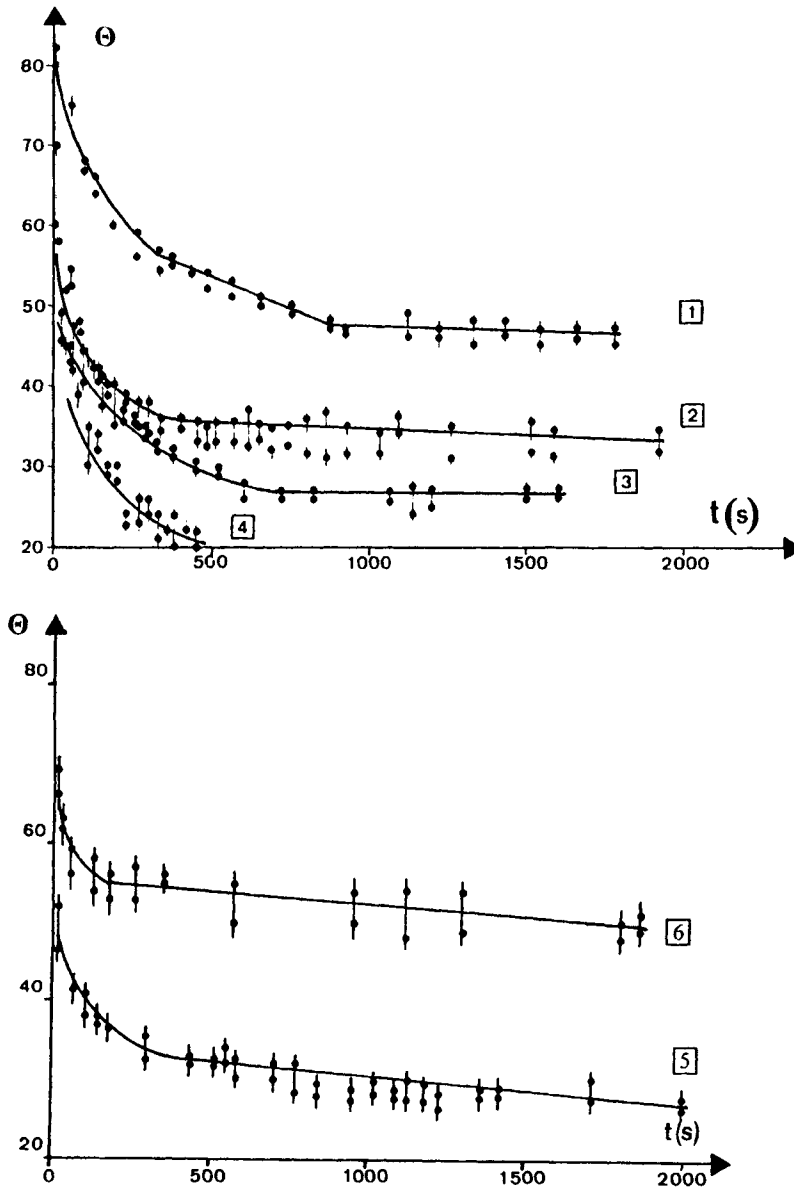
## 7.2. METALS ON METAL-LIKE CERAMICS

Refractory transition metal carbides, nitrides and borides (e.g., Table 7.10) are of great interest for both practical purposes and theoretical studies. This class of solids exhibits very high hardnesses and melting points, as indeed do many *covalent* compounds. However, most monocarbides (MeC) and mononitrides (MeN) crystallize in the sodium chloride structure, generally found with *ionic* compounds. Further, these ceramics also have aspects of *metallic* behaviour such as good thermal and electrical conductivities. This partly metallic bonding has repercussions on interfacial and adhesion properties with metals and we have seen in Sections 6.3 (Table 6.5) and 7.1.2 (Figure 7.22) that improvement in wetting and adhesion in metal/ionocovalent ceramic systems is obtained by creating metal-like compounds at the metal/ceramic interface.

**Table 7.10.** Wetting by Cu of metal-like carbides in a high vacuum at 1100°C (Ramqvist 1965). The equilibrium molar fraction of carbide metal Me dissolved in Cu,  $X_{\text{Me(Cu)}}^{\text{eq}}$ , is calculated from equation (7.16). Data for  $\Delta G_f^0$  (reference state: pure liquid metal Me) come from (Rosenqvist 1983) except for  $\text{Mo}_2\text{C}$  and  $\text{HfC}$  (Kubaschewski and Alcock 1979). Data for  $\overline{\Delta H}_{\text{Me(Cu)}}^\infty$  come from (Niessen et al. 1983).

Carbide $\text{Me}_n\text{C}_m$	$\theta$ (deg)	$W_a / W_c$	$\Delta G_f^0$ (kJ/g atom C)	$\overline{\Delta H}_{\text{Me(Cu)}}^\infty$ (kJ/mole)	$X_{\text{Me(Cu)}}^{\text{eq}}$
$\text{Mo}_2\text{C}$	18	0.98	-84	82	$2 \times 10^{-5}$
WC	20	0.97	-57	101	$10^{-6}$
$\text{Cr}_3\text{C}_2$	47	0.84	-59	51	$3 \times 10^{-3}$
$\text{NbC}_{0.97}$	70	0.67	-140	12	$2 \times 10^{-6}$
TaC	78	0.60	-163	9	$3 \times 10^{-7}$
TiC	112	0.31	-173	-40	$8 \times 10^{-6}$
ZrC	127	0.20	-179	-110	$2 \times 10^{-3}$
HfC	134	0.15	-216	-81	$7 \times 10^{-6}$

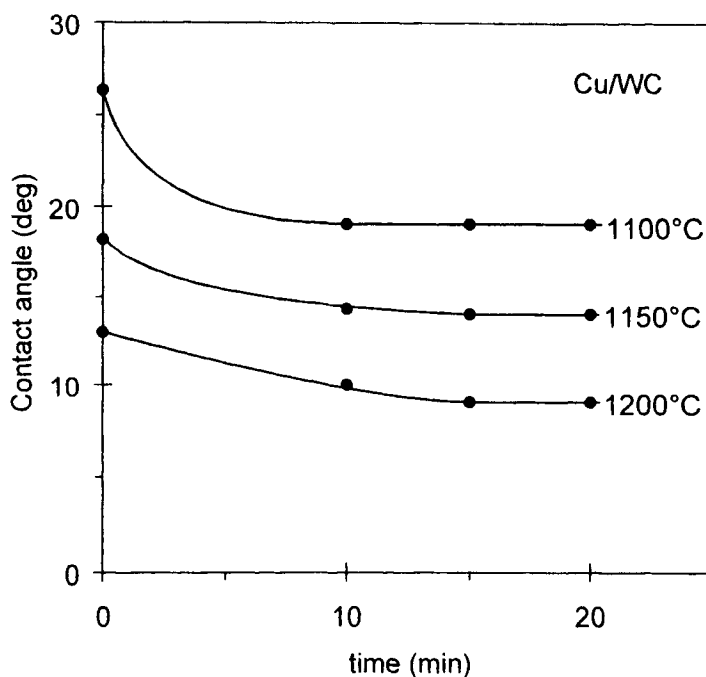
In fundamental studies of ceramic wetting, many difficulties can arise from the lack of monocrystalline high-purity materials. In most cases, sintered materials have been used that, even when free of sintering additives, contain typically 0.1 wt.% and more of oxygen and other impurities that can strongly affect wettability (Figure 7.28). Because of the high affinity of transition metals of Groups IVB and VB for O, as compared to C or N, these compounds are oxidizable and this exerts a



**Figure 7.28.** Variation of contact angle with time of Fe presaturated with  $\text{TiB}_2$  on different  $\text{TiB}_2$  substrates: sintered  $\text{TiB}_2$  with 0.68 wt.% oxygen (1), 0.33 wt.% oxygen (2), 0.26 wt.% oxygen (3), CVD  $\text{TiB}_2$  (4), sintered  $\text{TiB}_2$  with 0.30 wt.% oxygen (5), the same as (5) after surface oxidation (6). From (Ghetta et al. 1992) [25].

strong influence on wetting and adhesion. Finally, several of these substances possess a large range of non-stoichiometry. Bulk non-stoichiometry can be easily controlled during processing of the material but it is difficult to control surface non-stoichiometry, which may be very different (Lequeux 1997). Note that studies of the wettability of metal-like ceramics by liquid metals were performed in attempts to produce new cermets, mainly in the period 1960-75, and hence did not benefit from modern techniques for chemical analyses of surfaces and interfaces.

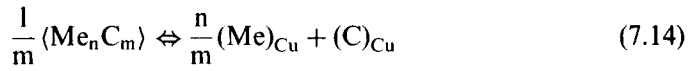
Table 7.10 presents results obtained for pure Cu on different nearly stoichiometric carbides. These results come from the extensive study performed by Ramqvist (1965) on the wetting by metals on various sintered metallic carbides carried out in a high vacuum. The contact angles given on Table 7.10 are equilibrium values obtained generally in less than 15 minutes. However, the change in  $\theta$  between  $t = 0$  and  $t = 15$  minutes was only a few degrees in many cases (Figure 7.29) indicating that a nearly equilibrium state was reached very rapidly on melting.



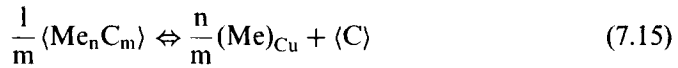
**Figure 7.29.** Contact angles of Cu on WC plotted as a function of time. Data from work reported in (Ramqvist 1965).

The results in Table 7.10 show contact angles varying from values typical of metal/oxide systems with van der Waals interactions at the interface ( $\theta \approx 130^\circ$ ,  $W_a/W_c \approx 0.15$ ) to values typical of metal/metal systems ( $\theta \approx 20^\circ$ ,  $W_a/W_c \approx 0.95$ ). It is noteworthy that the degree of wetting of Cu on metallic W (see Section 5.2) is nearly equal to that on WC.

In Section 6.1, we discussed a correlation between wettability and reactivity in metal/oxide systems: for a molar fraction of dissolved oxygen greater than  $10^{-5}$ , the contact angle decreases from about  $130^\circ$  to  $0^\circ$  (Figure 6.2). To check if a similar correlation holds for metal/metallic carbide systems, the reactivity between Cu and different carbides at  $1100^\circ\text{C}$  can be calculated for the dissolution of carbide  $\text{Me}_n\text{C}_m$  in Cu:



As the stoichiometric carbide is also in equilibrium with free graphite, meaning that the activity of C in the carbide is equal to that in pure graphite i.e., to unity (except for  $\text{Mo}_2\text{C}$  for which according to the Mo-C phase diagram (Massalski 1990) the activity of C is lower but close to unity), this yields:

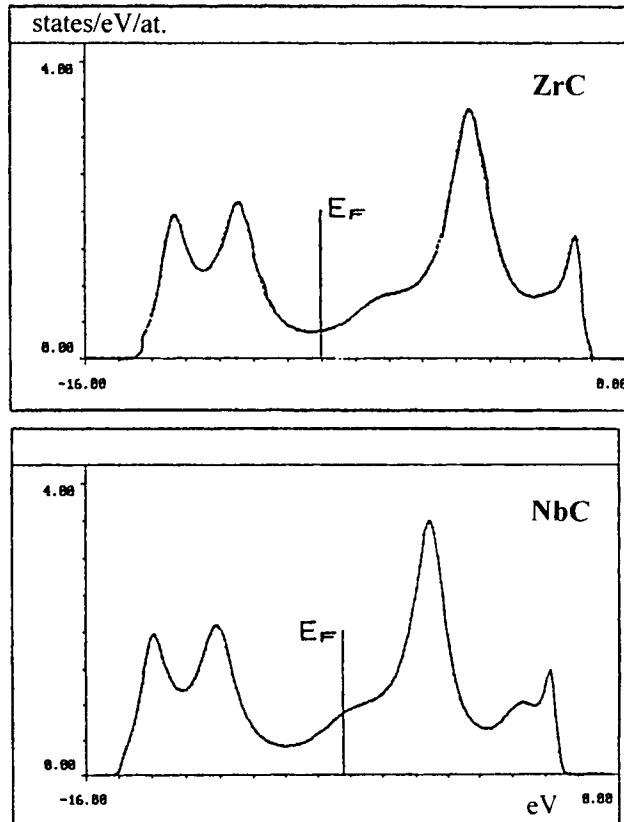


For reaction (7.15), the equilibrium molar fraction of carbide metal Me dissolved in Cu is:

$$X_{\text{Me}(\text{Cu})}^{\text{eq}} = \exp \left[ \frac{m}{nRT} \left( \Delta G_f^0 - \frac{n}{m} \overline{\Delta H}_{\text{Me}(\text{Cu})}^\infty \right) \right] \quad (7.16)$$

In this equation,  $\Delta G_f^0$  is the standard Gibbs energy of formation of the carbide  $\text{Me}_n\text{C}_m$  from graphite and pure liquid metal Me and  $\overline{\Delta H}_{\text{Me}(\text{Cu})}^\infty$  is the partial enthalpy of mixing of Me at infinite dilution in Cu. Results in Table 7.10 show that, although some correlation exists between contact angles and Gibbs energies of formation of carbides, there is no correlation between  $\theta$  and  $X_{\text{Me}(\text{Cu})}^{\text{eq}}$ . This means that the element Me is not active at Cu/carbide interfaces at a level of 0.1 at.% or less. Thus, the high values of  $W_a$  observed for carbides lying between  $\text{Mo}_2\text{C}$  and

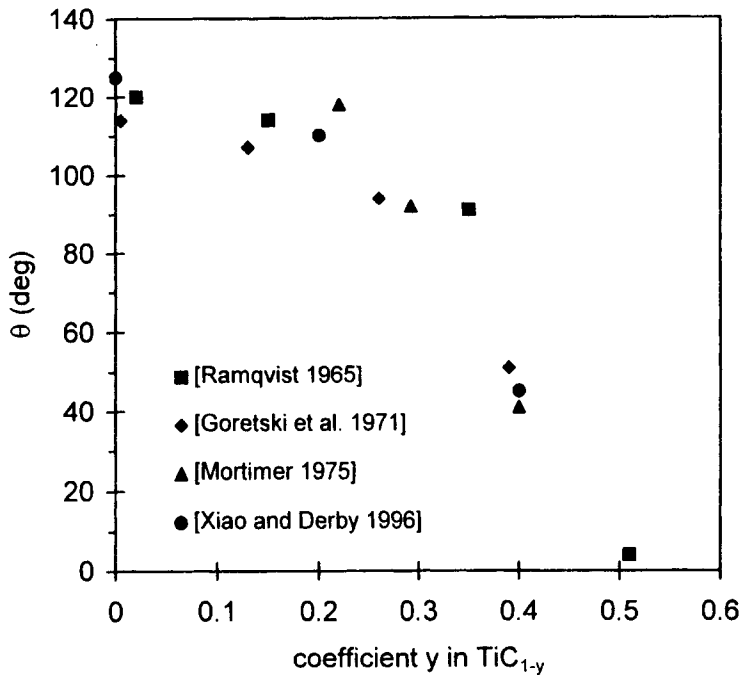
TaC in Table 7.10 have to be explained by the nature of the interfacial bonding between Cu and the carbide and not by an effect of dissolved carbide metal.



**Figure 7.30.** Density of electronic states (resulting from overlapping of d-orbitals of the metal and p-orbitals of carbon) and location of the Fermi level ( $E_F$ ) for ZrC and NbC (Le 1990).

Electronic structure calculations for transition metal carbides (Neckel 1990, Le 1990, Le et al. 1991) reveal significant contributions to cohesion by all three main types of chemical bonding. Covalent bonds are due to the formation of molecular orbitals by combining atomic d-orbitals of the metal with p-orbitals of C. Ionic bonds result from charge transfer from the metal to the non-metal. Metallic bonds are due to s electrons and also to a non-vanishing density of d-p electronic states (DOS) existing at the Fermi level (Figure 7.30). The main difference between the DOS curves calculated for stoichiometric ZrC, TiC or HfC and NbC, TaC or VC is

the position of the Fermi level. For carbides of transition metals of Group IVB (such as ZrC), the Fermi level is located at the minimum of DOS curve, while for carbides of metals of Group VB (such as NbC), it is shifted to the right of the minimum of the DOS curve i.e., towards antibonding states. This results in a low thermodynamic stability of carbides such as NbC compared to carbides such as ZrC.



**Figure 7.31.** The influence of stoichiometry of  $\text{TiC}_{1-y}$  on the wetting behaviour of Cu at 1100–1150°C.

The good adhesion and wetting observed between Cu and carbides of Mo, W, Cr, Nb and Ta can be explained by considering that metallic bonding can be established at the interface, although covalent and other types of interactions cannot be excluded. More surprising are the experimental results on TiC, ZrC and HfC for which  $W_a$  values are several times lower than those found on NbC and TaC, despite a significant DOS at the Fermi level. However, the experimental results in Table 7.10 for TiC, ZrC and HfC are questionable. This appears clearly in the case of TiC and TiN. Indeed, Ramqvist (1965), as well as other authors



(Livey and Murray 1956, Rhee 1970c, Xiao and Derby 1996), found non-wetting of Cu on stoichiometric TiC ( $\theta = 110\text{--}125^\circ$  at the melting temperature of Cu, see Figure 7.31 for  $y = 0$ ). However, other experiments carried out in very low  $P_{O_2}$  atmospheres led to much lower contact angles ( $\theta \cong 60^\circ$  (Whalen and Humenik 1960, Li 1993)). Similar differences have been found for Cu on stoichiometric TiN in high vacuum ( $\theta = 110^\circ$  (Xiao and Derby 1996) and  $\theta = 60^\circ$  (Lequeux et al. 1998)).

There are at least two possible explanations for the different results obtained in the Cu/TiC and Cu/TiN systems: (i) the non-wetting observed on stoichiometric TiC (or TiN) is due to pollution of the ceramics by oxygen (Li 1993), and (ii) the low final contact angles observed by some authors on initially stoichiometric substrates are due to the development at the substrate surface of an hypostoichiometric zone. This could have been caused, in the case of TiC, by C losses as CO produced by reaction with the O present in these materials at a level of 0.1 wt.% or by  $N_2$  evaporation in the case of TiN. Moreover, SIMS and nuclear microprobe analyses performed by Lequeux (1997) on *nominally* stoichiometric TiN substrates before being used in wetting experiments revealed a hypostoichiometric surface layer several tens of nanometers thick, probably formed during the cutting and polishing of the substrates. Therefore, the contact angles close to  $60^\circ$  found by Lequeux et al. (1997, 1998) were obtained in fact on hypostoichiometric TiN surfaces.

To eliminate these uncertainties about surface chemistry, further experiments were performed with TiN in a  $N_2 + H_2$  atmosphere. The role of  $H_2$  was to suppress or minimise oxidation caused by the reaction  $2TiN + (3/2)O_2 \rightleftharpoons Ti_2O_3 + N_2$  by decreasing  $P_{O_2}$ . The role of  $N_2$  was mainly to ensure a stoichiometric TiN surface. In these conditions, the contact angle of Cu on TiN was found to be  $96 \pm 2^\circ$  (van Deelen et al. 1998). This value corresponds to a  $W_a/(2\sigma_{LV})$  ratio of 0.45 higher than for pure Cu on ionocovalent oxides (0.20) but lower than for Cu on WC or  $Mo_2C$  ( $\approx 0.98$ , Table 7.10).

In the case of TiC, further work on substrates with well characterised bulk and surface compositions is needed to elucidate the diverging results of the literature. Whatever the explanation, it has to be recognized that the wettability of TiC and TiN, and probably of other stable and oxidizable carbides and nitrides such as ZrC, ZrN, HfC and HfN, is very sensitive to the furnace atmosphere.

When  $y$  varies for  $TiN_{1-y}$  and  $TiC_{1-y}$ , the activities of both Ti (Figure 7.32) and the non-metallic element vary, while the products  $a_{Ti} \cdot a_C$  and  $a_{Ti} \cdot a_N (= a_{Ti} \cdot P_{N_2}^{1/2})$  are nearly constant at a given temperature (Hultgren et al. 1973). If, instead of pure Cu, a Cu-Ti alloy is used, the activity of Ti at the interface and the stoichiometry parameter  $y$  are fixed by the Ti concentration in the alloy ( $y$  increases when the molar fraction of Ti in Cu increases, see Figure 7.33 taking  $Me = Ti$ ). The results in Figure 7.31 for TiC and Table 7.11 for various carbides

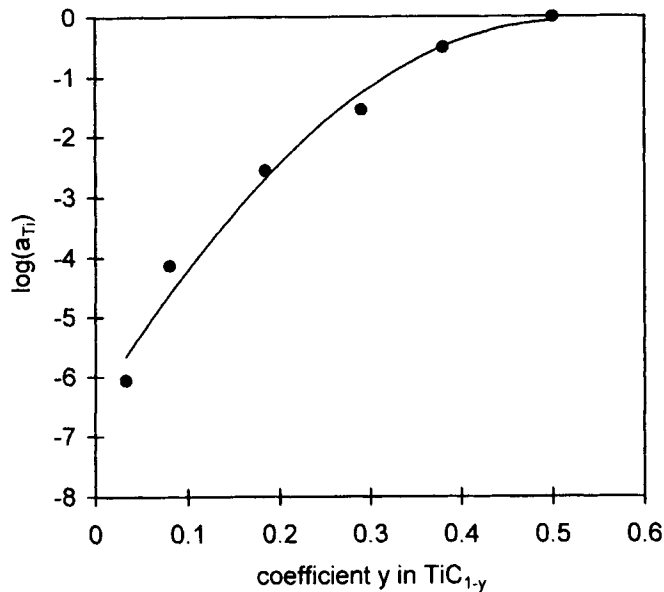


Figure 7.32. Activity of Ti in equilibrium with  $\text{TiC}_{1-y}$  at 1400K (Nicholas 1986).

show that hypostoichiometry favours wetting. This means that Ti additions to Cu are expected to improve wetting, which is indeed observed for both TiC and TiN (Xiao and Derby 1996, Lequeux et al. 1998). For instance, in the case of a Cu-5 at.% Ti alloy on TiN, for which the corresponding value of  $y$  is 0.20, the contact angle is only  $12^\circ$  (Lequeux 1997). Such a low contact angle is due at least partly to a modification of the interface at the solid-side (hypostoichiometry) but it is also possible that the liquid-side of the interface is modified by Ti adsorption, because Ti-TiN interactions are stronger than Cu-TiN interactions.

Ni, Fe and Co dissolve large amounts of carbides because of the relatively strong interactions between these metals and both carbon and the metal component of the carbide. For instance, at  $1500^\circ\text{C}$ , the molar fraction of carbide dissolved in Co lies between 0.05 for TaC and 0.23 for WC (Warren 1980). When a small piece of Co is placed on a MeC carbide substrate, the reaction between Co and MeC depresses the melting temperature of Co by 100 to  $200^\circ\text{C}$  because of the presence of eutectics in ternary Me-C-Co systems. Therefore, the final contact angle measured during such an experiment is for a Co alloy saturated with carbide. Furthermore, because of the dissolution process, the measured contact angle is only apparent and is lower than the true Young contact angle (see Figure 2.18). Despite this difficulty, the experimental results obtained by Ramqvist (1965) and

other authors (Whalen and Humenik 1960, Warren 1980) show very good wetting by ferrous metals on all carbides, including the high-stability carbides of Ti, Zr and Hf (Table 7.12).

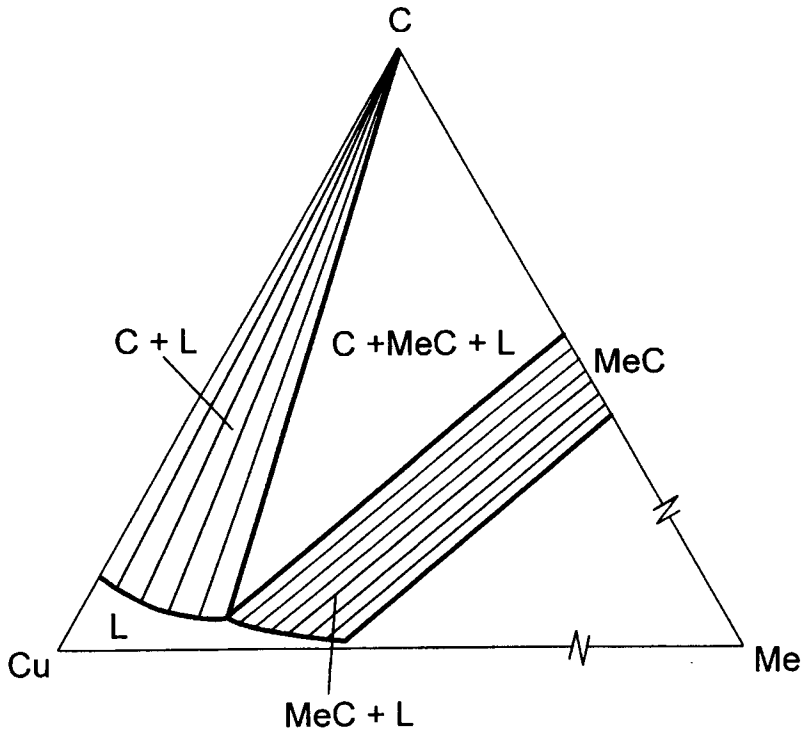
Ferrous metals are also known to wet stable nitrides with contact angles reported of 49° for Fe at 1590°C and 7° for Co at 1540°C on ZrN in vacuum (Kotsch 1967).

**Table 7.11.** Wetting by Cu of non-stoichiometric metal-like carbides in a high vacuum at 1100°C (Ramqvist 1965).

carbide	y	$\theta$ (deg)
TiC <sub>1-y</sub>	0	112
	0.15	108
	0.34	88
	0.51	0
TaC <sub>1-y</sub>	0	78
	0.06	75
	0.10	34
VC <sub>1-y</sub>	0.12	50
	0.17	38

**Table 7.12.** Contact angles of initially pure Ni, Co and Fe on different carbides (Ramqvist 1965).

Carbide	Ni at 1380°C $\theta$ (deg)	Co at 1420°C $\theta$ (deg)	Fe at 1490°C $\theta$ (deg)
TiC	23	25	28
ZrC	24	36	45
HfC	23	40	45
VC	17	13	20
NbC	18	14	25
TaC	16	13	23
Cr <sub>3</sub> C <sub>2</sub>	0	0	0
Mo <sub>2</sub> C	0	0	0
WC	0	0	0
TiC <sub>0.49</sub>	0	21	



**Figure 7.33.** Schematic representation of isothermal section of Cu-Me-C phase diagram when the carbide MeC exhibits a range of non-stoichiometry.

For metal-like borides, the selected contact angles given in Table 7.13 assumed by Cu and Ni exemplify weak and high reactivities. Ni dissolves several mole % of many borides and wets in high vacuum or neutral gas environments. Results obtained by the same investigators in different atmospheres show significant effects of furnace atmosphere on the contact angle for the more oxidizable borides  $\text{ZrB}_2$  and  $\text{TiB}_2$ . It may be noted that the results for Fe and Co are very similar to those for Ni.

In the case of relatively unreactive Cu, the dispersion of  $\theta$  values is even higher, so that for  $\text{TiB}_2$  both wetting contact angles and very marked non-wetting ones have been found by different investigators. However, for  $\text{CrB}_2$ , excellent wetting has been observed, as for Cu/ $\text{Cr}_3\text{C}_2$  (see Table 7.10). Note that for  $\text{CrB}_2$ , the furnace atmosphere has less influence on  $\theta$  than for  $\text{TiB}_2$ , probably owing to the lower stability of chromium oxide and to the formation of volatile chromium suboxides that promotes deoxidation at high temperatures.

**Table 7.13.** Wetting by Cu and Ni of different borides.

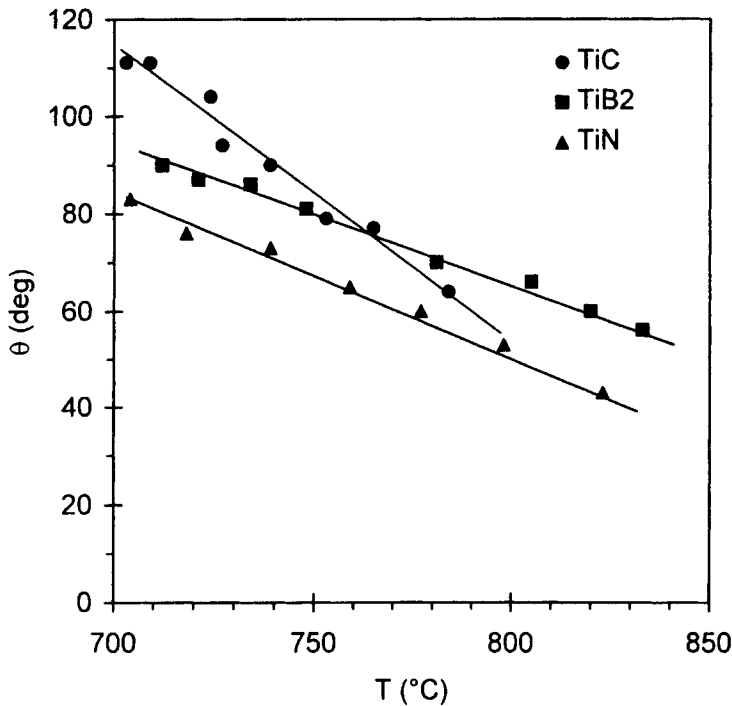
Boride	Cu			Ni		
	T (°C)	Atm.	$\theta$ (deg)	T (°C)	Atm.	$\theta$ (deg)
TiB <sub>2</sub>	1100	Ar	158 <sup>(1)</sup>	1480	He	38.5 <sup>(1)</sup>
TiB <sub>2</sub>	1120	vacuum	58 <sup>(2)</sup>	1500	vacuum	0 <sup>(2)</sup>
TiB <sub>2</sub>	1100	Ar	143 <sup>(3)</sup>	1480	vacuum	20 <sup>(4)</sup>
				1480	Ar	72 <sup>(4)</sup>
ZrB <sub>2</sub>	1120	vacuum	142 <sup>(2)</sup>	1500	vacuum	42 <sup>(2)</sup>
ZrB <sub>2</sub>	1100	Ar	135 <sup>(3)</sup>	1480	vacuum	65 <sup>(4)</sup>
ZrB <sub>2</sub>				1480	Ar	78 <sup>(4)</sup>
TaB <sub>2</sub>	1100	Ar	77 <sup>(1)</sup>	1500	Ar	43 <sup>(1)</sup>
CrB <sub>2</sub>	1430	He	50 <sup>(1)</sup>	1480	He	11 <sup>(1)</sup>
CrB <sub>2</sub>	1100	Ar	26 <sup>(3)</sup>	1450	vacuum	20 <sup>(4)</sup>
CrB <sub>2</sub>				1450	Ar	21 <sup>(4)</sup>

<sup>(1)</sup> (Eremenko and Naidich 1959), <sup>(2)</sup> (Merz and Kotsch 1963), <sup>(3)</sup> (Samsonov et al. 1973),

<sup>(4)</sup> (Samsonov et al. 1973b)

Finally, consider the wetting of Al on metallic ceramics. In this case, experimental difficulties in the determination of wetting properties arise not only from substrate oxidizability and impurities but also from oxidizability of Al. As we have seen in Section 6.4.2, in moderate vacuum or in neutral gas, spreading of Al at temperatures lower than 900°C is inhibited by an oxide layer covering its surface and this results in very large apparent contact angles (140–160°) of Al on various carbides, nitrides and borides. Much lower contact angles have been found by Rhee (1970) using a furnace evacuated to  $2 \times 10^{-7}$  mbar and less and sintered, low porosity, TiB<sub>2</sub>, TiC and TiN containing 0.2–0.5 wt.% of oxygen as the main impurity. For these ceramics, wetting was observed at temperatures higher than 750°C (Figure 7.34) while no reactivity at the micron scale was found at the Al/ceramic interface. The results of Rhee show an important improvement in wetting by temperature, perfect wetting of Al on TiC, TiB<sub>2</sub> and TiN being predicted at temperatures higher than 1000°C. This has been indeed observed for Al on TiC<sub>1-y</sub> at temperatures close to 1100°C for y values between 0 and 0.5 (Frumin et al. 1997). However, at these temperatures, wetting is accompanied by a significant reactivity which, depending on y, consists either of some dissolution of TiC<sub>1-y</sub> into molten Al or of Al<sub>4</sub>C<sub>3</sub> formation. As in the case of Cu on TiC, hypostoichiometry

of  $\text{TiC}_{1-y}$  greatly favours wetting of Al, even at temperatures close to the melting temperature of Al (Frumin et al. 1997).



**Figure 7.34.** Change of stationary contact angle with temperature for times of no more than 30 minutes for Al on TiC, TiB<sub>2</sub> and TiN. From data reported in (Rhee 1970).

To sum up, despite difficulties arising from the lack of monocrystalline high-purity substrates for wetting studies, some experimental facts on the wetting behaviour of non-reactive metals on metal-like carbides emerge that are similar to those of nitrides and borides. Thus the wetting and adhesion of metals on carbides of Mo, W and Cr are good and very similar to those observed in non-reactive metal/metal systems. Compared to  $\text{Mo}_2\text{C}$ , WC and  $\text{Cr}_3\text{C}_2$ , stoichiometric TiC, ZrC and HfC are less wetted by liquid metals but the intrinsic contact angles on these carbides are not well-known because of their high oxidizability. Hypostoichiometry of carbides or nitrides favours wetting and adhesion and this can be controlled by adding Ti to a liquid metal matrix because this element fixes *in*

*situ* hypostoichiometry at the alloy/carbide (or nitride) interface. For reactive couples such as Ni (or Co, Fe)/TiC, the presence of Ti in the alloy caused by dissolution of the substrate explains the excellent wetting observed. At present, there is no satisfactory fundamental understanding of wetting and adhesion in non-reactive metal/metal-like ceramic systems, as discussed by Xiao and Derby (1996). Such an understanding needs more work, both experimental and theoretical. Wetting studies must be combined with a detailed characterisation of surface chemistry and hypostoichiometry. Moreover, calculations of electronic structure and bonding, which exist at present only for bulk compounds, must also be performed for surfaces, taking into account electronic and atomic relaxations.

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## Chapter 8

# Wetting properties of metal/carbon systems

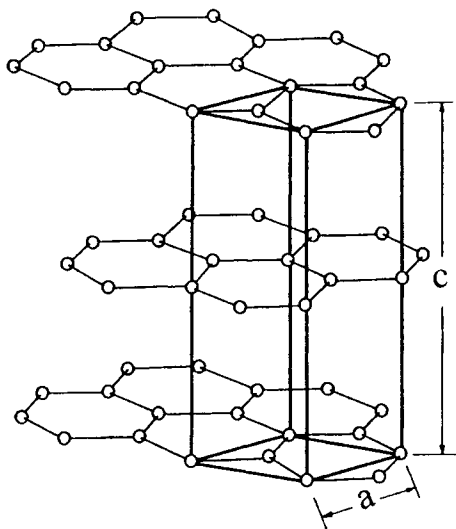
Carbon is not only the building block of life and organic chemistry but also an important ceramic in its own right and a constituent of carbides and carbo-nitride ceramics. The variety of these aspects of carbon chemistry reflect the fact that its electron shell is only half-filled and the four bonding electrons can form single, double or triple covalent carbon/carbon and carbon/non-carbon covalent bonds of varying length and energy. As indicated in Table 8.1 for a series of hydrocarbon compounds (Hill and Holman 1981), the C atoms approach closer and the bond energy increases as the bonding involves more electrons, so that the combustion of an unsaturated hydrocarbon such as acetylene is a more exothermic process than that of the saturated hydrocarbon ethane.

**Table 8.1.** Effects of bond type on characteristics.

Bond type	Length (nm)	Bond energy (kJ/mole)	Example
C–C	0.154	–346	ethane, C <sub>2</sub> H <sub>6</sub>
C=C	0.134	–610	ethylene, C <sub>2</sub> H <sub>4</sub>
C≡C	0.121	–835	acetylene, C <sub>2</sub> H <sub>2</sub>

Single and double bonds unite elemental C in its two principal allotropic forms, of which diamond is the simplest in structure but graphite is overwhelmingly the most common. In diamond, each atom is at the centre of a tetragonal array of others each of which subtends an angle of 109°, and to which it is linked by a single covalent bond. The C–C distance in the diamond lattice is 0.154 nm as it is in saturated hydrocarbons such as ethane.

The crystalline structure of the graphite allotrope is hexagonal and the lattice parameters are  $a = 0.246$  nm and  $c = 0.671$  nm (Figure 8.1). The atoms are arranged as planar hexagons containing oscillating single and double covalent bonds and are separated by a distance of 0.142 nm which lies between those for pure single or double bonding. These planes are linked to each other by weak van der Waals forces, as indicated by their separation distance of 0.335 nm and the low surface energy of the basal plane of 150 mJ/m<sup>2</sup> (see Section 4.2.3).



**Figure 8.1.** Structure of graphite.

A third allotrope, fullerene, has been identified (Kroto et al. 1985) but has not yet been used in high-temperature wetting studies. This Chapter, therefore, is concerned only with the two principal allotropes, diamond and graphite, which have physical properties that reflect their differing lattice structures and are sometimes markedly different as indicated by the typical values assembled in Table 8.2. Thus diamond has the highest known thermal conductivity and hardness, but graphite has a much higher electrical conductivity. The hardness, optical and thermal characteristics of diamonds have resulted in applications as cutting agents, as jewelry and as electronic heat sinks. The applications of graphite are very varied and depend on both inherent material characteristics as well as the effects of temperature and other processing parameters on microstructural features such as porosity and grain orientation. There are three main types of graphite of technical importance: *Bulk polycrystalline graphite* which has a coarse grain structure and contains several percent of gross open porosity. *Pyrolytic graphite* which is a dense and very anisotropic material formed by cracking hydrocarbons at 1400–3000°C. *Vitreous carbon* which has a very fine structure described as a tangle of graphitic ribbons only a few unit cells thick (Jenkins and Kawamura 1971) whose low density of 1.5 Mg/m<sup>3</sup> as against 2.26 Mg/m<sup>3</sup> for fully dense graphite is due to the presence of closed porosity at the nanometer scale. Because of its low density, vitreous carbon has a low dispersive (van der Waals) component of surface energy (32 mJ/m<sup>2</sup>) compared to that of monocrystalline graphite (150 mJ/m<sup>2</sup>, Section 4.2.3).

**Table 8.2.** Some physical properties of graphite and diamond.

Property	Graphite	Diamond
melting temperature ( $^{\circ}\text{C}$ )	3700	3550
density ( $\text{Mg/m}^3$ )	2.26	3.53
coefficient of thermal expansion ( $\text{K}^{-1}$ )	(*)	$0.8 \times 10^{-6}$
thermal conductivity at R.T. ( $\text{W m}^{-1} \text{K}^{-1}$ )	100	1000–3000 (**)
electrical conductivity ( $\Omega^{-1} \text{m}^{-1}$ )	$2.7 \times 10^6$ (***)	$10^{-15}$
bulk modulus (GPa)	33	1100
hardness (Mohs scale)	1.5	10

(\*)  $10^{-6} \text{K}^{-1}$  parallel and  $5 \times 10^{-6} \text{K}^{-1}$  perpendicular to basal planes of oriented material. Greater anisotropy is displayed by single crystals.

(\*\*) The precise value depends on the concentration of the  $^{13}\text{C}$  isotope.

(\*\*\*) in basal planes

Obviously, differences in bulk structure of the different types of graphite have repercussions on surface structure and properties. Thus effects on wetting behaviour can be expected but in studies with liquid metals, information given about carbon microstructure is usually insufficient. Further problems arise from the difficulty of preparing surfaces with a low roughness. This is particularly true for polycrystalline graphite, the form most used in published work, for which the average roughness  $R_a$  can be several hundreds of nanometers or even more even after careful polishing. This is due to the existence of some open porosity and especially to the weak cohesion between graphitic planes bonded only by van der Waals interactions, leading to detachment of particles by cleavage during polishing. Consequently, the resulting surface is rough and consists of microfacets of graphitic planes. The high  $R_a$  values can greatly affect equilibrium contact angles, especially in non-wetting systems for which deviations from Young contact angle as high as tens of degrees can be expected (see Section 3.3). Therefore, published data for this kind of system reveal only gross trends in contact angle and work of adhesion values.

In a limited number of studies, vitreous carbon ( $\text{C}_v$ ) substrates have been used whose surfaces can be polished to an average roughness of less than 10 nm. On this type of surfaces, it can be expected that the departure of the equilibrium contact angle from the Young contact angle is only a few degrees. However, it must be emphasized that wetting properties obtained for both non-reactive and reactive metals on  $\text{C}_v$  may differ significantly from intrinsic properties on graphite because the density of these substrates is very different and also because in  $\text{C}_v$  there is no preferred orientation of graphitic hexagons with regard to the surface.

In the following, we shall consider successively non-reactive pure metals, i.e., metals in which the maximum solubility of carbon is lower than 1 ppm (such as Cu or Au), then metals that can form carbides (such as Si or Ti) and finally metals dissolving large amounts of carbon without forming stable carbides (such as Ni).

### 8.1. NON-REACTIVE SYSTEMS

These systems consist of metals which do not form carbides and do not dissolve carbon significantly: for instance, Cu dissolves only 1 ppm of carbon at its melting point (Oden and Gokcen 1992). The results in Table 8.3, obtained on vitreous carbon in high vacuum at a temperature close to the melting point of the metal, show that non-reactive metals do not wet carbon. As for non-reactive metal/oxide couples, contact angle values change only slightly with temperature (of the order of 1 deg for 100K), as shown in Figure 8.2.

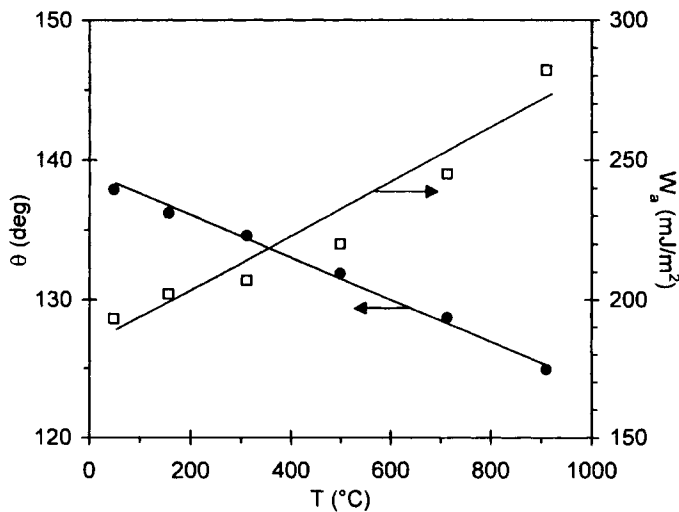
Despite the difficulties in obtaining well-defined contact angles on polished surfaces of polycrystalline graphite mentioned in the introduction, the results of the systematic study of Naidich and Kolesnichenko (1965) provide clear evidence that, as for vitreous carbon, contact angles on polycrystalline graphite are much higher than 90° whatever metal was used. Then, values lying between 135° and 150° were found for metals such as Cu, Ag, In, Ge and Sn in high vacuum between 1100°C and 800°C. This non-wetting behaviour, associated with the absence of reactivity, is well-known to metallurgists and is exploited in the use of graphite crucibles.

**Table 8.3.** Contact angles of non-reactive metals on vitreous carbon in high vacuum at a temperature close to the melting point of the metal.

Metal	$\theta$ (deg)	Reference
Ga	138	(Naidich and Chuvashov 1983)
In	145	(Chizhik et al. 1985)
Sn	151	(Chizhik et al. 1985)
Bi	142	(Chizhik et al. 1985)
Pb	142	(Chizhik et al. 1985)
Au	138	(Chizhik et al. 1985)
	135	(Dezellus and Eustathopoulos to be published)
Cu	139	(Dezellus and Eustathopoulos to be published)
	145	(Standing and Nicholas 1978)
Ni-Pd (*)	137	(Grigorenko et al. 1998)

(\*) composition with congruent fusion

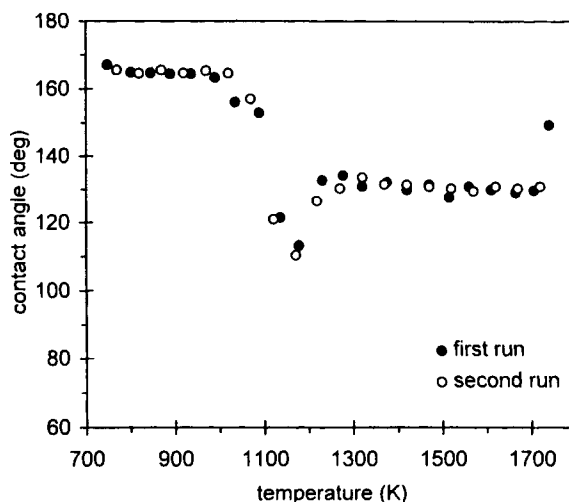
Large non-wetting contact angles have also been found on diamond (111) faces (Naidich 1981). However, the different faces of diamond exhibit structural modifications with temperature which can lead at high temperatures to surface graphitization and changes of several tens of degrees in contact angle values (Figure 8.3). Despite these transformations, the contact angles remain in all cases higher than  $90^\circ$ .



**Figure 8.2.** Contact angle and work of adhesion of Ga on vitreous carbon versus temperature. A variation of 900K leads to a contact angle change of only ten degrees. From data reported by Naidich and Chuvashov (1983).

The values of the work of adhesion corresponding to the contact angles of Table 8.3 are of the order of  $100 \text{ mJ/m}^2$  and are attributed to van der Waals interactions resulting from dispersion forces (Naidich 1981). According to the equation given in Figure 6.8.b for the van der Waals interactions between two condensed phases, the interaction energy is proportional to the atomic densities of the two phases in contact. The higher the atomic density of the carbon substrate, the larger is the dispersive (van der Waals) contribution to interaction energy, resulting in a higher adhesion energy and lower contact angle. Therefore, if the predominant interactions at non-reactive metal/carbon interfaces are van der Waals interactions, different values of contact angle would be expected for the same metal on *vitreous carbon* ( $C_v$ ) and *monocrystalline graphite* ( $C_{mg}$ ) which have very different atomic densities





**Figure 8.3.** Contact angles of liquid Sn on (100) plane of diamond versus temperature in an Ar-10% H<sub>2</sub> atmosphere. Data from work reported in (Nogi et al. 1998) [7].

(Table 8.4). In contrast to polycrystalline graphite, these types of carbon allow very smooth surfaces to be obtained with an average roughness of a few nanometers either by polishing for C<sub>v</sub> or by cleavage for C<sub>mg</sub>. Such surfaces of C<sub>mg</sub> are basal planes while no specific orientation is expected for polished C<sub>v</sub> surfaces. For such substrates, the measured contact angles are expected to be equal to the Young contact angle to within 2–3°. The results in Table 8.4 for Cu and Au, as well as the initial contact angle measured for Al before it reacts (see Figure 8.7), confirm predictions based on van der Waals interactions that the contact angle decreases with increasing density of C substrates. Note that if adhesion in this kind of system resulted from chemical interactions, the basal planes of high atomic density present on the surfaces of graphite single crystals would be less wetted than the low atomic density surfaces of vitreous carbon (see Section 5.1).

Further evidence of the effects of van der Waals interactions on metal/carbon bonding has been offered by Nogi et al. (1995) who used an atomic force microscope to measure the force resulting from van der Waals interactions between three differing faces of diamond and the probe and found these scaled well with experimental values of the work of adhesion for the interfaces formed by Bi, Pb or Sn.

It is interesting to note that Heyraud and Metois found that small, micron-size, solid particles of Au (Heyraud and Metois 1980) and Pb (Heyraud and Metois 1983) assumed equilibrium shapes at high temperatures on monocrystalline

graphite, with their (111) faces parallel to the graphite surface. The (111) plane is the most densely packed plane of a fcc metal so this orientation maximises the number of metal atoms per unit area in nearest-neighbour interactions with C atoms and this is consistent with the predominance of van der Waals interactions at the interface. In this study (Heyraud and Metois 1980), the contact angle of nearly spherical particles of Au on graphite was found to be  $127^\circ$ , a value close to that of liquid Au (Table 8.4). This concordance is expected because the changes of density and surface energy of a pure metal at melting are small and have opposing effects on  $\theta$ .

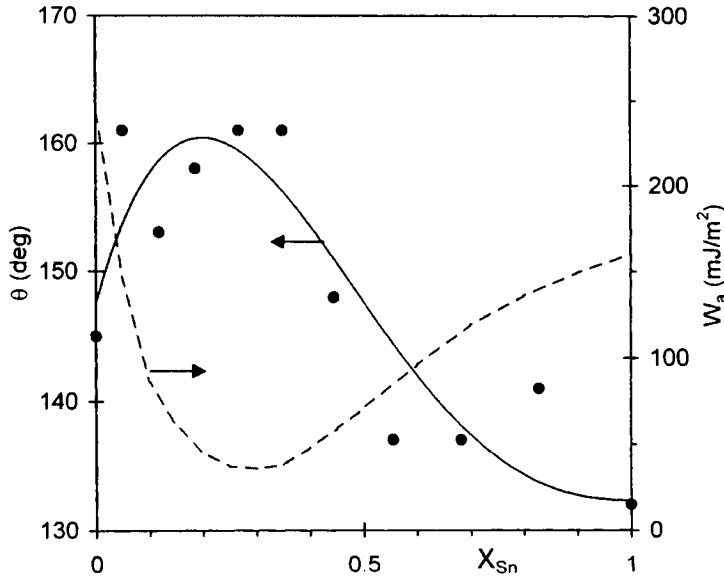
**Table 8.4.** Contact angle and work of adhesion of different metals on vitreous carbon ( $C_v$ ) and pseudomonocrystalline graphite ( $C_{mg}$ ). From (Dezellus and Eustathopoulos to be published) except for Al (Landry et al. 1998).

Substrate	Cu at 1373K		Au at 1373K		Al at 1100K	
	$\theta$ (deg)	$W_a$ (mJ/m <sup>2</sup> )	$\theta$ (deg)	$W_a$ (mJ/m <sup>2</sup> )	$\theta^{(*)}$ (deg)	$W_a$ (mJ/m <sup>2</sup> )
$C_v$ ( $\rho = 1.5 \text{ Mg/m}^3$ )	139	319	135	338	139	206
$C_{mg}$ ( $\rho = 2.26 \text{ Mg/m}^3$ )	122	611	119	595	123	383

(\*) initial contact angle before reaction

Effects of non-reactive alloying elements on contact angle and work of adhesion values can be discussed in terms of the thermodynamic model initially developed for non-reactive metal/oxide systems (see Section 6.5.1). This model allows prediction of the shape of  $\theta$  and  $W_a$  isotherms for binary alloys from the values of  $\sigma_{LV}$  and  $W_a$  of pure metals and the regular solution parameter  $\lambda$  defined in equation (4.3). As in metal/oxide systems, contact angles are very large and vary little between the different metals (Table 8.4) so the ratio  $W_a/\sigma_{LV}$  is approximately constant. It can be readily shown that binary alloys developing van der Waals interactions with carbon produce type (b) isotherms of Figure 6.29. For such systems, addition of B to A when  $\sigma_{LV}^B \ll \sigma_{LV}^A$  will decrease the work of adhesion of A and increase or decrease the contact angle depending on whether the contact angle of pure A,  $\theta_A$ , is higher or lower than a critical value  $\theta^*$  given by equation (6.35). An example is Cu-Sn on vitreous carbon at  $1150^\circ\text{C}$  for which, according to results of Standing and Nicholas (1978),  $W_a^{Cu} = 245 \text{ mJ/m}^2$  and  $W_a^{Sn} = 160$

$\text{mJ/m}^2$ . Taking the values  $\sigma_{\text{LV}}^{\text{Cu}} = 1350 \text{ mJ/m}^2$ ,  $\sigma_{\text{LV}}^{\text{Sn}} = 485 \text{ mJ/m}^2$  and  $\lambda = -15 \text{ kJ/mol}$  cited by Li et al. (1989), the calculated value of the critical contact angle  $\theta^*$  is  $133^\circ$  i.e., lower than the experimental value of  $\theta$  for pure Cu (Figure 8.4). Therefore, a maximum on the  $\theta$  isotherm is predicted, which is in agreement with experimental findings (Figure 8.4).



**Figure 8.4.** Contact angles of Cu-Sn alloys on vitreous carbon at  $1150^\circ\text{C}$  (Standing and Nicholas 1978) and corresponding values of  $W_a$  calculated using  $\sigma_{\text{LV}}$  values of Cu-Sn alloys compiled by Li et al. (1989).

More generally, any combination of two *liquid* metals developing van der Waals interactions with carbon is expected to result in small variations in contact angle of a few degrees or a few tens of degrees with respect to the pure components. Note however that a substantial decrease from  $117^\circ$  to  $100^\circ$  at  $285^\circ\text{C}$  for small Pb *crystallites* on graphite, corresponding to an increase of  $W_a$  by 50%, was obtained by adding only 0.5 at.% Ni to Pb (Gangopadhyay and Wynblatt 1994). At  $285^\circ\text{C}$ , Ni carbide ( $\text{Ni}_3\text{C}$ ) is not stable and the solubility of C in Pb-Ni alloys is expected to be extremely low. The effects of Ni on  $\theta$  and  $W_a$  are due to a strong adsorption of Ni at the Pb/graphite interface as demonstrated by applying the Gibbs adsorption equation and also by Auger analysis. It is not clear if the

strong adsorption of Ni results from the development of chemical Ni-C interactions at the interface or from elastic effects owing to differences in atomic sizes between Ni and Pb (see also Section 4.1.3).

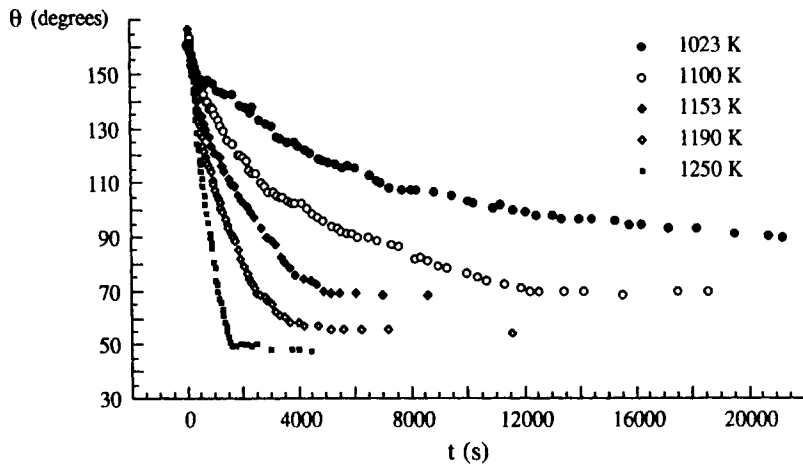
## 8.2. REACTIVE SYSTEMS

We will consider first the carbide-forming metals Al, Si, Ti and Cr and then the ferrous metals Fe, Co, Ni and Pd that dissolve carbon. Finally, the effect of alloying elements will be discussed.

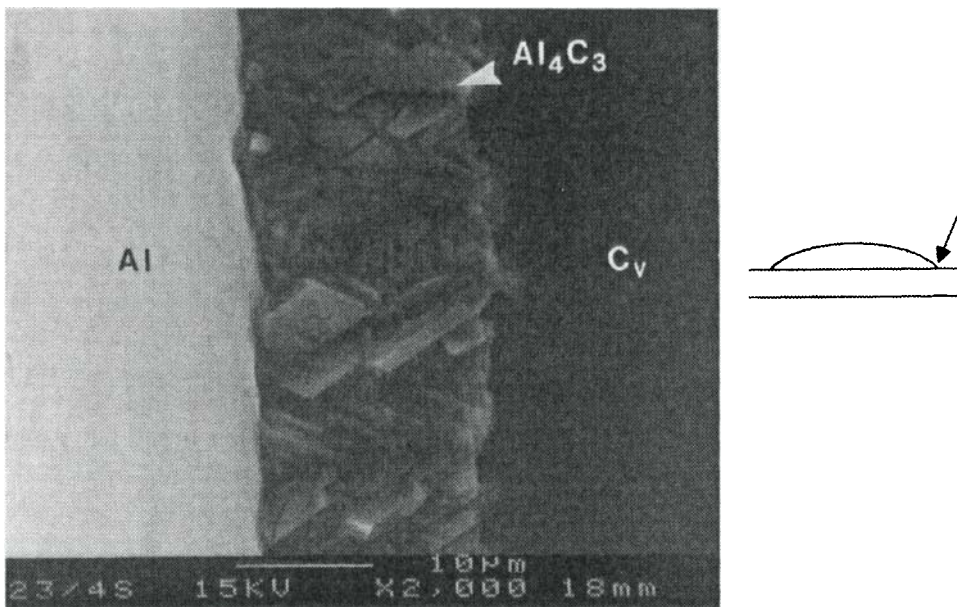
### 8.2.1 Carbide-forming metals

Because of the importance of Al in the metallurgical industry, and because the Al/C couple is a candidate for metal matrix composites, a great number of wettability studies have been devoted to Al/C systems. The solubility of C in molten Al is only a few ppm at 900°C (Jarfors et al. 1993), and molten Al reacts with C to form  $\text{Al}_4\text{C}_3$  which has a very significant degree of covalence (Table 7.1) (Jeffrey and Wu 1966). Pure Al wets  $\text{Al}_4\text{C}_3$  and a contact angle of 55° was measured at 1100°C for sintered carbide (Ferro and Derby 1995). Therefore Al should wet C substrates with the spreading being controlled by the rate of formation at the interface of a continuous layer of Al carbide. Figure 8.5 presents changes of  $\theta$  with time for 20 mg droplets of Al on vitreous carbon substrates at different temperatures. The initial contact angle of about 160° is that of oxidized Al. The first contact angle measured after deoxidation (130°–140° depending on the temperature) corresponds to that of nearly unreacted Al on vitreous carbon. The final contact angle of between 50° and 70° is that of Al on the reaction product layer, a few microns of  $\text{Al}_4\text{C}_3$  (Figure 8.6).

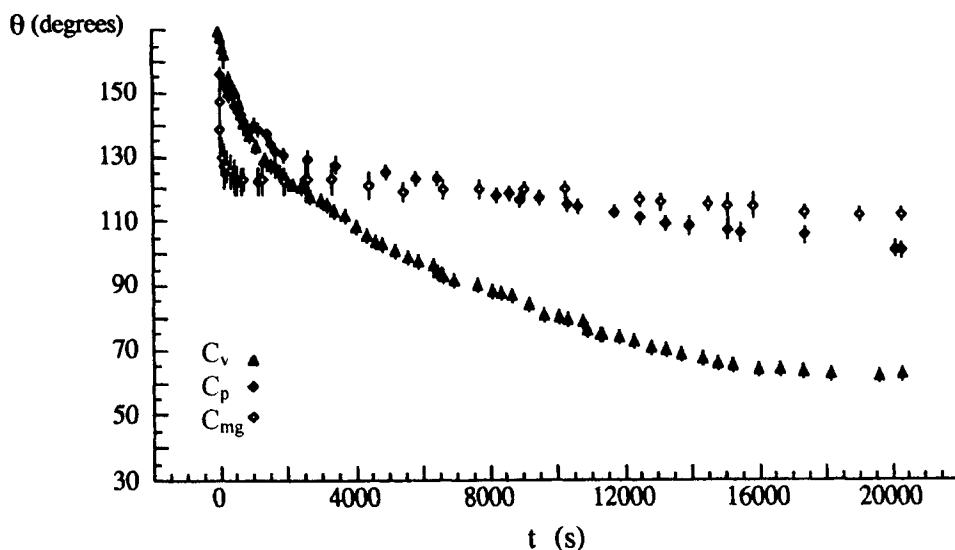
These  $\theta$  values correspond to a work of adhesion of about 75% of the work of cohesion  $W_c (= 2\sigma_{LV})$  of the liquid metal. Such a value of  $W_a$  is too high to be attributed to van der Waals forces and reflects the development of chemical interactions at the Al/ $\text{Al}_4\text{C}_3$  interface. As discussed in Section 2.2.2.2, the rate of spreading is controlled by the rate of the chemical reaction at the solid/liquid/vapour triple line after the drop deoxidation. From the data in Figure 8.5, the activation energy of this process was found to be about 230 kJ/mole (Landry et al. 1995, 1998). It was proposed that the formation of  $\text{Al}_4\text{C}_3$  at the triple line could be controlled by the rupture of C–C covalent bonds at the substrate surface. This process will be strongly affected by atomic defects in carbon, which are much more numerous in vitreous carbon than in monocrystalline graphite or pyrocarbon in which the majority of graphitic hexagons are parallel to the substrate surface (Landry et al. 1998). As a consequence, as shown in Figure 8.7, both the



**Figure 8.5.** Contact angle kinetics in the Al/vitreous carbon system at different temperatures (Landry et al. 1998) [17].



**Figure 8.6.** SEM micrograph taken from above of an Al/vitreous carbon specimen cooled from 1100K showing an  $\text{Al}_4\text{C}_3$  layer close to the triple line (Landry and Eustathopoulos 1996b).



**Figure 8.7.** Contact angle kinetics of Al on vitreous carbon ( $C_v$ ), pyrocarbon ( $C_p$ ) and monocrystalline graphite ( $C_{mg}$ ) at 1100K (Landry et al. 1998) [17]. For  $C_p$  and  $C_{mg}$ , no stationary contact angle was obtained after  $2 \times 10^4$  seconds.

reaction and spreading kinetics on vitreous carbon are much faster than those on monocrystalline graphite and pyrocarbon. Note that in the case of  $C_{mg}$ ,  $\theta$  remains nearly constant for about  $10^4$  seconds after the end of the first stage (deoxidation of Al), reflecting the very low reactivity between molten Al and basal planes of graphite.

On polycrystalline graphite, a material of interest for many applications, several tens of minutes at 1000°C are needed to obtain a contact angle lower than 90° (Mori et al. 1983, Nogi et al. 1988, Weirauch et al. 1995, Sobczak et al. 1996) due to the high activation energy of the wetting process. Extremely slow kinetics are observed at temperatures close to the melting point of Al, sessile drop experiments performed with deoxidized Al droplets on polycrystalline graphite showing no contact angle variations for several hours at 700°C (Mori et al. 1983, Nogi et al. 1988, Sobczak et al. 1996). Therefore, in this range of temperature, Al behaves as a non-reactive and non-wetting metal interacting with graphite by weak van der Waals dispersion forces.

Liquid Si dissolves little C at its melting point (the molar fraction of C in Si at saturation is less than  $10^{-3}$ ) but reacts with C to form predominantly covalent SiC. This product is well wetted by molten Si, the contact angle of Si on (0001) basal planes of  $\alpha$ -SiC being 30–40° (see Section 7.1.1). The wetting kinetics of Si on

vitreous carbon are fast because the melting point of Si is high (1410°C), the final contact angle of 40–50° being reached in less than one minute (Whalen and Anderson 1975). Contact angles of 10–30° on polycrystalline graphite have been reported (Whalen and Anderson 1975, Naidich 1981), but the differences between these values and those for vitreous carbon are hardly significant given the difficulties arising from porosity often present in polycrystalline graphite. Thus, according to Whalen and Anderson (1975), wetting by Si of this type of substrate was accompanied by penetration of Si into pores for up to several hundreds of microns from the interface.

The stationary contact angles observed for Al and Si on C substrates are close to those on Al<sub>4</sub>C<sub>3</sub> and SiC respectively. The good wetting of Si on SiC was attributed to the formation of covalent bonds between molten Si and Si or C atoms of the SiC surface (Drevet et al. 1993) (see Section 7.1.1.1). A similar explanation can be advanced for the high adhesion energy of Al on Al<sub>4</sub>C<sub>3</sub> since Al also has a low sp orbital capable of forming covalent bonds. This is in qualitative agreement with the results of molecular orbital calculations showing the establishment of strong chemical bonds between metallic Al and covalent ceramics (Li et al. 1988, Hoekstra and Kohyama 1998).

Pure Cr and Ti react with C to form carbides that are metallic conductors. It has been found (Weisweiler and Mahadevan 1972) that at 1775°C in Ar Cr wets well both graphite ( $\theta = 40^\circ$ ) and vitreous carbon ( $\theta = 35^\circ$ ). Similar results have been obtained at 1740°C in Ar using pure Ti for which the angles were 60° on polycrystalline graphite and 50° on vitreous carbon (Weisweiler and Mahadevan 1972)). These results are compatible with data given in Section 7.2 on wetting of transition metals on Ti and Cr carbides.

### **8.2.2 Ferrous metals**

The ferrous metals Fe, Co and Ni and also Pd and Pt dissolve relatively large amounts of C but do not form stable carbides (Fe carbides, for instance Fe<sub>3</sub>C, are metastable). Their wetting behaviour on C substrates is very complex and not yet understood due to the multiplicity of elementary phenomena acting simultaneously and to serious experimental difficulties. Experimental results suggest that metals presaturated with C do not wet graphite ( $\theta \gg 90^\circ$ ) while pure metals wet it well ( $\theta \ll 90^\circ$ ).

In principle, the Young contact angle can be measured only for a metal presaturated with C. In practice, two major difficulties exist: first, the high roughness and porosity of polycrystalline graphite, second, the difficulty of performing standard sessile drop experiments with metals fully presaturated in C (Hara et al. 1995). This second difficulty arises because substantial dissolution of

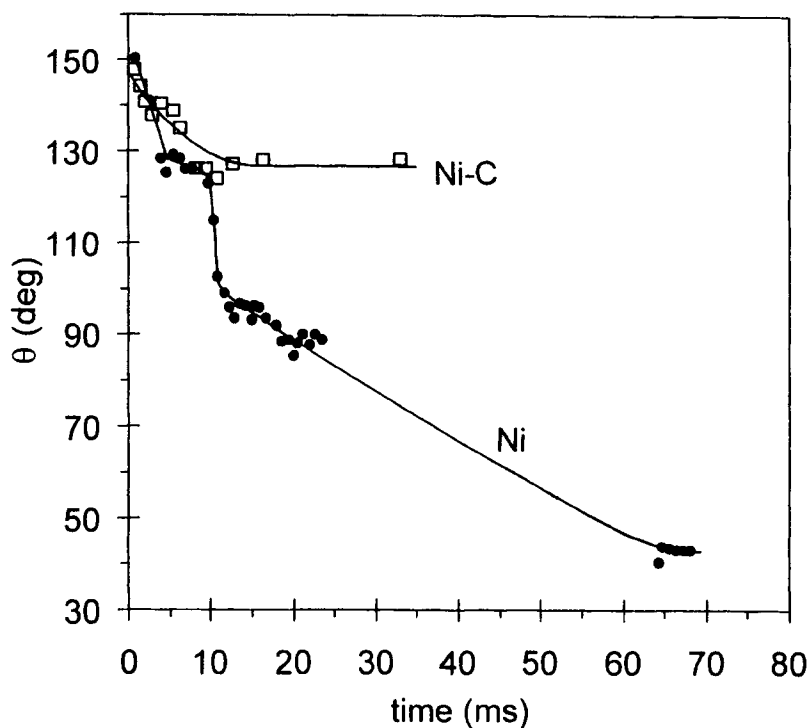
graphite substrate takes place even with nominally saturated alloys (there is evidence that at melting graphite precipitates in the drop bulk dissolve more slowly than the substrate itself). As a result, contact angle values measured by different investigators are very dispersed and probably associated with the extremely high contact angle hysteresis of up to  $100^\circ$  for such systems (Hara et al. 1995). These workers measured a stationary receding contact angle of about  $80^\circ$  for a carbon-saturated Ni drop at  $1350^\circ\text{C}$  on polycrystalline graphite after a dewetting process. Therefore, the true Young contact angle in this system must be  $\theta_{\text{Ni(C)}} \geq 80^\circ$  (see equation (1.37.b)). An upper limit for  $\theta_{\text{Ni(C)}}$  is given by results of Naidich et al. (1972) who studied the spreading of a carbon-saturated Ni drop transferred onto a graphite substrate from another graphite substrate (Figure 8.8). The final advancing contact angle is  $130^\circ$  so  $\theta_{\text{Ni(C)}} \leq 130^\circ$ . Therefore,  $130^\circ \geq \theta_{\text{Ni(C)}} \geq 80^\circ$ . Unless the true contact angle falls very close to the upper limit of  $130^\circ$ , all the other cases indicate that C-saturated Ni (and also C-saturated Fe and Co) wet carbon better than do the non-reactive metals of Table 8.3. As C does not change significantly the surface energy of liquid Ni or other ferrous metals (Hara et al. 1995), such an effect must be caused by a decrease in the solid/liquid interfacial energy. More experiments with well-characterized graphitic substrates are needed to confirm these points.

When a drop of pure Ni, or Fe or Co, is placed on a graphite substrate, melting starts at the Ni/graphite interface at a temperature corresponding to the eutectic transformation. Dissolution of carbon in Ni can produce at least three effects:

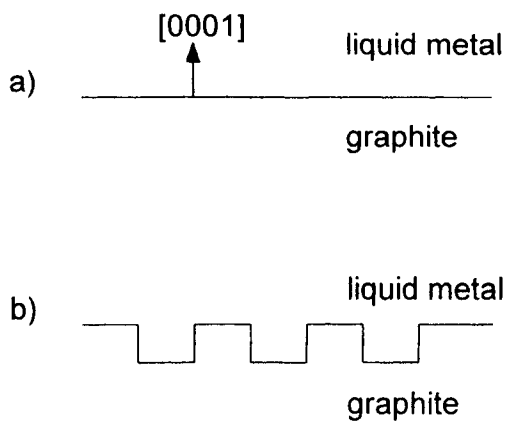
- 1) a modification of the characteristic interfacial energies of the system,
- 2) a change in the crystallographic orientation of the graphite surface. Dissolution may lead to the appearance of new orientations such as prismatic planes at the interface and hence bonding stronger than the van der Waals Ni-C interactions expected for interfacial basal planes (Figure 8.9).
- 3) the formation of a macroscopically concave solid/liquid interface (Barbangelo and Sangiorgi 1992, Hara et al. 1995), so that the visible or apparent contact angle cannot be described by the Young equation (see Figure 2.18).

The morphology of the solid/liquid interface close to the triple line, reflected by the value of the contact angle  $\theta_L$  defined in Figure 2.18.c, is not determined by the equilibration of interfacial energies according to the Smith equation (1.30) but by the dissolution process itself. Nevertheless, this dissolution of the substrate needs a certain time and in Figure 8.8 we can see that after  $10^{-2}$  second the contact angle for pure Ni is nearly equal to that for C-saturated Ni; then a further decrease of the contact angle to an apparent value as low as  $50^\circ$  is observed.





**Figure 8.8.** Spreading kinetics for C-presaturated Ni (squares) and pure Ni (full circles) on polycrystalline graphite at 1460°C. From data reported in (Naidich et al. 1972).

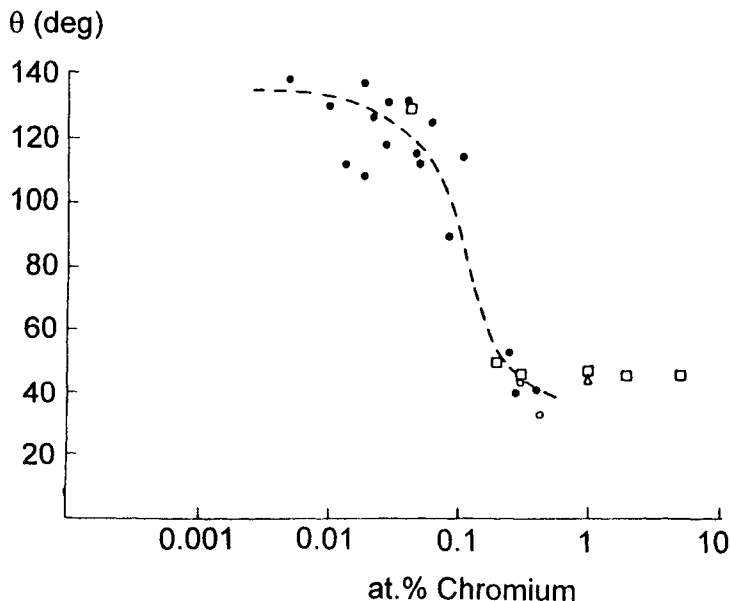


**Figure 8.9.** A possible effect of dissolution of graphite on wetting is the change of the crystallographic nature of the metal/graphite interface. a) Initial interface, b) interface during dissolution.

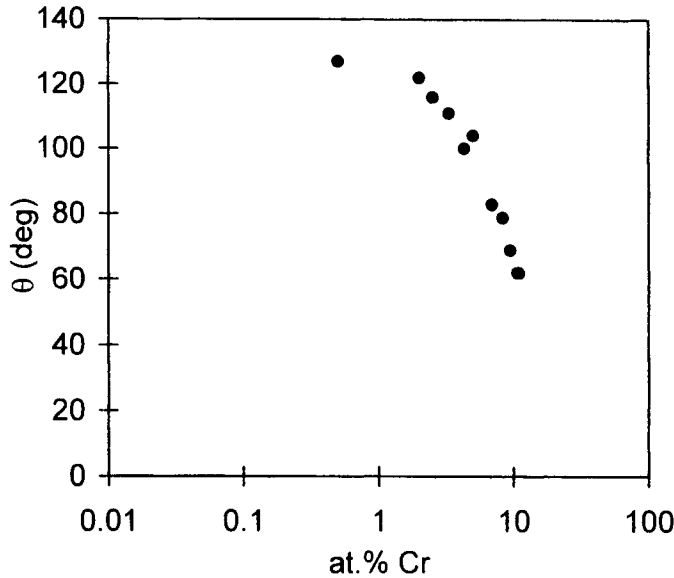
To sum up, wetting by ferrous metals can be described in terms of a contact angle measured on a nearly planar interface that is achievable only when using C-saturated metals. These contact angles are high but not as high as those observed for non-reactive metals. The formation of the interface for initially pure ferrous metals is a complex process due to both a slight lateral extension of the liquid on the substrate and deep attack of the substrate. Consequently, published contact angles of  $50^{\circ}$ – $70^{\circ}$  given for ferrous metals on graphite are only apparent values which are not governed by the Young equation.

### 8.2.3 Reactive alloying elements

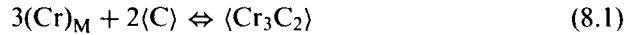
Attempts to improve wetting by non-reactive pure metals such as Cu by the addition of ferrous metals such as Ni or Fe have been unsuccessful (Naidich 1981). In contrast, improvements in wetting have been achieved by adding carbide-forming elements such as Cr or Ti. Additions of Cr to Cu above a critical value of the molar fraction of Cr,  $X_{Cr}^*$ , produce a sharp wetting transition (Figure 8.10) owing to the formation of a continuous layer of wettable Cr carbides in accord with the reaction:



**Figure 8.10.** Contact angles of Cu-Cr alloys on C at  $1150^{\circ}\text{C}$ . Full circles: diamond (Scott et al. 1975). Open circles: diamond (Naidich and Kolesnichenko 1964). Squares: vitreous carbon (Mortimer and Nicholas 1973). Triangle: graphite (Mortimer and Nicholas 1973) [2].



**Figure 8.11.** Contact angles of Ga-Cr alloys on graphite at 900°C. From data reported in (Naidich and Chuvashov 1983).

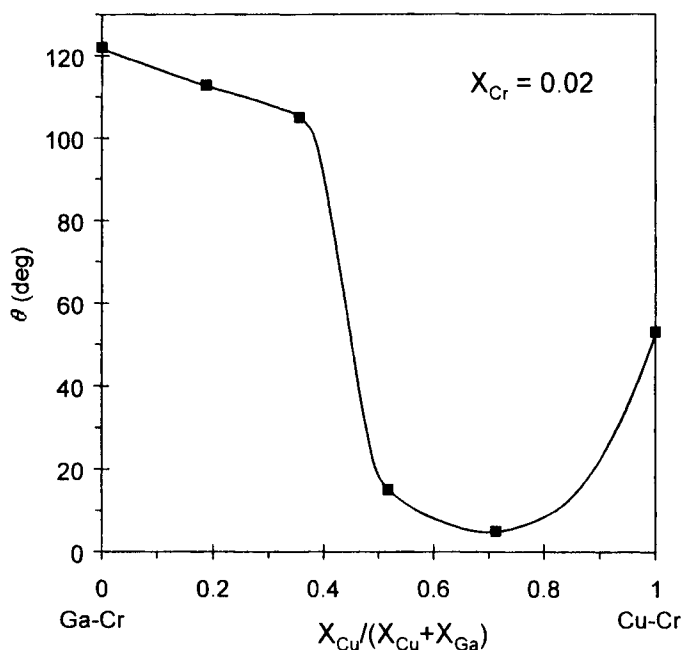


when M is Cu. The critical value  $X_{\text{Cr}}^*$  depends not only on the molar Gibbs energy of carbide formation,  $\Delta G_f^0$ , but also on the activity coefficient of Cr in the matrix M,  $\gamma_{\text{Cr}}$ :

$$X_{\text{Cr}}^* = \frac{1}{\gamma_{\text{Cr}}} \exp \frac{\Delta G_f^0}{3RT} \quad (8.2)$$

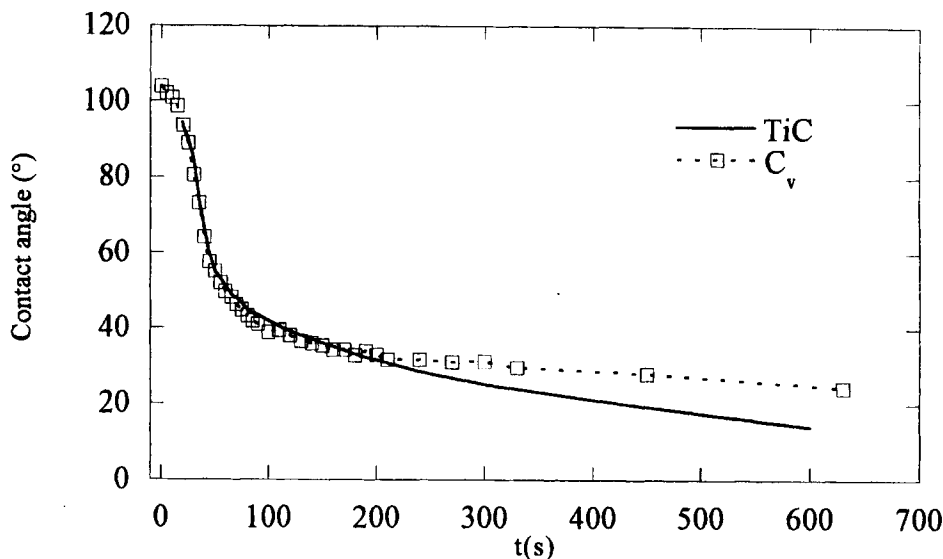
As Cu-Cr interactions in the liquid alloy are very weak,  $\gamma_{\text{Cr}}$  is much higher than unity and for dilute alloys is about 50 so values of  $X_{\text{Cr}}^*$  are small, as indicated by the wetting transition in Figure 8.10. In matrices such as Ga (Naidich and Chuvashov 1983) or Ni-Pd (Kritsalis et al. 1991), much lower values of  $\gamma_{\text{Cr}}$  cause the wetting transition to occur at much higher values of  $X_{\text{Cr}}^*$  (see Figure 8.11 for Ga-Cr alloys). It is interesting to note that contact angles lower than those obtained for Cu-Cr and Ga-Cr binary alloys have been observed with ternary

Cu-Ga-Cr alloys on graphite (Figure 8.12). Adding Cu to Ga while keeping  $X_{Cr}$  constant increases the activity of Cr and above a critical value causes formation of Cr carbide to induce wetting. On the other hand, adding Ga to Cu causes the surface energy of the liquid to diminish and the contact angle decreases in accord with the Young-Dupré equation (for instance, the addition of 20 at.% Ga to Cu decreases the surface energy of Cu by 30%). As a result, the contact angle isotherm of Ga-Cu-Cr alloys with constant  $X_{Cr}$  passes through a minimum (Figure 8.12).



**Figure 8.12.** Variation of contact angle for Ga-Cu-Cr alloys ( $X_{Cr} = 0.02$ ) on graphite at 1173K (except for Cu-Cr: 1423K). From data reported in (Naidich and Chuvashov 1983).

Ti additions to Cu and also to Sn, Ag (Naidich and Kolesnichenko 1968), Ga (Naidich and Chuvashov 1983) or Ni-Pd (Kritsalis et al. 1991) also produce a non-wetting/wetting transition due to the formation of a wettable reaction product (TiC). Note that although there is some uncertainty about the wettability of TiC by pure non-reactive metals, it is clearly established that TiC is wetted by these metals when they contain even low concentrations of Ti leading to the formation of hypostoichiometric TiC at the interface (see Section 7.2, Figure 7.32). An example

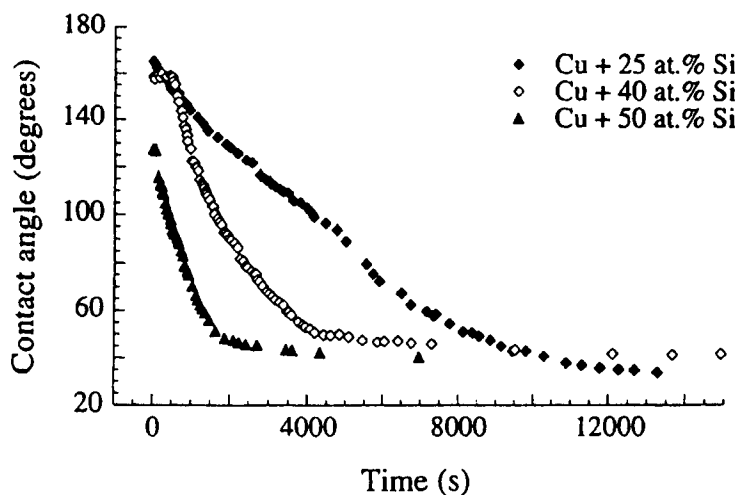


**Figure 8.13.** Variation of contact angle with time for CuAg-2.7 at.% Ti alloys on vitreous carbon and TiC at 830°C in high vacuum (Ljunberg et al. 1999).

is given in Figure 8.13 for CuAg-Ti alloys on vitreous carbon. Similar results have been obtained on graphite and diamond by alloying non-reactive metals such as Sn, Cu, Au or Ag with Ti, V, Nb or Ta which also form metal-like carbides (Naidich 1981).

Improvements in wetting by non-reactive metals can be produced also by adding Al or Si which form covalent carbides, as shown for Cu-Si alloys on vitreous carbon in Figure 8.14. In the Cu-Si/C system at 1100°C, formation of SiC occurs for  $X_{Si} > X_{Si}^J \cong 0.15$  (see equation 7.4). This relatively high value of  $X_{Si}^J$  is due to the low value of  $\Delta G_{f(SiC)}^0$ , compared to  $\Delta G_{f(TiC)}^0$  for instance, and to the small value of  $\gamma_{Si}$  in Cu, compared to  $\gamma_{Cr}$  in Cu for instance. For all Cu-Si alloys, the initial contact angle is that of a nearly unreacted alloy on C which is much higher than 90° (Figure 8.14). The kinetics of spreading are controlled by the formation of SiC at the alloy/C/vapour triple line, as for pure Si on C. However, because both the experimental temperature and the Si activity are much lower than for pure Si, the kinetics are 2 to 3 orders of magnitude slower than the 1 minute for pure Si (Section 8.2.1).

Several attempts have been made to improve wetting of Al on different kinds of C substrates by use of alloying elements, but no promising results have been obtained (Manning and Gurganus 1969, Nicholas and Mortimer 1971,



**Figure 8.14.** Contact angle kinetics for Cu-Si alloys on vitreous carbon at 1423K (Landry et al. 1996) [26].

Eustathopoulos et al. 1974). In certain cases, limited improvement in wetting has been observed due to an effect of the alloying element on the stability of the oxide layer covering Al rather than to an effect on intrinsic interfacial energies of the system. A typical example of this is provided by Mg additions (Eustathopoulos et al. 1974).

Landry et al. (1998) attempted to improve wetting of vitreous carbon by deoxidized Al by adding 0.8 at.% Ti. At the experimental temperature of 1223K, this concentration is close to the maximum solubility of Ti in liquid Al but neither the spreading kinetics nor the final contact angle were improved (Figure 8.15).  $\text{Al}_4\text{C}_3$  was observed on the carbon side of the interface and TiC on the liquid side at the centre of the drop. However, only  $\text{Al}_4\text{C}_3$  was observed in the vicinity of the triple line (Figure 8.15), due to the consumption of Ti to form a micron-thick layer of TiC in the central region during the initial spreading. For this reason, TiC formation does not affect the final contact angle of the system. Sobczak et al. (1996) avoided Ti exhaustion by using Al-Ti alloys supersaturated in Ti and observed contact angles as low as  $20^\circ$ .

### 8.3. CONCLUDING REMARKS

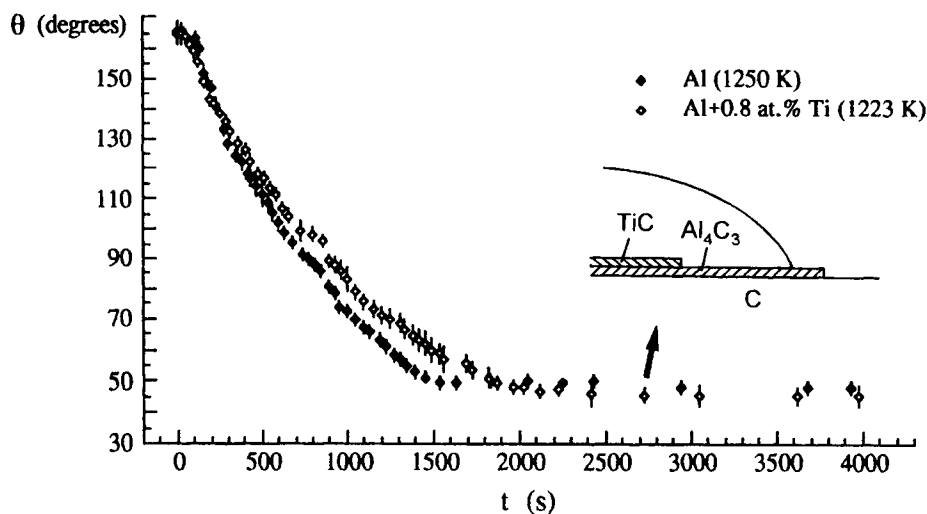
Non-reactive systems of graphite and Ag, Au, Cu, Pb, Sn, etc. are non-wetting with contact angles of about  $120^\circ$  due to the action of only van der Waals

dispersion forces between the metal and C atoms. As for non-reactive metal/ionocovalent oxide systems, contact angles and work of adhesion of metals on graphite change only slightly with temperature. An improvement in wetting is obtained by alloying with elements that form wettable metal-like carbides, such as Cr, V and Ti, or covalent carbides, such as Si and Al. In this case, spreading kinetics depend critically on temperature.

The ferrous metals Fe, Ni, Co, etc. dissolve graphite and the resultant wetting behaviour is very complex and not yet understood. More work is needed to quantify wetting in terms of true, Young, contact angles and to identify the effect on wetting of dissolved C and the crystallographic orientations of the graphite surface.

Pure Al and Si react with graphite substrates to form wettable Al and Si carbides. However, the reaction kinetics are so slow at temperatures close to the melting point of Al that Al behaves as a non-reactive and non-wetting metal.

These conclusions are also valid for vitreous carbon and diamond although some differences exist in the final contact angle for non-reactive metals and the spreading kinetics for reactive metals.



**Figure 8.15.** Contact angle kinetics for Al and Al-0.8 at.% Ti on vitreous carbon at 1250K and 1223K respectively (Landry et al. 1998) [17].

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## Chapter 9

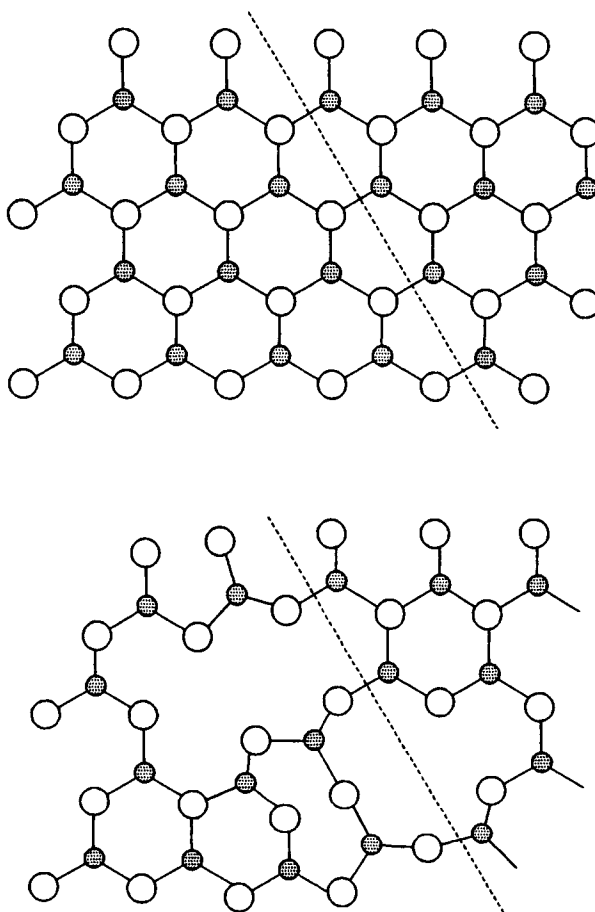
# Wetting by glasses and salts

A glass is a material that cools from the liquid state to form a rigid solid without crystallising. There are organic and metallic glasses but for the present purpose, attention will be confined to inorganic glasses and particularly those based on  $\text{SiO}_2$  or silicates. These glasses can be used to produce joints between metal or ceramic components by glazing, the inorganic analogue of brazing (see Section 10.4.3).

### 9.1. THE GLASSY STATE

Glasses do not have sharply defined melting temperatures, their structures being those of super-cooled liquids even when they are apparently and effectively rigid solids. The classic glass material is  $\text{SiO}_2$ , which as a crystalline solid has a lattice structure composed of a regular array of  $\text{Si}^{4+}$  ions surrounded by a tetrahedron of much larger  $\text{O}^{2-}$  ions, but the structure produced by fast cooling is a random network of tetrahedra. This randomness is difficult to illustrate for a three dimensional structure, particularly one composed of such disparate sized ions as  $\text{Si}^{4+}$  and  $\text{O}^{2-}$ , which have radii of 0.039 and 0.132 nm respectively, but some insight can be gained from the two dimensional analogue shown in Figure 9.1 for the hypothetical compound  $\text{J}_2\text{O}_3$ . A regular close-packed hexagonal array is shown as representative of the crystalline form, but the random glassy structure shown below contains broken chains and large holes. Thus the glassy form is more open and less rigid and will deform when subjected to even small stresses, exhibiting viscous flow. As the temperature is decreased below the melting temperature, the glass becomes stiffer and a temperature  $T_G$  can be identified below which it behaves like a rigid solid.

The characteristic features of inorganic glasses, large anion groups irregularly arranged to form broken networks containing large holes, define physical parameters of importance to capillarity. The size of the anion groups means that even fully liquid glasses have high viscosities compared to liquid metals, as demonstrated by the data summarised in Table 9.1 for some glassy silicates. Similarly, the surface energies of the glassy silicates are low compared to metals owing to at least two causes. First, the number of bonds broken per unit area during surface creation is lower than for crystalline oxides because of the numerous defects in bulk glasses, shown schematically in Figure 9.1. Second, their open structures readily permit small spatial adjustments to minimise the energy penalty



**Figure 9.1.** The two-dimensional structures of a hypothetical compound  $J_2O_3$  as, top, a crystalline solid and, bottom, a glass. The  $J^{3+}$  ions are shown as small shaded circles and the  $O^{2-}$  ions as open circles. The dashed lines represent the traces of surface planes. Because of the numerous defects contained in the glass, the surface energy change corresponding to the reversible creation of a new surface is lower than that of the corresponding crystalline solid.

of surface creation. For these reasons, the surface energy cannot be related in a simple way to pair energies in the bulk.

The differences between the values of viscosity,  $\eta$ , and liquid surface energy,  $\sigma_{LV}$ , of metals and glasses are of importance because the ratio  $\sigma_{LV}/\eta$  is of major significance in determining spreading rates (see equation (2.4)) and flow rates in capillaries (see equation (10.1)). For glassy materials, the ratio is less, and

sometimes much less, than  $0.1 \text{ m.s}^{-1}$ , as opposed to several hundred  $\text{m.s}^{-1}$  for liquid metals and alloys.

**Table 9.1.** Properties of some glassy silicates,  $\text{SiO}_2$  (Turkdogan 1983) and Cu. The values of density,  $\rho$ , viscosity,  $\eta$  and liquid surface energy,  $\sigma_{LV}$ , are for  $T_F$ .

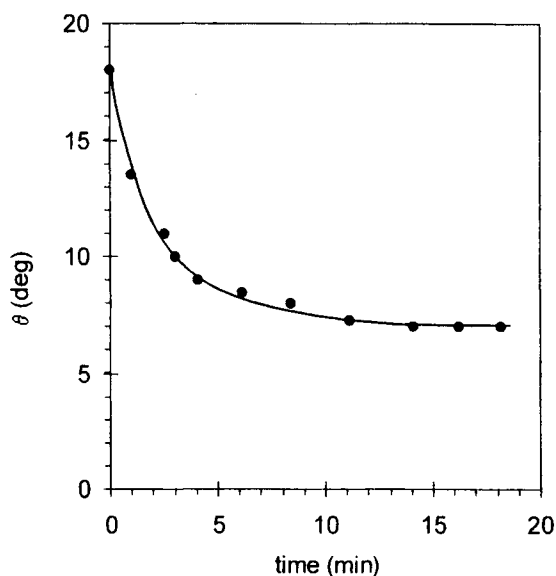
Material	$T_F$ (K)	$T_G$ (K)	$\rho$ ( $\text{Mg.m}^{-3}$ )	$\eta$ (Pa.s)	$\sigma_{LV}$ ( $\text{J.m}^{-2}$ )
$\text{Na}_2\text{O}-3\text{SiO}_2$	1043	775	2.14	7.8	0.28
$\text{Na}_2\text{O}-2\text{SiO}_2$	1147	725	2.25	2.8	
$\text{K}_2\text{O}-2\text{SiO}_2$	1318	763	2.20	8.0	0.22
$\text{Na}_2\text{O}-\text{Al}_2\text{O}_3-3\text{SiO}_2$	1391	1088	2.28	$>10^3$	
$\text{CaO}-\text{Al}_2\text{O}_3-2\text{SiO}_2$	1826	1086	2.45	4.0	0.40
$\text{SiO}_2$	1993	1373	2.08	$10^{5.6}$	0.31
Cu	1356	NA	8.0	$4.3 \times 10^{-3}$	1.35

## 9.2. WETTING BEHAVIOUR

As oxide materials, glasses can be expected to, and do, wet *oxide components* exceedingly well, Figure 9.2. Further, the growth of oxide films on metal substrates has been used to promote wetting, (Nicholas 1986a, Tomsia and Pask 1990). The basic reason for this behaviour is the similarity of the binding forces of the glass and the solid oxide and hence the high degree of electronic continuity across the solid/liquid interface. This reason explains why ionic non-oxide ceramics can be well wetted by glasses, as shown by the  $20^\circ$  contact angle of a lead zinc borate glass on  $\text{MgF}_2$  at  $600^\circ\text{C}$ , (Freeman et al. 1976).

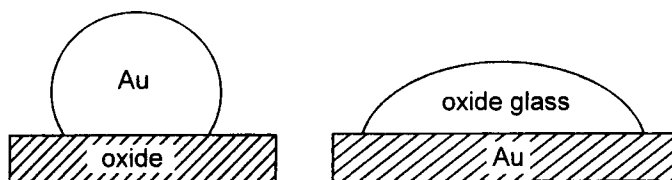
The excellent wetting of oxides by glasses is exploited in the bonding of  $\text{Si}_3\text{N}_4$  and other high temperature structural ceramics which, as discussed in Section 7.1.2, are usually covered by oxide, oxynitride or oxycarbide layers. The greatest success has been achieved with glass compositions that resemble those naturally present as intergranular phases, (Peteves et al. 1996). Particularly effective wetting has resulted from the use of compositions based on mixtures of the sintering additives  $\text{Al}_2\text{O}_3$ ,  $\text{Y}_2\text{O}_3$  and  $\text{MgO}$  and of  $\text{SiO}_2$  which is present as an impurity in  $\text{Si}_3\text{N}_4$ , (Mecartney et al. 1985). Other compositions found to be successful with  $\text{Si}_3\text{N}_4$  include reactive mixtures that dissolve some of the ceramic or form  $\text{Si}_2\text{N}_2\text{O}$  at the glaze/ceramic interface as a bonding phase. Thus compositions used to join  $\text{Si}_3\text{N}_4$  include  $\text{ZrO}_2$ - $\text{ZrSiO}_4$ ,  $\text{MgO}$ - $\text{SiO}_2$ - $\text{Al}_2\text{O}_3$ ,  $\text{Y}_2\text{O}_3$ - $\text{Al}_2\text{O}_3$ - $\text{SiO}_2$ ,  $\text{CaO}$ - $\text{SiO}_2$ - $\text{TiO}_2$

and  $\text{SiO}_2\text{-MgO-CaO}$ , (Becher and Halen 1985, Iwamoto et al. 1985, Peteves et al. 1996).



**Figure 9.2.** Variations of contact angle values with time observed for a  $\text{Al}_2\text{O}_3\text{-32.4SiO}_2\text{-30.6CaO}$  (wt.%) slag on  $\text{Al}_2\text{O}_3$  at  $1415^\circ\text{C}$ , (Towers 1954) [27].

The wetting behaviour of *glass/metal systems* was first examined in the pioneer work of Ellefson and Taylor (1938) in the case of a non-reactive system consisted of a sodium silicate glass (with a composition close to  $2\text{Na}_2\text{O-3SiO}_2$ ) on solid Au (see also the study performed by Pask and Tomsia (1981) in the same system). As Au has no affinity for O and the adsorption of O on Au is negligible, no reaction can be expected and the contact angle measured in a vacuum, as well as in  $\text{N}_2$  and  $\text{O}_2$  atmospheres, is  $55\text{--}60^\circ$ . These values correspond to a work of adhesion of only  $0.45\text{--}0.5\text{ J.m}^{-2}$ , which is typical of those obtained for liquid metal/solid oxide systems when only van der Waals forces act across the interface (see Section 6.2.2) even though the contact angles are much higher. According to the Young-Dupré equation  $\cos\theta = (W_a/\sigma_{\text{LV}}) - 1$ , the similar values of  $W_a$  imply that the differing wetting behaviour of liquid Au on a solid oxide and glass on solid Au, Figure 9.3, is due in the main to the differing values of  $\sigma_{\text{LV}}$ :  $1.14\text{ J.m}^{-2}$  for Au and about  $0.3\text{ J.m}^{-2}$  for oxide glasses, Table 9.1. Thus despite the low value of  $W_a$ , non-reactive glasses may wet metal surfaces because of their low surface energies.



**Figure 9.3.** Schematic representation of the configurations that can be assumed by Au-oxide systems. Molten Au does not wet ionocovalent oxides ( $\theta \cong 135^\circ$ ) while molten glasses wet solid Au ( $\theta \cong 60^\circ$ ).

In a  $N_2$  atmosphere and in vacuum, the sodium silicate glass wets Pt, the contact angle being  $60\text{--}65^\circ$ . However, in this case, a significant decrease of the contact angle was observed when the experiments were repeated in a  $O_2$  atmosphere. Regarding spreading rates, Ellefson and Taylor (1938) found that the spreading rate of sessile drops scales with the inverse of the viscosity of the glass.

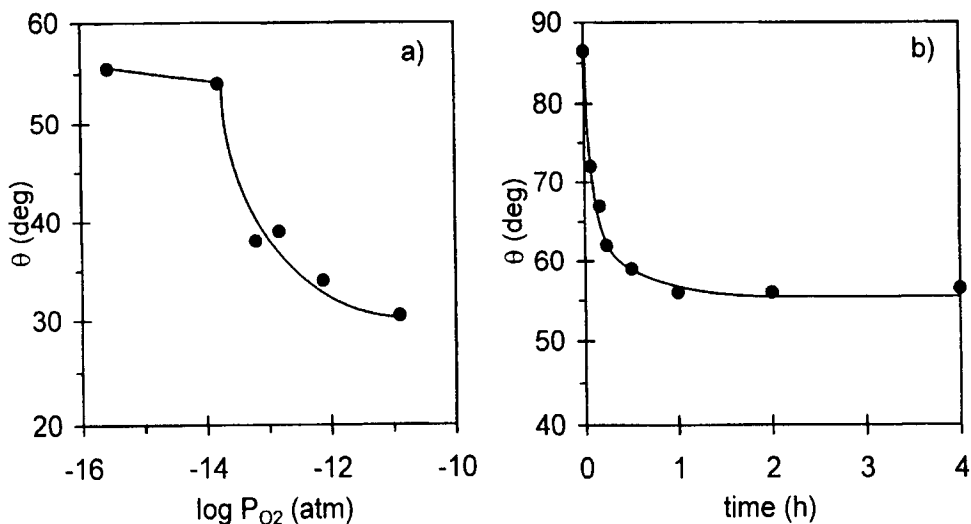
Good wetting with contact angles in the range  $40\text{--}60^\circ$  has also been observed for several slags containing chemically stable oxides such as  $Al_2O_3$ ,  $SiO_2$ ,  $CaO$  or  $MgO$  when in contact with Pt, Table 9.2. A systematic study by Towers (1954) showed that the contact angle values for non-reactive slag/Pt couples varied little with slag composition or temperature. The effect of the partial pressure of  $O_2$ ,  $P_{O_2}$ , when comparing measurements made in air or  $N_2$ , was weak but significant, Table 9.2. Similarly, the effect of  $P_{O_2}$  on the wetting of W by a  $SiO_2\text{--}20Al_2O_3\text{--}10CaO\text{--}10MgO$  (wt.%) mixture has been studied using gas buffer systems ( $CO/CO_2$  and  $H_2/H_2O$ ), (Ownby et al. 1995). Wetting was found to be independent of temperature in the range  $1300\text{--}1500^\circ C$  but the contact angle values were found to decrease when  $P_{O_2}$  was raised, Figure 9.4. Adsorption of oxygen can occur at both the metal/vapour and glass/metal interfaces and this will result in the formation of W-O bonds with a partially ionic character and to the development of ionic interactions between the modified W surface and the oxide glass, Figure 9.5.b. As with liquid metals in contact with solid oxides, the energy decrease of the metal/vapour surface is less than that of the glass/metal interface, so that  $W_a$  is increased and wetting is enhanced.

A further enhancement in wetting and bonding can occur if the metal surface has been oxidised. Thus a twofold increase in  $W_a$  was achieved when Fe and steel surfaces were oxidised before being contacted by silicate slags, Figure 9.5.c, (Perminov et al. 1961). Enhancement can be achieved also by the *in situ* oxidation of the metal by reaction with a slag oxide that has a low thermodynamic stability. Extensive studies of interfacial reactions and bonding in glass/metal systems have been performed by Pask and Tomsia, (1981, 1987, 1993), and these have shown that *in situ* oxidation of the metal and enhancement of wetting occur when CoO is added to Na-silicate glasses that are brought into contact with Fe, (Pask and

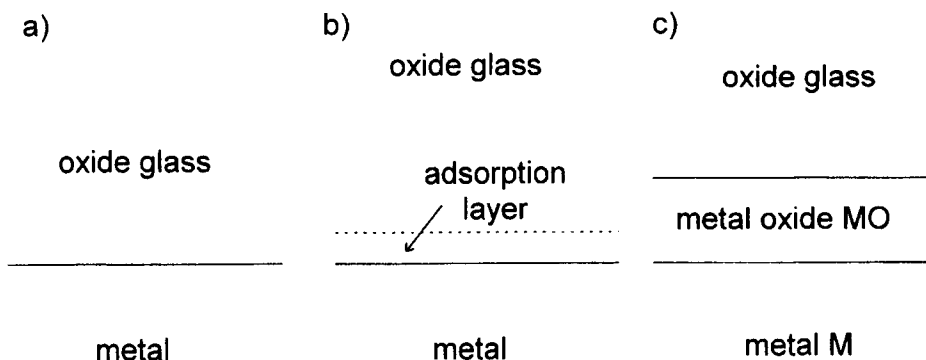
**Table 9.2.** Contact angle and work of adhesion values for slag/Pt systems, (Towers 1954).

Slag composition (wt.%)	Temperature (°C)	Atmosphere	$\theta$ (deg)	$\sigma_{LV}$ (J.m <sup>-2</sup> )	$W_a$ (J.m <sup>-2</sup> )
SiO <sub>2</sub> -40CaO	1500	air	49.5	0.37	0.60
SiO <sub>2</sub> -38CaO-20Al <sub>2</sub> O <sub>3</sub>	1300	N <sub>2</sub>	50	0.42	0.68
	1300	air	43	0.42	0.72
CaO-34SiO <sub>2</sub> -27Al <sub>2</sub> O <sub>3</sub>	1410-1550	air	42.5	0.45	0.77
SiO <sub>2</sub> -20MgO-18Al <sub>2</sub> O <sub>3</sub>	1410	N <sub>2</sub>	64.5	0.33	0.47
	1410	air	47	0.33	0.55
MnO-30SiO <sub>2</sub> (*)	1400	N <sub>2</sub>	2	0.49	0.99

(\*) there is a chemical reaction between the slag and Pt



**Figure 9.4.** Contact angle values for SiO<sub>2</sub>-20Al<sub>2</sub>O<sub>3</sub>-10CaO-10MgO (wt.%) on W at 1400°C plotted as (a) a function of log P<sub>O2</sub> and (b) as a function of time for log P<sub>O2</sub> = -15.5, (Ownby et al. 1995).



**Figure 9.5.** A schematic representation of glass/metal interactions: (a) a simple non-reactive oxide glass/metal interface across which only van der Waals interactions are developed; (b) a more intense interaction between the metal and the oxide glass is developed by the presence of an adsorption layer with a typical thickness of  $\sim 1$  nm that is rich in oxygen; (c) improved wetting and bonding produced by preoxidation or *in situ* oxidation of the metal that leads to the creation of a glass/MO interface.

Tomsia 1981). Similarly, the presence of MnO in the glass seems to be the cause of the almost perfect wetting of Pt by MnO-30SiO<sub>2</sub>, Table 9.2.

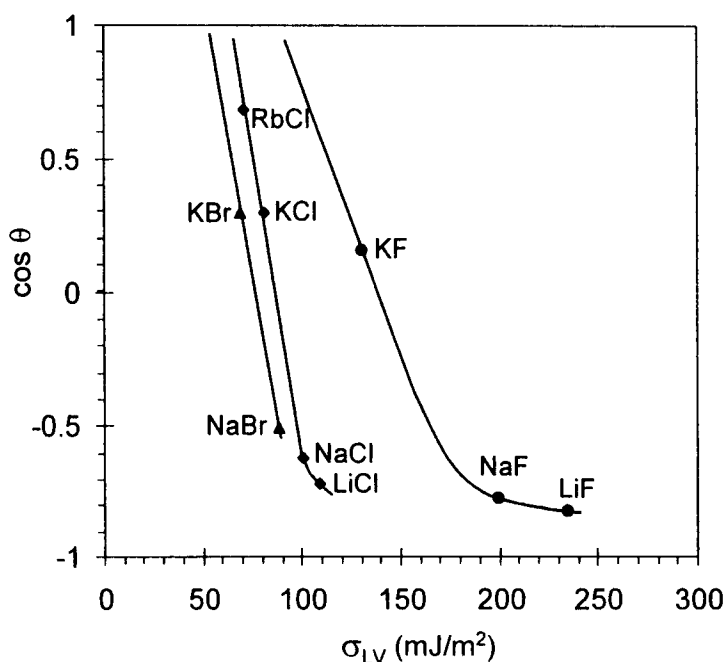
The viscosities of glasses are several orders of magnitude higher than those of metals so that spreading to assume an equilibrium contact angle can continue for minutes or even hundreds of minutes, Figure 9.4.b. Such spreading curves can be described by the de Gennes-Tanner model of viscous spreading for non-reactive couples (Section 2.1.2). However, marked departures from the predictions of this model can be observed in systems where spreading is accompanied or caused by chemical reactions at the liquid/solid interfaces, (Nicholas 1986b).

It is generally accepted that mixtures of molten oxides (glasses, slags) do not wet *graphite*. For instance, Ellefson and Taylor (1938), in their measurements of surface tension of molten silicates in N<sub>2</sub> by the sessile drop technique, used graphite substrates that produce contact angles as large as 130-160°. As these values were obtained on electrode graphite with a high porosity and a high surface roughness, they are only rough estimates of Young contact angles. However, these values suggest that interfacial bonding is ensured by weak, van der Waals, interactions. The non-wetting of graphite by oxide slags is regarded as one of the advantages of carbon bricks in the blast-furnace (Towers 1954). However, for certain slags, the contact angle appears to decrease with time towards values lower than 90° as a result of interfacial reactions between the slag components and carbon. For instance, initial contact angles close to 160° were measured on polished surfaces of graphite in N<sub>2</sub> at temperatures in the range 1330-1450°C for a slag SiO<sub>2</sub>-40CaO-20Al<sub>2</sub>O<sub>3</sub> (wt.%). Thereafter, the contact angle decreased slowly



and passed below  $90^\circ$  after a few hours. This decrease was explained by reactions occurring between the less stable component of the slag ( $\text{SiO}_2$ ) and carbon (Towers 1954).

As glasses, many molten halides ( $\text{NaCl}$ ,  $\text{NaF}$ ,  $\text{LiF}$ , etc) (Morel 1970) or mixtures of halides ( $\text{CaF}_2$ - $\text{MgF}_2$  of eutectic composition) (Minster 1984) do not wet graphite. However, some low-surface-energy halides wet graphite as shown by the correlations between  $\cos\theta$  and  $\sigma_{\text{LV}}$  given in Figure 9.6.



**Figure 9.6.** Contact angles of pure molten halides on graphite measured in a dry inert gas at  $1000^\circ\text{C}$  as a function of surface energies of halides (Morel 1970).

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## Chapter 10

# Wetting when joining

Brazing and soldering are widely used methods for joining metals and ceramics that employ a liquid metal or alloy as the bonding material. The term “brazing” arose from the original use of brass as the joining material but nowadays a wide range of alloys are used and brazing is differentiated from soldering by virtue of the joining materials having melting temperatures in excess of 450°C, (Schwartz 1995).

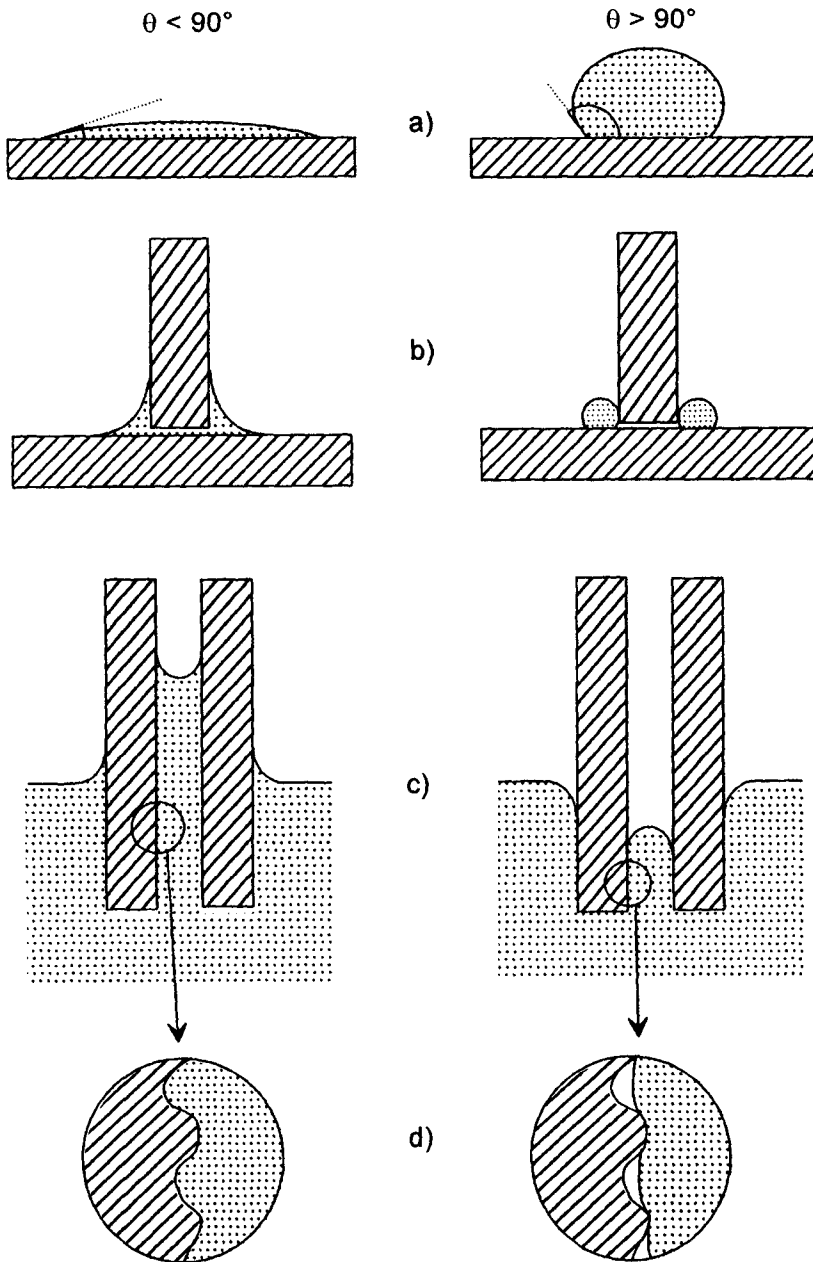
The process depends on a liquid metal flowing over surfaces to form a fillet between components and into the gap between the components, and then solidifying to form a permanent bond. Thus it is essential that the braze experiences high temperature capillary attraction. Without such attraction, solid braze material placed between components will flow out of the gap, “sweat”, when it melts. Any residue of non-wetting liquid that remains within the gap will not conform to the microscopic features of the component surfaces but form an array of voids, as illustrated schematically in Figure 10.1, that is mechanically deleterious and should be avoided if at all possible. The size of such voids can be decreased if an external pressure is used to confine a non-wetting liquid braze into a gap but cannot eliminate them because the pressure needed to shrink voids increases as they become smaller.

Successful brazing depends not only on the characteristics of the liquid and the solid materials and of the vapour phase but also on the geometry and size of the joint. In the first Section, flow of liquid metals into idealised capillary gaps will be discussed. Thereafter, since the techniques used to join them differ somewhat, the role of wetting during the brazing of metal and of ceramic components will be considered separately. Finally, the role of wetting behaviour during joining by brazing-related techniques and of its influence on joint strengths will be discussed.

### 10.1. FLOW INTO CAPILLARY GAPS

#### *10.1.1 Predicted penetration rates*

The idealised flow of non-reactive liquids in smooth channels has been considered by founding physicists such as Newton and Poiseuille and is well understood. Slow flow of a liquid is laminar or streamlined while rapid flow is turbulent with the transition occurring when the Reynolds number - the dimensionless parameter ( $Ud\rho/\eta$ ) in which  $U$  is the velocity of the liquid,  $\rho$  and  $\eta$  are the density and



**Figure 10.1.** Schematic illustration of the influence of contact angles on the profiles of (a) sessile drops, (b) fillets between T configuration components, (c) the entry of liquid into capillary gaps and (d) the microscopic contact between the liquid and the solid components.

viscosity of the liquid and  $d$  is the width of a parallel sided channel - exceeds one to two thousand, (Bird et al. 1960). Strictly the density term,  $\rho$ , is the difference between the advancing liquid and the fluid it displaces, but this refinement can be ignored when the displaced fluid is a gas. Laminar flow is characterised by a velocity profile that varies right across the channel width from zero at its walls to a maximum in its centre, while the velocity profile of turbulent flow is almost uniform except in thin boundary layers at the walls. Note that even at low flow rates when laminar behaviour should prevail, entry into a channel and flow to a distance of a few widths is turbulent. Even if the liquid near the front in a partially filled tube also experiences turbulent flow, so that it moves from the centre to the walls of the tube, the front still advances at a rate determined principally by the laminar flow of the bulk of the liquid behind it, (Milner 1958).

The Reynolds numbers for the flow of a molten metal along a capillary braze gap are usually less than 1000 as will be shown later, and the theoretical laminar flow rates for such configurations have been calculated by Milner (1958) for both horizontal and vertical joints. He regarded the flow into a horizontal joint induced by capillary attraction as being impeded only by viscous drag, and derived a simple parabolic expression to describe such behaviour,

$$t = \frac{3\eta l^2}{\sigma_{LV} \cos \theta_Y d} \quad (10.1)$$

in which  $l$  is the penetration distance,  $t$  is the time,  $\sigma_{LV}$  is the liquid surface energy and  $\theta_Y$  is the Young contact angle. This expression predicts that flow will continue indefinitely. However, penetration of a vertical capillary is helped or impeded also by gravitational forces, and this complicates analysis of the penetration kinetics, leading to the relationship

$$t = \left[ \frac{12\eta}{\rho^2 g^2 d^3} \right] \left[ -\rho g l d - 2\sigma_{LV} \cos \theta_Y \log_e \left( 1 - \frac{\rho g l d}{2\sigma_{LV} \cos \theta_Y} \right) \right] \quad (10.2)$$

where  $g$  is the acceleration due to gravity. This equation describes an asymptotic approach to the equilibrium penetration, but expansion of the logarithm shows that the early stages of ascent can be described by the parabolic relationship presented as equation (10.1).

The predicted behaviour of individual liquid metals depends on their specific physical properties, such as those listed in Table 10.1 for Hg and a number of solder and braze metals and alloy solvents. Substitution of these values into

equation (10.1) predicts that penetration time of completely wetted horizontal gaps by various metals should be virtually identical because of the similarity of their  $\sigma_{LV}/\eta$  ratios, as illustrated in Figure 10.2.a. However predictions of the penetration kinetics of vertical gaps are more complex: penetration should approach an equilibrium height,  $l_e$ , that depends on the liquid density as well as its surface energy and which is defined by the equation:

$$l_e = \frac{2\sigma_{LV} \cos \theta_Y}{\rho g d} \quad (10.3)$$

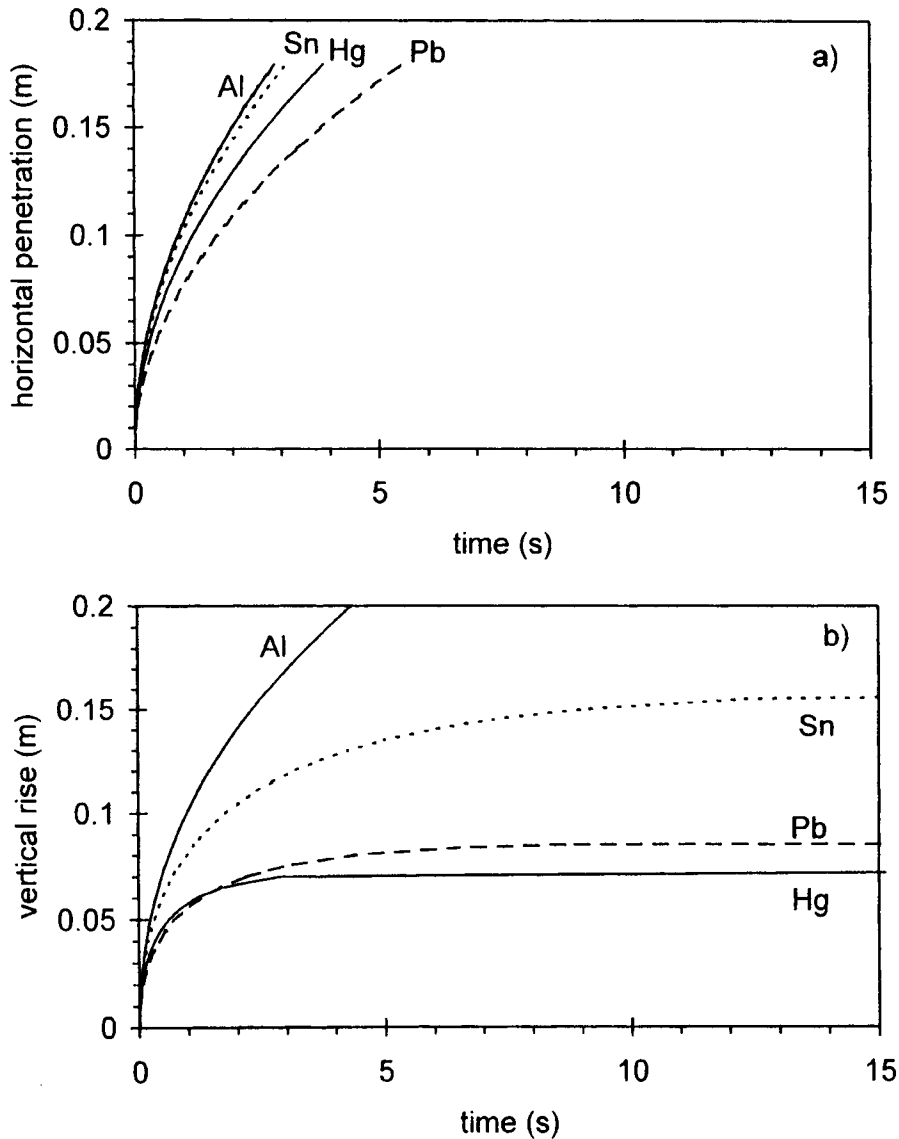
Note that equation (10.3) is similar to equation (1.55) for a gap of circular geometry. For completely wetted gaps,  $l_e$  differs up to one order of magnitude for the different metals of Table 10.1. For similar values of  $l_e$ , the penetration time decreases slightly with increasing  $\sigma_{LV}/\eta$ , as illustrated in Figure 10.2.b for Pb and Hg.

**Table 10.1.** Physical properties of some liquid metals (Iida and Guthrie 1988) and equilibrium rise,  $l_e$ , in a vertical perfectly wetted 0.1 mm wide parallel sided gap. Note that the  $\sigma_{LV}/\eta$  ratio for H<sub>2</sub>O is 70 and for a glass at a typical glazing temperature falls in the range of  $10^{-3}$  to  $10^{-4}$ .

Metal	$T_F$ (°C)	$\sigma_{LV}$ (J.m <sup>-2</sup> )	$\eta$ (mPa.s)	$\rho$ (Mg.m <sup>-3</sup> )	$\sigma_{LV}/\eta$ (m.s <sup>-1</sup> )	$l_e$ (m)
Hg	-39	0.50	2.0	13.7	250	0.07
Sn	232	0.56	1.8	7.0	311	0.16
Pb	328	0.46	2.6	10.7	176	0.09
Zn	420	0.78	3.5	6.6	222	0.24
Al	660	0.91	2.7	2.4	337	0.76
Ag	961	0.97	4.3	9.3	225	0.21
Au	1065	1.17	5.4	17.4	217	0.14
Cu	1083	1.30	4.3	8.0	302	0.32
Ni	1455	1.78	5.5	7.9	323	0.45

Differentiation of equation (10.1) to obtain a value of  $dl/dt$ ,  $U$ , permits the Reynolds number to be rewritten as equal to  $(\sigma_{LV} \cos \theta_Y \rho d^2 / (6\eta^2 l))$ . Assuming the workpieces are completely wetted, substitution of Table 10.1 data yields Reynolds numbers for a typical braze joint 0.1 mm wide and 10 mm long, (Schwartz 1995), ranging from 49.5 for Al to 117 for Au and even smaller numbers are obtained if the workpieces are not completely wetted so that  $\cos \theta_Y$  is less than 1. These values are much smaller than that needed to induce a transition in flow behaviour, and

therefore it can be predicted that even exceptionally wide or short braze joints will be filled by predominantly laminar flow.



**Figure 10.2.** Predicted flow of liquid metals into completely wetted 0.1 mm wide parallel sided gaps: (a) horizontal gaps, (b) vertical gaps.

### 10.1.2 Experimental results

Quantitative descriptions of the flow or spreading behaviour of real systems of relevance to high temperature capillarity are not numerous but the published observations do illustrate the importance of material and process factors. Most published work describes the spreading of sessile drops because of the easier experimental techniques (see Chapter 2).

*The flow along horizontal capillary channels* was observed by Latin (1946) who found that penetration of parallel sided channels made from tinned Cu by fluxed Sn was predicted precisely by equation (10.1) when  $\cos\theta_Y$  was equated to 1. However, flow along channels that had not been tinned was only half as fast even though  $\cos\theta_Y$  for Sn on Cu was about 0.9. This discrepancy implies that the rate of advance was controlled by a Sn-Cu interaction at the liquid front.

When analysing the behaviour of fluxed soldering or brazing systems, attention must be paid to the characteristics of the flux as well as the liquid metal so that, for example, the density term,  $\rho$ , should be replaced by the difference in density between the two fluids.

*Vertical penetration of capillaries* in sintered metal compacts was examined by Semlak and Rhines (1958) who found the rates of rise of molten Cu in Fe compacts and of Pb in Cu compacts up to heights of about 20% of the calculated equilibrium ascent to be in excellent quantitative agreement with the predictions of equation (10.2). However, the observed rate of rise of Ag in Cu compacts was twice that predicted by equation (10.2) because structural rearrangement of the compact during penetration increased the effective radius of the capillaries.

*Fillet formation* when brazing Al alloys with Al-Si brazes has been studied using a hot stage fitted in a scanning electron microscope, (Nicholas and Ambrose 1989). Joint formation is slow, a 2 mm high fillet taking minutes to form rather than the millisecond or less suggested by modelling ideal systems. This retardation is because the main constraint to braze flow and fillet formation is not viscosity but the  $\text{Al}_2\text{O}_3$  films present on the liquid and solid surfaces. That on the braze has to be disrupted by evolution of volatile Mg additions from the liquid, while that on the solid is displaced by "tunnelling" i.e., by penetration of the braze at the oxide/Al alloy interface through naturally occurring flaws of the oxide.

## 10.2. JOINING METAL COMPONENTS

*Braze fluidity* can be assured only if the joining temperature is higher than the braze liquidus. The viscosities of liquid metals are relatively low, only a few mPa.s, Table 10.1, and decrease slowly as the temperature is raised. A dramatic increase in viscosity can occur, however, if the temperature drops below the



liquidus so that the braze structure becomes a liquid-solid mixture. Other factors affecting the selection of a suitable joining temperature are the need for the braze liquidus to be lower than the component solidus, and often to be a lot lower if detrimental microstructural changes are to be avoided. Similarly, it is necessary for the braze solidus to be sufficiently high to withstand any possible service temperatures.

Brazes with very varied melting temperatures have been developed for joining metal components of steel, Ni base alloys or Al alloys and braze compositions have been codified in national and international standards. Al alloy brazes are recommended only for the joining of Al alloy components, but brazes based on Ag or Cu or their alloys can be used for the joining of a wide range of component materials including steels, Ni alloys, precious metals and refractory metals, while Ni alloy brazes find applications in the production of high temperature joints between steel or Ni alloy components. Such recommended brazes are generally a pure metal or are based on eutectic alloys that have singular melting temperatures, as can be seen in Table 10.2 which lists some widely used brazes. Selection of brazes with singular melting temperatures or sharp melting ranges enables the fabricator to specify very precisely defined joining temperatures and to avoid or at least minimise the possibility of "liquation", i.e., the premature flow of low melting temperature phases over surfaces or into gaps between components during the heating process as the temperature is raised through the solidus-liquidus range, which could leave refractory phases outside the joint and result in incomplete filling.

While the use of pure metals and eutectic alloys as brazes is generally good practice, exceptions do occur. Thus it may be necessary to use brazes that deviate from eutectic compositions to minimise the concentration of an embrittling temperature depressant, or to complicate the melting characteristics and accept degraded fluidity by introducing elements that enhance the corrosion resistance of the solidified braze. Thus recommended Al-Si brazes have hypo-eutectic compositions and Cr is introduced into Ni-P and Ni-Si-B braze alloys.

*The capillary attraction* exerted by clean metal surfaces on metallic brazes is high. Indeed the contact angles of liquid metals on clean metal substrates is invariably less than, and usually much less than, 90° even for chemically inert and mutually insoluble systems, as discussed in Chapter 5.

Of even more practical importance in determining the behaviour of systems is the tendency of many component materials, and some brazes, to form chemically stable and physically tenacious oxide films when their surfaces are exposed to even mildly oxidising environments. (Note that these oxides are in turn covered by absorbed layers of organic contaminants, but these can be removed relatively easily by washing in solvents, vapour degreasing or baking in a vacuum). Oxide films can

**Table 10.2.** Some brazes for metal components.

AWS code (*)	Alloy composition (wt.%)	Melting range (°C)	AWS code (*)	Alloy composition (wt.%)	Melting range (°C)
	Ag	960	BCu-1	Cu	1083
BAG-8	Ag-28Cu	780	BAu-1	Cu-37.5Au	990-1010
BAG-1a	Ag-15Cu-17Zn-18Cd	620-640	BCuP-2	Cu-7.5P	732
BAG-3	Ag-16Cu-16Zn-16Cd-3Ni	630-660	BCuP-4	Cu-6Ag-7P	643-813
BAG-5	Ag-30Cu-26Zn	690-775	BCuP-5	Cu-15Ag-5P	643-801
BAISi-2	Al-7.5Si	565-625	BNi-2	Ni-7Cr-3B-4.5Si-3Fe	970-1000
BAISi-3	Al-10Si-3Cu	550-570	BNi-3	Ni-3B-4.5Si-1.5Fe	980-1040
	Al-10Si-1.5Mg	555-577	BNi-4	Ni-2B-3.5Si-1Fe	980-1070
	Au	1065	BNi-5	Ni-19Cr-10Si	1080-1135
BAu-2	Au-20Cu	890	BNi-6	Ni-11P	880
BAu-4	Au-19Ni	950	BNi-7	Ni-14Cr-10P	890

(\*) American Welding Society

be responsible for beneficial characteristics such as the corrosion resistance of Al, Fe-Ni-Cr and Ni-Cr components conferred by surface coverage by  $\text{Al}_2\text{O}_3$  or  $\text{Cr}_2\text{O}_3$ , but other aspects of their presence are not beneficial. Oxides are wetted only by a few braze metals or alloys as described in Chapter 6, while the oxide films on molten brazes can inhibit liquid flow. Thus it is essential that oxide films on components and brazes should be destabilised, removed or at least disrupted if wetting is to be achieved. In practice this is achieved by using fluxes or controlled atmospheres.

The fluxes used when brazing are alkali halide and borate mixtures and compounds, and they have two main functions: first, to dissolve the oxide film on the component surface or at least to degrade its adhesion by penetration of naturally occurring flaws and electrolytic action at the oxide-substrate interface, and secondly to prevent formation on the liquid surface of oxide skins which would restrict braze flow. Fluxes can be contained in a bath held at the brazing temperature in which the, usually aluminium, component is placed or else applied as a paste to surfaces of the component or braze.

Fluxes for Al components based on  $\text{Na}_2\text{B}_4\text{O}_7/\text{KBF}_4$  mixtures were developed with the aim of dissolving  $\text{Al}_2\text{O}_3$  films from component surfaces and have been used successfully in practice for decades. However, this achievement is an illustration of serendipity because they do not dissolve the oxide films but merely undermine them, (Jordan and Milner 1956). Few systematic studies of flux action

for other brazing processes have been reported, but McHugh et al. (1988) examined some physical properties of a range of commercial fluoride/borate fluxes used with Ag or Cu brazes. They found that the fluxes had a network structure similar to glass which was degraded by an increasing F content. Flux viscosities were higher than those of the brazes with which they were used, varying over their working temperature ranges from  $10^3$  to  $5 \times 10^{-2}$  Pa.s and they were effectively impermeable to atmospheric  $O_2$ .

Adjustment of brazing torch chemistries can be used to produce reducing flames that not only heat but also clear away the oxide films on some component surfaces. Similarly, furnace brazing using controlled atmospheres of inert gases (generally Ar or He),  $H_2$  or reducing mixtures of  $N_2$  (or Ar)- $H_2$  (or CO), and vacua of  $10^{-4}$  mbar or less can be used to achieve environments in which flow is unrestrained by oxide skins and component surfaces are clean metals. Ag, Cu, Fe and Ni, but not Al, can destabilise their oxide skins at high temperatures by taking O into solution, (Massalski 1990), and  $Ag_2O$ ,  $Cu_2O$  and  $NiO$  also dissociate in even moderately O active environments (see Table 3.1). However, it is in practice impossible to achieve controlled atmospheres with  $O_2$  activities low enough to cause dissociation of stable oxides, thus dissociation of  $Cr_2O_3$  would require a partial pressure of less than  $10^{-45}$  bar at  $900^\circ C$  while that for  $Al_2O_3$  would be less than  $10^{-60}$  bar at  $600^\circ C$ . Nevertheless components covered with such oxides are brazeable. Thus the oxide films containing  $Cr_2O_3$  that are formed on surfaces of Fe-Cr-Ni components can be reduced when vacuum brazing by the presence of trace amounts of C in the steel, (Lugscheider and Zhuang 1982), or even by the low O activity within a liquid braze that covers a component surface, (Cohen et al. 1981, Thorsen 1984). The oxide can be removed also by penetration of naturally occurring flaws and undermining by dissolution of its metallic substrate, (Ambrose and Nicholas 1996). Again, the presence of Mo in the steel also can result in ready disruption of the surface oxides even in moderately oxidising environments, (Kubaschewski and Hopkins 1953, Gale and Wallach 1991), due to volatilisation of  $MoO_3$ , and volatilisation of Mg from Al-Si-Mg brazes causes disruption of the  $Al_2O_3$  films that otherwise encase the liquid braze and prevent its flow, (McGurran and Nicholas 1984).

The final treatment of the components before assembling to braze is often to create a particular surface finish. It is recognised that some roughening of a surface can result in enhanced wetting by inherently well wetting liquids in accord with the Wenzel equation (1.35). However, the use of very rough surfaces can degrade the strength of the braze/component interfaces. A British standard recommends that the roughness of a component surface should not be greater than  $1.6 \mu m R_a$  if the finish is anisotropic, (BS1723 1986a), while Schwartz (1995) recommends the use of abrasion with clean metallic grit to produce anisotropic roughness of  $0.8$ - $2.0 \mu m$

R<sub>a</sub>. The effects of substrate texture on wetting behaviour have been described in Section 1.3.1 and these lead to the expectation that anisotropic roughening will promote the spreading of very well wetting brazes but will impede that of moderately wetting brazes.

Relating these observations to brazing practice is complicated by the fact that the scientific studies showed the steepness of surface asperities can be a more significant characteristic than their maximum heights, but this parameter is not usually considered or quantified by brazing engineers. Thus the recommendations about component roughening cannot be assessed in terms of capillarity effects, and indeed it should be recognised that abrasion not only changes the topography of surfaces but also their chemistry by removing mature oxide films.

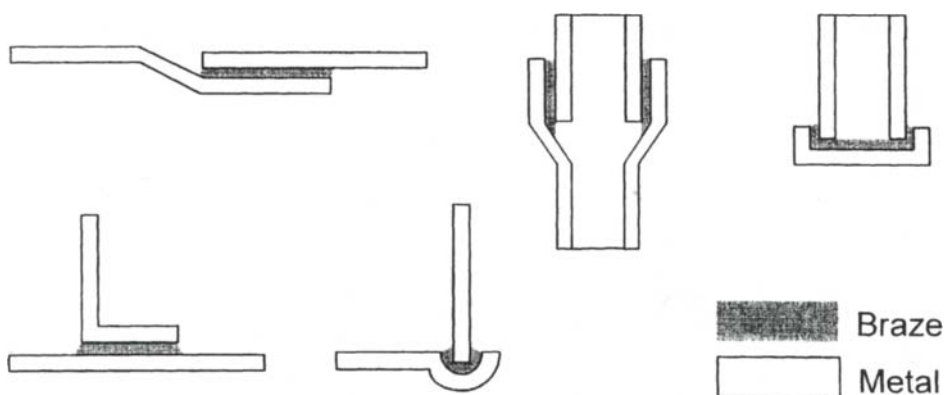
When suitable environments and surface preparation techniques are used, wetting should be achieved. Few recent data are available even for technically important braze/component systems apart from the early area of spread tests of Feduska (1959) with mainly Ni brazes on high-temperature base metals in high vacuum and dry He or H<sub>2</sub> and the more recent work of Keller et al. (1990) with Ag and Au brazes on stainless steels in high vacuum. These showed that interdiffusion induced by the differing complex chemistries of braze/component systems can affect the wetting behaviour of some systems quite markedly but does not completely obscure all the effects of process parameters and compositions. Thus it is clear that wetting is better for brazes with high liquidus, and therefore high use temperatures. Since the substrate surfaces were at least partially covered by oxide films, this temperature effect can be plausibly related to an increase in the rapidity with which these barriers to wetting are undermined and dispersed. As a general trend, at a fixed temperature, wetting in vacuum was superior to that obtained in dry H<sub>2</sub>. The data of Feduska and Keller et al. also show that further increasing the temperature at which a particular braze is used generally decreases the extent of wetting, and this can be attributed to the rapidity of braze/substrate interdiffusion resulting in premature solidification of the molten braze. Similar work by Amato et al. (1972) shows spreading of a Ni-13Cr-10P braze on a Ni alloy substrate at first increases and then diminishes as the temperature is raised progressively from 950 to 1050 and then to 1075°C.

Examination of the area-of-spread data of Keller et al. (1990) for AISI 304 stainless steel with a composition of a Fe-18Cr-10Ni-1Mn in wt.%, as are all compositions in this Chapter, shows that Au and Ag-Cu-Pd alloys wet extremely well and that the presence of a small amount of Ni or a large amount of Pd promotes wetting by Ag-Cu and Ag-Cu-Sn alloys. Similar effects on wetting have been observed for other Fe-Cr-Ni alloys, but the wetting of AISI 316 steel, (Fe-17Cr-12Ni-2.5Mo), was generally better than that of AISI 304 and this could be

due to the volatilisation of MoO providing more opportunity for liquid metal/solid metal contact and the creation of low energy interfaces.

The beneficial effects of Ni and Pd imply a decrease in the liquid/solid interfacial energy values, as discussed in Chapter 5. Work by researchers using other families of braze alloys has shown that the wetting of both steel and Ni alloy components by Ni brazes is promoted by the presence of B and Si which can flux, that is cause chemical reactions to disrupt the surface oxide, (Amato et al. 1972).

*Liquid flow* into joints will occur if the braze wets the component materials, but the penetration achieved is also a function of the configuration of the joint and, for vertical joints, the density of the liquid braze. Having selected a braze and an environment that promotes wetting, the configuration of the joint must be selected. Widely accepted standards of good design practice can be found in national and international specifications. These recommended designs take into account factors other than capillary phenomena, such as the general need to avoid tensile stressing of the brazed joint as it is cooled and to maximise its area to enhance its shear strength. Additionally, it is desirable that any machining or metalworking needed to form the configuration should be simple and that the joint should be held firmly in place without the use of complicated jigs. Satisfying these desires has led to a preference for lap, sleeve and pocket joints, such as those shown schematically in Figure 10.3, and hence to the creation of the narrow, capillary, gaps between the components that increase the driving force for flow of the liquid braze from its original location outside the joint.



**Figure 10.3.** Some preferred joint configurations for brazed metal components.

Despite the variations in wetting behaviour displayed by differing braze alloys, the range of gap widths with which acceptable joints can be formed readily does not vary greatly, as shown by the recommendations in Table 10.3. It should be noted that the gaps recommended when joining with Ni brazes includes zero, meaning that the braze alloy flows along the microscopic channels left between the contacting asperities on the surfaces of the components. When joining with Cu brazes, even fewer and smaller residual microscopic channels required so BS1723 (1986a) is able to recommend even negative gaps produced by shrink fitting prior to brazing. In general, however, there is a consensus that a gap of about 0.1 mm is acceptable for joining, except possibly when an Al braze is used. In principle, it is possible to calculate the optimum vertical or horizontal gap width by quantifying the effect of variations in the joint gap on the equilibrium penetration and the rate of flow of the liquid braze by assuming the system to behave in an ideal manner. In practice this exercise is thwarted by the lack of relevant data for technically important systems and the presence of oxide films on the surfaces of the components and sometimes also on the surface of the braze. Nevertheless, insight into probable effects of gap widths on braze flow can be gained by reference to the behaviour of simpler braze/component material combinations.

**Table 10.3.** Recommended braze gaps.

Braze	Typical widths (micron)	
	(BS1723 1986a)	(Schwartz 1995)
Ag alloys	25 - 150	0 - 130
Al alloys	50 - 250	50 - 250
Au alloys	25 - 125	0 - 130
Cu alloys	-50 - 150	0 - 130
Ni alloys	0 - 125	0 - 130

Figure 10.2 showed the predicted capillary penetration by some liquid metals which were assumed to wet perfectly. The predictions for all the systems suggest that both horizontal and vertical 0.1 mm wide braze gaps will be filled to a depth of 10 mm, a typical braze depth, in much less than 1 second.

Significant differences due to the varying importance of gravity with orientation and the nature of the liquid metal become apparent only for untypical gaps longer than about 100 mm, and therefore the consensus about recommended joint gap widths is not surprising. The sometime exception to this rule, Al brazing of Al

components, is probably due to the fact that the braze and component solvents are identical. The melting temperature of the braze is depressed by the addition of Si but this readily diffuses into solid Al and, therefore, premature isothermal resolidification of the Al-Si braze will occur if the joint is thin.

Rapid liquid flow into the capillary gaps should occur for simple liquid-solid systems. However, the predicted times of less than 1 second to fill a 10 mm deep gap shown in Figure 10.2 for some pure, perfectly wetting and non-reactive liquid metals are much less than the brazing temperature hold times of 100-1000 seconds that are typical of much brazing practice. These apparently excessively long hold times are necessary because the actual flow rates of liquid brazes are far less than those predicted by models of flow impeded only by viscous and gravitational forces. Thus hot stage microscope observations have measured flow rates of about  $1 \mu\text{m.s}^{-1}$  for the formation of Al-Si-Mg brazed Al component joints and the spread of Ni-11P braze over Fe-Cr surfaces, (Ambrose et al. 1988). The slowness of these rates was attributed to difficulties in removing oxide films from the component surfaces by undermining the substrate metal, and to the confinement of flow to the narrow undermined region, thereby increasing the viscous drag experienced by the liquid braze, (Ambrose et al. 1988, 1993).

### 10.3. JOINING CERAMIC COMPONENTS : CERAMIC-CERAMIC AND CERAMIC-METAL JOINTS

The same capillary phenomena affect brazing practice for joining both ceramic and metal components, but the relative importance of the phenomena differs, and this makes it convenient to discuss their effects in a different sequence. Further, most joining of ceramics is to metals and the different thermal expansion and mechanical characteristics of these two families of materials, as exemplified in Table 10.4, have a profound effect on joint design that is not related to capillarity.

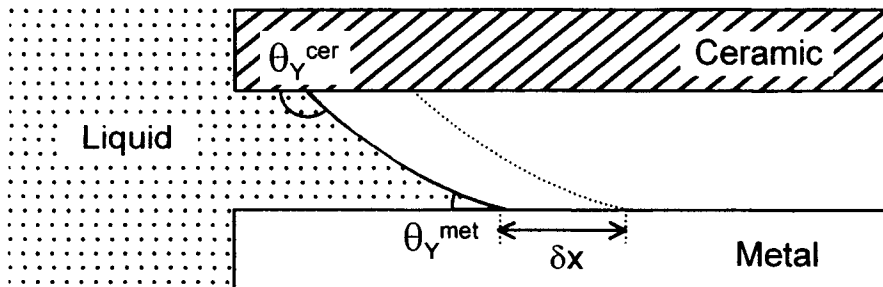
*The capillary attraction* for non-reactive metals exerted by ceramics is usually negative ( $\theta > 90^\circ$ ) as discussed in Chapters 6 to 8. For ceramic-ceramic joining, the braze must wet the ceramic surfaces but creating a ceramic-metal joint does not require the ceramic to be wetted but merely that the sum of the contact angles assumed by the ceramic and metal components should be less than  $180^\circ$ . This less demanding requirement arises because it is sufficient for the total energy for a liquid to advance while in contact with both component surfaces to be negative. Thus the energy change caused by the small advance  $\delta x$  shown in Figure 10.4 is  $\delta F$  where

$$\delta F = \delta x(\sigma_{\text{SL}} - \sigma_{\text{SV}})_{\text{metal}} + \delta x(\sigma_{\text{SL}} - \sigma_{\text{SV}})_{\text{ceramic}} \quad (10.4)$$

**Table 10.4.** Physical properties of some ceramics and metals.

Material	Melting temperature (°C)	Thermal conductivity (W.m <sup>-1</sup> .K <sup>-1</sup> )	Thermal expansion (10 <sup>6</sup> K <sup>-1</sup> )	Elastic modulus (GPa)
Al <sub>2</sub> O <sub>3</sub>	2030	35	7.9	387
SiO <sub>2</sub>	1720	1.5	3.0	354
ZrO <sub>2</sub>	2960	19	7.5	140
Si <sub>3</sub> N <sub>4</sub>	1900 (*)	17	2.5	176
TiN	2900	17	8.1	
SiC	2700 (*)	50	4.3	211
TiC	3140	36	7.2	422
WC	2777	84	5.2	704
graphite	3650	25	(**)	
Ag	960	425	19.1	83
Al	660	238	23.5	71
Cu	1083	379	16.6	130
Fe	1535	78	12.1	211
Mo	2615	137	5.1	325
W	3387	174	4.5	411

(\*) Does not melt but decomposes or vaporises

(\*\*) 1 to 5×10<sup>-6</sup> K<sup>-1</sup> for varyingly oriented polycrystalline material**Figure 10.4.** Infiltration of a liquid into a gap between metal and ceramic components.

Introducing the equilibrium contact angle of the liquid on the solid metal,  $\theta_Y^{\text{met}}$ , and on the ceramic,  $\theta_Y^{\text{cer}}$ , and taking into account the equilibrium condition  $d(\delta F)/d(\delta x) = 0$  leads to the conclusion that  $\theta_Y^{\text{met}} + \theta_Y^{\text{cer}} = 180^\circ$ . Thus the condition for the liquid to advance is  $\theta_Y^{\text{cer}} < 180^\circ - \theta_Y^{\text{met}}$ . For clean metal surfaces,



$\theta_Y^{\text{met}}$  is usually lower than  $50^\circ$ , (Chapter 5), and the consequential penetration requirement that  $\theta_Y^{\text{cer}} < 130^\circ$  is satisfied by many ceramics. However, while the condition  $\theta_Y^{\text{cer}} < 90^\circ$  is not necessary for creation of a ceramic-metal joint, it is desirable. Without wetting of the ceramic, formation of a braze/ceramic interface at the atomic scale is not assured and voids such as those shown in Figure 10.1.d may be present.

The development of brazing techniques for ceramics requires specialised techniques and materials. The most commonly brazed ceramic is  $\text{Al}_2\text{O}_3$  and this is usually achieved by “metallizing” the surface before using a braze suitable for metal components. This metallization can be the direct application of a metal to the ceramic by electroplating, by sputtering, by chemical or plasma activated vapour deposition or by plasma spraying techniques, (Bondley 1947, LaForge 1956, Kohl 1967, Twentyman 1975, Hey 1990), but the most widely adopted technique is to coat the  $\text{Al}_2\text{O}_3$  surface with a glass-metal mixture and then heat at a high temperature to achieve bonding and the formation of a metallic skin bonded to the ceramic by a glass interlayer. This is generally then overplated with Ni and is then ready for brazing. Recently, however, “active-metal” brazes have been identified that can be used without the need for prior metallization. Metallization practice will be discussed first and then attention will be concentrated on active metal brazes.

### ***10.3.1 Metallization using glass-metal mixtures***

The glass-metal mixture approach was first perfected during World War II, (van Houten 1959), as the “moly-manganese” process which applied a coating of Mo particles to the surfaces of debase  $\text{Al}_2\text{O}_3$  ceramics containing substantial amounts of glassy binder phases. On heating, some glass flowed from the ceramic grain boundaries to wet and bond to the surfaces of the Mo powder (glasses wet metallic surfaces, see Chapter 9). It was found that adhesion achieved by heating in  $\text{H}_2$  or  $\text{N}_2\text{-H}_2$  environments at a high temperature was improved substantially by mixing the Mo with Mn or  $\text{MnO}_2$  and later studies, (Twentyman 1975), have shown that this success depends on both chemical and capillary processes.

Heating at the normal metallizing temperature of  $1400^\circ\text{C}$  in  $\text{H}_2$  or  $\text{N}_2\text{-H}_2$  environments dissociates the oxide films on Mo surfaces, but the resultant formation of  $\text{H}_2\text{O}$  causes the environment to become damp. Similarly,  $\text{MnO}_2$  is reduced, or Mn is oxidised, to MnO by environments with a  $\text{H}_2\text{O}/\text{H}_2$  ratio of between  $4.3 \times 10^{-4}$  and 2.67. (While this ratio is of chemical significance, it is monitored in practice by measurement of a physical parameter, the Dew Point or

temperature at which the  $\text{H}_2\text{O}$  concentration is sufficient to cause condensation of water, (Bredz and Tennenhouse 1970)).

Heating to the metallizing temperature also causes the glassy binder phases to become relatively fluid and to wet Mo surfaces in damp, but not dry, environments. Thus the glassy phase flows from the ceramic grain boundaries into the fine capillaries between the spherical Mo particles to produce a composite coating with a Mo rich surface, which can be subsequently electroplated with Ni. The Mo particles are typically  $5\text{ }\mu\text{m}$  or less in diameter, (Johnson and Rowcliffe 1985), so the capillaries have equivalent radii of less than  $1\text{ }\mu\text{m}$ : smaller particles and capillaries would exert an even greater attraction but a lower particle size limit of about  $1\text{ }\mu\text{m}$  must not be passed if the Mo is not to sinter prematurely into large impenetrable agglomerates. Finally, the MnO is also mobile at the metallizing temperature and segregates to the glass-ceramic interface and then reacts with the  $\text{Al}_2\text{O}_3$  to form a spinel bridging compound that improves adhesion of the coating, (Twentyman 1975).

Recent years have seen a growing use of purer oxide ceramics that contain little glassy binder for which the original moly-manganese process is not suitable. However, some success has been achieved by modifying the coating composition to include oxide frits, based on binder phase compositions such as  $\text{Al}_2\text{O}_3\text{-SiO}_2$ ,  $\text{CaO-SiO}_2$  and  $\text{CaO-Al}_2\text{O}_3$ , (Reed et al. 1966), that can wet the Mo particles and penetrate the ceramic grain boundaries to provide anchorage. Some mixtures have been developed as commercial products, but many fabricators use in-house formulations found to suit their equipment, ceramics and performance requirements because considerable difficulties can be encountered in optimising process parameters to ensure low reject rates. Finally, similar processes involving both chemical and capillary interactions to promote metallization of non-oxide ceramics, and particularly  $\text{Si}_3\text{N}_4$ , have been investigated in laboratories using oxide frit additions based on binder phase materials such as  $\text{Al}_2\text{O}_3$ ,  $\text{MgO}$  and  $\text{Y}_2\text{O}_3$ , (Johnson and Rowcliffe 1985).

### **10.3.2. Active metal brazing**

This special class of brazes reacts chemically with the surfaces of ceramic components to produce wettable products with metallic characteristics, such as  $\text{TiO}$ ,  $\text{TiC}_{1-x}$  or  $\text{TiN}_{1-x}$  as described in Sections 6.3 and 7.2. Thus the wetting is due to an *in situ* "metallization". By definition, the brazes must contain chemically reactive elements such as Ti that are often added to eutectic brazes similar to those developed for joining metal components. Many sessile drop experiments have shown that active metal brazes can wet a wide range of ceramics when a suitable inert environment is used. Particularly high standards of environmental inertness

have to be achieved if flow of the liquids is not to be restrained by surface skins on the braze which by definition contains very reactive components. No fluxes have been developed for the active metal brazes but good technical vacua of  $10^{-4}$  mbar, high purity Ar or He and Ar-H<sub>2</sub> mixtures have been used successfully to produce active metal braze melts that are skin-free. However, unlike the eutectic brazes developed for joining metals, the active metal variants cannot be used in N<sub>2</sub>-H<sub>2</sub> environments due to the formation of skins of TiN which both restricts the fluidity of the liquid and depletes the amount of the “active” solute available for reaction with the ceramic.

The wetting achieved using inert environments is due to the formation of a wettable reaction product, Section 2.2.2.1, and quite large changes in sessile drop contact angle values can be produced by a small advance of the liquid front. For example, a decrease from 60 to 30° by a typical 0.01 ml sessile drop requires a contact area radius increase of only 0.7 mm. However, the relationship (10.3) between capillary rise and wettability for an inert system, which predicts a further 120 mm penetration of a 0.1 mm wide capillary by liquid Cu when  $\theta_Y$  decreases from 60 to 30°, is irrelevant in many cases. Although the contact angle assumed by the penetrating liquid front may be 30°, the advance of the liquid by lateral growth of a reaction product layer will exhaust the available supply of the active solute element long before the predicted 120 mm penetration is achieved (see also Section 2.2.2.1 and Figure 2.27).

*Braze fluidity* is as essential for the joining of ceramics as it is for metals. The brazes used to join metallized ceramics are preferably the pure metals and eutectic or near eutectic compositions discussed when considering the joining of metal components and need no further discussion. In practice, active metal brazes are also based on pure metals or eutectics, even though they do not have singular melting temperatures. The active metal brazes to which fabricators have paid most attention so far are alloys based on the Ag-Cu eutectic and precious metals. Exploitation of these is well established, as indicated by the range of commercially available compositions shown in Table 10.5. Those that have found most use so far are the Ag-Cu-Ti and Ag-Cu-In-Ti compositions, which have been applied in the mass production of components for the automobile and electrical industries, (Mizuhara and Huebel 1986, Bucklow et al. 1992, Ito and Taniguchi 1993).

These brazes have experienced major metallurgical and fabrication developments in the last few years. Thus the concentration of Ti has been reduced from about 10% or 5% to 2 or 1% by slightly varying the Ag/Cu ratio or by introducing elements such as Sn and In which seem to increase the thermodynamic activity of Ti. The purpose of the decreases of Ti concentration is mainly to improve the ductility of the brazed joints (Ti intermetallics are usually brittle),

**Table 10.5.** Some commercially available active metal brazes.

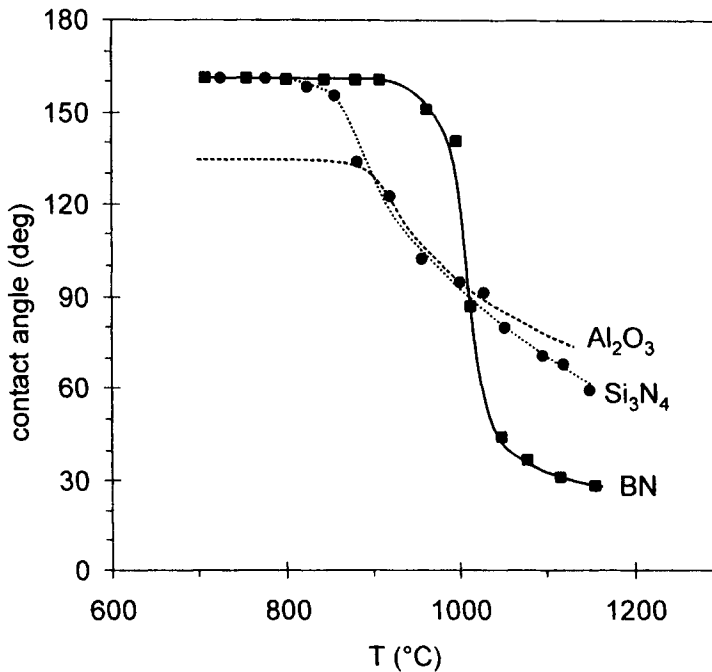
Composition (wt%)	Melting range (°C)
Au-3Ni-0.6Ti	1003 - 1030
Cu-3Si-2Al-2.25Ti	958 - 1024
Au-15.5Ni-1.75V-0.75Mo	940 - 960
Ag-5Cu-1Al-1.25Ti	860 - 912
Ag-26.7Cu-4.5Ti	830 - 850
Ag-35.25Cu-1.75Ti	780 - 815
Ag-34.25Cu-1Sn-1.75Ti	775 - 806
Ag-27Cu-9.5In-1.25Ti	625 - 755
Ag-27.5Cu-12.5In-1.25Ti	605 - 715

(Mizuhara and Huebel 1986), but in fact the early high concentrations of Ti were not necessary for good wetting to be achieved because phase diagram studies show that the Ag-Cu-Ti system contains a large liquid immiscibility region and that the maximum solubility of Ti in the liquid eutectic is about 2%, (Chang et al. 1977). Similarly, the initial fabrication of Ag-28Cu-Ti brazes as multi-layer Ag/Ti/Cu, Cu/Ag/Ti/Ag/Cu or Ag-Cu/Ti/Ag-Cu structures produced by rolling or electroplating has been replaced first by alloy sheets rolled from cast ingots and then by thin amorphous alloy sheets formed by rapid solidification. This has resulted in better product consistency and immediate availability of Ti for reaction with the ceramic when the braze melts, since this element does not have to be dissolved by the adjacent low melting Ag or Ag-Cu but is already present as a solute or fine equilibrated phase.

Not all active metal brazes are based on Ag-Cu or precious metal solvents. Thus, Al reacts with and can wet a wide range of ceramics in vacua at high super-heat temperatures, Figure 10.5, when the surface skin of  $\text{Al}_2\text{O}_3$  degenerates to volatile  $\text{Al}_2\text{O}$  and permits direct contact of the liquid metal with the ceramic. Similarly, Al-Si alloys can be caused to wet at modest super-heat temperatures by mechanical disruption of the oxide skins when a small pressure is applied while using components with rough surfaces, as can Al-Si-Mg alloys whose oxide skin is disrupted by volatilisation of Mg. These alloys have been used to fabricate electrical and electronic prototypes, (Guy et al. 1988, Yamada et al. 1991), but high volume applications have yet to be established.

Ni brazes are attractive when components must endure high service temperatures and evaluation of the potential of Ni eutectic brazes containing additions of Cr, such as BNi-5 and BNi-7 (Ni-19Cr-10Si and Ni-14Cr-10P), as the active metal for joining  $\text{Si}_3\text{N}_4$  and SiC ceramics has been vigorous, (McDermid et al. 1989,

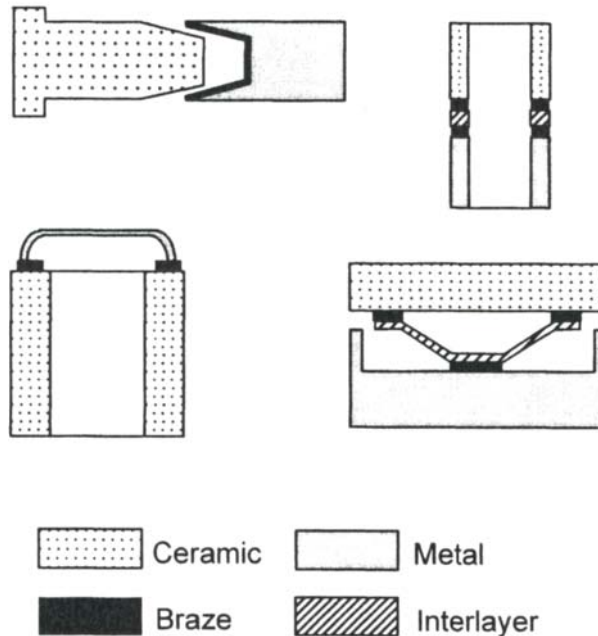
Cecccone et al. 1995). However, this effort has not yet resulted in application of the alloys for the mass production of ceramic-metal components because of excessive formation of embrittling silicides by BNi-5 and unacceptably poor wetting by BNi-7. Recently, high melting-point brazes have been developed to join SiC based materials, with use temperatures up to 1000°C, that have good wetting, negligible reactivity with SiC and form strong braze/SiC interfaces (Moret and Eustathopoulos 1993, Moret et al. 1998).



**Figure 10.5.** The wetting behaviour of sessile drops of Al on reactive ceramic substrates (Si<sub>3</sub>N<sub>4</sub>, BN) and Al<sub>2</sub>O<sub>3</sub> during temperature rise at about 5 K/min in a high vacuum, (Nicholas et al. 1990) [2].

*Liquid flow* into ceramic-metal joints will be affected by their design. The joint gaps used when the ceramic component has been metallized will be similar to the 0.1 mm recommended for the brazing of most metal components, but usually the preferred gaps when using active metal brazes will be quite wide so that a reasonable reservoir of reactant is available. However, the principal consideration determining joint designs, regardless of whether the process involved is metallization followed by bonding with normal brazes or the active metal brazing

of unmetallized ceramics, is the difference in physical properties of ceramics and metals. In particular, attention has to be paid to the smaller thermal expansivities of ceramics and to their brittleness. Thus it is desirable to ensure that the ceramic members are subjected to small compressive stresses as the assembly cools after being joined. Finite element modelling, experiment and experience have led to the development of a number of successful designs that possess the desired stressing characteristics and some of these are shown schematically in Figure 10.6.



**Figure 10.6.** Designs for ceramic-metal joints.

Each of the applications shown in Figure 10.6 is different, but they all accommodate the mismatched thermal expansivities of ceramics and metals. The top left hand sketch shows a tapered joint between  $\text{Si}_3\text{N}_4$  and a steel shaft in which the circumferential compressive stress on the ceramic is attenuated by the progressive thinning of the steel wall, (Mizuhara and Huebel 1986). Progressing clockwise, the next sketch shows a tubular  $\text{Si}_3\text{N}_4$ /steel device that uses a thick Mo interlayer to decrease thermal expansion mismatch stresses, (Schwartz 1995). In the bottom right hand corner is shown a ceramic crowned engine tappet that uses a flexible metal interlayer to accommodate mismatched thermal expansions,

(Bucklow et al. 1992), and the remaining sketch shows a ceramic tube capped by a flexible metal member, (Mizuhara and Huebel 1986).

Rapid fluid flow cannot be achieved with active metal brazes because of the need to form solid wettable reaction product layers for their liquid fronts to advance. Equations (10.1) to (10.2) relating liquid flow rates to the opposed effects of surface energy imbalances and of viscous drag are not relevant. Actual penetration rates are so slow, usually of the order of  $1 \mu\text{m.s}^{-1}$ , that the usual practice is to place the active metal braze alloy within the joints rather than expecting it to fill them, and, as explained already, gap width is not the dominant consideration when designing ceramic-metal joints.

The thermal cycles used to braze ceramic-metal and ceramic-ceramic assemblies are usually prolonged with slow heating and cooling rates being used to minimise thermal gradients, and hence stresses, within the ceramics. Common practice is to heat at about  $10^\circ\text{C.min}^{-1}$  to just below the solidus temperature and then to hold for several minutes before continuing to heat at perhaps  $3^\circ\text{C.min}^{-1}$  to the brazing temperature. The dwell times at the brazing temperature are typically 10 to 30 minutes, fortuitously enabling a quasi-equilibrium joint microstructure to be achieved through braze/component chemical reactions and slow spreading of the liquid braze.

#### 10.4. JOINING BY RELATED TECHNIQUES

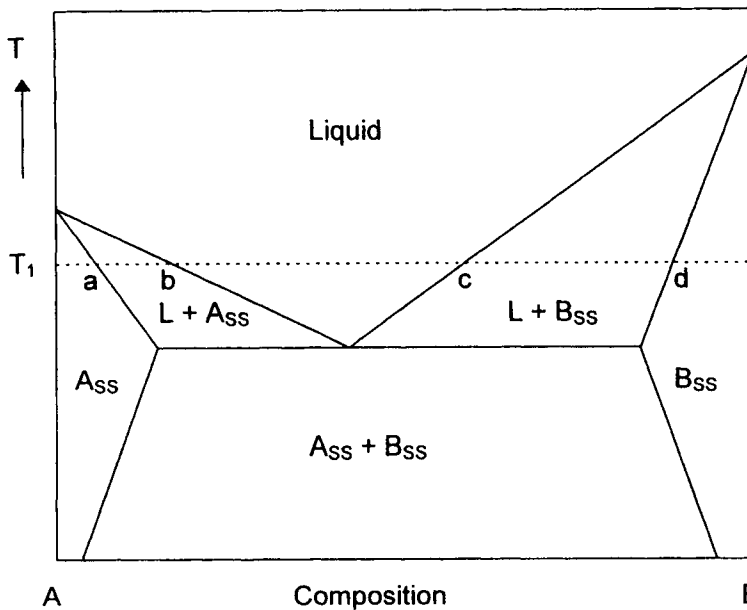
Brazing is such a long established technique that is not surprising that many variations have been developed. Some of these such as active metal brazing have been referred to already, but this Section starts with comments on other techniques in which the liquid bonding phase is formed *in situ* by interdiffusion or chemical interaction with the environment. Finally, a small sub-section is devoted to “glazing”, i.e., joining metals and ceramics by glasses.

##### 10.4.1 Transient liquid phase bonding

This technique employs a thin and chemically different metal or metal alloy interlayer placed between the surfaces of metallic components so that contact results in interdiffusion and the transient production of a composition that is liquid and wets the solids, (Zhou et al. 1995).

The changes in the phase structure of a hypothetical eutectic system caused by interdiffusion of the interlayer and component materials are illustrated schematically in Figure 10.7 for contact between an interlayer of pure metal A and a component of pure metal B brought into contact at a temperature  $T_1$  that is lower than the melting point of either A or B. Ingress of B into A and of A into B

initially causes the  $A_{ss}$  and  $B_{ss}$  solid solutions to be formed, but ultimately the solubility limits identified as a and d in the figure are exceeded and a liquid phase is formed with a composition between b and c that wets and spreads over the whole solid surfaces. Formation of this liquid, therefore, increases the rate of interdiffusion and ultimately all the interlayer is consumed. However, interdiffusion does not cease and the liquid becomes richer in B and commences to resolidify isothermally when its composition becomes d.



**Figure 10.7.** Phase diagram illustrating the changes caused by interdiffusion of A and B at a temperature of  $T_1$ .

Modelling the progress of a transient liquid phase bonding between components and an interlayer, therefore, is largely a matter of considering rates of interdiffusion and solubility limits. Wetting behaviour can be assumed to be excellent if the process progresses at all because the liquid can be formed only after metal-metal contact has been achieved. Thus the onset of transient liquid phase bonding may be delayed by the need to disrupt and disperse oxide films on substrate surfaces but once metal-metal contact has been achieved in some locations the oxide film residues can be undermined by the volume changes



associated with interdiffusion and penetration of oxide/substrate interfaces by the liquid phase. While oxide removal can be a relatively slow process, the time taken is only a small fraction of that needed for the whole bonding process and in particular of that needed to achieve isothermal resolidification.

Such excellent or at least adequate capillary behaviour is also typical of the process variant known as eutectic bonding in which the transient creation of a liquid phase is caused by the interdiffusion of two chemically different metal alloy component materials. In the laboratory variant process known as partial transient liquid phase bonding, (Shalz et al. 1992), a coated interlayer is used for ceramic-ceramic or ceramic-metal joints. In this process the interlayer is a ductile metal or alloy whose surface is coated with a thin layer of a lower melting temperature metal or alloy, for example Ni-20Cr coated with 2 microns of Au. The bonding temperature is chosen so that only the coating melts and the ductility of the interlayer helps to accommodate mismatches in the coefficient of thermal expansion of the component materials.

A particular advantage of the transient liquid phase bonding technique is that the joints are produced at relatively low temperatures but have elevated service temperature capabilities comparable to those of diffusion bonded structures, (Locatelli et al. 1995).

#### ***10.4.2 Direct bonding***

This technique exploits the ability of some gaseous environments to react with metals to form low melting temperature eutectic compositions on the surfaces of metal components. Systems such as Ag-P, Ag-S, Al-Si, Co-O, Cr-O, Cr-S, Cu-O, Cu-P, Cu-S, Fe-O, Mo-Si, Ni-O and Ni-P have been identified as being useful for the formation of metal-metal joints, (Burgess et al. 1973, 1975). The most vigorous commercial exploitation of this effect, however, is in the direct bonding of Cu to  $\text{Al}_2\text{O}_3$  which can be achieved by holding at a temperature such as  $1072^\circ\text{C}$  in an environment containing at least  $1.5 \times 10^{-3}$  mbar of  $\text{O}_2$  so that a surface film forms of the Cu-Cu<sub>2</sub>O eutectic which contains 0.43 wt.% O, melts at  $1065^\circ\text{C}$ , wets the ceramic and reacts with it to form mixed Cu and Al oxides (Courbière et al. 1986).

#### ***10.4.3 Joining by glasses: glazing***

Inorganic glasses based on  $\text{SiO}_2$  can be used to produce joints between metal or ceramic components by glazing, the inorganic analogue of brazing.

Some of the glassy silicate materials cited in Table 9.1 have been used as joining materials in laboratory studies but most are unsuitable for realistic applications. Thus the Na and K silicates are soluble in water and hence unsuitable

for many service conditions. The glasses that are applied in practice usually have complex compositions, as do braze alloys, and are based on  $\text{SiO}_2$ . The openness of glassy  $\text{SiO}_2$  makes it relatively easy to introduce other oxides into the structure and hence modify its properties. Thus additions of  $\text{B}_2\text{O}_3$  enter the network structure of  $\text{SiO}_2$  glasses to decrease their viscosity while  $\text{Na}_2\text{O}$  and several other alkali oxides modify the  $\text{SiO}_2$  network to decrease the softening temperature. These and other composition-induced structural effects have permitted development of a range of commercial glasses, including some developed especially for the joining of metal components, and thermal data for a number of these are summarised in Table 10.6. These compositional changes affect not only the behaviour of the glass when it is being worked but also its properties after it has cooled, such as its coefficient of thermal expansion, and detailed analyses of expansion data for a wide range of glasses has permitted development of additive relations. These show that the alkali oxides  $\text{K}_2\text{O}$  and  $\text{Na}_2\text{O}$  cause very large increases in expansivity and that  $\text{BaO}$ ,  $\text{CaO}$ ,  $\text{PbO}$  and  $\text{Al}_2\text{O}_3$  cause significant increases but that  $\text{B}_2\text{O}_3$ , and  $\text{MgO}$  cause decreases.

**Table 10.6.** Thermal properties of  $\text{SiO}_2$  and some commercial glasses (Holloway 1973).  $T_G$ : temperature of glass transition below which the glass behaves as a rigid crystalline solid,  $T_S$ : softening temperature above which the glass is soft enough to be worked or moulded, CTE: coefficient of thermal expansion.

Material	Additives (mol %) (*)							$T_G$ (K)	$T_S$ (K)	CTE ( $\times 10^6 \text{ K}^{-1}$ )
	$\text{B}_2\text{O}_3$	$\text{Na}_2\text{O}$	$\text{Al}_2\text{O}_3$	$\text{K}_2\text{O}$	$\text{CaO}$	$\text{MgO}$	$\text{PbO}$			
$\text{SiO}_2$								1373	1873	0.5
alumina-silicate	7		15		3	14		1000	1210	3.3
pyrex	11	4	1					840	1100	3.2
soda-lime-silica		15	1		7			780	970	9.2
lead glass		9		5			7	700	890	9.1
kovar sealant	14	4	2	1				830	1043	3.75
W sealant	20	3	2	3				765	990	4.7

(\*) compositions have been rounded to the nearest %

As shown in Chapter 9, glasses can wet and wet well a wide range of ceramic and metallic components and that, therefore, predictions of the extent of capillary flow (equations (10.1) and (10.2)) can make use of the approximation that  $\cos\theta$  is equal to 1. However, these penetrations are not achieved instantly and the main rate-determining material characteristic is the  $\sigma_{LV}/\eta$  ratio, which is much smaller

for glassy materials than for metals, typically less than  $0.1 \text{ m.s}^{-1}$  as compared to the several hundred  $\text{m.s}^{-1}$  for metals. Another factor that must be considered when joining with glasses is their brittleness when solid and stressed in tension. Thus the designs of glazed joints usually minimise gap widths and ensure that the joint is not stressed or preferably is subjected to a modest compression.

## **10.5. EFFECTS ON MECHANICAL PROPERTIES**

The prime requirement for successful brazing is that capillarity causes the molten braze to flow into gaps between the components to be joined. Unless the capillary attraction is sufficient to achieve this, the joint cannot be formed. Having formed a joint, the next requirement of the ultimate user is usually that it should be robust (strong or tough and preferably both strong and tough). Whether this requirement can be met also depends substantially, but not exclusively, on capillary phenomena.

If the system is wetting, joints can be formed but a quantitative connection between capillary attraction and the mechanical properties of the joints is not easy to achieve. Capillary attraction can be clearly defined and quantified in terms of a work of adhesion of so many  $\text{J.m}^{-2}$  but the mechanical behaviour of a joint is manifest in strength and toughness characteristics that can be measured and quantified in many different ways. A wide range of mechanical test procedures have been developed for brazed joints. Standardised tensile, fatigue, impact, bend and hardness tests procedures developed for monolithic materials have been adapted while others such as peel, push-off and a range of shear tests have been specially developed, often using configurations markedly influenced by very specific application considerations. Descriptions of some of the more commonly used tests will be found in references such as (ASTM F19-64 1964, Christensen and Sheward 1982, BS1723 1986b, Moorhead and Becher 1987). However, there is no unique relationship between the values generated by the various tests and hence no single actual or even normalised data set with which values for capillary attraction can be compared. Thus both high tensile strength and toughness values are desirable attributes for a mechanically satisfactory joint but in practice a particular joint may have a high tensile strength but not be tough or be tough but weak, and hence be suitable for some applications but not for others.

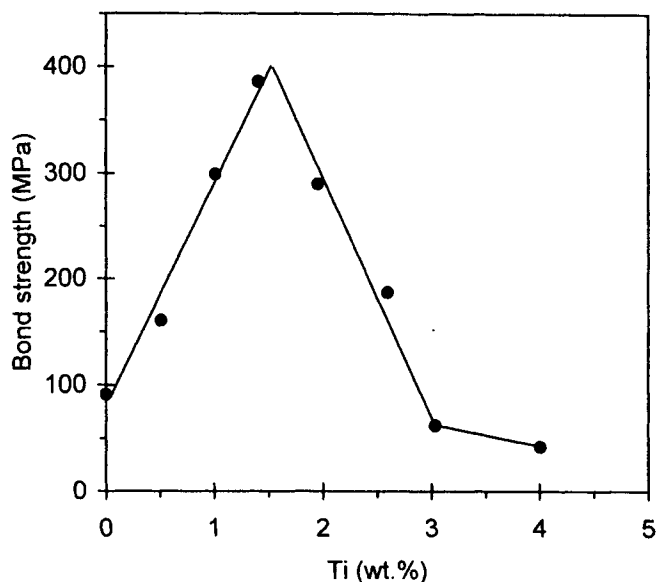
### ***10.5.1 Influence of thermodynamics***

Despite the lack of a unique parameter that describes the mechanical characteristics of joints, it is possible to divine some of the influences of variations in capillarity and other joint formation phenomena by examining the limited mechanical data sets for particular types of joints or families of joint materials. Thus it is clear that

the greater filling of vertical joints associated with the use of more wetting systems, as described by equation (10.3) results in enhanced failure *loads* without any change in the strength per unit area of joint being required.

In principle, an equality between the thermodynamic work of adhesion of liquid-solid systems and the work needed to separate an interface might be expected for simple systems and this has been observed for failure of adhesive-polymer interfaces bonded by van der Waals forces, (Kinloch 1987). Similarly, empirical correlations of interfacial strengths and work of adhesion values of solidified interfaces have been reported for some nominally non-reactive pure metal/ceramic systems. However, mechanical separation of such interfaces is a complex process that usually involves plastic deformation of the lattices, and hence their works of fracture are often at least ten and sometimes one hundred times larger than the works of adhesion, (Howe 1993). Nevertheless, for non-reactive metal/ceramic couples, it is now widely recognised that the energy dissipated by plasticity (and as a result the fracture energy of the interface) scales with the thermodynamic work of adhesion (Reimanis et al. 1991, Howe 1993, Tomsia et al. 1995).

In practice, many brazes for metals and virtually all those for ceramics are chemically reactive. Indeed, brazes for ceramic components have to be reactive to ensure that the solid surface is converted into a wettable layer and this change in the structure of the ceramic surface will affect the mechanical properties of the solidified braze/ceramic interface. Studies with transparent ceramics such as diamond or sapphire have shown that the reaction product layer nucleates as islands that increase in size and number as the reaction proceeds and that this increase is associated with an overall strengthening of the interface, (Scott et al. 1975). Thus increasing the concentration of the reactive solute initially increases the strength of the interface as more and more of it is converted, but no further increase is possible once there is complete coverage by the reaction product layer. This covering layer can be quite thin, 0.1 to 0.2 micron for diamonds contacted by Cu alloyed with Cr or Ti or V, and in practice the continuation of the reaction usually results in a weakening of the joint. Three types of joint failure can be associated with such weakness : adhesive failure with separation at weakly bonded insufficiently reacted interfaces, cohesive failure within the (ceramic) component when interfacial bonding is strong and material characteristics such as coefficients of thermal expansion are mismatched, failure within reaction product layers that have grown thick due to volume mismatch stresses or delamination of multiphase structures, (Scott et al. 1975, Wan et al. 1996). In contrast, strong joints are usually associated with mixed adhesive/cohesive failure. Thus increasing the extent of the reaction by raising the concentration of the reactive solute in a metal, causes the strength values to peak, as illustrated in Figure 10.8.

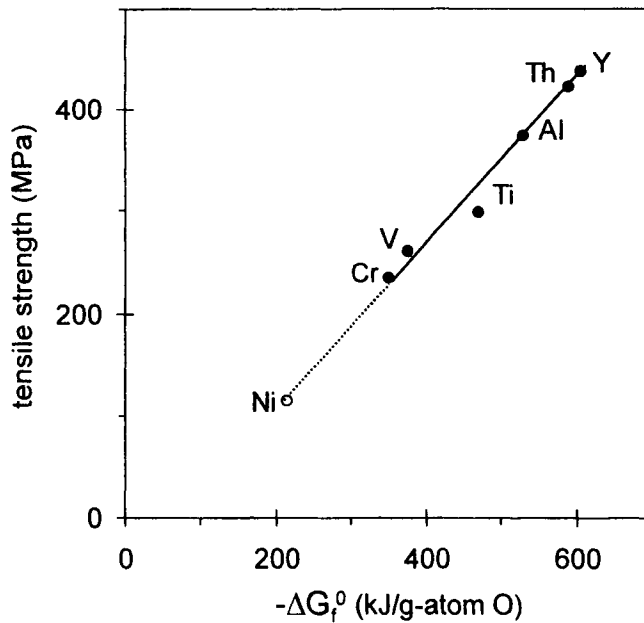


**Figure 10.8.** The room-temperature tensile strengths of solidified sessile drop interfaces formed between  $\text{Al}_2\text{O}_3$  and Cu-Ti alloys plotted as a function of the Ti concentration, (Nicholas 1986).

Peaking of strength values has been observed for many reactive alloy-ceramic systems and attempts have been made to correlate the strength maxima with other system characteristics. Thus comparisons between peak strength values and the chemical affinity of the solute for O have revealed empirical correlations, such as that shown in Figure 10.9 for  $\text{Al}_2\text{O}_3$  bonded by Ni alloys and by pure Ni. It is interesting to note that all solutes of Figure 10.9 are known (or expected) to improve wetting and thermodynamic adhesion on alumina. However, the detailed mechanism responsible for such a correlation has yet to be established and it has to take into account the fact that the extent of reaction and the morphology of the reaction product layers can vary significantly from system to system. For instance, in low  $\text{P}_{\text{O}_2}$  environments, no reaction product forms between  $\text{Al}_2\text{O}_3$  and pure Ni and Ni-Al and Ni-Cr alloys (only a slight dissolution of  $\text{Al}_2\text{O}_3$  occurs in these alloys) while Ti in Ni reacts with  $\text{Al}_2\text{O}_3$  to form different Ti oxides depending on Ti concentration.

The thermodynamic driving force for interface creation for clean metal-metal systems, defined in terms of the work of adhesion, is invariably large as shown in Chapter 5 and hence generates the expectation that the mechanical properties of metal-metal interfaces will be excellent. This is usually observed in practice when wetting produces complete and intimate contact of the braze and component

materials, but there is not always complete interfacial contact and the presence of flaws can have a profound effect on mechanical properties of both metal-metal and metal-ceramic interfaces.



**Figure 10.9.** Peak room-temperature tensile strength values of the interfaces formed by  $\text{Al}_2\text{O}_3$  with sessile drops of Ni or Ni-metal M alloys plotted as a function of the standard Gibbs energy of formation of M oxide, (Crispin and Nicholas 1976). Full circles: Ni alloys; hollow circle: Ni; from (Nicholas 1968).

### 10.5.2 Influence of interfacial flaws

Interfaces can exhibit both physical and chemical flaws, as exemplified by the presence of small voids in the valleys of roughened surfaces brought into contact with a non-wetting liquid ( $\theta > 90^\circ$ ), or retained islands of unwettable oxide on the surfaces of metal components or of surface contaminants on both metal and ceramic components. Such flaws can have detrimental effects on mechanical properties because at the very least their presence decreases the bonded area. Thus the mechanical preparation and cleaning of component surfaces are crucially important steps of the brazing process.

The formation of composite interfaces when very rough surfaces are contacted by liquids that do not wet, (Cassie and Baxter 1944), results in the presence of microvoids at the interface between the component and the solidified liquid (see Section 1.3.1 and Figure 1.27). This effect should seldom be of importance when brazing metal components because of their generally excellent wettability, but it can be of significance when joining ceramic components and similar populations of microvoids can be produced when metal components with rough surfaces are diffusion bonded, by bringing solid components surfaces into contact by applying pressure at a high but sub-solidus temperature, (Baker and Partridge 1991). The influence of such populations of flaws on mechanical properties depends on the type of stressing to which the interface is subjected as well as the characteristics of the joining and component materials. Thus diffusion bonded Ti-4Al-4Mo-2Sn samples can accommodate 10%, or more, of their interfaces being microvoids without any noticeable deterioration of tensile strength, but the fatigue strength is decreased by about 30% and the impact strength by 50-75%, (Baker and Partridge 1991).

The roughened surface topographies of ceramic components can have a particularly detrimental marked effect on mechanical properties both because of their influence on wetting behaviour and the likelihood of microvoid formation in valley bottoms and because the mechanical treatments may nucleate microscopic surface cracks that can propagate and cause premature failure when the interface is stressed. However, these microscopic cracks can be healed by subsequent heat treatment that promotes the flow of glassy binder phases. Thus the effect of re-firing ground surfaces of 99.5% pure  $\text{Al}_2\text{O}_3$  at  $1650^\circ\text{C}$  on its joining to  $6.5 \times 32$  mm strips of Kovar using Ag-28Cu active metal brazes was to increase the peeling loads of the joints from 77 to 112N when 1 wt.% Ti alloy was used and from 32 to 120N when the Ti content was 3 wt.%, (Mizuhara and Mally 1985).

Of similar importance when preparing components prior to brazing is the need to clean their surfaces, (Schwartz 1995), so that microvoids and unbonded regions are not formed where the liquid metal contacts weakly bound and poorly wetted contamination such as grease. This is such standard practice that few data are available that exemplify the problems caused by failing to do so, but some of the effects of using different cleaning procedures can be realised by reference to the mechanical properties of diffusion bonded joints. Thus Table 10.7 summarises the effects of using different cleaning fluids to prepare the surfaces of Fe-0.45C samples prior to bonding by applying a pressure of 20 MPa for 10 minutes at  $1200^\circ\text{C}$ . Unfortunately, while some of the strength variations are quite marked, there is no supporting chemical evidence to explain why, for example,  $\text{CCl}_4$  was a more effective cleaning agent than the other organic solvents.

**Table 10.7.** Effects of cleaning processes on the tensile strengths of diffusion bonded Fe-0.45C steel (Kazakov 1985).

Cleaning procedure	Interfacial strength (MPa)
none	320
degreasing with $C_2H_5OH$	460
degreasing with $CH_2COCH_3$	455
degreasing with $CCl_4$	570
pickling in acid	460

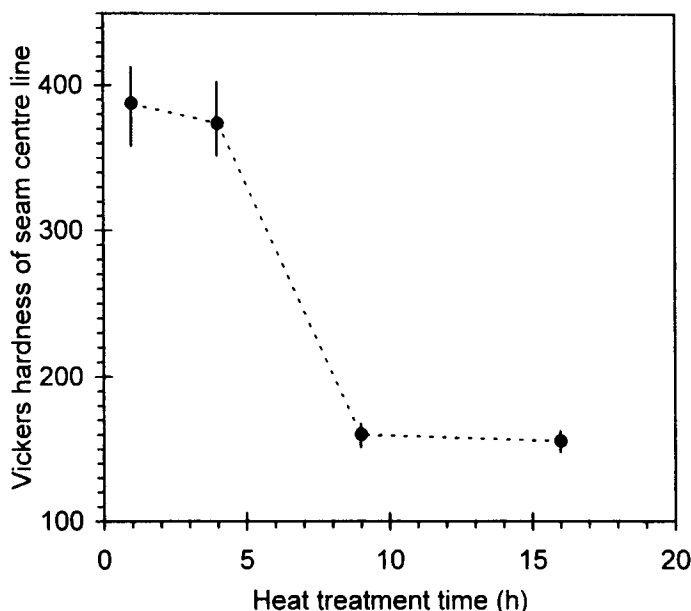
### 10.5.3 Influence of interfacial interdiffusion

By definition, brazes have a different composition from the components they are used to join and hence interdiffusion will occur during and after interface creation. Reference has been made already to the detrimental effects of the growth of thick reaction products at metal-ceramic interfaces and similar effects can occur with metal-metal systems. Thus it is not good practice to use Al brazes for the joining of steel or Cu components or to use Ni brazes containing Si for the joining of refractory metal components because of the rapid formation of fragile layers of intermetallic compounds.

However, some braze alloys are inherently brittle and interdiffusion with certain component materials can confer a degree of ductility. This effect is particularly important and often essential for the successful application of Ni brazes based on the Ni-11Si, Ni-11P or the Ni-3.6B eutectics such as those listed in Table 10.2 which wet steels and Ni super alloys well but solidify to produce continuous seams or dense clustered islands of brittle intermetallic along the braze centre lines unless interdiffusion causes egress of the temperature depressants. These solutes are quite mobile and hence significant egress from the joint can occur during a normal brazing cycle, but in practice it is usually necessary to use very prolonged braze dwells or subsequent heat treatment at a sub-solidus temperature to achieve complete egress. The effect of this chemical change is to convert the braze seam into a single-phase structure of a Ni-base solid solution that has greatly enhanced toughness and impact characteristics but is softer, as illustrated in Figure 10.10.

The detrimental effect of such intermetallic phases in Ni brazed joints is particularly severe when the microstructures are coarse, and this is true also of Si precipitated from Al-Si brazes that are slow cooled from the brazing temperature. Finally it should be noted that while egress of embrittling species can enhance the mechanical characteristics of the braze joints, their ingress can initially degrade





**Figure 10.10.** Microhardness of the BNi-5 brazed joints between AISI 316 samples. The joints were formed in vacuum at 1150°C by holding for 15 minutes and then heat treated at 1050°C. After (Reid et al. 1994) [20].

those of the components. Ultimately, however, the distribution of the embrittling temperature depressants will approach homogeneity as at the conclusion of the transient liquid phase bonding process.

#### ***10.5.4 Influence of braze composition***

The compositions of useful braze alloys have been carefully devised to ensure satisfactory wetting of the proposed component materials, but other adjustments have been made to achieve desirable mechanical characteristics of the joints. This adjustment has been made for virtually all commercial braze families and has been particularly important in the development of active metal brazes for ceramic components.

The prime requirement of an active metal braze is that it should be able to change the chemistry of the ceramic surface to make it wettable, usually by forming hypostoichiometric TiC, TiN or TiO. This necessitates using alloys with high Ti activities, but alloys with high Ti concentrations are seldom suitable as brazes. Thus, Cu alloyed with 5 or 10 wt.% of Ti wets many ceramics well but

these alloys are not useful brazes because their reservoir of Ti permits thick reaction-product layers to form and they are too stiff to accommodate the strains caused by the mismatched coefficients of thermal expansion of ceramic and metal components.

These difficulties led to attention being focused on the use of the Ag-28wt.% Cu alloy as a solvent because it is ductile and its lower melting temperature diminishes the severity of mismatched expansivities. It is also very important that the activity coefficient of Ti in Ag-Cu is higher than in Cu, and hence even a small concentration of Ti will have a high activity in the alloy. These considerations led to the development of Ag-28Cu-2Ti as a commercial active metal braze alloy that could be used with a wide range of ceramics. The alloy is relatively soft and ductile and the diminished Ti reservoir means that thick, and fragile, reaction product layers are less readily formed. This slimming of the reaction product layer is also favoured by the lower melting temperatures of the Ag-Cu-Ti alloys. Recently, however, further developments have occurred to increase the activity of Ti in the alloys and hence decrease the concentration of Ti still more. This was achieved by the introduction of about 12wt.% of In which permitted the Ti concentration needed to achieve reliable wetting and strong tough bonding to be decreased to about 1wt.%.

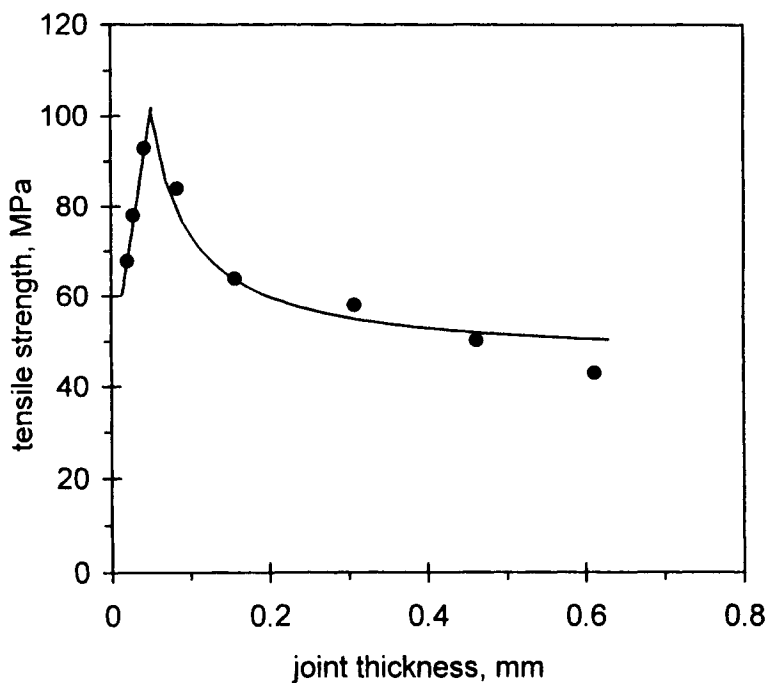
#### ***10.5.5 Influence of joint gaps***

The selection of a suitable joint gap is primarily influenced by considerations of wetting behaviour and the extent and rapidity of capillary flow but also affects the mechanical characteristics of the finished product. Thus the most extensive equilibrium vertical penetration is achieved with thin joints because the attractive force is a function of the perimeter length while the opposing gravitation drag is proportional to the cross-sectional area. Thin joints should also usually have the highest strengths because deformation of the generally weaker braze material is more constrained by the relatively rigid components. Thus Hill, (1950), used slipline field theory to predict that plastic deformation of the joint requires a stress  $S_J$  such that

$$S_J = 0.5S_Y \left( \frac{w}{d} + 3 \right) \quad (10.5)$$

where  $S_Y$  is the yield stress of the unconstrained braze,  $w$  is the joint width or length and  $d$  is its thickness. Thus joint strengths should be high if  $w/d$  is large even though the unconstrained braze yields readily.

The enhancement of joint strength at room and elevated temperatures as the separation of the components is decreased has been observed with both metal-ceramic and metal-metal systems and data for a Ag brazed steel system are presented in Figure 10.11. The right hand branch of the curve in the figure was derived from equation (10.5) with  $w$  equal to 0.18 mm and an assumed value of 30.7 MPa for  $S_Y$  and fits the experimental data reasonably well. Extrapolation of the data lead to the expectation that the joint will be as strong as the steel when the gap is 0.007 mm or less but the most notable feature of the figure is the peaking of the joint strength at a value of about 105 MPa when the gap is about 0.06 mm. The weakening of the joint as the gap becomes even thinner is due to technical reasons rather than a failure of slipline field theory. It requires exceptional care to machine components to very precise dimensions so that the resultant capillary gaps are extremely narrow and of uniform width. Even if this is achieved, incomplete filling of the joints may occur because of the difficulty of sweeping oxide and flux debris out of very narrow gaps as the braze penetrates.



**Figure 10.11.** The room-temperature tensile strengths of stainless steel joints brazed with a fluxed Ag-Cu-Zn-Cd alloy. After (Udin et al. 1954).

Narrowing the joint gap affects not only strength but toughness characteristics. Thus both the toughness of low alloy steel samples brazed with Cu and the fracture energy of  $\text{Al}_2\text{O}_3$  samples bonded with Au increased as the joint gap was widened, (Baker and Kavishe 1987, Reimanis et al. 1991). Therefore, while the thinnest filled joints may be the strongest, they can also have the greatest probability of failing prematurely because of easy crack propagation. It is interesting to therefore note that the maximum recommended joint gaps quoted in Table 10.3 for Ag and other braze families of 125-250 microns are significantly larger than the 60 microns suggested by the peak strength for Ag-brazed stainless steel in Figure 10.11.

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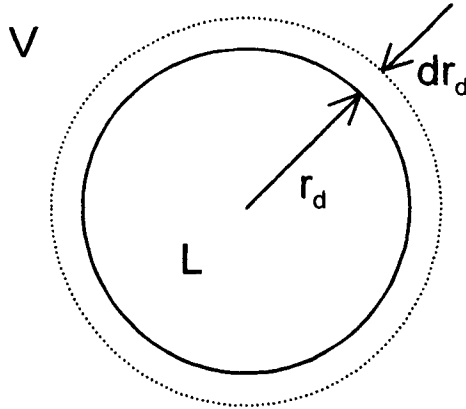
## Appendix A

### The Laplace equation

Consider a spherical liquid (L) drop of radius  $r_d$  in a vapour V. The volume of this drop is increased slowly, for instance by using a syringe to inject fresh liquid inside the drop (Figure A.1). The increase of drop radius from  $r_d$  to  $r_d + dr_d$  leads to an increase of the surface energy of the system equal to  $d(4\pi r_d^2 \sigma_{LV}) = 8\pi r_d \sigma_{LV} dr_d$ . If  $P_L$  is the pressure inside the drop and  $P_V$  the pressure in the vapour, the increase of  $r_d$  is associated with mechanical work to displace the surface by a distance  $dr_d$ , i.e.  $(P_L - P_V)4\pi r_d^2 dr_d$ . Equating the two amounts of work yields:

$$P_L - P_V = \frac{2\sigma_{LV}}{r_d} \quad (\text{A.1})$$

In the general case of a surface with a curvature  $R_1^{-1} + R_2^{-1}$  where  $R_1$  and  $R_2$  are the principal radii (see Figure 1.8), equation (A.1) remains valid if  $2/r_d$  is replaced by  $R_1^{-1} + R_2^{-1}$ .



**Figure A.1.** Displacement of a liquid surface allowing derivation of the Laplace equation.



## Appendix B

### Free energy of formation of a meniscus on a vertical plate in the gravitational field

During the formation of a meniscus of height  $z^*$  (Figure 1.9) and for a triple line of unit length, the free energy change  $\Delta F_{s,l}$  resulting from the substitution of a S/V surface by a S/L interface is:

$$\Delta F_{s,l} = z^*(\sigma_{SL} - \sigma_{SV}) \quad (B.1)$$

The meniscus rise  $z^*$  can be related to the instantaneous contact angle  $\theta$  by means of the Laplace equation (1.20) relating the pressure difference across a curved surface at point Q to the curvature. The pressure inside the liquid is higher than that in the vapour phase for the configuration shown in Figure 1.8, but the opposite occurs in the case of a wetting liquid on a vertical plate (Figure 1.9.a) i.e.,  $P_L(z) < P_V(z)$ . Moreover, because of the cylindrical symmetry,  $1/R_2 \rightarrow 0$ , so

$$P_L(z) - P_V(z) = \frac{\sigma_{LV}}{R_1} \quad (B.2)$$

and for the concave liquid surface in Figure 1.9.a,  $R_1$  is negative. Since

$$P_L(z=0) - P_V(z=0) = 0 \quad (B.3)$$

if the differences in vapour pressure with  $z$  are neglected,  $P_V(z=0) = P_V(z)$ , then:

$$P_L(z) - P_L(z=0) = \frac{\sigma_{LV}}{R_1} \quad (B.4)$$

This difference is equal to the hydrostatic pressure of a column of height  $z$ . Accordingly,

$$\frac{\sigma_{LV}}{R_1} = -\rho g z \quad (B.5)$$

where  $\rho$  is the liquid density and  $g$  the acceleration due to gravity. The calculation of the radius of curvature at any point on the L/V surface and at the triple line leads to (Neumann and Good 1972):

$$z^* = \pm \left( \frac{2\sigma_{LV}}{\rho g} \right)^{1/2} (1 - \sin \theta)^{1/2} = \pm l_c (1 - \sin \theta)^{1/2} \quad (\text{B.6})$$

where a positive value of  $z^*$  corresponds to  $0 \leq \theta \leq 90^\circ$  and a negative value to  $90 \leq \theta \leq 180^\circ$  and  $l_c = (2\sigma_{LV}/(\rho g))^{1/2}$ . Substituting this expression for  $z^*$ , equation (B.1) becomes:

$$\Delta F_{s,1} = \pm (\sigma_{SL} - \sigma_{SV}) l_c (1 - \sin \theta)^{1/2} \quad (\text{B.7})$$

The term  $\Delta F_{s,2}$  accounts for the increase in the L/V area during meniscus formation and for a plate of unit width this can be related to the increase  $\Delta l$  in the length of the L/V line:

$$\Delta F_{s,2} = \sigma_{LV} \Delta l \quad (\text{B.8})$$

with:

$$\Delta l = \int_{x=0}^{\infty} (ds - dx) \quad (\text{B.9})$$

where the increment of L/V length,  $ds$ , is such that:

$$ds^2 = dx^2 + dz^2. \quad (\text{B.10})$$

$\Delta l$  can be calculated by introducing equation (B.10) into equation (B.9) to obtain:

$$\Delta F_{s,2} = \sigma_{LV} l_c [2^{1/2} - (1 + \sin \theta)^{1/2}] \quad (\text{B.11})$$

The variation of the potential energy  $\Delta F_b$  can be calculated by considering a small column of liquid of rectangular cross section  $l \cdot dx$  (we recall that the liquid column in the  $y$ -axis is of unit length). The column is composed of successive increments of volume  $l \cdot dx \cdot dz$ . The work done in lifting each of these elements from

$z = 0$  to  $z$  is  $\rho \cdot g \cdot z \cdot dx \cdot dz$ . Integrating first over all the elements of the column and then over all the columns yields:

$$\Delta F_b = \frac{\rho g}{2} \int_{x=0}^{\infty} z^2 dx \quad (\text{B.12})$$

and then one gets:

$$\Delta F_b = \frac{\sigma_{LV} l_c}{3} [(2 - \sin \theta)(1 + \sin \theta)^{1/2} - 2^{1/2}] \quad (\text{B.13})$$

By combining equations (B.7), (B.11) and (B.13), one obtains the expression (1.21) for the total free energy change (Neumann and Good 1972).

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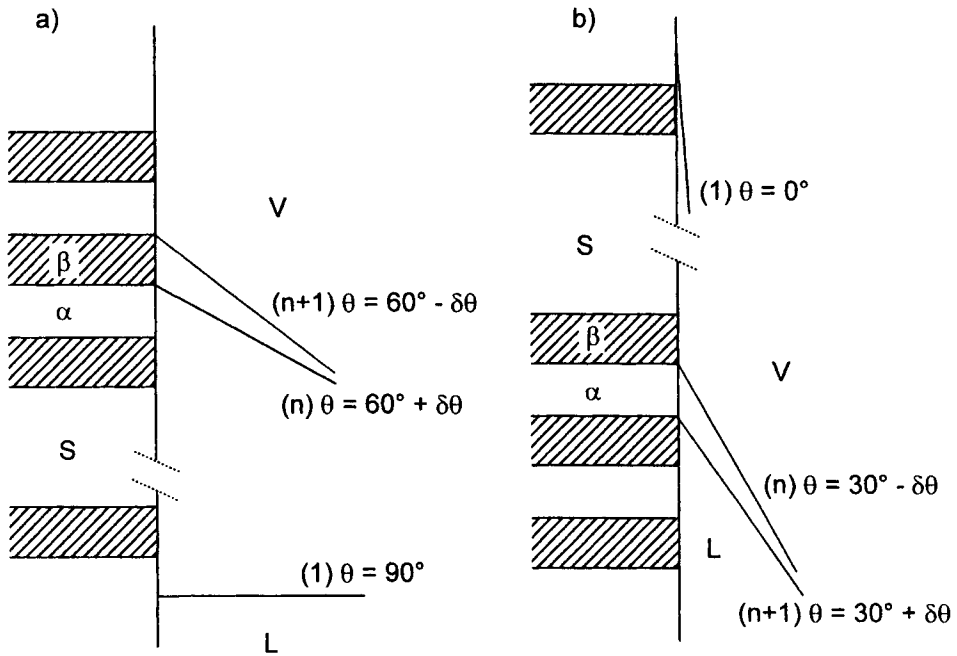
Neumann, A. W. and Good, R. J. (1972) *J. Colloid and Interface Science*, **38**, 341

## Appendix C

### Contact angle hysteresis for heterogeneous solid surfaces

Consider a composite solid consisting of alternate strips parallel to the triple line of  $\alpha$  and  $\beta$  phases with contact angles  $\theta^\alpha = 60^\circ$  and  $\theta^\beta = 30^\circ$ . If the initial position (1) of TL corresponds to a macroscopic contact angle  $\theta_M = 90^\circ$  (horizontal surface of the liquid in Figure C.1.a), the movement of TL from this position up to the position  $n$ , corresponding to a line of separation from  $\alpha$  to  $\beta$  with  $\theta_{(n)} = 60^\circ + \delta\theta$  ( $\delta\theta > 0$ ), will occur spontaneously. Then, TL contacts a  $\beta$  phase with an intrinsic contact angle  $\theta^\beta$  lower than  $\theta_{(n)}$ . Thus, displacement of TL over this  $\beta$  strip up to the position  $(n + 1)$  will also be spontaneous. However, at this position, the contact angle is now  $\theta_{(n+1)} = 60^\circ - \delta\theta$  which is lower than the intrinsic contact angle  $\theta^\alpha$  of the next adjacent  $\alpha$  strip. As a consequence, TL can be pinned in this position, leading to equation (1.42.a) ( $\theta_a(\max) = \theta^\alpha$ ). In practice, TL can move further by jumping over the least wetted  $\alpha$  strips and the final position will depend on the vibrational energy of the system and the strip width. As a result, the observed contact angle will lie between  $\theta_a(\max)$  and the contact angle corresponding to the stable equilibrium for a heterogeneous surface i.e.,  $\theta_C$  (equation (1.41)).

Similarly, if we consider an initial position (1) of TL with  $\theta_M \cong 0^\circ$  (Figure C.1.b), the displacement of TL is spontaneous until it reaches a line of separation from  $\alpha$  to  $\beta$  (position  $(n + 1)$ ) with  $\theta_{(n+1)} = 30^\circ + \delta\theta$ . As the next adjacent  $\beta$  strip has an intrinsic contact angle  $\theta^\beta$  lower than  $\theta_{(n+1)}$ ,  $\theta_M$  can increase no more and TL is blocked in position  $(n+1)$ , a situation described by equation (1.42.b).



**Figure C.1.** Advancing (a) and receding (b) contact angles associated with TL positions  $(n + 1)$  on heterogeneous surfaces with  $\alpha$  and  $\beta$  strips parallel to the triple line ( $\theta^\alpha = 60^\circ$ ,  $\theta^\beta = 30^\circ$ ).

## Appendix D

### Estimation of the mass of a sessile drop needed for an optimised $\sigma_{LV}$ measurement

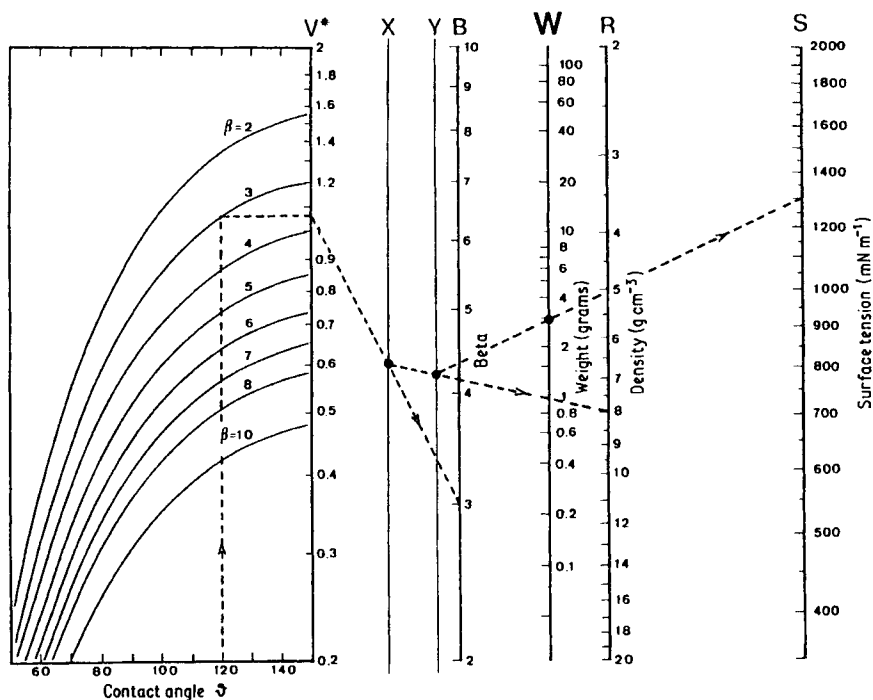
As shown in (Sangiorgi et al. 1982), a value of  $\beta > 2$  (see equation (3.8)) is needed to obtain a high-accuracy measurement of  $\sigma_{LV}$ . This requirement can be satisfied using a drop with an optimised mass  $m_d$ . To estimate  $m_d$ , we need to link it to  $\beta$  through the values of the density  $\rho$ ,  $\sigma_{LV}$ ,  $\theta$  and the drop volume  $v$ :

$$m_d = v^*(\rho g)^{-1/2} \sigma_{LV}^{3/2} \beta^{3/2} \quad (D.1)$$

with  $v^* = v/b^3$  where  $b$  is the curvature radius at the drop apex. This equation is represented in nomographic form in Figure D.1. The procedure needs the approximate knowledge of the quantities  $\theta$ ,  $\rho$  and  $\sigma_{LV}$ . Take for example a metal with  $\rho = 8 \text{ g.cm}^{-3}$ ,  $\sigma_{LV} = 1300 \text{ mJ.m}^{-2}$  and  $\theta = 120^\circ$ . If the desirable value is  $\beta = 3$ ,  $m_d = 3\text{g}$ .

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**Figure D.1.** Nomographic chart for determining the optimum drop mass (noted W on the figure) from a given set of  $\sigma_{LV}$  (noted S),  $\rho$  (noted R),  $\theta$  and  $\beta$  (noted B) values. Reprinted from (Sangiorgi et al. 1982) [2] with kind permission of the authors.

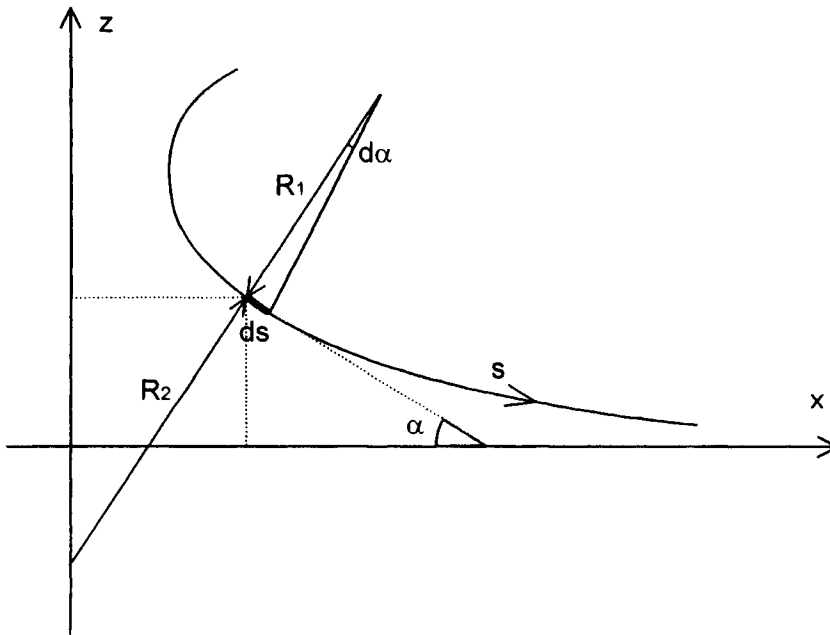
## Appendix E

### Wetting balance : the case of cylindrical solids

The geometrical quantities used to describe the profile of a meniscus formed on a cylinder of radius  $r_0$  are plotted on Figure E.1. Using the cartesian coordinates, the Laplace equation becomes:

$$\frac{d(x \sin \alpha)}{dx} = - \frac{\rho g}{\gamma_{LV}} z x \quad (\text{E.1})$$

where  $\rho$  is the liquid density and  $g$  the acceleration due to gravity.

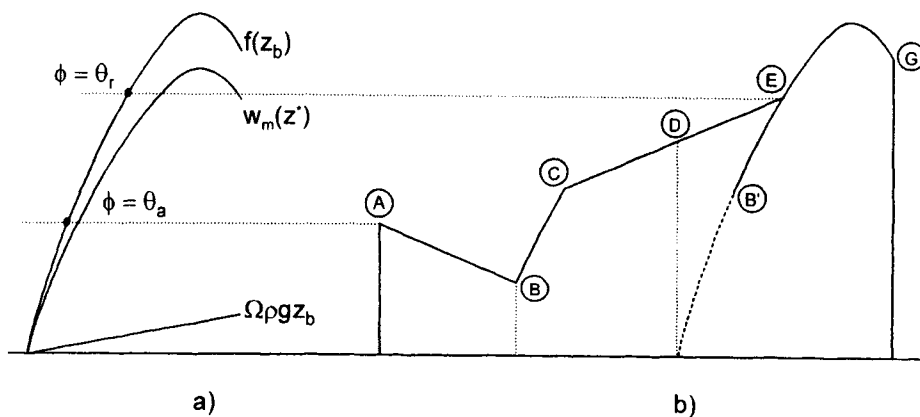


**Figure E.1.** Geometrical quantities used to describe the profile of a meniscus formed around a circular and constant section cylinder. From (Rivollet et al. 1990) [2].

The coordinates of the joining point of the liquid on the solid are  $z^*$ ,  $x_0 = r_0$  and  $\alpha_0 = 90^\circ - \phi$  where  $\phi$  is the joining angle defined in Figure 3.16. Hartland and



Hartley (1976) solved the differential equation (E.1) numerically to calculate  $\alpha_0$  for each value of  $z^*$  and to obtain a theoretical curve of the weight of the meniscus  $w_m$  as a function of  $z^*$  (for  $x_0 = r_0$  and a given value of the liquid surface tension  $\gamma_{LV}$ ). Then, as shown on Figure E.2.a in the wetting case, the  $f(z_b)$  curve, which represents the variations of the force  $f$  exerted on the cylinder when the meniscus is connected to the solid base of area  $\Omega$  ( $z^* = z_b$  where  $z_b$  is the coordinate of the solid base), is obtained simply by adding  $w_m(z^*)$  to the buoyancy contribution  $\Omega\rho g z_b$ . Furthermore, joining the part B-C of the experimental curve (Figure E.2.b) to the part E-G, a new curve B'-G is obtained, the origin of which being located at the vertical of point D corresponding to  $z_b = 0$ . The value of  $\gamma_{LV}$  is then determined by fitting the theoretical  $f(z_b)$  curve to the experimental one (Rivollet 1986).



**Figure E.2.** (a) Construction of a theoretical curve  $f(z_b)$  and (b) comparison with the experimental curve B'-G in the wetting case (see Figure 3.18).

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## Appendix F

### Surface energies of cubic diamond structure compounds

The surface energy of dense-packed faces (111) of Si and diamond will be estimated taking as a reference value that for Ge at its melting point and applying the expression (1.15) of  $\sigma_{SV}$  established in the framework of the simple broken bond model of Skapski. As a first approximation, the effect of temperature on  $\sigma_{SV}$  will be neglected.

The surface energy of Ge is calculated by the Young equation  $\sigma_{SV} = \sigma_{LV} \cos \theta + \sigma_{SL}$  taking  $\sigma_{LV} = 587 \text{ mJ/m}^2$  (Table 4.1) and  $\sigma_{SL} = 251 \text{ mJ/m}^2$  (Eustathopoulos 1983). The contact angle of molten Ge on (111) face of Ge is  $15^\circ$  (Bardsley et al. 1974), which leads to  $\sigma_{SV}^{\text{Ge}} = 818 \text{ mJ/m}^2$  at 1210K.

According to expression (1.15),  $\sigma_{SV}$  is proportional to the sublimation energy  $L_s$  of the crystal. The atomic area  $\omega$  can be calculated from the molar volume  $v_m$  as follows:

$$\omega = f_c \left( \frac{v_m}{N_a} \right)^{2/3} \quad (\text{F.1})$$

where  $f_c$  is a compacity factor depending on the type of the lattice and on the surface plane (Skapski 1948). Parameters  $f_c$  (equation (F.1)) and  $m_l$  (equation (1.15)) are the same for the faces (111) of Ge and Si, so that

$$\sigma_{SV}^{\text{Si}} = \sigma_{SV}^{\text{Ge}} \frac{L_s^{\text{Si}}}{L_s^{\text{Ge}}} \left( \frac{v_m^{\text{Ge}}}{v_m^{\text{Si}}} \right)^{2/3} \quad (\text{F.2})$$

From sublimation energy data (Hultgren 1973) and molar volumes (Lucas 1984),  $\sigma_{SV}^{\text{Si}} = 1080 \text{ mJ/m}^2$ . Similarly, the value  $\sigma_{SV} = 3980 \text{ mJ/m}^2$  is calculated for a face (111) of diamond. This very high value compared to  $\sigma_{SV}^{\text{Si}}$  is due to two factors: (i) the carbon-carbon bond energy is higher by a factor 1.6 than the Si-Si bond energy and (ii) the number of atoms per unit area on diamond surface i.e., of atoms having broken bonds, is higher by a factor 2.3 than that on Si surface.

Although a rigorous evaluation of the uncertainty on the estimated values of  $\sigma_{SV}$  for Si and diamond cannot be made, it is expected to be less than 50%.

The (111) faces of cubic SiC (as well as basal planes of hexagonal SiC) are polar i.e., can terminate either as a C layer or a Si layer (see Section 7.1.1). However, following the nearest-neighbour model of Skapski, the surface energy of the two faces is the same, and lies between those for Si and diamond. The value of the surface energy of a (111) face of cubic SiC can be estimated from data for Ge using an equation analogous to (F.2). Knowing that  $\Delta H_f^{SiC} \cong (L_s^{Si} + L_s^C - 2L_s^{SiC})$ , the sublimation energy  $L_s^{SiC}$  is first calculated from the experimental value of enthalpy of formation of SiC,  $\Delta H_f^{SiC}$ , and from sublimation energies of Si,  $L_s^{Si}$ , and diamond,  $L_s^C$ . Then equation (F.2) yields  $\sigma_{SV}^{SiC} = 1450 \text{ mJ/m}^2$ . As the atomic structure of the (0001) face of hexagonal  $\alpha$ -SiC is very similar to that of the (111) face of cubic SiC, the calculated value of  $\sigma_{SV}^{SiC}$  can be used for both faces. The value of  $1450 \text{ mJ/m}^2$  is lower but close to the value of  $1767 \text{ mJ/m}^2$  estimated by Takai et al. (1985) using Monte-Carlo simulations for a relaxed (111) face of cubic SiC.

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## Appendix G

### Enthalpy of mixing of binary liquid alloys

Table G.1 reproduces values calculated by Miedema's model (Niessen et al. 1983) for the partial enthalpy of solution at infinite dilution of a liquid metal solute  $i$  in a liquid metal solvent  $j$ ,  $\overline{\Delta H}_{i(j)}^\infty$  (in kJ/mole). For a  $i$ - $j$  alloy, the regular solution parameter  $\lambda$  can be approximated by  $[\overline{\Delta H}_{i(j)}^\infty + \overline{\Delta H}_{j(i)}^\infty]/2$ .

**Table G.1.** Enthalpy of solution (in kJ/mole) at infinite dilution (Niessen et al. 1983).

solvent→ ↓ solute	Ag	Al	Au	Bi	Cd	Cr	Cu	Fe	Ga	Ge	In	Mn
Ag	0	-18	-21	6	-8	119	10	123	-20	-21	-5	57
Al	-17	0	-80	31	12	-43	-34	-48	3	-8	24	-83
Au	-23	-92	0	6	-43	-1	-42	37	-79	-39	-40	-53
Bi	9	48	9	0	5	136	35	146	20	24	-6	16
Cd	-9	14	-41	4	0	81	3	77	3	-7	2	10
Cr	98	-36	-1	74	60	0	51	-6	-2	-23	66	9
Cu	8	-28	-30	19	2	49	0	50	-19	-24	8	15
Fe	102	-41	28	80	58	-6	53	0	-6	-12	63	1
Ga	-21	4	-75	14	3	-3	-26	-8	0	-12	10	-60
Ge	-21	-8	-36	16	-6	-28	-30	-15	-11	0	-3	-84
In	-7	31	-45	-5	2	102	12	95	12	-4	0	13
Mn	46	-70	-39	9	7	8	15	1	-45	-69	8	0
Mo	146	-20	13	123	103	2	82	-9	25	-3	114	22
Na	1	58	-52	-69	-12	329	74	276	21	-39	-21	235
Ni	56	-82	25	31	7	-27	14	-6	-53	-41	5	-33
Pb	13	50	10	0	7	153	41	160	22	23	-3	38
Si	-13	-9	-48	47	13	-87	-40	-75	-1	9	23	-120
Sn	-14	19	-46	5	-1	53	-6	56	4	0	-1	-37
Ta	61	-78	-125	32	35	-30	9	-67	-37	-101	48	-17
Ti	-6	-118	-180	-45	-28	-33	-40	-74	-88	-157	-19	-36
U	1	-132	-177	-53	-33	-13	-33	-53	-101	-170	-27	-25
V	63	-61	-69	33	32	-8	21	-29	-29	-70	40	-3
W	172	-8	44	151	124	4	101	0	41	20	135	28
Zr	-87	-189	-302	-140	-103	-58	-110	-118	-163	-260	-94	-74

Table G.1. (continued)

solvent→ ↓ solute	Mo	Na	Ni	Pb	Si	Sn	Ta	Ti	U	V	W	Zr
Ag	150	1	68	9	-14	-10	60	-6	1	73	171	-78
Al	-20	46	-96	34	-9	14	-75	-119	-114	-69	-8	-164
Au	14	-52	33	8	-57	-38	-135	-203	-171	-87	48	-294
Bi	191	-80	58	0	77	6	47	-69	-69	57	229	-184
Cd	118	-11	9	5	16	-1	39	-33	-34	42	136	-106
Cr	1	220	-27	86	-77	32	-24	-27	-9	-8	4	-41
Cu	67	49	14	23	-34	-3	7	-33	-23	19	80	-78
Fe	-7	195	-6	91	-67	34	-54	-62	-38	-28	0	-85
Ga	28	18	-69	16	-2	3	-40	-98	-96	-36	44	-156
Ge	-3	-31	-51	16	10	0	-99	-159	-148	-80	20	-225
In	148	-20	8	-3	32	-1	61	-25	-31	58	171	-107
Mn	18	152	-33	21	-106	-22	-14	-30	-18	-3	23	-52
Mo	0	311	-32	139	-76	70	-19	-14	8	0	-1	-23
Na	389	0	139	-64	23	-31	392	312	274	342	391	257
Ni	-27	100	0	40	-86	-13	-105	-126	-98	-69	-11	-165
Pb	207	-70	73	0	75	7	73	-38	-40	81	242	-147
Si	-72	18	-98	48	0	21	-149	-190	-175	-128	-54	-239
Sn	97	-32	-21	6	30	0	-13	-101	-99	-4	125	-188
Ta	-20	302	-133	51	-165	-10	0	6	12	-4	-30	10
Ti	-15	225	-154	-26	-202	-74	5	0	-1	-7	-23	-1
U	9	232	-139	-32	-217	-84	14	-1	0	4	5	-13
V	0	231	-75	49	-121	-3	-4	-6	3	0	-3	-13
W	-1	326	-14	166	-58	92	-29	-23	4	-3	0	-34
Zr	-27	208	-236	-117	-299	-161	12	-1	-13	-17	-39	0

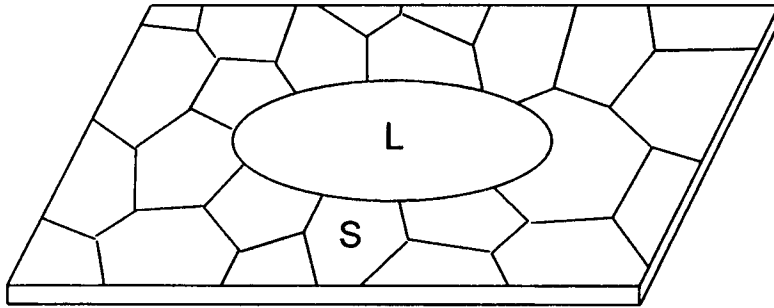
## REFERENCE

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## Appendix H

### Secondary wetting

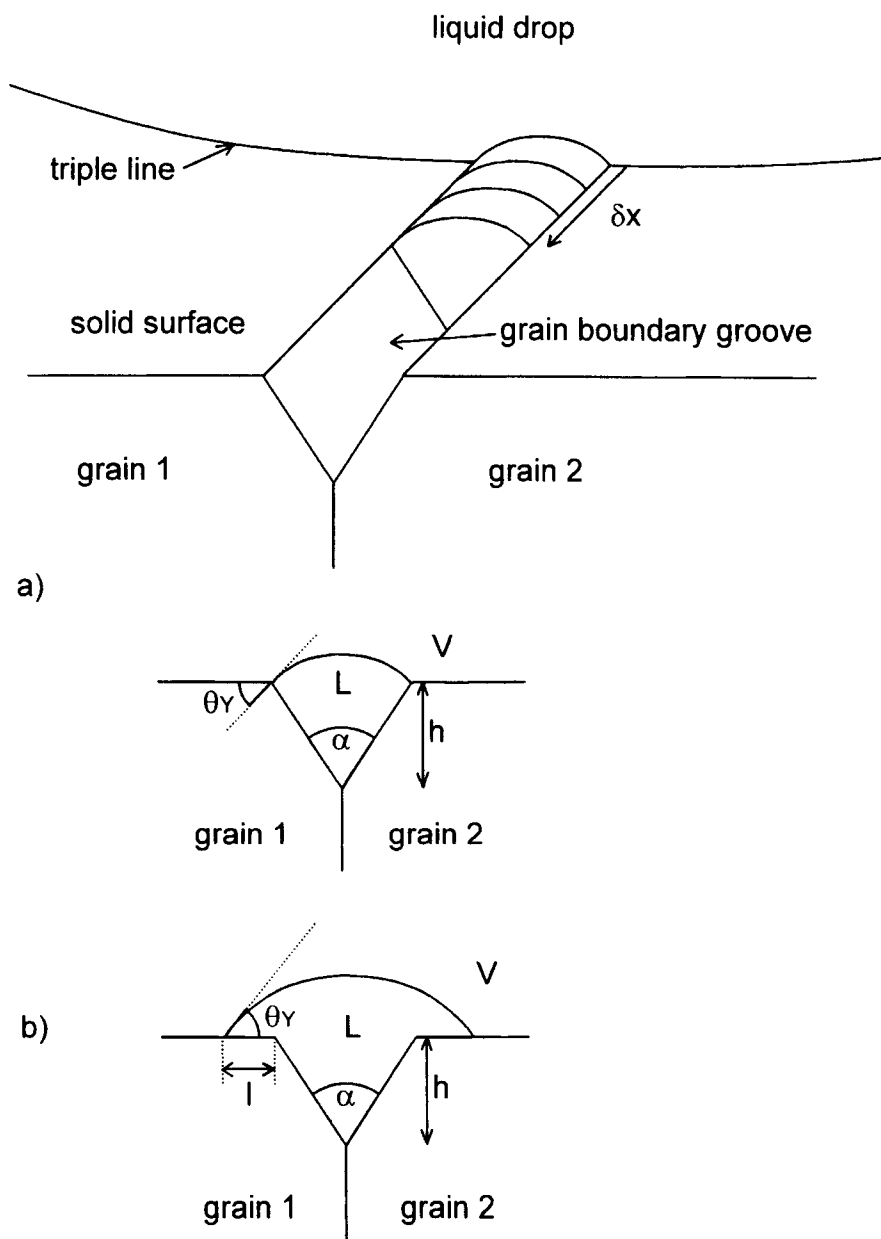
Consider a drop of non-reactive liquid metal on a smooth surface of a polycrystalline metallic solid (Figure H.1). After a first fast spreading, a much slower spreading process is often observed, called “secondary wetting” (Bailey and Watkins 1951-52, Sharps et al. 1981, Weirauch and Krafick 1996, Lequeux et al. 1998) that is generally attributed to enhancement of wetting by grain boundaries. This can be due to an increase of surface roughness (leading to a better wetting for systems with  $\theta_Y \ll 90^\circ$ , according to the Wenzel equation (1.35)) produced by grain-boundary grooves formed either at the free S/V surface or at the S/L interface (see Figure 4.8).



**Figure H.1.** Sessile drop on a polycrystalline solid.

Grooves formed at the S/V surface create open “capillaries” on the solid surface along grain boundaries ahead of the triple line which can be infiltrated by the liquid (Figure H.2.a). The change in interfacial free energy of the system for a small linear displacement  $\delta x$  of the liquid along the groove, causing a replacement of a S/V surface by an equal area of S/L interface and by a L/V surface of area  $(2h \sin(\alpha/2) \theta_Y \delta x) / (\cos(\alpha/2) \sin(\theta_Y))$  (Lorrain 1996) is:

$$\delta F_s = \frac{2h}{\cos(\alpha/2)} \left[ \frac{\sin(\alpha/2)}{\sin(\theta_Y)} \theta_Y \cdot \sigma_{LV} + \sigma_{SL} - \sigma_{SV} \right] \delta x \quad (\text{H.1})$$

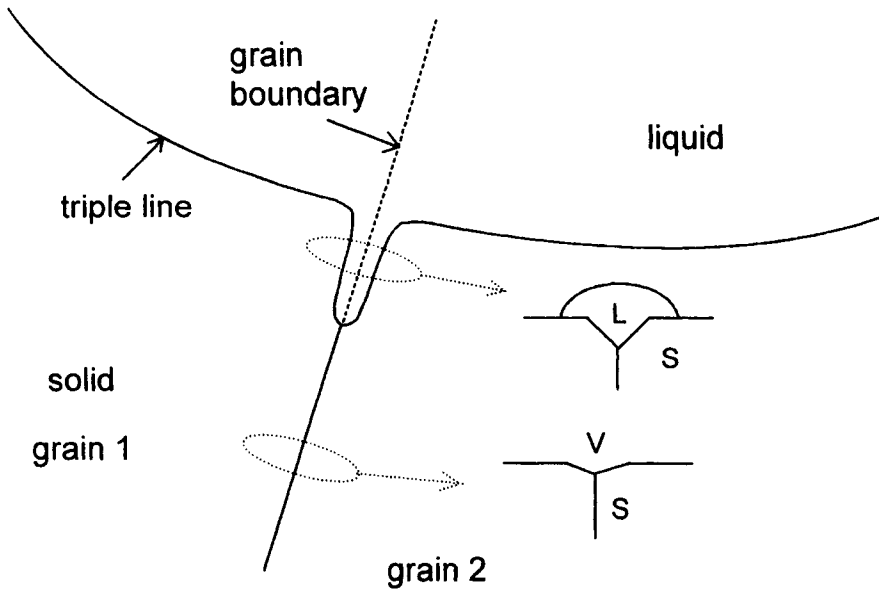


**Figure H.2.** a) Infiltration of pre-existing grain boundary grooves at S/V surface. b) Extension of the liquid on both sides of the groove.

Introducing the Young equation into (H.1) and setting  $d(\delta F_s)/d(\delta x) = 0$ , shows that infiltration is possible if the experimental dihedral angle is lower than the value  $\alpha^*$  given by:

$$\sin\left(\frac{\alpha^*}{2}\right) = \frac{\cos(\theta_Y) \sin(\theta_Y)}{\theta_Y} \quad (\text{H.2})$$

As  $0 \leq \alpha \leq 180^\circ$ , this equation cannot be verified for  $\theta_Y > 90^\circ$ , so that secondary wetting is not expected to occur for non-wetting liquids. For  $\theta_Y = 50^\circ$ ,  $\alpha^* = 69^\circ$  and for  $\theta_Y = 20^\circ$ ,  $\alpha^* = 134^\circ$ . Experimentally, the dihedral angles  $\psi$  formed on *thermal* grain boundary grooves are usually higher than  $150^\circ$  (see Table 4.4) so that this type of groove cannot affect wetting significantly. However, values of the dihedral angles  $\Phi$  formed at S/L interfaces lie between  $0$  and  $140^\circ$  (Eustathopoulos 1983) for different systems and temperatures, so the condition  $\Phi < \alpha^*$  may hold in many cases. Thus spreading on polycrystalline materials can continue by flow of liquid to fill grooves of grain boundaries that radiate from the nominal triple line (Figure H.3).



**Figure H.3.** Formation of a grain boundary groove filled by liquid ahead of the nominal triple line.



When the condition  $\Phi < \alpha^*$  is fulfilled, the liquid wets not only the groove but it also expands on the free solid surface on both sides of the groove to a distance  $l$  as shown on Figure H.2.b. The equilibrium value of  $l$  can be calculated by minimising the interfacial free energy of the system for a small lateral displacement  $\delta l$  of the liquid perpendicularly to the groove (Lorrain 1996):

$$l_{eq} = \frac{[\theta_Y \sin(\alpha/2) / \sin(\theta_Y)] - \cos(\theta_Y)}{\cos(\theta_Y) - [\theta_Y / \sin(\theta_Y)]} \frac{h}{\cos(\alpha/2)} \quad (H.3)$$

Thus  $l_{eq}$  depends not only on the contact angle,  $\theta_Y$ , and the dihedral angle,  $\alpha$ , but also on the groove depth,  $h$ . As this depth increases with time according to a power law  $h \approx t^{1/3}$  (see equation (1.33)), the width of the liquid cap supported by the groove increases too. At the nominal triple line, the liquid is partially in contact with a grain surface (whose contact angle  $\theta_1$  equals  $\theta_Y$ ) and partially with a liquid filled groove. As a liquid wets perfectly a liquid of the same nature, the local contact angle with the groove,  $\theta_2$ , is  $0^\circ$ . Therefore, the macroscopic contact angle, which is a combination of local contact angles  $\theta_1$  and  $\theta_2$  as given by Cassie's equation (1.41) derived for heterogeneous surfaces, will be  $\theta_C(t) < \theta_Y$  and will tend towards zero with increasing time as the liquid channels coalesce.

In the case of a liquid eutectic Ag-Cu alloy on a solid solution of Cu in equilibrium with the liquid, the contact angle measured on Cu substrates with very large grain size (1 cm) is  $\theta_Y \cong 19^\circ$  (Sharps et al. 1981). For this system  $\Phi = 0$  (Smith 1948) and  $\alpha^* = 136^\circ$ , so that the condition of infiltration of grain boundary grooves is fulfilled. For Cu substrates with small grain size (20  $\mu\text{m}$ ), Sharps et al. (1981) observed the formation of a network of liquid channels along grain boundary grooves ahead of the triple line, resulting in a macroscopic contact angle nearly equal to zero.

Conversely, in the Cu/W system for which Lorrain (1996) found a contact angle of  $50^\circ$  at  $1100^\circ\text{C}$ , secondary wetting was not observed, even after one hour at this temperature. Indeed, for this system, the experimental value of  $\Phi$  (see Table 4.4) is much higher than the value  $\alpha^* = 69^\circ$  calculated from equation (H.2) taking  $\theta_Y = 50^\circ$ .

The thermodynamic condition for secondary wetting described by equation (H.2) is expected to hold for many metal combinations and more seldomly for metal/ceramic couples. In practice, a detailed study of this phenomenon is difficult to perform because other phenomena can complicate the analysis. For example, dissolution of the solid in the liquid or diffusion of a component of the liquid in the solid could occur during prolonged experiments. In the last case, the liquid volume

decreases which leads to a change of the macroscopic contact angle from an advancing to a receding configuration.

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## Appendix I

### Evaluation of the work of adhesion of Ni on SiC

This evaluation will be made using experimental results for the work of immersion of non-reactive Ni-Si alloys on SiC (Section 7.1.1.1) using the atomistic model described in Section 6.5.1. According to this model, the slope of the  $\sigma_{SL}$  versus  $X_{Ni}$  curve for  $X_{Ni} \rightarrow 0$  is related to the adsorption energy of Ni at the Si/SiC interface,  $E_{Ni(Si)}^{\infty,SL}$ , by:

$$\left. \frac{d\sigma_{SL}}{dX_{Ni}} \right|_{X_{Ni} \rightarrow 0} = \frac{RT}{\Omega_m} \left( 1 - \exp - \left( \frac{E_{Ni(Si)}^{\infty,SL}}{RT} \right) \right) \quad (I.1)$$

with

$$\begin{aligned} E_{Ni(Si)}^{\infty,SL} &= -(W_a^{Ni} - W_a^{Si})\Omega_m + (\sigma_{LV}^{Ni} - \sigma_{LV}^{Si})\Omega_m - m_l\lambda \\ &= [(\sigma_{SL}^{Ni} - \sigma_{SV}) - (\sigma_{SL}^{Si} - \sigma_{SV})]\Omega_m - m_l\lambda = [W_i^{Ni} - W_i^{Si}]\Omega_m - m_l\lambda \end{aligned} \quad (I.2)$$

In this equation,  $\Omega_m$  is the molar surface area,  $m_l$  is a structural parameter defined in Section 1.1 (see Figure 1.3) and  $\lambda$  is the regular solution parameter of Ni-Si alloy defined by equation (4.3). From the slope of the  $\sigma_{SL}(X_{Ni})$  curve for  $X_{Ni} \rightarrow 0$ , the adsorption energy is found to be  $E_{Ni(Si)}^{\infty,SL} = -8.2$  kJ/mole. Thus, in equations (I.2), all the quantities are known (or can be easily estimated), except  $W_a^{Ni}$  and  $W_i^{Ni}$  which represent respectively the work of adhesion and the work of immersion of pure liquid Ni in metastable equilibrium with SiC (i.e., for a supposed non-reactive pure Ni/SiC system). The values deduced from equation (I.2) are  $W_a^{Ni} = 3.17$  J/m<sup>2</sup> and  $W_i^{Ni} = -1.35$  J/m<sup>2</sup> for pure Ni. They are reported in Figure 7.6 along with the corresponding value of contact angle.

# List of symbols

## Fundamental constants

$g$	acceleration due to gravity
$k$	Boltzmann constant
$N_a$	Avogadro's number
$R$	gas constant

## Abbreviations

$L$	liquid
$MPE$	multiphase equilibrium
$P$	reaction product
$S$	solid
$TL$	triple line
$V$	vapour
$2D(3D)$	two (three) dimensions

## Common symbols

$a_i$	thermodynamic activity of component $i$
$b$	radius of curvature at sessile drop apex
$C$	concentration
$d$	width of a parallel sided gap or joint
$D$	diffusion coefficient
$e$	thickness of reaction product at the solid/liquid interface
$E$	potential energy of a bulk atom
$E'$	potential energy of a surface atom
$E_b$	energy barrier
$E_c$	cohesion energy
$E_{diss}$	dissipated energy
$E_g$	gap energy
$E_p$	potential energy of a spreading drop
$E_v$	vibrational energy
$E_{i(j)}^{\infty, LV}$	adsorption energy at liquid/vapour surface of solute $i$ at infinite dilution in solvent $j$

$E_{i(j)}^{\infty,SL}$	adsorption energy at solid/liquid interface of solute i at infinite dilution in solvent j
f	force
$f_c$	compacity factor
$f_d$	driving force
$f^i$	surface fraction of phase i
$f_{in}$	inertial force
$f_v$	viscous force
F	free energy
$F_b$	free energy of bulk phase
$F_s$	surface free energy
G	Gibbs energy
$\Delta G_{f(i)}^0$	standard Gibbs energy of formation of compound i
$\overline{\Delta G_{i(j)}^{xs,\infty}}$	partial excess Gibbs energy of mixing at infinite dilution of a solute i in a solvent j
h	height of wetting ridge or depth of grain boundary groove
H	sessile drop height
$\Delta H_{f(i)}$	enthalpy of formation of compound i
$\Delta H_{f(i)}^0$	standard enthalpy of formation of compound i
$\overline{\Delta H_{i(j)}}$	partial enthalpy of mixing of component i in component j
$\overline{\Delta H_{i(j)}}^{\infty}$	partial enthalpy of mixing at infinite dilution of a solute i in a solvent j
$\Delta H_m$	enthalpy of mixing of an alloy
$K_1$	constant first used in equation (2.4)
$K_2$	constant in equation (2.20)
$K_D$	equilibrium constant of a dissolution reaction
$K_P$	equilibrium constant of reaction of formation of a new phase
l	distance
$l_c$	capillary length
$l_e$	equilibrium rise or depression of a liquid in a parallel sided gap
$L_e$	energy or heat of evaporation
$L_f$	length of a facet on a sawtooth surface
$L_m$	energy or heat of melting
$L_s$	energy or heat of sublimation
$m_1$	for a bulk atom, fraction of nearest neighbour lying in an adjacent plane
$m_2$	for a bulk atom, fraction of nearest neighbour lying in the same plane
$m_d$	mass of a drop
n	power term in equation (1.33)
n	coordination number of an oxygen atom dissolved in a metallic phase (equation (6.20))

$n_i$	number of moles of component $i$
$p$	perimeter
$P$	pressure
$P_c$	capillary pressure
$P_h$	hydrostatic pressure
$P_i$	partial pressure of species $i$
$P_{N_2}^d$	nitrogen partial pressure for dissociation of a nitride
$P_{O_2}$	oxygen partial pressure
$P_{O_2}^f$	oxygen partial pressure in the furnace atmosphere
$P_{O_2}^l$	equivalent oxygen partial pressure at a solid/liquid interface
$P_{O_2}^{d(MO)}$	oxygen partial pressure for decomposition of oxide MO
$P_{O_2}^{ox(M)}$	oxygen partial pressure for oxidation of metal M
$P_{sat}$	partial pressure at saturation of a species
$r$	radius
$r_d$	radius of a spherical drop
$R$	base radius of a sessile drop
$R_0$	initial sessile drop base radius
$R_1, R_2$	principal radii of curvature of a surface
$R_a$	average height of asperities on a surface
$R_F$	final or stationary drop base radius
$s$	length of line on a liquid surface
$s_r$	roughness parameter of Wenzel (equation (1.35))
$S_J$	joint strength
$S_Y$	yield strength
$S_s$	surface excess entropy
$\overline{\Delta S}_{i(j)}^{xs,\infty}$	partial excess entropy of mixing of solute $i$ at infinite dilution in solvent $j$
$t$	time
$t_0$	time corresponding to the initial contact angle $\theta_0$
$t_F$	time needed to reach a constant drop base radius $R_F$
$T$	temperature
$T_F$	melting temperature
$u$	fluid velocity
$U$	triple line velocity
$U_0$	initial triple line velocity
$U_r$	rate of reaction
$v$	volume
$v_m$	molar volume
$w$	length of a parallel sided joint

$w_m$	weight of a meniscus
$W_a$	work of adhesion
$W_a^0$	work of adhesion in the absence of adsorption on the solid
$W_c$	work of cohesion
$W_d$	work of capillary forces (equation (2.2))
$W_i$	work of immersion
$W_s$	work of spreading
$x$	horizontal coordinate
$x_{90}$	equatorial radius of a sessile drop
$X_i$	molar fraction of component i
$X_i^j$	molar fraction of component i in phase j
$X_i^I$	molar fraction of component i at the solid/liquid interface
$X_i^{eq}$	molar fraction of component i for a reaction at equilibrium
$X_i^J$	molar fraction of component i at point J corresponding to a three phase equilibrium (figure 7.2)
$X_O^S$	molar fraction of oxygen at the liquid surface
$Y_i$	molar fraction of component i adsorbed at surface or interface monolayer
$Y_i$	molar fraction of component i around oxygen atoms dissolved in an alloy i-j (equation (6.19))
$z$	vertical coordinate
$z_{90}$	equator-apex height of a sessile drop
$z^*$	meniscus height
$z_{max}^*$	maximum (or equilibrium) meniscus height
$z_b$	depth to which the base of a solid is immersed in a liquid bath
$z_c$	equilibrium rise or depression of a liquid in a circular cross section capillary
$Z$	coordination number i.e. number of nearest neighbour atoms
$\alpha$	angle
$\alpha$	reduction of the metallic bond energy due to oxygen (equation (6.20))
$\alpha$	evaporation coefficient
$\beta$	slope of surface asperities
$\beta$	inclination of a surface to the vertical
$\beta$	parameter in equation (3.7)
$\varepsilon$	elastic strain
$\varepsilon_{ij}$	bond energy between i and j atoms
$\varepsilon_O^I$	Wagner interaction parameter between oxygen and solute i
$\phi$	joining angle of a meniscus on a solid surface
$\Phi$	dihedral angle of grain boundary groove at solid/liquid interface

$\Phi_i$	dihedral angles at a triple line ( $i = 1, 2, 3$ )
$\Phi_O$	flow of oxygen
$\gamma_i$	activity coefficient of species $i$
$\gamma_i^\infty$	activity coefficient of species $i$ at infinite dilution in a solvent
$\gamma_{LV}$	liquid/vapour surface tension
$\gamma_{SV}$	solid/vapour surface tension (equation (1.3))
$\Gamma_i$	absolute adsorption of species $i$
$\Gamma_i^j$	relative adsorption of species $i$ with respect to species $j$
$\eta$	dynamic viscosity
$\phi$	angle between the normal to the liquid surface and the axis of rotation of a sessile drop
$\kappa$	curvature
$\lambda$	regular solution parameter
$\lambda_{i-j}$	regular solution parameter of a binary $i$ - $j$ solution
$\lambda_a$	average wavelength of asperities on a surface
$\Lambda$	Gibbs-Thomson parameter
$\mu$	chemical potential
$\theta$	contact angle
$\theta_0$	initial contact angle or contact angle in the absence of reaction (equation (2.14))
$\theta_a$	advancing contact angle
$\theta_{app}$	apparent contact angle
$\theta_C$	Cassie contact angle on a chemically heterogeneous surface
$\theta_{eq}$	equilibrium contact angle
$\theta_{equiv}$	equivalent contact angle of a small solid drop
$\theta_F$	final or stationary contact angle
$\theta^i$	contact angle on solid phase $i$
$\theta_i$	contact angle of liquid phase $i$
$\theta_M$	macroscopic contact angle
$\theta_P$	equilibrium contact angle on a reaction product
$\theta_r$	receding contact angle
$\theta_W$	Wenzel contact angle on a rough surface
$\theta_Y$	Young contact angle
$\rho$	mass density
$\sigma_{LV}$	liquid/vapour surface energy
$\sigma'_{LV}$	temperature coefficient of liquid/vapour surface energy
$\sigma_{SV}$	solid/vapour surface energy
$\sigma_{SV}^d$	van der Waals component of solid/vapour surface energy
$\sigma_{SV}^0$	solid/vapour surface energy in the absence of adsorption or reaction



$\sigma_{\text{SL}}$	solid/liquid interfacial energy
$\sigma_{\text{SL}}^0$	solid/liquid interfacial energy in the absence of reaction
$\sigma_{\text{gb}}$	grain boundary energy
$\tau$	specific excess free energy of triple line
$\omega$	atomic surface area
$\Omega$	surface area
$\Omega$	base area of solid in wetting balance test
$\Omega_{\text{m}}$	molar surface area
$\psi$	dihedral angle of grain boundary groove at solid/vapour surface
$\psi^0$	dihedral angle of grain boundary groove at adsorption free solid/vapour surface

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